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# **A novel insight into the enhanced electrochemical performance of Mg-air battery in mixed aqueous and organic electrolytes**

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## **Abstract**

A new strategy of utilizing mixtures of ethanol and complexing agents on Mg-air battery is investigated systematically. The presence of ethanol promotes formation of a dense inner layer with a high portion of oxide in the discharge film, leading to significantly enhanced utilization efficiency. The highest utilization efficiency of Mg anode has been increased from 53.6 % to 85.7 % and the discharge potential is decreased 300 mV, when discharges in mixed electrolyte. The adsorption/deposition of S-like species on metal surface is evidenced in ethanol and 5-sulfosalicylate acid containing solution, resulting in inhibition of the hydroxide-rich outer layer growth.

**Keywords:** Primary Mg-air battery; Utilization efficiency; Time-of-flight secondary ion mass spectrometry; Additive

## **1. Introduction**

The high volumetric capacity (3832 mAh g<sup>-1</sup>) and low standard electrolyte potential (-2.37 V vs. SHE) of Mg make primary Mg-air batteries a promising power source for offshore devices and electric vehicles [1-6]. However, practical application of Mg-air battery is greatly limited due to two main issues [7-13]. Firstly, rapid self-corrosion rate of anode, related to high hydrogen evolution rate (HER) during discharge, which largely reduces the utilization efficiency of the Mg anode and shortens its service life. Secondly, appearances of undissolved discharge products on anode surface, which induces significant decrease of reaction kinetics, and is detrimental to the discharge

voltage. In this case, undissolved Mg matrix appears on discharge products and dissolve into electrolyte, further reducing the utilization efficiency and specific capacity of anode [14, 15]. It has been proved that tailoring the chemical composition of the anode or electrolyte can effectively enhance the discharge performance of Mg-air batteries.

Alloying or heat treatment of Mg-based electrode materials is beneficial to change the phases (composition or morphology) inside, which leads to uniform dissolution during battery operating and high discharge performance [4, 16-23]. Deng et al. [18] found that the redeposition of In element at the interface of substrate/oxide film disrupted the discharge product film and inhibited the NDE effect of the anode. Mg-0.1Ca-0.2In alloy exhibited superior utilization efficiency, e.g., 80.2% at 5 mA cm<sup>-2</sup>. It was reported by Sha et al. [19] that addition of 0.5 wt.% Y element promoted the formation of intermetallic phase (Mg<sub>24</sub>Y<sub>5</sub>) in Mg-4Li anode. The Mg<sub>24</sub>Y<sub>5</sub> phase facilitated the grain refinement of Mg-4Li alloy, which reduced the weight loss during discharge. Chen et al. [4] concluded that heat treatment greatly reduced the potential difference between Mg matrix and second phases (Mg<sub>7</sub>Zn<sub>3</sub> and Mg<sub>17</sub>Al<sub>12</sub>). The micro-galvanic corrosion process of Mg alloys was inhibited and high utilization efficiency of Mg-6Zn alloy was enhanced from 44% to 56% after heating at 693K for 20 h.

The modification of electrolyte through the addition of specific compounds has a significant effect on improving the discharge performance of Mg-air batteries [5, 14, 24-34]. It has been reported that complexing agents can act as electrolyte additives due to their Mg<sup>2+</sup> and Fe<sup>3+</sup> complexing ability [25, 26, 35, 36]. The strong Mg<sup>2+</sup> complexing agent effectively removes discharge products and maintains a stable discharge voltage. Furthermore, the addition of complexing agents chelates with Fe<sup>3+</sup> and inhibits the micro-galvanic corrosion process, leading to increased utilization efficiency. It was verified by Vaghefinazari et al. [31] that ethylenediaminetetraacetic acid (EDTA) prevented the deposition of discharge products and decreased the self-corrosion process caused by the re-deposition of Fe. The electrochemical activity of anode was greatly enhanced and 1.62 V of discharge voltage was shown after introduction of 0.1 M EDTA at 5 mA cm<sup>-2</sup>. Wang et al. [28] investigated that the effect of different concentrations of 2,6-dihydroxybenzoate (2,6-DHB) on the discharge performance of the Mg anode. It

was demonstrated that 0.2 M 2,6-DHB was sufficient to hinder the deposition of discharge products on surface. The HER of anode during discharge was inhibited in 0.2 M 2,6-DHB containing solution and the specific energy of AM50 Mg alloy was increased from 1640 to 1850 Wh kg<sup>-1</sup> after the introduction of 0.2 M DHB at 10 mA cm<sup>-2</sup>. Complexing agents accelerate the dissolution rate and enhance the transfer process of ions. However, Mg anode shows high self-corrosion rate during discharge with addition of strong Mg<sup>2+</sup> complexing agent, which decreases the utilization efficiency and specific capacity, especially under low current densities.

Recently, it was found that organic solvent has a great effect on regulating the electrochemical behavior of the Mg anode [11, 37, 38]. Kurchavov et al. [38] investigated the NDE of Mg sample in ionic liquid and water mixture electrolytes, more specifically in [mPEG<sub>n</sub>MPyr]AcO-H<sub>2</sub>O. They concluded that oxygen atoms of [mPEG<sub>n</sub>MPyr]<sup>+</sup> bonded the released water, leading to the great inhibition of the reaction between free H<sup>+</sup> and Mg sample. The mixture of water/organic electrolytes can also be efficient to decrease the corrosion of Mg-based anode. It was demonstrated that 0.5 wt.% ethanol enhanced the corrosion resistance of Mg sample and reduced the actual weight loss during discharge [37]. The composition of discharge products showed a decreased of Mg(OH)<sub>2</sub> deposition on surface, which enhanced the discharge performance of anode. Nevertheless, the improvement of utilization efficiency and specific capacity by ethanol was shown to be limited and the Mg anode demonstrated low discharge voltage compared to that in blank NaCl solution.

Strong Mg<sup>2+</sup> complexing agents (Mg<sup>2+</sup> constant stability > 5) might have great potential to increase the electrochemical activity of anode [8, 35, 39]. Therefore, three complexing agents are selected as electrolyte additives in the present study: 4,5-dihydroxy-1,3-benzenedisulfonic acid disodium salt (Tiron), 3,4-dihydroxybenzoic acid (3,4-DHB) and 5-sulfosalicylic acid (SSA). The Mg<sup>2+</sup> constant stabilities of the complexing agents are listed in Table S1. In order to inhibit the detrimental effect of H<sup>+</sup> on the self-corrosion process of Mg sample, ethanol is used as another additive into electrolyte. In present experiment, the impact of additives on the discharge performance and corrosion of pure Mg in NaCl solution, their effect on the discharge products and corrosion



mechanism are investigated. Specifically, the composition and distribution of discharge products on surface in different solutions is investigated. Moreover, the discharge mechanism through the electrolyte additives that enhanced the discharge performance of anode is also clarified.

## **2. Experimental methods**

### **2.1. Preparation of anodes and electrolytes**

In this study, commercial pure Mg samples, the same as in our previous studies [40], were used as the anodes. All specimen were ground by using silicon carbide papers and dried in air (2000 grit). The based solution used in this study was 3.5 wt.% NaCl electrolyte, and the additives included 30% volume of ethanol (> 99.9%), 0.1 M 4,5-dihydroxy-1,3-benzenedisulfonic acid disodium salt (Tiron), 0.1 M 3,4-dihydroxybenzoic acid (3,4-DHB) and 0.1 M 5-sulfosalicylic acid (SSA) (MacLin, Shanghai, China). The pH of different electrolytes was tailored to a pH of  $7 \pm 0.2$  by using NaOH. The conductivity and resistivity of various solutions were measured by ROOKO Surface Resistance Tester (FT-400AHXM, Ningbo, China) according to MIL-DTL-81706B.

### **2.2. Electrochemical tests of samples**

A comprehensive description of experimental details is provided in supplementary material.

### **2.3. Analysis of sample and electrolyte after discharge**

After discharge, the morphology of Mg sample was detected by scanning electron microscope (Quanta250FEG, FEI, USA). X-ray diffraction (XRD) equipped with Cu K  $\alpha$  radiation was carried out using a Smartlab instrument (Model SmartLab, Rigaku, Tokyo, Japan) to analysis the discharge products formed on surface. The step size for the XRD test was  $5^\circ \text{ min}^{-1}$  and the test was conducted in the range of  $10^\circ$  to  $90^\circ$ . Raman spectra was collected in the range of  $4000\text{--}50 \text{ cm}^{-1}$  on Raman microscope (Model RXploRA Plus, Horiba, Kyoto, Japan) to confirm the composition of discharge products after discharge in mixtures. Hydra/Medusa® software (USA) was carried out to simulate the chemical composition of surface and electrolytes after discharge for 10 h.

Time-of-flight secondary ion mass spectrometry (ToF-SIMS) was utilized to investigate the composition and distribution of species on anode surface after discharge for 5 min in different solutions. A ToF-SIMS V spectrometer (ION TOF Münster, Germany) with an operating pressure of  $10^{-9}$  mbar was employed for ToF-SIMS in-depth profiling. For further analysis, a pulsed 25 keV  $\text{Bi}^+$  primary ion source delivering a 1.2 pA current over a  $100 \times 100 \mu\text{m}^2$  area was performed. Sputtering was adopted by 2 keV  $\text{Cs}^+$  giving a 100 nA target current over  $300 \times 300 \mu\text{m}^2$  area. The analysis was performed in the negative mode to get better sensitivity to the oxide species. Flood-gun was employed for charge neutralization. Analysis of post-processing and data acquisition was used with the Ion-Spec software (version 4.1).

### **3. Results**

#### **3.1. Electrochemical measurements**

##### **3.1.1. EIS test**

Fig. 1 displays the impedance spectra of the Mg sample after being immersed in various electrolytes for 1 h. The spectra was fitted using the equivalent circuit depicted in Fig. 2a, where  $R_s$  corresponds to the solution resistance,  $R_f$  and  $\text{CPE}_f$  represent the resistance and capacitance of corrosion product film, respectively,  $R_{ct}$  represents the resistance of charge transfer, while  $\text{CPE}_{dl}$  stands for the capacitance of double layer [41, 42]. The inductive loop observed at low frequency is influenced by the possible non-stationary state, which is discarded from the fitting process [43]. The fitted EIS results are displayed in Fig. 2b and Table 1.

The largest capacitive loop can be observed with the addition of ethanol (Fig. 1a). As shown in Fig. 1b, the impedance value at low frequency rises from  $523 \Omega \cdot \text{cm}^2$  (for NaCl) to  $5720 \Omega \cdot \text{cm}^2$  (for ethanol), suggesting that the degradation behavior of Mg is inhibited in ethanol containing electrolyte. The inhibition is also confirmed from a significant increase of the  $R_{total}$  (sum of  $R_f$  and  $R_{ct}$ ) by  $4890 \Omega \cdot \text{cm}^2$  with reference to the NaCl electrolyte (Fig. 2b and Table 1).

However, the dissolution process of Mg samples is significantly promoted by the presence of  $\text{Mg}^{2+}$  complexing agent in solutions without ethanol. A narrow capacitive loop and a visible inductive loop can be observed in the presence of Tiron for 1 h (a

zoom of Nyquist plot presented as an inset in Fig. 1a). In this solution, the lowest impedance value at 0.01 Hz reduced by  $513 \Omega \cdot \text{cm}^2$  is observed with reference to the NaCl electrolyte (Fig. 1b). Similarly, significant dissolution of the Mg sample can be also confirmed in 3,4-DHB containing solution as the low impedance (Fig. 1b) and a narrow phase angle (Fig. 1c). Slightly higher impedance as well as larger phase angle can be detected for SSA complexing agent. However, it can be found that introduction of complexing agent contributes to high dissolution rate of Mg sample, as evidenced by the small capacitive loop, low impedance and small phase angle (Fig. 1a, b and c, respectively). It is also observed from Fig. 2b and Table 1 that the  $R_{\text{total}}$  decreases to 6.8, 19.8 and  $160.6 \Omega \cdot \text{cm}^2$ , respectively in Tiron, 3,4-DHB and SSA containing solution, further indicating the high dissolution rate of Mg samples in these solutions.

