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# A three-dimensional study on premixed flame propagation in narrow channels considering hydrodynamic and thermodiffusive instabilities

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## Abstract

In numerical studies of quasi-2D problems, such as laminar flame propagation through a slit, the quasi-2D assumption is commonly applied to simplify the problem. However, the impact of the third dimension (in the thickness between walls) can be significant due to strong curvature. The intrinsic Darrieus-Landau instability, the Saffman-Taylor instability, and the thermodiffusive instability lead to curved flame fronts in both the transverse and normal directions and radically change the global flame speed. This study investigates the interaction of these instabilities and their impact on premixed flames freely propagating in narrow channels. Two lean fuel-air mixtures are considered: one with unity Lewis number  $Le = 1$  and another with  $Le = 0.5$ . A single-step Arrhenius-type reaction is used for combustion modeling. Joulin Sivashinsky's model [1], termed the 2D+ model, is implemented to capture the confinement effect due to walls. By comparing 3D Direct Numerical Simulations (DNS) and 2D simulations at unity  $Le$ , we find that the 2D+ model accurately reproduces confinement effects for channel width  $h$  up to  $3.6\delta_T$  ( $\delta_T$ : thermal flame thickness), extending the validity of Darcy's law.

However, for larger  $h$ , interactions between flame curvatures in two directions result in higher flame surface increment and consumption speed. Besides, for 3D cases with  $Le = 0.5$ , positive curvature regions on the flame front primarily contribute to the global reaction due to the Lewis effect. Statistical studies on flame dynamics between walls in 3D cases are also

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conducted, and results show that both the flame surface increment and the Lewis effect on curvature (if  $Le = 0.5$ ) are approximately consistent. 2D simulations for the thickness between walls can predict the acceleration from flame dynamics between walls in the 3D domain for both mixtures.

Keywords: Hydrodynamic instability; Thermodiffusive instability; Confined flow; Premixed flame

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## 1. Novelty and Significance Statement

This study is the first three-dimensional study on premixed flame freely propagating in narrow channels considering both hydrodynamic, including Darrieus-Landau (DL) and Saffman-Taylor (ST) instabilities, and thermodiffusive (TD) instabilities. It is also the first to validate the Joulin-Sivashinsky model's ability to incorporate wall confinement effects in 2D simulations across various narrow channel widths through comparisons with 3D direct numerical simulations. This research is significant as it explores the interplay between confinement effect and DL and TD instabilities. It is also significant for its investigation on the interaction of flame curvature in both normal and transverse directions, a phenomenon previously underexplored in confined geometries, and its exploration on the essential impact of flame curvature and the Lewis effect ( $Le < 1$ ) between walls on global flame dynamics at wider channels.

## 2. Author Contributions

- Z. Chen performed research, analyzed data and wrote the paper
- S. Zhao analyzed data and revised the paper
- B. Denet supervised project and revised the paper
- C. Almarcha supervised project and revised the paper
- P. Boivin supervised project and revised the paper

### 1 3. Introduction

2 Accurately simulating flame regimes in confined environments is cru-  
3 cial for micro-scale combustion devices, where stable combustion is essential  
4 for efficiency and safety. Premixed laminar flames exhibit various intrin-  
5 sic instabilities which profoundly affect flame dynamics: Darrieus-Landau  
6 (DL) instability arising from the density contrast across the flame front and  
7 yielding a positive growth rate of flame wrinkling and deforming the flame  
8 front [2–6]; thermodiffusive (TD) instability which results from the compe-  
9 tition between heat and species diffusion across the flame front, and thus  
10 could stabilize or destabilize flames depending on the Lewis number and the  
11 curvature of the flame front; Saffman-Taylor (ST) instability occurring be-  
12 tween two fluids with different viscosity [7] (ST instability is also inherently  
13 hydrodynamic [8]). Investigations on the destabilizing/stabilizing of gravity  
14 (Rayleigh-Taylor instability) and the interaction between flame dynamics  
15 and acoustics have been done in further studies [9–14].

16 The effects of Darrieus-Landau (DL) and thermodiffusive (TD) instabil-  
17 ities on planar flame stability have been widely studied through theoretical  
18 analysis. In the linear regime, perturbations on the flame front either grow  
19 or decay exponentially. Matalon et al. [5] developed a dispersion relation  
20 to quantify the growth rate of these perturbations, assuming an effective  
21 Lewis number close to unity. In contrast, Sivashinsky et al. [2] formulated a  
22 model that accommodates a broader range of Lewis numbers but is limited  
23 to small density contrasts across the flame front.

24 In the non-linear regime, theoretical analysis has derived a general non-  
25 linear equation - the Michelson-Sivashinsky equation - based on limiting  
26 approximations to describe the unstable flame dynamics [2]. Further theo-  
27 retical and numerical studies found that the domain size strongly influences  
28 equidiffusive premixed flame evolution. Within certain domain sizes (around  
29 40 times flame thickness), the flame stabilizes into a single cusp-like struc-  
30 ture pointing toward the burnt gases. In larger domains, continuous merging  
31 and splitting of cusps result in unsteady flame dynamics, a phenomenon ex-  
32 tensively studied both experimentally and numerically. A well-established  
33 configuration for studying this instability is the Hele-Shaw burner, which  
34 consists of two parallel plates separated by a narrow channel width  $h$ , where  
35 premixed flames propagate between the walls. Experimental studies using  
36 this setup have provided valuable insights into flame dynamics and have  
37 shown strong agreement with theoretical predictions [6, 15].

38 In confined environments, such as the Hele-Shaw burner, momentum  
39 and heat losses at the walls influence hydrodynamic instabilities. Joulin

1 and Sivashinsky conducted a linear stability analysis on these effects [1]. By  
2 modeling the flame as an effective interface and using Euler-Darcy equa-  
3 tions for both unburnt and burnt gases, they introduced a viscosity-based  
4 exchange coefficient  $f \sim \mu/h^2$  ( $\mu$ [kgm<sup>-1</sup>s<sup>-1</sup>]: gas dynamic viscosity) to in-  
5 clude the momentum losses into the momentum equation, demonstrating  
6 that friction induced pressure gradients, coupled with viscosity contrast,  
7 would enhance the Saffman-Taylor instability. Further numerical studies  
8 extended the Joulin-Sivashinsky model to the Navier-Stokes equations for  
9 reacting flows and performed linear stability analyses [8, 16, 17]. Assuming  
10 Poiseuille and isobaric flow, these studies found that momentum losses due  
11 to wall friction destabilize the flame and significantly impact its dynam-  
12 ics. Free flame propagation is considered in [8, 16], while the analysis in [1]  
13 is with the fresh gases flow moving at the planar flame speed against the  
14 flame. Further studies in [18, 19] conducted similar linear stability anal-  
15 ysis in the presence of fresh gases flow and it is observed that the flow  
16 against the flame propagation results in a larger growth rate than the one  
17 predicted by Darrieus-Landau theory, while a flow following the flame prop-  
18 agation direction leads to a smaller growth rate. However, the validation of  
19 the Joulin-Sivashinsky model in capturing confinement effects on free flame  
20 propagation through comparison with 3D cases is still required.

21 Fernandez et al. [20–22] simplified the problem to a quasi-2D form us-  
22 ing Darcy’s law to model the momentum losses of an equidiffusive flame  
23 freely propagating through a Hele-Shaw burner. Simulations in [22] have  
24 shown that this quasi-2D approach accurately captures the confinement ef-  
25 fects observed in 3D simulations in the limit  $h/\delta_T \rightarrow 0$ . However, for chan-  
26 nel widths exceeding one thermal flame thickness, it overestimates the cusp  
27 size. Moreover, as the channel width increases and the flame front becomes  
28 asymmetric between the walls, the flame curvature in the normal direction  
29 significantly affects the global propagation speed. Despite these findings, a  
30 detailed analysis of the flame structure is still required to understand the  
31 interactions between different curvature components and their impact on  
32 flame dynamics.

33 Moreover, the confinement effects on thermodiffusive instability are rarely  
34 explored. Numerical studies by Kang et al. [16] found that DL and ST in-  
35 stabilities favor the formation of large scale cells through the merging pro-  
36 cess, while TD instability enhances the cell splitting mechanism and results  
37 in smaller cellular structure. The global flame speed essentially depends  
38 on the interaction of these instabilities. On the other hand, the Lewis ef-  
39 fect on flame front curvature is extensively explored for lean hydrogen/air  
40 mixtures [23–25]. It has been found that the thermodiffusive instability

1 strengthens local reaction and influences flame global speed. It would be  
 2 interesting to study the Lewis effect on flame curvature between walls and  
 3 the impact on global dynamics, as a stable asymmetric flame front shape  
 4 can be established in narrow channels for premixed flames with smaller than  
 5 unity Lewis number [26–28]. Studies in [28] also explored the thermodiffu-  
 6 sive instability of flames propagating in a Poiseuille shear flow through 3D  
 7 simulations, and observed that the flame front configuration between walls  
 8 and along the transverse direction at various channel widths are influenced  
 9 by the flow rate with  $Le < 1$ . Yet for freely propagating flames, a detailed  
 10 study of the interaction between the normal and transverse flame configu-  
 11 rations is still needed.

12 In this study, we investigate the effect of confinement on premixed flames  
 13 freely propagating in narrow channels using compressible simulations. In ad-  
 14 dition to conducting 3D and 2D direct numerical simulations (DNS), we ex-  
 15 tend Joulin-Sivashinsky model within the compressible Navier-Stokes equa-  
 16 tions to incorporate wall confinement effects and compare it against 3D  
 17 simulations at various channel widths. The interaction of hydrodynamic  
 18 and thermodiffusive instabilities is then investigated. Furthermore, we an-  
 19alyze flame curvature in both the transverse and normal directions in 3D  
 20 simulations by comparing them with 2D simulations.

