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How chemical defects influence the charging of nanoporous carbon supercapacitors

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Ion desolvation and confinement are key physical processes in 1 porous-carbon based supercapacitors undergoing charging and dis-2 charging cycles. We investigate electrolyte interactions between po-3 larized porous carbon with subnanometer pore sizes and aqueous 4 sodium chloride electrolyte using molecular dynamics. Inspired by 5 recent first principles calculations, we developed a scheme account-6 ing for chemical defects in electrodes where only the non-sp2 carbons species carry an extra negative charge (on the anode) and an 8 extra positive charge (on the cathode) due to voltage polarization. 10 This drives electrolyte species (ions and solvent molecules ; water in this work) to adsorb at the electrode surface and in subnanomet-11 ric pores upon polarization. First we observe an asymmetrical des-12 olvation process of sodium and chloride ions at the external surface 13 of the electrodes. The ionic distribution at the external surface of 14 the electrodes is consistent with the Debye-Hückel electric potential 15 equation and empirical trends observed for non-porous electrodes. 16 In a second stage, we demonstrate that the nanoporosity of the elec-17 trodes is filled with ions and scarce water molecules and contributes 18 to about 20% of the overall capacitance. A fraction of desolvated ions 19 are irreversibly trapped in the core of electrodes during discharge. 20 While maintaining the overall electroneutrality of the simulation cell, 21 we found that anodes and cathodes do not carry the same amount of 22 23 ions at all time steps leading to charge imbalance.

Ionic adsorption | Molecular dynamics | dehydration

nderstanding ions in nano-confinement is the key element to get the fundamental physical basis of electrochemical 2 energy storage underlying modern electrochemistry devices 3 like batteries and supercapacitors (1, 2). In particular, fundamental understanding of the ionic adsorption processes and 5 confinement inside nanoporous carbon electrodes is essential 6 for predicting and improving the capacitance (3) or deion-7 isation efficiency of carbon-based devices (4, 5). Recent in 8 situ X-ray (6) and neutron scattering (7) have shown that 9 subnanometric pores of carbon electrodes enhance the ionic 10 adsorption and its overall capacitance performance (8). In 11 fact, if the pores are of the same size as electrolyte ions, high 12 capacitances (leading to the term supercapacitor) have been 13 observed that does not follow existing theories and empirical 14 trends (9-12). 15

The term of electrical double layer (EDL) capacitor comes 16 from the classical picture of non porous electrodes that accu-17 mulate oppositely charged ions at their vicinity upon voltage 18 polarisation in a mean-field dielectric continuum description 19 of the solvent populated with point charged ions at a given 20 concentration. This picture although very popular obviously 21 does not hold for porous electrodes with sub nanometric pores. 22 In particular, the mean-field Gouy–Chapman–Stern descrip-23 tion of a EDL fails in high molar concentrations and for pore 24

sizes smaller than a few nanometers (typically 4 nm for car-25 bon substrates) (13, 14). EDL predictions usually rely on 26 the Poisson-Boltzmann theory and modified versions such as 27 Debye-Hückel (15, 16) and Donnan models (17). More recent 28 approaches based on thermodynamics theory for heterogeneous 29 ionic fluids allow to take into account ionic size hence ionic 30 position correlations(18). Recently, this statistical physics 31 description of an EDL theoretical prediction was extended to 32 include time dependence and study the dynamics of the ionic 33 charging process of a planar electrode (19). 34

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Presently, there is no theory capable of solving the electrostatics problem for ions confined in the nanopores of a disordered porous carbon material commonly used in electrochemical devices. Nowadays, atomistic simulation techniques implement statistical physics methods that are able of describing both the intrinsic textural disorder of a porous carbon materials at the nanoscale and the movement of electrolyte species (solvent molecules and ions) in their pores under operational functioning conditions of a supercapacitor device (i.e. under polarization) (20–23).

