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A detonation run-up distance database: data-driven existing models improvement and new model development

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Abstract

A comprehensive database of detonation run-up distances (x_{DDT}) in unobstructed tubes/channels is compiled. Eight fuels are included, i.e., hydrogen, methane, ethane, ethylene, acetylene, propane, butane and carbon monoxide. Oxygen is used as oxidizer with different diluents under a wide range of tube/channel sizes. In total 559 points are collected and analyzed. The global x_{DDT} trends observed in the data as a function of the initial conditions (i.e., fuel type, equivalence ratio (ϕ), hydraulic diameter (D_h), and pressure (p)) reveal that x_{DDT} decreases with increasing p , decreasing D_h , and $\phi \rightarrow 1$. The correlation of the normalized run-up distance x_{DDT}/D_h with geometrical parameters and fundamental combustion properties shows that most of the variance in the experimental data can be captured by the ratio of D_h to the flame thickness (D_h/δ_f), the expansion ratio ($\sigma - 1$) and that of the Chapman-Jouguet to the laminar flame speed ($V_{CJ}/\sigma s_L$). With these, a non-linear (NLM) and a logarithmic model (LM) are proposed using a non-linear least squares regression to fit a user-defined function. The NLM and LM are shown to outperform the widely used Silvestrini and Dorofeev models by a large margin since they are capable of explaining $\sim 70 - 80\%$ of the variance in the experimental x_{DDT}/D_h data in contrast to only $\sim 20\%$ of the original Silvestrini and Dorofeev models. The poor performance of the original models is due to the limited amount of data used to determine the models constants. An update to these constants is also carried out using the database collected in this work resulting in a notable improvement of their predictive capabilities over the original models. The database is publicly available so that it can be used freely to guide future research in the combustion community (e.g., by identifying conditions where there is a lack of data), and as a test bed for further data-driven model development.

Keywords: Deflagration-to-detonation transition; detonation run-up distances; data-driven models; flame acceleration; fuel safety

Information for Colloquium Chairs and Cochairs, Editors, and Reviewers

1) Novelty and Significance Statement

The novelty of this research is the compilation of large detonation run-up distance, x_{DDT} database comprising 559 data points for 8 fuels under a wide range of experimental conditions, i.e., hydraulic channels/tubes diameters ($0.5 \leq D_h \leq 406$ mm), equivalence ratios ($0.2 \leq \phi \leq 5.8$), diluents (N_2 , Ar, He, CO_2), initial pressure ($0.1 \leq p \leq 25$ bar), and temperature ($298 \leq T \leq 473$ K). It is significant because with this database two data-driven models were developed capable of explaining $\sim 70 - 80\%$ of the variance in the experimental x_{DDT}/D_h data in contrast to only $\sim 20\%$ that the most widely used correlations currently capture (e.g., Silvestrini and Dorofeev). This constitutes a sizeable advancement over the state of the art. Moreover, the database is freely available to the combustion community so that anyone can exploit the synergies between physics-based reasoning and data-driven learning.

2) Author Contributions

- **C. Mejía-Botero:** performed the research, analyzed data, wrote the paper
- **F. Virost:** analyzed data, reviewed & edited.
- **L.F. Figueira da Silva:** analyzed data, reviewed & edited.
- **J. Melguizo-Gavilanes:** designed the research, analyzed data, wrote the paper, reviewed & edited.

3) Authors' Preference and Justification for Mode of Presentation at the Symposium

The authors prefer **OPP** presentation at the Symposium, for the following reasons:

- The subject is approached originally and the focus is placed on outcomes and results
- Our contribution is expected to prompt/benefit from fruitful room-audience-level discussions
- An extensive database (559 points) for x_{DDT} in unobstructed channels is compiled
- The most widely-used correlations for x_{DDT} predictions are shown to perform poorly against our database
- Well-known models are challenged and 2 data-driven alternatives that capture 70 – 80% of the experimental variance are proposed

1. Introduction

Under certain conditions, after accidental ignition of a reactive cloud, the initial flame may accelerate and transit to detonation, the so-called, deflagration-to-detonation-transition (DDT) phenomenon. Detonation is a supersonic combustion propagation regime that is much stronger and more destructive than a flame. Although in most cases DDT occurs due to flame/shock/obstacles interactions, it can also occur in unobstructed spaces, such as gas compartments and hoses in fuel cells, battery packs, electrolyzers, among others. The DDT run-up distance, x_{DDT} , is the distance between the ignition of the flame and the onset of detonation. The determination of x_{DDT} is not only important for safety but also for the optimal design of pulse detonation engines (PDE) [1].

One way to estimate x_{DDT} is using experimental data together with phenomenological models. For the latter, those proposed by Silvestrini et al. [2] and Dorofeev et al. [3] are the most widely used for predicting x_{DDT} in unobstructed channels. In [2] an expression for x_{DDT}/D_h is proposed, where D_h is the hydraulic diameter of the tube/channel; hereinafter, the word channel(s) will be used to refer to either. The model assumes that the flame: (i) is ignited at the closed end and propagates towards the open end; (ii) its speed, V_F , increases exponentially with the relative axial position of the channel, x/D_h , i.e., $V_F = A\sigma s_L \exp[B(\sigma - 1)(x/D_h)(D_h/D_{\text{ref}})^n]$, where s_L is the laminar flame speed, σ is the expansion ratio, D_{ref} is a reference diameter, and A, B, and n are constants.

