

Exogenous-endogenous surfactant interaction yields heterogeneous spreading in complex branching networks

Richard Mcnair, Fernando Temprano-Coleto, François Jean Peaudecerf, Frédéric Gibou, Paolo Luzzatto-Fegiz, Oliver E Jensen, Julien R. Landel

▶ To cite this version:

Richard Mcnair, Fernando Temprano-Coleto, François Jean Peaudecerf, Frédéric Gibou, Paolo Luzzatto-Fegiz, et al.. Exogenous-endogenous surfactant interaction yields heterogeneous spreading in complex branching networks. 2024. hal-04833558v1

HAL Id: hal-04833558 https://hal.science/hal-04833558v1

Preprint submitted on 12 Dec 2024 (v1), last revised 24 Jan 2025 (v2)

HAL is a multi-disciplinary open access archive for the deposit and dissemination of scientific research documents, whether they are published or not. The documents may come from teaching and research institutions in France or abroad, or from public or private research centers. L'archive ouverte pluridisciplinaire **HAL**, est destinée au dépôt et à la diffusion de documents scientifiques de niveau recherche, publiés ou non, émanant des établissements d'enseignement et de recherche français ou étrangers, des laboratoires publics ou privés.



Distributed under a Creative Commons Attribution 4.0 International License

SUPPLEMENTAL MATERIAL

Exogenous–endogenous surfactant interaction yields heterogeneous spreading in complex branching networks

Richard Mcnair,¹ Fernando Temprano-Coleto,² François J. Peaudecerf,³ Frédéric Gibou,⁴ Paolo Luzzatto-Fegiz,⁴ Oliver E. Jensen,¹ Julien R. Landel^{5,1,1}

¹Department of Mathematics, University of Manchester, Manchester M13 9PL, UK

²Andlinger Center for Energy and the Environment, Princeton University, Princeton, New Jersey 08544, USA ³Institut de Physique, Université de Rennes, F-35000 Rennes, France

⁴Department of Mechanical Engineering, University of California, Santa Barbara, California 93106, USA

⁵ Universite Claude Bernard Lyon 1, Laboratoire de Mecanique des Fluides et d'Acoustique (LMFA), UMR5509,

CNRS, Ecole Centrale de Lyon, INSA Lyon, 69622 Villeurbanne, France

(Dated: December 10, 2024)

S1 Maze geometry and experimental parameters



Figure S1: Left: Picture at $t^* = 0$ s of the experiment conducted by Temprano-Coleto et al. [1], showing a numbering scheme for the branches. Right: Graph of the mobility f(W) found from (S4g), with the sum truncated at n = 1000, plotted against the branch aspect ratio W in blue, with f(0.94) circled in red. The sum (S4g) converges to 2 significant figures for n < 100 for the values of W shown. We take W = 0.94 to be the aspect ratio of the branches of the maze.

We model the transport dynamics in the maze experiment conducted by Temprano-Coleto et al. [1], as presented in their Fig. 2 and with the corresponding video showing the large maze at [1] (at 1:47 min). A picture of the experiment at what we define to be the initial time, $t^* = 0$ s (with a star denoting dimensional quantities), is shown in Fig. S1 (right), along with a branch numbering scheme. The experimental conditions and protocol are detailed in [1]. In table SI we report estimated ranges of values for the material parameters involved in the experiment. For the length of the solution path, the range of values is estimated by measuring the shortest and longest direct line through the solution path. The error associated with the measurement of lengths from image analysis is less than 1 mm. The parameter values related to the milk properties, the density ρ^* , the dynamic viscosity μ^* and the nominal surface tension γ_0^* (assuming that only natural endogenous surfactant are present at the milk surface), are approximations for the milk-cream mixture used in the experiment [1]. The lowest surface tension of the milk-cream γ_c^* when the surfactant concentration is maximum during the experiment is estimated based on a crude approximation for soapy water. The Marangoni force $S^* = \gamma_0^* - \gamma_c^*$, calculated from the values γ_0^* and γ_c^* , gives a sensible range of values. The viscosity of the milk-cream mixture is approximately 30

¹Corresponding author: julien.landel@univ-lyon1.fr

Parameter	Symbol	Units	Estimated
			range in
			experiments
Length of solution path	L_M^*	$10^{-1} {\rm m}$	1.36 - 1.84
Initial height of liquid film	h_0^*	$10^{-3} \mathrm{m}$	3.0 - 3.5
Acceleration due to gravity	g^*	${ m ms^{-2}}$	9.8
Liquid density	$ ho^*$	$10^3 {\rm ~kg m^{-3}}$	0.98 - 1.0[2]
Dynamic viscosity	μ^*	10^{-2} Pas	3 - 4 [3]
Surface tension of milk-cream mixture	γ_0^*	$10^{-2} \rm N m^{-1}$	3-5[4]
Surface tension of surfactant-laden interface	γ_c^*	$10^{-2} \rm \ N m^{-1}$	2.0 - 2.5
Marangoni force	$S^* = \gamma_0^* - \gamma_c^*$	$10^{-2} \text{ N} \text{m}^{-1}$	0.5 - 3.0

Table SI: Table showing the relevant dimensional parameters of the maze experiment conducted by Temprano-Coleto et al. [1]. The range of values for the Marangoni force, below the double lines, has been calculated from other values in the table. The parameter values related to the milk properties are approximations for the milk-cream mixture used in the experiment [1].

Dimensionless group	Definition	Model	Estimated
		assumption	range in experiments
Aspect ratio of liquid film ϵ	h_{0}^{*}/L_{M}^{*}	≪1	$1.7\times 10^{-2} - 2.4\times 10^{-2}$
Inverse capillary number C	$\epsilon^2 \gamma_c^* / S^*$	$\ll 1$	$9.7 \times 10^{-4} - 1.0 \times 10^{-2}$
Bond number G	$\epsilon^2 \rho^* g^* L_M^{*2} / S^*$	$\gg 1$	10 - 40
Reduced Reynolds number $\epsilon^2 Re$	$\epsilon^2 \rho^* S^* h_0^* / \mu^{*2}$	$\ll 1$	$1.6 \times 10^{-3} - 1.6 \times 10^{-2}$

Table SII: Table of relevant dimensionless groups for the maze experiments [1], calculated using the dimensional parameter values from table SI.

to 50 times the viscosity of water. The main effect is to have slowed down the spreading dynamics of the surfactant Marangoni driven flow compared to experiments with water as the liquid medium. The red dye (red food color McCormick®) used as tracer in the experiments of [1] is water based and fully miscible in the milk-cream mixture. The dye is slightly buoyant in the milk-cream mixture, such that it remains at the surface to closely follow the exogenous surfactant spreading in the maze. We can notice that the fronts of the red dye remain fairly sharp in the experiments, as seen on the videos and images. This is due to the absence of external stirring or perturbations in the laminar flow, and slow molecular diffusion processes. The typical diffusion length is estimated to be less than 1 mm during the time of the experiments, based on a conservative estimate of the surface diffusivity of $5 \times 10^{-9} \text{ m}^2 \text{s}^{-1}$, which is of the order of the spatial resolution in the images.

In table SII we report estimated values for non-dimensional groups. The model we use to simulate the experiment is based on a one-dimensional (1D) lubrication theory approximation to Stokes flow (see section S2). Inertial forces are dominated by viscous forces when the reduced Reynolds number $\epsilon^2 Re$ is small, where $\epsilon \ll 1$ is the aspect ratio of the main flow path, which is consistent with the values taken from table SI. The equation we use for the transport dynamics assumes that gravity dominates over surface tension and surface tension gradients to maintain a flat surface. Any curvature effects of the film surface associated for instance with the contact angle at the side contact lines are assumed negligible. Accordingly, the Bond number G is found to be large and the inverse capillary number C small, which is consistent with these assumptions.

The dimensionless length L_i of branch *i*, for i = 0, 1, 2, ..., 37, is shown in table SIII, where we define one unit as the length of the solution path $L_M^* = 155 \text{ mm}$. These lengths were calculated by counting pixels from the video of the experiment [1], with all dimensional lengths measured with less than 1 mm accuracy. The maze video was taken directly overhead, minimizing optical distortion.

Branch No. (i)	0	1	2	3	4	5	6	7	8	9	10	11	12
$L_i / 10^{-2}$	$L_0/10^{-2}$	9.6	19	6.0	14	6.5	6.4	10	16	3.4	6.3	9.6	3.4
Branch No. (i)	13	14	15	16	17	18	19	20	21	22	23	24	25
$L_i / 10^{-2}$	6.5	13	3.2	3.2	9.9	6.7	6.6	3.2	6.5	13	6.5	13	6.5
Branch No. (i)	26	27	28	29	30	31	32	33	34	35	36	37	
$L_i / 10^{-2}$	6.5	3.3	3.2	6.3	6.9	3.1	3.2	9.5	9.9	3.3	7.9	71	

Table SIII: Table of the branch lengths of the maze, where one unit represents the length of the solution path $(L_M^* = 155 \text{ mm})$. The branch are numbered based on the scheme showed in Fig. S1 (left). The length of the inlet branch L_0 is defined in section S2.2 as a function of δ , the ratio of endogenous to exogenous initial surfactant concentration.