#### 21 4. General formulation

22 A one-step irreversible global reaction model is applied here, with the  
 23 reaction rate governed by the Arrhenius-type kinetic model  $F + O \rightarrow P$ ,  
 24 where  $F$  and  $O$  denote respectively the fuel and oxidizer, and  $P$  is the  
 25 products. Here a lean mixture is assumed, hence the oxidizer mass frac-  
 26 tion remains approximately constant, as explained in [22]. The amount  
 27 of fuel consumed per unit volume and per unit time is given by  $\Omega =$   
 28  $B\rho^2Y \exp(-E/R_gT)$ , where the  $B$  is the pre-exponential factor,  $\rho$  is the  
 29 mixture density,  $Y$  is the fuel mass fraction,  $T$  the temperature,  $R_g$  the  
 30 universal gas constant, and  $E = \beta RT_b^2/(T_b - T_u)$  is the overall activation  
 31 energy with  $\beta$  the Zeldovich number and subscripts  $u$  and  $b$  for the unburnt  
 32 and burnt gas states in one-dimensional planar flame, respectively. Gases  
 33 are assumed as ideal gas, with a constant expansion ratio  $q = \rho_u/\rho_b = 6$   
 34 with  $\rho_u = 1.277 \text{ kg/m}^3$ , and a constant Schmidt number  $Sc = 0.7$ , and two  
 35 Lewis numbers studied:  $Le = 1$  and  $Le = 0.5$ .

36 The Arrhenius parameters are then chosen as to obtain the desired Lewis  
 37 number, planar flame velocity  $S_L$ , thermal flame thicknesses ( $\delta_T = (T_b -$   
 38  $T_u)/\max(\nabla T)$ ), and diffusive flame thicknesses ( $\delta_D = D_{th}/S_L$ ).  $D_{th}$  is the

1 thermal diffusivity. The values of remaining characteristic parameters of the  
2 two flames at 1D planar regime are shown in Table 1. The parameters are  
3 carefully chosen to reflect practical significance and the flame thickness and  
4 speed with units are the real physical quantities and are used directly in the  
5 simulations. It is important to note that the primary objective of the present  
6 study is not to perform a direct comparison between the two mixtures, and  
therefore, it is not necessary for all parameters to be identical.

Table 1: Characteristic parameters of two flames

Parameters	$Le$	$\beta$	$\delta_D$	$\delta_T$	$S_L$
	[-]	[-]	[mm]	[mm]	[m/s]
Flame_1	1	10	0.1	0.43	1
Flame_05	0.5	14	0.128	0.5	0.78

7  
8 The mass, momentum, energy and species equations are solved under  
9 conservative form. The simulation is carried out in the reference frame at-  
10 tached to the flame moving at the flame consumption rate  $\mathbf{U}_{ref} = (u_{ref}, 0, 0)$ ,  
11 with  $u_{ref} = S_c$  and  $S_c$  defined as

$$S_c = -\frac{1}{\rho_u Y_{F,u} h} \int_0^{L_x} \int_0^{L_y} \int_0^h \dot{\omega}_F dx dy dz \quad (1)$$

12 where  $Y_F$  is the fuel mass fraction, and  $\dot{\omega}_F$  is the fuel reaction rate. The  
13 mass and momentum equations are then in the following forms:

$$\begin{aligned} \frac{\partial \rho}{\partial t} + \nabla \cdot [\rho(\mathbf{u} - \mathbf{U}_{ref})] &= 0 \\ \frac{\partial \rho \mathbf{u}}{\partial t} + \nabla \cdot [\rho \mathbf{u}(\mathbf{u} - \mathbf{U}_{ref})] &= -\nabla p + \nabla \cdot \Gamma \end{aligned} \quad (2)$$

14 where  $\mathbf{u}$  is the velocity in the laboratory reference,  $p$  is the pressure, and  $\Gamma$   
15 is the viscous tensor defined as

$$\Gamma = \mu \{ (\nabla \mathbf{u} + (\nabla \mathbf{u})^T) - \frac{2}{3} (\nabla \cdot \mathbf{u}) \mathbf{I} \} \quad (3)$$

16 with  $\mathbf{I}$  representing the identity matrix. Each component in  $\Gamma$  is then in form  
17 of  $\tau_{ij} = \mu (\frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i}) - \frac{2}{3} \delta_{ij} \nabla \cdot \mathbf{u}$ . The conservation of species is considered  
18 as:

$$\frac{\partial \rho Y_F}{\partial t} + \nabla \cdot [\rho(\mathbf{u} - \mathbf{U}_{ref}) Y_F] = \nabla \cdot (\rho D_F \nabla Y_F) + \dot{\omega}_F \quad (4)$$

1 where  $Y_F$  is the mass fraction of the fuel. The diffusion term is evaluated  
 2 through Fickian approximation. Naturally we have  $Y_P = 1 - Y_F$  for the  
 3 product.  $D_F$  stands for fuel's mass diffusion coefficient, and  $\dot{\omega}_F$  is its reaction  
 4 rate. The energy conservation is originally calculated in the form of total  
 5 energy ( $E_t$ ) in our Lattice-Boltzmann based solver ProLB [29]. The detailed  
 6 formulation is provided in Appendix A. However, it can also be expressed  
 7 in other forms such as enthalpy and temperature. Here for the sake of  
 8 simplicity, we give the formulation in the form of temperature ( $T$ ), as follows:

$$9 \quad \rho C_P \left[ \frac{\partial T}{\partial t} + (\mathbf{u} - \mathbf{U}_{\text{ref}}) \cdot \nabla T \right] = \frac{Dp}{Dt} + \nabla \cdot (\lambda \nabla T) + \dot{\omega}_T, \quad (5)$$

10 with the reaction term  $\dot{\omega}_T = (h_P - h_F)\dot{\omega}_F$  and the calculation of species  
 11 enthalpy  $h_k$  ( $k \in \{F, P\}$ ) is provided in Appendix B.  $\lambda$  is the ther-  
 12 mal conductivity and  $\lambda = \frac{\mu C_p}{Pr}$  with  $\mu$  the dynamic viscosity following the  
 13 temperature power-law  $\mu = \mu_0 \left(\frac{T}{T_0}\right)^{0.7}$ .  $T_0$  the reference temperature and  
 14  $T_0 = 298.15$  K. It is noteworthy that the comparison in [22] between con-  
 15 stant or temperature-dependent viscosity has highlighted the importance of  
 16 variable viscosity on global flame speed for narrow channel widths.  $Pr$  is  
 17 the constant Prandtl number. Ideal gas equation of state  $\frac{\rho RT}{W} = p$  is applied  
 18 for thermodynamic closure with  $W$  the mean molecular weight.

19 In two-dimensional simulations of the front-view plane, vectors in Eqs. 2,  
 20 4, and 5 only have  $xy$  plane components. However, the effect of confinement  
 21 on the wall yields momentum losses, and the ST instability would strengthen  
 22 the instability, as studied in [1, 8, 16, 17, 22, 30]. Additional terms should  
 23 be added to consider this effect. Here the momentum loss is included in the  
 24 form of viscous force  $\mathcal{F} = (\partial\tau_{zx}/\partial z, \partial\tau_{zy}/\partial z)$ , and added to the momentum  
 25 equation:

$$\frac{\partial \rho(\bar{\mathbf{u}} - \mathbf{U}_{\text{ref}})}{\partial t} + \nabla \cdot [\rho \bar{\mathbf{u}}(\bar{\mathbf{u}} - \mathbf{U}_{\text{ref}})] = -\nabla p + \nabla \cdot \Gamma^{2D} + \mathcal{F}, \quad (6)$$

26 where the viscous tensor  $\Gamma^{2D}$  is also defined as in Eq. 3 including only  $xy$   
 27 plane components.  $\tau_{zx}$  and  $\tau_{zy}$  defined as follows:

$$\begin{aligned} \tau_{zx} &= \mu \left\{ \frac{\partial(u_x - u_{\text{ref}})}{\partial z} + \frac{\partial u_z}{\partial x} \right\} \\ \tau_{zy} &= \mu \left\{ \frac{\partial u_y}{\partial z} + \frac{\partial u_z}{\partial y} \right\}. \end{aligned} \quad (7)$$

28 with  $u_x$  and  $u_y$  representing the  $x$  and  $y$  components of velocity vector,  
 29 and the second terms on the right hand side ( $\frac{\partial u_z}{\partial x}$  and  $\frac{\partial u_z}{\partial y}$ ) negligible. The

1 velocity field here is modeled by the Poiseuille flow assumption:

$$\mathbf{u} = -6\bar{\mathbf{u}}\left(\frac{z^2}{h^2} - \frac{z}{h}\right) \quad (8)$$

2 where  $\bar{\mathbf{u}} = \bar{\mathbf{u}}_{x,y}$  is the flow velocity averaged along  $z$  direction. So we have

$$\begin{aligned} \frac{\partial \tau_{zx}}{\partial z} &= \mu \frac{\partial^2 u_x}{\partial z^2} = -\mu \frac{12\bar{u}_x}{h^2} \\ \frac{\partial \tau_{zy}}{\partial z} &= \mu \frac{\partial^2 u_y}{\partial z^2} = -\mu \frac{12\bar{u}_y}{h^2} \end{aligned} \quad (9)$$

3 Applying this assumption can include the viscous friction term in the  
4 momentum equation without solving the flow in  $z$  direction. After adding  
5 this friction force, the momentum equation becomes:

$$\begin{aligned} \frac{\partial \rho(\bar{\mathbf{u}} - \mathbf{U}_{ref})}{\partial t} + \nabla \cdot [\rho \bar{\mathbf{u}}(\bar{\mathbf{u}} - \mathbf{U}_{ref})] &= -\nabla p + \\ &\nabla \cdot \Gamma^{2D} + f \bar{\mathbf{u}} \end{aligned} \quad (10)$$

6 where  $f = \frac{-12\mu}{h^2}$ . This formulation is hereafter termed the 2D+ simulation,  
7 whereas the two-dimensional simulation without this body force term will  
8 be denoted as pure 2D simulation. Note that the 2D+ simulations are  
9 slightly different from Joulin and Sivashinsky Euler-Darcy formulation [1],  
10 which includes the friction term but neglects  $\Gamma^{2D}$  to simplify the theoretical  
11 calculations.

