

Supplementary Material

Deriving Cool Flame Propagation Speeds by Means of an Ozone-Seeded, Stagnation Plate Burner Configuration

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Figure S1. Direct comparison between the conventional PIV image processing and the image processing developed in this study. Both flames conditions are $\phi = 0.4$, $x_{O_3} = 1.9\%$, with inlet velocities respectively equal to 0.75 m.s^{-1} and 1.10 m.s^{-1} .

Figure S2. Evolution of the standard deviation on the determination of the reference axial velocity $S_{u,\text{ref}}$ depending on the number of grid points used in the simulation of the axial velocity profile. Simulations are performed with the O_3 -submechanism from Jian et al [1].

Figure S3. Experimental (open diamonds) PIV measurement of the axial velocity profile for the cool flame at $\phi = 0.5$, $x_{O_3} = 1.5\%$, and simulated (continuous lines) profiles with different domain sizes l . Simulations are performed with the O_3 -submechanism from Jian et al [1].

Figure S4. Evolution of the standard deviation on the determination of the value of $S_{u,\text{ref}}$ (a) and its position (b) depending on the size of the simulated domain. Simulations are performed with the O_3 -submechanism from Jian et al [1].

Figure S5. Comparison between experimental axial velocity profiles measured by PIV (□) and simulated ones with different O_3 submechanisms, respectively from Jian et al. [1], Halter et al. [2] and Zhao et al. [3], for the cool flame at $\phi = 0.4$, $x_{O_3} = 1.7\%$, at different strain rates.

Figure S6. Comparison between experimental axial velocity profiles measured by PIV (□) and simulated ones with different O_3 submechanisms, respectively from Jian et al. [1], Halter et al. [2] and Zhao et al. [3], for the cool flame at $\phi = 0.4$, $x_{O_3} = 1.9\%$, at different strain rates.

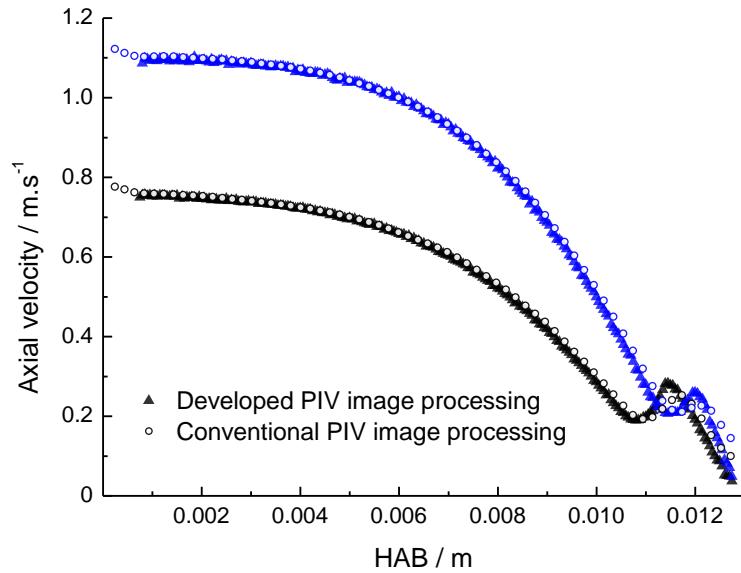
Figure S7. Comparison between experimental axial velocity profiles measured by PIV (□) and simulated ones with different O_3 submechanisms, respectively from Jian et al. [1], Halter et al. [2] and Zhao et al. [3], for the cool flame at $\phi = 0.45$, $x_{O_3} = 1.7\%$, at different strain rates.

Figure S8. Comparison between simulated axial velocity profiles with O_3 -submechanism from Jian et al. [1] and from Jian et al. with O_3+M reactions from Halter et al. [2], for the cool flame at $\phi = 0.5$, $x_{O_3} = 1.5\%$ and strain rate of 127 s^{-1} .

