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# Thermodynamic Calculations of Ti Ion Concentrations and Segregation Coefficients During Ti:sapphire Crystal Growth

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## Abstract

The theoretical phase diagrams of the binary  $\text{Al}_2\text{O}_3\text{-Ti}_2\text{O}_3$  and  $\text{Al}_2\text{O}_3\text{-TiO}_2$ , as systems calculated using the FactSage<sup>TM</sup> software and its thermodynamic databases, are re-optimized. This has been performed on the basis of a literature survey on experimental precipitation limits of  $\text{Ti}_2\text{O}_3$  and  $\text{TiO}_2$  in the  $\text{Al}_2\text{O}_3$  solid solution. The appropriate oxygen partial pressure ( $p_{\text{O}_2}$ ) range for controlling the valence state of Ti ions during Ti:sapphire crystal growth is obtained with respect to the calculated Ellingham type predominance diagram. Factors affecting the  $p_{\text{O}_2}$  such as furnace gas, crucible material and graphite heating elements are analyzed. The influence of  $p_{\text{O}_2}$  on  $\text{Ti}^{3+}$  and  $\text{Ti}^{4+}$  concentrations in the solid and liquid phases were derived from thermodynamic equilibrium calculations. The equilibrium segregation coefficients of  $\text{Ti}^{3+}$  and  $\text{Ti}^{4+}$  in sapphire are calculated to be 0.046 and 0.011, respectively. Taking into account values extrapolated from experiments, a value of  $0.06 \pm 0.02$  is proposed for

the equilibrium segregation coefficient of total Ti under low  $p_{O_2}$ .

**Key words:** Ti:sapphire, Solid solubility, Phase diagram, Oxygen partial pressure, Thermodynamic equilibrium calculations, Segregation coefficient

## 1 Introduction

Since the large tunable ability from 660 to 1070 nm of Ti:sapphire was discovered by Moulton,<sup>1</sup> these crystals have been receiving great attention from optical experimenters, especially their applications in laser systems such as ultra-short pulse laser generation<sup>2</sup> and high-power amplification.<sup>3</sup> This motivated the crystal growth community to increase the efforts to produce Ti:sapphire crystals with higher optical quality. The reported Ti doping level, for laser applications, ranges from 0.07 to 0.41 mol%.<sup>4</sup> The excellent performance of Ti:sapphire comes from the contribution of doping  $Ti^{3+}$  ions. However, whatever the crystal growth method, it is always difficult to eliminate  $Ti^{4+}$  ions, that are detrimental to the laser efficiency. Their presence leads to the well-known “residual absorption ” resulting from  $Ti^{3+} - Ti^{4+}$  pairs.<sup>5</sup> The figure of merit (FOM), which is related to the relative concentration ratio of  $Ti^{3+}/Ti^{4+}$ , is used to evaluate the optical quality of Ti:sapphire.<sup>6</sup> The contents of  $Ti^{4+}$  could be reduced through annealing but this process is time consuming. Therefore, controlling the valence of Ti ions during Ti:sapphire growth is of critical importance for improving the optical properties of the resulting single crystal.

Crystal growth atmosphere, essentially the partial pressure of oxygen,  $p_{O_2}$ , plays an important role in determining the valence of Ti ions.<sup>7,8</sup> The effect of  $p_{O_2}$  on Ti ion

valences can be predicted through the Ellingham type predominance diagram. This diagram can be calculated using Gibbs energy minimization software like FactSage,<sup>9</sup> Thermo-Calc<sup>10</sup> or Pandat<sup>11</sup> in combination with optimized thermodynamic databases. Crystal growth occurs under conditions where the Gibbs energy has a minimum value which means a physical or chemical equilibrium is established. Ti:sapphire growth proceeds at high temperature and usually lasts several hours to several weeks and even longer time so that thermodynamic equilibrium can be assumed for the gas phase, liquid phase and solid-liquid interface. Therefore, thermodynamic equilibrium calculations can be performed to obtain some physical or chemical parameters relevant during crystal growth and then gain a deeper understanding of the experimentally observed phenomena.

The influence of oxygen partial pressure  $p_{O_2}$  and related effects need to be considered in order to understand the Ti ion valences. Most importantly, the variation of  $p_{O_2}$  during the crystal growth influences the Ti ion concentrations in both the solid and the liquid phase and thereby the segregation coefficients. Measured effective segregation coefficients of total Ti ( $k_{Ti}$ ) in Ti:sapphire were reported from 0.05 to 0.23 (see Table 1). To the best of our knowledge, no one has independently measured the segregation coefficients of  $Ti^{3+}$  ( $k_{Ti^{3+}}$ ) and  $Ti^{4+}$  ( $k_{Ti^{4+}}$ ), that are key growth parameters for the understanding and control of ion valence distributions in the grown crystal.

The purpose of this contribution is to revisit the Ti:sapphire single crystal growth process using a thermodynamic approach. All presented calculations are performed with FactSage<sup>TM</sup> software using its thermodynamic databases “FToxid” for

all condensed phases and “FactPS” for the gas species. The thermodynamic data was modified to model the phase diagrams with respect to collected experimental precipitation limits of TiO<sub>2</sub> and Ti<sub>2</sub>O<sub>3</sub>. The factors influencing  $p_{O_2}$  in crystal growth atmosphere are analyzed including filling gas and furnace materials. The influence of oxygen partial pressure on the concentrations of Ti<sup>3+</sup> and Ti<sup>4+</sup> in the solid and liquid phases is studied. The segregation coefficients of Ti<sup>3+</sup>, Ti<sup>4+</sup> and total Ti are calculated from these results and compared to the experimental values.

**Table 1.** Measured Ti effective segregation coefficient in Ti:sapphire grown by different techniques.

$k_{Ti}^{eff}$	Crystal growth method	Pulling rate m.s <sup>-1</sup>	Crucible	Atmosphere	FOM
0.23	Heat exchanger <sup>12</sup>	Unknown	Mo	He	124.6 and 131.2
< 1	Heat exchanger <sup>13</sup>	Unknown	Mo	Vacuum	Unknown
0.2	Kyropoulos <sup>14</sup>	Unknown	Mo	Unknown	Unknown
0.21	Kyropoulos <sup>15</sup>	Unknown	Mo	Vacuum	200
0.2	Kyropoulos <sup>16</sup>	Unknown	Mo	Unknown	Unknown
0.17 - 0.2	Czochralski <sup>17</sup>	$2.78 \times 10^{-7}$	Ir	Ar/CO	>100
0.12	Czochralski <sup>8</sup>	$1.06 \times 10^{-7}$	Ir	N <sub>2</sub> or N <sub>2</sub> +0.1 vol% H <sub>2</sub>	Unknown
0.11	Czochralski <sup>18</sup>	$8.47 \times 10^{-8}$ - $7.06 \times 10^{-7}$	Unknown	N <sub>2</sub>	Unknown