To estimate the constants, six $V_F(x)$ experimental data for hydrogen (H_2), propane (C_3H_8), and ethylene (C_2H_4) in air [4, 5] were used. These tests were performed in 150, 250, and 1400 mm diameter channels. Only one $V_F(x)$ profile per mixture was considered during curve fitting. The criterion to predict x_{DDT}/D_h is that V_F must achieve a critical value suitable to trigger the DDT, that is, half of the Chapman-Jouguet detonation velocity, $V_F = V_{\text{CJ}}/2$. Silvestrini's model is thus

$$\frac{x_{\text{DDT}}}{D_h} = \frac{1}{B(\sigma - 1)} \left(\frac{D_{\text{ref}}}{D_h} \right)^n \ln \left(F \frac{V_{\text{CJ}}}{\sigma s_L} \right), \quad (1)$$

where $B = 0.0061$, $n = 0.4$, $D_{\text{ref}} = 0.15$ m, and $F = 0.5/A = 0.077$. Since the constants were not determined directly using x_{DDT} data but with $V_F = f(x)$ profiles, the model prediction is limited by the $V_F = V_{\text{CJ}}/2$ assumption.

On the other hand, the model proposed in [3] is derived via a mass balance considering that the flame propagation speed is affected by the hydrodynamic boundary layer (BL) growth in the tube/channel whose relative thickness is denoted by Δ . To estimate Δ , the BL is assumed to grow linearly with the tube's wall roughness, d and axial position, x , i.e., $x/\Delta = [\ln(\Delta/d)/\kappa + K]/C$, where C , κ and K are constants. x_{DDT}/D_h is obtained upon substitution of

the latter expression into the mass balance, and assuming that DDT occurs when V_F reaches the sound speed in burnt gases, i.e., $V_F = c_b$. Dorofeev's model is

$$\frac{x_{\text{DDT}}}{D_h} = \frac{\Gamma}{C} \left[\frac{1}{\kappa} \ln \left(\Gamma \frac{D_h}{d} \right) + K \right], \quad (2)$$

$$\text{where } \Gamma = \left[\frac{c_b}{\zeta(\sigma - 1)^2 s_L} \left(\frac{\delta_f}{D_h} \right)^\xi \right]^{\frac{1}{2m+7/3}},$$

and $\delta_f = \alpha/s_L$ is the laminar flame thickness with α denoting the mixture thermal diffusivity; ζ and m are additional constants. To estimate the constants, $V_F(x)$ data from [6–10] were used. A total of nine tests, eight for $\text{H}_2\text{-O}_2$ /air mixtures and only one for hydrocarbons (HC). Four of these were performed using channels with blockage ratio ≈ 0.1 , which is known to modify the DDT behavior compared with unobstructed channels. The D_h range considered was $D_h \in [15, 520]$ mm resulting in $C = 0.2$, $\kappa = 0.4$, $K = 5.5$, $\zeta = 2.1$, $\xi = 1/3$ and $m = -0.18$.

It is evident that the models performance hinges on the appropriate determination of the constants. The limited data used in [2] and [3] did not consider a wide range of fuels, diluents, compositions/equivalence ratios (ϕ) and D_h , so their predictions are expectedly restricted. Indeed in [11], Silvestrini's model was evaluated against data from [12, 13] showing poor performance for all the experimental conditions tested. For DDT predictions, large amounts of data are required to account for the randomness/variability of the process.

To fill this gap, here, a large database is compiled using all the x_{DDT} data for unobstructed channels available in the literature. In total, 559 tests were collected, including both HCs and H_2 over a wide range of experimental conditions (D_h , ϕ , pressure (p) and temperature (T)). The constants of the Silvestrini and Dorofeev models are updated resulting in a significant improvement of their predictive capabilities. Furthermore, two additional simpler expressions that outperform the original Silvestrini and Dorofeev models by a large margin are proposed.

2. Database description

To collect the data a systematic search was performed in *Scopus*. As criteria, only scientific papers reporting experimental x_{DDT} values obtained in unobstructed channels using weak ignition sources to avoid direct detonation initiation were considered. x_{DDT} is compiled together with the mixture initial conditions, i.e., T , p , and ϕ . Geometrical information such as D_h , length (L), cross-section (CS) and boundary conditions (BC) are also included. The latter refers to channels with Closed/Closed (C/C) or Closed/Opened ends (C/O). Table 1 summarizes the data collected. A total of 36 references were reviewed. The data are split into C/O and C/C chan-

1 nels, and ordered according to the fuel used. Experi-
 2 mental data obtained for the current work in the two-
 3 directional schlieren visualization set-up described in
 4 [14, 15] are included as well.