S2 The surfactant transport equation

The spreading of insoluble surfactant at the free surface of a thin two-dimensional (2D) layer of incompressible viscous fluid under the action of surface-tension gradients can be described by a nonlinear diffusion equation, as we briefly explain. We use 2D Cartesian coordinates with horizontal coordinate x^* . A liquid of viscosity μ^* is confined between a horizontal solid wall and a free surface, at height $h^*(x^*, t^*)$ on which a surfactant with concentration $\Gamma^*(x^*, t^*)$ is present at time t^* . The surface tension γ^* of the free surface is assumed to diminish linearly as a function of Γ^* for $\delta\Gamma_c^* \leq \Gamma^* \leq \Gamma_c^*$ from a maximum value γ_0^* to a minimum value γ_c^* , with δ the ratio of endogenous to exogenous initial surfactant concentration such that $\delta\Gamma_c^*$ is the endogenous surfactant concentration initially. We define $S^* = \gamma_0^* - \gamma_c^*$. We consider the evolution of Γ^* and h^* over horizontal distances L_M^* that are much larger than the characteristic film height h_0^* , and define $\epsilon = h_0^*/L_M^*$. Adopting scales appropriate to lubrication theory, we define $x = x^*/L_M^*$, and $t = \epsilon S^* t^*/(L_M^* \mu^*)$. We define the dimensionless film thickness and surfactant concentration as $h(x,t) = h^*/h_0^*$ and $\Gamma(x,t) = \Gamma^*/\Gamma_c^*$, respectively, and the surface tension as $\gamma = (\gamma^* - \gamma_c^*)/S^* = 1 - \Gamma$. Then, when the reduced Reynolds number is sufficiently small $(\epsilon^2 \rho^* S^* h_0^*/\mu^{*2} \ll 1)$, the flow is governed by the coupled evolution equations [5]

$$h_t - \frac{1}{2} \left(h^2 \Gamma_x \right)_r - \frac{1}{3} G \left(h^3 h_x \right)_r + \frac{1}{3} C \left(h^3 h_{xxx} \right)_r = 0, \tag{S1a}$$

$$\Gamma_t - (\Gamma h \Gamma_x)_x - \frac{1}{2} G \left(\Gamma h^2 h_x \right)_x + \frac{1}{2} C \left(\Gamma h^2 h_{xxx} \right)_x = 0,$$
(S1b)

where $C = \epsilon^2 \gamma_c^* / S^*$ is the inverse capillary number and $G = \epsilon^2 \rho^* g^* L_M^* / S^*$ the Bond number, which are dimensionless parameters representing the strength of surface tension and gravity relative to surface tension gradients, respectively. Surface diffusion of surfactant and surface rheological stresses are neglected. Spreading of surfactant from some initial condition can generate deflections of the free surface, although h never exceeds 2 and cannot reach zero in the absence of disjoining pressure, with gravity suppressing deflections at large times [5]. The limit $G \gg 1$ is consistent with the experiment (Table SII). Expanding h and Γ in powers of 1/G about the base state h = 1 and imposing no-flux conditions at the ends of the domain, (S1), to leading order in ϵ , reduces to the nonlinear diffusion equation [6]

$$\Gamma_t = \frac{1}{4} \left(\Gamma \Gamma_x \right)_x,\tag{S2}$$

which can be rearranged as $\Gamma_t = (\Gamma^2)_{xx}/8$. This captures the essential features of self-induced spreading of an insoluble surfactant on a thin film via Marangoni forces.

S2.1 Surfactant transport along a channel

The factor of 1/4 in (S2) is appropriate for a thin film, but it takes no account of the lateral no-slip boundary conditions that constrain spreading along a channel in a maze having rectangular cross section with finite width-to-height aspect ratio W. We refine the approximation to determine the mobility f(W)of the surfactant as follows, where $f \to 1/4$ in the thin-film limit in which $W \to \infty$. We again assume (i) no out-of-plane deflection of the air-liquid interface and no externally imposed pressure gradient, so that the volume flux along the channel is uniformly zero, and (ii) the channel is long compared to its width and height so that rapid lateral Marangoni spreading quickly eliminates lateral surfactant concentration

gradients [7]. Under (i) and (ii), the axial velocity component $u^*(x^*, y^*, z^*, t^*)$ is driven by a surfactant gradient $-\Gamma_{x^*}^*(x^*, t^*)$ moving the bulk liquid forward and a counter pressure gradient $-p_{x^*}^*(x^*, t)$ driving a return flow in the bulk (arising via incompressibility from the no-interfacial-deflection condition and the fact that the channels are closed at all ends), where y^* and z^* are coordinates spanning the cross-section of the channel in the transverse and vertical directions, respectively. Adopting scalings introduced above, the leading-order axial velocity component satisfies $\nabla^2_{\perp} u \equiv u_{yy} + u_{zz} = p_x$ across the cross-section of the channel, with u = 0 on the bottom and lateral walls of the channel $(z = 0, y = \pm W/2)$ and the shear stress condition $u_z = -\Gamma_x$ on the interface at z = 1. Linearity allows the field to be decomposed as $u(x, y, z, t) = -p_x(x, t)u^b(y, z) - \Gamma_x(x, t)u^m(y, z)$ where $\nabla^2_{\perp} u^b = -1$ and $u^b_z = 0$ on z = 1, and $\nabla^2_{\perp} u^m = 0$ and $u^m_z = 1$ on z = 1. Averaging u over the rectangular cross-section defines volume fluxes $Q^{b}(W)$ and $Q^{m}(W)$, and condition (i) then requires $0 = -Q^{\bar{b}}p_{x} - Q^{m}\Gamma_{x}$, which determines p_{x} in terms of Γ_x . Finally, the surfactant field is advected by the transversely-averaged surface velocity $\overline{u}_s \equiv W - 1 \int_{-W/2}^{W/2} u(x, y, 1, t) \, \mathrm{d}y$, which can be expressed as $\overline{u}_s = -p_x \overline{u}_s^b - \Gamma_x \overline{u}_s^m$. Eliminating p_x recovers the nonlinear diffusion equation

$$\Gamma_t = f(W)(\Gamma\Gamma_x)_x, \quad \text{where} \quad f(W) = \overline{u}_s^m - (\overline{u}_s^b Q^m / Q^b).$$
 (S3)

In the limit of large W, $u^b = z - \frac{1}{2}z^2$, $u^m = z$, $\overline{u}_s^b = \frac{1}{2}$, $\overline{u}_s^m = 1$, $Q^b = 1/3$ and $Q^m = 1/2$ giving $f = \frac{1}{4}$. For finite W, we use separation of variables to obtain the following expressions for u^b , u^m , \overline{u}_s^b , \overline{u}_s^m ,

 Q^b, Q^m and f:

$$u^{b}(y,z) = -\frac{1}{2}(z^{2} - 2z) \\ -\sum_{n=1}^{\infty} \frac{2\sin\left[(n - \frac{1}{2})\pi z\right] \left[\sinh\left[(n - \frac{1}{2})\pi(y + W/2)\right] - \sinh\left[(n - \frac{1}{2})\pi(y - W/2)\right]\right]}{\sinh\left[(n - \frac{1}{2})\pi W\right] (n - \frac{1}{2})^{3}\pi^{3}};$$
 (S4a)

$$u^{m}(y,z) = -\sum_{n=1}^{\infty} \frac{W(-1)^{n} \cos\left(\frac{2(n-\frac{1}{2})\pi}{W}y\right) \sinh\left(\frac{2(n-\frac{1}{2})\pi z}{W}\right)}{(n-\frac{1}{2})^{2}\pi^{2} \cosh\left(\frac{2(n-\frac{1}{2})\pi}{W}\right)};$$
(S4b)

$$\overline{u}_{s}^{b} = \frac{1}{2} + \sum_{n=1}^{\infty} \frac{2(-1)^{n} [2\cosh\left[(n-\frac{1}{2})\pi W\right] - 2]}{\sinh\left[(n-\frac{1}{2})\pi W\right](n-\frac{1}{2})^{4}\pi^{4}W};$$
(S4c)

$$\overline{u}_{s}^{m} = \sum_{n=1}^{\infty} \frac{W \tanh\left[2(n-\frac{1}{2})\pi/W\right]}{(n-\frac{1}{2})^{3}\pi^{3}};$$
(S4d)

