

## Phase diagram of gas-hydrate slurries in gas-shortage

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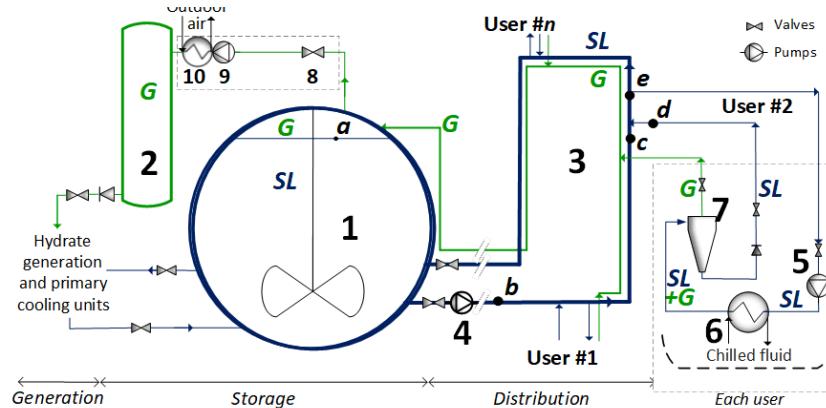


### Warning: bad motivations

- Severe addiction to Thermodynamics
  - Attraction for useless issues
  - Neurotically excessive attention to tiny details

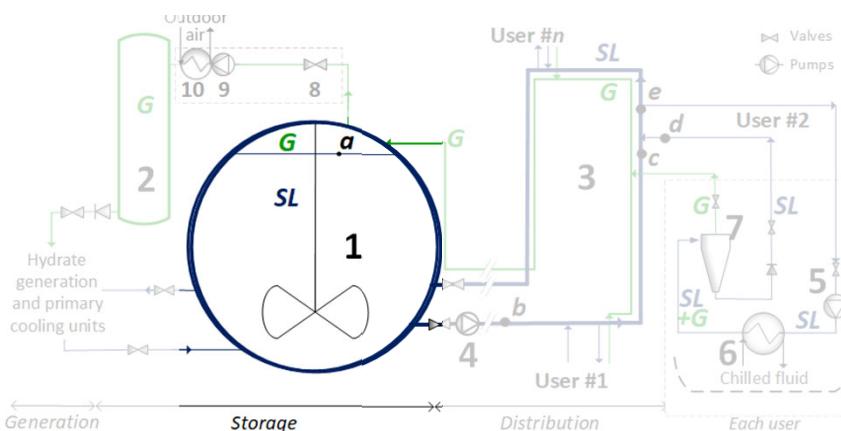
## Context - 1

- Slurries of mixed-gas-hydrate (typically CO<sub>2</sub>+TBPB) in secondary refrigeration processes (storage and transport of cold): *numerical simulation, performance analysis.*



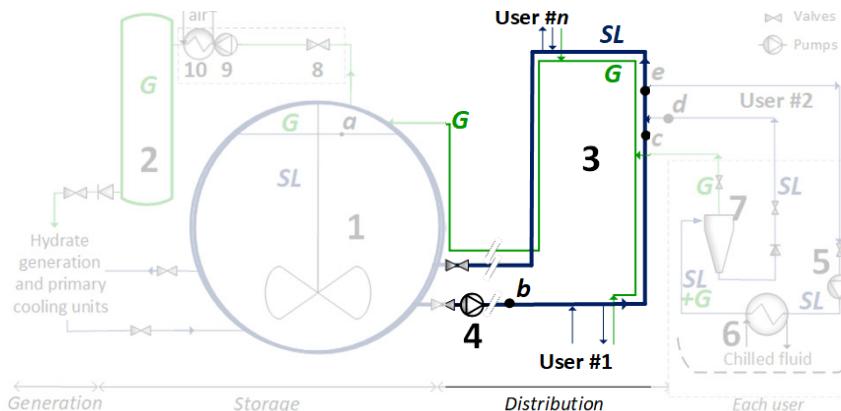
## Context - 2

- Storage tank **1**: Stirred slurry bath (**SL**) and Gas blanket (**G**), the point **a** is at the free surface.



