

## Supporting Information:

The effect of solvent on convectively-driven silica particle assembly: Decoupling surface tension, viscosity, and evaporation rate

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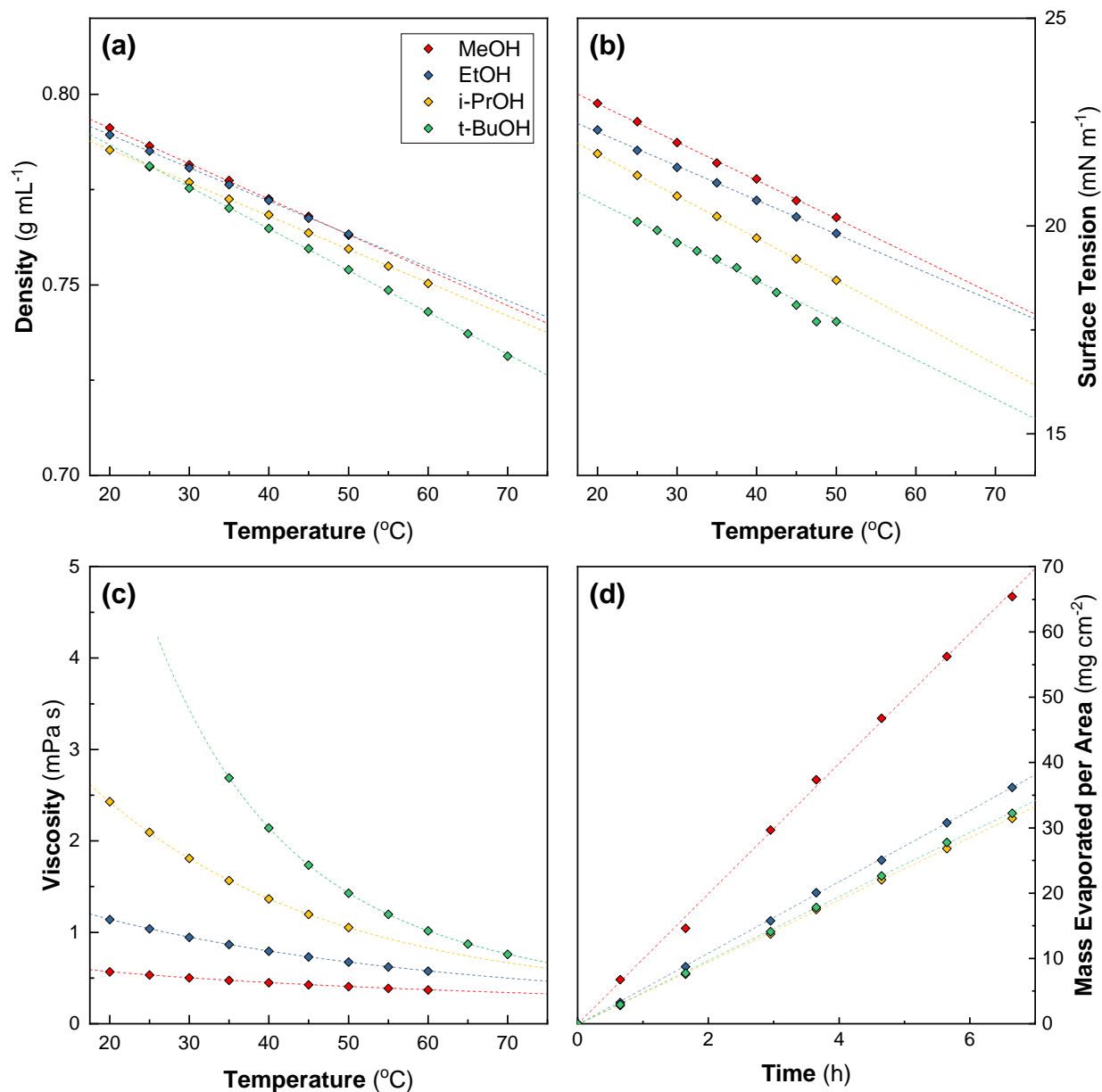
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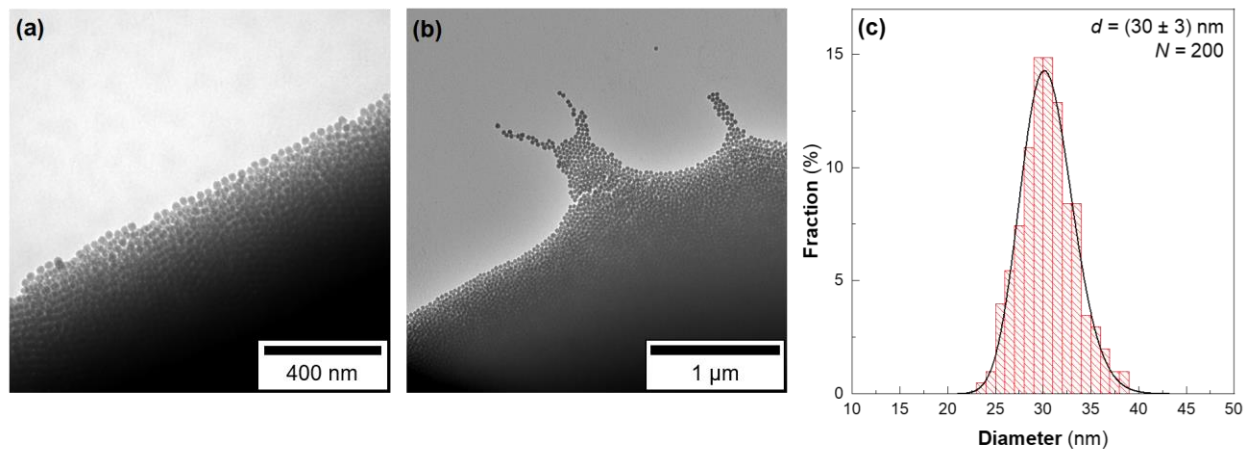
## Section S1. Physical properties of methanol, ethanol, isopropanol and t-butanol