## 12 5. Numerical setup

13 A Hele-Shaw burner with two open ends is used to study the propagation  
14 of a premixed laminar flame while minimizing acoustic perturbations. The  
15 top ( $z = h$ ) and bottom walls ( $z = 0$ ) are set as adiabatic, no-slip boundaries.  
16 A constant pressure outlet at 1 bar is applied on the burnt side, formulated  
17 as

$$x \longrightarrow -\infty : \frac{\partial \mathbf{u}}{\partial x} = \frac{\partial T}{\partial x} = \frac{\partial Y_k}{\partial x} = 0. \quad (11)$$

18 A non-reflecting boundary condition is applied on the fresh side (see Table  
19 9.4: B2 in [31]) to simulate an infinitely long domain. The domain length  
20 is set to twice the width to avoid effects from the open ends. Periodic  
21 boundary conditions are applied along the transverse sides. A schematic of  
22 the configuration is shown in Fig. 1.

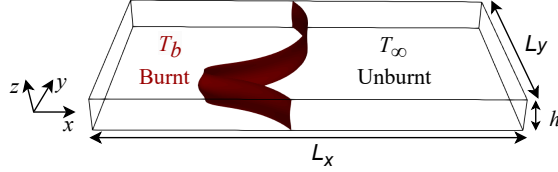


Figure 1: Configuration sketch of curved flame propagating between two walls.

1 The domain is initially filled with a premixed mixture at a temperature  
 2 of  $T_\infty = 300$  K and pressure  $p = 1$  bar. The initial condition consists of  
 3 an initially planar flame, perturbed by a sinusoidal perturbation in the  $xy$   
 4 plane, with an amplitude  $A = 0.4\delta_T$ . Additionally, for 3D cases, a tilted  
 5 planar flame is set in the  $xz$  plane to trigger potential asymmetric flame  
 6 solutions. The mass, momentum, energy and species equations are solved  
 7 under conservative form using the Lattice-Boltzmann solver ProLB [29, 32–  
 8 34]. For a detailed derivation of Lattice-Boltzmann methods (LBM), the  
 9 reader is referred to [34]. Structural mesh resolution of  $\Delta x = 0.1\delta_T$  is chosen  
 10 to resolve the flame. A finer mesh with  $\Delta x = 2 \times 10^{-5}$  m is used for the  
 11 smallest channel width for Flame\_1 to capture the flame dynamics between  
 12 walls, while for the smallest channel width for Flame\_05, a resolution of  
 13  $\Delta x = 10^{-5}$  m is chosen, which will be explained in Section 6.2. The mesh  
 14 resolutions in the present study show numerical convergence.

## 15 6. Results and analysis

16 In Section 6.1 the capability of 2D+ simulation to recover the momen-  
 17 tum loss is analyzed using Flame\_1. Section 6.2 investigates the effect of  
 18 interaction between hydrodynamic and thermodiffusive instabilities using  
 19 Flame\_05.

### 20 6.1. 2D+ simulation validation

21 According to [22] where Flame\_1 is applied, there is a critical transverse  
 22 domain size  $\hat{L}_y$  (around  $20\delta_T$ ) above which the flame front would exhibit an  
 23 unsteady oscillatory behavior. Therefore, a 3D computational domain size  
 24 of  $L_y = 5.7$  mm is chosen here to obtain a steady one-cusp structure for  
 25 Flame\_1. The domain length is chosen as  $L_x \approx 2L_y$  and different channel  
 26 widths are set.

1 6.1.1. Momentum loss

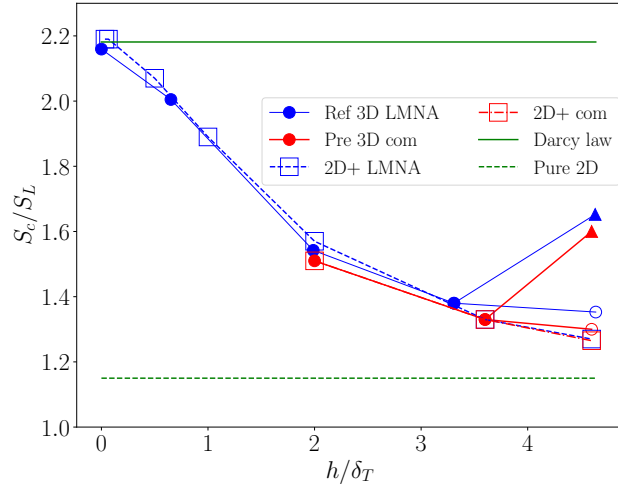


Figure 2: Flame\_1, the variation of consumption speed with channel width. Blue circles and triangles represent results from 3D simulations in reference [22], while red circles and triangles correspond to the present 3D simulations. In both studies, solid circles indicate stable, symmetric flame shapes between the walls, while for channel widths  $h$  greater than a critical value, stable solutions with asymmetric flame shapes are shown as solid triangles and unstable symmetric solutions—obtained by imposing symmetry boundary conditions as done in [22]—are represented by hollow circles. Hollow squares stand for the present 2D+ simulations, with colors blue and red standing for fully-compressible and LMNA formulations. Green dashed and solid lines representing results from pure 2D simulation and reference [22] using Darcy’s law, respectively.

2 The variation in flame consumption speed with channel width ( $h$  ranging  
3 from  $0.033\delta_T$  to  $4.6\delta_T$ ) is shown in Fig. 2. All values are derived from steady-  
4 state solutions. In addition to both 3D and 2D+ cases with the numerical  
5 setup described in Section 5, additional 2D+ simulations are carried out  
6 with low-Mach number approximation (LMNA) to solve pressure-velocity  
7 coupling in order to ensure mass conservation, and the same closed-inlet  
8 boundary condition as in [22] to enable comparisons (3D simulations results  
9 from [22] are referred as 3D reference), given that for ultra narrow channel  
10 widths ( $h \leq 1\delta_T$  in the present case), the significant pressure increase on the  
11 flame front affects the reaction and the flow with fully compressible codes.  
12 In the figure, results with LMNA are represented by blue color, while red  
13 color represents fully compressible codes described in Section 5. Compared  
14 to 3D cases, the consumption speed is underestimated in the pure 2D case  
15 (green dashed line); in contrast, Darcy’s law (green solid line) overestimates

1 the consumption speed except for  $h \rightarrow 0$ , as discussed in [22].  
 2 The comparison between the 3D reference, the present 3D and 2D+  
 3 simulations is divided into three parts:

- 4 •  $h \leq \delta_T$   
 5 A strong agreement is observed for  $h \leq \delta_T$  between the 3D refer-  
 6 ence (blue circles) and the present 2D+ model (blue squares). The  
 7 flame consumption speed increases as the channel width decreases and  
 8 the Saffman-Taylor instability is enhanced. Moreover, in the limit  
 9  $h/\delta_T \rightarrow 0$ , the flame speed predicted by Darcy’s law is recovered by  
 10 the present 2D+ simulation. It should be mentioned that for this  
 11 range of  $h$ , LMNA and the same closed-inlet boundary condition as in  
 12 reference [22] are necessarily activated to enable the comparison.
- 13 •  $\delta_T < h \leq 3.6\delta_T$   
 14 For this range of  $h$ , the 2D+ simulation (squares) also accurately re-  
 15 produces the 3D flame consumption speed (circles). Furthermore, the  
 16 difference between 2D+/reference 3D cases using LMNA and closed-  
 17 inlet boundary condition (blue squares/circles) and 2D+/3D cases us-  
 18 ing fully compressible codes and open inlet (red squares/circles) is  
 19 negligible. Hereafter, we only discuss results with fully compressible  
 20 codes and open-inlet end as in Section 5. The temporal evolution of  
 21 flame consumption speeds for 3D and 2D+ cases is provided in Fig. 3  
 22 to highlight the good agreement between 3D and 2D+ simulations for  
 23 symmetric cases.

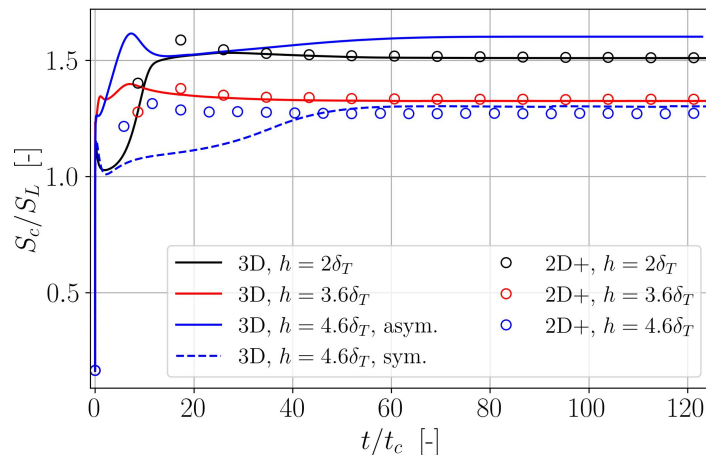


Figure 3: Flame\_1, evolution of flame consumption speed with time.

