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The growth of Ti₃SiC₂ coatings onto SiC by reactive chemical vapor deposition using H₂ and TiCl₄

H. Fakih, S. Jacques, M.-P. Berthet, F. Bosselet, O. Dezellus, J.-C. Viala

Laboratoire des Multimatériaux et Interfaces – UMR 5615 University of Lyon 1 / CNRS

43 Boulevard du 11 Novembre 1918 F – *69622 Villeurbanne Cedex, France*

Address for manuscript correspondence:

Laboratoire des Multimatériaux et Interfaces – UMR 5615 University of Lyon 1 / CNRS

Bâtiment Claude Berthollet, 43, Boulevard du 11 Novembre 1918

F – 69622 Villeurbanne Cedex

France

E-mail address: sylvain.jacques@adm.univ-lyon1.fr

Telephone: +33 (0)4 72 43 13 92

Fax: +33 (0)4 72 44 06 18

Abstract:

 $(SiC/Ti_3SiC_2)_n$ multilayered coatings composed of n layers alternately of continuous SiC and Ti_3SiC_2 sub-layers were prepared on carbon substrates. The method consists in depositing SiC by classical chemical vapor deposition (CVD) and then producing a new Ti-containing sublayer from a reaction between SiC and a H₂/TiCl₄ gaseous mixture by reactive CVD (RCVD), and repeating this sequence n times. In accordance with thermodynamics, this RCVD method produces only pure TiC sub-layers when a low dilution ratio of TiCl₄ in H₂ (R=[H₂]/[TiCl₄]) is used. With a high R value, the growth of pure Ti₃SiC₂ thin continuous sub-layers from solidgas reaction is observed for short deposition times. But for long deposition times, the simultaneous growth of additional Ti₅Si₃C_x and TiC sub-layers occurs from solid state diffusion when the initial Ti₃SiC₂ sub-layer thickness exceeds about 1 µm. In that case, the repeating of the sequence results in the further conversion of the additional phases into new Ti₃SiC₂ sublayers from solid state reactions involving TiSi₂ as an intermediate phase and SiC.

Keywords: reactive CVD; Ti3SiC2; multilayer coating; solid-gas reaction; solid state diffusion

1. Introduction

Titanium carbide-silicide Ti_3SiC_2 exhibits unique properties; it is soft and easily machinable, behaves plastically and maintains its strength at high temperature and is resistant to oxidation and thermal shock [1].

As a thin coating, Ti₃SiC₂ has interesting mechanical properties in prospect: it can deform through the formation of kink bands and delamination cracks [2-3]. It is also an excellent electrical and thermal conductor [1] and therefore can be considered for electrical contact layers and connectors at high temperature [4]. In addition, this material exhibits a thermal expansion coefficient around 9×10^{-60} C⁻¹ over the range 25 - 1200°C [5], which is halfway between SiC (around 4×10^{-60} C⁻¹) and most metals (Ag: 19×10^{-60} C⁻¹, Cu: 17×10^{-60} C⁻¹, Fe: 12×10^{-60} C⁻¹...). This ternary compound that combines the advantage of both metals and ceramics could be used as an interlayer to join these two dissimilar materials for thermostructural applications.

However, few studies have reported the synthesis of Ti₃SiC₂ films. Thin coatings could be prepared recently by physical vapor deposition [6]. In earliest works, Ti₃SiC₂ coatings were deposited by chemical vapour deposition (CVD) from different gaseous mixtures such as TiCl₄-SiCl₄-CCl₄-H₂ [7-9] or TiCl₄-SiCl₄-CH₄-H₂ [10]. CVD allows complex geometrical shape substrates to be coated but these studies highlighted that the deposition of pure Ti₃SiC₂ is difficult.

A previous thermodynamic analysis [11] showed that it is theoretically possible to obtain Ti₃SiC₂ as a single solid phase by reactive CVD (RCVD) through the reaction of H₂/TiCl₄ gaseous mixture on solid SiC with a concentration ratio R ([H₂]/[TiCl₄]) equal to 4 (Fig. 1.a) if the correct reactant gas/solid ratio is achieved. But, the experimental procedure did not allow the growth of the pure ternary phase. This was attributed to the impossibility of exceeding

several nanometers in thickness during the first growth of SiC by RCVD (the method used in the previous study) and so to control the gas to solid ratio through matter diffusion [11].