**Figure S1.** (a) Experimental densities of alcohols used in this study as a function of temperature as taken from the literature.<sup>1-4</sup> The lines are linear fits. (b) Experimental surface tensions of alcohols used in this study as a function of temperature, taken from literature.<sup>5,6</sup> The lines are linear fits. (c) Experimental dynamic viscosities of alcohols used in this study as a function of temperature, taken from literature.<sup>2,7,8</sup> The lines are an exponential decay function fitted to the data. (d) Evaporative fluxes of MeOH, EtOH, i-PrOH, and t-BuOH at 50 °C. Evaporative fluxes were 33 mg h<sup>-1</sup> cm<sup>-2</sup> for MeOH, 18 mg h<sup>-1</sup> cm<sup>-2</sup> for EtOH, 16 mg h<sup>-1</sup> cm<sup>-2</sup> for i-PrOH, and 16 mg h<sup>-1</sup> cm<sup>-2</sup> for t-BuOH. The lines are linear fits.

## Section S2. SiO<sub>2</sub> seed particles (30 nm)

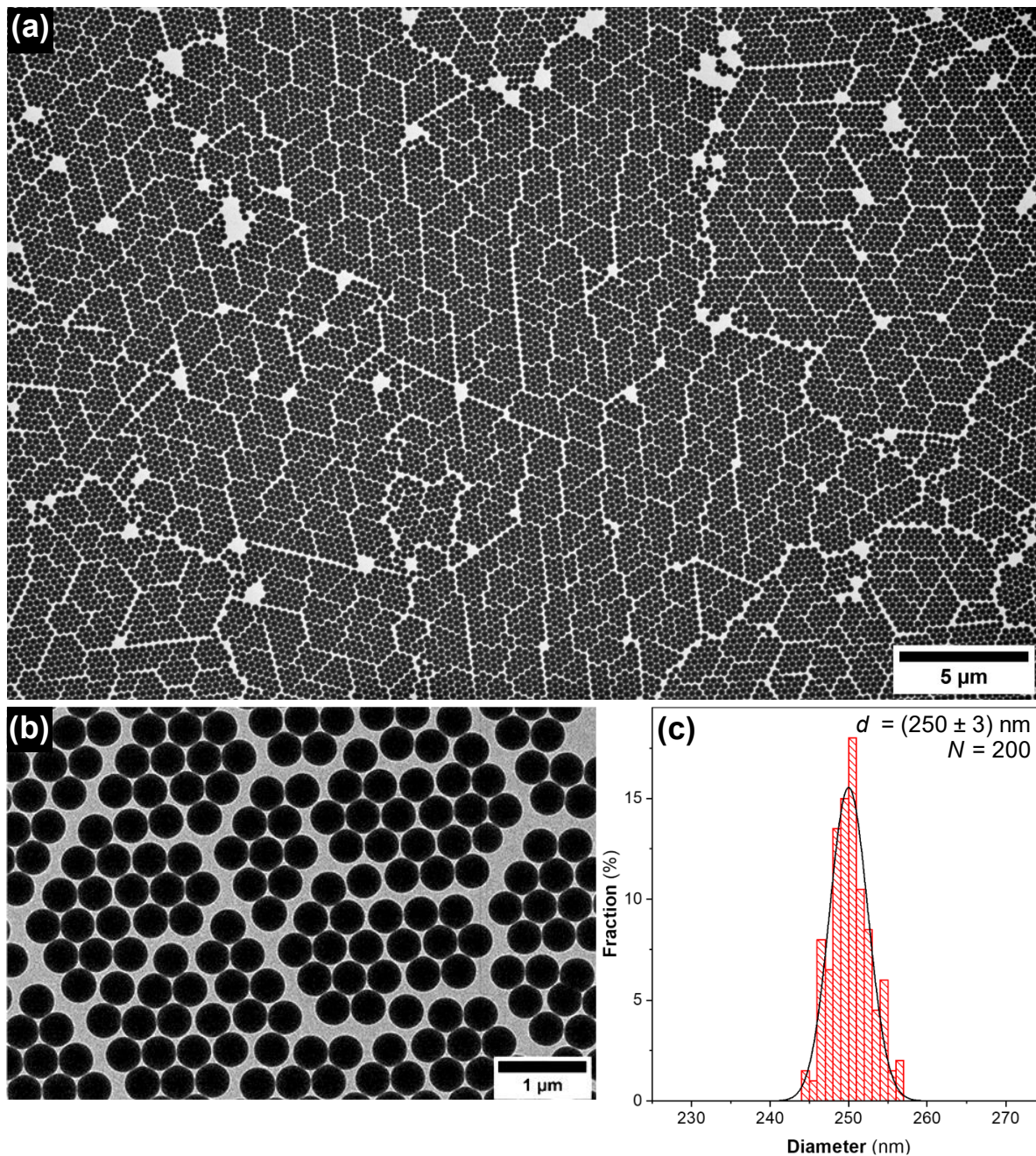
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**Figure S2.** (a & b) TEM micrographs of as-prepared SiO<sub>2</sub> seed particles (30 nm) used in this study. (c) Measured size distribution of the SiO<sub>2</sub> seed particles. Diameter,  $d$ , is given as  $(d \pm \sigma_d)$  nm.

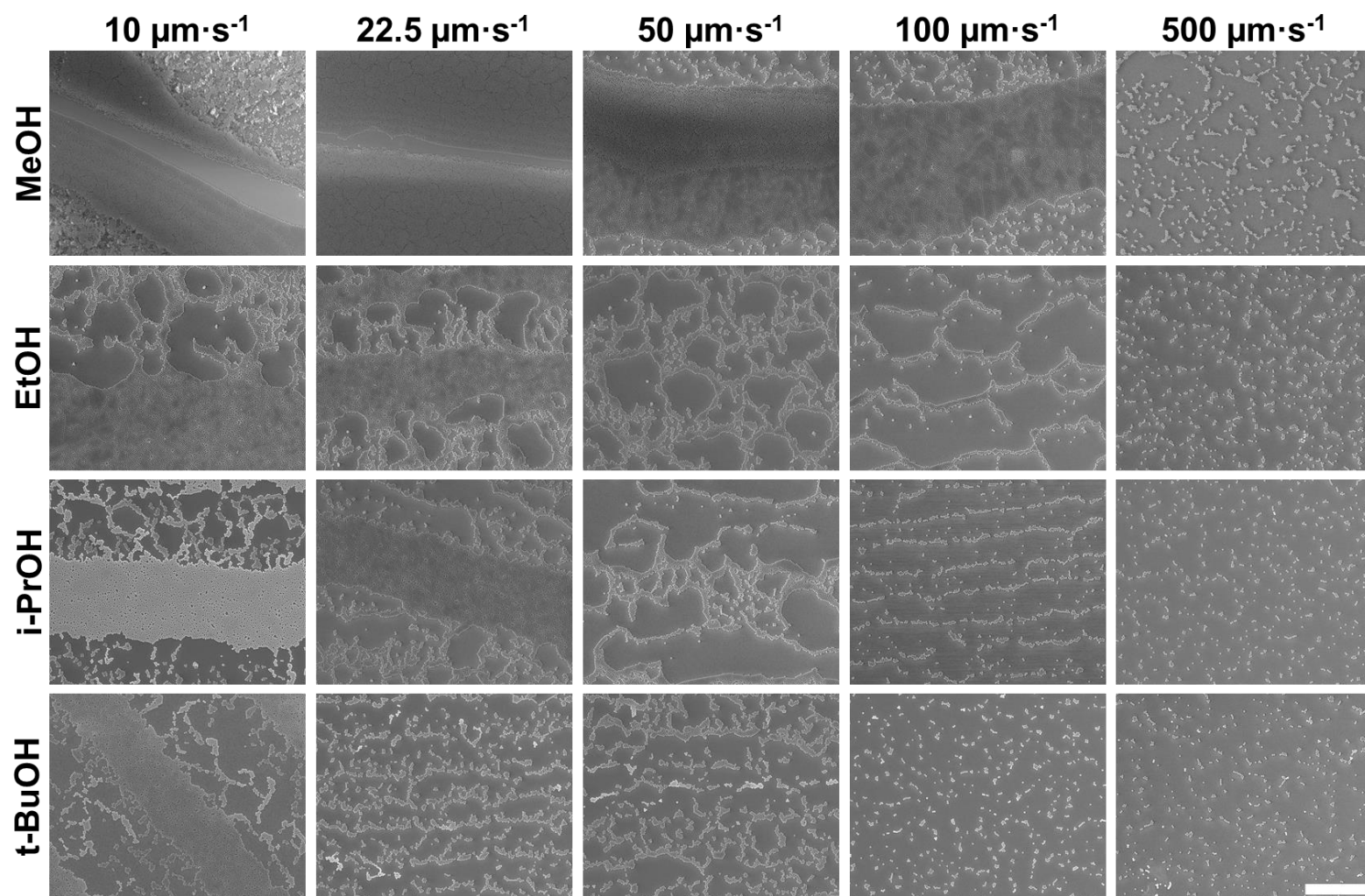
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### Section S3. Synthesis of SiO<sub>2</sub> particles (250 nm)