Table T1 : Cool flame conditions

Table T2. Reactions and rate constant parameters for the three O₃-submechanisms used in the current study

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The image processing with an IWS of 32×32 pixels results in 64 points axial velocity profiles, while the present methodology allows the determination of the axial velocity profiles with 241 points. It results in a more accurate determination of the reference velocity $S_{u,\text{ref}}$.

Figure S2. Evolution of the standard deviation on the determination of the reference axial velocity $S_{u,\text{ref}}$ depending on the number of grid points used in the simulation of the axial velocity profile. Simulations are performed with the O₃-submechanism from Jian et al [1].

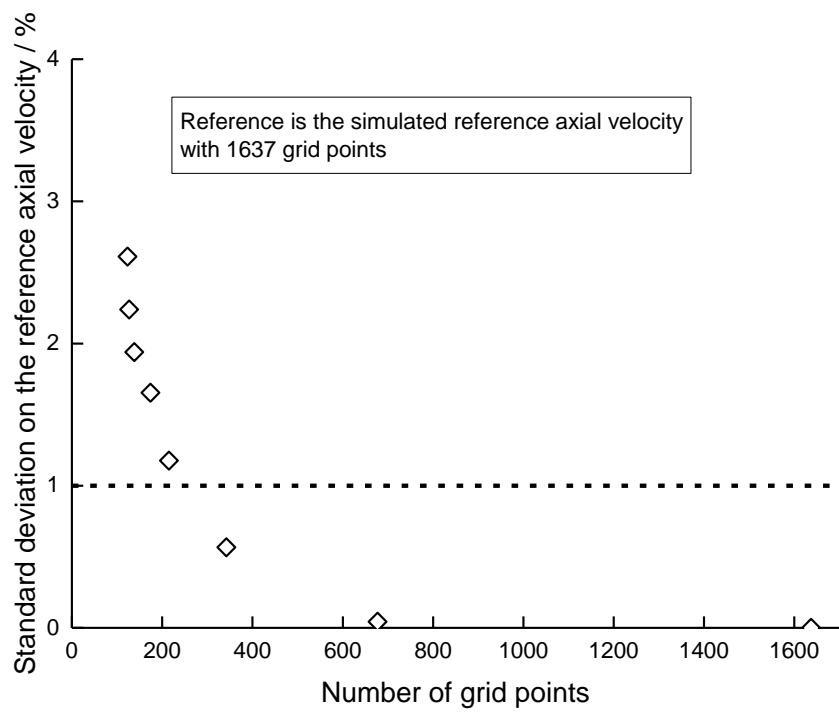


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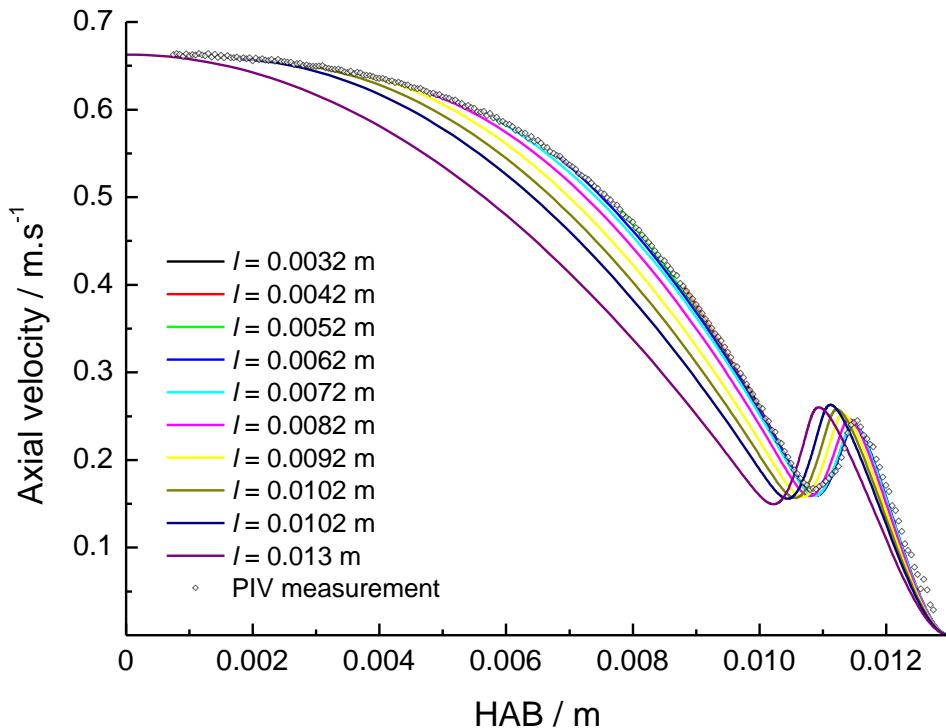