In mixtures, when the ethanol is added to the electrolytes containing the complexing agents, the increase of impedance value at low frequency (Fig. 1b) and the wider phase angle (Fig. 1c) are regularly observed. The highest increase can be noticed in 3,4-DHB and ethanol solution, where the impedance value at low frequency reaches  $112.5 \Omega \cdot \text{cm}^2$ , which indicates 5-fold increase with reference to a single 3,4-DHB solution (Fig. 1b). This indicates that the dissolution rate is reduced in the mixture solutions compared to the single complexing agent solutions based on water solvent. Comparing to value of  $R_{\text{total}}$  after fitted, it could be verified that Mg samples show higher corrosion resistance in mixtures than in solutions with addition of single complexing agents (Fig. 2b and Table 1). For instance, the  $R_{\text{total}}$  of Mg sample increases to  $109.8 \Omega \cdot \text{cm}^2$  after immersion in 3,4-DHB and ethanol containing solution. Mg sample shows  $160.6 \Omega \cdot \text{cm}^2$  of  $R_{\text{total}}$  after soaking in the presence of SSA and ethanol, which is  $311.5 \Omega \cdot \text{cm}^2$  higher than in the water-based solution.

The compactness and thickness of corrosion film can be also evaluated by impedance spectra (Fig. 2 and Table 1). Due to the porosity, roughness, and non-uniform conductivity of surface layer, a non-ideal capacitive behavior (CPE) was used to fit the double-layer capacitor, which deviate from ideal dielectric behavior [44, 45].

To account for the corrosion film formed on the surface in different solutions, two parallel capacitances are used. The final capacitance value (CPE) can be determined using equation (5) [44]:

$$CPE = S CPE_{dl} + (1 - S) CPE_f \quad (5)$$

S represents the fraction of the active surface, corresponding to substrate exposed to electrolyte (which can be found in the film pores and defects). Depending on the property of corrosion film formed on surface, CPE<sub>f</sub> is used for evaluating the CPE of film in electrolyte with single ethanol (protective film) whereas CPE<sub>dl</sub> plays a dominant role in determining CPE of films in other electrolytes (defective films, as evidence by the narrow capacitive loops and phase angles) [37, 46]. Table 1 also shows the CPE<sub>dl</sub> of 10<sup>-2</sup> and n<sub>ct</sub> value of 0.99 (close to 1) in electrolyte with addition of single Tiron. This implies that the CPE corresponds almost to a double layer capacitance of 10<sup>-2</sup> F cm<sup>-2</sup> in this solution [47].

The effective capacitance (C<sub>eff</sub>) was calculated using the simplified Brug formula (6), where R<sub>s</sub> can be ignored when R<sub>s</sub> is much smaller than R<sub>ct</sub> and R<sub>f</sub> [46, 48]:

$$C_{eff} = CPE \frac{1}{n} (R_s)^{\frac{1-n}{n}} \quad (6)$$

It is found that C<sub>eff</sub> value for the single ethanol containing solution (1.3 × 10<sup>-5</sup>) is the lowest among various solutions (Table 1).

The thickness of the surface film can be calculated using the Cole-Cole diagram [49, 50]. To do so, the complex capacitance C(ω), expressed by equation (7), needs to be determined [49, 51]:

$$C(\omega) = \frac{1}{j\omega(Z(\omega) - R_e)} \quad (7)$$

Where ω is equal to 2 × Π × f (frequency) Hz, Z(ω) is related to impedance value, and R<sub>e</sub> represents the solution resistance from fitting process.

From equation (7), the real and imaginary parts of C(ω) can be separated, resulting in two equations, (8) and (9) [49]:

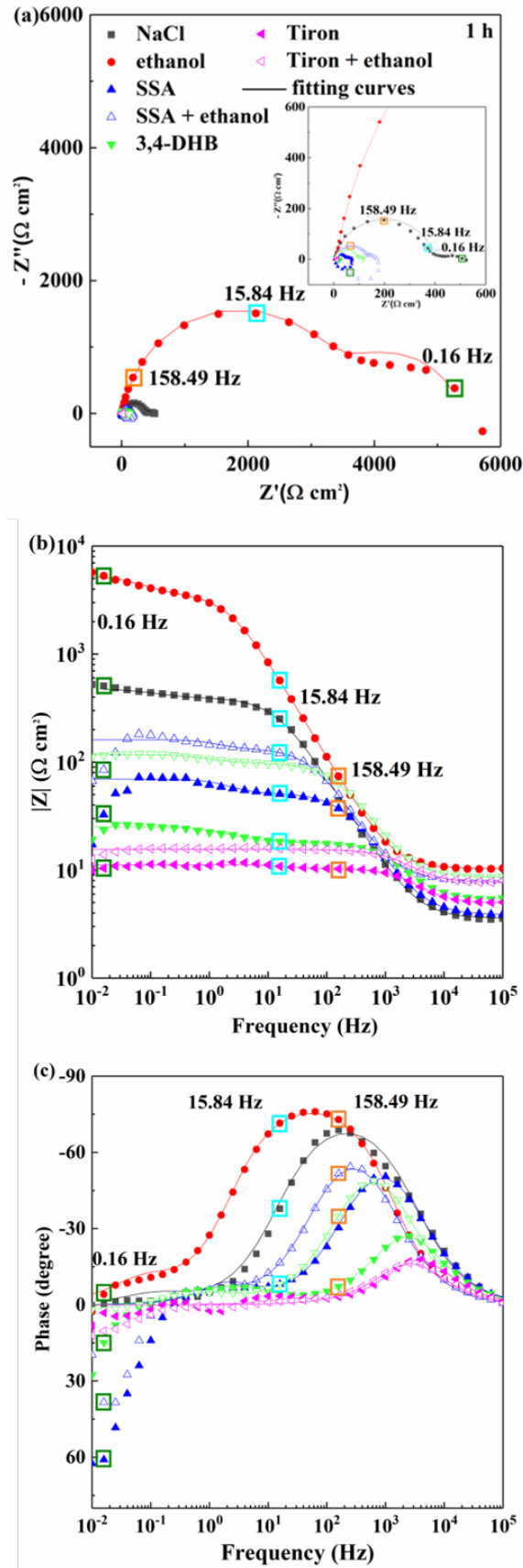
$$Re(C(\omega)) = - \frac{Im(Z)}{\omega(Re(Z)_{corr}^2 + Im(Z)^2)} \quad (8)$$

$$Im(C(\omega)) = -\frac{Re(Z)_{corr}}{\omega(Re(Z)_{corr}^2 + Im(Z)^2)} \quad (9)$$

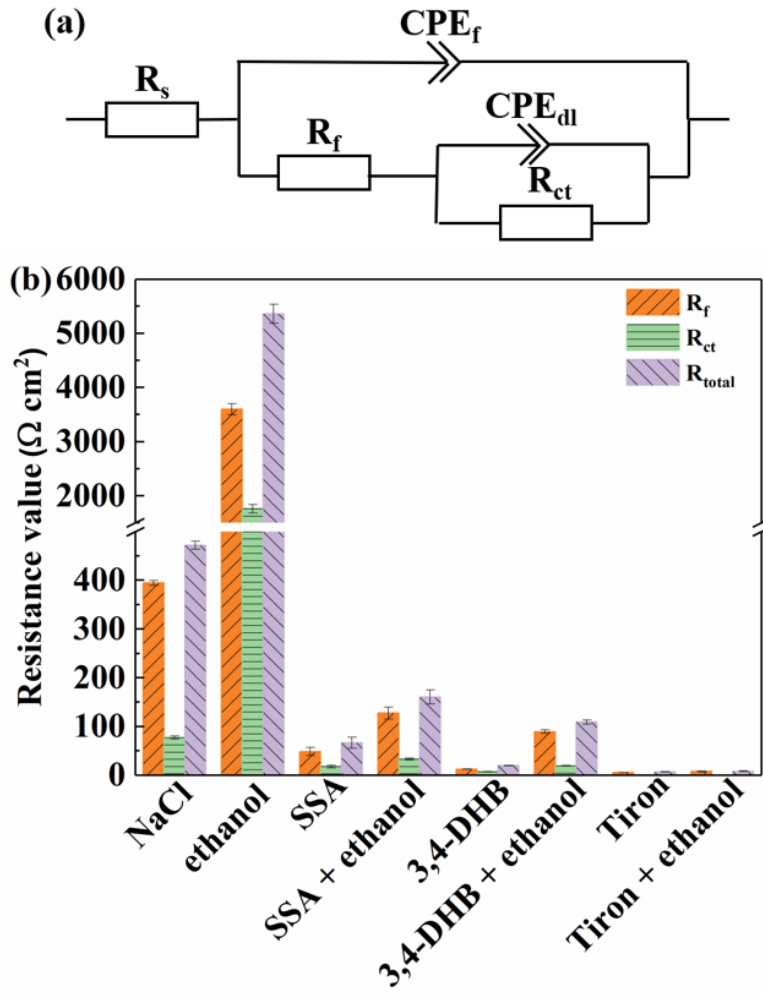
The limit of  $Re(C(\omega))$  at infinite frequency is the infinite capacitance  $C(\infty)$ , which is used for calculating the thickness of film using equation (10) [49, 51]. In the case of current work,  $C(\infty)$  is determined at frequency of 10 kHz.

$$\delta = \frac{\varepsilon\varepsilon_0}{C_\infty} \quad (10)$$

In this equation,  $\varepsilon$  is the relative dielectric constant of MgO ( $\varepsilon = 10$ ), and  $\varepsilon_0$  is the vacuum permittivity ( $\varepsilon_0 = 8.85 \times 10^{-14} \text{ F cm}^{-2}$ ) [52]. The calculations reveal that a 194 nm-thick corrosion film is formed in blank NaCl solution, while significantly smaller values were observed in solutions containing single complexing agents. For example, a 54 nm-thick film was formed on the surface in the presence of Tiron (Table 1). The highest film thickness observed in blank NaCl solution implies that significant amounts of corrosion products accumulate on the surface, due to severe corrosion occurring during the immersion process. The presence of single ethanol is effective in slightly reducing the film thickness, as evidenced by the formation of a 185 nm-thick surface layer (Table 1), indicating the lower corrosion rates. Thicker corrosion films are formed on the surface with addition of the mixtures compared to those containing single complexing agents. For instance, the film thickness is 159 nm in solution with Tiron and ethanol, which is 105 nm thicker with reference to the single Tiron containing solution (Table 1). The modifications and the properties of the surface layers across different electrolytes will be addressed in the discussion section. It is important to note that for this calculation it is assumed that the film is only composed of MgO and the dielectric constant of MgO is used for calculation. The actual corrosion film contains high amounts of  $Mg(OH)_2$ , thus estimating the total film thickness by only considering MgO might be inaccurate.



**Fig. 1.** EIS spectra of Mg samples after 1h-immersion in various electrolytes: (a) Nyquist plot, (b) Bode plots impedance spectra and (c) Phase angle.



**Fig. 2.** Equivalent circuit used for the EIS fitting (a) and values of resistances (b) for Mg specimen after 1h-immersion in different electrolytes.

**Table 1.** Fitting values obtained for components of EIS equivalent circuit for Mg sample after immersion in various electrolytes with additives for 1 h.