5 2.1. Geometrical parameters

6 The ranges of L and D_h for which data were found
 7 are $L \in [0.4, 40]$ m and $D_h \in [0.6, 406]$ mm, and
 8 $L \in [0.8, 24]$ m and $D_h \in [0.5, 159]$ mm for C/O
 9 and C/C channels, respectively. The minimum and
 10 maximum L/D_h ratios in the dataset are $L/D_h = 6$
 11 and 4000.

12 2.2. Mixtures and initial conditions

13 A total of eight fuels are included, i.e., H_2 ,
 14 methane (CH_4), ethane (C_2H_6), C_2H_4 , acetylene
 15 (C_2H_2), C_3H_8 , butane (C_4H_{10}) and carbon monox-
 16 ide (CO). Almost all are fuels of a single component,
 17 except for some in [30] that correspond to CH_4/C_2H_6 ,
 18 some in [26] that used H_2/C_3H_8 , and some mea-
 19 sured by the current authors using H_2/CH_4 blends.
 20 Oxygen (O_2) is the oxidizer. Nitrogen (N_2), helium
 21 (He), argon (Ar) and carbon dioxide (CO_2) are used
 22 as diluents. The initial conditions ranges are $T \in$
 23 [298, 473] K, $p \in [0.1, 25]$ bar, and $\phi \in [0.2, 5.8]$.

24 2.3. Number of data points and distribution

25 Table 1 also shows the number of data points (DP)
 26 per fuel. 202 and 357 DP were collected for C/O and
 27 C/C which correspond to a total of 559 tests. H_2 and
 28 C_2H_4 are the most often used fuels, with 193 and 191
 29 DP, respectively. These are followed by C_3H_8 (95
 30 DP), and CH_4 (29 DP). The less used are C_2H_2 (18),
 31 CO (15 DP), C_2H_6 (9 DP), and C_4H_{10} (9 DP).

32 Figure 1 shows the D_h , Φ and p histograms for
 33 (a) C/C, and (b) C/O. Tests carried out with H_2 and
 34 HC are plotted with different colors; the 15 DP with
 35 CO are not included. The histograms reveal that for
 36 both BCs most of the tests were performed in chan-
 37 nels with $D_h \leq 50$ mm.

38 Regarding mixture compositions, the normalized
 39 equivalence ratio, $\Phi = \phi/(1 + \phi)$ is used to cen-
 40 ter the distribution at $\phi = 1.0$ (i.e., $\Phi = 0.5$). For
 41 C/O, most of the tests are performed with HC fuels of
 42 which 81 DP correspond to stoichiometric ($\Phi = 0.5$),
 43 28 to lean ($\Phi < 0.5$), and 37 to rich ($\Phi > 0.5$)
 44 conditions. For H_2 , 29 DP correspond to $\Phi = 0.5$, 11
 45 to $\Phi < 0.5$, and 16 to $\Phi > 0.5$. For C/C, the data
 46 is distributed as follows: 171 DP at $\Phi = 0.5$, 14 at
 47 $\Phi < 0.5$, and 20 at $\Phi > 0.5$ for HC mixtures. For
 48 H_2 mixtures, 81 DP correspond to $\Phi = 0.5$, 29 to
 49 $\Phi < 0.5$, and 27 to $\Phi > 0.5$. Finally, the p histogram
 50 shows, expectedly, that all the tests with C/O channels
 51 are performed at atmospheric pressure, i.e., $p \approx 1$ bar.
 52 For C/C, most of the tests are carried out at $p < 1$ bar
 53 with 157 and 14 DP for HC and H_2 mixtures, respec-
 54 tively. For $p > 1.0$ bar, 21 (HC) and 92 (H_2) DP were

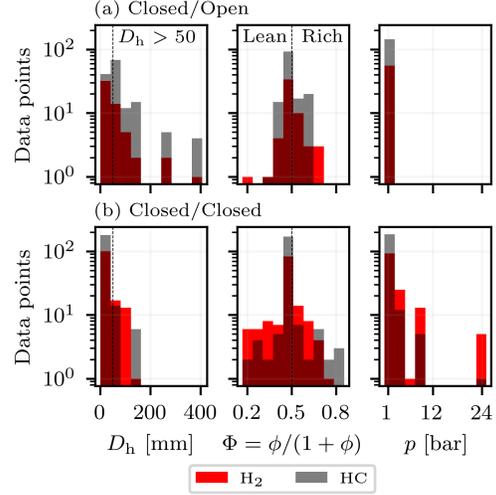


Fig. 1: Histograms for D_h , Φ and p . (a) Closed/Open; (b) Closed/Closed channels.