There are currently two main approaches to describe atomic systems under polarization, the constant voltage (CV) and the constant charge (CC) methods. (i) The CV approach assumes a perfectly conducting substrate hence accumulating/depleting charges only on the atoms at the pore and external surfaces with no regards to the intrinsically defective nature of porous

Significance Statement

Nanoporous carbon texture makes fundamental understanding of the electrochemical processes challenging. Based on DFT results, the proposed atomistic approach takes into account topological and chemical defects of the electrodes and attributing them a partial charge that depends on the applied voltage. Using a realistic carbon nanotexture, a model is developed to simulate the ionic charge both at the surface and in the subnanometric pores of the electrodes of a supercapacitor. Before entering the smallest pores, ions dehydrate at the external surface of the electrodes leading to an asymmetric adsorption behavior. Ions in subnanometric pores are mostly fully dehydrated. The simulated capacitance is in qualitative agreement with experiments. Part of these ions remain irreversibly trapped upon discharge.

R.D, K.I, and R.P. designed, wrote the manuscript, discussed and analyzed the results, R.D. and P.-L. V. performed the calculations

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carbons (see Fig. 1(a)). Applied to porous carbon materi-51 als, the CV approach thus assumes that all carbon atoms 52 are in the sp2 hybridisation state, i.e. conducting electrons. 53 The main assumption of the CV method is, therefore, the 54 55 metallic approximation - the electrodes are considered ideal 56 conductors with no localisation of electric charge except at the material boundaries in contact with the electrolyte. In 57 recent simulation works(10), pore surfaces are treated as an 58 extension of the external electrode surface. It is important 59 to indicate that the charging process of substrate atoms is 60 in the order of fs while ion diffusion occurs at the scale of 61 ns (24, 25). Thus upon polarisation, the charges on the solid 62 matrix species attract ions first. Once equilibrium is reached, 63 thermal agitation of adsorbed ions can induce (in a constant 64 voltage description) charge fluctuation on electrode atoms that 65 in turn can redistribute ions in their vicinity. This is the main 66 advantage of the CV approach; its main drawback is that it 67 ignores charge localisation due to chemical heterogeneity. As 68 a result, within the CV approach, ion docking is only observed 69 at the external surfaces of the electrodes or in large nanopores; 70 the subnanopores being found not to participate to the ca-71 pacitance in sharp contract to experiment of activated carbon 72 based super-capacitors (see Fig. 1(b))(3). 73

(ii) The standard CC approach gives all substrate atoms 74 75 the same fixed charge. The main drawback of the CC approach 76 is that substrate charges are not allowed to fluctuate upon ion docking. Thus, this method only simulates the initial ion dock-77 ing dynamics before charge self-regulation takes place. In the 78 literature, it was reported that the CC approach may lead to 79 an unphysical temperature increase(26). In the supplementary 80 materials we give evidence that this issue might come from 81 the configurational setup of the simulation cell with bouncing 82 walls for ions in a rigid electrodes approximation. With a 83 full periodic cell simulating a stack of immersed electrodes. 84 using NVE simulation under polarization we found that the 85 86 temperature was well tempered (after initial relaxation at 87 300K). However, this leads to unphysical ion docking deep in the electrodes regardless the pore size (see Fig. 1(b)). In 88 sum, both the standard CC and CV methods fail for different 89 reasons hence, are not able to reliably simulate the adsorption 90 of ions in subnanoporous polarized electrodes (see Figs. 1(a, a)91 b)). 92