Electrolyte	$R_s$ ( $\Omega \text{ cm}^2$ )	$CPE_f$ ( $\Omega^{-1} \text{ s}^{-n} \text{ cm}^{-2}$ )	$R_f$ ( $\Omega \text{ cm}^2$ )	$n_f$	$CPE_{dl}$ ( $\Omega^{-1} \text{ s}^{-n} \text{ cm}^{-2}$ )	$R_{ct}$ ( $\Omega \text{ cm}^2$ )	$n_{ct}$	$R_{total}$ ( $\Omega \text{ cm}^2$ )	$C_{eff}$ ( $\text{F cm}^{-2}$ )	$d$ (nm)
NaCl	3.5±0.1	5.2×10 <sup>-5</sup>	394.6±5.2	0.98	9.1×10 <sup>-5</sup>	77.5±3.1	0.99	472.1±8.3	1×10 <sup>-4</sup>	194
NaCl + ethanol	10.3±0.2	2.9×10 <sup>-5</sup>	3600±101	0.91	5.3×10 <sup>-3</sup>	1762±76	0.88	5362±177	1.3×10 <sup>-5</sup>	185
NaCl + SSA	3.3±0.3	3.0×10 <sup>-5</sup>	48.6±8.3	0.88	4.0×10 <sup>-3</sup>	17.9±2.9	0.95	66.5±11.2	5.6×10 <sup>-3</sup>	86
Mix NaCl + SSA + ethanol	7.9±0.1	4.4×10 <sup>-5</sup>	127.4±12.4	0.88	7.2×10 <sup>-3</sup>	33.2±1.6	0.92	160.6±14	1.3×10 <sup>-2</sup>	168
NaCl + 3,4-DHB	3.3±0.1	3.6×10 <sup>-5</sup>	12.7±0.2	0.87	1.7×10 <sup>-2</sup>	7.1±0.2	0.85	19.8±0.4	3.9×10 <sup>-2</sup>	66
Mix NaCl +3,4-DHB + ethanol	8.5±0.3	2.7×10 <sup>-5</sup>	89.5±3.5	0.88	1.1×10 <sup>-2</sup>	19.6±0.6	0.89	109.1±4.1	2.4×10 <sup>-2</sup>	165
NaCl + Tiron	3.4±0.2	3.3×10 <sup>-5</sup>	5.5±0.2	0.89	1.0×10 <sup>-2</sup>	1.3±0.1	0.99	6.8±0.3	1.1×10 <sup>-2</sup>	54
Mix NaCl + Tiron + ethanol	7.7±0.1	3.4×10 <sup>-5</sup>	7.8±0.8	0.88	6.6×10 <sup>-3</sup>	0.4±0.2	0.99	8.2±1	7.1×10 <sup>-3</sup>	159



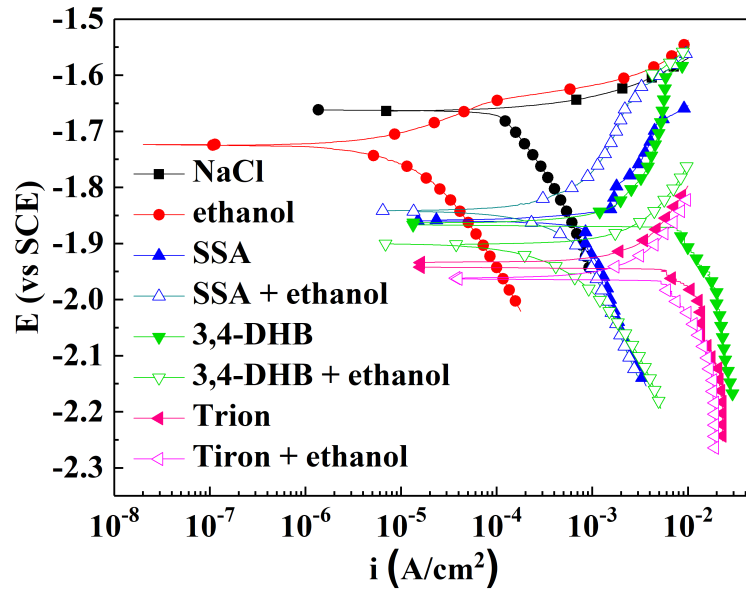
### 3.1.2. Polarization test

The corrosion behavior of Mg specimen after soaking in various solutions for 1 h is evaluated by polarization test, as shown in Fig. 3. Table S2 lists the corrosion potential ( $E_{\text{corr}}$ ) and corrosion current densities ( $i_{\text{corr}}$ ) of the samples.

The lower anodic and cathodic current densities are observed for Mg sample in NaCl solution with ethanol, indicating that ethanol inhibits the anodic dissolution process and cathodic  $\text{H}_2$  evolution reaction. The corrosion density of Mg specimen decreases by  $120 \mu\text{A cm}^{-2}$  due to the introduction of ethanol (Table S2), which confirms the improved corrosion resistance.

However, after addition of complexing agents to the NaCl electrolyte,  $i_{\text{corr}}$  of Mg sample significantly increases. For instance, the  $i_{\text{corr}}$  of sample reaches  $13943.4 \mu\text{A cm}^{-2}$  in the presence of Tiron. This reflects that Mg sample shows high dissolution rate in the presence of single complexing agent. It should be noted that the anodic branches move towards higher current densities, confirming the promotion of dissolution process.

In comparison to blank NaCl solution, the anodic and cathodic branches shift to the higher currents in the presence of mixtures. It means that Mg samples show higher dissolution rates in mixtures (complexing agents and ethanol) than in the water-based solutions. However, after exposition to the mixtures for 1 h, lower  $i_{\text{corr}}$  of Mg sample can be observed ( $7348.3 \mu\text{A cm}^{-2}$ ) in Tiron and ethanol containing solution than a single Tiron ( $13943.4 \mu\text{A cm}^{-2}$ ). In the case of 3,4-DHB and ethanol mixture, the  $i_{\text{corr}}$  is ten times lower than in the case of simple addition of complexing agent ( $764.1$  vs  $7235.5 \mu\text{A cm}^{-2}$ , respectively). Thus, single ethanol is efficient in decreasing the corrosion rate of Mg in comparison to the solution with a single complexing agent.



**Fig. 3.** Potentiodynamic polarization curves of Mg specimen after 1h-immersion in various electrolytes.

### 3.2. Discharge properties of anode in half-cell test

The discharge property of Mg samples exposed to NaCl solutions with and without additives is investigated using half-cell discharge test.

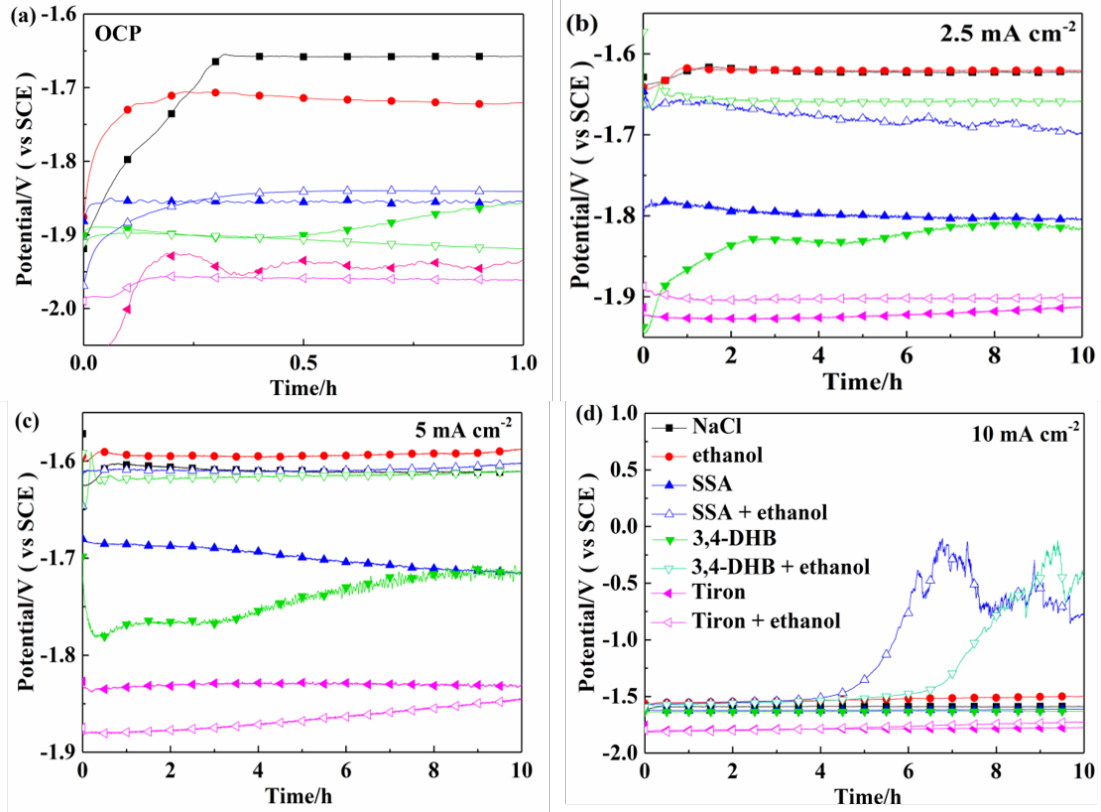
Similar OCP in ethanol containing solution with reference to based solution can be observed, which implies that single ethanol has a weak effect on enhancing the electrochemical activity of Mg sample (Fig. 4a and Table 2).

The Mg anode demonstrates low open circuit potential (OCP) in the presence of single complexing agents. The lowest OCP of -1.94 V is observed in the presence of Tiron. After addition of SSA and 3,4-DHB, the OCP of Mg anode decreases to -1.86 V (Fig. 4b and Table 2). The relatively low OCP of the Mg anode indicates high electrochemical activity of Mg sample in these solutions. Complexing agents effectively decrease the discharge potential of the anode at different current densities (Fig. 4b-d and Table 2). At 2.5 mA cm<sup>-2</sup>, a discharge potential of -1.92 V is observed after introduction of Tiron and -1.83 V in the presence of 3,4-DHB. As for SSA, the average potential of specimen significantly decreases from -1.62 to -1.8 V (Fig. 4). As the current density increases, Mg samples still show high dissolution behavior in NaCl

solution with single complexing agents (Table 2 and Fig. 4d). Apparently, discharge potential of -1.79 V is demonstrated for Mg in single Tiron containing solution. With the addition of 3,4-DHB, the discharge potential of the Mg anode is still 40 mV lower than that of blank NaCl solution.

In mixture solutions, OCP of Mg sample decreases with the lowest value of -1.96 in Tiron and ethanol. Other mixtures also have great influence on decreasing the OCP of Mg sample (Fig. 4a and Table 2). Interestingly, the effect of mixtures on the discharge behavior changes with the increase of current density. At  $2.5 \text{ mA cm}^{-2}$ , it is worth noting the lower discharge potential with addition of ethanol and Tiron (-1.9 V) compared to that in NaCl solution (-1.62 V). At the same current density, in the presence of ethanol and SSA, the Mg anode shows a discharge potential of -1.68 V, which is 60 mV lower than that of the reference (Fig. 4b).

Discharge potential of samples increases as current density increases (Fig. 4c and d) in mixtures. It is illustrated that Mg sample exhibits a high discharge potential of -1.61 V with the addition of SSA and ethanol. A similar average anode discharge potential is observed after introduction of 3,4-DHB and ethanol. When a current density of  $10 \text{ mA cm}^{-2}$  is applied, the discharge potential of the Mg anode sharply increases after discharging for 5 h in mixtures containing SSA and 3,4-DHB (Fig. 4d).



**Fig. 4.** Electrochemical behaviour of samples in NaCl electrolytes with or without additives. (a) OCP, (b) 2.5 mA cm<sup>-2</sup>, (c) 5 mA cm<sup>-2</sup> and (d) 10 mA cm<sup>-2</sup>.

This significant rise in discharge potential may be attributed to the high solution resistance and the substantial deposition of discharge products. Equation 5 is employed in order to explain the discharge potential of anode in solutions with or without additives at different current densities [39, 53].