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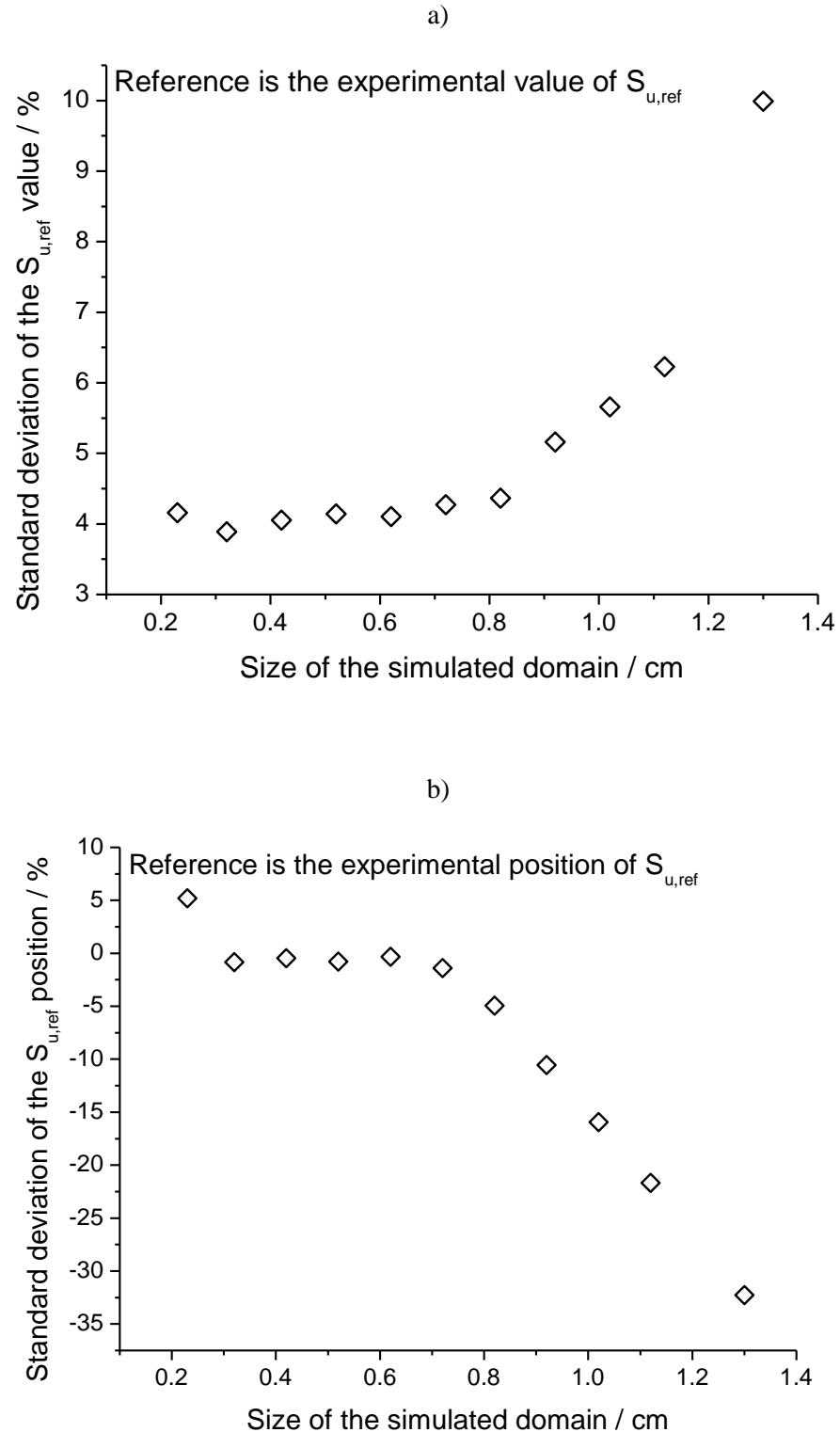