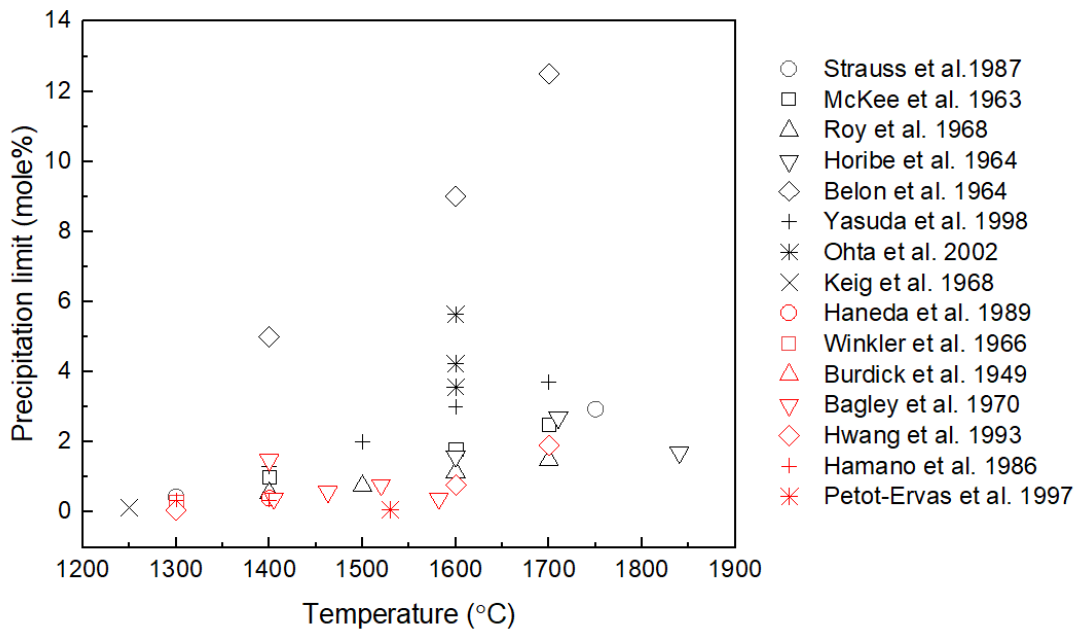
0.05	Czochralski <sup>19</sup>	$2.78 \times 10^{-7}$	Ir	N <sub>2</sub>	Unknown
0.1	Czochralski <sup>20</sup>	$2.78 \times 10^{-7}$	Ir	Unknown	Unknown
0.2	$\mu$ -pulling down <sup>21</sup>	Unknown	Ir	Ar	Unknown
0.1	Floating zone <sup>22</sup>	Unknown	Mo	N <sub>2</sub> or Ar + 5~20 vol % H <sub>2</sub>	Unknown
0.21	Gradient freeze technique <sup>23</sup>	Unknown	Mo	Ar or He	Unknown
0.15	Horizontal directional solidification <sup>24</sup>	$1.39 \times 10^{-7}$ - $5.56 \times 10^{-7}$	Mo	Ar+5 vol% reductants	>150
0.12 - 0.15	Horizontal directional solidification <sup>25</sup>	$1.39 \times 10^{-7}$ - $5.56 \times 10^{-7}$	Mo	Ar	Unknown
< 0.2	Unknown <sup>26</sup>	Unknown	Unknown	Unknown	100, $\geq 150$
0.14	Unknown <sup>27</sup>	Unknown	Unknown	Unknown	Unknown
0.1	Unknown <sup>28</sup>	$6.94 \times 10^{-8}$	Ir	N <sub>2</sub> or Ar	Unknown

## 2 Literature information on solid solubility and phase diagrams

### 2.1 Ti ion solubilities in sapphire

Ti:sapphire is usually grown by doping Ti<sub>2</sub>O<sub>3</sub> or TiO<sub>2</sub> into alumina raw material. Depending on the crystal growth atmosphere, Ti<sup>3+</sup> and Ti<sup>4+</sup> substitution ions are obtained in the sapphire crystal in both cases. However, this process could be accompanied by the formation of precipitates when the solid concentration exceeds the solubility limits of Ti<sup>3+</sup> and Ti<sup>4+</sup>. For example, when  $p_{O_2}$  is high, precipitates such as

rutile ( $\text{TiO}_2$ ) may form inside the crystal. When  $p_{\text{O}_2}$  is low, most  $\text{Ti}^{4+}$  ions are reduced to  $\text{Ti}^{3+}$  and  $\text{Ti}_2\text{O}_3$  precipitates could form. Therefore, the solubilities of  $\text{Ti}^{3+}$  or  $\text{Ti}^{4+}$  are critically important. A thorough assessment of the underlying phase diagram is necessary and will be used to compute Ti ion concentrations and segregation coefficients.



**Figure 1.** Solid precipitation limit of  $\text{Ti}_2\text{O}_3$  and  $\text{TiO}_2$  in  $\alpha\text{-Al}_2\text{O}_3$ . Black symbols represent the precipitation limit of  $\text{Ti}_2\text{O}_3$  and red symbols represent the precipitation limit of  $\text{TiO}_2$ .<sup>23,29-42</sup>

The reported solid solubilities of  $\text{Ti}^{3+}$  and  $\text{Ti}^{4+}$  in alumina are summarized in Figure 1. Both solubilities of  $\text{Ti}^{3+}$  and  $\text{Ti}^{4+}$  increase with elevating temperature. It is observed that  $\text{Ti}^{3+}$  is more soluble in  $\alpha\text{-Al}_2\text{O}_3$  than  $\text{Ti}^{4+}$ . This is reasonable because no extra charge compensator is required for the incorporation of  $\text{Ti}^{3+}$  while one aluminum vacancy is created together with the incorporation of every three  $\text{Ti}^{4+}$  to maintain

electroneutrality.

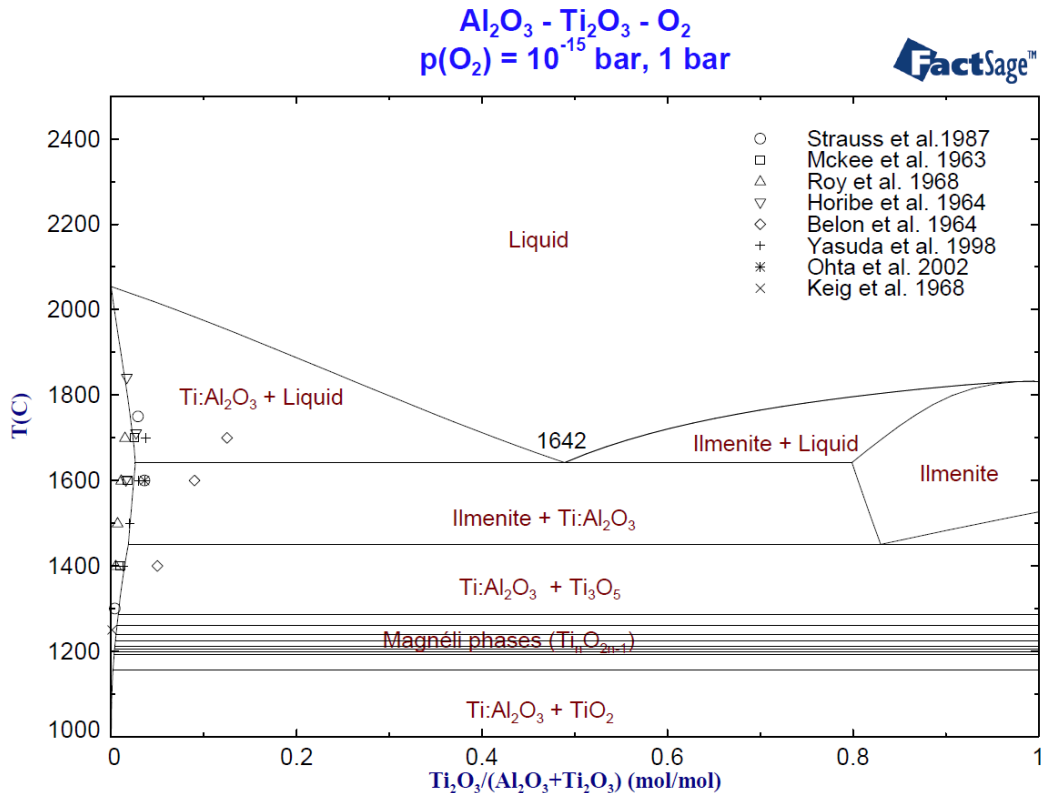
There may exist some uncertainties for part of the solubility data. For example, under reducing atmosphere,  $\text{Ti}^{3+}$  should be expected while Roy et al. ascribed their obtained solubility data to  $\text{Ti}^{4+}$ .<sup>40</sup> The solubility of  $\text{Ti}^{4+}$  given by Winkler et al. is measured in polycrystalline  $\text{Al}_2\text{O}_3$ , not in a single crystal.<sup>34</sup> Even though, their results are still considered as a reference by most researchers. Ohta et al. measured the solubility of  $\text{Ti}^{3+}$  in  $\text{Al}_2\text{O}_3$  at 1600 °C in the ternary  $\text{Al}_2\text{O}_3$ - $\text{SiO}_2$ - $\text{TiO}_x$  system but not in the pure  $\text{Al}_2\text{O}_3$ - $\text{Ti}_2\text{O}_3$  system.<sup>31</sup> For papers where  $p_{\text{O}_2}$  is not known, it is assumed that  $\text{Ti}^{3+}$  solid solubilities were obtained under reducing atmosphere (low  $p_{\text{O}_2}$ ) and  $\text{Ti}^{4+}$  solid solubilities were obtained under oxidizing atmosphere (high  $p_{\text{O}_2}$ ). These experimental solubility data will be further discussed under the following phase diagrams.