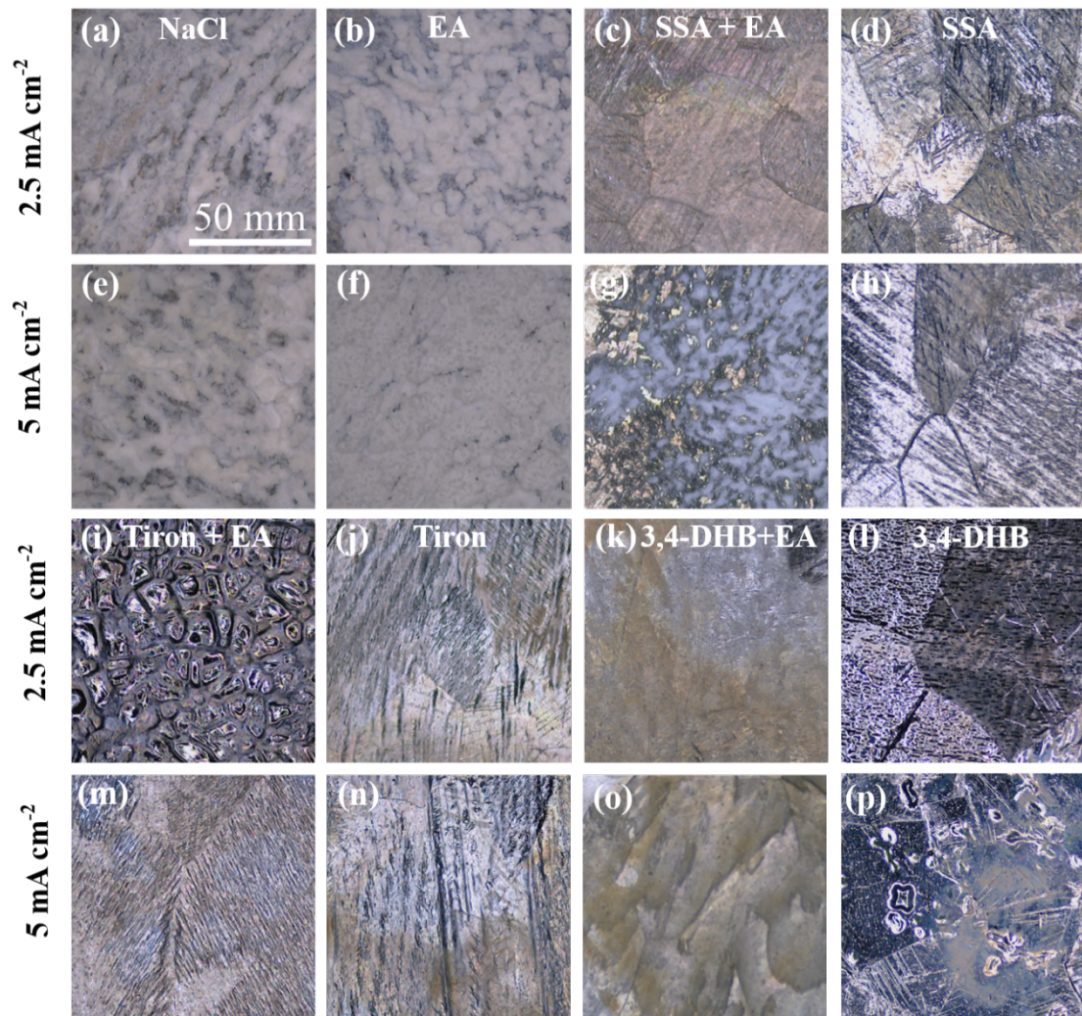
$$E_{anode} = E_{ocp} - \eta_{ct} - \eta_{diff} - IR \quad (11)$$

The average open circuit and discharge potential is presented by  $E_{ocp}$  and  $E_{anode}$ , respectively,  $\eta_{ct}$  corresponds to the drop of potential induced by resistance of charge transfer,  $\eta_{diff}$  to the overpotential of diffusion resulted from the discharge product, and  $IR$  to the potential drop, which is related to the applied current density and solution resistance. Except from solution with single ethanol, low OCP of anode is demonstrated after introduction of different additives. However, Mg samples show higher discharge potentials in ethanol and mixture solutions than in blank water-based solution at high current densities. It means that the  $\eta_{ct}$ ,  $\eta_{diff}$  and  $IR$  determine the average discharge potential of Mg sample. Table S3 displays the conductivity and resistivity of different electrolytes that are used in this study. It can be seen that

introduction of ethanol increases the resistivity of electrolyte due the reduction of free  $H^+$ . High current density further leads to the large potential drop. Similarly, the potential drop ( $IR$ ) is larger in mixtures than in NaCl-based solutions, especially at high current densities (Table S3). On the contrary, single complexing agents leads to the increase of the conductivity of solution due to the dissociation of molecules (Table S3). Thus, the  $IR$  after addition of single complexing agents is lower than that of NaCl solution.

Fig. S1 shows the EIS spectrum of discharged samples in various electrolytes. The wide capacitive loops can be observed for all current densities in electrolytes containing ethanol (Fig. S1a-c), indicating the large  $\eta_{ct}$  and  $\eta_{diff}$  during discharge. However, Mg samples show narrow capacitive loops in solutions with single complexing agents (Fig. S1a-c), implying that single complexing agents have great effect on reducing the  $\eta_{ct}$  and  $\eta_{diff}$ . Apparently, the narrowest capacitive loop is shown in the presence of 0.1 M Tiron containing solution. In case of mixture solutions, Mg samples show narrow capacitive loops after discharge (Fig. S1a), especially in solution composed of Tiron and ethanol. However, as the applied current density increases, the capacitive loops in mixtures (SSA and ethanol, 3,4-DHB and ethanol) become more wider compared to those in NaCl solution. This widening suggests increased charge transfer and diffusion resistance ( $\eta_{ct}$  and  $\eta_{diff}$ ) at high current densities (Fig. S1b and c).

Fig. 5 displays the optical morphology of discharged samples in different electrolytes. The apparent discharge products deposits on anode surface in NaCl solution and ethanol containing solution (Fig. 5a, b, e and f) could be observed. However, the presence of discharge products is scarce in solutions containing complexing agents (Fig. 5d, h, j, n, l and p). This confirms that the contributions of  $\eta_{ct}$  and  $\eta_{diff}$  resulting from discharge products in solutions with single complexing agents are minimal. In the case of mixture solutions, a smaller accumulation of discharge products appears on surface in solutions containing Tiron and ethanol (Fig. 5i and m). Mixtures containing 3,4-DHB and ethanol, SSA and ethanol effectively suppress the appearances of discharge products (Fig. 5c and k). However, with the increase of current density, significant amounts of discharge products accumulate on surface in these two mixtures (Fig. 5g and o), which is detrimental to the discharge process of the Mg anode. The surface state of discharged specimen, as observed through optical microscopy, correlates with the impedance test.

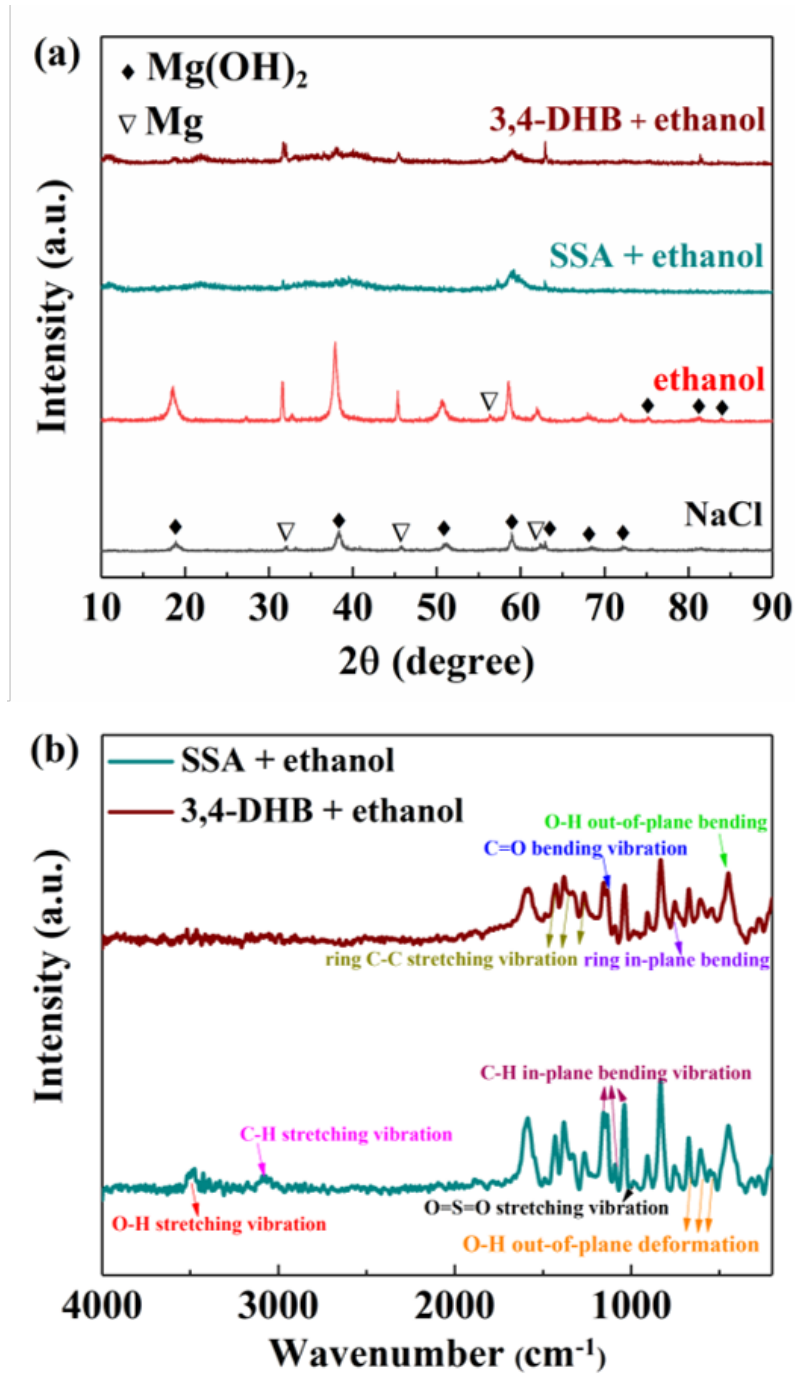


**Fig. 5.** Optical surface micrography of Mg samples after discharge at different current densities for 10 h in various electrolytes.

In order to investigate the reason of the sharp increase in discharge potential observed in mixtures during discharge at  $10 \text{ mA cm}^{-2}$ , the composition of discharge products is examined using X-ray diffraction (XRD) and Raman spectroscopy (Fig. 6). It is evident that discharge products, primarily consisting of  $\text{Mg(OH)}_2$ , deposit on the surface after discharge in various solutions for 10 hours. The substantial accumulation of discharge products impedes the contact area between the anode and the electrolytes, thereby contributing to the high discharge potential (Fig. 6a). As shown in Fig. 6b, peak at  $3474 \text{ cm}^{-2}$  is associated with the O-H stretching vibration, which indicates the presence of  $\text{Mg(OH)}_2$  [54]. The peaks at  $694$ ,  $607$  and  $551 \text{ cm}^{-2}$  correspond to the O-H out-of-plane deformation vibration, and peak at  $325 \text{ cm}^{-2}$  to the O-H out-of-plane bending mode. The presence of C-H stretching vibration is related to the peak at  $3079 \text{ cm}^{-2}$ . The peaks at  $1253$ ,  $1153$  and  $1036 \text{ cm}^{-2}$  are identified as C-H in-plane bending vibration. The C=O bending vibration is related to  $1323 \text{ cm}^{-2}$ , while peaks at  $1572$ ,  $1487$  and  $1375 \text{ cm}^{-2}$  are matched with the ring C-C stretching vibration [54, 55]. A peak at  $748 \text{ cm}^{-2}$  is considered as ring in-plane bending mode. The peak at  $990 \text{ cm}^{-2}$  refers to the O=S=O stretching vibration [56]. Peaks associated with C-H in-plane vibration, C=O bending vibration, and O=S=O stretching vibration indicate the presence of species induced by complexing agents in the surface layer of the Mg anode during discharge at  $10 \text{ mA cm}^{-2}$ . The adsorption/deposition of these species on surface further amplifies the  $\eta_{ct}$  and  $\eta_{diff}$ , potentially leading to the sharp increase in discharge potential observed in mixtures at high current densities.

Thus, ethanol not only leads to the higher solution resistance, but also is inefficient in reducing the amount of discharge products formed on anode surface, which is detrimental to the discharge potential of anode. Single complexing agents effectively mitigate  $\eta_{ct}$  and  $\eta_{diff}$  resulting from discharge products, maintaining a low discharge potential across different current densities. Mixtures (SSA and ethanol, 3,4-DHB and ethanol) inhibit the deposition of discharge products at low current densities. However, the enhanced  $IR$ ,  $\text{Mg(OH)}_2$  and the adsorption/deposition of species (resulting in high  $\eta_{ct}$  and  $\eta_{diff}$ ) collectively impede the continuous discharge process.