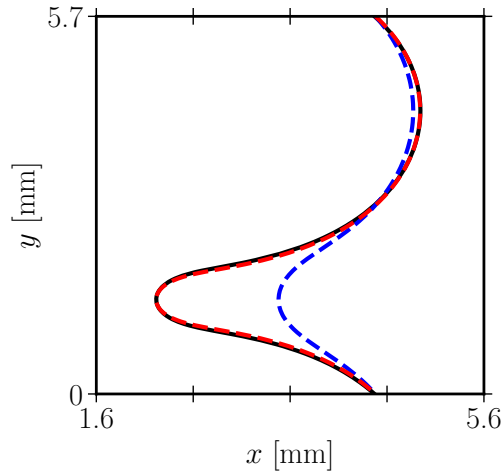


Figure 4: Flame\_1, with  $h = 2\delta_T$ , isocontours of  $c = 0.8$  with black curve standing for 3D case in the plane  $z = \frac{1}{2}h$ , blue curve for pure 2D simulation and red curve for 2D+ simulation.

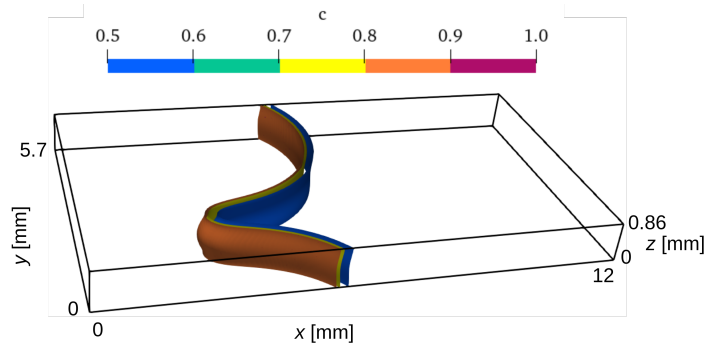


Figure 5: Flame\_1, with  $h = 2\delta_T$ , isocontours of  $c = 0.5$ ,  $c = 0.8$ , and  $c = 0.9$ .

1 Given the unity Lewis number, the consumption speed is solely due to  
 2 the flame surface increment. Figure 4 illustrates the flame front mor-  
 3 phology represented by isocontours of progress variable  $c = 0.8$  with  
 4  $c = 1 - Y_F$  for a channel width  $h = 2\delta_T$ . The black curve standing  
 5 for 3D case in the plane  $z = \frac{1}{2}h$ , while blue and red curves represent  
 6 the pure 2D simulation and the 2D+ simulation, respectively. Com-  
 7 pared to the pure 2D simulation, the friction force contributes to the  
 8 elongation of the cusp [8], yielding a larger cusp. On the other hand,  
 9 the flame front between walls is slightly curved and symmetric, yield-  
 10 ing negligible contribution to the global surface increment, as shown  
 11 in in Fig. 5, which presents the isosurfaces at  $c = 0.5, 0.8$  and  $0.9$   
 12 from the left to the right. Overall, with the increase of channel width,  
 13 the consumption speeds from both the 3D and 2D+ simulations de-  
 14 crease and converge towards the values from pure 2D simulations as  
 15 the confinement effect diminishes.

- 16 •  $h = 4.6\delta_T$   
 17 However, for  $h = 4.6\delta_T$ , the 3D case yields a stable asymmetric so-  
 18 lution which exhibits an increase in consumption speed whereas the  
 19 2D+ simulation keeps decreasing. The temporal evolution of  $Sc/S_L$   
 20 is shown in Fig. 3. This contrast is due to the flame losing its sym-  
 21 metry around the central plane of the channel, which further enhances the  
 22 consumption speed. The unstable symmetric solution has also been  
 23 investigated by imposing symmetric boundary in the central plane be-  
 24 tween walls, as has been done in [22]. The consumption speed of the  
 25 forced symmetric solution closely matches that predicted by the 2D+  
 26 simulation, confirming that the 2D+ model can accurately reproduce  
 27 the 3D results when the flame is symmetric between the walls.

28 Figure 6 illustrates the isocontours of progress variable at  $c = 0.5,$   
 29  $0.8$  and  $0.9$  for forced symmetric and asymmetric solutions with  $h =$   
 30  $4.6\delta_T$  in 3D simulation. As a reference, in the forced symmetric case,  
 31 the flame front between walls is slightly curved and symmetric (see  
 32 Fig. 6a), whereas the stable asymmetric solution (see Fig. 6b) is highly  
 33 curved between walls, yielding a larger flame front surface compared to  
 34 forced symmetric one. Additionally, the cusp sizes vary significantly  
 35 along the normal direction, implying the interaction between flame  
 36 curvatures in transverse and normal directions. Together with Fig. 5,  
 37 it is noteworthy that for each case, there is no observable difference  
 38 between different isocontours. To analyze the sensibility of the flame  
 39 front surface to choices of isosurface, Fig. 7 shows the variation of flame

1 front surface increment  $A_f/A_0$  with the isosurface  $c$  for the case with  
 2  $h = 2\delta_T$  and  $h = 4.6\delta_T$ .  $A_0$  is the domain section surface  $A_0 \equiv L_y \times h$   
 3 and the global flame front surface  $A_f$  is calculated by

$$A_f = \int_V \sum(\mathbf{x}, t) dV \quad (12)$$

4 with the flame surface density (FSD) representing the local, instan-  
 5 tantaneous surface area of an isosurface per unit volume. Beyond stud-  
 6 ies focusing on its estimation [35] and its role in turbulent combus-  
 7 tion [36–39], other research has employed laminar flame data and FSD  
 8 formulations to estimate the instantaneous flame surface area [40]. As  
 9 done in [41], the flame surface density at an isosurface at  $c(x, t) = c_0$   
 10 can be calculated as the product of the magnitude of  $\nabla c$  and the “fine  
 11 gained” PDF:

$$\sum(\mathbf{x}, t) = |\nabla c| \delta(c - c_0), \quad (13)$$

12 where  $\delta$  is the Dirac delta function. It is observed that for both cases  
 13 the flame surface increment is insensible to the  $c$  value, as expected.

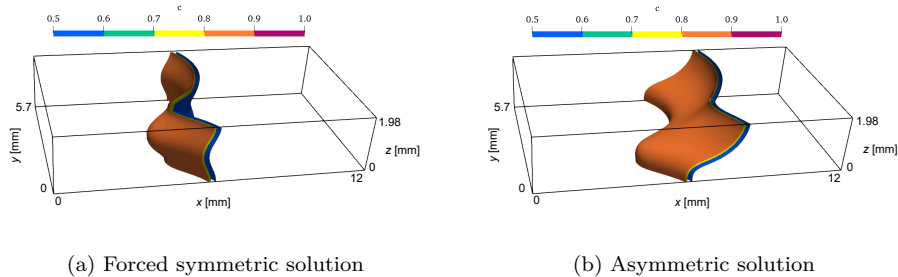


Figure 6: Flame\_1: for  $h = 4.6\delta_T$ , isocontours of  $c = 0.5$ ,  $c = 0.8$ , and  $c = 0.9$ .

### 14 6.1.2. Flame curvature interaction

15 This section investigates the interaction of flame front curvature in both  
 16 transverse and normal directions for  $h = 4.6\delta_T$ , where the flame front be-  
 17 tween walls is asymmetric.

18 From left to right, the three figures in Fig. 8 illustrate the isocontours  
 19 of  $c = 0.8$  in the plane  $z = \frac{1}{3}h$ ,  $z = \frac{1}{2}h$ , and  $z = \frac{2}{3}h$  for  $h = 4.6\delta_T$ , in  
 20 comparison with pure 2D simulation and 2D+ simulations. It is observed  
 21 that the cusp size varies with the  $z$  position. While the 2D+ simulation

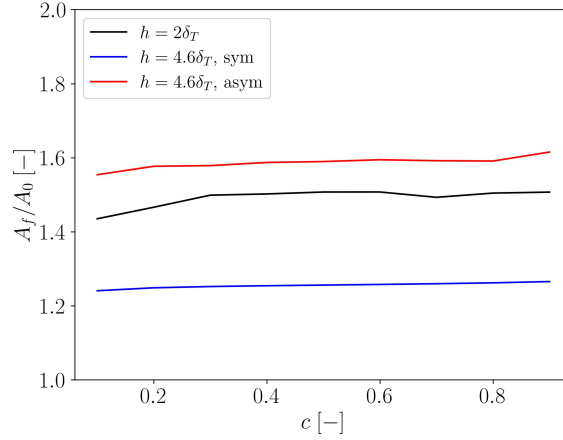


Figure 7: Flame\_1, sensitivity of flame front surface increment  $A_f/A_0$  to isosurface  $c$ .

1 closely matches the 3D case at  $z = \frac{1}{3}h$ , it overestimates the cusp size at  
 2 planes  $z = \frac{1}{2}h$  and  $z = \frac{2}{3}h$ . Pure 2D simulation, on the other hand, aligns  
 3 well with the 3D case at  $z = \frac{1}{2}h$ . This variation in cusp size in the 3D case  
 4 results from the asymmetric flame front morphology between walls. Overall,  
 5 in the  $xy$  plane, the cusp near the bottom wall is more elongated than the  
 6 one near the top wall, as the flame front between walls is concave toward  
 7 fresh gases near the bottom wall and forms an elliptic concave topology.