$$Q^{b} = 1/3 - \sum_{n=1}^{\infty} \frac{4(\cosh\left[(n-\frac{1}{2})\pi\right] - 1)}{\sinh\left[(n-\frac{1}{2})\pi W\right](n-\frac{1}{2})^{5}\pi^{5}W};$$
(S4e)

$$Q^{m} = \sum_{n=1}^{\infty} \frac{W^{2} (\cosh\left[2(n-\frac{1}{2})\pi/W\right] - 1)}{2(n-\frac{1}{2})^{4}\pi^{4}\cosh\left[2(n-\frac{1}{2})\pi/W\right]};$$
(S4f)

$$f(W) = \sum_{n=1}^{\infty} \frac{W \tanh\left(\frac{2(n-\frac{1}{2})\pi}{W}\right)}{(n-\frac{1}{2})^3 \pi^3} - \frac{\sum_{n=1}^{\infty} \frac{W^2 (\cosh\left[2(n-\frac{1}{2})\pi/W\right] - 1)}{2(n-\frac{1}{2})^4 \pi^4 \cosh\left[2(n-\frac{1}{2})\pi/W\right]}}{1/3 - \sum_{n=1}^{\infty} \frac{4(\cosh\left[(n-\frac{1}{2})\pi W\right] - 1)}{\sinh\left[(n-\frac{1}{2})\pi W\right](n-\frac{1}{2})^5 \pi^5 W}} \left(\frac{1}{2} + \sum_{n=1}^{\infty} \frac{2(-1)^n [2\cosh\left[(n-\frac{1}{2})\pi W\right] - 2]}{\sinh\left[(n-\frac{1}{2})\pi W\right](n-\frac{1}{2})^4 \pi^4 W}\right).$$
 (S4g)

Fig. S1 (left) shows that for W = 0.94, which is the approximate aspect ratio of the channel in the experiment, $f \approx 0.15$, which indicates a 40% reduction approximately in the surfactant mobility in comparison to the wide-channel limit.

In addition to gravitational suppression of interfacial deflections, as used to derive (S2) from (S1), surface tension can also have an significant role in suppressing deflections in a channel flow via pinning of contact lines to the channel edges. Any interfacial deflection will have two components of curvature: a short length comparable to the channel width; and a longer axial scale induced by competition between viscous and capillary forces, as represented in (S2a). The former can be expected to dominate over the latter, as it acts over shorter lengthscales, and it will act alongside gravity in maintaining a near-uniform liquid depth.

Transport of a single surfactant species in a shallow channel (S2) can be expressed dimensionally as $\Gamma_{t^*}^* + (u^*\Gamma^*)_{x^*} = 0$, where $u^* = -\frac{1}{4}(h_0^*A^*/\mu^*)\Gamma_{x^*}^*$. Here $A^* = S^*/\Gamma_c^*$ is the activity of the surfactant (the magnitude of the slope of the assumed-linear relationship between surface tension and surfactant concentration). The equivalent model for a mixture of two surfactant species with concentrations Γ_1^* and Γ_2^* is $\Gamma_{i,t}^* + (u^*\Gamma_i^*)_{x^*} = 0$ for i = 1, 2 with $u^* = -\frac{1}{4}(h_0^*/\mu^*)(A_1^*\Gamma_{1,x^*}^* + A_2^*\Gamma_{2,x^*}^*)$, again assuming a linear equation of state. Defining $\Gamma^* = (A_1^*\Gamma_1^* + A_2^*\Gamma_2^*)/(A_1^* + A_2^*)$, $A^* = A_1^* + A_2^*$ and summing the evolution equations weighted respectively by A_1^* and A_2^* recovers exactly the evolution equation for a single species Γ^* , equivalent to (S2). While for simplicity we assume that endogenous and exogenous surfactant have identical properties in the present analysis, the model accommodates two non-diffusing species with different activities.

S2.2 Surfactant transport in a maze

We now extend the 1D model to show that exogenous surfactant added to pre-existing endogenous surfactant can simulate the maze-solving behavior seen in the experiments [1]. This behavior consists of the exogenous surfactant spreading from the end of branch 0 (see numbering scheme in Fig. S1, left) to the start of branch 37, while also not spreading to the end of the lateral branches.

To model the maze-solving behavior of the out-of-equilibrium surfactant field, we solve the simplified time-dependent surfactant transport equation (S3) in a network of connected 1D domains (1DDs). Equation (S3) solves the transport of both the exogenous and endogenous surfactants, as they are assumed to form a single field. Each 1DD represents one of the 36 branches of the maze, where the length of the *i*th 1DD, L_i , is the length of the *i*th branch. These lengths are given in table SIII. Additionally, we simulate the square branches 0 and 37 at the inlet and outlet of the maze, respectively, with two more 1DDs of longer lengths. The length of the outlet 1DD, L_{37} , is calculated to simulate the surface area of branch 37 in the experiment. Counting the number of pixels P_{37}^* constituting branch 37 in the image in Fig. S1 (left) and, for example P_1^* , the number of pixels that constitute branch 1, we define $L_{37} = L_1 P_{37}^*/P_1^*$. The length of the inlet 1DD simulating branch 0, L_0 , is estimated independently to represent the mass of exogenous surfactant M_{ex}^* introduced in this branch at the start of the experiment, as discussed below.

We use subscripts to number the 1DDs, so that for example $\Gamma_0(x_0, t)$ denotes the concentration in the inlet 1DD, for $0 \le x_0 \le L_0$ along the branch, and at time t. Each 1DD receives a coordinate direction such that, for example, along 1DD *i* the coordinate direction is x_i , and this coordinate increases in the direction away from the junction nearest to the inlet 1DD. We solve the governing equation (S3) for the surfactant transport equation throughout the 1D network along with the following initial, continuity and boundary conditions, which simulate the conditions in the maze experiment,

$$\Gamma_0(x_0, 0) = 1 \quad \text{for all } 0 \le x_0 \le L_0,$$
(S5)

$$\Gamma_1(x_1, 0) = \begin{cases} \frac{1}{2}(1-\delta)\cos\left(\pi x_1/x_f\right) + \frac{1}{2}(1+\delta) & 0 \le x_1 \le x_f, \\ \delta & x_f < x_1 \le L_1. \end{cases}$$
(S6)

$$\Gamma_i(x_i, 0) = \delta \quad \text{for all } 0 \le x_i \le L_i, \quad \text{for } i = 2, 3, \dots, 37.$$
(S7)

$$\frac{\partial}{\partial x_0} \Gamma_0(0,t) = 0, \quad \frac{\partial}{\partial x_{37}} \Gamma_{37}(L_{37},t) = 0, \tag{S8}$$

$$\frac{\partial}{\partial x_i} \Gamma_i(L_i, t) = 0 \tag{S9}$$

for all 1DDs *i* not connecting to a junction at L_i ,

$$\Gamma_j(0,t) = \Gamma_i(L_i,t) \tag{S10}$$

for every 1DD *i* terminating at a junction, and for all 1DDs $j \in J(i)$ where J(i) is the set of all branches such that $x_j = 0$ locates the same junction as $x_i = L_i$. Finally,

$$\frac{\partial}{\partial x_i}\Gamma_i(L_i, t) = \sum_{j \in J(i)} \frac{\partial}{\partial x_j}\Gamma_j(0, t),$$
(S11)

for the same set of 1DDs as (S10). The initial, continuity and boundary conditions stated above, (S5)–(S11), closely model the experimental conditions described in section S1. The initial condition in the 1DD representing the inlet branch, i = 0, is that the surfactant concentration is uniformly equal to 1 (S5). All the other 1DDs have a uniform surfactant concentration of smaller value $\delta < 1$, which represents the initial ratio of concentrations of endogenous surfactant to exogenous surfactant (S7). The only exception is in the 1DD which connects the inlet 1DD to the rest of the maze, where a short section of length $x_f = 0.032$ smoothly connects the two uniform surfactant concentrations with half a cosine wave (S6). The dynamics are driven by the gradient of the surfactant concentration, so we impose the initial condition to be C^1 continuous so that the initial velocity is defined everywhere. The smooth profile in branch 1 has been added to avoid numerical issues at early times. Its influence on the overall transport dynamics is negligible. The boundary condition at unconnected ends of 1DDs in the network is no flux of surfactant, such as at the start of the inlet and end of the outlet branches (S8), and at the end of the peripheral 1DDs (S9). At junctions where multiple 1DDs are connected, the conditions are continuity of surfactant concentration (S10), and continuity of flux of surfactant (S11).