55 found, and at $p = 1.0$ bar, 27 (HC) and 31 (H_2) DP
 56 were collected

57 A key advantage of this visualization is that it per-
 58 mits to identify regions where there is little to no data
 59 available in the literature. This may serve as a guide
 60 for future DDT research. As an example, only 9 data
 61 points were collected at 473 K for C/C channels [22].
 62 The remaining of the data were obtained at room tem-
 63 perature, i.e., ≈ 298 K. This shows high research
 64 potential of the effect of T on x_{DDT} in unobstructed
 65 channels since most of the industrial processes where
 66 DDT may occur are either at high T , e.g., electrolyz-
 67 ers and nuclear reactors, or low T , e.g., cryogenic fuel
 68 or oxidizer transportation. Additionally, the lack of
 69 data for $D_h > 50$ mm is evident, which corresponds
 70 to most of the industrial pipelines in service. Data is
 71 missing for C_2H_2 , C_2H_6 , and C_4H_{10} , HC extensively
 72 used in many industries. Likewise for CO, of interest
 73 because it is one of the main components of Syngas
 74 which is expected to play an important role in the en-
 75 ergy transition. Finally, note that most data exist at
 76 stoichiometric conditions but many accidents are the
 77 result of accidental ignition of a reactive cloud after
 78 leakage/mixing of fuel/oxidizer effectively resulting
 79 in scenarios where lean/rich mixtures are present.

80 2.4. Preprocessing of database

81 Three conditions were identified for which the
 82 DP follow different trends compared to most of the
 83 tests in the database: (i) channels with $D_h < 3$ mm;
 84 123 DP from [23–25, 33–35, 41, 42]. These include
 85 tests with both H_2 and HC for C/O and C/C at
 86 $\phi \in [0.7, 1.7]$, and $p \in [0.1, 2.4]$ bar performed
 87 mostly in spiral channels or with central ignition.
 88 (ii) channels with non-unity aspect ratio (AR); 119
 89 DP from [27, 36] with AR ranging from 1:1.5 to

Table 1: Database summary.

Fuel	BC	ϕ	Diluents	D_h [mm]	L [m]	p [bar]	CS	DP	References
H ₂	C/O	0.25 – 2.1	N ₂ , Ar, He	3 – 406	1 – 40	1	Cir.; Sqr.	56	[5, 11, 12, 14, 16–21], CW
	C/C	0.2 – 2.8	N ₂ , Ar, He, CO ₂	0.5 – 159	0.8 – 24	0.1 – 25	Cir.; Rec.	137	[6, 7, 13, 22–29]
CH ₄	C/O	1.0	N ₂	10 – 50	1 – 11	1	Cir.; Sqr.	12	[11, 15, 18, 30], CW
	C/C	0.35 – 2.0	N ₂	15 – 20	1.5 – 2.9	0.3 – 25	Cir.; Sqr.	17	[22, 31]
C ₂ H ₂	C/O	–	–	–	–	–	–	–	–
	C/C	0.27 – 5.8	N ₂	15	2.9	1 – 5	Cir.	18	[22]
C ₂ H ₄	C/O	0.63 – 1.7	N ₂	0.6 – 406	0.4 – 40	1	Cir.; Sqr.	55	[5, 11, 18, 32–35]
	C/C	0.35 – 2.7	N ₂	10 – 127	1 – 6	0.1 – 1.7	Cir.; Rec.	136	[7, 28, 36–39]
C ₂ H ₆	C/O	1.0	N ₂	26 – 50	2 – 11	1	Cir.	9	[18, 30]
	C/C	–	–	–	–	–	–	–	–
C ₃ H ₈	C/O	0.5 – 1.7	N ₂	25.4 – 406	0.5 – 40	1	Cir.	61	[5, 11, 30, 32, 40]
	C/C	1.0	N ₂	0.5 – 3	2	0.1 – 1	Cir.	34	[26, 41]
C ₄ H ₁₀	C/O	1.0	N ₂	50.8	11	1	Cir.	9	[30]
	C/C	–	–	–	–	–	–	–	–
CO	C/O	–	–	–	–	–	–	–	–
	C/C	0.4 – 2.0	–	50	2.9	5 – 25	Cir.	15	[22]

Legend: current work (CW); circular (Cir.); square (Sqr.); rectangular (Rec.). Refs. [27, 36] include channels with AR \neq 1.

1 1:30. These include tests with stoichiometric H₂ and
 2 C₂H₄ at $p < 0.7$ bar. (iii) the use of CO as fuel,
 3 with 15 DP from [22]; these tests were carried out
 4 at high pressure, i.e., $p \in [5 - 25]$ bar. Only data
 5 that did not meet the conditions above are considered
 6 in the analysis that follows. A total of 302 DP are
 7 thus retained after filtering: 132 for H₂ and 170
 8 for HC mixtures. The final experimental ranges are
 9 $D_h \in [3, 406]$ mm, $\phi \in [0.2, 5.8]$, $p \in [0.12, 25]$ bar,
 10 and $T \in [298, 474]$ K.

11
 12 The database and scripts will be made publicly
 13 available as a github repository.