## 2.2 $\text{Al}_2\text{O}_3$ - $\text{Ti}_2\text{O}_3$ and $\text{Al}_2\text{O}_3$ - $\text{TiO}_2$ quasi-binary systems

Under reducing atmosphere, the major fraction of titanium in the system is present as  $\text{Ti}^{3+}$ . The calculated phase diagram of  $\text{Al}_2\text{O}_3$ - $\text{Ti}_2\text{O}_3$  system at  $p_{\text{O}_2} = 10^{-15}$  bar accompanied by the experimental solubility data of  $\text{Ti}^{3+}$  from the literature is shown in Figure 2, as calculated using FastSage 8.0 software. It is assumed that no metal phase (Al, Ti, TiAl, TiAl<sub>3</sub> ...) is formed in the solid phase. The solidus and solvus lines of  $\text{Al}_2\text{O}_3$  show a good agreement with the  $\text{Ti}^{3+}$  solid solubility data in Figure 2 except the results of Belon et al which reported a precipitation limit of  $\text{Ti}_2\text{O}_3$  in  $\text{Al}_2\text{O}_3$  as high as 12.5 mole% at 1700 °C.<sup>42</sup> All other reported precipitation limits of  $\text{Ti}_2\text{O}_3$  in  $\text{Al}_2\text{O}_3$  are



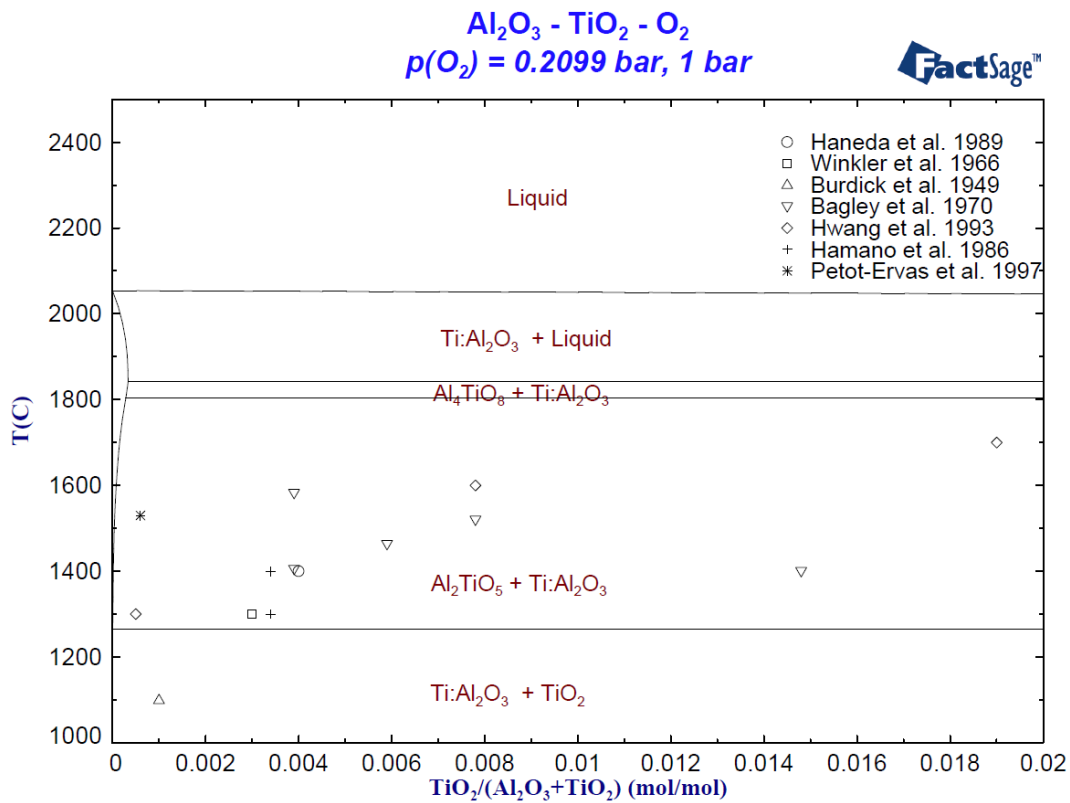
lower than 4 mole%. Except  $\text{Ti}_2\text{O}_3$  (ilmenite-type phase), several other titanium oxides, Magnéli phases ( $\text{Ti}_n\text{O}_{2n-1}$ ,  $4 \leq n \leq 20$ ), are also present in the quasi-binary  $\text{Al}_2\text{O}_3$ - $\text{Ti}_2\text{O}_3$  system. These Magnéli phases are considered as stoichiometric compounds in the temperature range 1200 – 1300 °C.<sup>43</sup>



**Figure 2.** Phase diagram of quasi-binary  $\text{Al}_2\text{O}_3$ - $\text{Ti}_2\text{O}_3$  system at fixed oxygen partial pressure of  $p_{\text{O}_2} = 10^{-15} \text{ bar}$  and  $p_{\text{total}} = 1 \text{ bar}$ .<sup>23,29–32,40–42</sup>

The calculated phase diagram of the quasi-binary  $\text{Al}_2\text{O}_3$ - $\text{TiO}_2$  system in air, zoomed on the low Ti concentration range, is shown in Figure 3. The solubility data of  $\text{Ti}^{4+}$  from the literature are plotted together with the calculated phase boundaries. According to FactSage result, titanium ions are totally incorporated into Ti:sapphire for low concentrations only (in the left small area of Figure 3). However, the experimental

solubility data does not agree with the calculated phase diagram. This is due to the fact that, in the commercial FactSage software and its databases, the solubility data of  $Ti^{4+}$  in the  $Al_2O_3$  solid phase is neglected and not modelled. The calculated solubility of Ti in  $Al_2O_3$  in Fig.3 is due to  $Ti^{3+}$  ions only. It is therefore impossible to calculate the equilibrium concentrations of  $Ti^{3+}$  and  $Ti^{4+}$  in the solid phase and to determine the corresponding segregation coefficients. Therefore, the solid database must be optimized to reproduce the experimental solubility data for  $Ti^{3+}$  and  $Ti^{4+}$  ions.



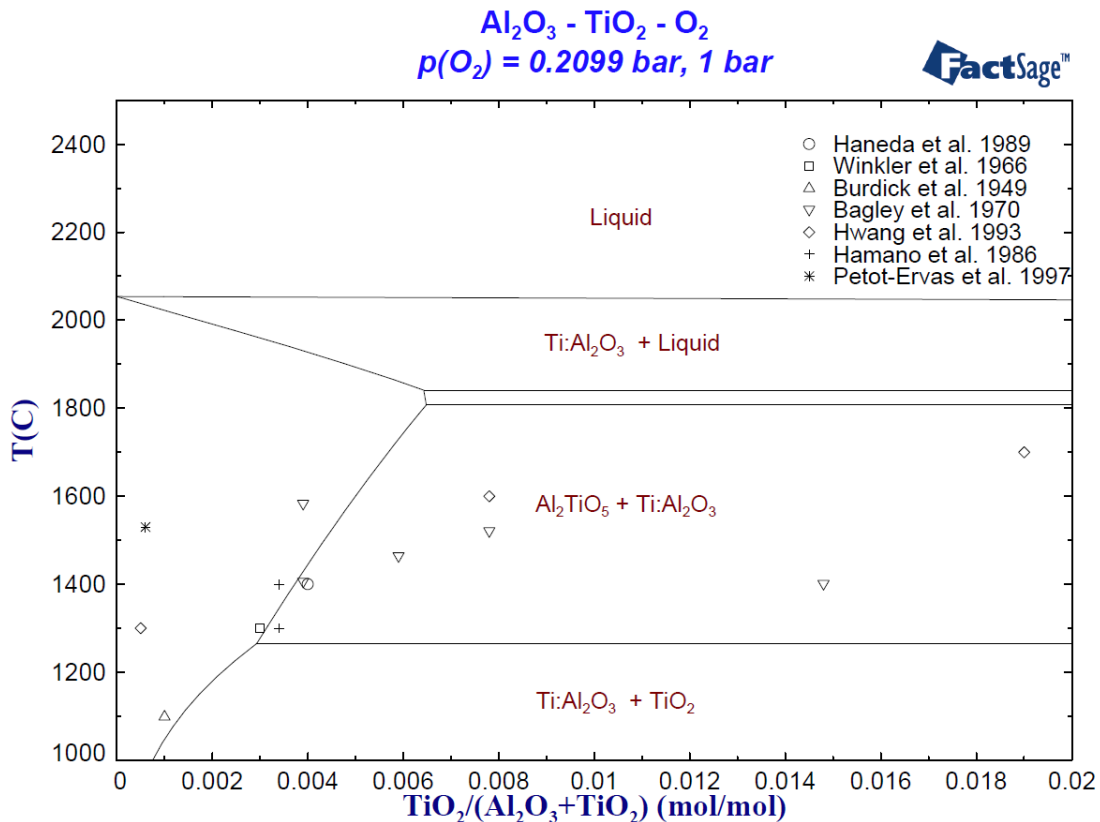
**Figure 3.** Zoomed phase diagram of the  $Al_2O_3$ - $TiO_2$  system in air and  $p_{total} = 1$  bar.<sup>33-39</sup>