This hindrance contributes to the elevated discharge potential of Mg anode at 10 mA cm<sup>-2</sup>.



**Fig. 6.** Analysis of deposited discharge products in various electrolytes at 10 mA cm<sup>-2</sup> for 10 h: (a) XRD spectra and (b) Raman spectra.

### 3.3. Full-cell battery test in various electrolytes

The discharge voltage curves of Mg-air battery in various electrolytes and current densities are depicted in Fig. 7. Since ethanol and two mixtures (SSA and ethanol, 3,4-

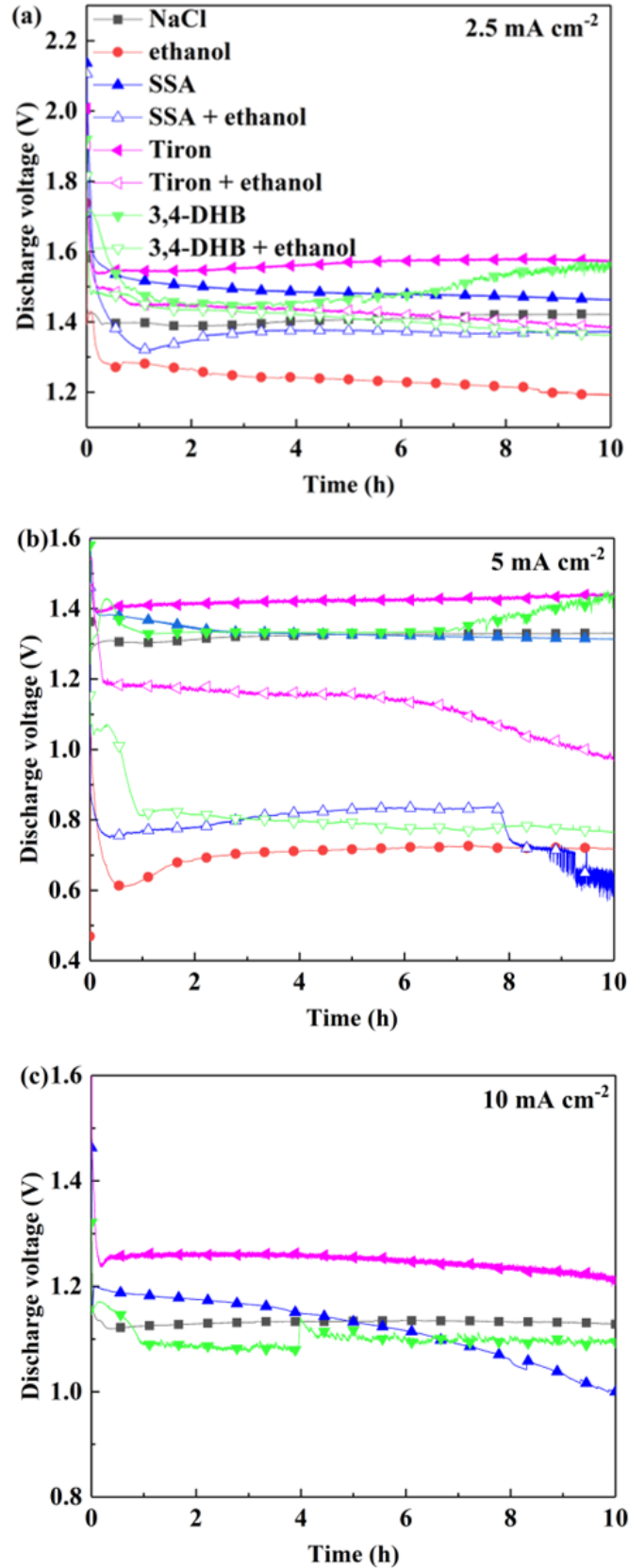


DHB and ethanol) electrolytes are hard to yield satisfactory results under high current densities in half-cell discharge, full-cell battery tests are conducted at low current densities.

The addition of ethanol to the electrolyte results in a lower discharge voltage compared to that in NaCl solution (Fig. 7a-c). Conversely, the presence of complexing agents leads to higher discharge voltages under low applied current densities. Obviously, the average discharge voltage of 1.57 V is achieved in the presence of Tiron (Fig. 7a and Table 2). However, with exception for Tiron, similar average discharge voltages are observed in NaCl solution and solutions containing single complexing agents at high current densities (Fig. 7c and Table 2).

In mixtures, Mg sample exhibits an average voltage of 1.47 V in the presence of Tiron and ethanol solution. Compared to blank solution, the Mg anode shows a similar discharge voltage when ethanol is added to solution containing SSA and 3,4-DHB (Fig. 7a and Table 2). However, as the current density increases, the Mg anode yields low discharge voltage in these mixtures. Notably, a discharge voltage of 0.81 V is observed in the presence of ethanol and 3,4-DHB, which is 0.51 V lower than that in NaCl solution at  $5 \text{ mA cm}^{-2}$  (Fig. 7b and Table 2). According to Equation 5, the power density of the anode depends on the average discharge voltage. Fig. 8 shows the power density of aqueous and ethanol-based battery in electrolytes with kinds of additives. Apparently, single ethanol decreases the power density of the Mg anode. At low current densities, the Mg anode exhibits high power density in the presence of complexing agents. Specifically, the power density of the anode increases from  $3.53$  to  $3.93 \text{ mW cm}^{-2}$  with the addition of Tiron. However, due to the decreased discharge voltage, complexing agents are ineffective at enhancing power density at high current densities. Compared to that in NaCl solution, Mg anode shows a slightly higher power density of  $3.68 \text{ mW cm}^{-2}$  in the Tiron and ethanol containing solutions. Mg anode also maintains a power density of  $3.5 \text{ mW cm}^{-2}$  in mixtures with SSA and 3,4 DHB. However, at high discharge current densities, the anode demonstrates low power density in these mixtures.

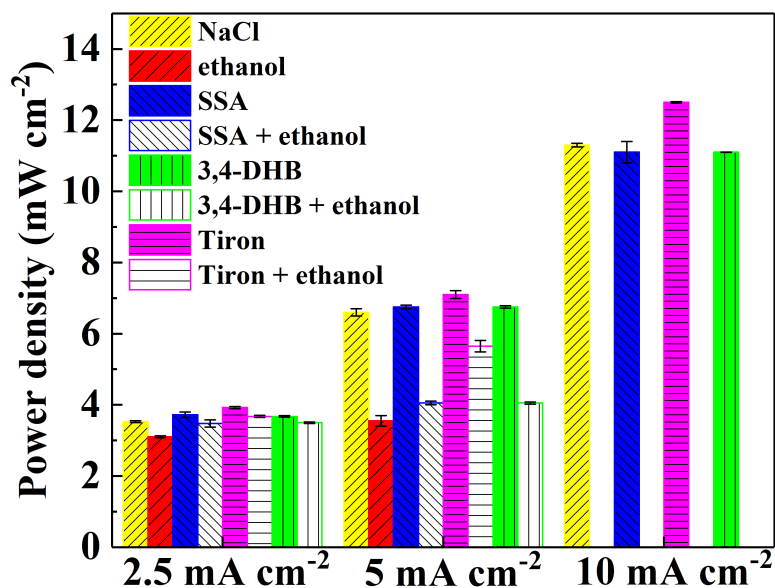
High solution resistance and the formation of discharge products lead to low electrochemical activity of the Mg anode. Additionally, the sluggish cathodic oxide reduction reaction (ORR) further decreases the discharge voltage <sup>[31]</sup>. Consequently, the Mg anode shows low discharge performance with the addition of ethanol at various current densities. Complexing agents significantly inhibit the deposition of discharge products, resulting in higher discharge voltage and power density. Due to low value of resistance of charge transfer, Mg anode demonstrates excellent discharge performance with addition of mixtures under low current densities. However, at high current densities, the combined effects of the discharge products on the surface, adsorbed/deposited additives, high solution resistance, and ORR collectively result in a low discharge voltage of anode in mixtures.



**Fig. 7.** Discharge voltage profiles of Mg-air battery at different current densities: (a) 1 mA cm<sup>-2</sup>, (b) 2.5 mA cm<sup>-2</sup> and (c) 5 mA cm<sup>-2</sup> and (d) 10 mA cm<sup>-2</sup> in various electrolytes.

**Table 2.** Electrochemical behavior of anodes in various electrolytes at different current densities in half cell and full cell.

	Electrolyte	NaCl	NaCl + ethanol	NaCl + SSA	Mix NaCl + SSA + ethanol	NaCl + 3,4-DHB	Mix NaCl + 3,4-DHB + ethanol	NaCl + Tiron	Mix NaCl + Tiron + ethanol
Average discharge potential (vs. SCE) in half cell									
current density	0 (OCP)	-1.66	-1.72	-1.86	-1.85	-1.86	-1.91	-1.94	-1.96
	2.5	-1.62	-1.61	-1.8	-1.68	-1.83	-1.67	-1.92	-1.9
$\text{mA cm}^{-2}$	5	-1.61	-1.59	-1.71	-1.61	-1.73	-1.62	-1.87	-1.83
	10	-1.59	-1.53	-1.62	-	-1.63	-	-1.79	-1.77
Average discharge voltage (V) in full cell									
current density	2.5	1.41	1.24	1.49	1.39	1.5	1.4	1.57	1.47
	5	1.32	0.71	1.35	0.81	1.35	0.81	1.42	1.13
$\text{mA cm}^{-2}$	10	1.13	-	1.11	-	1.11	-	1.25	-



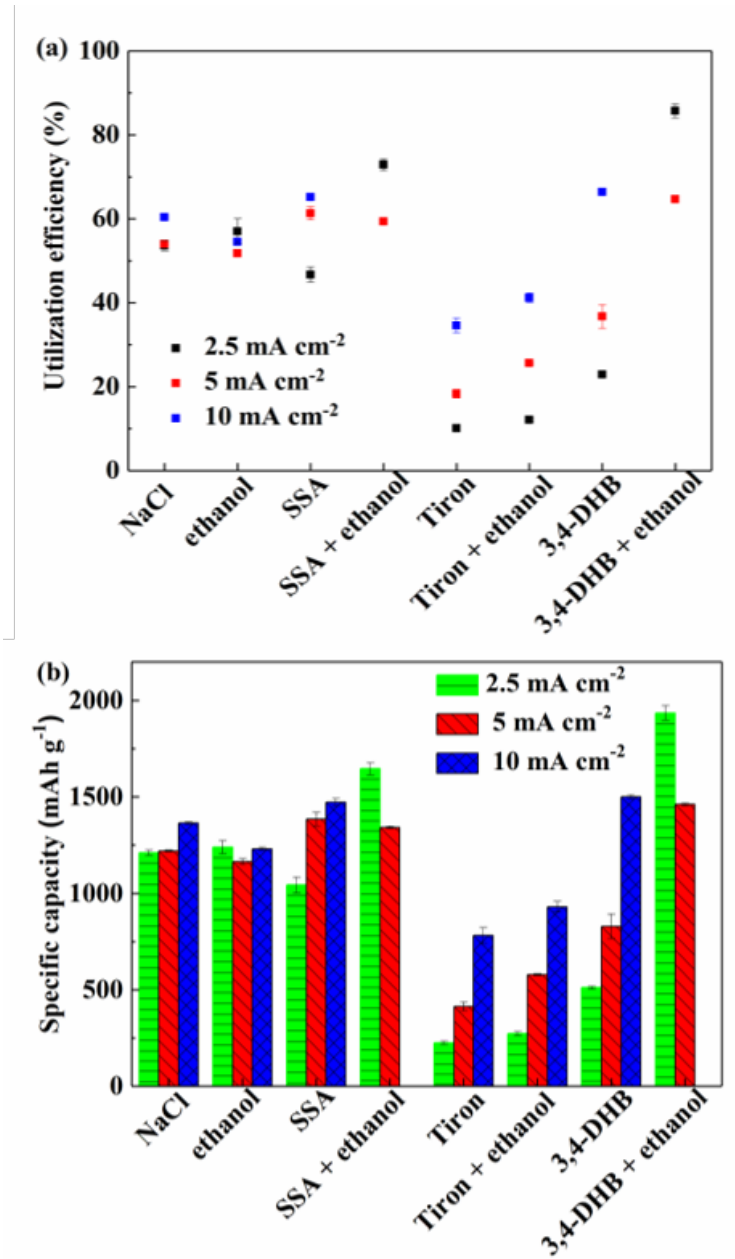
**Fig. 8.** Power density of Mg in NaCl solutions with and without additives.