In the present study, we propose to start with a micrometer-thick SiC film deposited by a classical CVD route (in which both silicon and carbon are provided by the gaseous phase) and then to use RCVD for the growth of Ti₃SiC₂ through SiC consumption. For that purpose, we have used a classical low pressure hot wall CVD reactor in which the gaseous pressure and flow are maintained constant during the growth of each layer. As long as solid SiC is available, the gas to solid ratio is therefore controlled by the thickness of the second growing layer, i.e. by the RCVD processing time.

2. Thermodynamic analysis

For the thermodynamic analysis, the computer program used was Gemini 2 and the thermodynamic data were from the Scientific Group Thermodata Europ (Saint Martin d'Hères, France). The temperature was of 1100°C, which is a maximum for our reactor chamber made of silica. The total pressure was set as low as 5 kPa in order to favor coating homogeneity. The calculation details are given in reference [11].

With R = 4, Fig. 1a shows that, if the H₂/TiCl₄ gaseous reagent reacts in too large excess with SiC (i.e. more than 4000 moles of TiCl₄ for one mole of SiC), the solid phase obtained at equilibrium is no longer Ti₃SiC₂ but TiC, silicon being vented in the by-product gaseous phase as silicon chlorides: SiCl_p (p = 2, 3 and 4). In the case of a very large excess of gaseous reagent, using an R ratio as high as R = 35 allows Ti₃SiC₂ to be obtained at equilibrium (Fig. 1b) according to (1):

$$2 \operatorname{SiC}_{(s)} + 3 \operatorname{TiCl}_{4(g)} + 5 \operatorname{H}_{2(g)} \rightarrow \operatorname{Ti}_{3}\operatorname{SiC}_{2(s)} + \operatorname{SiCl}_{2(g)} + 10 \operatorname{HCl}_{(g)}(1)$$

But it can be also co-deposited with $Ti_5Si_3C_x$ particularly if silicon can not be evacuated in the gaseous phase as $SiCl_2$ (Fig. 1b) according to (2): (6-x) $SiC_{(s)} + (14-3x)TiCl_{4(g)} + 2(14-3x)H_{2(g)} \rightarrow (3-x)Ti_3SiC_{2(s)} + Ti_5Si_3C_{x(s)} + 4(14-3x)HCl_{(g)}$ (2)

where x is a constant value in the range $0 \le x \le 1.1$ [12,13].

3. Experimental procedure

3.1. Ti-Si-C layer growth

The coatings were deposited on polycrystalline graphite disks (12 mm in diameter, Ellor 30 from Carbone Lorraine France) placed inside the hot area of a CVD reactor chamber. The CVD apparatus included a horizontal silica tube (30 mm in inner diameter) heated by an electrical resistor furnace. The temperature was 1100°C within the hot area. It was regularly checked between two deposition runs with three Process Temperature Control Rings (type LTH from Ferro Electronic Materials B.V., Uden, The Netherlands) submitted to the same conditions in the reactor as the graphite disks. The total pressure was maintained in the apparatus at a constant value during the deposition of each kind of layer by a vacuum pump through a regulating valve and a pressure gauge. Liquid nitrogen traps permitted the condensation of corrosive by-products such as HCl. Mass flowmeters were used to control the partial gas flow rates of H₂ and CH₃SiCl₃ (MTS).