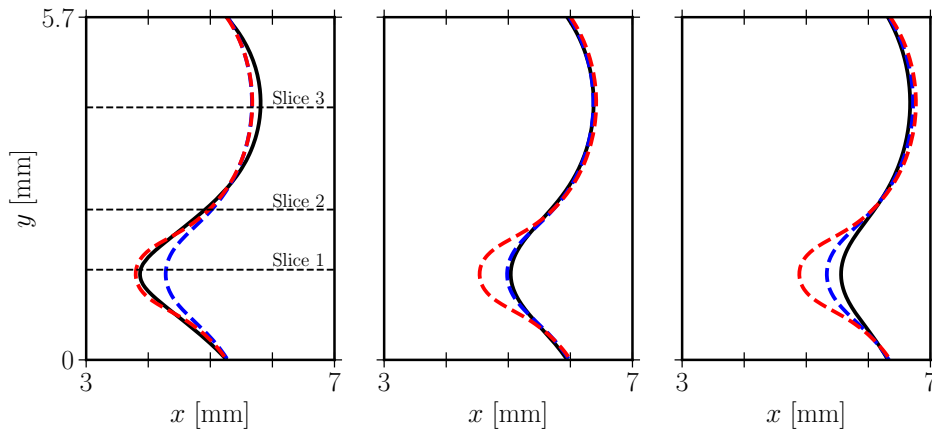


Figure 8: Flame\_1, for  $h = 4.6\delta_T$ , isocontours of  $c = 0.8$ , with black curves standing for 3D case in the plane  $xy$ , blue curves for pure 2D simulation and red curves for 2D+ simulation. From left to right: plane  $z = \frac{1}{3}h$ ;  $z = \frac{1}{2}h$ ;  $z = \frac{2}{3}h$ .

1 To better assess the interaction between flame topology in the  $xy$  and  $xz$   
 2 planes, a 2D configuration between walls is also set, as shown in Fig. 9. The  
 3 boundary conditions in the longitudinal and normal directions are set the  
 4 same as in the 3D configuration. A steady flame front is established using  
 5 the same  $L_x$  and  $h$  as in the 3D case.

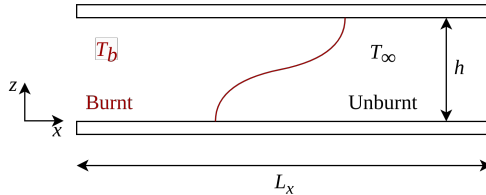


Figure 9: 2D configuration sketch between walls.

6 Figure 10 compares the flame front shape between walls at different  
 7  $y$  positions with the steady solution obtained from the 2D configuration in  
 8 Fig. 9. It is observed that while flame fronts between walls are all asymmetric  
 9 at different  $y$  positions, the extent of elongation varies depending on the  
 10 location relative to the cusp and tip in the  $xy$  plane. In Fig. 10a, which  
 11 compares the contours at plane  $y = 1.5$  mm (Slice 1 annotated in Fig. 8) with  
 12 the solution from the 2D simulation between walls, the flame front exhibits a  
 13 longer elongation due to the emergence of a cusp in the  $xy$  plane. In contrast,  
 14 at the plane  $y = 4.2$  mm (Slice 3 annotated in Fig. 8) corresponding to the  
 15 tip in the  $xy$  plane, the elongation is shorter than in the 2D simulation, see  
 16 Fig. 10c. Between the two extremes, at  $y = 2.5$  mm (Slice 2 annotated in  
 17 Fig. 8), the flame fronts in the 3D slice and the 2D simulation between walls  
 18 are approximately the same, as depicted in Fig. 10b. These observations  
 19 indicate that the interaction between flame front curvature in the transverse  
 20 and normal directions significantly influences the local flame morphology.

### 21 6.1.3. Flame curvature between walls

22 For further insight into the flame curvature between walls, slices along  
 23 the planes  $xz$  with a width of  $2\Delta x$  are extracted from the 3D case. The  
 24 flame surface increment is calculated as  $A_f/A_0$ ,  $A_0 = h \times 2\Delta x$  the slices  
 25 section surface from the  $yz$  plane, and  $A_f$  the flame front surface of each  
 26 slice as defined in Eq. 12. Additionally, to separate the stretch due to the  
 27 curvature in the plane  $xy$ ,  $A_{f,xz}$  is calculated considering only components

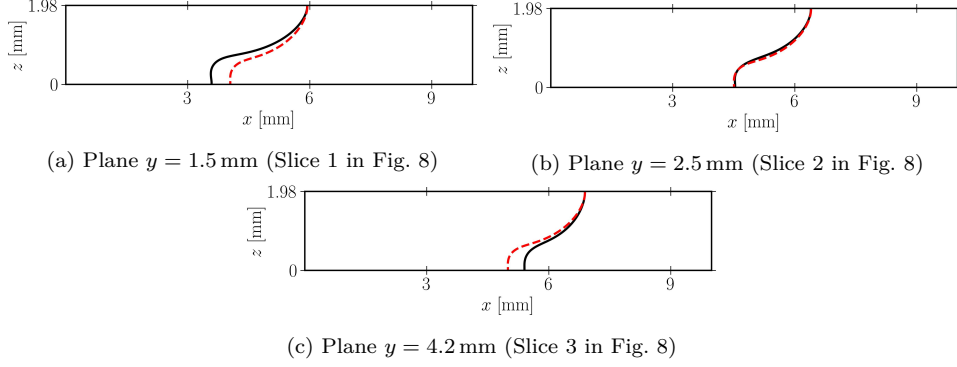


Figure 10: Flame\_1, comparison of flame front contours at  $c = 0.8$  between 2D simulation between walls (red curve) and 3D slice (black curve) in planes  $y = 1.5$  mm (a),  $y = 2.5$  mm (b),  $y = 4.2$  mm (c).

1 in the plane  $xz$  of  $\nabla c$ :

$$A_{f,xz} = \int_V \sum (\mathbf{x}, t)_{xz} dV \quad (14)$$

2 with

$$\sum (\mathbf{x}, t)_{xz} = |\{\nabla c\}_{xz}| \delta(c - c_0). \quad (15)$$

3 Both  $A_f$  and  $A_{f,xz}$  are calculated at the slice isosurface  $c = 0.8$ . Their  
 4 probability distribution function is shown in Fig. 11. For both  $A_f$  and  
 5  $A_{f,xz}$ , the first peak appears around  $A_f/A_0 = 1.35$ , corresponding to the  
 6 region near the plane  $y = 4.2$  mm, where is located the flame front tip  
 7 in the  $xy$  plane. The difference in the second peak ( $\{A_f/A_0\}_{3D} = 1.78$   
 8 vs.  $\{A_{f,xz}/A_0\}_{3D} = 1.68$ ) arises from the stretch effect around the cusp in  
 9 the  $xy$  plane. A wider range of  $A_f/A_0$  also indicates this strong flame  
 10 stretch. The average flame surface increment between walls in the 3D  
 11 case  $\{ave(A_{f,xz}/A_0)\}_{3D} = 1.46$  is close to the 2D simulation between walls  
 12 ( $\{A_f/A_0\}_{2D} = 1.49$ ) (represented by the blue dashed line in the figure),  
 13 while the average value of  $A_f/A_0$  overestimates the flame surface increment  
 14 due to the additional stretch effect in the  $xy$  plane.

15 The sensibility of  $A_f/A_0$  of slices to choices of  $c$  is also analyzed, as shown  
 16 in Fig. 12. All three flame surface increments are approximately constant  
 17 despite different  $c$ . Moreover,  $A_{f,xz}/A_0$  remains close to the value from the  
 18 2D configuration.

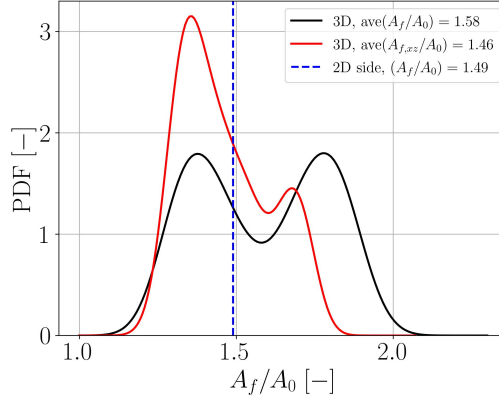


Figure 11: Flame\_1, probability distribution of flame front surface increment  $A_f/A_0$  of slices with  $h = 4.6\delta_T$  and  $L_y = 5.7$  mm.

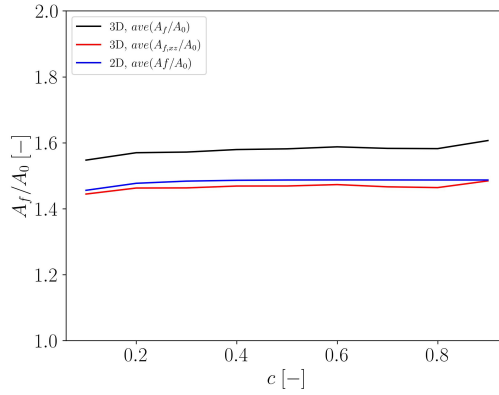


Figure 12: Flame\_1, sensitivity of flame front surface increment  $A_f/A_0$  of slices to iso-surface  $c$  for  $h = 4.6\delta_T$ .

## 1 6.2. Interaction between hydrodynamic and thermodiffusive instabilities

2 The aforementioned sections focus solely on hydrodynamic instabili-  
3 ties (ST and DL instabilities). In this section, the confinement effect on  
4 Flame\_05, which also exhibits intrinsic thermodiffusive instability, will be  
5 studied. According to 2D studies, the critical channel width for Flame\_05  
6 to sustain a stable asymmetric flame is  $h_c = 0.8\delta_T$ . To investigate the flame  
7 structure and the interaction of intrinsic instabilities with the asymmetric  
8 flame between walls, two 3D cases are considered. Both have a transverse  
9 width of  $L_y = 7.2\delta_T$ .