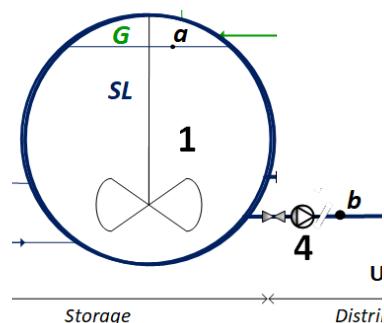
## Context - 3

- Distribution loop **3**: users in series, probably separate circuits for the gas (**G**) and the solid & liquid phases (slurry **SL**), point **b** at the outlet of the distribution pump **4**.



## What about pressurized slurries?

- Point **a** at the free surface: 3-phase equilibrium (**SLG**)
- Point **b** in the bulk of slurry: only two phases (**SL**),
- From **a** to **b**, the slurry is pressurized ...
  - ... first by the hydrostatic pressure field,
  - ... then by the distribution pump.
- Present issue: What is the thermodynamic state of the pressurized slurry at point **b**?

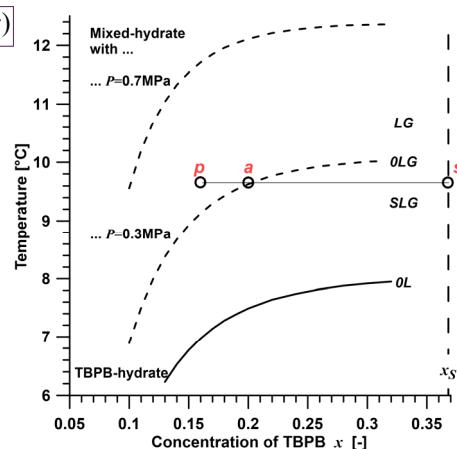


## Mixed Hydrate of TBPB + CO<sub>2</sub>: phase diagram

- Diagram  $T$  vs.  $x$  ( $x$ =TBPB concentration in the solution)

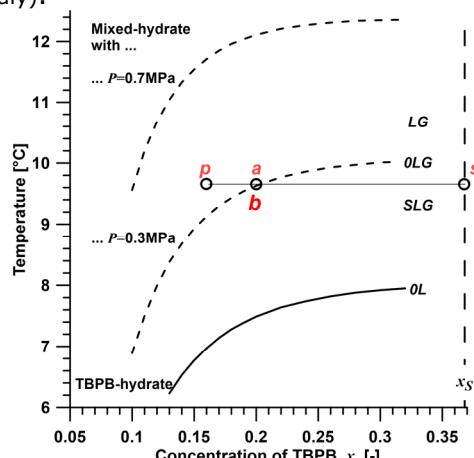
- For the hydrate crystal: Vertical line  $x = x_s$ .

- EoS for the liquid solution  $T = fT_{eq}(P, x)$   
-> dashed (- - -) equilibrium curves with  $P$  as parameter.
- 3-phase equilibrium in the H<sub>2</sub>O + TBPB + CO<sub>2</sub> system:  
when  $P \uparrow$  while  $T \rightarrow$  (path **a**->**p**)  
then,  $x$  must  $\downarrow$
- This is obtained only when hydrate crystals (**s**) are generated
- Which requires supply of gaseous CO<sub>2</sub>
- **But there is no gas available** between points **a** and **b**.



## What happens between points **a** and **b**?

- Liquid and solid phases are not changed by mechanical pressurization (hardly).
- Point **b** (pressurized slurry) is very close to point **a**, and remains distant from equilibrium (point **p**).
- *The lack of gas prevents the system to move from **b** to **p**.*
- **The slurry is in gas-shortage.**
- Thermodynamic analysis, first for the 3-phase equilibrium.