In each case, a SiC layer was previously deposited by classical CVD from H₂/MTS to be used as solid carbon and silicon sources for the following Ti-Si-C layer growth. For SiC deposition, the ratio [H₂]/[MTS] was 4, the total gas flow rate was 250 sccm (standard cm³min⁻¹, i.e. at P = 101 kPa and T = 20°C) and the total pressure 3 kPa. Then, after evacuation, the H₂/TiCl₄ gaseous mixture was introduced in the reactor and the pressure was set at 5 kPa, which allowed the growth of Ti-Si-C layer(s) by SiC consumption. The titanium tetrachloride vapor was carried by hydrogen through a bubbler at room temperature. The reactant concentration ratio R ([H₂]/[TiCl₄]) was adjusted to 4 or 35 by adding pure H₂ with an extra parallel hydrogen feed line and taking into account the value of TiCl₄ partial pressure at room temperature. For instance, with a room temperature equal to 20°C, the TiCl₄ partial pressure in the bubbler was 1.28 kPa. The H₂ flow rate was set to 26 sccm through the bubbler and to 290 sccm in the second parallel hydrogen line. With a pressure equal to 5 kPa in the feed lines, the TiCl₄ gas flow rate carried out from the bubbler was estimated to 9 sccm, which corresponded to R = 35. To obtain R = 4, the H₂ flow rate was set to 80 sccm through the bubbler (TiCl₄ gas flow rate ≈ 19 sccm) and to 30 sccm in the second parallel hydrogen line. In each case, the deposition sequence (CVD treatment at 3 kPa with H₂/MTS, evacuation, RCVD at 5 kPa with H₂/TiCl₄, and evacuation) was repeated several times in order to obtain a total coating thick enough for further characterization. A repetitive deposition sequence was designated as (S₈/T_t)_n were s was the number of minutes used for each previous SiC sub-layer deposition, t the time in minutes chosen for each RCVD reaction with H₂/TiCl₄ and n the total number of repeated sequences.

3.2. Characterization

The coated disk surfaces were characterized by X-ray diffraction (XRD: X'Pert Pro MPD from Panalytical, equipped with an X'Celerator detector monochromator, CuK α radiation, Almelo, The Netherlands). Then, the coated graphite disks were broken and the fracture surfaces of the coatings were observed with a scanning electron microscope (SEM: S800 from Hitachi, Tokyo, Japan). With sufficiently thick enough sub-layers (i.e. above 1 μ m), cross section composition profiles were determined by electron probe micro-analysis (EPMA: CAMEBAX from CAMECA, Courbevoie, France). EPMA was operated under an accelerating

voltage of 10 kV. After background subtraction, the counting rates obtained for Si and Ti were referred to those recorded under the same conditions on pure and freshly polished standards. After correction for atomic number, absorption and fluorescence, the Si and Ti contents, in percent, were obtained within an error bar not higher than 1 at.%. The carbon content was obtained by subtracting the Ti and Si contents to 100%.

Transmission electron microscopy (TEM) was used (TOPCON 002B, Tokyo, Japan) for thin sub-layers utilizing bright field (BF) and selected area electron diffraction (SAED) techniques. The microscope was equipped with a Kevex energy dispersive spectroscopy (EDS) device for chemical analysis. The chosen spot size for EDS was 56 nm. Only titanium and silicon were considered in the coating analysis (not carbon). Quantitative composition measurements were obtained using the standard Cliff-Lorimer equation. The relative elemental concentration (C_{Ti} and C_{Si}) are related to the measured X-ray peak surfaces above background (S_{Ti} and S_{Si} , respectively) by $C_{Ti}/C_{Si} = k_{SiTi} S_{Si}/S_{Ti}$, where k_{SiTi} is the sensitivity or k-factor. The value of k_{TiSi} was determined from Ti₃SiC₂ grains identified first by SAED in the samples. Ti₃SiC₂ is indeed known as a stoichiometric compound and can serve as a standard. To obtain cross sections for TEM, two pieces of broken coated graphite disks were stuck together with an epoxy resin (Micro-Measurements-Wishay adhesive, Reference M-Bond 610) and mechanically thinned. The thin sheets were then ion-milled (GATAN PIPS, USA) until the electron transparency.

4. Results

4.1. Experimental RCVD with R = 4

Figs. 2 and 3 show that a 240 minutes long treatment of a SiC layer by a H₂+TiCl₄ gaseous mixture with a molar ratio H₂/TiCl₄ = 4 (R = 4) results in the growth of a TiC coating of about 3 μ m in thickness. Fig. 4 shows the SEM observation of a multilayered coating obtained with shorter treatments. SAED patterns confirm that these RCVD treatments of SiC layers lead also to the formation of pure titanium carbide (Fig. 5). Furthermore, the presence of pores can be noticed in the first one-third part of the TiC layers near the previously deposited SiC layer (Figs. 4 and 5).