1 6.2.1. Flame structure in 3D

2 Two cases with different channel widths ( $h = 1.2\delta_T$  and  $h = 2\delta_T$ ) are  
 3 set and initialized both with sinusoidally perturbed planar flames. For both  
 4 cases, the flame fronts converge to an ultimate steady structure in time,  
 5 which consists of three cusps, as depicted by the isosurface  $c = 0.8$  in Fig. 13.  
 6 In the steady state, the consumption speeds for the two cases:  $h = 1.2\delta_T$   
 7 and  $h = 2\delta_T$ , are listed in Table 2, represented by  $S_c/S_L$ . The increase in  
 8 the flame speed mainly comes from: (1) likewise, both the curvature in the  
 9 transverse direction and between walls in 3D cases result in a significant in-  
 10 crease in flame surface and consequently the consumption speed, represented  
 11 by the flame surface increment parameter  $A_f/A_0$ ; (2) preferential diffusion  
 12 on the flame front with positive curvature between walls strengthens local  
 13 reaction rates, evaluated by the amplification factor  $I_0 = \{S_c/S_L\}/\{A_f/A_0\}$ .  
 14 The isosurface at  $c = 0.8$  is chosen as representative of the flame front, and  
 15  $A_0 = L_y \times h$ . Table 2 also summarizes the values of these parameters of  
 16 interest for the two cases. As can be observed in Fig. 13, a larger channel  
 17 width leads to a higher flame front surface increment, whereas the amplifica-  
 18 tion factor decreases, which is related to the flame front positive curvature.  
 19 Figure 14 presents the PDF results of curvature on the flame front at  $c = 0.8$   
 20 for the two cases. The curvature is adimensionlized by multiplying by the  
 21 thermal flame thickness. In addition to a higher positive curvature at the  
 22 peak probability, a larger positive curvature distribution is also found with  
 23 smaller channel width, which favors the reactivity owing to the Lewis effect.

24 This enhancement because of the Lewis effect on curvature is also illus-  
 25 trated in Fig. 13 through the distribution of  $HRR_{norm}$  and the curvature  $\kappa$   
 26 in the isosurface  $c = 0.8$  in 3D simulations.  $HRR_{norm}$  is the ratio of heat  
 27 release rate ( $HRR$ ) to the value of  $HRR$  in 1D planar flame at  $c = 0.8$ .  
 28 Figure 13 shows a considerable increase ( $\times 100$ ) in reaction where the flame  
 29 front is convex toward fresh gases. On the other hand, flame decelerates  
 30 where the flame front is concave toward fresh gases.

Table 2: Flame\_05, the mean value of flame consumption speed  $S_c/S_L$ , flame front surface  $A_f/A_0$ , and the amplification factor  $I_0$  from 3D cases with channel widths  $h = 1.2\delta_T$  and  $h = 2\delta_T$ .

$h/\delta_T$	$S_c/S_L$	$A_f/A_0$	$I_0$
1.2	6.74	3.19	2.11
2	7.81	4.29	1.82

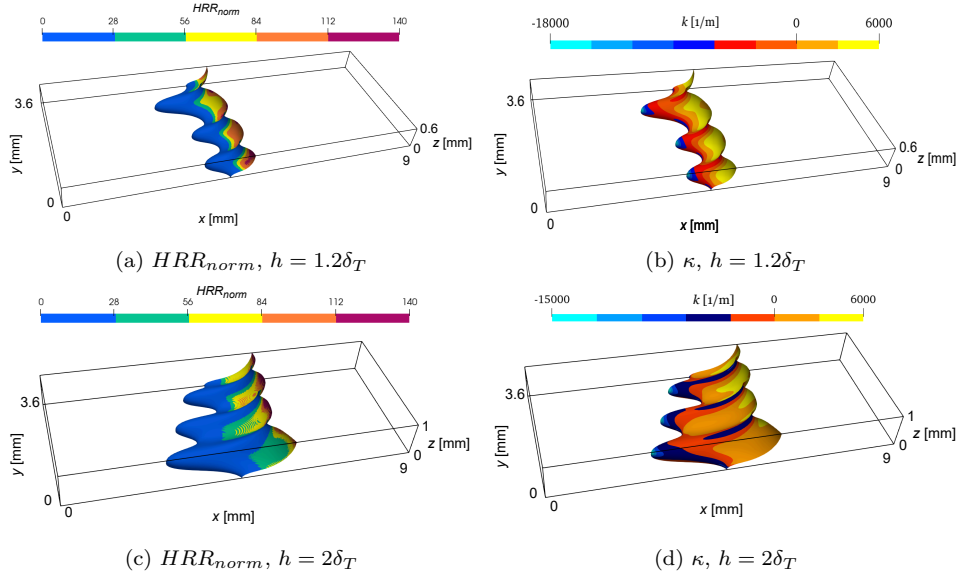


Figure 13: Flame\_05, HRR ( $HRR_{norm}$ ) and curvature ( $\kappa$ ) distribution on isosurface  $c = 0.8$ .

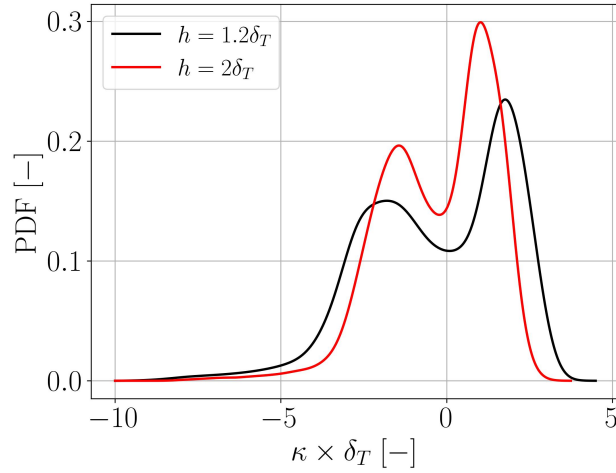


Figure 14: Flame\_05, probability distribution of curvature on flame front at isosurface  $c = 0.8$ .

- 1 Figure 15 presents the proportions of negative curvature and positive
- 2 curvature (black bars) on the flame front, as well as their contributions to
- 3 the total heat release rate (red bars). For both  $h = 1.2\delta_T$  and  $h = 2\delta_T$ , the

1 surface ratios of convex and concave regions on the flame front are largely  
 2 equivalent, while more than 90%  $HRR$  comes from the convex part.

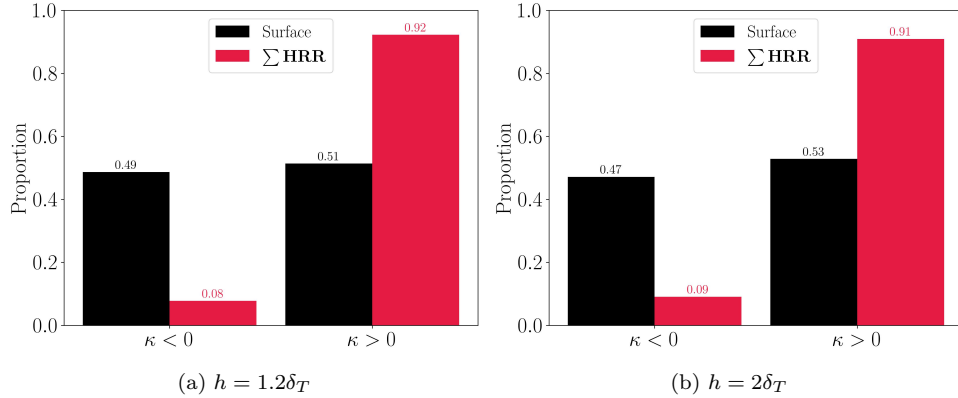


Figure 15: Flame\_05, the proportions of positive and negative curvature  $\kappa$  and their contribution to total heat release rate  $HRR$  with  $h = 1.2\delta_T$  (a) and  $h = 2\delta_T$  (b).

3 In the  $xy$  plane, the cusp size on the flame front varies along the direc-  
 4 tion  $z$ , similar to the case with Flame\_1. The elongation of cusps in the  
 5 plane  $xy$  near the bottom wall is greater than the one near the top wall  
 6 due to the cusp in the plane  $xz$ , which also locates near the bottom wall.  
 7 The conjunction of these two cusps yields an elliptic concave topology, as  
 8 discussed in Section 6.1.2, and greatly decreases the reaction. This explains  
 9 why the region from the bottom wall to  $y = \frac{1}{4}h$  has a negligible contribution  
 10 to  $HRR$ .

11 Moreover, the flame inner structure for the 3D case with  $h = 1.2\delta_T$  is  
 12 analyzed through the norm of progress variable divergence  $|\nabla c|$ , as shown  
 13 in Fig. 16a. The maximum of conditional average for the 3D case is around  
 14 three times higher than the one for 1D planar flame, indicating a much  
 15 thinner flame. The grid resolution of  $10^{-5}$  m is thus chosen to well resolve  
 16 the flame inner structure.