To improve the database for the thermodynamic equilibrium calculations,  $Ti^{4+}$  ions can be introduced into the solid phase by adding  $TiO_2$  as diluted component into

the solid solution through the Henrian relation given as:

$$\log_{10} \gamma_i = \frac{A}{T} + B \quad (1)$$

where  $\gamma_i$  is the dimensionless activity coefficient of  $\text{Ti}^{4+}$ ,  $A$  and  $B$  are constants,  $T$  is the temperature in Kelvin. The solidus and solvus lines in quasi-binary  $\text{Al}_2\text{O}_3$ - $\text{TiO}_2$  phase diagram change with  $A$ ,  $B$  parameters and with the oxygen partial pressure  $p_{\text{O}_2}$ . The thermodynamic data of pure  $\text{TiO}_2$  (rutile) from the FTPS pure substance database<sup>9</sup> was selected as diluted component in the modelling of the  $\text{Ti}:\text{Al}_2\text{O}_3$  solid solution to calculate realistic  $\text{Al}_2\text{O}_3$ - $\text{TiO}_2$  equilibria at high temperature. By dichotomy, it was found that  $A=4360$  and  $B=0$  result in an acceptable fit of the phase diagram with the experimental solubility data.



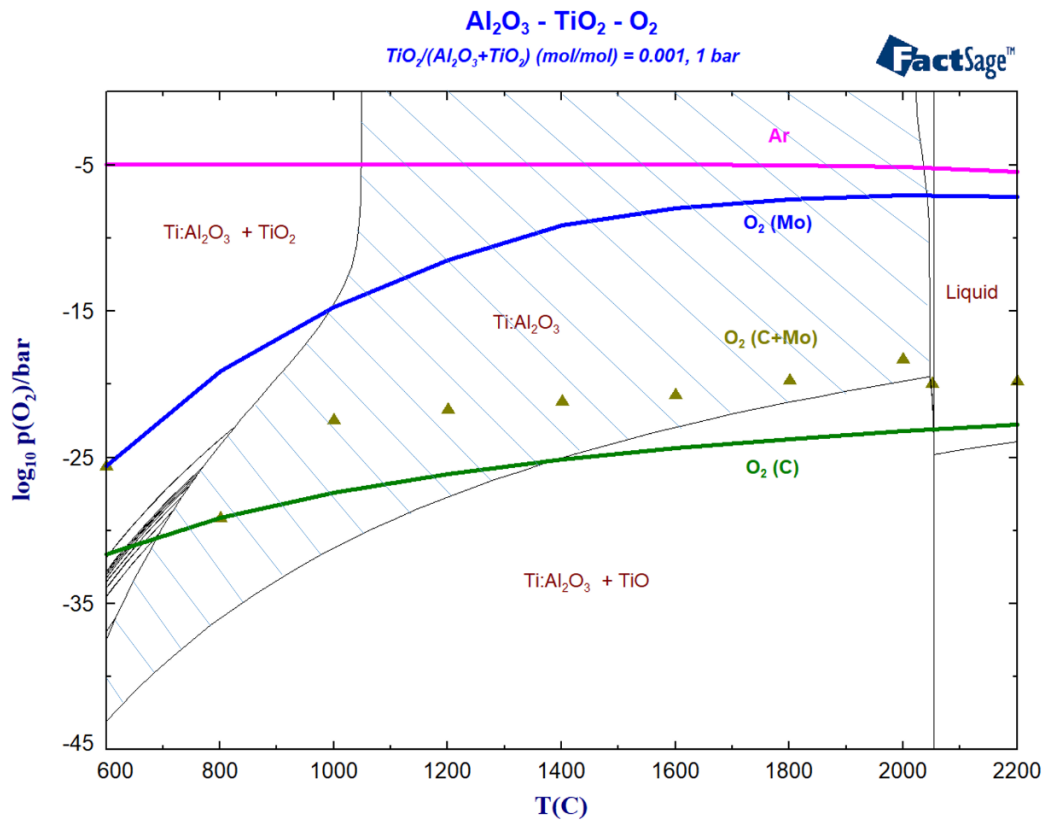
**Figure 4.** Optimized phase diagram of  $\text{Al}_2\text{O}_3$ - $\text{TiO}_2$  system in air after imported  $\text{Ti}^{4+}$  into the solid phase and  $p_{\text{total}} = 1 \text{ bar}$ .

The new phase diagram of  $\text{Al}_2\text{O}_3\text{-TiO}_2$  with the diluted solution is presented in Figure 4 along with the experimental solubility data of  $\text{Ti}^{4+}$  ions. Compared to Figure 3, the solubility data of  $\text{Ti}^{4+}$  distributes well on the solvus line. The phase diagram of  $\text{Al}_2\text{O}_3\text{-Ti}_2\text{O}_3$  system has nearly no change compared to the initial diagram. This new modified thermodynamic database is used for all further calculations presented in this contribution.

The valence of Ti in the crystal is a function of temperature and oxygen partial pressure. An important point to mention is that there exist large temperature differences in a crystal growth setup. For example, in Kyropoulos and Czochralski crystal growth setups, the temperature of the crucible wall is higher than that in the center of the melt and the temperature on the earlier grown part (top of the crystal) is lower than the temperature of the bottom part which is close to the solid-liquid interface. The temperature varies also drastically during crystal cooling process. Therefore, for the aim of getting the desired valence of  $\text{Ti}^{3+}$ , oxygen partial pressures must be carefully controlled to fit the phase diagram at any temperature. At high temperature, it is possible that  $\text{O}_2$  gas is decomposed into O atoms, but from the experimental aspect,  $p_{\text{O}_2}$  has much more physical meaning than  $p_{\text{O}}$  and it is easier to compare the results with experiments. Therefore, in the thermodynamic calculations,  $p_{\text{O}_2}$  is used to describe the oxygen partial pressure.

Based on the optimized database, an Ellingham type predominance diagram of the  $\text{Al}_2\text{O}_3\text{-TiO}_2$  system (see Figure 5) can be calculated and shows the relation of the oxygen partial pressure  $p_{\text{O}_2}$  with temperature as well as its influence on the Ti ion

valence. The  $\text{Al}_2\text{O}_3$  solid solution, “Ti:Al $_2\text{O}_3$ ” and the ionic “Liquid” coexist at high temperature. The solid phase containing  $\text{Ti}^{3+}$  and  $\text{Ti}^{4+}$  ions, without the precipitation of other phase, exists only within the shaded area (Ti:Al $_2\text{O}_3$ ). So, in order to grow this solid solution, the oxygen partial pressure  $p_{\text{O}_2}$  should be higher than  $10^{-20}$  bar. At high temperature ( $T > 1000$  °C), for  $p_{\text{O}_2}$  lower than  $10^{-20}$  bar, TiO may appear. At low temperature ( $T < 1000$  °C), rutile (TiO $_2$ ) precipitates may form in the crystal. It has been observed in the sintering experiments of Hamano et al., that excess TiO $_2$  precipitates as rutile at temperatures below 1350 °C.<sup>38</sup>