Fig. 6 presents the change of the TiC layer thickness versus the duration of the treatment which can be interpolated by a parabolic curve (square root of time) except for the last point at 240 minutes.

4.2. *RCVD* with R = 35

4.2.1 "Thick layers"

As shown by the thermodynamic analysis, a way to favor the formation of Ti₃SiC₂ by RCVD is to increase the R ratio by dilution in hydrogen. A first multilayered coating was deposited with R = 35 by following three sequences: (S₆₀/T₉₀)₃. The XRD pattern presented in Fig. 7 reveals the presence of five phases in the multilayered film: SiC, TiC, Ti₃SiC₂, TiSi₂ and Ti₅Si₃C_x. EPMA coupled with SEM observation allows the different phases to be localized across the coating (Fig. 8). As a general trend, the coating consists of a succession of continuous single-phased sub-layers. But surprisingly, even though the three CVD sequences were identical, the three resulting sub-layer sequences found in the whole coating are different from each other. From the carbon disk substrate surface, the coating (about 30 µm thick)) can be described as follow: The first sequence is made of one SiC sub-layer covered with a Ti₃SiC₂ then with a TiSi₂ thin sub-layer (about 1 µm) and then with a last sub-layer of global composition Ti_x-Si_y-C_z that is likely to contain a mixture of TiC and Ti₃SiC₂. The second

sequence is similar to the first one but here the last sub-layer clearly corresponds to Ti_3SiC_2 . The third sequence is quite different from the others: after the SiC sub-layer, a thin TiC sublayer (about 1 µm in thickness) is first observed before the Ti_3SiC_2 sub-layer. Then the sequence ends with a thick (about 4 µm) $Ti_5Si_3C_x$ sub-layer. Each Ti_3SiC_2 sub-layer detected in the coating is about 2-3 µm thick.

A second multilayered coating was deposited with R = 35 but, in this case, the duration chosen for the SiC_(s) + H₂/TiCl_{4(g)} RCVD reaction was divided by three: (S₃₀/T₃₀)₆. SEM observation confirms the presence of the six (SiC/Ti-Si-C) bi-layers in the coating (Fig. 9). The corresponding XRD pattern is similar to the previous one except for the TiC phase that was not detected (Fig. 10). A TEM observation performed in the area of sub-layer n°5 reveals the presence of Ti₃SiC₂ crystals (Fig. 11). The total coating thickness is 35 µm but here the thickness of each sub-layer is barely enough for EPMA analysis. So, Si and Ti EDS composition measurements were performed in the TEM on the Ti-Si-C sub-layers n°2, n°5 and n°6 of the thin foil (Fig. 12). This multilayer is quite similar to (S₆₀/T₉₀)₃. Roughly, Ti-Si-C sub-layer n°2 is only made of Ti₃SiC₂, Ti-Si-C sub-layer n°5 is made of three sub-layers: Ti₃SiC₂/TiSi₂/Ti₃SiC₂, and the last Ti-Si-C sub-layer is made of two sub-layers: Ti₃SiC₂/ Ti₅Si₃C_x.

4.2.2 "Thin layers"

By reducing more the duration of each deposition sequence, it is possible to obtain submicrometer thin sub-layers as shown in Fig. 13 for $(S_{10}/T_{10})_n$ and $(S_{3'}/T_{3'})_n$. In both cases, the XRD patterns only reveal the presence of SiC and especially Ti₃SiC₂ (Fig. 14). In that case, the formation of TiC, Ti₅Si₃C_x and TiSi₂ is avoided and the resulting deposited film is a $(SiC/Ti_3SiC_2)_n$ multilayered coating. It is important to note that from SEM observations, the Ti₃SiC₂ coatings are characterized by plate-like microstructure with grains oriented perpendicular to the substrate surface. This orientation is confirmed by XRD: the {008} peak is missing whereas the {110} reflection appears stronger than for a calculated powder diffraction pattern, which indicates that the basal crystallographic planes are oriented perpendicular to the substrate [14]. This result is similar to the previous CVD studies [7-10]