S2.3 Boundary between the exogenous and endogenous surfactants

As shown in [8], in the absence of surface diffusion, the front of exogenous surfactant, added to a surface with a pre-existing endogenous surfactant concentration, moves like a material element transported at the surface velocity generated through the surfactant-induced Marangoni stress. To simulate the experiment, the evolution of the front location $x_j = \tilde{\Lambda}_j(t)$ (the tilde denotes a simulated solution to avoid confusion with the experimental data Λ_j) of exogenous surfactant in 1DD j, given (S3), satisfies

$$\frac{\mathrm{d}\tilde{\Lambda}_{j}(t)}{\mathrm{d}t} = -f(W)\frac{\partial}{\partial x_{j}}\Gamma(x_{j} = \tilde{\Lambda}_{j}(t), t), \qquad (S12)$$

for all 1DDs j where a front exists. When $\Lambda_j(t) = L_j$, the front ceases to exist in 1DD j, and appears in all 1DDs $i \in J(j)$, where J(j) is the set of 1DDs originating at the head junction of 1DD j. The initial conditions are that initially a front only exists in 1DD 1, and

$$\Lambda_1(0) = x_f,\tag{S13}$$

and we impose that $\widetilde{\Lambda}_i(t_b) = 0$ whenever the front in 1DD *i* appears at time $t = t_b$. The equation (S12) is solved simultaneously with (S3). The maze simulation is completed when $\widetilde{\Lambda}_{36} = L_{36}$.

S2.4 Key non-dimensional parameters in the model

The model has three unknown parameters to be determined empirically. The first is δ , the ratio of initial endogenous surfactant concentration to the reference exogenous surfactant concentration. The second is τ_{end} , which is the ratio of simulation completion time to experiment completion time t_{ref} . We use τ_{end} to improve the comparison to the experiment of the dynamic behavior of exogenous surfactant along the solution path (see section S6 for further details), but τ_{end} does not affect the model dynamics significantly. The third *a priori* unknown parameter is L_0 , the length of the inlet 1DD. As detailed below, the length L_0 is used to simulate the mass of exogenous surfactant M_{ex}^* in the inlet branch 0.

Examining the video of the experiment [1], we observe complex dynamics occurring in the inlet branch 0 at early times. The exogenous surfactant is not added instantaneously, nor is it added to the entire area initially occupied by the dye. Part of branch 0 is unoccupied by the dye, and remains unoccupied throughout the duration of the experiment. Moreover, our quantitative analysis of how the dye front moves at early times from branch 0 to branch 1 shows a very fast dynamics, with a short time scale characteristically different from the dynamics throughout the internal branches of the maze. We assume that this rapid dynamics is associated with the inlet branch being a large square, rather than a narrow channel, such that the dynamics is mostly 2D, rather than 1D as assumed in our model. To avoid adding unnecessary complexity to our model, we do not model this early time dynamics at the inlet branch as it has limited impact on the long-time dynamics throughout the maze. We find that the overall maze dynamics is well-captured by a 1D inlet branch, whose length is slightly different from the geometric

value. Nevertheless, we still assume that the inlet branch is occupied uniformly by exogenous surfactant at t = 0. Thus, the inlet branch length is chosen to represent the mass of exogenous surfactant deposited at t = 0, rather than its geometric size. The actual size of branch 0 is not crucial to explaining the key behavior of the experiment (unlike branch 37). The role of branch 0 is to act as a (finite) reservoir of exogenous surfactant.

Owing to conservation of mass, we can estimate the exogenous mass of surfactant M_{ex}^* , which is used to determine L_0 , by examining the video of the experiment at late times. At late times, the surface tension throughout the maze approaches a constant value. Under the modelling assumption that the material parameters of the exogenous surfactant are the same as the endogenous surfactant, this uniform surface tension means that the concentrations of both species of surfactant also evolve to a constant value, which we call Γ_u^* . Furthermore, under the assumptions that the surfactant species do not mix and that the red dye closely follows the exogenous–endogenous interface, the endogenous surfactant occupies the area of the maze which is white, and the exogenous surfactant occupies the area of the maze which is red. Calling the dimensional masses of exogenous and endogenous surfactant M_{ex}^* and M_{en}^* respectively, we make the approximations that

$$M_{en}^* \approx \int_{A_w^{\infty^*}} \Gamma_u^* \, \mathrm{d}S^* = \Gamma_u^* A_w^{\infty^*}, \quad \text{and} \quad M_{ex}^* \approx \int_{A_r^{\infty^*}} \Gamma_u^* \, \mathrm{d}S^* = \Gamma_u^* A_r^{\infty^*}, \tag{S14}$$

where $A_w^{\infty*}$ and $A_r^{\infty*}$ are the surface areas of the maze not occupied by the dye, and occupied by the dye respectively when the system reaches a steady state at the end of the video. The concentration Γ_u^* cancels when calculating the ratio of masses, which we exploit to impose the condition that the ratio of dimensionless masses in our model to be the same as the ratio of masses in the experiment. The non-dimensional exogenous surfactant mass relates to the dimensional mass by $M_{ex}^* = M_{ex}\Gamma_c^*L_M^*W^*$, where W^* is the dimensional width of the maze branches, with a similar identity holding for the endogenous surfactant mass M_{en} . Thus, $M_{ex}/M_{en} = A_r^{\infty*}/A_w^{\infty*}$ provides an identity for M_{ex} in terms of δ

$$M_{ex} = M_{en} \frac{A_r^{\infty *}}{A_w^{\infty *}} = \delta \left[\sum_{i=1}^N L_i - x_f \right] \frac{A_r^{\infty *}}{A_w^{\infty *}},\tag{S15}$$

where the quantity $\left[\sum_{i=1}^{N} L_i - x_f\right]$ is the total length of all the 1DDs in the model not initially occupied by the exogenous surfactant. From the initial conditions, the exogenous surfactant mass satisfies

$$M_{ex} = \int_0^{L_0} \Gamma_0(x_0, 0) dx_0 + \int_0^{x_f} \Gamma_1(x_1, 0) dx_1$$

= $\int_0^{L_0} 1 dx_0 + \int_0^{x_f} \left[\frac{1}{2} (1 - \delta) \cos(\pi x_1 / x_f) + \frac{1}{2} (1 + \delta) \right] dx_1 = L_0 + \frac{1 + \delta}{2} x_f.$ (S16)

Using (S15) and (S16), the dimensionless length of the inlet 1DD (i = 0) can be estimated as

$$L_{0} = \delta \left[\sum_{i=1}^{N} L_{i} - x_{f} \right] \frac{A_{r}^{\infty *}}{A_{w}^{\infty *}} - \frac{1+\delta}{2} x_{f},$$
(S17)

where $A_r^{\infty^*}$ and $A_w^{\infty^*}$, are measured from the video, the dimensionless lengths L_i , i = 1, ..., N are taken from table SIII. We note that the precise value of x_f (chosen as 0.032) has negligible impact on the maze dynamics. The remaining dimensionless parameters δ and τ_{end} are determined through comparison with the experiment (see section S6).

S3 Numerical methods

S3.1 Spatial discretisation

We model the transport dynamics in the maze by the time-dependent equation (S3) along a connected network of 1DDs, subject to the initial, continuity and boundary conditions (S5)-(S11) presented in

section S2.2. The endogenous–exogenous surfactant interface, assumed to be the front of the red dye, is calculated through (S12) under the initial condition (S13). We solve a discretised approximation of the continuum formulation of the problem on a network having the same topology as the maze, exploiting the methodology of mimetic finite differences. We represent the maze as a directed graph. Every junction and every unconnected end of a 1DD is represented by a vertex, and within each 1DD we add vertices to refine the discretisation with oriented edges between them. The number of vertices \mathbb{N}_i within the *i*th 1DD is chosen such that these vertices are equally spaced at a distance $\Delta x_i = L_i/(\mathbb{N}_i + 1)$, where Δx_i is as close as possible to a chosen global discretisation value Δx such that it gives an integer \mathbb{N}_i . This is accomplished by

$$\Delta x_i = \frac{L_i}{\operatorname{round}(L_i/\Delta x)}.$$
(S18)

As a convention, we choose the orientation of every edge to point away from the vertex nearest to the inlet. Following the orientation of each edge, its vertex nearest to the inlet is designated as tail vertex, and its other vertex is designated as head vertex. The topology of the directed graph is encapsulated by its signed incidence matrix which is defined by

$$A_{ij} = \begin{cases} +1 & \text{Edge } i \sim \text{Vertex } j | \text{Edge } i \text{ points towards Vertex } j, \\ -1 & \text{Edge } i \sim \text{Vertex } j | \text{Edge } i \text{ points away from Vertex } j, \\ 0 & \text{Edge } i \nsim \text{Vertex } j, \end{cases}$$
(S19)

with *i* and *j* two integers such that $1 \le i \le m$, $1 \le j \le n$ for a graph with *m* edges and *n* vertices, and where ~ and ~ mean 'connected to' and 'not connected to', respectively. Each row of A corresponds to an edge of the graph and has exactly two non-zero entries: +1 corresponding to the head vertex of the edge, and -1 corresponding to the tail vertex of the edge. We designate A_u the unsigned incidence matrix, which is the defined via $A_{u(ij)} = |A_{ij}|$. The labelling of edges and vertices is arbitrary. A subset of adjacent vertices is represented by a vector (or chain) **D** of length *n* whose components are 1 for every vertex in the subset and zero otherwise. Non-zero components of the chain AD identify the oriented edges bounding the domain represented by **D**.