Additionally, Fig. 16 distinguishes  $|\nabla c|$  with positive and negative cur-  
 vature by black and red colors, respectively. It is observed that positive  
 curvature drastically increases  $|\nabla c|$ , i.e. strong convexity of the flame front  
 thins the flame thickness due to the Lewis effect. Figure 16b and c show  
 the distribution of  $|\nabla c|$  for  $z > \frac{9}{10}h$  and  $z < \frac{1}{10}h$ , respectively. Given the  
 asymmetric flame front shape between walls (see Fig. 13), which exhibits  
 convexity close to the top wall ( $z = h$ ) and concavity near the bottom wall

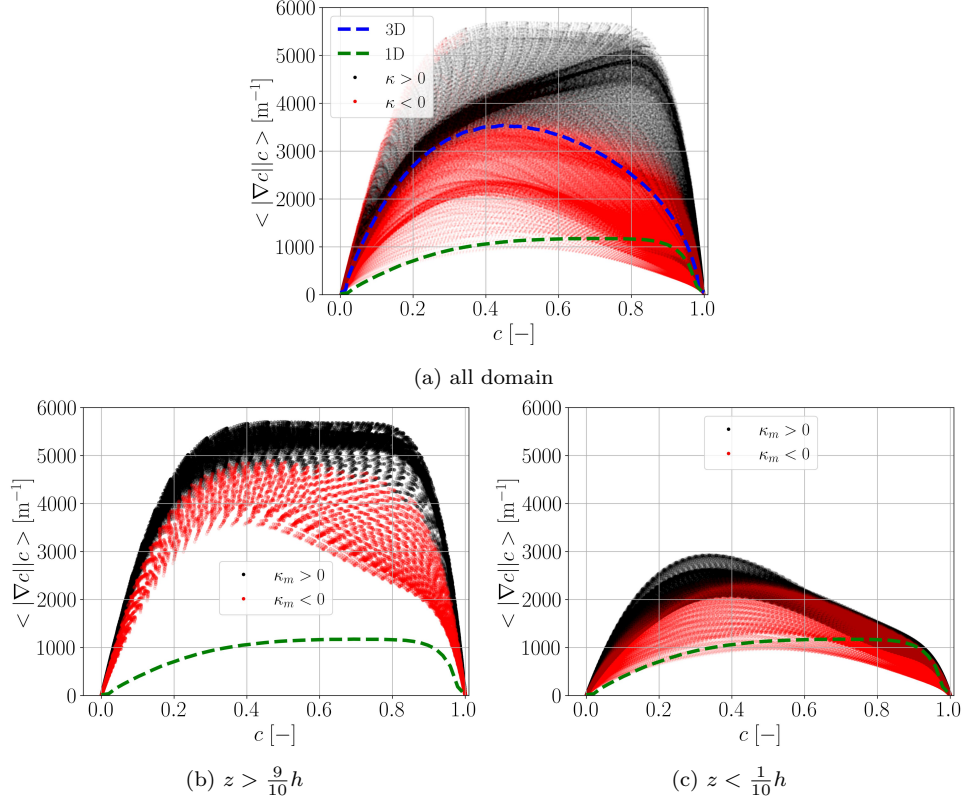


Figure 16: Flame\_05, (a) norm of progress variable divergence  $|\nabla c|$  across the entire domain with  $h = 1.2\delta_T$ , where black and red points indicate positive/negative curvature, respectively. The conditional average is represented by blue (3D) and green (1D) dashed lines. (b) and (c) show  $|\nabla c|$  for regions  $z > \frac{9}{10}h$  and  $z < \frac{1}{10}h$ , respectively, with black/red points representing positive/negative curvature in the  $xy$  plane.

( $z = 0$ ), of interest here is the positive average curvature  $\kappa_m$ , defined as

$$\kappa_m = \nabla \cdot n_{xy}, \quad n_{xy} = \{\nabla c\}_{xy} / |\{\nabla c\}_{xy}|,$$

- 1 where  $\{\nabla c\}_{xy}$  only has components in the  $xy$  plane. Hence,  $\kappa_m$  represents
- 2 the flame front convexity in the plane  $xy$ . Together with Fig. 16a, it can be
- 3 observed that convexity in the  $xz$  plane dominates the flame inner structure,
- 4 yielding considerably higher  $|\nabla c|$  for  $z > \frac{9}{10}h$ . This highlights the critical
- 5 role of asymmetric flame dynamics in confined environments, as they sub-
- 6 stantially impact the overall flame structure. Furthermore, convexity in the
- 7 plane  $xy$  modulates the amplitude of  $|\nabla c|$ : positive  $\kappa_m$  leads to higher  $|\nabla c|$

1 compared to negative  $\kappa_m$ .

## 2 6.2.2. Flame dynamics between walls

3 Similar to Section 6.1.2, slices along the planes  $xz$  with a width of  $2\Delta x$   
4 are extracted from 3D cases to investigate the flame dynamics between walls  
5 for Flame\_05. The flame surface increment is calculated as  $A_f/A_0$ , with  $A_f$   
6 the flame front surface calculated at isosurface  $c = 0.8$  of each slice, and  
7  $A_0 = h \times 2\Delta x$  the slices section surface from the  $yz$  plane. Here  $c = 0.8$  is  
8 chosen as a representation of the flame front. Previous studies reveal that  
9 regions with negative curvature have a negligible contribution to the global  
10 reaction, and the flame front convexity in the plane  $xy$  is consistent as shown  
11 in Fig. 13. Besides, the convex part ( $\kappa_m > 0$ ) also contributes more than  
12 90% of the global reaction rate. Of interest here are the slices with positive  
13 average curvature  $\kappa_m$ . Hereafter, the star superscript  $*$  refers to slices with  
14  $\kappa_m > 0$ .

15 The probability distribution function (PDF) of  $A_f/A_0$  is shown in Fig. 17.  
16 Taking into account all slices (black curve) results in a higher average flame  
17 surface increment between two walls since the flame elongation toward burnt  
18 gases for slices with negative  $\kappa_m$  is larger, as explained in Section 6.1.2.  
19 The PDF distribution of the flame front surface with positive average  $\kappa_m$   
20 (red curve, termed  $A_f^*/A_0$ ), however, exhibits one significant maximum  
21 around 1.6 for  $h = 1.2\delta_T$ , which is close to the value from 2D simula-  
22 tion between walls (1.74). Likewise, the flame surface increment without  
23 the stretch from the plane  $xy$  is also calculated using Eqs. 14 and 15,  
24 which exhibits a narrower range and a more significant peak located at  
25  $\{ave(A_{f,xz}^*/A_0)\}_{3D} = 1.55$ . A similar observation is obtained in Fig. 17b for  
26  $h = 2\delta_T$ . Likewise, compared to a more homogeneous distribution for all  
27 slices, the surface increment of slices with positive  $\kappa_m$  shows a peak around  
28 2, also close to the value 2.12 in the 2D simulation between walls. Without  
29 the stretch from the curvature in the plane  $xy$ ,  $\{ave(A_{f,xz}^*/A_0)\}_{3D}$  shows a  
30 more significant peak at  $\{ave(A_{f,xz}^*/A_0)\}_{3D} = 1.9$ .

31 It should be mentioned that the isosurface area for  $Le = 0.5$  is sensitive  
32 to the  $c$  value (a difference greater than 70% between isosurfaces  $c = 0.1$   
33 and  $c = 0.9$  in 3D). A sensitivity analysis of the choice of isosurface on the  
34 flame front surface is conducted. Figure 18 presents the variation of flame  
35 surface increment with the choice of isosurface  $c$  on the flame front, from  
36 both 3D and 2D configurations. It is observed that for both configurations,  
37  $A_f/A_0$  increases considerably with  $c$ . Moreover, all curves exhibit the same  
38 variation trends. Besides, the surface increment without the stretch from

- 1 the curvature in the plane  $xy$  ( $\{ave(A_{f,xz}^*/A_0)\}_{3D}$ ) is close to the value  
 2  $\{ave(A_f/A_0)\}_{2D}$  from 2D configuration.

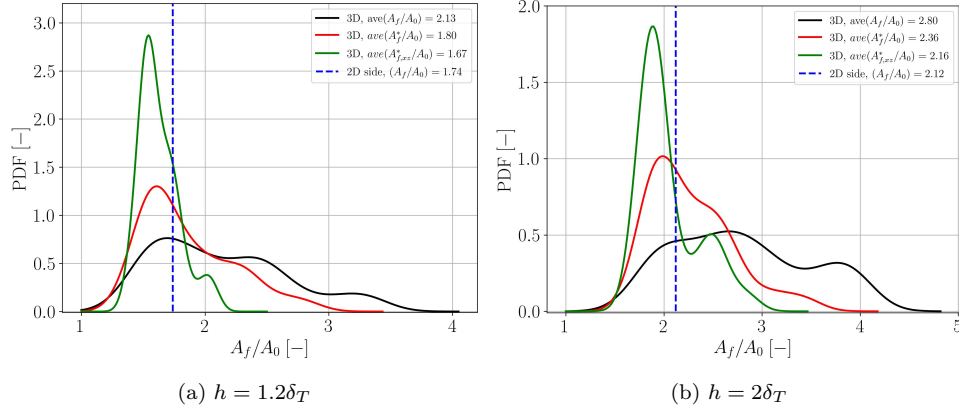


Figure 17: Flame\_05, probability distribution of flame front surface increment  $A_f/A_0$ , with (a)  $h = 1.2\delta_T$  and (b)  $h = 2\delta_T$ .

2

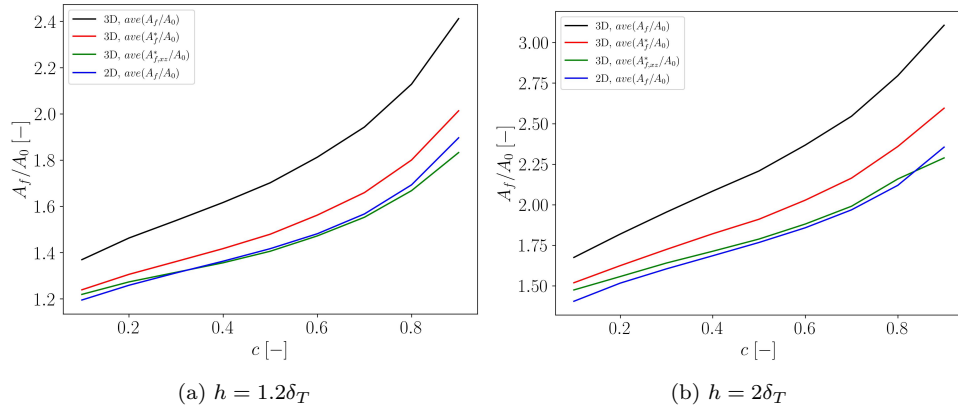


Figure 18: Flame\_05, sensitivity of flame front surface increment  $A_f/A_0$  of slices to isosurface  $c$ .