## Variance analysis - the Gibbs rule

$$\bullet V = C + 2 - \Phi$$

### Equilibrium with 3 components and 3 phases

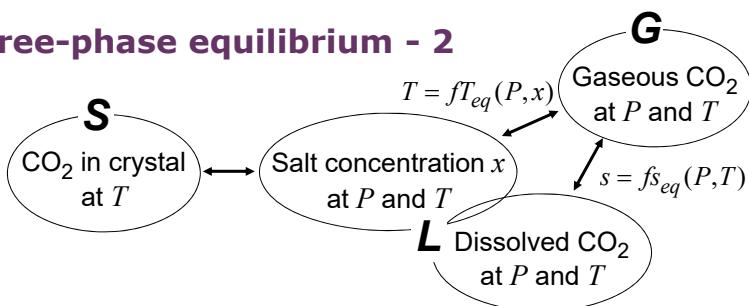
we are familiar with

$$V = 2.$$

- **Two degrees of freedom:**  
typically *Temperature and Pressure*.

- The system of unknowns & equations can be solved only when **two equations of state** (EoS) are given:
  - One for the *3-phase equilibrium with hydrate*:  $T = fT_{eq}(P, x)$
  - One for the *CO<sub>2</sub>-dissolution equilibrium*:  $s = fs_{eq}(P, T)$

## Three-phase equilibrium - 2



- CO<sub>2</sub> is the only component present in the three phases.

**Three-phase equilibrium  $\Leftrightarrow$**

CO<sub>2</sub> has the **same chemical potential** in each phase, solid (part of hydrate crystal), liquid (dissolved) and gas.

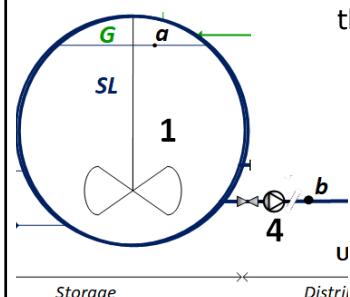
## And when the gas phase is absent (i.e. for slurries in gas-shortage) ...

$$\bullet V = C + 2 - \Phi$$

- With  $\Phi=2$ ,  $V=3$ : there is an **additional degree of freedom**.
  - Although distant from the 3-phase equilibrium, the pressurized slurry SL is not out-of-equilibrium, it has its own equilibrium.**
  - Herein, the amount of CO<sub>2</sub> contained in the slurry SL is chosen as the additional degree of freedom, if below the maximum allowed by crystals and dissolution at given  $T$  and  $P$ .

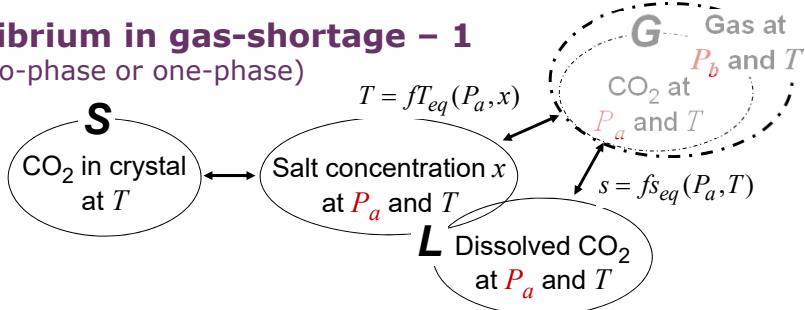
## And when the gas phase is absent - 2

- With that additional degree of freedom, only **one** equation of state is needed.
- CO<sub>2</sub> has same chemical potential in the solid and liquid phases.
  - Mechanical compression alone (without gas and adiabatic) does not change composition of the solid and liquid phases between **a** and **b**.
    - The state at point **b** is described by the equations of state written at point **a**:  $T = fT_{eq}(P_a, x)$  and  $s = fs_{eq}(P_a, T)$ .
    - P<sub>a</sub>** emerges as a kind of **CO<sub>2</sub>-partial-pressure at point b**, obviously with  $P_a < P_b$ .



## Equilibrium in gas-shortage – 1

(two-phase or one-phase)



- From that notion of  $\text{CO}_2$ -partial-pressure one can **imagine a virtual gas** at total pressure  $P_b$ , consisting of  $\text{CO}_2$  at partial pressure  $P_a$  plus a perfectly inert gas.
- $\text{CO}_2$  in that gas would have the **same chemical potential** as that of  $\text{CO}_2$  in the liquid and solid phases (*solid when relevant*).
  - For the sake of generality, the  $\text{CO}_2$ -partial-pressure is now  $P_{CD}$ , and the total pressure  $P_{tot}$ .