To define physically meaningful operators on the graph, we include metric information describing the physical system represented by the graph. We define the edge length metric tensor as the diagonal matrix of size $m \times m$

$$\mathsf{L} = \operatorname{diag}(\Delta x_0, \dots, \Delta x_0, \dots, \Delta x_1, \dots, \Delta x_1, \dots, \Delta x_2, \dots),$$
(S20)

where Δx_0 , Δx_1 , etc. are the lengths of the edges of the graph, each obtained from (S18), ordered the same as the rows of A. We define the associated vertex length metric tensor as

$$\mathsf{V} = \operatorname{diag}\left(\frac{1}{2}\mathsf{A}_{u}^{T}\mathsf{L}\mathbb{1}_{e}\right),\tag{S21}$$

where $\mathbb{1}_{e}$ is the *m*-vector (or chain) $(1, 1, \ldots, 1)$ identifying all the edges of the graph. The quantity V_{jj} is half the sum of edge lengths of all edges connected to vertex j. We define Γ_{v} as the *n*-vector (co-chain) of surfactant concentrations defined on the *n* vertices of the graph, and Γ_{v}^{2} as the component-wise square of this vector. The incidence matrix can be used as an operator which can act on Γ_{v}^{2} . For instance, $A\Gamma_{v}^{2}$ is a differencing operation on Γ_{v}^{2} that returns a co-chain of variables defined on the edges of the graph, where the value on each edge is the difference of the square of the concentration on the bounding vertices of the edge. Thus, using (S20) we can define a gradient operator on Γ_{v}^{2} as $L^{-1}A\Gamma_{v}^{2}$. This is equivalent to a second-order-accurate central-difference approximation of the gradient of Γ_{v}^{2} defined at the midpoint of each edge. We can therefore approximate the continuous flux $-f(W)(\Gamma^{2})_{x}/2$ in the rearranged version of (S3) by the discrete expression

$$\mathbf{q}_e = -\frac{f(W)}{2} \mathsf{L}^{-1} \mathsf{A} \mathbf{\Gamma}_v^2. \tag{S22}$$

The flux \mathbf{q}_e is defined on the edges of the graph. The vector $\nabla \mathbf{\Gamma}_v$ can be interpreted as the mass of sufactant associated with each vertex. Then $\langle \mathbf{D}, \mathbf{\Gamma}_v \rangle \equiv \mathbf{D}^T \nabla \mathbf{\Gamma}_v$ can be interpreted as the mass of surfactant in the simply connected domain represented by the chain \mathbf{D} . Mass conservation at each individual vertex (in the absence of sources and sinks) is expressed as

$$\frac{\mathrm{d}}{\mathrm{d}t} \mathsf{V} \mathbf{\Gamma}_v = \mathsf{A}^T \mathbf{q}_e. \tag{S23}$$

Here, $A^T \mathbf{q}_e$ returns a co-chain of variables defined on the vertices of the graph giving the net amount of flux entering each vertex. Indeed, each row of A^T corresponds to a vertex of the graph, where the components in the row are either +1 or -1 for each edge (corresponding to its column) pointing towards or pointing away from that vertex, respectively. Equivalently, from (S23), $-V^{-1}A^{T}$ is the analogue of the divergence operator applied to all the vertices. Therefore, for a fixed metric V in time, the discrete analogue of the surfactant transport equation (S3) in a maze of a given topology is

$$\frac{\mathrm{d}\mathbf{\Gamma}_v}{\mathrm{d}t} = \mathbf{V}^{-1}\mathbf{A}^T\mathbf{q}_e = -\frac{f(W)}{2}\mathbf{V}^{-1}\mathbf{A}^T\mathbf{L}^{-1}\mathbf{A}\mathbf{\Gamma}_v^2.$$
(S24)

Left-multiplying (S24) by $\mathbf{D}^T \mathbf{V}$ gives

$$\frac{\mathrm{d}}{\mathrm{d}t} \langle \mathbf{D}, \mathbf{\Gamma}_v \rangle = (\mathbf{A}\mathbf{D})^T \mathbf{q}_e.$$
(S25)

We recognise $(AD)^T q_e$ as the net flux entering the boundary of the domain represented by **D**. This provides a discrete analogue of the divergence theorem on the graph. When implemented numerically, this formulation conserves mass to machine precision.

S3.2Temporal discretisation

We solve (S24) using a semi-implicit time-stepping finite-difference scheme. At the (k + 1)th time step, we approximate Γ_v^2 as $Q\Gamma_v^{(k+1)}$ where $Q = \text{diag}(\Gamma_v^{(k)})$. Therefore, (S24) can be approximated by

$$\frac{\mathbf{\Gamma}_{v}^{(k+1)} - \mathbf{\Gamma}_{v}^{(k)}}{\Delta t} = -\frac{f(W)}{2} \mathbf{V}^{-1} \mathbf{A}^{T} \mathbf{L}^{-1} \mathbf{A} \mathbf{Q} \mathbf{\Gamma}_{v}^{(k+1)}.$$
(S26)

The solution at the (k + 1)th time step is then obtained by solving the linear system

$$\left(\mathsf{I} + \frac{f(W)}{2}\Delta t\mathsf{V}^{-1}\mathsf{A}^{T}\mathsf{L}^{-1}\mathsf{A}\mathsf{Q}\right)\mathbf{\Gamma}_{v}^{(k+1)} = \mathbf{\Gamma}_{v}^{(k)},\tag{S27}$$

where I is the $n \times n$ identity matrix. As discussed, the boundary conditions (S9) to (S11) are implemented automatically within the formulation (S27). The initial conditions are imposed by projecting (S5)-(S7)onto the vertices of the graph, whereby we obtain the initial concentration vector $\mathbf{\Gamma}_{v}^{(0)}$. This is done using the same order for the components of $\Gamma_v^{(0)}$ as we have ordered the columns of A (this ordering is arbitrary but must be consistent). The numerical scheme is found to converge with second-order spatial accuracy following Δx^2 , with $\Delta x \to 0$. This is consistent with Brio et al. [9], who found that the rows of (S24) are a second-order accurate approximation of the Laplacian at each vertex of a graph.

Equation (S12) is solved simultaneously with (S27) to keep track of the fronts of exogenous surfactant. We define $\Lambda^{(k)}$ as the vector of locations of exogenous surfactant fronts. This vector has the same number of components as the number of edges in the graph. To impose the initial conditions (S13), every component of $\Lambda^{(0)}$ is zero except the $|x_f/\Delta x_1|$ components which represent the first $\lfloor x_f/\Delta x_1 \rfloor$ edges in 1DD 1, where |a| means the floor of a, returning the largest integer smaller than a. These components of $\mathbf{\Lambda}^{(0)}$ are set to Δx_1 . We set the $\lfloor x_f/\Delta x_1 \rfloor + 1$ component in 1DD 1 equal to $x_f - \Delta x_1 \lfloor x_f/\Delta x_1 \rfloor$.