Discussion

The use of different durations for the RCVD treatments allows the relationship between spatial and time sequence to be drawn. With R = 35, the rapid growth of pure Ti₃SiC₂ is first observed at the very beginning of the treatment. As long as the treatment duration t does not exceed a critical time denoted as t_{crit} (t < t_{crit}, with 10 min < t_{crit}' < 30 min), the pure Ti₃SiC₂ layer still grows but at a reduced rate: 1.1 µm thick in 3 minutes to only 1.3 µm thick in 10 minutes. Then, the very last unit of each multi-layered coating (the one not covered by a new SiC film) must be considered to describe the spatiotemporal growth, i.e. the sixth Ti-Si-C layer in (S₃₀/T₃₀)₆ and the third one in (S₆₀/T₉₀)₃. For t > t_{crit}, a second layer made of Ti₅Si₃C_x grows at a fast rate: 1.9 µm thick in 30 minutes and 6.0 µm thick in 90 minutes. At the same time, the first Ti₃SiC₂ sub-layer located near the previously deposited SiC still grows very slowly (1.7 µm thick in 30 minutes and 2.8 µm thick in 90 minutes). For a reaction time longer than 30 minutes, a third and thin TiC sub-layer also develops between SiC and Ti₃SiC₂.

These results tend to show that a one step growth of a pure Ti_3SiC_2 layer thicker than 1.5 µm is impossible by RCVD. A way to circumvent this limit and obtain a thick pure Ti_3SiC_2 film should be to repeat short SiC/Ti_3SiC_2 coating sequences by reducing each SiC sub-layer deposition duration till it is totally consumed, i.e. by realizing $(S_{s'}/T_{t'})_n$ with $t \le t_{crit}$ and s < t. Experiments are planned to check up on that assumption..

For "thick" Ti-Si-C sub-layers prepared with $t > t_{crit}$, if a new SiC film is deposited on the three-phased TiC/Ti₃SiC₂/Ti₅Si₃C_x coating, two new solid state reactions can develop consistently with the Ti-Si-C phases diagram [11,15-17]. On the one hand, SiC reacts with

Ti₅Si₃C_x to form Ti₃SiC₂ and TiSi₂. On the other hand, the TiC thin layer formed onto SiC is slowly converted into Ti₃SiC₂ by reaction with Ti₅Si₃C_x and TiSi₂. Development of these solidstate reactions explains why the brittle Ti₅Si₃C_x phase is no more present in the sub-layers covered by SiC. The texture difference between a Ti₃SiC₂ sub-layer located near the previously deposited SiC film and a Ti₃SiC₂ sub-layer located near the next SiC film (Fig. 8 and 9) evidences the difference between both mechanisms: mainly solid-gas (SiC-H₂/TiCl₄) reaction for the first one and solid-solid (Ti₅Si₃C_x-SiC) reaction for the second one.

At first sight, in the case of solid-gas reactions, this work seems to raise discrepancies between thermodynamic calculations and experimental results. The reasons for this discrepancies will be analyzed in the following by considering different cases: low R value (i) or high R value (ii) and for a high R value: thin coatings (iia) and thick coatings (iib).

When R = 4 (i), Fig. 1a shows that we should obtain pure Ti₃SiC₂ rather than the TiC obtained experimentally (Fig. 5). The previously calculated deposition diagram [11] showed that to obtain TiC at equilibrium, R should be less than 2.3 for a co-deposition with Ti₃SiC₂ and equal to about 0.5 for pure TiC growth. This first seeming discrepancy could originate from a mere shift between the R ratio used for calculation and the experimental ratio and more particularly by a shift between the ratio corresponding to the gaseous system H₂/TiCl₄ introduced in the CVD reactor and the actual ratio for H₂ and TiCl₄ molecules really reaching the SiC substrate surface where the reaction takes place. As H₂ is nearly one hundred times less dense than TiCl₄ gas, after convection through the reactor, the gas may be poorer in hydrogen at the bottom part of the hot area where the carbon disk substrates are set. Also, the diffusion rates of hydrogen across the boundary layer at the substrate surface could be different from the one of titanium chloride, which might be responsible for a change of the R ratio.