- 3 The correlation of  $S_c^*/S_L$  with  $A_f^*/A_0$  (from slices with positive average  
 4 curvature  $\kappa_m$ ) is illustrated in Fig. 19. There is a positive linear correlation  
 5 between the two parameters, indicating the contribution from flame surface  
 6 increment to consumption rate. The contribution of the Lewis effect on flame  
 7 front curvature to reaction rate can be evaluated through the amplification  
 8 factor  $I_0 = S_c^*A_0/S_LA_f^*$ . The average value  $I_{0,3D-slice}$  for  $h = 1.2\delta_T$  is 4.12  
 9 with a variance of 0.22. While in the 2D between wall case, the amplification

1 factor  $I_{2D,side}$  is 3.09. The difference comes from the elliptic convex form  
 2 in the 3D case, where preferential diffusion would further increase the local  
 3 reaction because of two positive principal curvatures, while in the 2D case  
 4 there is only one. Likewise, the average amplification factor for 3D slices  
 5 with  $h = 2\delta_T$  is 3.90 with a variance of 0.11, while in the 2D configuration  
 6 between walls  $I_0 = 2.69$ .

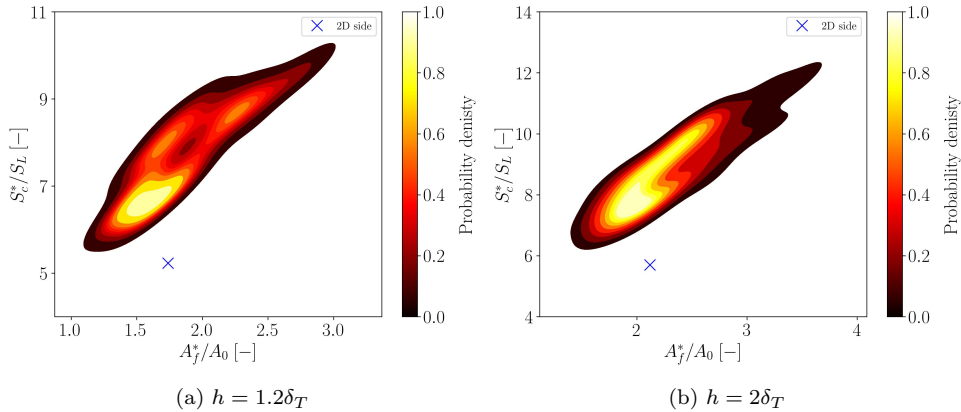


Figure 19: Flame\_05, joint probability distribution of consumption rate  $S_c/S_L$  with flame surface  $A_f/A_0$  for all slices with positive mean curvature, with (a)  $h = 1.2\delta_T$  and (b)  $h = 2\delta_T$ . Blue crosses are from 2D simulations between walls.

7 The statistical analysis of flame dynamics for 3D slices reveals that ac-  
 8 celeration due to both the flame morphology between walls and the Lewis  
 9 effect can be well depicted by the relation  $S_c/S_L = I_0 \times A_f/A_0$ . And the  
 10 value of both the amplification factor and the flame surface increment can  
 11 be approximately predicted with 2D simulations between walls.

## 12 7. Conclusions

13 In this study, we investigated the effect of wall confinement due to two  
 14 adiabatic walls on premixed flames freely propagating in narrow channels  
 15 using compressible simulations. Two lean fuel-air mixtures are considered:  
 16 one with unity Lewis number  $Le = 1$  considering solely hydrodynamic insta-  
 17 bilities, and another with  $Le = 0.5$  to include the thermodiffusive instability.  
 18 To evaluate the impact of confinement on flame instability, we conducted 3D  
 19 numerical simulations (DNS) with varying channel widths and pure 2D sim-  
 20 ulations in the  $xy$  plane (no confinement). Additionally, we extended the

1 Joulin-Sivashinsky model to incorporate friction due to wall confinement  
2 effects into 2D simulations (2D+).

3 By setting a premixed equidiffusive flame ( $Le = 1$ ), results from 3D  
4 simulations show that the confinement effect enhances the hydrodynamic  
5 instability and results in a larger single cusp on the flame front in the  $xy$   
6 plane, while the impact diminishes as the channel width increases, consistent  
7 with previous findings. Moreover, 2D+ model accurately captures the effects  
8 of confinement on flame dynamics at various channel widths and recovers the  
9 flame speed, provided that the flame front remains symmetric between the  
10 walls. For 3D cases where the flame front shape is asymmetric, the flame  
11 curvature in the transverse direction is significantly influenced by strong  
12 curvature between walls. Compared to both pure 2D and 2D+ simulations,  
13 the 3D simulations exhibit a smaller cusp in the  $xy$  plane where forms a  
14 convex curvature between walls, while interactions between cusps in two  
15 directions lead to larger cusp sizes in the  $xy$  plane. These interactions also  
16 impact the flame dynamics in the normal direction. Compared to the 2D  
17 simulation between walls, the stretch induced from the  $xy$  plane alters the  
18 flame surface increment between walls, leading to a longer elongation near  
19 the flame front cusp and a smaller elongation near the tip in the  $xy$  plane.  
20 Moreover, by separating the stretch effect from the plane  $xy$ , it is found  
21 that the flame surface increment between walls is close to that from the 2D  
22 configuration.

23 For  $Le = 0.5$ , 3D simulations with asymmetric flame shapes between  
24 walls are studied. It is found that the Lewis effect amplifies the role of  
25 curvature: regions with positive curvature on the flame front mainly con-  
26 tribute to the global reaction. In addition, flame front curvature between  
27 walls dominates the flame inner structure and results in significantly thin-  
28 ner thermal flame thickness. Overall, the statistical analysis shows that the  
29 flame dynamics between walls are consistent across configurations. Similar  
30 to equidiffusive flames, the flame surface increment between walls (without  
31 the stretch effect from the  $xy$  plane) is close to the value from the 2D con-  
32 figuration between walls. In addition, the acceleration between walls can be  
33 well described by the product of the flame front surface increment and the  
34 amplification factor, both of which can be predicted by the 2D configuration  
35 between walls.

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1 Appendix A. Energy equation in the form of total energy

2 The energy conservation equation in terms of total energy is expressed as:

$$\frac{\partial \rho E_t}{\partial t} + \nabla \cdot [\rho(\mathbf{u} - \mathbf{U}_{ref})E_t] = -\nabla \cdot \mathbf{q} + \nabla \cdot [(\Gamma - p\mathbf{I})(\mathbf{u} - \mathbf{U}_{ref})] \quad (\text{A.1})$$

3 where  $E_t \equiv e + \frac{1}{2}(\mathbf{u} - \mathbf{U}_{ref}) \cdot (\mathbf{u} - \mathbf{U}_{ref})$  and  $e$  is the internal energy defined as

$$e \equiv h - \frac{p}{\rho} = \sum_k Y_k h_k - \frac{p}{\rho} = \sum_k Y_k \left( \int_{T_0}^T C_{p,k} dT + \Delta h_{f,k}^0 \right) - \frac{p}{\rho} \quad (\text{A.2})$$

4 with  $k \in \{F, P\}$  referring to the fuel ( $F$ ) and the product ( $P$ ),  $C_{p,k}$  the species heat capacity at constant pressure (NASA polynomials systems for fuel and product are provided in Appendix B),  $T_0$  the reference temperature  $T_0 = 298.15$  K, and  $\Delta h_{f,k}^0$  the species mass formation enthalpy. For the heat energy flux  $\mathbf{q}$ , we have:

$$\mathbf{q} = -\lambda \nabla T - \rho \sum_k h_k D_k \nabla Y_k \quad (\text{A.3})$$

8 Appendix B. NASA polynomials for F  $\longrightarrow$  P chemistry

The species  $F$  and  $P$  have different NASA 7 polynomials systems [42] for their thermochemical parameters such as the specific heat and enthalpy. NASA polynomials of both fuel and product are listed in the table below. For  $T \leq 1000$  K, we have

Parameters	$F$	$P$
$a_1$	3.543	3.543
$a_2$ - $a_5$	0.0	0.0
$a_6$	0	$-(T_b - T_u)a_1$
$a_7$	0	0
$a_8$	3.543	3.543
$a_9$ - $a_{12}$	0	0
$a_{13}$	0	$-(T_b - T_u)a_1$
$a_{14}$	0	0

Table B.3: NASA polynomials for F  $\longrightarrow$  P chemistry.

$$\frac{C_{p,k}}{R} = a_1 + a_2 T + a_3 T^2 + a_4 T^3 + a_5 T^4,$$

and

$$\frac{h_k}{RT} = a_1 + a_2 \frac{T}{2} + a_3 \frac{T^2}{3} + a_4 \frac{T^3}{4} + a_5 \frac{T^4}{5} + a_6 \frac{1}{T}.$$

Otherwise

$$\begin{aligned} \frac{C_{p,k}}{R} &= a_8 + a_9 T + a_{10} T^2 + a_{11} T^3 + a_{12} T^4, \\ \frac{h_k}{RT} &= a_8 + a_9 \frac{T}{2} + a_{10} \frac{T^2}{3} + a_{11} \frac{T^3}{4} + a_{12} \frac{T^4}{5} + a_{13} \frac{1}{T}. \end{aligned}$$