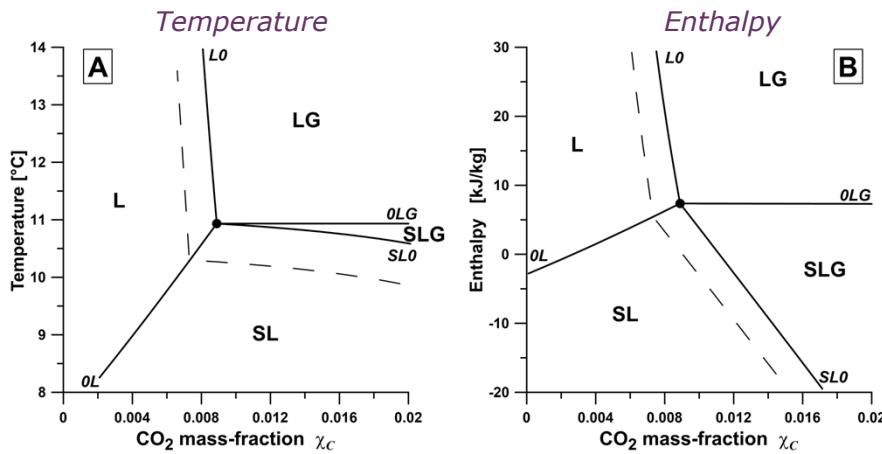
## Equilibrium in gas-shortage – 2

- THE equation of state is implicit:**

- Three degrees of freedom:  $T, P_{tot}, \chi_{CD}$  (total amount of  $\text{CO}_2$ )
  - For any value of the  $\text{CO}_2$ -partial-pressure  $P_{CD}$ , one has:
    - $s = fs_{eq}(P_{CD}, T)$  -> amount of  $\text{CO}_2$  dissolved in the liquid,
    - $T = fT_{eq}(P_{CD}, x)$  ->  $x$  salt concentration in the liquid phase,  
 -> solid mass fraction, -> amount of  $\text{CO}_2$  in the solid phase,  
 -> total amount of  $\text{CO}_2$ ,
- For **one** value of  $P_{CD}$ , that total amount of  $\text{CO}_2$  equates  $\chi_{CD}$ .
  - Note:  $T, \chi_{CD}, P_{CD}, s$ , and  $x$  are fully coupled but  $P_{tot}$  is absolutely independent from them (mechanical compression of the slurry does keep concentrations  $x$  and  $s$  constant).

## Phase diagram of slurry in gas-shortage

- $T$  and  $h$  vs. global  $\text{CO}_2$ -mass-fraction (at  $P=0.5 \text{ MPa}$ ):  
4 domains SLG, SL, LG & L; the dashed curves are for  $P_{CD} = 0.8 \times P$ .



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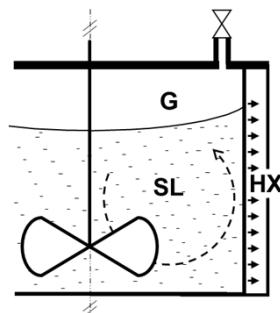
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## Another case of gas-shortage

- When cooling a slurry (SL) in a stirred bath covered by a gas (G) blanket (e.g. when generating hydrate crystals), convection in the bath moves elements of slurry towards the cold heat-exchanger (HX); close to that heat-exchanger, hydrate crystals should form, but they can't, just because there is no gas below the free surface. (once again: gas-shortage).



- Next question: What happens when a slurry in gas-shortage is cooled?

