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Depolymerization of fractionated wood by hydrothermal liquefaction

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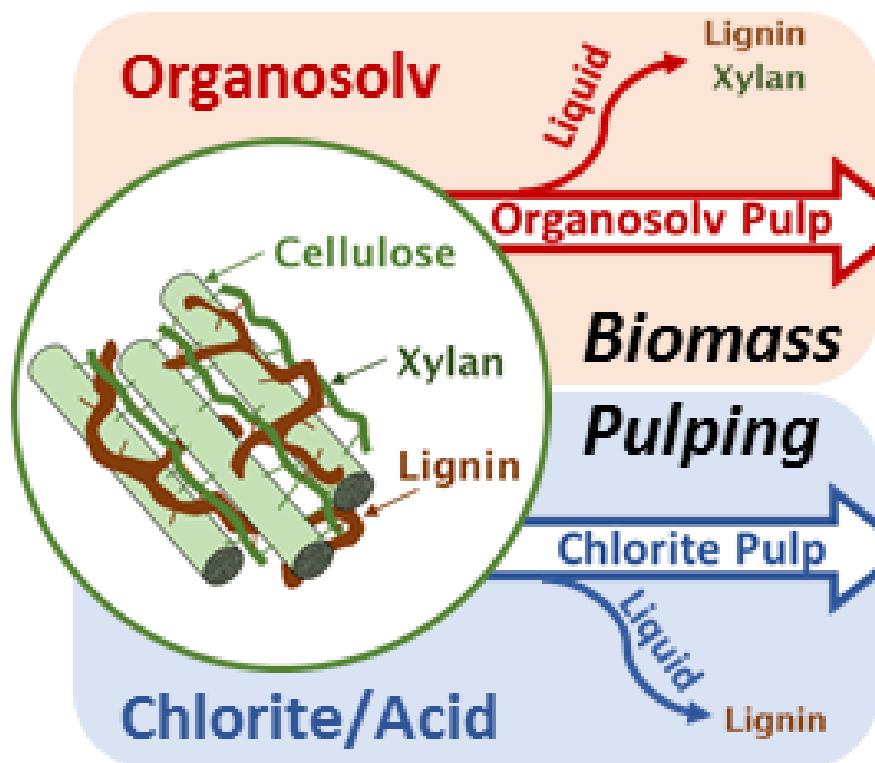


Hydrothermal liquefaction of fractionated wood

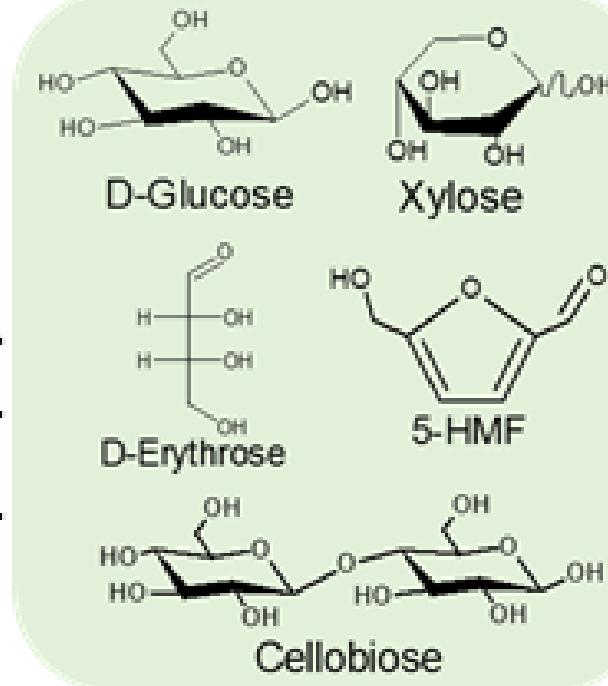
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Hydrothermal liquefaction of cellulosic pulps



Hot-compressed water



1. Liquefaction of pure cellulose (operating conditions)
2. Fractionation of beech wood and then hydrothermal liquefaction of the cellulosic pulp
 - Batch reactor
 - Semi-continuous reactor