Figure S5. Comparison between experimental axial velocity profiles measured by PIV (\square) and simulated ones with different O_3 submechanisms, respectively from Jian et al. [1], Halter et al. [2] and Zhao et al. [3], for the cool flame at $\phi = 0.4$, $x_{O_3} = 1.7\%$, at different strain rates.

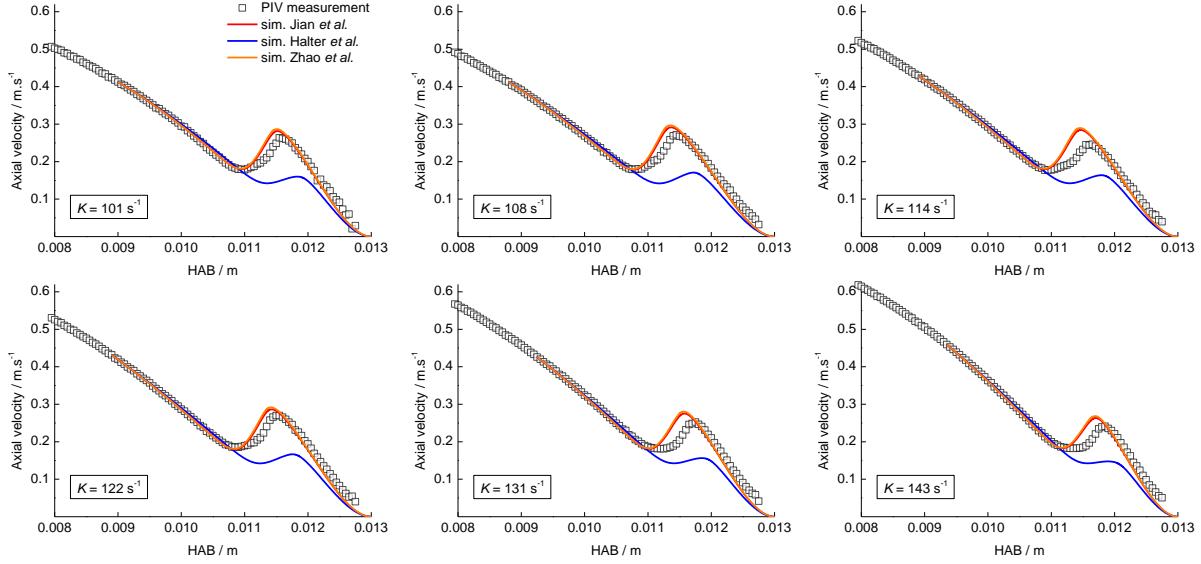


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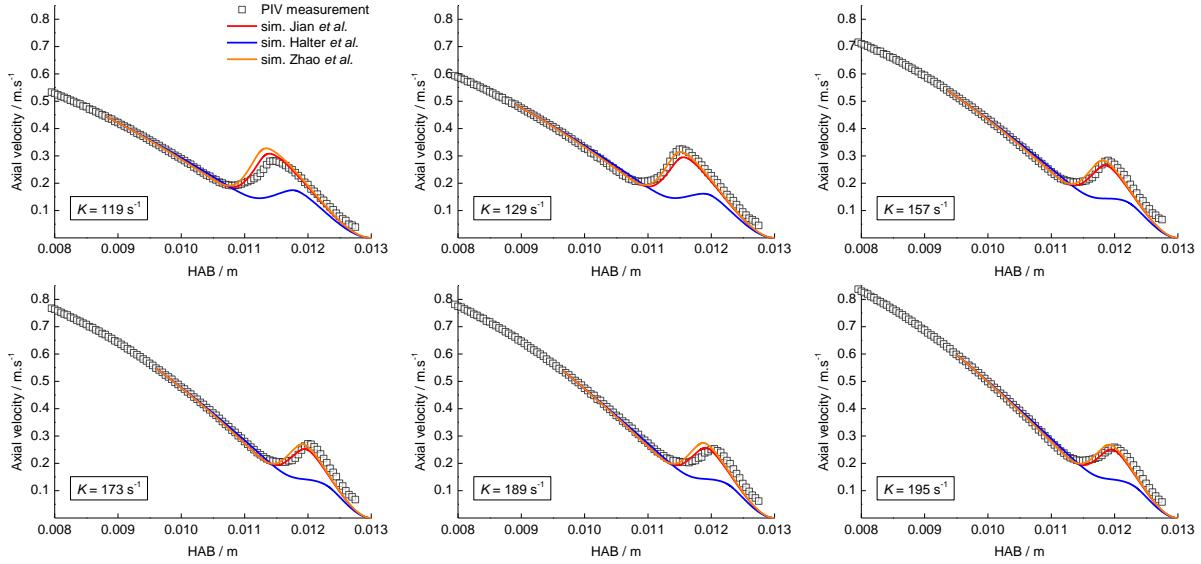