**Figure S3.** (a) Low magnification TEM micrograph (600×) of as-prepared SiO<sub>2</sub> particles (250 nm) used in this study. (b) Higher magnification TEM micrograph (6000×) of the same as-prepared SiO<sub>2</sub> particles. (c) Measured size distribution of the SiO<sub>2</sub> particles.

Section S4. Films drawn from alcohols with varying viscosity and withdrawal rate



**Figure S4.** Colloidal films prepared *via* dip-coating in different solvents at different withdrawal rates using 0.1 vol% 250 nm SiO<sub>2</sub> particles with a chamber temperature of 50 °C. All images were taken at the same magnification. The scale is the same for all images, the scale bar represents 10  $\mu\text{m}$ .

## Section S5. Normalizing withdrawal velocity for evaporative effects

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The surface coverage of a dip-coated film can be approximated by:<sup>9</sup>

$$S = c_1 L_c C a^{\frac{2}{3}} + c_2 L_c \frac{V_e}{V} \quad (\text{S1})$$

Where  $S$  is the surface coverage,  $c_1$  and  $c_2$  are constants,  $L_c$  is the capillary length,  $Ca$  is the capillary number,  $V_e$  is the evaporative flux, and  $V$  is the withdrawal velocity. In the convective regime  $c_1 L_c C a^{2/3} \ll c_2 L_c \frac{V_e}{V}$ , hence the contributions of the first term can be ignored, and the expression rearranged to:

$$\frac{S}{L_c V_e} = \frac{c_2}{V} \quad (\text{S2})$$

Which is constant for a fixed withdrawal velocity, hence for two solvents  $S_1$  and  $S_2$ :

$$\frac{S^{(S_1)}}{L_c^{(S_1)} V_e^{(S_1)}} = \frac{S^{(S_2)}}{L_c^{(S_2)} V_e^{(S_2)}} \quad (\text{S3})$$

If EtOH is selected as a reference solvent ( $S_2$ ), this can be rearranged to:

$$S^* = S \frac{L_c^{(\text{EtOH})} V_e^{(\text{EtOH})}}{L_c V_e} \quad (\text{S4})$$

Which gives the expected surface coverage when rescaled by the capillary length and evaporation rate of ethanol. Ethanol was arbitrarily chosen as the reference solvent, which changes the absolute magnitude, but not the relative magnitude of the rescaled surface coverage values. Any difference in the relative magnitudes of the surface coverage before and after rescaling would thus suggest that evaporative effects are responsible for the observed changes in surface coverage. We can insert this value into eq. S2 to derive a normalized withdrawal velocity,  $V^* = V \frac{L_c V_e}{L_c^{(\text{EtOH})} V_e^{(\text{EtOH})}}$ , which is rescaled to account for differences in evaporation rate.