We also equip our scheme with an indicator vector $I^{(k)}$ which has the same number of components as there are edges. Each component is either 1 if a front of the exogenous surfactant is present in that edge or 0 if not. We set the $|x_f/\Delta x_1| + 1$ component of $I^{(0)}$ in 1DD 1 to 1, and every other component to 0. The numerical scheme which solves equation (S12), relating time-step k to k-1, is

$$\boldsymbol{\Lambda}^{(k)} = \boldsymbol{\Lambda}^{(k-1)} - f(W)\boldsymbol{I}^{(k)} \circ \boldsymbol{\mathsf{L}}^{-1}\boldsymbol{\mathsf{A}}\boldsymbol{\Gamma}_{v}^{(k-1)}, \tag{S28}$$

where \circ is the component-wise product of vectors. The *j*th component of $\mathbf{I}^{(k-1)} \circ \mathbf{\Lambda}^{(k)}$, if it is non-zero, corresponds to an exogenous surfactant front within the *j*th edge of the graph. After time-step k we check whether every non-zero component of $I^{(k-1)} \circ \Lambda^{(k)}$ is within some small tolerance ε of Δx_i , where *i* is the index of the 1DD where the edge corresponding to the component is located. If $|\Delta x_i - \Lambda_i^{(k)}| < \varepsilon$ for this component j, we 'hand over' this surfactant front to the connecting edges by setting the component of $I^{(k)}$ for that edge to 0, and the forward connecting edges to 1. The other components of $I^{(k)}$ remain the same as $I^{(k-1)}$. To reduce error we also set the components corresponding to the forward connecting edges of $\Lambda^{(k)}$ to $\Delta x_i - \Lambda_j^{(k)}$. We also take into account receding effects by testing whether or not the fronts have receded to the start of any edge, in which case we pass the front location back to the previous edge following a similar algorithm. The location of the exogenous surfactant front within any 1DD at time-step k is given by the sum of the components of $\Lambda^{(k)}$ corresponding to the edges representing that 1DD. If we call J(i) the set of indices corresponding to the edges discretising 1DD i, and we assume a uniform time step Δt ,

$$\widetilde{\Lambda}_i(k\Delta t) = \sum_{j\in J(i)} \mathbf{\Lambda}^{(k)}(j).$$
(S29)

S4 Linearisation and modal decomposition of the transport model

S4.1 Linear modes

We can approximate the nonlinear diffusion equation (S3) in the limit of small gradients of surfactant concentration as a linear diffusion equation. If we assume that the surfactant concentration has the form $\Gamma = \overline{\Gamma} + \widehat{\Gamma}(x, t)$ where $\widehat{\Gamma} \ll \overline{\Gamma}$, the nonlinear diffusion equation projected onto the discrete representation of the maze (S24) becomes, to leading order,

$$\frac{\mathrm{d}\hat{\boldsymbol{\Gamma}}}{\mathrm{d}t} = -\kappa \boldsymbol{\mathsf{V}}^{-1} \boldsymbol{\mathsf{A}}^T \boldsymbol{\mathsf{L}}^{-1} \boldsymbol{\mathsf{A}}\hat{\boldsymbol{\Gamma}},\tag{S30}$$

where $\kappa = f(W)\overline{\Gamma}$, and we identify the Laplacian operator

$$\kappa \mathsf{V}^{-1} \mathsf{A}^T \mathsf{L}^{-1} \mathsf{A}. \tag{S31}$$

If we define $\mathbf{U} = V^{1/2} \hat{\mathbf{\Gamma}}$ then (S30) becomes

$$\mathbf{U}_t = -\kappa \mathbf{V}^{-1/2} \mathbf{A}^T \mathbf{L}^{-1} \mathbf{A} \mathbf{V}^{-1/2} \mathbf{U}.$$
 (S32)

The operator $\kappa V^{-1/2} A^T L^{-1} A V^{-1/2}$ is symmetric, and therefore has orthogonal eigenvectors, so that $\mathbf{U}_i^T \mathbf{U}_j = \delta_{ij}$ for normalised eigenvectors \mathbf{U}_i and \mathbf{U}_j , with distinct eigenvalues λ_i and λ_j (as the maze is not symmetric, all eigenvalues are distinct), and where δ_{ij} is the Kronecker delta. Thus, we can express $\hat{\Gamma}$ in terms of orthonormal eigenvectors $\phi_i = V^{-1/2} \mathbf{U}_i$ of (S31) that satisfy

$$\boldsymbol{\phi}_i^T \boldsymbol{\mathsf{V}} \boldsymbol{\phi}_j = \langle \boldsymbol{\phi}_i, \boldsymbol{\phi}_j \rangle = \delta_{ij}. \tag{S33}$$

This defines the natural inner product for the Laplacian operator (S31), which is the operator governing the linearised dynamics of the transport in the maze. The Laplacian (S31) is positive semi-definite, with a single zero eigenvalue corresponding to a constant eigenvector representing steady state concentrations as $t \to \infty$.

We can use a truncated sum of the first N eigenvectors to construct an approximate solution for the vector of surfactant concentrations defined on the vertices of the graph,

$$\Gamma(t) = \sum_{i=0}^{N} A_i \phi_i e^{-\lambda_i t},$$
(S34)

where the coefficients A_i are the amplitudes of the eigenvectors ϕ_i , and λ_i are the corresponding eigenvalues of (S31). Utilising the orthogonality of these eigenvectors with respect to this inner product we can project an initial concentration profile $\Gamma(0)$ onto this basis. The amplitudes for the *i*th mode will be given by

$$A_i = \langle \boldsymbol{\phi}_i, \boldsymbol{\Gamma}(0) \rangle. \tag{S35}$$

We find the modes look similar to cosine waves through the solution path of the maze. The gradients of the cosine waves have discontinuities at the locations of junctions, which is to be expected due to the internal boundary condition (S11). The first 20 eigenvalues are plotted in Fig. S2(a).



Figure S2: (a) The first 20 eigenvalues of the Laplacian (S31) (circles). In magenta is the approximation $\pi^2 n^2/L_W$, where $L_W = 3.36$ is the nondimensional length of the solution path. In blue is the approximation $\pi^2 n^2/L_T$, where $L_T = 5.07$ is the sum of the lengths of all the branches in the maze. The first expression approximates the dominant eigenvalues well, but the higher order modes are much better approximated by the second expression. (b) Results of the parameter optimisation. The blue line shows $E_{sp}(\delta)/\min E_{sp}(\delta)$ calculated from (S41), the normalised square error between the front location in the experiment and simulation along the solution path. The red line shows $E_{pb}(\delta)/\min E_{pb}(\delta)$ calculated from (S42), the normalised square error between experiment and simulation of the fronts in the lateral branches. Both error calculations give minima which are close to each other. The vertical dashed line represents the minimum of the sum of the two normalised data sets, which is the optimal value we use for δ at 0.15.

S4.2 Approximation of transport with the linear modes

We can capture qualitatively the main behaviours observed in the experiment (maze solving, receding in dead-end sections) with only three eigenmodes. We are however unable to capture the initial conditions even approximately with only three modes. To replicate the key behaviours we therefore need to adjust δ and L_0 . Using a fitting parameter Φ , we replace L_0 with ΦL_0 . We perform a parameter sweep over $1 \leq \Phi \leq 40$ and $0.01 \leq \delta \leq 0.1$ to find a minimum error between experiment and simulation using the same error quantification as in section S6. We find a minimum of the combined data sets at $\delta = 0.03$ and $\Phi = 25$.

S5 Experimental data

Experimental data to compare with the model predictions were obtained through image analysis of the video of the experiment [1]. The video of the maze experiment was converted into a time series of N + 1 JPEG images, with each image taken at regular times T_i , where i = 0, 1, 2, ..., N. The time T_0 is the start time and the corresponding image is given in Fig. S1 (left), and T_N is the completion time t_{ref} (chosen when the dye front just enters the outlet branch 37). We imported these images into MATLAB as matrices of dimension $h \times v \times 3$ where h and v are the number of rows and columns of pixels constituting the image, and for each pixel, the three numbers in the third index take integer values from 0 to 256, corresponding to the 8-bit light intensity value of the red, green and blue components at this pixel. We normalise these data by dividing by 256, such that ideal white is created by the 3-tuple [1, 1, 1], and ideal red by [1, 0, 0].

In each image of the time series, we average the pixel values in the transverse direction across the branches, for every branch in the maze, in order to obtain a 1D network of pixels representing the maze. For instance, let us say a horizontal (east-west orientation) section of a branch in a given image has P_w pixels in the east-west direction and P_l pixels in length in the north-south direction, then its image is a

 $P_w \times P_l \times 3$ matrix P. We transform this matrix into a $P_l \times 3$ matrix p defined by

$$\mathsf{p}(j,k) = \frac{1}{P_w} \sum_{i=1}^{P_w} \mathsf{P}(i,j,k).$$
(S36)

Likewise, for a vertical section of a branch, its image is a $P_l \times P_w \times 3$ matrix, which we transform by

$$\mathsf{p}(i,k) = \frac{1}{P_w} \sum_{j=1}^{P_w} \mathsf{P}(i,j,k).$$
(S37)

At corners we neglect the transverse averaging, and instead trace a line of pixels diagonally from the middle of one branch section incident to the corner, indexing this line with the first index of a matrix c(i, k), where k are once again the 3 RGB components. Junctions are taken to belong wholly to the branch nearest the inlet. We then concatenate the matrices of the form (S36) and (S37), and corner sections. For example, the *i*th branch of a maze at time T_j consists of first a horizontal section, which we turn into a matrix of form (S36), which we call p_{h1} , followed by a corner matrix c_1 , followed by a vertical section of the form (S37), which we call p_{v1} , followed by a corner c_2 , and so on; the matrix representing the branch is then

$$\mathsf{B}_{i}^{T_{j}} = \begin{bmatrix} \mathsf{p}_{h1} & \mathsf{c}_{1} & \mathsf{p}_{v1} & \mathsf{c}_{2} & \mathsf{p}_{h2} & \mathsf{c}_{3} & \mathsf{p}_{v2} & \dots \end{bmatrix}^{\top}.$$
 (S38)

The image of all 36 branches in the maze are thus transformed into matrices of the form (S38), where the first index represents the pixel location along the branch with its index increasing in the direction away from the junction nearest to the inlet, and the second index gives the transverse averaged pixel intensities at that location. This operation was repeated for each image in the time series from T_0 to T_N .