When R = 35 and when only thin layers are deposited by RCVD during short deposition times (iia), the precursor gas phase is in direct contact with uncovered SiC solid substrate. As

a gaseous phase is less dense than a solid phase, this case should correspond to a small quantity of TiCl₄ reacting with SiC, i.e. $n(TiCl_4) < n(SiC)$. In that case, as long as SiC is still present at equilibrium, Ti₃SiC₂ should be co-deposited with TiSi₂ (Fig. 1b). Experimentally, if thin Ti₃SiC₂ layers could be actually obtained in these conditions, TiS₂ was never detected in thin coatings realized in less than 10 minutes (Fig. 14). Once again, if a decrease of the R ratio is admitted, the thermodynamic calculations that predict the growth of pure Ti₃SiC₂ by partial consumption of SiC when R is less or equal to 20 (and superior to 2.3) are in accordance with the experimental result.

Finally, for thick coatings prepared with a high R value (iib), after the formation of pure Ti_3SiC_2 , the growth of Ti_3SiC_2 and $Ti_5Si_3C_x$ is observed as predicted by the thermodynamic calculations for $n(TiCl_4) > n(SiC)$ (Fig. 1b) and R > 6.7 [11]. This point can be achieved when the Ti₃SiC₂ sub-layer is thick enough (\sim 1.5 µm) to isolate the SiC substrate from the gaseous molecules, which results in the vanishing of SiC from the system at equilibrium according to thermodynamics. However, the simultaneous formation of both ternary compounds does not result from the expected co-deposition since the phases are not mixed in one layer but separated in two distinct continuous sub-layers. It is worth noting that, once a continuous reaction layer has formed at the substrate surface by RCVD, this layer acts as a diffusion barrier. Further reaction between the substrate and the gas phase can then only proceed by solid state volume diffusion through the barrier layer. Even if local equilibria still exist at the substrate/layer and layer/gas interfaces, chemical potential gradients take place in the barrier layer and the underlying substrate is no more in equilibrium with the gas phase [18,19]. Thus, the thermodynamic analysis presented in this paper and in reference [11] is actually no more valid when $t \gg t_{crit}$, and particularly it can no longer be used to account for the experimental results when $(TiCl_{4(g)}) >> n(SiC_{(s)})$.

At this point, the diffusion path concept and solid state reaction-diffusion models [18-20] appear as the most appropriate tools to describe further development of the RCVD process. The parabolic curve presented in Fig. 6 for a low R value is thus typical of a diffusion mechanism. (The plateau observed for very long time deposition can be attributed to the development of pores in TiC by Kirkendall effect that end up by cuting off the diffusion path.) The introduction of inert markers should be useful in further work for better understanding of the growth of thick Ti-Si-C layers by RCVD.

Conclusion

The RCVD method allows a sub-micrometer SiC surface layer to be converted into Ti_3SiC_2 in a few minutes if a sufficient dilution of the titanium tetrachloride vapor in hydrogen is used to avoid the direct growth of TiC. These results accord with thermodynamics if a shift between the R ratio used for calculation and the experimental ratio is admitted. Hence, with periodic changes of the gases introduced in the CVD reactor, it is possible to deposit $(SiC/Ti_3SiC_2)_n$ multilayered coatings as long as short enough treatment times are used for the growth of each Ti_3SiC_2 thin sub-layer. For long deposition times, the RCVD treatment of SiC results in the formation of TiC and $Ti_5Si_3C_x$ additional sub-layers through solid state diffusion. The alternation of these thick coatings with SiC layers results in the further conversion of the additional brittle phases into new Ti_3SiC_2 sub-layers from solid state reactions that involve $TiSi_2$ as an intermediate phase.