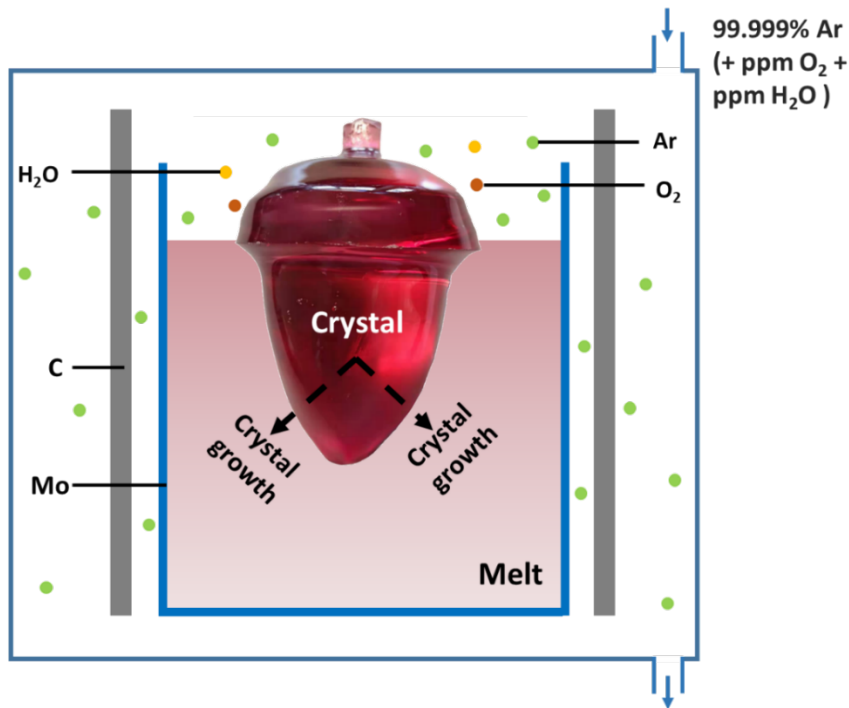


**Figure 5.** Ellingham type predominance diagram of the  $\text{Al}_2\text{O}_3$ -TiO $_2$  system. “Ar” shows the  $p_{\text{O}_2}$  for Ar + 10 ppm O $_2$  + 10 ppm H $_2\text{O}$ ; “O $_2$  (Mo)” shows the  $p_{\text{O}_2}$  for Ar + 10 ppm O $_2$  + 10 ppm H $_2\text{O}$  in equilibrium with Mo; “O $_2$  (C)” shows the  $p_{\text{O}_2}$  for Ar +

10 ppm  $O_2$  + 10 ppm  $H_2O$  in equilibrium with graphite elements; " $O_2(C+Mo)$ " (gray triangles) shows the  $p_{O_2}$  for the two steps calculation with C and Mo (see text).

### 3 $p_{O_2}$ during Ti:sapphire growth

The oxygen partial pressure inside the furnace at any time is conditioned by the crystal growth conditions (temperature, atmosphere, crucible, furnace structure and materials). For example, Figure 6 shows a simplified sketch of a setup used for growing Ti:sapphire using the Kyropoulos method. The crystal is grown under flowing Ar gas.



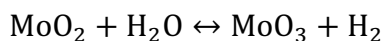
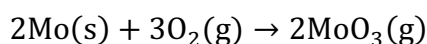
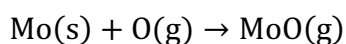
**Figure 6.** Kyropoulos crystal growth sketch for Ti:sapphire. The inserted crystal picture has been obtained by extracting a crystal from the melt during growth.<sup>44</sup>

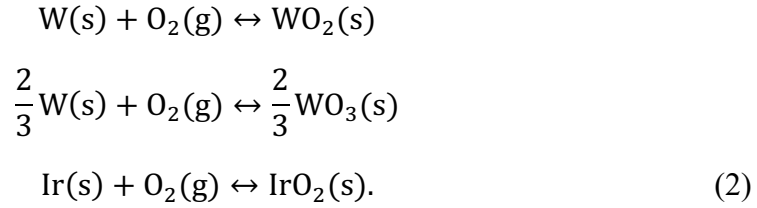
But, even the purest commercial Ar gas always contains small amounts of dioxygen ( $O_2$ ) and water vapor. In addition, the furnace cannot be perfectly sealed. Small amounts of dioxygen and water vapor leaking in from the ambient air still have a chance to enter

in the furnace. Thus, it is assumed that 10 ppm O<sub>2</sub> and 10 ppm H<sub>2</sub>O (g) trace impurities are present inside the flowing furnace gas.<sup>17</sup> The raw material, composed of pure alumina crackles and Ti doped Al<sub>2</sub>O<sub>3</sub> powder, is melted in a metallic Mo crucible and the crystal is grown along radial and downward directions. Graphite elements are used as casing, susceptor and insulation for uniformly heating the crucible. The gas (initially Ar + 10 ppm O<sub>2</sub> + 10 ppm H<sub>2</sub>O (g)) exists everywhere inside the furnace.

Except for specific study purposes, Ti:sapphire is always grown under pure inert gas or reducing gas to obtain a sufficient concentration of Ti<sup>3+</sup> ions for an application in laser materials. Reported Ti:sapphire crystals were grown under pure Ar, N<sub>2</sub>, and H<sub>2</sub> atmospheres.<sup>45,46</sup> In contrast to pure inert gases, mixtures of inert gas with small amounts of reducing gas in the growth or annealing processes contribute to further improve crystal quality. It is already reported that Ti:sapphire grown under the mixtures of 99.34 % Ar + 0.6% CO + 0.06 % H<sub>2</sub> can lower the [Ti<sup>4+</sup>]/[Ti<sup>3+</sup>] ratio.<sup>47</sup> The results of Uecker et al. suggest that the mixtures of 95% Ar + 5% CO is efficient in maintaining titanium ions at the +3 valency.<sup>17</sup>

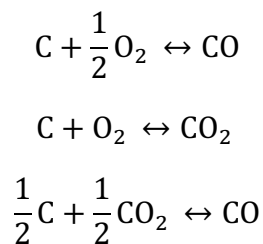
Mo, W and Ir metals are three typical crucible materials used in Ti:sapphire crystal growth. Trace impurities of O<sub>2</sub> and H<sub>2</sub>O (g) in the growth atmosphere can oxidize the crucible metal through below reactions:<sup>48,49</sup>



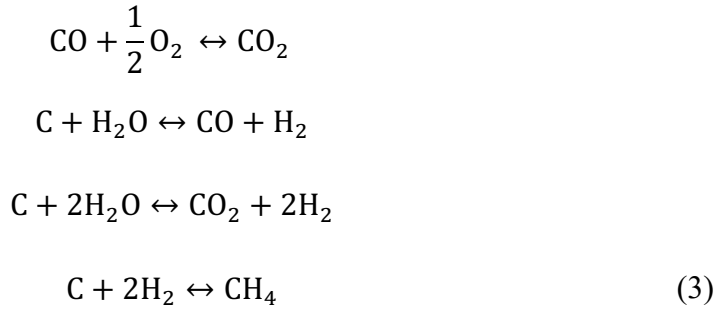


These produced oxides are volatile so that the crucible is decomposed and destroyed when the oxygen partial pressure  $p_{\text{O}_2}$  is too high. In the liquid phase, it is calculated that the potential reaction among alumina melt, crucible materials and furnace gas leads to the lowest oxygen partial pressure of  $8.87 \times 10^{-8}$  bar at sapphire melting point for Mo crucible while W crucible gives a  $p_{\text{O}_2} = 4.27 \times 10^{-7}$  bar and Ir crucible gives a  $p_{\text{O}_2} = 6.22 \times 10^{-6}$  bar, respectively. Besides, Ir is expensive and W is rather difficult to machine, especially for the small die pieces used for the EFG (Edge-defined Film-fed Growth) process. Therefore, Mo crucible is favored by industrial crystal growers as well as the RSA le Rubis SA company providing us samples. Sometimes, a Mo crucible is used without graphite insulation. In this case,  $\text{Al}_2\text{O}_3$  or  $\text{ZrO}_2$  casings are used. Without Mo crucible (only  $\text{Al}_2\text{O}_3$  + gas), an oxygen partial pressures  $p_{\text{O}_2}$  of  $6.22 \times 10^{-6}$  bar is obtained. This means that even with a casing made of oxides, the Mo crucible still controls the  $p_{\text{O}_2}$  in the liquid phase. It may also be possible that oxygen in the melt or gas diffuses through the Mo crucible but this is not considered in the present study.

However, most of the time, graphite casing is used. The graphite elements inside the furnace also can react with  $\text{O}_2$  (g) and  $\text{H}_2\text{O}$  (g):







As the Factsage Gibbs energy minimization software calculates the global equilibrium, all these reactions are considered automatically while establishing the final thermodynamic equilibrium under a given set of constraints (temperature, pressure, composition).