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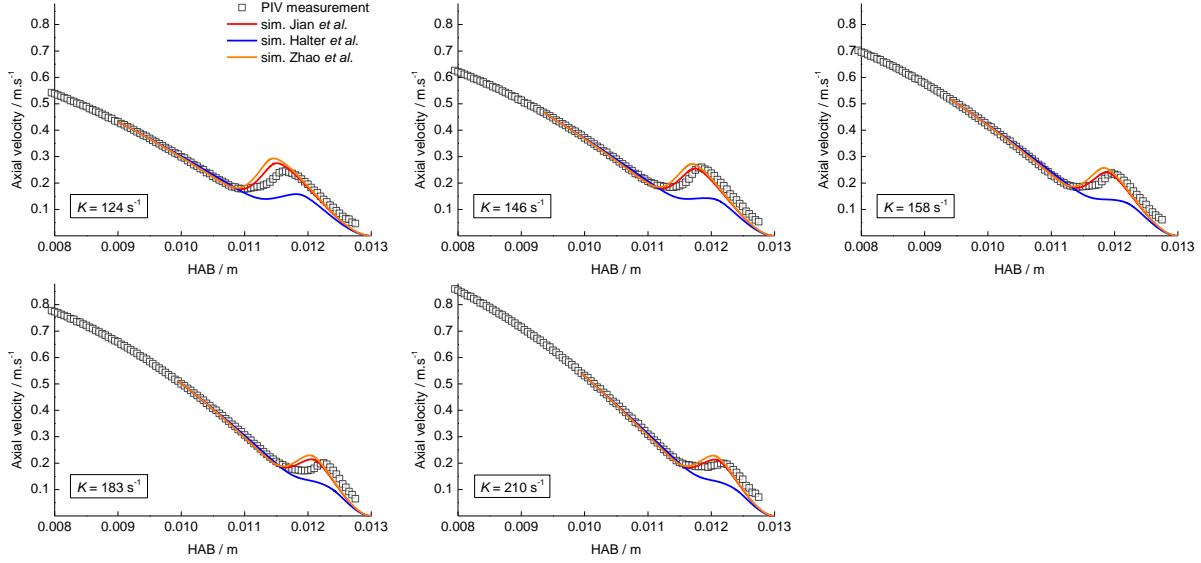


Figure S8. Comparison between simulated axial velocity profiles with O_3 -submechanism from Jian et al. [1] and from Jian et al. with O_3+M reactions from Halter et al. [2], for the cool flame at $\phi = 0.5$, $x_{O_3} = 1.5\%$ and strain rate of 127 s^{-1} .