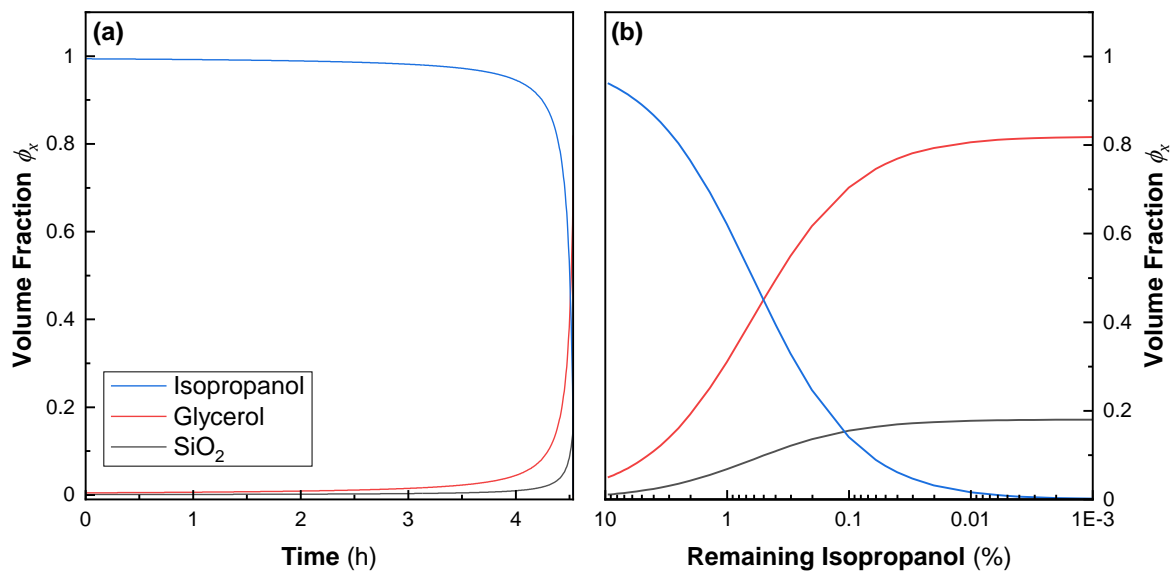
$$S^* = \frac{L_c^{(\text{EtOH})} V_e^{(\text{EtOH})}}{L_c V_e} \frac{c_2 L_c V_e}{V} = \frac{c_2 L_c V_e}{V^*} \quad (\text{S5})$$

## Section S6. Isopropanol/glycerol/silica composition evolution during evaporation

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**Table S1.** Composition of solutions used in the rheology measurements shown in Figures 3a, S5, and S6. All concentrations are expressed as volume fractions. Equivalent solutions contain the same ratio of glycerol to isopropanol as the isopropanol – glycerol – SiO<sub>2</sub> particle solutions to the right.