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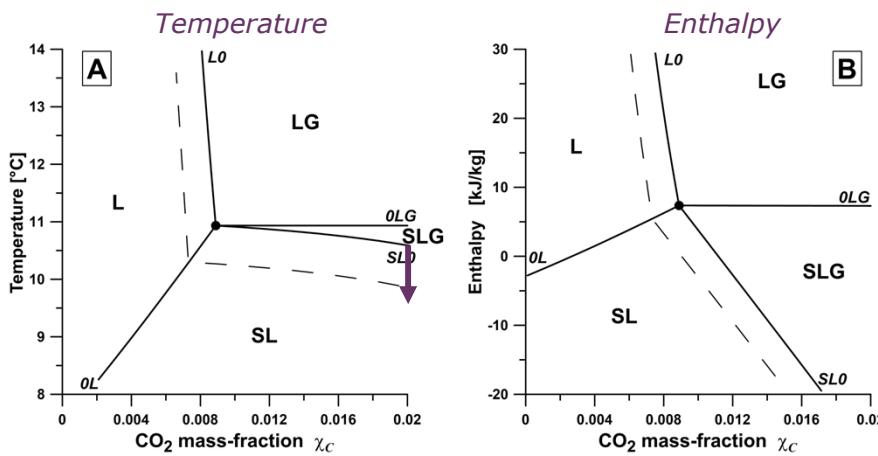
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16

## Cooling a slurry in gas-shortage

- Let us reduce the temperature of a slurry in gas-shortage by 1K.  
First, the partial pressure  $P_{CD}$  decreases (by more than 20%).



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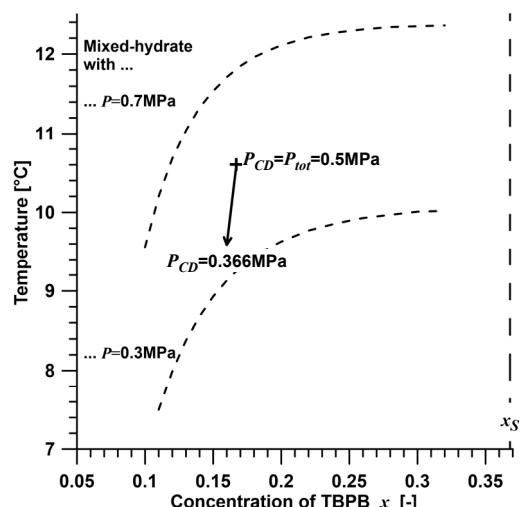
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## ... in the $T-x$ diagram ... plus mass balances ...

- The value of  $x$  slightly decreases**  
(from 0.167 to 0.160),
- $P_{CD} \searrow \Rightarrow$  the amount of dissolved  $\text{CO}_2$  decreases**  
(from 0.0078 to 0.0058)
- All that  $\Rightarrow$  crystals are generated**  
(from 0.173 to 0.201,  
i.e. not few)
- Now, what about the enthalpy balance?**



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## ... and the enthalpy balance for $\Delta T=-1K$

- **Enthalpy change ...**
- ... **by sensible heat** ( $C_p.dT$ ) = **-3.7kJ/kg**
- and **by latent heat** ( $\Delta h.dm$ ) = **-5.0kJ/kg**, i.e. with ...
  - ... release of dissolved CO<sub>2</sub> (endothermal)
  - and generation of hydrate crystals (exothermal)
- Apparently, there is only a temperature drop.
  - However, some dissolved CO<sub>2</sub> is released for forming new hydrate crystals.
  - Big surprise: in that redistribution of CO<sub>2</sub>, the latent heat is larger than the sensible heat!

- ## Other comments
- When **heating a slurry in gas-shortage**, there is no gas release, until  $P_{CD} = P_{tot}$ .  
*(a probably unexpected behaviour)*
  - Slurries of **single gas-hydrate** (CH<sub>4</sub>, CO<sub>2</sub>...) may also be in gas-shortage
  - Present analysis is on **equilibrium states only**.  
*Actual behaviours involve other effects, the understanding of which however always refers to equilibrium states.*

## Conclusion

- **Slurries in gas-shortage have their own equilibria**  
(independent from the 3-phase equilibrium).
  - There may be **transfers of CO<sub>2</sub>** between **dissolved state** and **hydrate crystals**.
  - In such cases, the **latent heat** may be **more significant** than the sensible heat.
- 
- **THANK YOU FOR YOUR ATTENTION**  
*to that tiny useless issue.*

## Imagine ...

- A 'system'  
(= given amounts of water, TBPB and CO<sub>2</sub>)  
enclosed in a balloon  
submitted to external pressure  
and temperature conditions  
with increasing pressure  
or decreasing temperature.