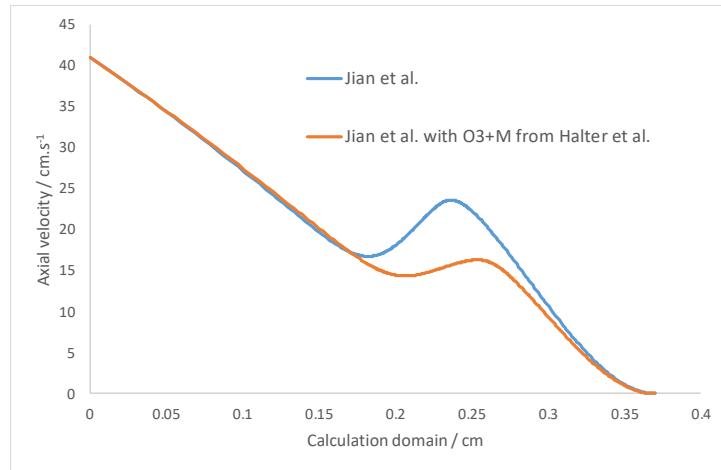


Table T1 : Cool flame conditions

Conditions	Size of the domain for the axial velocity profiles simulation (Pre-Mixed Burner Stagnation Flame module) / cm	Inlet velocity / cm.s ⁻¹	Imposed radial strain rate / s ⁻¹	Measured* flame speed / cm.s ⁻¹
$\phi = 0.5$ $x_{O3} = 1.5\%$ ($x_{DME} = 0.144$ $x_{O2} = 0.841$ $x_{O3} = 0.015$)	0.42	39.9	50.5	16.6
	0.41	40.3	55.6	16.8
	0.4	40.8	59.4	17.0
	0.39	42.5	61.6	17.0
	0.37	41.0	63.7	17.3
$\phi = 0.4$ $x_{O3} = 1.7\%$ ($x_{DME} = 0.119$ $x_{O2} = 0.864$ $x_{O3} = 0.017$)	0.40	41.3	50.6	17.8
	0.42	41.3	53.9	17.9
	0.41	43.0	56.8	17.7
	0.41	43.2	61.2	18.5
	0.375	42.6	65.3	18.1
	0.365	45.9	71.5	18.2
$\phi = 0.3$ $x_{O3} = 2.0\%$ ($x_{DME} = 0.092$ $x_{O2} = 0.881$ $x_{O3} = 0.02$)	0.44	41.3	51.5	18.6
	0.445	42.7	53.4	19.4
	0.42	43.1	57.1	18.6
	0.42	44.5	61.2	19.8
	0.42	46.4	61.7	19.9
	0.385	47.7	66.7	19.1
	0.375	49.0	72.8	19.8
	0.325	49.9	82.6	19.0
	0.345	54.7	85.0	19.7
$\phi = 0.4$ $x_{O3} = 1.9\%$ ($x_{DME} = 0.119$ $x_{O2} = 0.862$ $x_{O3} = 0.019$)	0.42	44.6	59.5	19.1
	0.41	48.9	64.6	20.5
	0.365	54.1	78.5	20.4
	0.34	54.8	86.4	20.4
	0.335	54.0	94.3	20.2
	0.35	59.9	97.6	20.9
$\phi = 0.45$ $x_{O3} = 1.7\%$ ($x_{DME} = 0.132$ $x_{O2} = 0.851$ $x_{O3} = 0.017$)	0.40	43.2	62.1	17.8
	0.365	46.8	72.8	18.4
	0.36	51.8	79.2	18.5
	0.305	51.1	91.4	18.3
	0.305	54.0	105.3	18.4

*Measured using the numerically assisted non-linear extrapolation method

Table T2. Reactions and rate constant parameters for the three O₃-submechanisms used in the current study

Units: A (cm³, mole, s), E_a (cal)