For each image in the time series, we compute upper and lower bounds for the locations of the fronts of exogenous surfactant in each branch, as a measure of the spread of the front. We define the upper bound Λ^u as the pixel with the smallest index which has both green and blue components above 180, and the lower bound Λ^l as the pixel with the minimum index where both green and blue were above 120. The difference in these values represent approximately a quartile of colour intensity. For larger values than 180, or smaller values than 120, we find a smooth approximation of the front location is unobtainable due to noise. Indeed, in both the video images, and transverse averaged 1D network, the pixel components creating the white of the milk and the red of the dye are noisy, such that any given pixel usually has RGB components in the range $[0.9, 0.9, 0.9] \leq I_{milk} \leq [1, 1, 1]$ and $[0.9, 0, 0] \leq I_{red} \leq [1, 0.1, 0.1]$. If the number of rows in matrix B_i is P_B , then these locations are

$$\Lambda_i^u(T_j) = \max_{D:(B_i^{T_j}(D,2)>180)\cup(B_i^{T_j}(D,3)>180)} \frac{W}{P_B}L_i, \text{ and } \Lambda_i^l(T_j) = \max_{D:(B_i^{T_j}(D,2)>120)\cup(B_i^{T_j}(D,3)>120)} \frac{W}{P_B}L_i.$$
(S39)

The difference $|\Lambda_i^l(T_j) - \Lambda_i^u(T_j)|$ gives us an experimental error for the exogenous front location. We define $\Lambda_i(T_j)$ as the mean of the upper and lower bounds

$$\Lambda_i(T_j) = \frac{1}{2} \left(\Lambda_i^u(T_j) + \Lambda_i^l(T_j) \right).$$
(S40)

The initial location of the unique exogenous front as used in (S7), (S13), and (S17) is given by $\Lambda_1(0) = x_f = 0.032$.

S6 Comparison of the model predictions with the experiment

We compare the predictions for the time evolution of the fronts of the exogenous surfactant Λ_i , obtained from solving the MFD formulation (S27) and (S28), with the experimental data $\Lambda_i(T_j)$. We analyze two distinct behaviours. The first is the front location of exogenous surfactant along the solution path, and the second is the late time behavior of the front locations in the lateral branches. Hence, we define two separate error quantification procedures for the two behaviours and perform a parameter sweep over δ to find the values which minimise both errors.

S6.1 Minimisation of the error along the solution path

We define $E_{sp}(\delta)$ as the difference between simulation and experiment for the front location along the solution path, defined by branches 1, 3, 5, 7, 9, 12, 14, 18, 22, 30, 32, 34 and 36 (Fig. S1, left). We choose a set of M equally spaced points along the solution path, and for each point χ_i find the time taken $\tilde{\tau}_i$ for the exogenous surfactant front to arrive in a simulation run with a given δ . Then, we use the data set obtained from the experiment of exogenous front locations to find an analogous data set from the experiment. The data set found in S5 maps points equally spaced in time T_j to the spatial location of the exogenous front in branch i, $\Lambda_i(T_j)$. Using MATLAB[®]'s 'interp1' function we interpolate between these data points to find the data set mapping the same set of spatial points χ_i along the solution path to the time of arrival at those points τ_i .

We obtain two normalised, comparable data sets from simulation and experiment $\tilde{\tau}_i/\tilde{\tau}_M$ and τ_i/τ_M , respectively, for i = 1, 2, ..., M. We impose that experiment and simulation start at the same time, but we allow the finish time to vary by scaling the simulation data set by a parameter $0.5 \leq \tau_{end} \leq 1.5$. This secondary parameter provides a slightly better fit, but has negligible impact on the fundamental dynamics underpinning the model. To obtain a positive definite error we compute

$$E_{sp}(\delta) = \min_{0.5 \le \tau_{end} \le 1.5} \sum_{i=1}^{M} \left(\frac{\tau_i}{\tau_M} - \tau_{end} \frac{\widetilde{\tau}_i(\delta)}{\widetilde{\tau}_M(\delta)} \right)^2.$$
(S41)

We compute $E_{sp}(\delta)$ for a range of values $0 < \delta < 1$. The normalised error $E_{sp}(\delta)$ is shown in Fig. S2(b) (blue). The minimum of $E_{sp}(\delta)$ is found at $\delta \approx 0.075$.

S6.2 Minimisation of the error in the lateral branches

We quantify the error $E_{pb}(\delta)$ between experiment and simulation for the front location in the lateral branches. We consider branches, $I = \{2, 4, 6, 8, 10, 11, 13, 15, 19, 23, 24, 31, 33\}$ (Fig. S1, left). We neglect branch 35 where the experimental front does not penetrate. We record the location of the front inside each of the lateral branches in the set I at the set of time points $1 \leq j \leq M$ described in subsection S6.1, in both simulation $\tilde{\Lambda}_i(\tilde{\tau}_j)$ and experiment $\Lambda_i(\tau_j)$. We compute the error as

$$E_{pb}(\delta) = \sum_{i \in I} \sum_{j=1}^{M} \frac{\left(\Lambda_i(\tau_j) - \widetilde{\Lambda}_i(\widetilde{\tau}_j)\right)^2}{L_i^2}.$$
(S42)

The normalised error $E_{pb}/\min E_{pb}$ is plotted in Fig. S2(b) (red) for a range of δ . The minimum is at $\delta \approx 0.195$.

S6.3 Optimal value for the endogenous concentration

The errors $E_{sp}(\delta)$ and $E_{pb}(\delta)$, defined in (S41) and (S42) respectively, give well-defined minima with different optimal values for δ . We added these normalised data sets together, and found a combined minimum at $\delta \approx 0.15$ with $\tau_{end} \approx 1.24$, which are the values used in the simulation results shown in this study. We note that all values $0.02 \leq \delta \leq 0.175$ would give a reasonable fit between the model predictions and the experiments along the solution path, and all values $0.125 \leq \delta \leq 0.21$ would give a reasonable fit of the dynamics in the lateral branches.

S7 Dynamics in lateral branches

In addition to the results presented in Fig. 3(a) (inset) in the main paper, we show the front dynamics in the first 9 lateral branches in the experiment and in the simulation using the optimal value of δ calculated in section S6, Fig. S3. We can observe the same receding effect of the front locations in the simulation and in the experiment. This is explained physically by the finite mass of surfactant available from the inlet branch (in contrast to a fixed concentration at the inlet) spreading through the solution path causing non-monotonic behavior of the surfactant concentration closer to the inlet. The concentration increases



Figure S3: Evolution of the front in time in the first 9 lateral branches for both the optimal prediction from the nonlinear model (black curve, $\delta = 0.15$) and the experimental data (red curve) (S40). The red shaded area shows the experimental error (S39) for the front location. We observe receding behavior in both simulation and experiment as the non-monotonic behavior of surfactant concentration in the early branches of the maze cause a Marangoni flow in the opposite direction in these branches. The receding in the experiment seems to occur over shorter timescales than we achieve in the simulation. We note that the 3-mode linear model (see section S4) has not been plotted in this figure, as we find that for most of these lateral branches the linear model produces no or little flow. This explains why, overall, the full model yields a more quantitative fit to the experimental data throughout all the branches of the maze, based on the global fitting criterion explained in section S6.

substantially initially in the first lateral branches of the solution path, but then decreases at later times. This late time behavior causes a receding Marangoni flow in the opposite direction in branches 2, 4, 6, 8, 10, 11, 13, and 15.

S8 Two-dimensional dynamics

We use COMSOL to simulate the spreading of surfactant in some of the individual branches, and use the particle-tracing feature to track the dynamics of the front of exogenous surfactant. We do this for the section which consists of part of branches 7 and 14, and branches 8, 9, 10, 11, 12 and 13 (Fig. S1, left). In this section, we solve the 2D equation

$$\frac{\partial \Gamma}{\partial t} = f(W) \boldsymbol{\nabla} \cdot (\Gamma \boldsymbol{\nabla} \Gamma), \tag{S43}$$

implementing no flux boundary conditions on all boundaries except at the inlet ($\Gamma = 1$) and outlet $\Gamma = \delta$. The initial conditions are $\Gamma = (1 - \delta) \cos(\pi x/2)/2 + (1 + \delta)/2$ for $0 \le x_7 \le 2$, and $\Gamma = \delta$ everywhere else.