### 3.4. Actual anode weight loss during discharge

Fig. 9 and Table 3 shows the discharge performance of specimen in various electrolytes. It can be seen that the utilization efficiency of anode is slightly increased in ethanol containing solution (Fig. 9a and Table 3). However, as the current density increases to  $5 \text{ mA cm}^{-2}$ , ethanol fails to enhance the discharge performance of the anode, decreasing the utilization efficiency by 2.2% (Fig. 9a and Table 3). The addition of single complexing agents significantly reduces the utilization efficiency and specific capacity of the anode at low current densities. In the presence of Tiron, the Mg anode achieves only 12.1% utilization efficiency (Fig. 9a and Table 3). Similarly, 3,4-DHB decreases the specific capacity of the anode from 1210.8 to 511.7  $\text{mAh g}^{-1}$  (Fig. 9b and Table 3). In contrast to ethanol, the Mg anode demonstrates high discharge performance with addition of single complexing agents at high current densities. Notably, SSA enhances these two parameters of Mg anode to 61.3% and 1384.8  $\text{mAh g}^{-1}$  at  $5 \text{ mA cm}^{-2}$ , respectively (Fig. 9a, b and Table 3). At  $10 \text{ mA cm}^{-2}$ , the Mg anode shows the highest utilization efficiency in the 3,4-DHB containing solution among various solutions, reaching 66.7% (Fig. 9a and Table 3).

The Mg anode demonstrates superior utilization efficiency and specific capacity in the presence of mixtures, except for Tiron-containing solution. Notably, the utilization

efficiency of 85.7% is achieved in a mixture of 3,4-DHB and ethanol, which is 32.7% higher than the blank NaCl solution (Fig. 9a and Table 3). Mixtures of SSA and ethanol, and 3,4-DHB and ethanol, continue to significantly enhance the utilization efficiency of samples ( $5 \text{ mA cm}^{-2}$ ). At  $10 \text{ mA cm}^{-2}$  of current density, Mg anode shows higher discharge performance in a mixture of Tiron and ethanol in compared to the NaCl-based solution. However, it has been observed that a sharp increase of average potential occurs in mixtures of SSA and ethanol, and 3,4-DHB and ethanol at  $10 \text{ mA cm}^{-2}$ , indicating that these two mixtures are unsuitable for use at high current densities (Fig. 4d). Therefore, calculating these two parameters of anode in these mixtures at this current density is meaningless.



**Fig. 9.** Discharge behaviour of specimen in solutions with kinds of additive: (a) utilization efficiency (%) and (b) specific capacity (mAh g<sup>-1</sup>).

**Table 3.** Utilization efficiency and specific capacity of anodes in various electrolytes at different current densities.

	Current density (mA cm <sup>-2</sup> )	NaCl	NaCl + ethanol	NaCl + SSA	Mix NaCl + SSA + ethanol	NaCl + 3,4-DHB	Mix NaCl + 3,4-DHB + ethanol	Tiron	Mix NaCl + Tiron + ethanol
Utilization efficiency (%)	2.5	53.6±1.2	57±3	46.7±1.8	72.9±1.4	22.9±0.3	85.7±1.7	10.1±0.4	12.1±0.5
	5	54±0.2	51.8±0.7	61.3±1.6	59.4±0.3	36.7±2.8	64.7±0.3	18.3±1	25.6±0.2
	10	60.4±0.3	54.5±0.4	65.2±0.9	-	66.4±0.5	-	34.6±1.8	41.2±1.2
Specific capacity (mAh g <sup>-1</sup> )	2.5	1210.8±13.5	1240.1±33.5	1043.4±40.3	1646.8±31.6	511.7±6.8	1935.9±38.4	225.6±9.1	273.3±11.3
	5	1219.9±4.5	1164.5±15.8	1384.8±36.1	1341.8±6.8	829±63.3	1456.6±6.8	413.4±22.6	578.3±4.5
	10	1364.4±6.8	1231.1±9	1472.9±20.3	-	1499.9±11.3	-	781.6±40.7	930.7±27.1



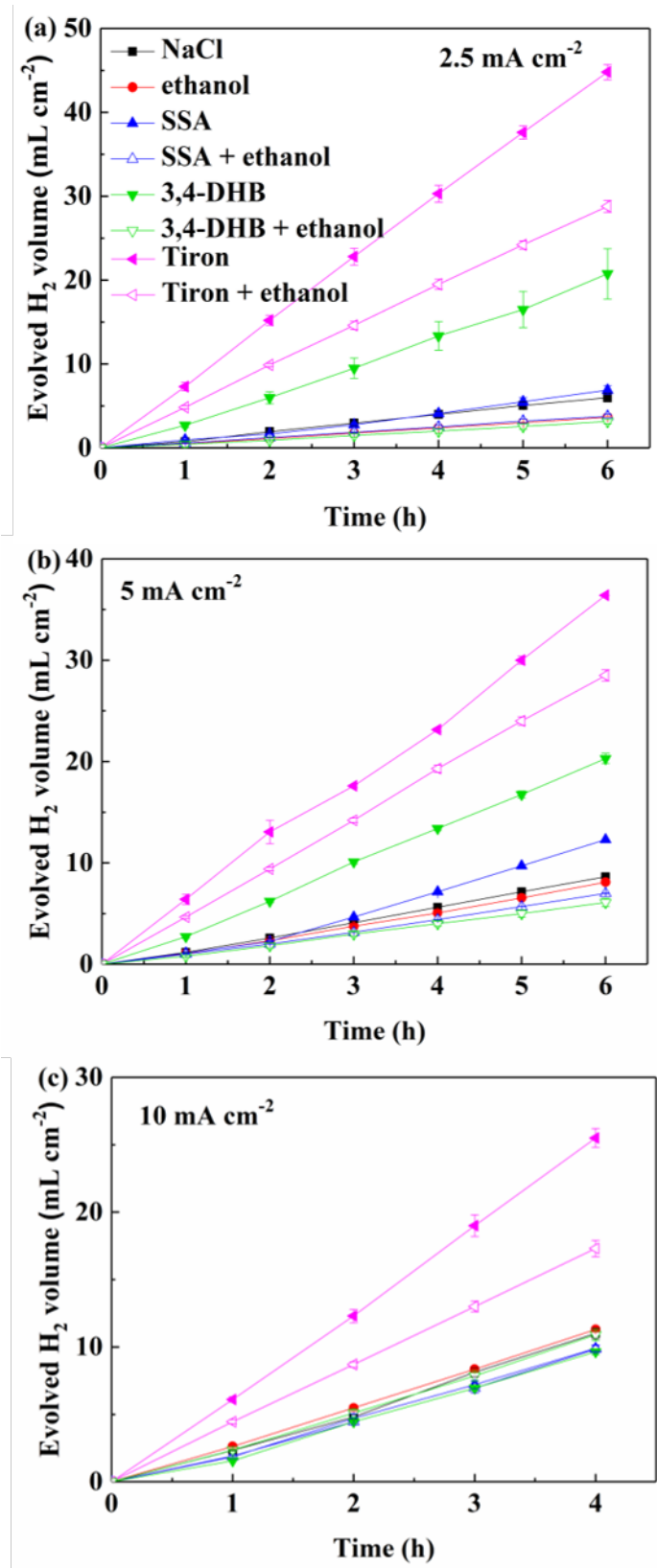
The actual weight loss  $\Delta W$  during the discharge test can be represented by Equation 6 [28].

$$\Delta W = \Delta W_{theo} + \Delta W_{self-corr} + \Delta W_{chunk\ effect} \quad (12)$$

$\Delta W_{theo}$  represents the theoretical weight loss associated with the electronic transport,  $\Delta W_{self-corr}$  corresponds to anode weight loss resulted from self-corrosion process during discharge, while  $\Delta W_{chunk\ effect}$  is related to the undissolved Mg substrate surrounded by discharge products. It is apparent that low  $\Delta W_{self-corr}$  and  $\Delta W_{chunk\ effect}$  determine the high utilization efficiency.

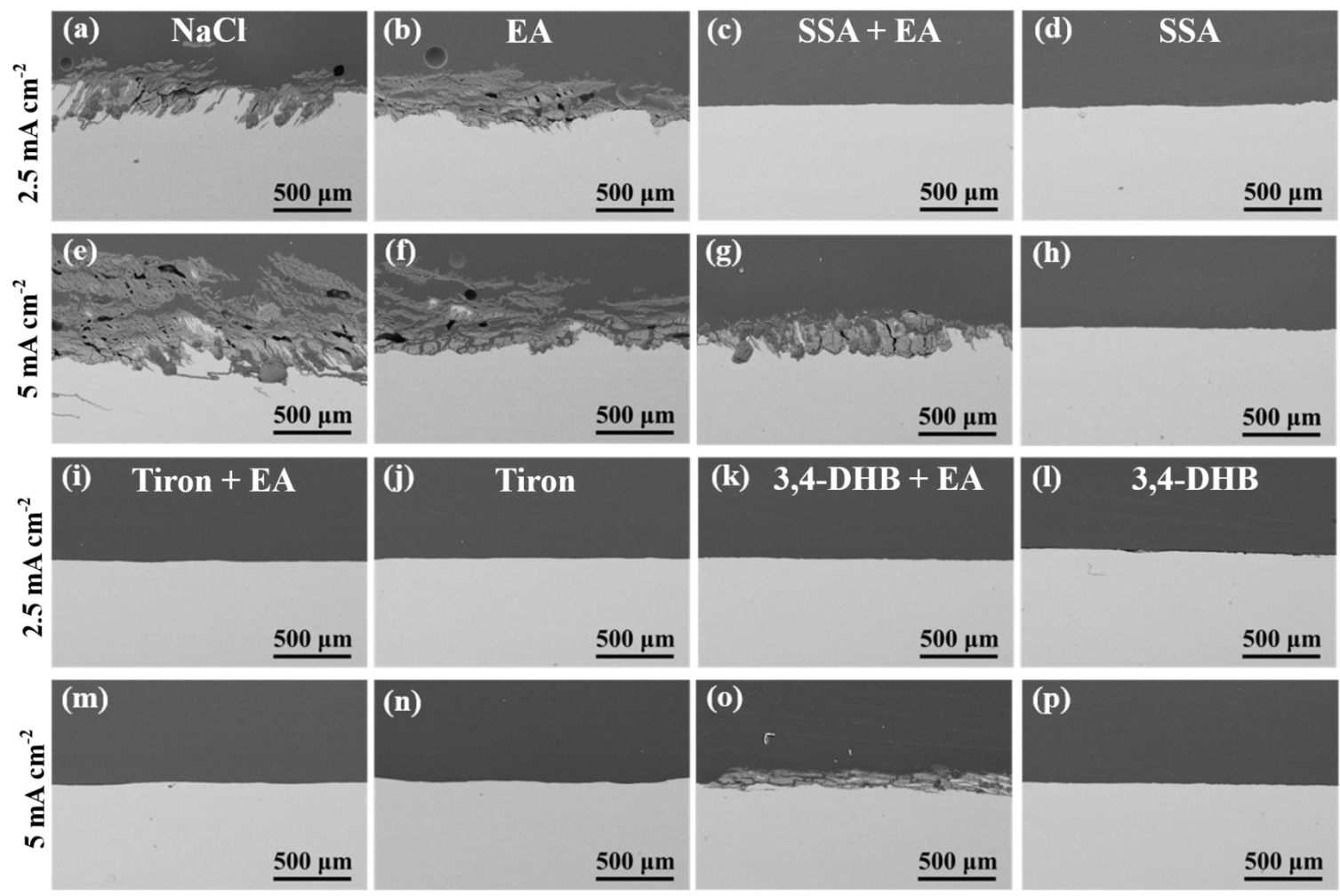
Real-time hydrogen tests during discharge are employed to investigate the self-corrosion rate of the anode in different electrolytes (Fig. 10). After extended discharge tests, undissolved Mg matrix appears in the discharge products (chunk effect). This undissolved Mg matrix, surrounded by discharge products, can detach from the sample and lead to increase of H<sub>2</sub> evolution and weight loss ( $\Delta W_{self-corr}$ ). Therefore, 6 h of discharge at 2.5 and 5 mA cm<sup>-2</sup>, and 4 h at 10 mA cm<sup>-2</sup>, are used to evaluate the actual self-corrosion rate.