14 3. x_{DDT} trends

15 3.1. x_{DDT} vs. D_h , Φ , and p

16 It is of practical interest (safety/propulsion) to
 17 identify/verify the general dependence of x_{DDT} on geo-
 18 metrical and initial conditions. Figure 2 shows these
 19 trends as a function of D_h , Φ , and p . For ease of visu-
 20 alization, selected cases were taken from the database
 21 to isolate the effect of the respective variable on x_{DDT} ,
 22 however, the trends hold for all mixtures considered.
 23 Concerning D_h , stoichiometric ($\Phi = 0.5$) H₂/air and
 24 C₂H₄/air at $p = 1$ bar from [5, 16, 32]. The plot
 25 shows that x_{DDT} increases almost linearly with D_h
 26 for both mixtures. Regarding Φ , H₂/air and C₃H₈/air
 27 mixtures from [16, 32] tested in $D_h = 50$ mm chan-
 28 nels at $p = 1$ bar. A U-shape curve is observed with
 29 x_{DDT} exhibiting a minimum around $\Phi = 0.5$. Finally
 30 for p , part of the experiments presented in [22]
 31 for H₂/O₂ and CH₄/O₂ in $D_h = 15$ mm channels at
 32 $\Phi = 0.5$ are shown. There is a pronounced decrease
 33 in x_{DDT} as p increases. The trends reveal that HC-air

34 always lead to longer x_{DDT} compared to H₂-air. Con-
 35 versely, the use of pure O₂ as oxidizer significantly
 36 decreases x_{DDT} for both types of mixtures. Based on
 37 the database collected, for PDE design where short
 38 x_{DDT} values are desirable, small D_h channels at high
 39 pressure and under stoichiometric conditions using
 40 pure O₂ as oxidizer are advised; the opposite holds
 41 for safety applications.

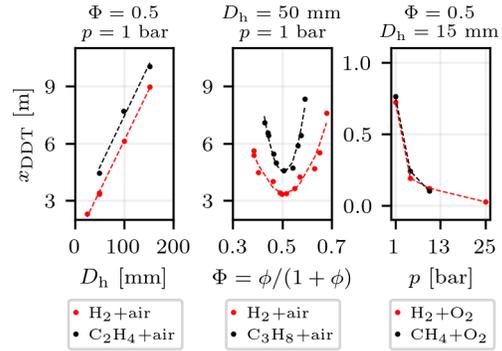


Fig. 2: x_{DDT} trends vs. D_h , Φ , and p for selected cases.

3.2. x_{DDT}/D_h vs. fundamental combustion properties

The effect on x_{DDT} of the (ratios of) fundamen-
 tal combustion properties (i.e., V_{C1}/σ_{sL} , c_b/s_L , and
 $\sigma - 1$) and that of the channel size to the laminar flame
 thickness (i.e., D_h/δ_f) used in the Silvestrini and Do-
 rofeev models is evaluated next to assess whether the
 dependencies assumed hold, and to identify poten-
 tially overlooked relevant variables. The analysis is
 carried out on x_{DDT}/D_h to absorb channel size effects

1 on the output variable. The hydraulic diameter to deto- 42
 2 onation induction length ratio, D_h/l_{ind} , the Zel'dovich 43
 3 number, $\beta = E_a(T_b - T_u)/(RT_b^2)$, and the heat capa- 44
 4 city ratio, $\gamma = c_p/c_v$, are also evaluated. E_a is the 45
 5 effective activation energy, T_b and T_u are the burnt 46
 6 and unburnt/fresh gases temperature, respectively; c_p 47
 7 and c_v are the heat capacity at constant pressure and 48
 8 volume. All properties were computed with Cantera 49
 9 using GRI 3.0 chemical mechanism, except for 50
 10 C_4H_{10} for which the San Diego mechanism was used. 51
 11 Figure 3 shows the Pearson autocorrelation matrix for 52
 12 the properties considered which measures colinearity 53
 13 between two sets of data. Values close to unity indicate 54
 14 a strong correlation, and suggest that these vari- 55
 15 ables capture the x_{DDT}/D_h dependencies observed in 56
 16 the data. 57

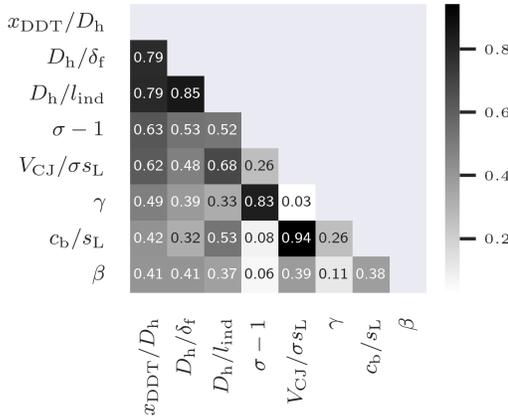


Fig. 3: Pearson autocorrelation matrix for x_{DDT}/D_h .