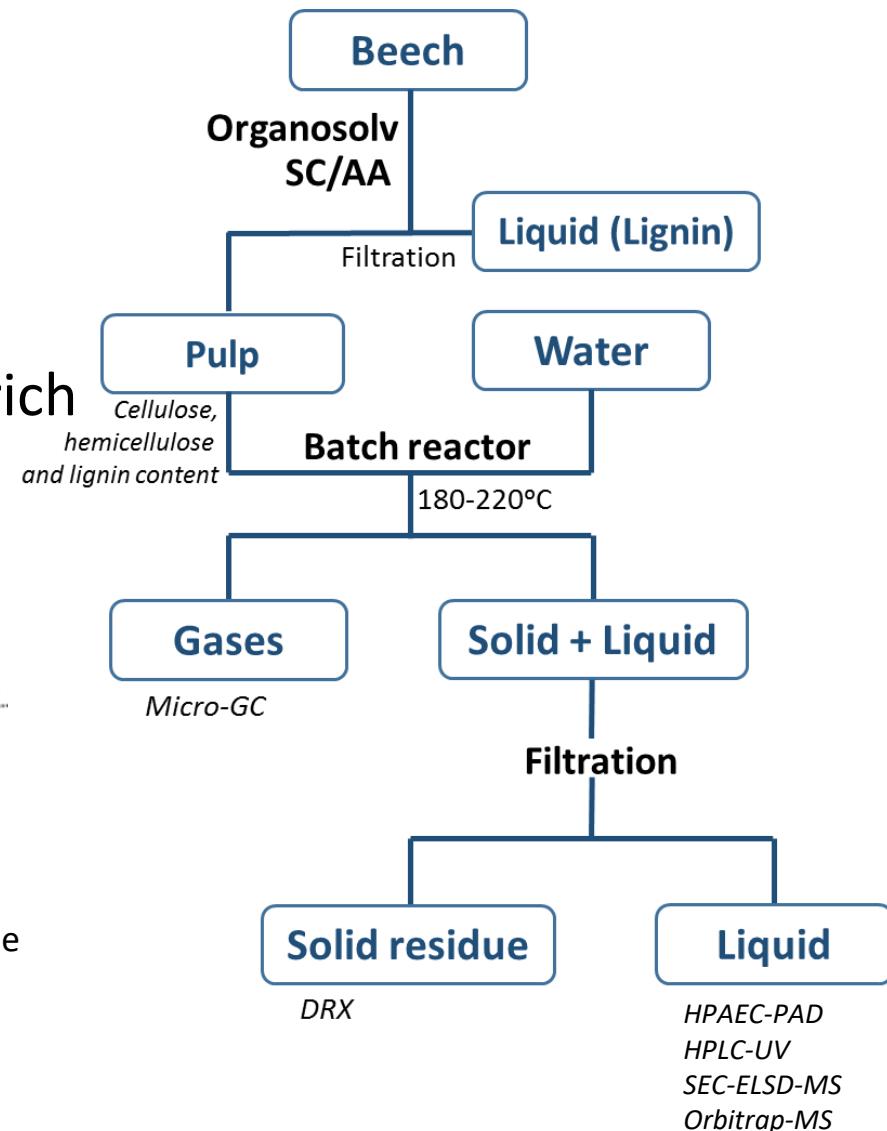
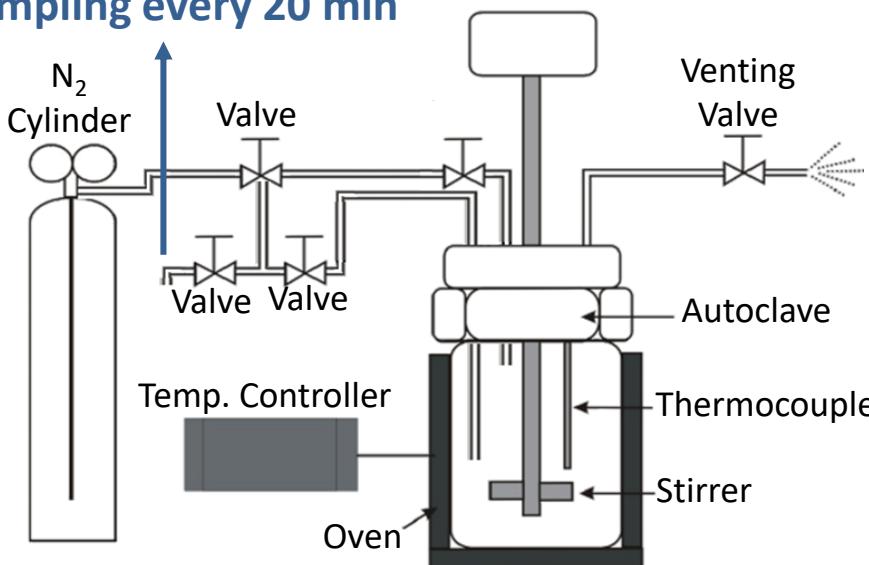
Hydrothermal Liquefaction (Batch)

Fractioning:

- Organosolv ($\text{EtOH}/\text{H}_2\text{O}$)
180°C, 1h, H_2SO_4
- S. Chlorite/A. Acid
70°C, 6h (glass reactor)

Solid= Cellulosic pulp, Liquid= lignin rich

Sampling every 20 min



Analytical methods

Gas products

- Permanent gases
- μ GC-TCD

Soluble products

Composition Screening

- SEC-ELSD/MS

Carbohydrates/Volatiles

- Total carbohydrates
- HPAEC-PAD
- LC-LTQ-Orbitrap-MS

Organic acids

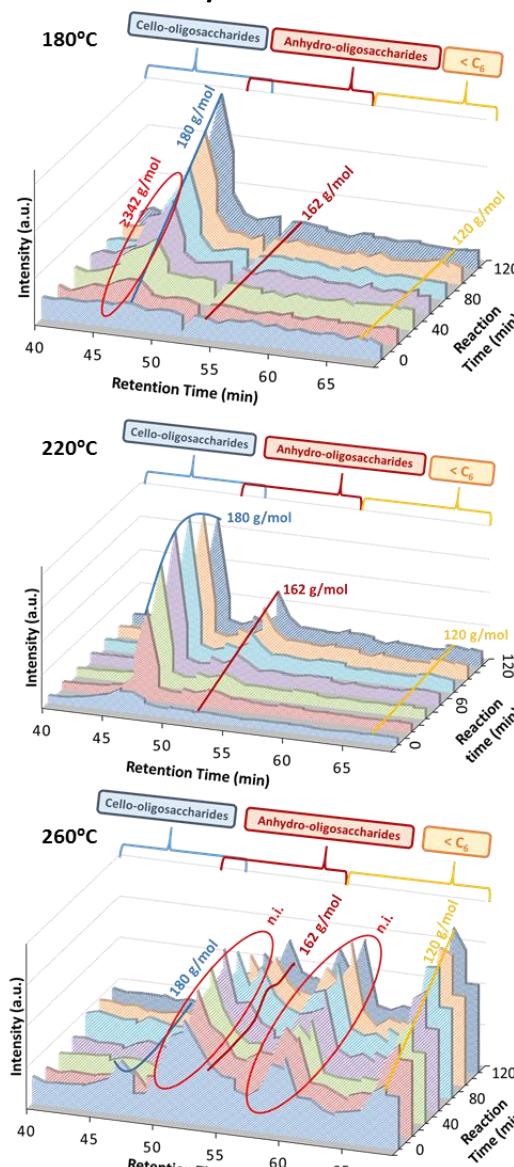
- HPLC-UV-RID

Solid residue

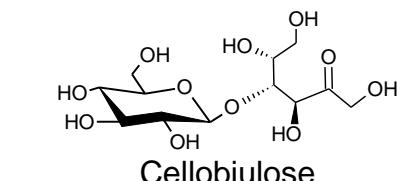
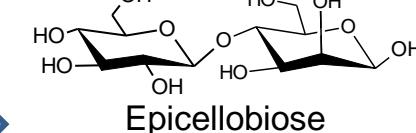
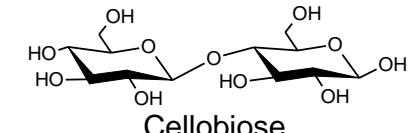
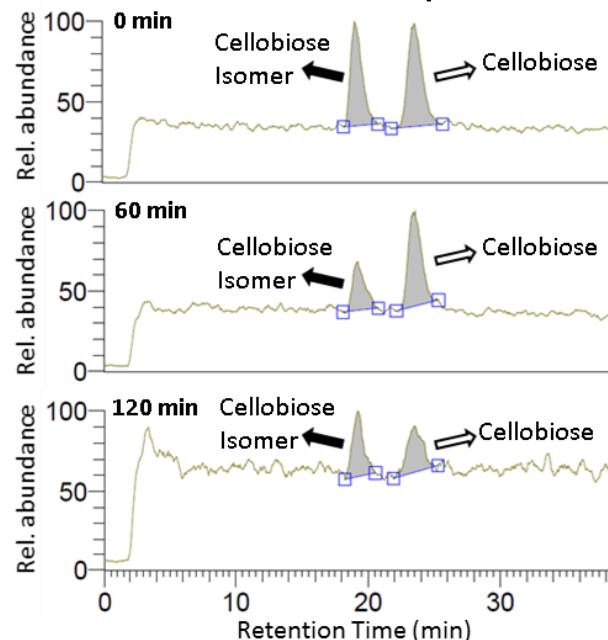
- Structure
- DRX