At 2.5 mA cm<sup>-2</sup>, ethanol reduces the H<sub>2</sub> volume from 6 to 3.65 mL cm<sup>-2</sup> (Fig. 10a). However, Mg anode shows a higher released H<sub>2</sub> volume in solutions containing complexing agents compared to NaCl solution at low current density. It is worth to be mentioned that lower H<sub>2</sub> volume is demonstrated in mixtures, especially in 3,4-DHB and ethanol solution with 3.15 mL cm<sup>-2</sup> of H<sub>2</sub> after discharge for 6 h (Fig. 10a). At a current density of 5 mA cm<sup>-2</sup> (Fig. 10b), the H<sub>2</sub> volume in NaCl solution with added ethanol is similar to that in pure NaCl solution. Complexing agents lead to a high release of H<sub>2</sub> volume during discharge, indicating a high self-corrosion rate. In contrast, Mg samples exhibit low H<sub>2</sub> volume in mixtures, as shown of 6.1 mL cm<sup>-2</sup> (Fig. 10b) with addition of 3,4-DHB and ethanol. When current density increases to high value (Fig. 10c), ethanol and mixtures increase the H<sub>2</sub> release rate during discharge. However, except for Tiron, complexing agents significantly inhibit H<sub>2</sub> evolution. The H<sub>2</sub> volume in the presence of 3,4-DHB is 1.35 mL cm<sup>-2</sup>.



**Fig. 10.** Real-time hydrogen evolution measurements of Mg sample during discharge at (a) 2.5 mA cm<sup>-2</sup>, (b) 5 mA cm<sup>-2</sup> and (c) 10 mA cm<sup>-2</sup> in NaCl solution with different additives.

The cross-sectional morphology of specimen after discharge in different solutions for 10 h is demonstrated in Fig. 11. The discharge products with chunk effect are shown on surface in NaCl and ethanol-based solutions (Fig. 11a, b, e and f). Then, the chunk effect is hardly visible on Mg surfaces with the addition of complexing agents. At low current densities, the chunk effect is unobserved in mixtures (Fig. 11c, i and j). However, at  $5 \text{ mA cm}^{-2}$ , the introduction of ethanol into solutions containing 3,4-DHB and SSA results in deposition of discharge products on the anode surface (Fig. 11g and o) and apparent chunk effect.

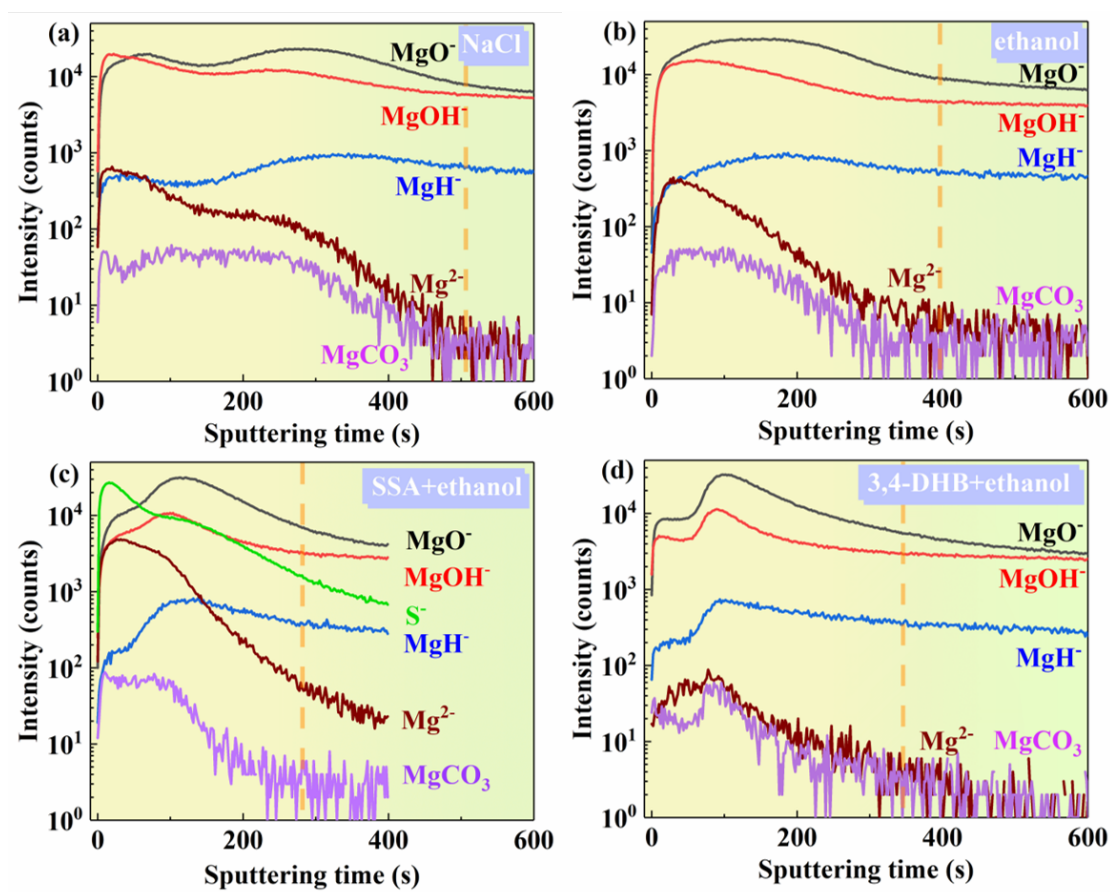


**Fig. 11.** Cross-sectional SEM images of discharged specimen at different current densities in various electrolytes.

Real-time hydrogen test reflects the weight loss as it is deduced from  $\Delta W_{self-corr}$ . The presence of ethanol reduces  $\Delta W_{self-corr}$  at low current densities, while accelerates the self-corrosion rate of anode as current density increases. Large  $\Delta W_{self-corr}$  contributes to the low utilization efficiency in solutions with complexing agents at low current density. However, single complexing agents reduce the  $\Delta W_{chunk\ effect}$  across different current densities. Moreover,  $\Delta W_{self-corr}$  caused by SSA and 3,4-DHB is significantly reduced at  $10\text{ mA cm}^{-2}$ , leading to high discharge performance of the anode. In the case of mixture solutions (SSA and ethanol, 3,4-DHB and ethanol), they not only reduce the evolved  $\text{H}_2$  volume during discharge, but also suppress the appearances of discharge products. Therefore, both  $\Delta W_{self-corr}$  and  $\Delta W_{chunk\ effect}$  are inhibited in the presence of mixtures at  $2.5\text{ mA cm}^{-2}$ , greatly enhancing the discharge performance of anode (3,4-DHB and ethanol, SSA and ethanol). However, at high current density, these two factors (high self-corrosion rate of sample and severe chunk effect) result in the low discharge performance of the Mg anode.

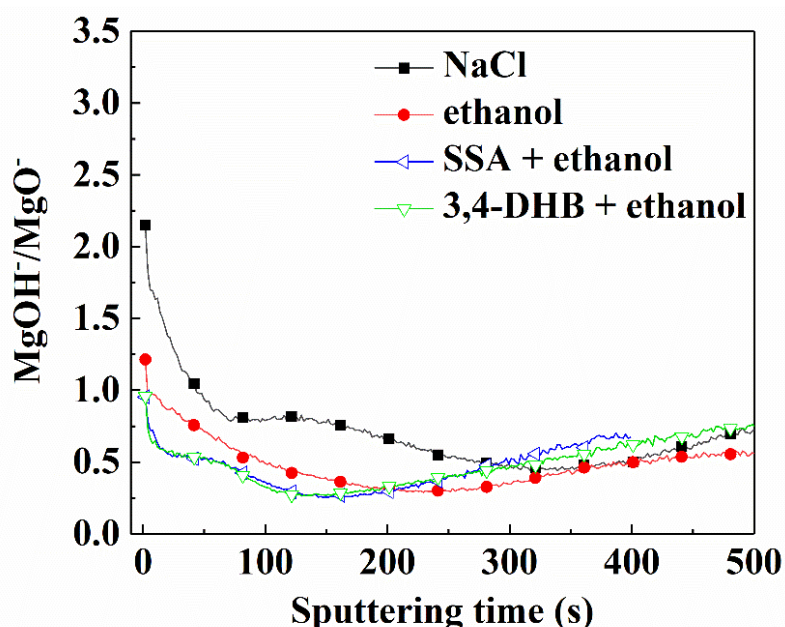
In order to understand the decreased evolution of  $\text{H}_2$  and improved utilization efficiency of Mg anode in electrolytes with ethanol and mixtures at  $2.5\text{ mA cm}^{-2}$ , ToF-SIMS negative ion depth profiles are employed to investigate the surface film layers formed on the Mg anode after 5 min of discharge (Fig. 12). Different ion intensities reflect various chemical compositions of the surface layers [37].  $\text{MgO}^-$ ,  $\text{MgOH}^-$ ,  $\text{MgH}^-$  and  $\text{MgCO}_3^-$  ions correspond to MgO, Mg(OH)<sub>2</sub> and MgCO<sub>3</sub>, respectively. The  $\text{S}^-$  signal represents SSA adsorbed on the Mg surface in SSA and ethanol containing solution. The 80 % of maximum intensity of  $\text{MgO}^-$  signal is set to evaluate the thickness of the surface layer [32, 57]. Assuming the sputtering rate of 0.1 nm/s, the thickness of total oxide-hydroxide layer was calculated and it shows a decrease in the following order: NaCl (51 nm) > ethanol (40 nm) > 3,4-DHB and ethanol (35 nm) > SSA and ethanol (28 nm) [37]. These mixtures, i.e. 3,4-DHB with ethanol and SSA with ethanol, significantly inhibit the growth of the surface layer compared to the NaCl electrolyte. The  $\text{MgOH}^-$  signal reaches its maximum intensity first in the blank NaCl solution (Fig. 12a), indicating that the outer surface layer primarily consists of Mg(OH)<sub>2</sub>. Subsequently, the  $\text{MgO}^-$  signal exhibits maximum intensity after the  $\text{MgOH}^-$  signal,

indicating that MgO contributes to the formation of the inner layer. A similar distribution of hydroxide and oxide is observed in ethanol-based electrolyte (Fig. 12b). However, it is noteworthy that the mixtures influence the distribution of the hydroxide and oxide layers. In the SSA and ethanol (Fig. 12c), 3,4-DHB and ethanol electrolytes (Fig. 12d), the maximum intensity of hydroxide ( $\text{MgOH}^-$ ) coincides almost exactly with that of the oxide ( $\text{MgO}^-$ ), indicating the formation of a more mixed oxide-hydroxide layer. Additionally, the maximum intensity of  $\text{S}^-$  appears before the peaks of  $\text{MgO}^-$  and the  $\text{Mg}^{2-}$  signals in the SSA and ethanol-containing solutions (Fig. 12c). This suggests that S-containing species are prone to depositing in the outer surface layer during discharge.



**Fig. 12.** ToF-SIMS negative in-depth ion profiles of discharge product layer after 5 min-discharge in NaCl solution with and without electrolyte additives at current density of  $2.5 \text{ mA cm}^{-2}$ .