In a practical crystal growth run, the gas inside furnace reacts with Mo and graphite in a complex way and at different temperatures. As shown in the crystal growth setup (Figure 6), the crucible is located at the center of the furnace and is surrounded by the graphite elements. So, it is expected that the filling gas reacts first with the outer graphite elements and then reacts later with the central crucible. Consequently, the  $p_{\text{O}_2}$  around crystal and melt at a given temperature is computed in two steps: 1<sup>st</sup>, the gas inside furnace reacts with graphite elements; 2<sup>nd</sup> the resulting gases react with Mo crucible.

To observe the influence of the growth atmosphere on the Ti valence during Ti:sapphire growth, various computed oxygen partial pressures  $p_{\text{O}_2}$  are plotted in the  $\text{Al}_2\text{O}_3$ - $\text{TiO}_2$  predominance diagram (Figure 5). The plots show that pure Ar gas (pink line) always results in an oxygen partial pressure  $p_{\text{O}_2}$  of around  $10^{-5}$  bar with no significant change with temperature: there is a risk of  $\text{TiO}_2$  precipitation below  $1100^\circ\text{C}$ . The successive reactions of C, then Mo (gray triangles, several temperatures are

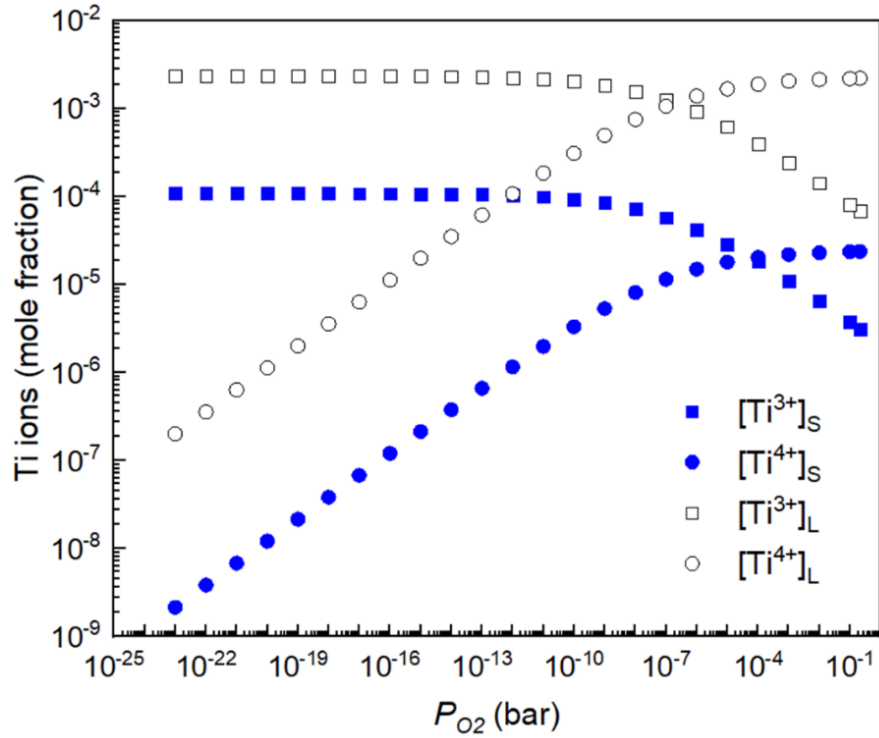
computed) decrease the oxygen partial pressure  $p_{O_2}$  by 13 orders of magnitude compared to Mo action alone (blue line). However, when furnace gases react only with C (green line), it results in the formation of TiO precipitates for temperatures larger than 1400 °C instead of forming the pure  $Al_2O_3$  solid solution where only  $Ti^{3+}$  and  $Ti^{4+}$  exist. It is then concluded that the presence of the Mo crucible, close to liquid and crystal, is likely to suppress the formation of TiO precipitates.

The successive effects of C and Mo results in an oxygen partial pressure  $p_{O_2} = 1.1 \times 10^{-20}$  bar that allows growing the desired  $Ti^{3+}$  and  $Ti^{4+}$  solid solution. During the cooling process, the  $p_{O_2}$  partial pressure must be further decreased, otherwise solid rutile ( $TiO_2$ ) precipitates may appear. Therefore,  $p_{O_2}$  must be carefully controlled during the crystal growth and the cooling process. If it is considered that precipitation is a slow process below 1000 °C, growth in presence of C+Mo or even Mo alone are acceptable situations for obtaining crystals without solid precipitates.

## **4 Ti ion concentrations and segregation coefficients**

### **4.1 Ti ion concentrations**

The  $p_{O_2}$  partial pressure in the gas phase affects the Ti valence during the crystal growth and as a consequence the concentrations of  $Ti^{3+}$  and  $Ti^{4+}$  ions present in the crystals. For a sapphire crystal doped with 0.1 mole%  $TiO_2$ , the concentrations of  $Ti^{3+}$  and  $Ti^{4+}$  in the solid and liquid phases at the solid-liquid equilibrium (2053 °C), are computed as function of  $p_{O_2}$  partial pressure (Figure 7), based on the previously optimized database.



**Figure 7.** Ti ion concentrations in the  $Al_2O_3$  solid solution in equilibrium with the liquid and their dependence on  $p_{O_2}$  at 2053 °C. The data are calculated from 1 mole  $Al_2O_3 + 10^{-3}$  mole  $TiO_2 + 1$  mole  $Ar +$  appropriate amount of  $O_2$  under fixed  $p_{O_2}$ .

In the liquid phase, when the fixed  $p_{O_2}$  partial pressure is smaller than  $10^{-7}$  bar,  $Ti^{3+}$  concentration is larger than the concentration of  $Ti^{4+}$  while above this pressure,  $Ti^{4+}$  concentration becomes the larger one. In the solid phase, the concentration of  $Ti^{4+}$  becomes larger than  $Ti^{3+}$  when  $p_{O_2} > 1 \times 10^{-4}$  bar. Mohapatra et al. also observed this reverse concentration phenomenon by annealing Ti:sapphire crystals at 1600 °C under different atmospheres.<sup>50</sup> Therefore, when a crystal is grown or annealed under a given temperature, desired Ti ion concentrations can be adjusted through carefully controlling the oxygen partial pressure  $p_{O_2}$ . In addition, when the  $p_{O_2}$  partial pressure is low ( $p_{O_2} < 10^{-20}$  bar), the presence of  $Ti^{4+}$  ions still can be observed. When  $p_{O_2}$  is high, e.g. 1

bar, the concentration of  $Ti^{3+}$  ions is only one-order of magnitude lower than the  $Ti^{4+}$  ions so that its concentration cannot be neglected. Therefore, no matter whether the  $p_{O_2}$  partial pressure is very high or very low,  $Ti^{3+}$  and  $Ti^{4+}$  ions always co-exist in grown crystals. Consequently, most reported empirical formula<sup>51,52</sup> used to estimate the concentrations of  $Ti^{3+}$  and  $Ti^{4+}$  through the absorption coefficient and cross section are not reliable because all these formulas are obtained on the assumption that “only  $Ti^{3+}$ ” or “only  $Ti^{4+}$ ” ions exist in the calibration crystal.

## 4.2 Ti ion segregation coefficients

Ti has a segregation coefficient lower than unity in sapphire (see Table 1) resulting in more Ti remaining in the melt than incorporated into the crystal. This is consistent with Figure 7, i.e.  $[Ti^{3+}]_L > [Ti^{3+}]_S$  and  $[Ti^{4+}]_L > [Ti^{4+}]_S$ . The segregation coefficients of Ti ions are defined as the ratio of Ti ion concentration in the solid phase to the concentration in the liquid phase:

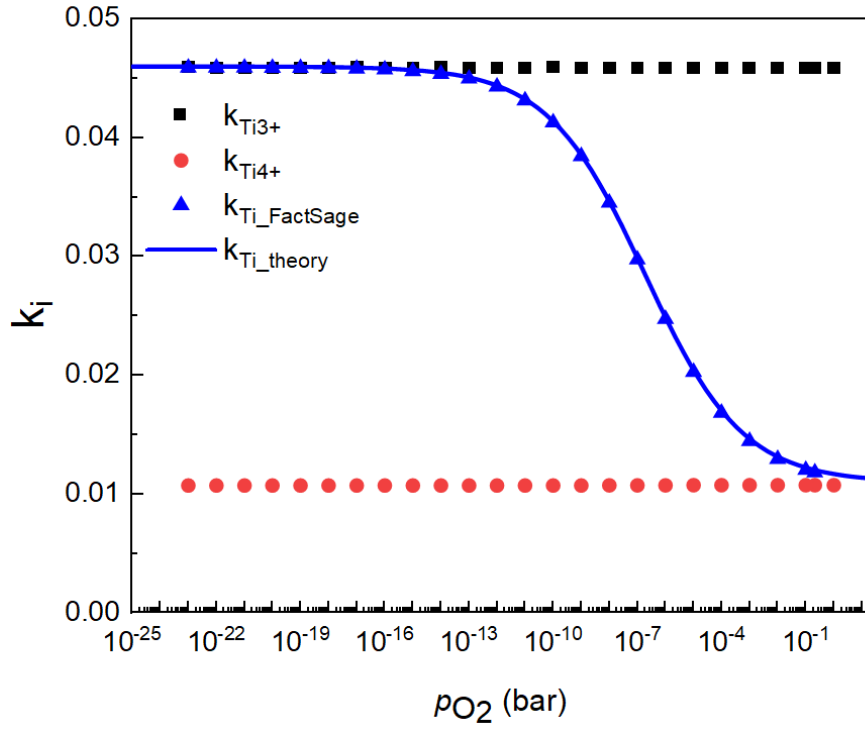
$$k_{Ti^{3+}} = \frac{[Ti^{3+}]_S}{[Ti^{3+}]_L}, \quad (4)$$

$$k_{Ti^{4+}} = \frac{[Ti^{4+}]_S}{[Ti^{4+}]_L}. \quad (5)$$

It is important to mention that the total Ti segregation coefficient does not equal the sum of the segregation coefficients of  $Ti^{3+}$  and  $Ti^{4+}$  but is described as:

$$k_{Ti} = \frac{[Ti^{3+}]_S + [Ti^{4+}]_S}{[Ti^{3+}]_L + [Ti^{4+}]_L}. \quad (6)$$

According to the Ti ion concentrations shown in Figure 7, the segregation coefficients of  $Ti^{3+}$ ,  $Ti^{4+}$  and total Ti at 2053 °C are computed and are presented in Figure 8. It is found that  $k_{Ti^{3+}} > k_{Ti} > k_{Ti^{4+}}$ .



**Figure 8.** Ti segregation coefficients dependence on  $p_{O_2}$  at 2053 °C.  $k_{Ti\_theory}$  is calculated by Eq.(14).

When the oxygen partial pressure  $p_{O_2}$  is very small (reducing atmosphere), most Ti is present as  $Ti^{3+}$ . It follows from equation (6) that

$$k_{Ti} = \frac{[Ti^{3+}]_s + [Ti^{4+}]_s}{[Ti^{3+}]_L + [Ti^{4+}]_L} \approx \frac{[Ti^{3+}]_s}{[Ti^{3+}]_L} = k_{Ti^{3+}}. \quad (7)$$

Similarly, when the partial pressure  $p_{O_2}$  is very high (oxidizing atmosphere), most Ti is present as  $Ti^{4+}$ . Then  $k_{Ti}$  can be approximated as

$$k_{Ti} = \frac{[Ti^{3+}]_s + [Ti^{4+}]_s}{[Ti^{3+}]_L + [Ti^{4+}]_L} \approx \frac{[Ti^{4+}]_s}{[Ti^{4+}]_L} = k_{Ti^{4+}}. \quad (8)$$

Therefore, the increase of  $p_{O_2}$  leads to  $k_{Ti}$  decreasing gradually from the maximum value  $k_{Ti^{3+}} = 0.046$  to the minimum value  $k_{Ti^{4+}} = 0.011$ . This can be seen on Figure 8. The variation of  $p_{O_2}$  has no significant effect on  $k_{Ti^{3+}}$  and  $k_{Ti^{4+}}$ : a variation lower than 0.5% is found from  $10^{-20}$  to  $10^{-1}$  bar.

Defining the ratio of  $[Ti^{4+}]$  and  $[Ti^{3+}]$  in the liquid phase as

$$\frac{[\text{Ti}^{4+}]_{\text{L}}}{[\text{Ti}^{3+}]_{\text{L}}} = \alpha, \quad (9)$$

it can be written as

$$\alpha = K_{eq} \cdot p_{\text{O}_2}^{\frac{1}{4}}, \quad (10)$$

where  $K_{eq}$  is the equilibrium constant of the simplified liquid phase reaction:



with  $K_{eq}$  as:

$$K_{eq} = \frac{[\text{TiO}_2]}{[\text{TiO}_{1.5}] \cdot p_{\text{O}_2}^{\frac{1}{4}}} = \exp\left(-\frac{\Delta G^\circ}{RT}\right), \quad (12)$$

where  $\Delta G^\circ$  is the standard molar Gibbs energy given by FactSage database:

$$\Delta G^\circ = -202.262 + 0.055 \cdot T \text{ (kJ} \cdot \text{mol}^{-1}\text{)}. \quad (13)$$

At 2053 °C, the Gibbs energy of reaction (11) is calculated to be -74.86 kJ·mol<sup>-1</sup> using the “Reaction” module in FactSage. It follows from equations (6), (9), (10) and (12) that the theoretical value for the segregation coefficient of total Ti is:

$$k_{\text{Ti\_theory}} = \frac{k_{\text{Ti}^{3+}} + 48 \cdot k_{\text{Ti}^{4+}} \cdot p_{\text{O}_2}^{1/4}}{1 + 48 \cdot p_{\text{O}_2}^{1/4}}. \quad (14)$$

The relation between  $k_{\text{Ti\_theory}}$  and  $p_{\text{O}_2}$  is also plotted in Figure 8. It is found that the thermodynamically calculated  $k_{\text{Ti\_FactSage}}$  is very close to the theoretical deduction  $k_{\text{Ti\_theory}}$ . This shows that the theoretical expression, based on the simplified reaction (11), gives useful accurate values.

Experimentally measured effective segregation coefficients for total Ti are sometimes referred as  $\text{Ti}^{3+}$  segregation coefficient,<sup>14</sup> based on the assumption that all Ti is present as  $\text{Ti}^{3+}$  and nearly no  $\text{Ti}^{4+}$  is present in the crystal. But in a practical crystal growth process, there are always  $\text{Ti}^{4+}$  ions present in the grown crystals, as shown by

the results on Fig 7. It is noted that the calculated  $k_{Ti^{3+}}$  is much smaller than reported experimental values listed in Table 1. This is because the measured experimental values are the effective segregation coefficient for total Ti while the calculated values are thermodynamic equilibrium segregation coefficients of  $Ti^{3+}$ . Additionally, the reported values vary upon crystal growth techniques and conditions, depending on rotation and pulling rates. It was shown that a slow growth rate and rotation rate tend to increase the segregation of dopants, while fast growth rate and rotation rate tend to decrease dopant segregation.<sup>53</sup> So, the exact thermodynamic segregation coefficients of  $Ti^{3+}$ ,  $Ti^{4+}$  and Ti, cannot be determined directly from experiments. Further, the segregation experiments in the literature show that the effective segregation coefficient is necessarily larger than the thermodynamic one ( $k_0 < k_{eff} < 1$ ).

There are very few papers discussing the equilibrium segregation coefficient of Ti and its relationship with growth and rotation rates. According to the well-known Burton, Prim, Slichter (BPS) equations and boundary layer thickness ( $\delta$ ) for the Czochralski crystal growth process:<sup>54,55</sup>

$$\delta = 1.6D_L^{1/3} \nu_{viscosity}^{1/6} \omega^{-1/2}, \quad (15)$$

$$k_{Ti}^{eff} = \frac{k_0}{k_0 + (1-k_0)e^{-(V_{growth}\delta/D_L)}},$$

it is obtained that

$$k_{Ti}^{eff} = \frac{a}{a + (1-a)e^{-(b \times V_{growth})}}, \quad (16)$$

where  $D_L = 5 \times 10^{-9} \text{ m}^2 \cdot \text{s}^{-1}$  is the diffusion coefficient of Ti in the liquid alumina,  $\nu_{viscosity} = 1.9 \times 10^{-5} \text{ m}^2 \cdot \text{s}^{-1}$  is the kinematic viscosity of the alumina melt,<sup>56</sup>  $\omega$  is the rotation rate,  $a = k_0$  and  $b = 1.6D_L^{-2/3} \nu_{viscosity}^{1/6} \omega^{-1/2}$ . This equation describes the relation between the effective segregation coefficient and the corresponding crystal growth and rotation rates.