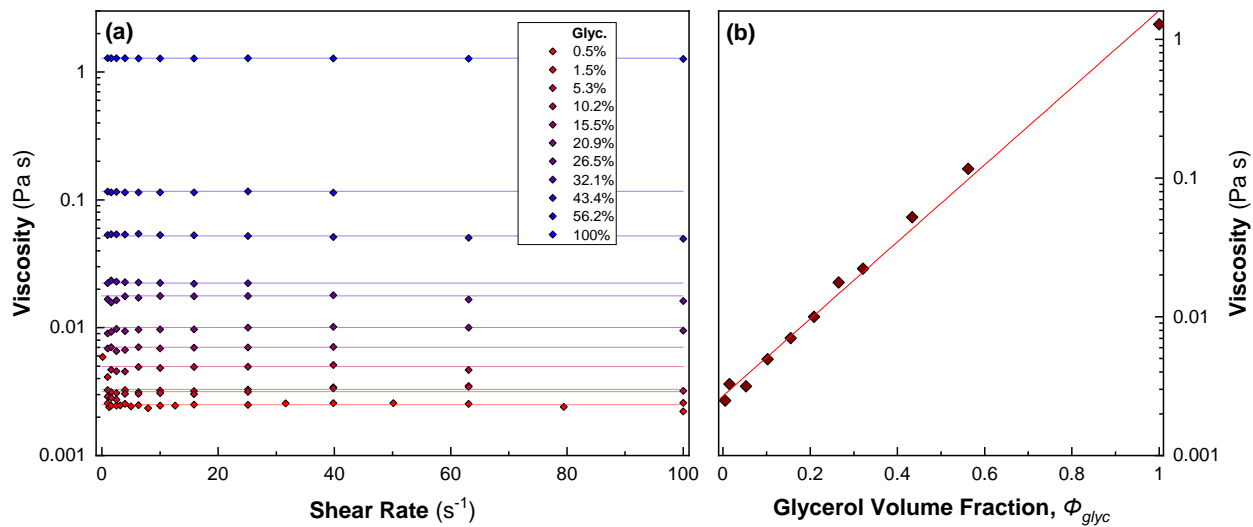
Isopropanol – Glycerol – SiO <sub>2</sub> solutions				Equivalent Isopropanol – Glycerol solutions	
<b>Glycerol</b>	<b>SiO<sub>2</sub></b>	<b>Isopropanol</b>		<b>Glycerol</b>	<b>Isopropanol</b>
$\phi_{\text{glyc}}$	$\phi_{\text{SiO}_2}$	$\phi_{\text{IPA}}$		$\phi_{\text{glyc}}$	$\phi_{\text{IPA}}$
--	--	--		0	1
0.005	0.0011	0.994	→	0.005	0.995
0.015	0.0033	0.982	→	0.015	0.985
0.05	0.011	0.939	→	0.053	0.947
0.1	0.022	0.878	→	0.102	0.898
0.15	0.033	0.817	→	0.159	0.841
0.2	0.044	0.756	→	0.209	0.791
0.25	0.055	0.695	→	0.269	0.731
0.3	0.066	0.634	→	0.321	0.679
0.4	0.088	0.512	→	0.434	0.566
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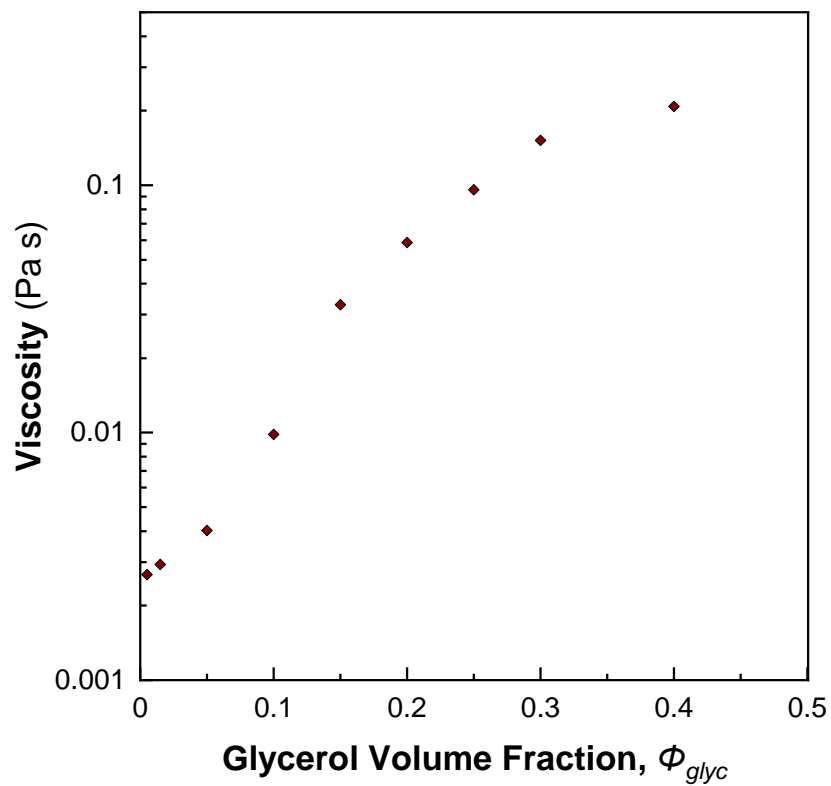
**Figure S5.** (a) Calculated volume fractions of isopropanol, glycerol and SiO<sub>2</sub> as a function of time during evaporation from a typical 6 mL cuvette used during dip coating. The evaporation rates used to calculate  $\phi_x$  were taken from a fit to the experimentally determined values in (a), the presence of the SiO<sub>2</sub> particles was assumed to not affect evaporation rate and the evaporation of glycerol was considered negligible. (b) The same data expressed as a function of the remaining isopropanol percentage.



## Section S7. Rheology of isopropanol – glycerol and isopropanol – glycerol-silica mixtures



**Figure S6.** (a) Dynamic viscosity of isopropanol – glycerol mixtures as a function of shear rate in the absence of  $SiO_2$  particles. The glycerol percentages selected correspond to concentrations seen in the solutions in Figure S7.