To gain better insight into the chemical modifications of the surface layer, the ratio of  $\text{MgOH}^-$  to  $\text{MgO}^-$  is presented in Fig. 13. Initially, these ratios decrease and then increase with sputtering time, indicating different compositions of the outer and inner surface layers in various solutions. The highest content of hydroxide deposit (2.15 for  $\text{MgOH}^-$  to  $\text{MgO}^-$  ratio) in the outer surface layer is evident in the reference. In solution with ethanol, the reduction of the  $\text{MgOH}^-$  to  $\text{MgO}^-$  ratio in the outer and inner layer can be observed, implying an enrichment in  $\text{MgO}$ . Notably, mixtures significantly influence the ratio of  $\text{MgOH}^-$  to  $\text{MgO}^-$  in the outer surface layer. The ratios decrease to around 0.25 in mixtures with 3,4-DHB and SSA, indicating a substantial restriction on the growth of hydroxide in the outer layer.



**Fig. 13.** Ratio of  $\text{MgOH}^-$  and  $\text{MgO}^-$  in deposited surface layer after discharge at  $2.5 \text{ mA cm}^{-2}$  for 5 min in various solutions.

In summary, the mixtures facilitate the formation of a surface layer enriched in  $\text{MgO}$ , reducing the contact area between  $\text{H}^+$  and  $\text{Mg}$  substrate and inhibiting self-corrosion. Additionally, electrolyte additives are effective in preventing the excessive deposition of  $\text{Mg}(\text{OH})_2$  on surface, significantly reducing the cathodic sites (dark regions) for HER [58-60]. This is reflected by the low self-corrosion rate observed during discharge in ethanol and mixture solutions. Interestingly, the  $\text{Mg}$  anode exhibits lower  $\text{H}_2$  evolution

in mixtures compared to ethanol-containing solutions. As seen in Fig. 12c and d, a relatively thin layer deposits on the surface in mixtures compared to other solutions. S-containing species are clearly observed in the outer surface layer of the Mg surface in SSA and ethanol solution. Moreover, the ratio of  $\text{MgOH}^-$  to  $\text{MgO}^-$  confirms that the outer layer consists has a high portion of MgO in the presence of mixtures. This MgO rich layer blocks the cathodic sites and inhibits the continuous growth of the hydroxide-rich layer on the surface. The presence of S-like species and high content of MgO together form a compact layer, resulting in the lowest HER of the anode in mixtures among these electrolytes during discharge.

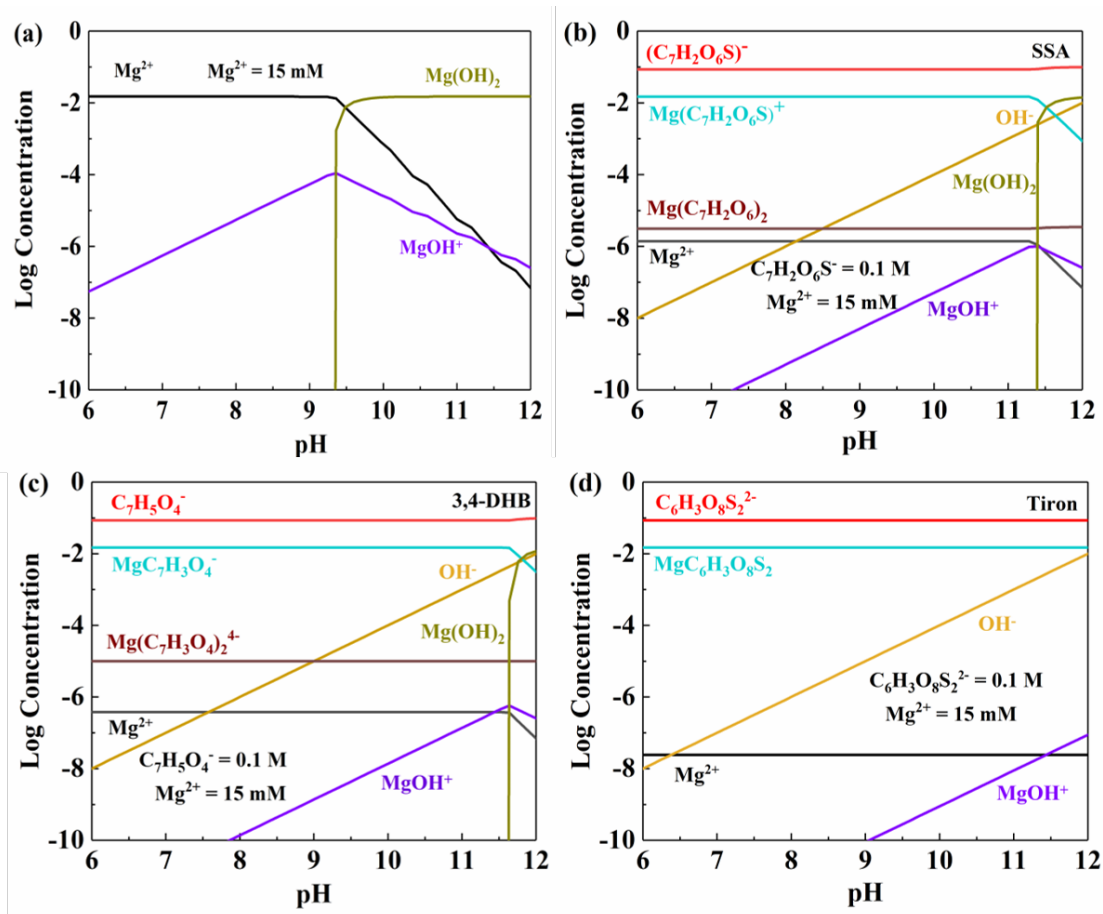
#### 4. Discussion

In the present work, the influence of various additives on the electrochemical performance of Mg sample is systematically studied by means of electrochemical tests and surface analysis. Ethanol reduces the free  $\text{H}^+$  in the electrolyte and leads to high solution resistance, which is detrimental to discharge voltage. At low current densities, addition of ethanol results in the formation of an oxide-rich inner surface layer, restricting the reaction between  $\text{H}^+$  and Mg matrix during discharge. Furthermore, ethanol inhibits the formation of  $\text{Mg}(\text{OH})_2$  on surface, reducing the cathodic sites for HER. Thus, high utilization efficiency of Mg anode with addition of ethanol is achieved at low current densities. As current density increases, discharge products tend to deposit on surface as demonstrated in Fig. 5f. Large amounts of  $\text{Mg}(\text{OH})_2$  on the surface act as strong local cathodes, significantly increasing HER during the discharge process [58]. Consequently, undissolved Mg matrix appears in discharge products on surface, which detaches from Mg sample without actual charge transfer [15, 18]. This large weight loss of self-corrosion process and chunk effect leads to low discharge performance.

Fig. 14 shows thermodynamic equilibrium diagram of the electrolyte after discharge in solutions containing complexing agents, simulated by Hydra/Medusa® software. Clearly, the pH of  $\text{Mg}(\text{OH})_2$  formation is set at 9.4 after discharge in reference (Fig. 14a). The pH for the accumulation of discharge products increases to 11.4 and 11.6



with addition of SSA and 3,4-DHB, respectively (Fig. 14b and c). It should be noted that Tiron hinders the formation of  $\text{Mg}(\text{OH})_2$  on the Mg surface, as depicted by the presence of  $\text{Mg}^{2+}$  complex ( $\text{MgC}_6\text{H}_3\text{O}_8\text{S}_2$ ) in the electrolyte (Fig. 14d).



**Fig. 14.** Thermodynamic calculation of the solution composition and precipitation species formed upon Mg discharge in (a) NaCl, (b) SSA, (c) 3,4-DHB and (d) Tiron.

The deposition of discharge products significantly reduces the contact area between the anode and the electrolyte, which is detrimental to the continuous discharge process. Complexing agents chelate with  $\text{Mg}^{2+}$  and inhibit the accumulation of discharge products, leading to high discharge voltage and power density. However, strong complexing agents facilitate the dissolution process, resulting in a large volume of released  $\text{H}_2$  during discharge at low current density. Strong HER is observed in the presence of complexing agents, causing significant weight loss ( $\Delta W_{self-corr}$ ).

However, at high current densities of  $10 \text{ mA cm}^{-2}$  (Fig. 10c), SSA and 3,4-DHB reduces the  $\text{H}_2$  evolution in comparison to blank NaCl solution due to lower quantity of discharge products ( $\text{Mg}(\text{OH})_2$ ) acting as cathodic sites which promote the dissolution process HER [58]. Thus, these two complexing agents are capable of reducing the cathodic effects caused by discharge products, thereby decreasing the self-corrosion rate of the anode and greatly suppressing the chunk effect. The reduced weight loss induced by  $\Delta W_{self-corr}$  and  $\Delta W_{chunk\ effect}$ , determines the high values of two parameters of anode in solutions with single complexing agent at high current densities. The introduction of ethanol into solutions containing complexing agents greatly reduces the conductivity of water-based electrolyte, which means that transfer rate of species, e.g. complexes, ( $\text{Mg}(\text{C}_7\text{H}_2\text{O}_6\text{S})^+$ ,  $\text{Mg}(\text{C}_7\text{H}_3\text{O}_4)^-$  and  $\text{Mg}(\text{C}_7\text{H}_3\text{O}_4)_2^{4-}$ ) are reduced. These species prefer to deposit/absorb into the surface layer instead of dissolving into the electrolytes, as evidenced by the deposition of S-like species detected by ToF-SIMS. However, mixtures still have the ability to reduce the amount of discharge products on surface at low current densities. Therefore, the similar discharge voltage and power density of the anode is maintained compared to that in blank NaCl solution. With the increase of current density, large  $\eta_{ct}$  and  $\eta_{diff}$  caused by discharge products, adsorbed/deposited complexes and high  $IR$  together lead to the low discharge voltage and power density of the anode. Regarding utilization efficiency and specific capacity, complexes adsorb/deposit in the outer surface layer, which further reduces the area exposed to electrolyte and hinders the growth of hydroxide-rich layer on surface. A thin surface layer, consisting of complexes and  $\text{MgO}$ , inhibits the HER during discharge, leading to low weight loss from the self-corrosion process. Low weight loss of  $\Delta W_{self-corr}$  and  $\Delta W_{chunk\ effect}$  synergistically results in a relatively high utilization efficiency in mixtures at low current densities. However, mixtures are insufficient to chelate large amounts of generated  $\text{Mg}^{2+}$  at high current density. Therefore, large amounts of discharge products, deposit on surface and form local cathodic sites, which increase the self-corrosion rate of the anode. At the same time, the chunk effect is

evident in discharge products and detaches into the electrolytes, further reducing the actual mass loss of Mg anode.

## 5. Conclusions

(1) A mixture of 30 vol% ethanol and 0.1 M complexing agent has been utilized for the first time as the electrolyte in Mg-air battery. Mg anode shows great discharge performance in NaCl solution with 30 vol% ethanol and 0.1 M 3,4-DHB, achieving utilization efficiency of 85.7%.

(2) 30 vol% ethanol reduces the free  $H^+$  and promotes the formation of double surface layer (hydroxide outer layer and oxide-rich inner layer). However, in the mixtures the mixed oxide-hydroxide layer with a decreased quantity of hydroxide can be observed. This type of layer hinders the formation of cathodic sites and decreases of self-corrosion rate of anode.

(3) The adsorption/deposition of complexes in outer surface layer inhibits the growth of hydroxide-rich layer. The thin surface layer, primarily composed of complexes and MgO, along with the inhibited chunk effect, result in the highest utilization efficiency and specific capacity of Mg anode among various solutions.

### Author Contributions

Yuxin Zhou: Conceptualization, Methodology, Investigation, Writing- Original draft preparation. Xiaopeng Lu: Conceptualization, Investigation, Writing- Reviewing and Editing, Supervision, Funding acquisition. Jolanta Światowska: Conceptualization, Supervision, Data curation, Writing- Reviewing and Editing. Antoine Seyeux: Formal analysis, Data curation. Fuhui Wang: Writing- Reviewing and Editing, Supervision, Funding acquisition.

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### **Conflicts of interest or competing interests**

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

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