RESULTS

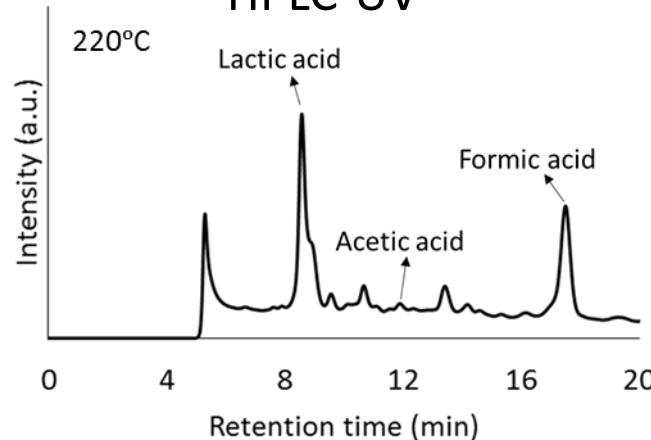
SEC/SEC-MS



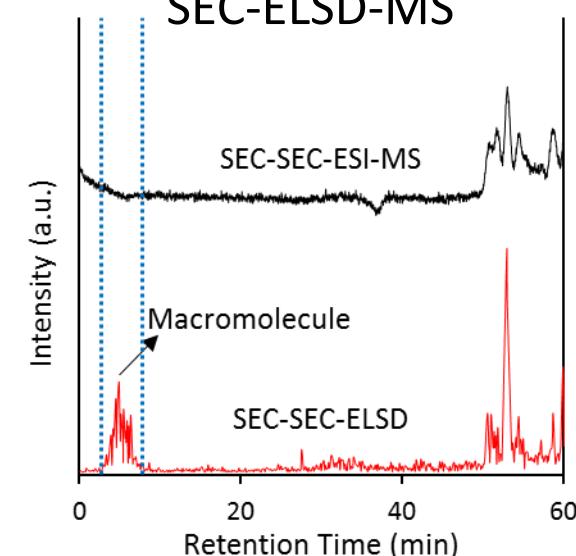
LC-LTQ-Orbitrap MS



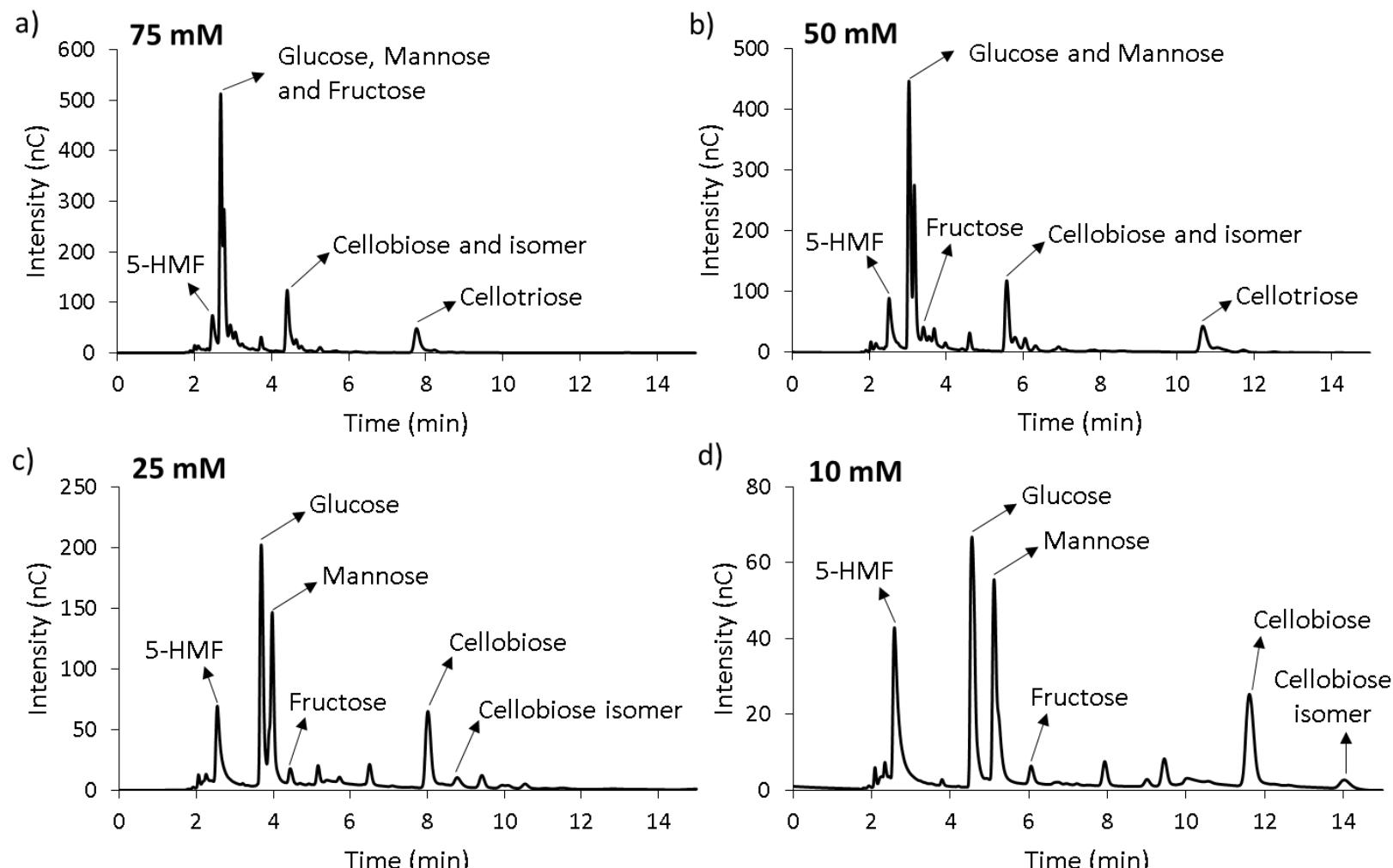