Reaction	A	n	E _a
Halter <i>et al.</i> [2]			
O ₃ + N ₂ → O ₂ + O + N ₂	4.00E+14	0	22667
O ₂ + O + N ₂ → O ₃ + N ₂	1.60E+14	-0.4	-1391
O ₃ + O ₂ → O ₂ + O ₂ + O	1.54E+14	0	23064
O ₂ + O ₂ + O → O ₃ + O ₂	3.26E+19	-2.1	0
O ₃ + O ₃ → O ₂ + O ₃ + O	4.40E+14	0	23064
O ₂ + O ₃ + O → O ₃ + O ₃	1.67E+15	-0.5	-1391
O ₃ + H <=> O ₂ + OH	8.43E+13	0	934
O ₃ + O <=> O ₂ + O ₂	4.82E+12	0	4094
O ₃ + OH <=> O ₂ + HO ₂	1.85E+11	0	831
O ₃ + HO ₂ <=> O ₂ + OH + O ₂	6.02E+09	0	938
O ₃ + H ₂ O <=> O ₂ + H ₂ O ₂	6.62E+01	0	0
O ₃ + CH ₃ <=> O ₂ + CH ₃ O	3.07E+12	0	417
O ₃ + H <=> O + HO ₂	4.52E+11	0	0
O ₃ + H ₂ <=> OH + HO ₂	6.00E+10	0	19840
O ₃ + CH ₄ <=> CH ₃ O + HO ₂	8.13E+10	0	15280
Jian <i>et al.</i> [1]			
O ₂ + O + M <=> O ₃ + M	1.00E+19	-2	0
N ₂ = 1.3 ; O ₂ = 1.2 ; Kr = 1 ; Ar = 1 ; O ₃ = 0			
O ₂ + O + O ₃ <=> O ₃ + O ₃	1.00E+23	-3	0
O ₃ + O <=> O ₂ + O ₂	1.10E+13	0	4300
O ₃ + H <=> OH + O ₂	8.43E+13	0	934
O ₃ + HO ₂ <=> O ₂ + O ₂ + OH	5.80E-04	4.57	-1377
O ₃ + OH <=> HO ₂ + O ₂	1.20E+05	2.5	800
Zhao <i>et al.</i> [3]			
O ₃ (+M) <=> O ₂ + O (+M)			
Low-Pressure	2.23E+28	-4.37	27297
High-Pressure	1.37E+15	-0.67	25990
Troe Parameters (0.6417 3.91E-04 8680.74 6060.75)			
Ar = 1 ; He = 1.2 ; N ₂ = 1.5 ; H ₂ = 3 ; O ₂ = 1.5 ; O ₃ = 3.75 ; O = 6			
O ₃ + O <=> O ₂ + O ₂	4.82E+12	0	4094
O ₃ + O <=> O ₂ (sing) + O ₂	1.44E+11	0	4094
O ₃ + O <=> O ₂ + OH	8.43E+13	0	934
O ₃ + H <=> O + HO ₂	4.52E+11	0	0
O ₃ + OH <=> O ₂ + HO ₂	1.85E+11	0	831
O ₃ + H ₂ O <=> O ₂ + H ₂ O ₂	6.62E+01	0	0
O ₃ + HO ₂ <=> OH + O ₂ + O ₂	6.62E+09	0	994
O ₃ + CO <=> O ₂ + CO ₂	6.02E+02	0	0
O ₃ + HCO <=> O ₂ + H + CO ₂	5.00E+11	0	0
O ₃ + CH ₃ <=> CH ₃ O + O ₂	5.83E+11	0	0

References

- [1] J. Jian, H. Hashemi, H. Wu, A.W. Jasper, P. Glarborg, A reaction mechanism for ozone dissociation and reaction with hydrogen at elevated temperature, *Fuel.* 322 (2022) 124138.
- [2] F. Halter, P. Higelin, P. Dagaut, Experimental and Detailed Kinetic Modeling Study of the Effect of Ozone on the Combustion of Methane, *Energy Fuels.* 25 (2011) 2909–2916.
- [3] H. Zhao, X. Yang, Y. Ju, Kinetic studies of ozone assisted low temperature oxidation of dimethyl ether in a flow reactor using molecular-beam mass spectrometry, *Combustion and Flame.* 173 (2016) 187–194.