Figure S4: Sequence of images showing an experiment to solve a liquid maze with surfactant using different experimental conditions than in the original experiments of [1] (see §S9.1 and experiment #1 in table SIV). (a) A pipette is used to introduce 20 μ l of isopropyl alcohol (undyed). The maze was previously filled with glycerol, and seeded with pliolite particles (nominal diameter around 100 μ m), which float at the surface. (b)-(d) show flow evolution. Tracks for each particle, starting from t = 0, are shown in color. (Length scale: the sides of the large entrance square inlet and outlet measure approximately 20 mm.)

S9 Additional experiments

Our main conclusion is that the maze solving behavior is primarily due to the interaction between the exogenous and endogenous surfactants. We sought to demonstrate that the maze-solving behavior is robust, and does not rely on the specific liquids and surfactant used in the original experiments of [1], which are also shown in our Letter. The original experiments of [1] used a mixture of milk and cream as the liquid medium, and the exogenous surfactant consisted of an aqueous soap solution. The flow was visualized using an aqueous red dye solution.

Here we show that a similar maze-solving behavior can be observed as long as the following requirements are met:

- The exogenous surfactant solution, as well as any passive tracers, must be less dense than the background liquid. This ensures that the surfactant and tracer move along the surface;
- The background liquid must be of sufficiently high viscosity to keep the flow essentially laminar; and



Figure S5: Sequence of images showing another experiment to solve a liquid maze with surfactant using different experimental conditions than in the original experiments of [1] (see §S9.2 and experiment #2 in table SIV). (a) A pipette is used to introduce a mixture of 50% isopropyl alcohol (2-propanol) and 50% dye (by mass). The background liquid is a solution of 10% 2-propanol and 90% glycerol. The amount added is 1 ml. (b)-(d) show flow evolution. (Length scale: the sides of the large entrance square inlet and outlet measure approximately 20 mm.)

• The exogenous surfactant must be mild enough (as measured by the slope of the surface tension change with concentration), such that the associated Marangoni flow does not immediately lead to complete coverage of the interface.

The experiments of [1] leveraged the fact that soap in milk or cream behaves as a much milder surfactant than soap in water (see for example [10] for data and discussion on the interaction between milk casein and Sodium Dodecyl Sulfate from soap). Because we now wish to use a background fluid other than milk, we choose isopropyl alcohol (i.e. 2-propanol), which acts as a mild surfactant in water, as measured by the ratio between adsorption and desorption coefficients [11]. To maximize viscosity and density in the background liquid, we used glycerol mixtures. We report here two representative experiments, which are summarized in table SIV and are shown in Figs S4 and S5.

S9.1 Glycerol background and 2-propanol added, visualized with particles

The first experiment is shown in Fig. S4, and aimed to also remove possible complications arising from the presence of dye. We therefore used glycerol (99% purity) as the maze liquid, and 2-propanol (99% concentration) as the exogenous surfactant. The flow was visualized by plastic particles (Pliolite, nominal

diameter approximately 100 μ m) that were dispersed on the surface before the endogenous surfactant was introduced. The particles had nominal density $1.04 \cdot 10^{-3} \text{ kg/m}^3$, such that they floated over the glycerol, whose density was around $1.25 \cdot 10^{-3} \text{ kg/m}^3$. A pipette was used to introduce 20 μ l of 2-propanol at t = 0.

In the experiments of [1], the bottom of the channels was transparent and a light source was placed below the maze, such that the white milk stood out against the black maze. In our new experiment shown in Fig. S4, the particles are white, and we cannot use the same lighting technique of [1], as the particles would be invisible against the background lighting. Instead, we manufactured a matt black maze, and illuminated it from above, such that the particles stood out against the background, as shown in Fig. S4

In order to calculate particle tracks, images were analyzed using the Trackmate plugin in FIJI [12]. Selected snapshots are shown in panels (a) through (d) of Fig. S4. The tracks show how the surface flow in the main branch is directed primarily to the maze exit; this is especially evident in the final image, namely Fig. S4(d). The tracks also visualize motion in the side branches and in the reservoir. For example, we can see that particles in the destination reservoir (on the left of each panel in Fig. S4) began moving well before any particles from the main branch approached the end of the maze, as shown in Fig. S4(c,d); this observation is consistent with the long-range interactions associated with our transport model.

S9.2 Background and added liquids both comprising 2-propanol and glycerol

To further illustrate the robustness of the maze-solving behavior arising from exogenous/endogenous surfactant interaction, we performed another experiment where the background and added liquids both contained glycerin and the same surfactant (2-propanol), but in different proportions. A small amount of red dye was introduced in the added liquid as a passive tracer. Specifically, the maze liquid was a solution (by mass) of 10% 2-propanol and 90% glycerol, whereas the added liquid consisted of 50% 2-propanol and 50% glycerol.

The experiment is depicted in Fig. S5. The dyed fluid reached the outlet in approximately one minute, yielding a pattern similar to that shown in Fig. 1 of our Letter, although with fuzzier edges, as shown in Fig. S5(d). This result further supports our proposed model for the surfactant-solving mechanism.

There are additional interesting observations that can be made from Fig. S5. At late stages, a thin ridge of dye is visible ahead of each dye front. We hypothesize that this is due to a secondary effect, which partially analogous to the 'tears of wine' phenomenon, as well as to the 'coffee ring' effect. Namely, we believe the effect may be driven by alcohol evaporation near the exogenous surfactant front, resulting in surface tension that is locally slightly higher than that of the following liquid. The locally higher tension draws dyed liquid to the front, where dye accumulates as the alcohol evaporates.

S9.3 Summary of new experiments

In summary, for the different systems tested, the same underlying maze solving behavior is still observed. This provides further experimental evidence to support the main conclusion of this study. We expect that the maze solving behavior is possible with a wide range of liquids, surfactants and tracers, as long as they meet the conditions listed above – namely that the surfactant must be mild, that the exogenous surfactant and tracer must float above the maze liquid, and that the flow remains laminar (e.g. the viscosity must be high enough). Therefore, we anticipate that analogous interactions between exogenous and endogenous surfactants in confined geometries can be important in other systems where surfactant concentrations are out-of-equilibrium.

References

- F. Temprano-Coleto, F. J. Peaudecerf, J. R. Landel, F. Gibou, and P. Luzzatto-Fegiz, Phys. Rev. Fluids 3, 100507 (2018).
- [2] W. D. Rutz, C. Whitnah, and G. Baetz, J. Dairy Sci. 38, 1312 (1955).
- [3] A. Bakshi and D. Smith, J. Dairy Sci. 67, 1157 (1984).

Experiment	Maze	Exogenous	Passive	
#	medium	surfactant	tracers	
1	99% glycerol	2-propanol	Pliolite $100\mu m$	
2	90% glycerol + $10%$ 2-propanol	50% 2-propanol + $50%$ glycerol	Dye	

Table SIV: Table describing the experimental conditions of the qualitative experiments conducted to test the main conclusion of our modelling study: that the maze solving dynamics reported in [1] is primarily due to the interaction between exogenous and endogenous surfactants.

- [4] D. Kristensen, P. Jensen, F. Madsen, and K. Birdi, J. Dairy Sci. 80, 2282 (1997).
- [5] O. E. Jensen and J. B. Grotberg, J. Fluid Mech. 240, 259 (1992).
- [6] O. E. Jensen and D. Halpern, J. Fluid Mech. **372**, 273 (1998).
- [7] R. Mcnair, O. E. Jensen, and J. R. Landel, J. Fluid Mech. 930, A15 (2022).
- [8] J. Grotberg, D. Halpern, and O. Jensen, J. Appl. Physiol. 78, 750 (1995).
- [9] M. Brio, J.-G. Caputo, and H. Kravitz, Appl. Numer. Math. 172, 99 (2022).
- [10] Q. Tian, L. Lai, Z. Zhou, P. Mei, Q. Lu, Y. Wang, D. Xiang, and Y. Liu, J. Agric. Food Chem. 67, 6336 (2019).
- [11] C.-H. Chang and E. I. Franses, Colloids Surf. A Physicochem. Eng. Asp. 100, 1 (1995).
- [12] D. Ershov, M.-S. Phan, J. W. Pylvänäinen, S. U. Rigaud, L. Le Blanc, A. Charles-Orszag, J. R. W. Conway, R. F. Laine, N. H. Roy, D. Bonazzi, G. Duménil, G. Jacquemet, and J.-Y. Tinevez, Nat. Methods 19, 829 (2022).