HPLC-UV



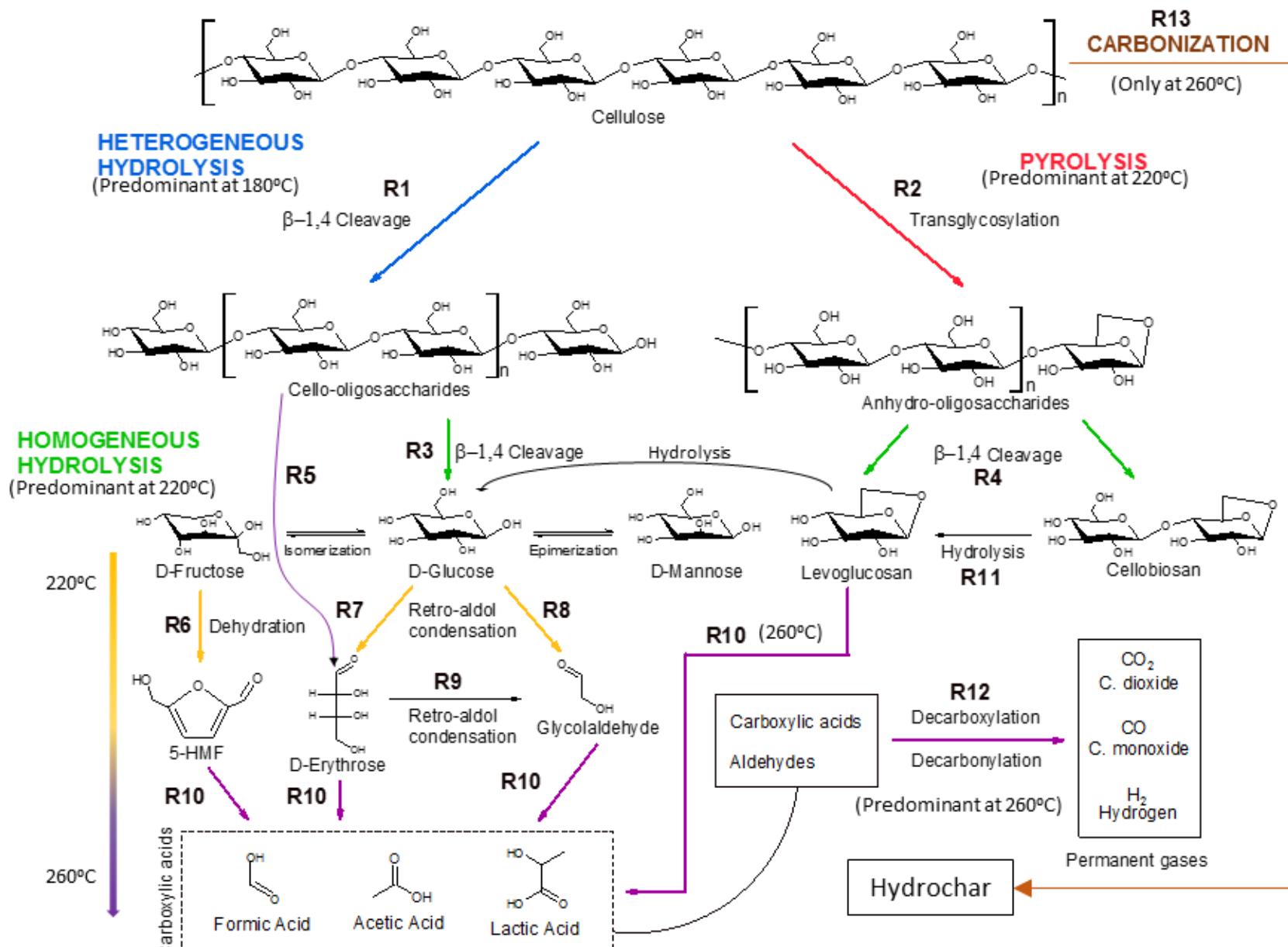
SEC-ELSD-MS



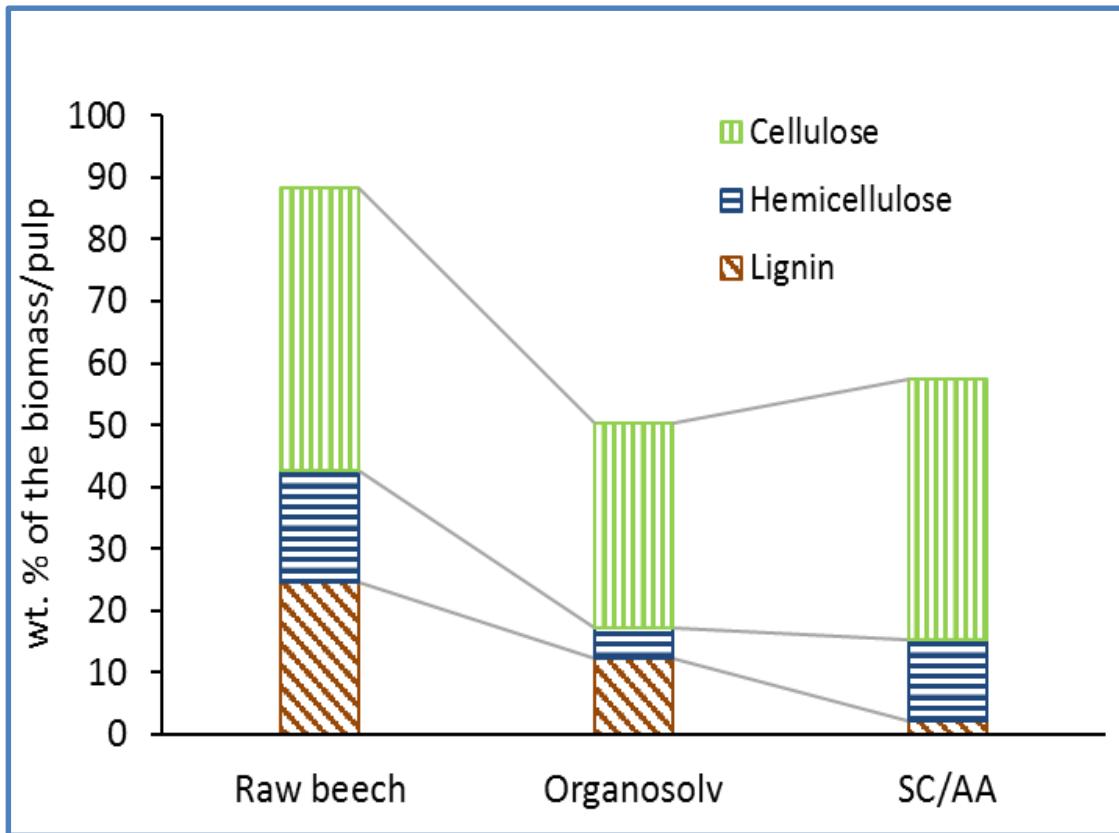
Analysis of carbohydrates by HPAEC-PAD



