

WET GRANULATION IN HIGH SHEAR MIXER: EFFECT OF PHYSICOCHEMICAL PROPERTIES ON THE GROWTH KINETICS



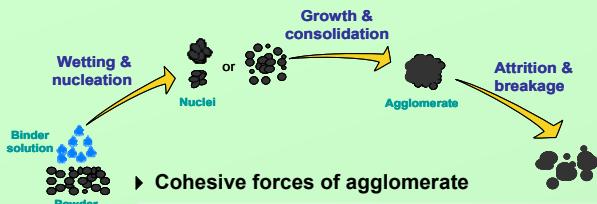
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Introduction

Wet granulation mechanisms (Lister et al., 2001)



Cohesive forces of agglomerate

Tensile strength of agglomerate

$$\sigma_t = C \frac{(1 - \varepsilon)}{\varepsilon} \frac{|F_{\text{bound}}|}{d^{2-p}}$$

► Static force (Rumpf, 1962)

► Dynamic force (Ennis et al., 1991)

Capillary number Ca



Ca = $\frac{\text{Dynamic force}}{\text{Static force}}$

• $Ca < 10^{-3}$: Viscous term made negligible contribution to bridge strength (Ennis et al., 1990)

• $Ca > 1$: Viscous force predominate and the granule growth depends on viscous force

Objective

- Study of wet granulation of microcrystalline cellulose powder, MCC (Avicel PH101), by aqueous solutions of polymers using high-shear mixer granulators
- Understand the effect of physicochemical properties, such as the liquid viscosity μ_L , the liquid surface tension γ_L and the wettability of a binder solution on solid particles surfaces (contact angle, θ), on the agglomeration kinetics

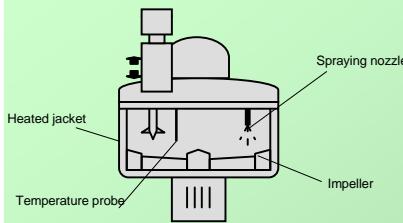


Origin of the interparticles cohesion forces:

Static forces or Dynamic forces?

Granulation equipment

Zanchetta Roto high-shear mixer



Advantages

- Short process time (5min)
- Less liquid binder are needed
- Granulation of cohesive materials
- Production of dense granule with low porosity
- Porosity of the granule can be controlled

Granulation parameters

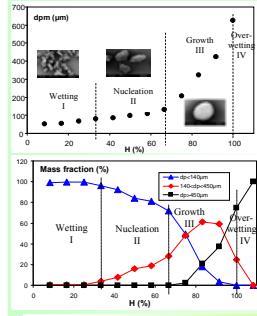
- Capacity: 10L
- Impeller speed N: 400 rpm
- T° drying: 80°C
- Powder weight: 600 g
- Solution flow rate: 50 g/min

Granulation process stages

- Dry mixing of powder
- Liquid addition
- Wet massing
- Drying

Typical example of granulation

Granulation profile



Studied criteria

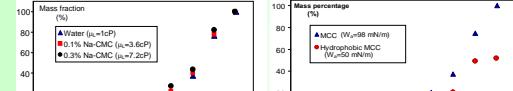
- Mean diameter: $d_p = \frac{\sum f_i d_i}{\sum f_i}$
- Growth rate: $X = \frac{d_p - d_{p_0}}{d_{p_0}}$
- Three characteristic size classes fraction:
 - Fine class: diameter less or equal to 140 μm
 - Intermediate class: 140<dp<450 μm
 - Coarse class: dp>450 μm
- Liquid content: $H = \frac{\text{Liquid mass}}{\text{Dry solid mass}} \times 100$

$$\text{Growth kinetic constant } K = \frac{d}{dH} \ln \left(\frac{x'_{\text{fin}}}{x_{\text{fin}}} \right)$$

The evolutions of the three characteristic size classes versus H in the regime II and III are similar with those of first order consecutive chemical reactions: A→B→C.

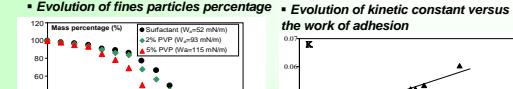
Effect of the work of adhesion: $Ca' < 1$

Evolution of coarse agglomerates percentage



The granule growth is not affected by an increase of the solution viscosity

Evolution of fines particles percentage



$W_a \Rightarrow$ a smaller amount of liquid binder required to enhance the growth

$W_a \Rightarrow$ a faster disappearance of the fines particles

The kinetic constant K is directly related to the work of adhesion

Materials

Binders solutions

- Characteristics of the binder solutions, liquid/solid adhesion work and capillary viscous number values

Binder solution/particles	γ_L (mN/m)	μ_L (cP)	Adhesion work W_a (mN/m)	Ca'
Water/MCC	72	1.0	98	0.06
Water/MCC hydrophobic	72	1.0	50	0.12
surfactant/MCC	26	1.0	52	0.11
2% PVP/MCC	62	1.1	93	0.07
3% PVP/MCC	61	1.1	104	0.07
5% PVP/MCC	61	1.5	115	0.08
0.1% Na-CMC1/MCC	72	3.6	94	0.22
0.3% Na-CMC1/MCC	72	7.2	92	0.46
1% Na-CMC1/MCC	73	25.4	91	1.64
1% HPMC/MCC	53	10.0	73	0.80
2% HPMC/MCC	54	50.0	75	3.90

*non-Newtonian solutions. The apparent viscosity is calculated for a velocity gradient of 1000 s⁻¹

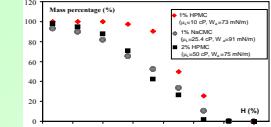
- Capillary number : $Ca' = \frac{\mu_L U}{W_a}$ with $W_a = \gamma_L (1 + \cos \theta)$, $U = \pi ND$ and $N = 400$ rpm

- Non ionic surfactant $\Rightarrow \gamma_L \nabla W_a \nabla \mu_L$ is not affected
- ↗ (w/w) PVP $\Rightarrow \gamma_L \nabla W_a \nabla \mu_L$ is not affected
- ↗ (w/w) Na-CMC $\Rightarrow \mu_L \nabla \gamma_L \nabla W_a$ are weakly affected
- ↗ (w/w) HPMC $\Rightarrow \mu_L \nabla \gamma_L \nabla W_a$ are weakly affected

Influence of the physicochemical properties

Influence of the viscosity: $Ca' \geq 1$

Evolution of fines particles percentage



$W_a \Rightarrow$ decrease of the amount of liquid to achieve agglomerate growth

$\mu_L \Rightarrow$ increase of the growth rate, X, by a factor of 2

Conclusion

The results of our study on wet granulation of the microcrystalline cellulose show that :

- The viscosity of the solution has no significantly effect on the granulation process for a capillary number lower than 1.64. In these conditions, the increasing the work of adhesion enhances the growth kinetics
- For a capillary viscous number higher than 1.64, the granule growth is controlled by the viscous dissipation forces

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