17 The most correlated with x_{DDT}/D_h are D_h/δ_f and 18
 19 D_h/l_{ind} , both with correlation coefficients of 0.79. 20
 21 Note however that these two variables are also correla- 22
 22 ted with each other indicating that they provide simi- 23
 23 lar statistical information about x_{DDT}/D_h . D_h/δ_f is 24
 24 retained since for flame propagation and acceleration 25
 25 δ_f is a more sensible length scale to consider. Notably, 26
 26 the latter ratio is included in Dorofeev's and not in 27
 27 Silvestrini's model. The next in line is $\sigma - 1$ which 28
 28 was found to have a strong effect on the x_{DDT}/D_h pre- 29
 29 dictions that will be presented in section 5, and to be 30
 30 highly correlated to γ ; both Silvestrini and Dorofeev 31
 31 include $\sigma - 1$ and omit γ in their models. The fol- 32
 32 lowing is V_{CJ}/σ_{sL} (used in Silvestrini) which in turn 33
 33 is correlated to c_b/s_L (used in Dorofeev). The former 34
 34 ratio is retained because of its higher correlation 35
 35 with x_{DDT}/D_h . Finally, β exhibits a correlation coef- 36
 36 ficient of 0.41. While similar to that of c_b/s_L , it does 37
 37 not seem to be correlated to any of the other variables 38
 38 considered. The addition of this property to the models 39
 39 proposed in section 5 had a very modest effect on their 40
 40 performance, consequently, it was not considered further. 41

41 Figure 4 shows the trends of x_{DDT}/D_h with D_h/δ_f , 42
 42 V_{CJ}/σ_{sL} , and $\sigma - 1$. The BC type does not seem 43

42 to have an important effect on x_{DDT}/D_h since both 43
 43 C/O and C/C follow the same behavior. D_h/δ_f is 44
 44 inversely proportional to x_{DDT}/D_h . Large D_h/δ_f val- 45
 45 ues indicate that the flame is thin compared to the 46
 46 tube/channel dimensions, which in turn favors the de- 47
 47 velopment of surface instabilities and large flame sur- 48
 48 face area. This results in increased flame accelera- 49
 49 tion leading to a decrease in x_{DDT}/D_h . On the other 50
 50 hand, x_{DDT}/D_h is directly proportional to V_{CJ}/σ_{sL} . 51
 51 A mixture with high V_{CJ} must be accelerated more 52
 52 prior to transition, and a low σ_{sL} is representative of 53
 53 mixtures with slow laminar flame speeds. It is thus 54
 54 expected that a large V_{CJ}/σ_{sL} ratio results in large 55
 55 x_{DDT}/D_h values. Finally, of interest is that $\sigma - 1$, 56
 56 exhibits different slopes for H_2 and HC while both 57
 57 being inversely proportional to x_{DDT}/D_h . The latter 58
 58 observation stems from the fact that there is a large 59
 59 difference in σ between both fuel types. For the con- 60
 60 ditions of interest (i.e., flame acceleration in channels 61
 62 ignited at the closed end), higher σ values lead to in- 63
 63 creased acceleration rates during the early stages of 64
 64 flame propagation.

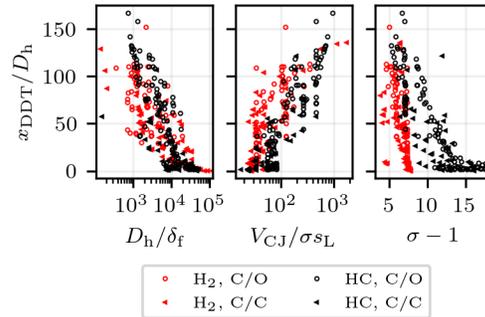


Fig. 4: x_{DDT}/D_h vs. ratios of fundamental combustion properties.

4. Existing model evaluation

4.1. Silvestrini and Dorofeev vs. database

66 Figure 5 compares the models predictions against 67
 67 the experimental database. A 45° line showing the 68
 68 ideal performance is added as a visual aid. That is, 69
 69 values that are predicted well by the models are ex- 70
 70 pected to fall on this line. Most references do not re- 71
 71 port the standard deviation of their x_{DDT} data, hence 72
 72 an arbitrarily defined deviation band of $\pm 15\%$ is plot- 73
 73 ted to account for experimental uncertainties. The coef- 74
 74 ficient of determination (R^2) is used as our metric 75
 75 to assess the models performance. It was computed 76
 76 using standard functions from the scikit-learn pack- 77
 77 age [43]. The best possible score is $R^2 = 1$ and it can 78
 78 be negative. A negative R^2 implies that a model fits 79
 79 the data worse than a horizontal line at a height equal 80
 80 to the mean of the observed data. This occurs when a 81
 81 wrong model is chosen or nonsensical constraints are 82
 82 inadvertently applied.

1 Both models performed poorly with R^2 of -0.88 42
 2 and 0.23 for Silvestrini and Dorofeev, respectively. 43
 3 R^2 was also computed for H_2 and HC mixtures separately. 44
 4 The scatter is higher for H_2 mixtures ($R_{H_2}^2 =$ 45
 5 -3.5 (Silvestrini) and -0.05 (Dorofeev)) than with 46
 6 HCs ($R_{HC}^2 = 0.54$ (Silvestrini) and 0.37 (Dorofeev)). 47

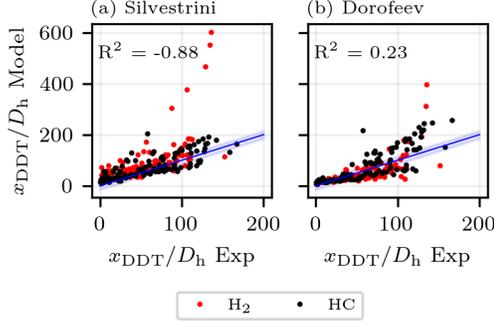


Fig. 5: Original models performance against database: a) Silvestrini and b) Dorofeev.