RESULTS



Beech wood fractionation

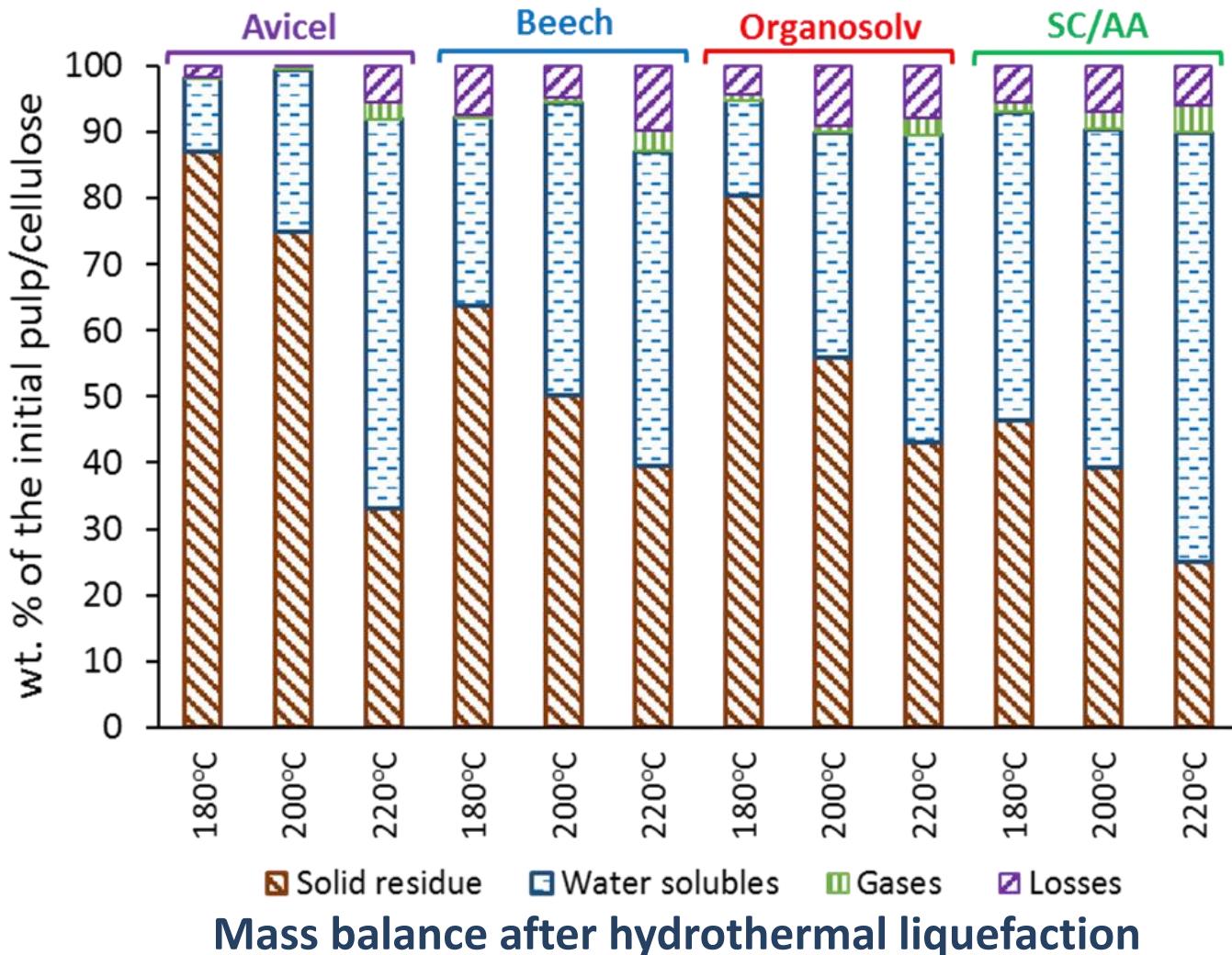


Composition of the solid fraction showing cellulose, hemicellulose and lignin content