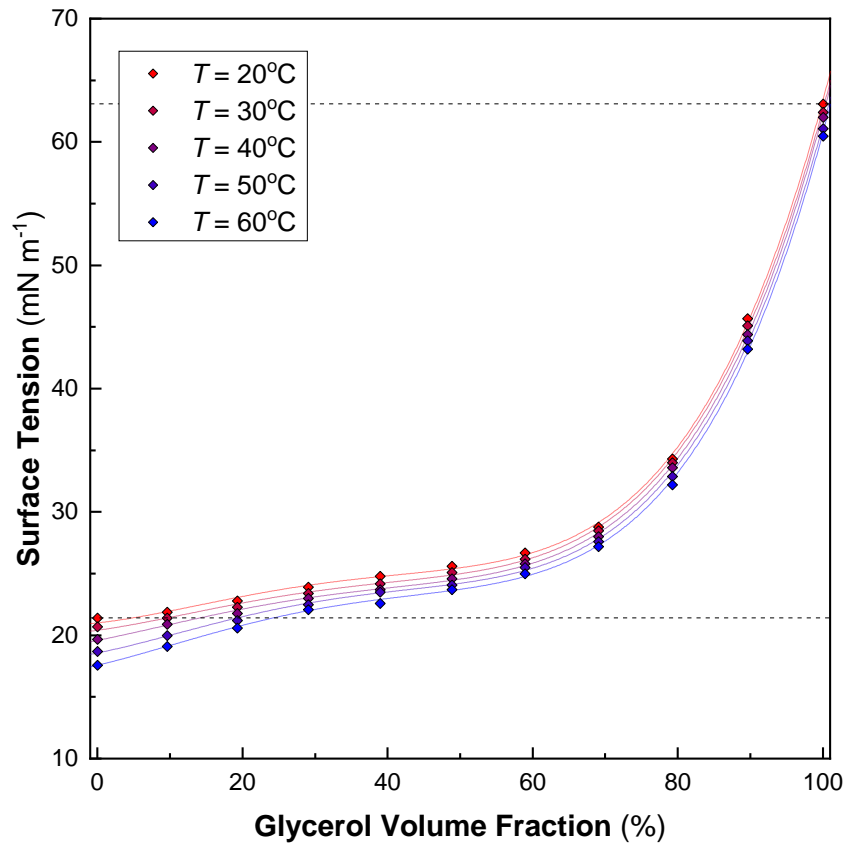
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**Figure S7.** Dynamic viscosity of isopropanol – glycerol – SiO<sub>2</sub> particle mixtures as a function of glycerol volume fraction,  $\phi_{glyc}$ . Because the solutions display shear-thinning, viscosities are given at a single shear rate of 26.83 s<sup>-1</sup>.

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## Section S8. Tensiometry of isopropanol – glycerol mixtures

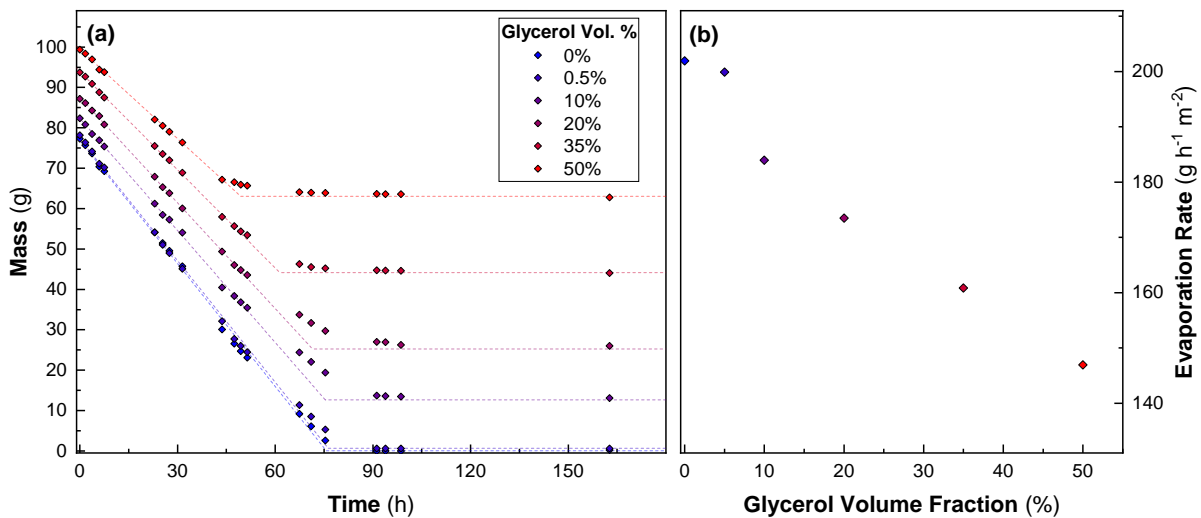
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**Figure S8.** Surface tension of isopropanol-glycerol mixes between 20-60 °C, values taken from the literature.<sup>10</sup>