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Legends

- Fig. 1. Calculated quantities of solid species produced at equilibrium from $\{H_2/TiCl_4\}$ gaseous mixture reaction on 1 mole of SiC for R = 4 (a) and R = 35 (b) versus the quantity of TiCl₄ (R = H₂/TiCl₄, 1100°C, 5 kPa).
- Fig. 2. SEM observation of $(S_{150}/T_{240})_1$ coating deposited with R = 4.
- Fig. 3. EPMA of $(S_{150'}/T_{240'})_1$ coating deposited with R = 4.
- Fig. 4. SEM observation of $(S_{20'}/T_{t'})_4$ coating deposited with t = 15, 25, 35 and 45 minutes and with R = 4.
- Fig. 5. BF TEM observation and SAED pattern (insert) of the fourth bi-layer ($S_{20'}/T_{45'}$) of $(S_{20'}/T_{t'})_4$ coating {t' = 15', 25', 35' and 45'} deposited with R = 4.
- Fig. 6. Thicknesses of TiC layers deposited with R = 4 versus treatment durations.
- Fig. 7. XRD pattern of $(S_{60'}/T_{90'})_3$ deposited with R = 35.
- Fig. 8. SEM observation and EPMA of $(S_{60'}/T_{90'})_3$ deposited with R = 35.
- Fig. 9. SEM observation of $(S_{30}/T_{30})_6$ coating deposited with R = 35.
- Fig. 10. XRD pattern of $(S_{30'}/T_{30'})_6$ deposited with R = 35.
- Fig. 11. BF TEM observation and SAED patterns (inserts) of sub-layer n°5 of $(S_{30'}/T_{30'})_6$ deposited with R = 35.
- Fig. 12. TEM EDS analysis of Ti-Si-C sub-layer n° 2 (a), sub-layer n° 5 (b) and sub-layer n° 6 (c) of $(S_{30}/T_{30})_6$ coating deposited with R = 35. (carbon concentration not represented)
- Fig. 13. SEM observation of $(S_{10'}/T_{10'})_n$ (a) and $(S_{3'}/T_{3'})_n$ (b) deposited with R = 35.
- Fig. 14. XRD pattern of $(S_{3'}/T_{3'})_n$ deposited with R = 35.

Figures



Fig. 1. Calculated quantities of solid species produced at equilibrium from $\{H_2/TiCl_4\}$ gaseous mixture reaction on 1 mole of SiC for R = 4 (a) and R = 35 (b) versus the quantity of TiCl₄ (R = H₂/TiCl₄, 1100°C, 5 kPa).



Fig. 2. SEM observation of $(S_{150}/T_{240})_1$ coating deposited with R = 4.



Fig. 3. EPMA of $(S_{150'}/T_{240'})_1$ coating deposited with R = 4.



Fig. 4. SEM observation of $(S_{20}/T_t)_4$ coating deposited with t = 15, 25, 35 and 45 minutes and with R = 4.



Fig. 5. BF TEM observation and SAED pattern (insert) of the fourth bi-layer $(S_{20'}/T_{45'})$ of $(S_{20'}/T_{t'})_4$ coating {t' = 15', 25', 35' and 45'} deposited with R = 4.



Fig. 6. Thicknesses of TiC layers deposited with R = 4 versus treatment durations.



Fig. 7. XRD pattern of $(S_{60'}/T_{90'})_3$ deposited with R = 35.



Fig. 8. SEM observation and EPMA of $(S_{60'}/T_{90'})_3$ deposited with R = 35.



Fig. 9. SEM observation of $(S_{30'}/T_{30'})_6$ coating deposited with R = 35.



Fig. 10. XRD pattern of $(S_{30'}/T_{30'})_6$ deposited with R = 35.



Fig. 11. BF TEM observation and SAED patterns (inserts) of sub-layer n°5 of $(S_{30}/T_{30})_6$ deposited with R = 35.



Fig. 12. TEM EDS analysis of Ti-Si-C sub-layer n° 2 (a), sub-layer n° 5 (b) and sub-layer n° 6 (c) of $(S_{30'}/T_{30'})_6$ coating deposited with R = 35. (carbon concentration not represented)



Fig. 13. SEM observation of $(S_{10'}/T_{10'})_n$ (a) and $(S_{3'}/T_{3'})_n$ (b) deposited with R = 35.



Fig. 14. XRD pattern of $(S_{3'}/T_{3'})_n$ deposited with R = 35.