7 4.2. Updated Silvestrini and Dorofeev constants

8 An update to Silvestrini and Dorofeev model constants 42
 9 was done using the database collected in this 43
 10 work which includes a much wider range of operating 44
 11 conditions and fuels. As the fitting target is 45
 12 x_{DDT} rather than $V_F = f(x)$ data, it allows for 46
 13 a direct prediction/estimate of the variable of interest. 47
 14 80 % of the data were used as the training 48
 15 set and 20 % as the test set. That is, 242 DP 49
 16 were used to determine the constants and 60 DP to 50
 17 evaluate the performance of the models. To select 51
 18 these data, the `train_test_split()` function of scikit- 52
 19 learn [43] was used. It splits the data randomly 53
 20 by selecting a user-defined percentage. The initial 54
 21 conditions ranges for the training data are $D_h \in$ 55
 22 $[3, 406]$ mm, $\phi \in [0.2, 5.8]$, $p \in [0.12, 25]$ bar, 56
 23 and $T \in [298, 474]$ K, and for the test data $D_h \in$
 24 $[3, 406]$ mm, $\phi \in [0.21, 2.8]$, $p \in [0.21, 25]$ bar, and
 25 $T \in [298, 474]$ K. The fitting was carried out using
 26 the `optimize.curve_fit()` function of SciPy which
 27 essentially uses a non-linear least squares regression
 28 method to fit a function. The updated constants are
 29 listed in Table 2.

30 Figure 6 shows the fitting results with the training 52
 31 data and the performance with the test data for the 53
 32 updated a) Silvestrini, and b) Dorofeev. The 54
 33 improvement is evident with R^2 values of 0.74 and 55
 34 0.73 for the respective models. Their performance 56
 35 with the test data have R^2 of 0.7 and 0.71 , respectively.
 36 Again, this represents significant improvements compared to the original models, and indicates that $\sim 70\%$ of the variance in x_{DDT}/D_h can now be explained by the updated models. The remaining $\sim 30\%$ can be attributed to unknown lurking variables or inherent variability. Note that the model's

underlying assumptions were carefully verified to ensure that the updated constants values did not lead to non-physical flame velocities (Silvestrini) or unreasonable BL growth (Dorofeev) as a function of the axial position in the channel. Silvestrini/Dorofeev resulted in a measurable/modest increase/decrease compared to that originally obtained. The revised $V_F(x)$ and $\Delta(x)$ dependence better reflects the experimentally observed trends (not shown).

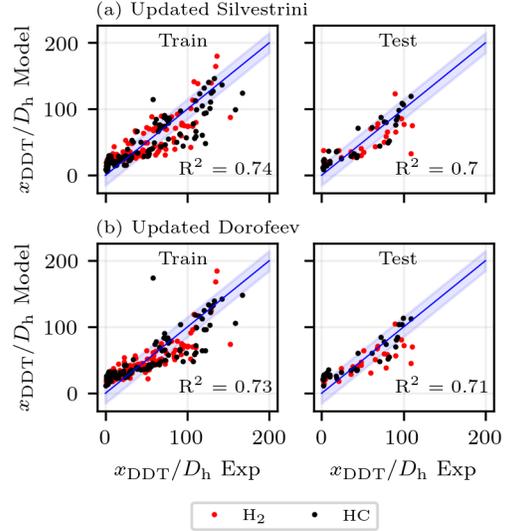


Fig. 6: Updated a) Silvestrini and b) Dorofeev performance for training and test data.

5. Proposed models

52 Two additional simpler models are proposed, i.e., 53
 54 non-linear (NLM) and logarithmic (LM), that leverage 55
 56 the learnings from the data analysis carried out in the previous sections. The expressions are shown in Equation 3, and Equation 4, respectively.

$$\frac{x_{DDT}}{D_h} = \frac{a_0}{(\sigma - 1)^{a_1}} \left(\frac{D_h}{\delta_f} \right)^{-a_2} \left(\frac{V_{CJ}}{\sigma_{SL}} \right)^{a_3}, \quad (3)$$

$$\frac{x_{DDT}}{D_h} = \frac{b_0}{(\sigma - 1)^{b_1}} \ln \left[b_2 \left(\frac{D_h}{\delta_f} \right)^{-1} \left(\frac{V_{CJ}}{\sigma_{SL}} \right) \right]. \quad (4)$$

57 NLM considers the influence of the most important 58
 59 variables discussed in subsection 3.2 to estimate four 60
 61 constants: a_0 , a_1 , a_2 , and a_3 . Note that this expression 62
 63 is general and does not take into account any information 64
 65 regarding the x_{DDT}/D_h trends observed in Figure 4. On the other hand, LM accounts for the logarithmic trend that x_{DDT}/D_h exhibits when plotted as a function of D_h/δ_f and V_{CJ}/σ_{SL} . Three constants need being estimated: b_0 , b_1 , and b_2 . The constraint $b_2 > (D_h/\delta_f)(V_{CJ}/\sigma_{SL})^{-1}$ was enforced during the

1 regression so that the argument of the natural loga-
 2 rithm is always greater than unity thereby ensuring
 3 that all the x_{DDT}/D_h estimates are positive; Table 2
 4 lists the fitting results.