Delignification yields	
Organosolv	= 50.4 wt.%
Chlorite/acid	= 91.3 wt.%

Cellulose recovery	
Organosolv	= 62.3 wt.%
Chlorite/acid	= 67.2 wt.%

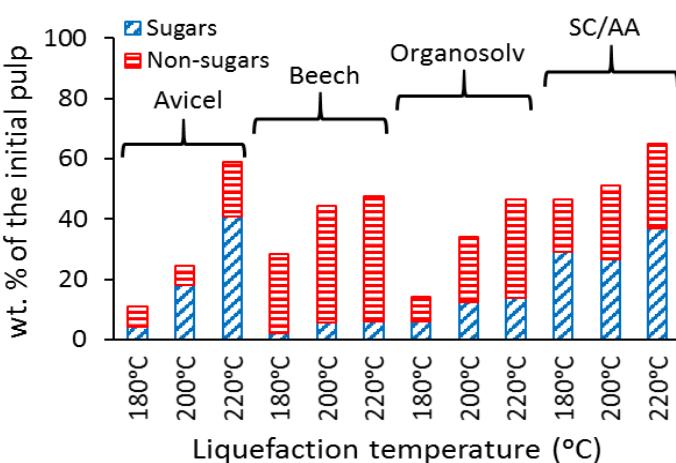
Hydrothermal liquefaction of pulps



RESULTS

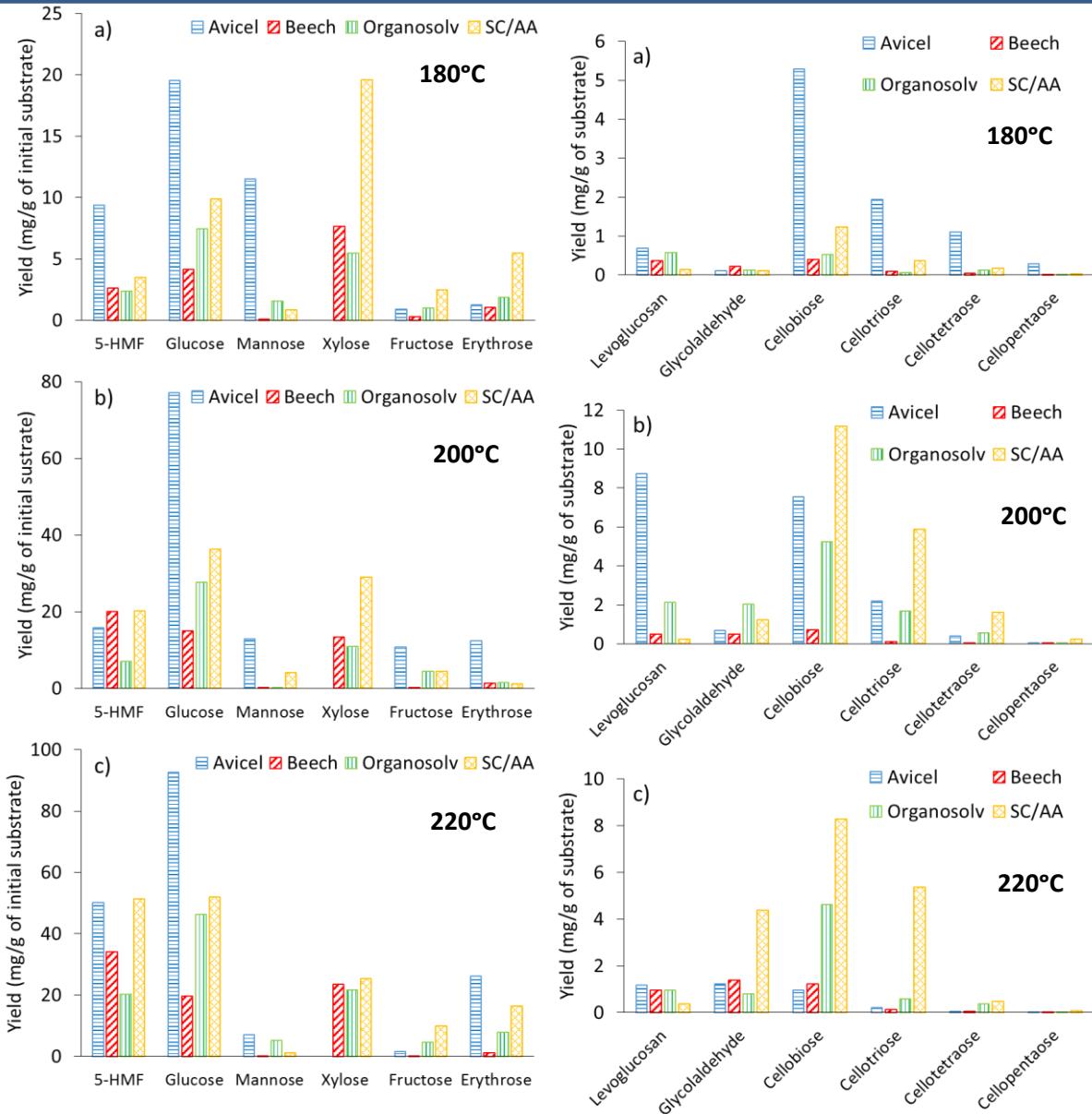
Sugar yield

Total carbohydrates and sugar quantification by HPAEC-PAD after 2 h of reaction



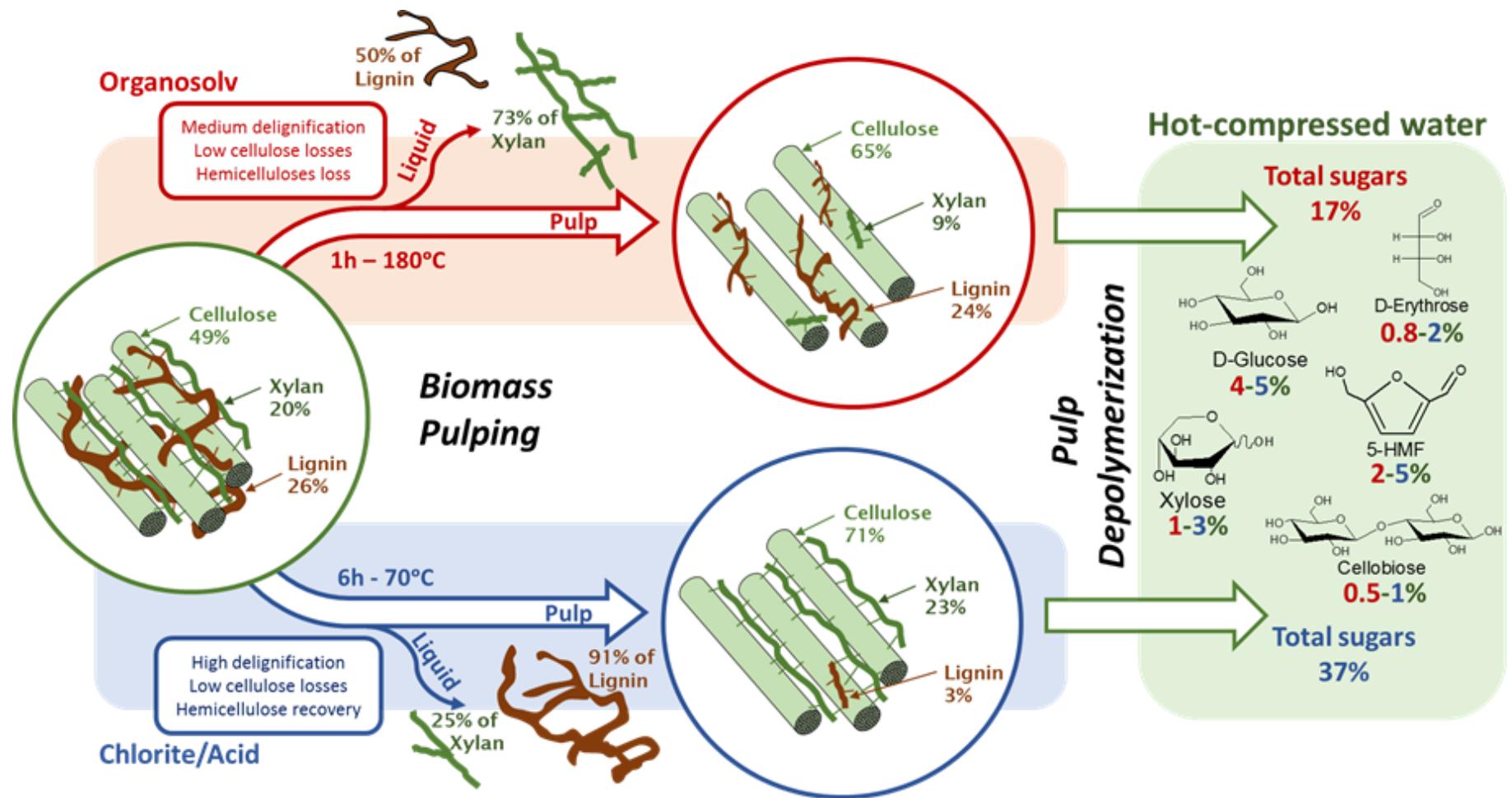
Best case at 220°C:

- Avicel=40.7 %
- Beech=6.1 %
- Organosolv=17.3 %
- SC/AA=36.8 %



RESULTS

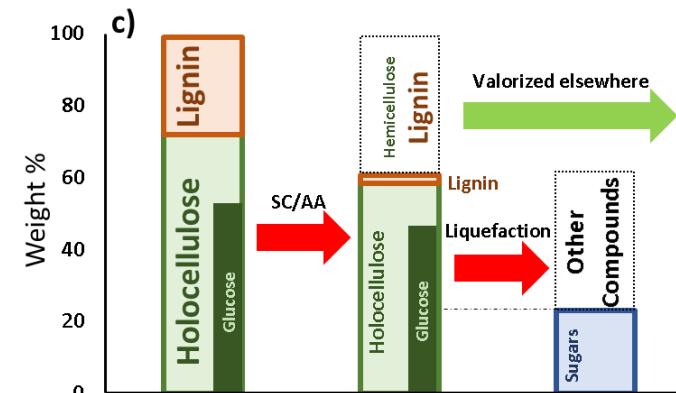
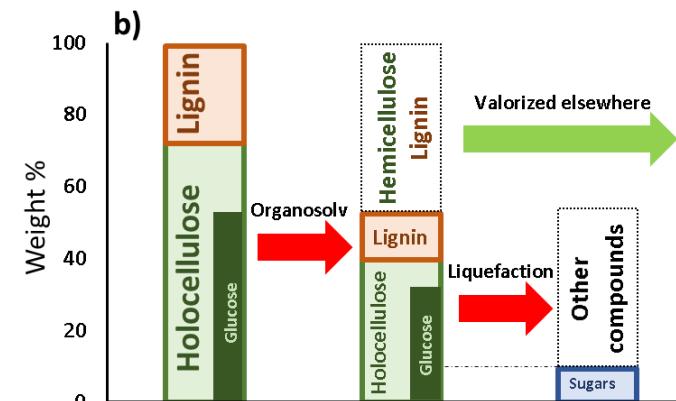
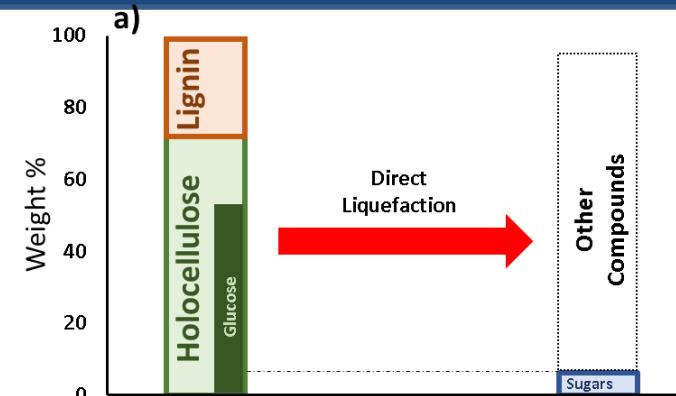
From wood to sugars