**Table 2.** Effective segregation coefficient of Ti measured in Ti:sapphire grown by the Czochralski process under different growth and rotation rates.

$k_{Ti}^{eff}$	Pulling rate (m.s <sup>-1</sup> )	Rotation rate (min <sup>-1</sup> )
0.17-0.20 <sup>17</sup>	$2.78 \times 10^{-7}$	10-15 <sup>57</sup>
0.12 <sup>8</sup>	$1.06 \times 10^{-7}$	5
0.11 <sup>18</sup>	$8.47 \times 10^{-8}$ - $7.06 \times 10^{-7}$	5

The experimental results of Uecker et al.<sup>17</sup> and Kokta et al.<sup>8,18</sup> are listed in Table 2. As calculated from equations (15), the differences in rotation rates do not change significantly the segregation coefficients. Therefore, these effective segregation coefficients of Ti are fitted as function of growth rate using equation (16). The fitting result gives the equilibrium segregation coefficient of Ti in sapphire to be  $k_0 = 0.085 \pm 0.005$ . It matches well with the reported values of  $k_0$ , 0.079 and 0.087, obtained from optical absorption measurement around seeding in sapphire doped with 0.5 wt.% Ti<sub>2</sub>O<sub>3</sub> and 0.3 wt.% Ti<sub>2</sub>O<sub>3</sub> and grown by the gradient freeze technique.<sup>23</sup> The fitted value is comparable to the thermodynamically calculated value  $k_0 = 0.046$ .

On one side, it is possible that, if the mismatch between Ti<sup>4+</sup> solid solubility in the Al<sub>2</sub>O<sub>3</sub> solid solution and the Al<sub>2</sub>O<sub>3</sub>-TiO<sub>2</sub> phase diagram could be further improved, the calculated  $k_0$  value may be closer to the extrapolated experimental value. An attempt to adjust the solidus and liquidus lines in the phase diagram based on a private database from FactSage technical support with respect to the experimental data of Belon et al did not lead to an improved description.<sup>42</sup>

On the other side, strictly speaking, the fitted value  $k_0 = 0.085$  is not the equilibrium segregation coefficient but the BPS equation fitted with the unrealistic  $V_{growth} = 0$ .<sup>58</sup> Since the BPS equation (15) always gives a  $k_0 \leq k_{Ti}^{eff} \leq 1$ , then the  $k_0 = 0.085$  obtained from  $k_{Ti}^{eff}$  should be the threshold value. Therefore, both FactSage value 0.046 and fitted value 0.085 could be right. Consequently, a mean value of  $k_0 = 0.06 \pm 0.02$  is proposed as the equilibrium segregation coefficient of Ti in



Ti:sapphire grown under reducing atmosphere.

Our calculated equilibrium segregation coefficient of Ti is much smaller than the effective segregation coefficient reported in Table 1 except the result of Fielitz et al. Their small value could be caused by large rotation rate which increases the homogeneity of solute in the melt, leading to effective segregation coefficient close to the equilibrium segregation coefficient. From the experimental data in Table 1, <sup>12,15</sup> it is noticed that Ti:sapphire grown by heat exchanger and Kyropolous methods with Mo crucible under vacuum or reducing atmosphere usually give a high effective segregation coefficient around 0.2 and high FOM values, i.e. high concentration ratio of  $Ti^{3+}/Ti^{4+}$ .

## 5 Conclusion

The thermodynamic database of the solid phases in the  $Al_2O_3$ - $TiO_2$  system is updated to study the influence of the oxygen partial pressure  $p_{O_2}$  on the Ti ion valence, Ti ion concentrations and segregation coefficients in the  $Al_2O_3$  solid solution by referring to the experimental solid solubility limit of  $Ti^{3+}$  and  $Ti^{4+}$ . Through taking into account the effect of furnace gas, graphite heating elements and a Mo crucible, the calculation results show that the  $p_{O_2}$  partial pressure should not be lower than  $10^{-20}$  bar during Ti:sapphire growth. In addition, the graphite elements show considerably more influence on  $p_{O_2}$  than the Mo crucible. By varying  $p_{O_2}$  at 2053 °C, it is found that the threshold oxygen partial pressure to obtain  $[Ti^{3+}]_L > [Ti^{4+}]_L$  is  $p_{O_2} < 10^{-7}$  bar and the threshold oxygen partial pressure to obtain  $[Ti^{3+}]_S > [Ti^{4+}]_S$  is  $p_{O_2} < 10^{-4}$  bar.

From the calculated Ti ion concentrations in the solid and liquid phases, the thermodynamic equilibrium segregation coefficients of  $Ti^{3+}$  and  $Ti^{4+}$  in Ti:sapphire are computed to be  $k_{Ti^{3+}} = 0.046$  and  $k_{Ti^{4+}} = 0.011$ . A formula is derived in order to calculate the decrease of  $k_{Ti}$  from  $k_{Ti^{3+}}$  to  $k_{Ti^{4+}}$  as function of the increase of  $p_{O_2}$ .

Taking into account extrapolation of experimental effective segregation coefficients, a value of  $k_0 = 0.06 \pm 0.02$  is proposed for the equilibrium segregation coefficient of Ti in Ti:sapphire under reducing atmosphere.

These results will be used for a proper resolution of the model of  $Ti^{3+}$  and  $Ti^{4+}$  distributions in Ti:sapphire after growth, as described in previous results.<sup>59</sup>

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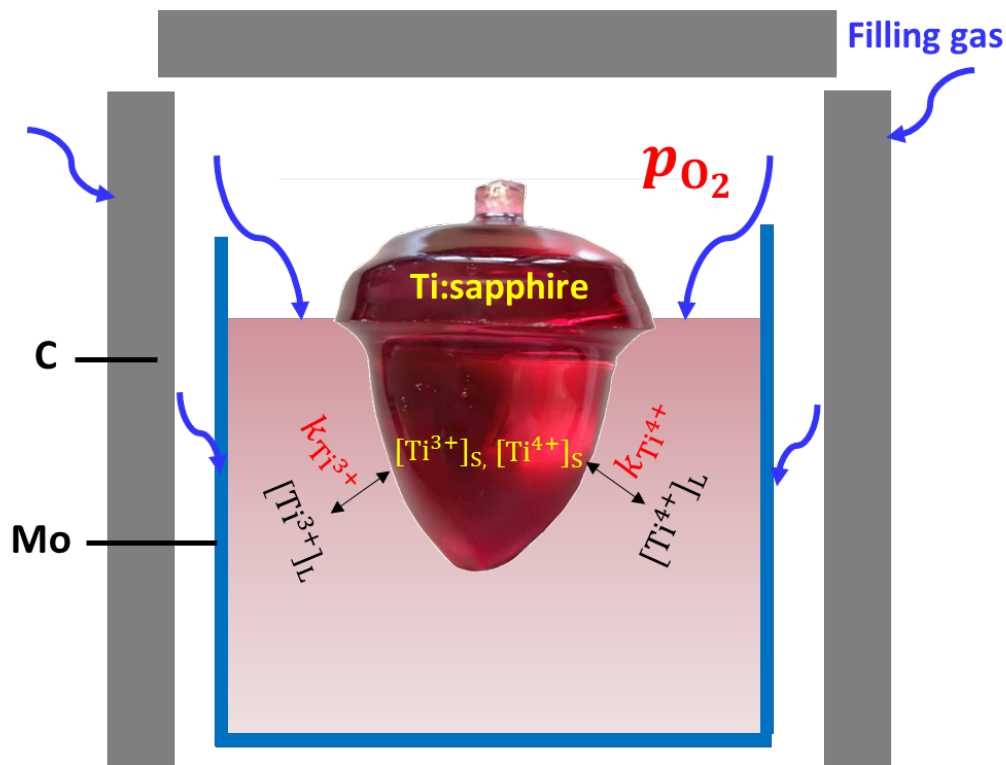
# For Table of Contents Use Only

**Title:** Thermodynamic Calculations of Ti Ion Concentrations and Segregation Coefficients During Ti:sapphire Crystal Growth

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*The influence filling gas on graphite elements and Mo crucible on  $p_{O_2}$  thereby the concentration of  $Ti^{3+}$  and  $Ti^{4+}$  in the solid and liquid phases and their segregation coefficients during Ti:sapphire growth process.*