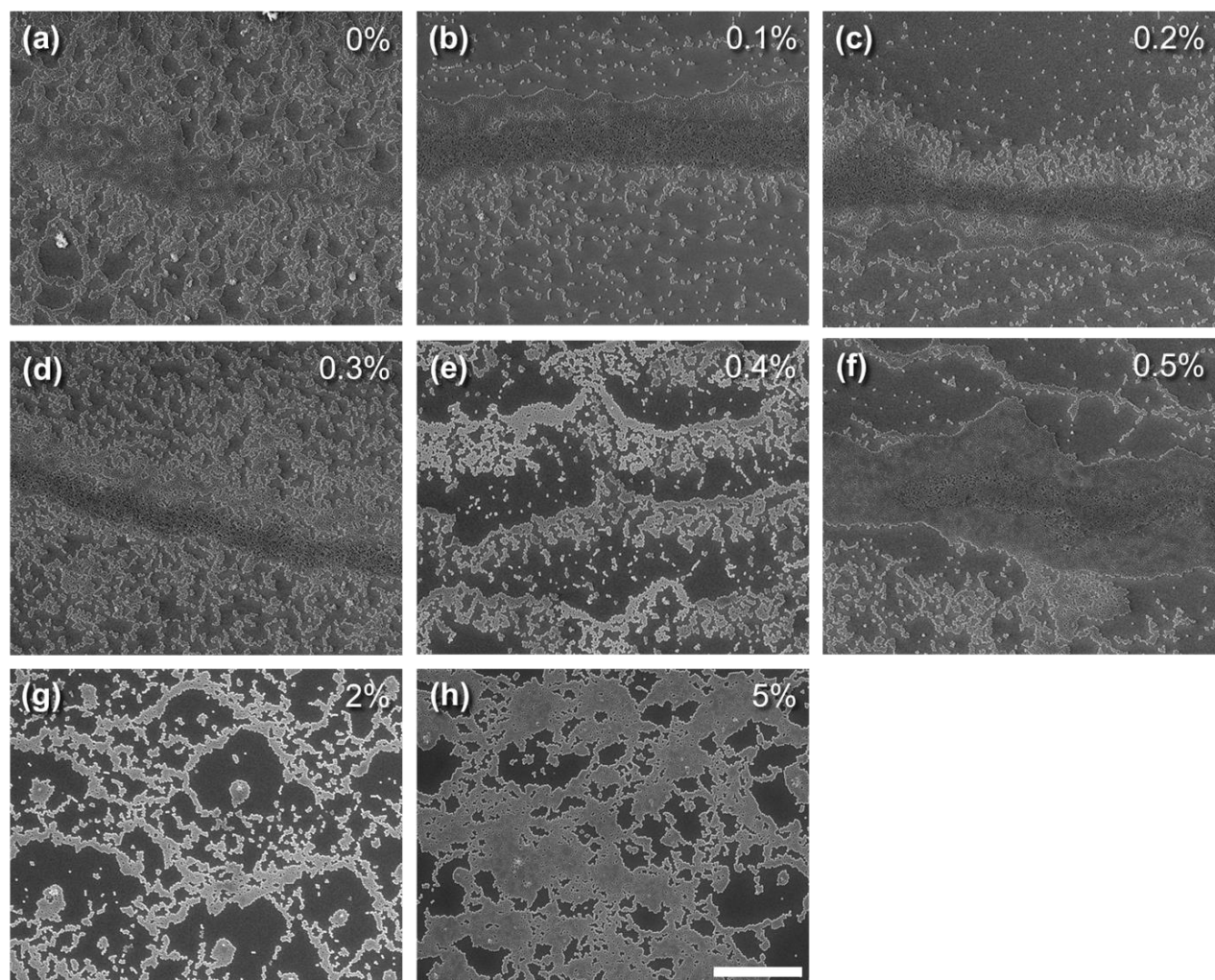
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**Figure S9.** (a) Mass evaporated over time for i-PrOH - glycerol mixtures at 50 °C. (b) Evaporative fluxes as measured from the initial linear section of each mass evaporation curve in (a) as a function of glycerol volume fraction.

## Section S9. Patterns of films deposited from a mixture of glycerol and i-PrOH

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**Figure S10.** SEM images of dip-coated films prepared at 50 °C, withdrawn at 50 μm s<sup>-1</sup>, using an initial concentration of 0.11 vol% SiO<sub>2</sub> particles and (a) 0, (b) 0.1 (c) 0.2, (d) 0.3, (e) 0.4, (f) 0.5, (g) 2 and (h) 5 vol% glycerol. All images have the same scale, the scale bar represents 10 μm.

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## References

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