Raw Beech Batch Liquefaction

Organosolv Pulp Batch Liquefaction

SC/AA Pulp Batch Liquefaction



Liquefaction of pulps



Curtin University

Semi-continuous Reactor

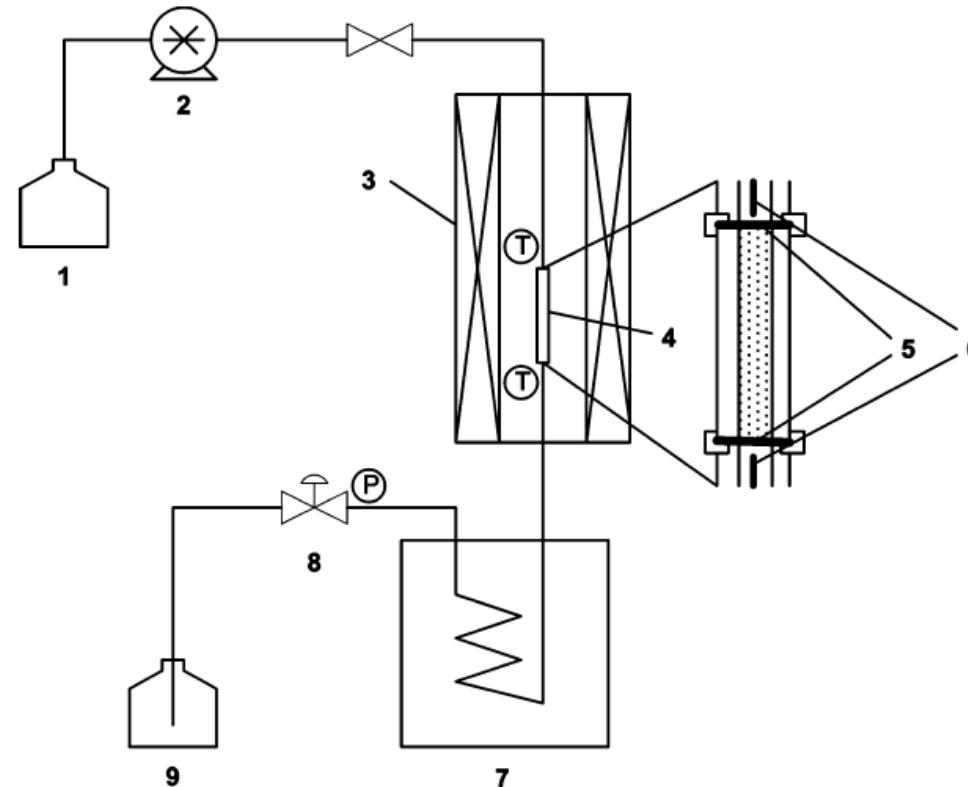
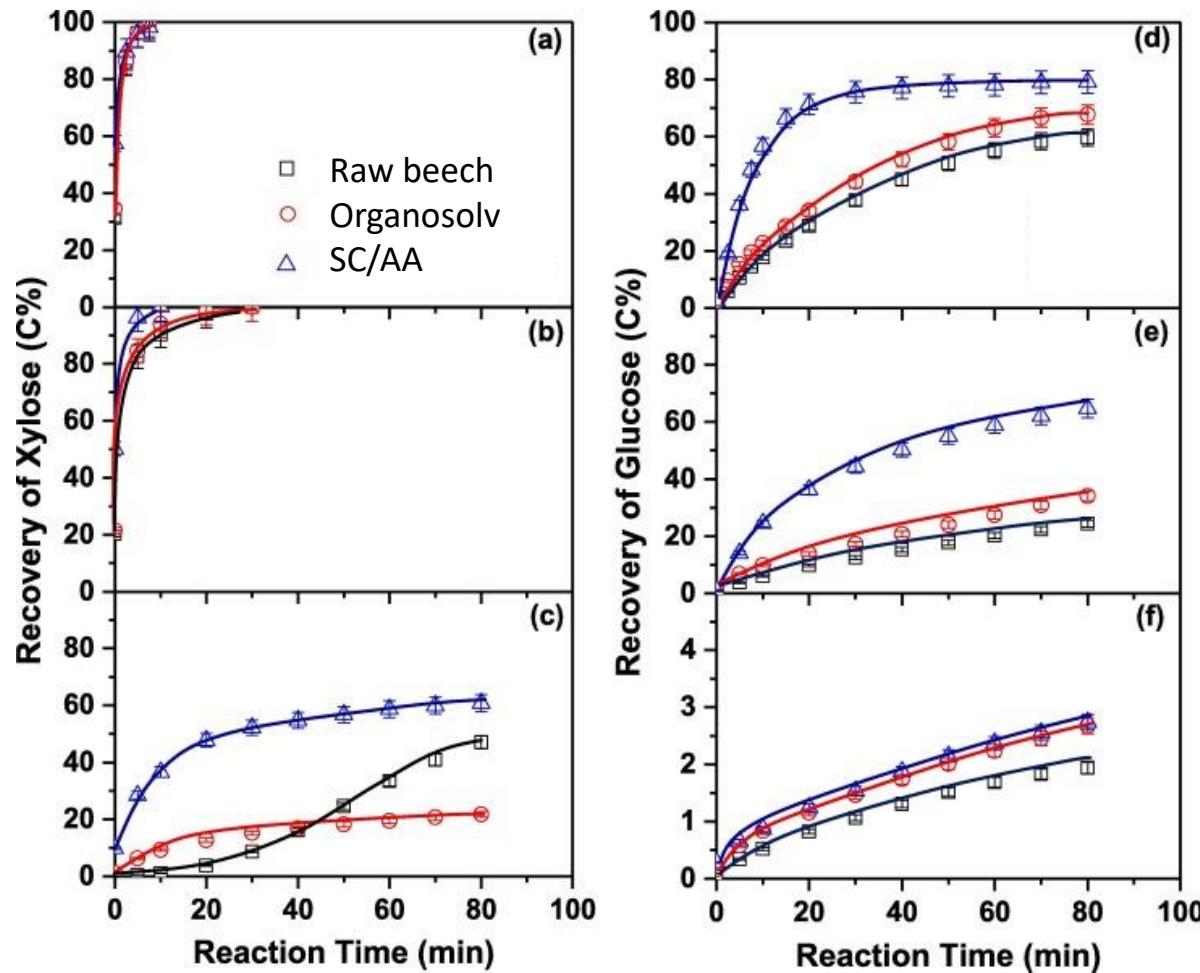


Figure 1. Schematic diagram of the semicontinuous reactor system used in this study: (1) Water reservoir; (2) HPLC pump; (3) infrared image furnace; (4) reactor; (5) sintered stainless steel filter; (6) thermocouple; (7) cooling unit; (8) back-pressure regulator; (9) liquid product collector.

Yu, Y., & Wu, H. (2009). Characteristics and precipitation of glucose oligomers in the fresh liquid products obtained from the hydrolysis of cellulose in hot-compressed water. *Ind. & Eng. Chem. Res.*

Semi-continuous liquefaction

Yields of sugar recovery (relative to the initial sugar content)



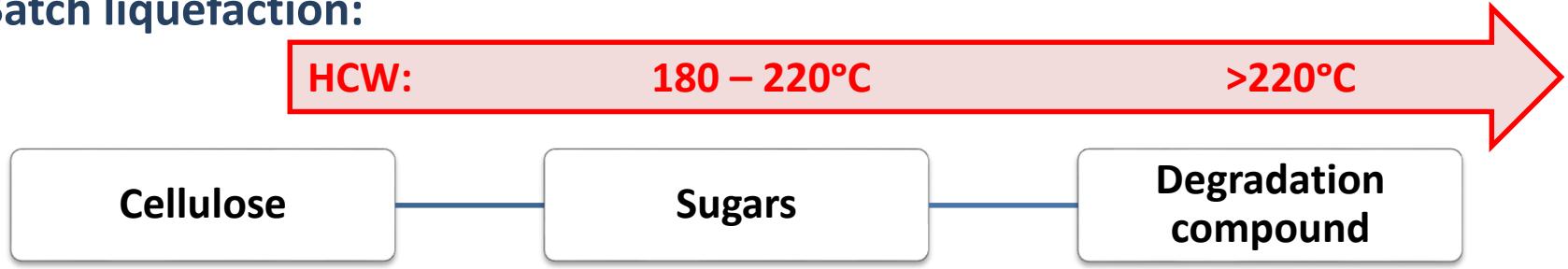
Song, B., Buendia-Kandia, F., Yu, Y., Dufour, A., & Wu, H. (2019). Importance of lignin removal in enhancing biomass hydrolysis in hot-compressed water. *Bioresource technology*

Conclusion

Fractionation:

Delignification yields of 50.4 and 91.3 % were achieved by Organosolv and SC/AA treatments.

Batch liquefaction:



Organosolv and SC/AA liquefaction pulps increased the total sugar yield relative to the raw beech wood, but yields are still low.

Semi-continuous liquefaction:

Around 95 wt.% of xylose and 80 wt.% of glucose can be recovered with temperatures around 250°C.

Thank you