Table 2: Models constants.

Model	Eq.	Constants	
		Original	Updated
Silvestrini	eq. (1)	$B = 0.0061$	$B' = 0.0057$
		$n = 0.4$	$n' = 0.07$
		$F = 0.077$	$F' = 0.084$
Dorofeev	eq. (2)	$C = 0.2$	$C' = 0.26$
		$\kappa = 0.4$	$\kappa' = 0.13$
		$K = 5.5$	$K' = -1.75$
		$\zeta = 2.1$	$\zeta' = 0.046$
		$\xi = 1/3$	$\xi' = 1.32$
		$m' = -0.18$	$m' = 1.46$
NLM	eq. (3)	$a_0 = 184$	
		$a_1 = 0.82$	
		$a_2 = 0.11$	
		$a_3 = 0.29$	
LM	eq. (4)	$b_0 = 50$	
		$b_1 = 0.7$	
		$b_2 = 4500$	

5 Figure 7 shows the fitting with the train, and
 6 the evaluation with the test data for a) NLM, and b) LM.
 7 Both train and test data are the same sets used in the
 8 previous sections to enable a meaningful comparison
 9 of the models performance. The LM has a better fit to
 10 the training data with an R^2 of 0.78 compared to 0.72
 11 for the NLM. This was also reflected in the performance
 12 with the test data, with a R^2 of 0.84 for the LM
 13 and 0.74 for the NLM. The prediction of both models
 14 is much better than that of the original Dorofeev
 15 and Silvestrini, and have higher (LM)/similar (NLM)
 16 R^2 values than those obtained with the updated Sil-
 17 vestrini and Dorofeev models. Additionally, note the
 18 improvement in the predictions for $x_{DDT}/D_h \text{ Exp} <$
 19 50 when using the LM. This provides evidence of the
 20 value of simple data manipulations (e.g., non-linear
 21 regressions) to enhance the predictive capabilities of
 22 existing models and/or inform the development of
 23 new simpler expressions/correlations with compar-
 24 able or better performance. The most important aspect
 25 is the use of large properly curated data sets covering
 26 a wide range of experimental conditions, fuels, and
 27 geometries to guide the choice of variables that ex-
 28 plain the variance of the experimental measurements.

29 6. Conclusions

30 A large database is compiled using a comprehen-
 31 sive set of x_{DDT} data for unobstructed channels avail-
 32 able in the literature. It comprises an extensive range
 33 of experimental conditions and mixtures. The global
 34 x_{DDT} trends as a function of D_h , ϕ , and p were evalu-
 35 ated. The data shows that x_{DDT} decreases as D_h de-
 36 creases, p increases, and $\phi \rightarrow 1$. An analysis of the

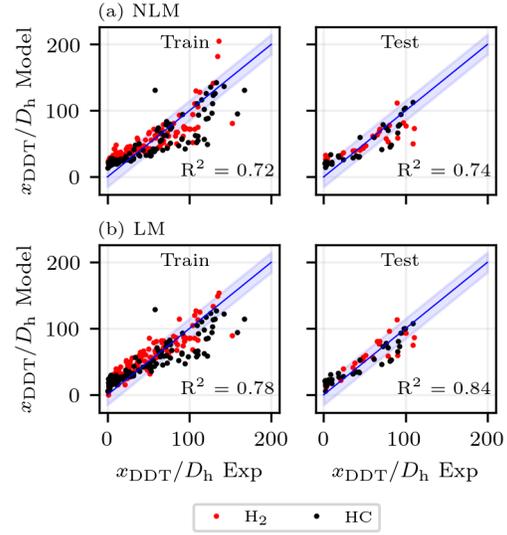


Fig. 7: a) Non-linear (NLM) and b) Logarithmic (LM) models performance for training and test data.

37 effect of the ratios of fundamental combustion prop-
 38 erties on x_{DDT}/D_h revealed that those that most affect
 39 it are D_h/δ_f , V_{CJ}/σ_{SL} and $\sigma - 1$. The most widely
 40 used models for x_{DDT} predictions, i.e., Silvestrini and
 41 Dorofeev, were tested against the database perform-
 42 ing rather poorly. An update to the models con-
 43 stants was carried out via a non-linear least squares
 44 regression using the large database compiled. This
 45 resulted in significant improvements in their perfor-
 46 mance. Finally, two simplified models were pro-
 47 posed. Their predictions are significantly better than
 48 those of the original Silvestrini/Dorofeev models and
 49 higher (LM)/similar (NLM) to those obtained with the
 50 updated models. Future work will include the use of
 51 the database to: (i) train a model that will be tested on
 52 obstructed channels using an expression that captures
 53 the experimental dependence of x_{DDT} as a function of
 54 the blockage ratio; (ii) develop x_{DDT}/D_h models valid
 55 for $D_h < 3$ mm and non-unity AR channels.

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