Therefore, we modified the CC method guided by ex-93 perimental and theoretical results showing the key role of 94 chemical defects and subnanopores in the building up of the 95 capacitance (9, 27-34). With this method, there is no ad-96 ditional computational cost compared to classical MD-CC 97 calculations. The local electrostatic field generated by the 98 matrix defects (in the present work non sp2-carbon atoms and 99 edge hydrogen species) drives ion adsorption on the electrode 100 external surface as well as in the whole porosity including the 101 subnanopores. Our electrodes are made of porous carbon tex-102 ture that is found to be realistic for charcoal, activated carbon 103 as well as for mature kerogen(35, 36). It was obtained using 104 Hybrid reverse Monte Carlo(37) with a density around 1g/cc. 105 Note that our activated carbon texture contains subnanomet-106 ric pores of 0.5-0.9nm (see Fig. 1(d). This sharply contrasts 107 from Carbide-Derived-Carbons (CDC) (38) previously used 108 in supercapacitor simulations that only contains pores above 109 1nm. 110

We propose a chemically driven charge localization model

(CDCL) that locates partial charges to defective species through the entire electrodes including species at the external or pore surface that are by nature defective. It takes advantage of both CC and CV methods while correcting their main drawbacks opening the path for modelling the adsorption of ions in subnanoporous defective electrodes including the role of doping of elements as such as N, S, F, etc.

We demonstrate that using MD simulations with the COM-119 PASS force field (39, 40) at 300K, the CDCL approach unravels 120 many subnanometric features underlying the physics of ion 121 docking in the charged electrodes ranging from the differenti-122 ated desolvation mechanism of cations with respect to anions 123 and their asymmetric adsorption/desorption mechanism inside 124 the nanopores. The pore size distribution shows a maximum 125 at 0.5-0.6 nm (Fig. 1(d)). Sodium and chloride ions can only 126 dock as single bare ions (i.e. unsolvated) in those pores. The 127 electrodes are separated by 30Å on both sides. The system is 128 periodic in all directions and it is initially prepared with 6100 129 water molecules, 60 sodium and 60 chloride ions in the inter-130 electrodes regions corresponding to a salt concentration of 0.67 131 mol/L (see Methods). As shown in Fig. 1(e), the texture of 132 the electrode near the ions contains defects (incomplete rings 133 or rings with 5 members). Fig.1(f) shows the ion density after 134 polarization and we can observe ion docking inside the porous 135 electrodes. 136

1. Results and discussion

In view of the limitations identified for the CC and the CV 138 method, we have chosen to develop the CDCL approach guided 139 by the chemical attributes of the electrodes. Our electrodes 140 are made of 70% sp2 carbon atoms i.e. having three carbon 141 neighbors as immediate neighbors with a typical angle between 142 consecutive carbon atoms around 120 degrees. The other 30% 143 of carbon atoms can be considered as defects where charges 144 are localised (an increase of partial charge for anode atoms, 145 a decrease for cathode species) (41) (see DFT calculations in 146 S.I.). 147

Upon polarization. DFT calculations show that excess 148 charges in absolute value are localized on the defects or 149 at their vicinity (30). Therefore, the CDCL scheme for 150 the attribution of additional charges consists in applying 151 a Δ_a value to the non-sp2 carbon atoms while attributing 152 a null charge to sp2 carbon atoms. The sp2 character is 153 hereafter determined based on the C-C-C angle between three 154 consecutive carbon atoms (see S.I.). For the sake of simplicity, 155 we assume the following linear formula for the excess charge 156 estimate: 157

$$\Delta_q = \Delta_{q,max} * (|(\Theta - \Theta_{max})|/10) \forall \Theta \in [\Theta_{max} - 10, \Theta_{max} + 10]$$

$$\Delta_q = \Delta_{q,max} \forall \Theta \notin [\Theta_{max} - 10, \Theta_{max} + 10]$$

[1] 159

where Θ_{max} is the value of the C-C-C angle in a perfect sp2 160 matrix (equal to 120 degrees) and $\Delta_{q,max}$ is the maximum 161 excess charge (positive for the anode and negative for the 162 cathode), which magnitude depends on the applied voltage. 163 We calculated that a value of +/- $\Delta_{q,max}$ =0.0337 e gives an 164 excess/deficit average charge on the anode/electrode of Δ_q 165 equals +/-0.02 e. In order to compare our results with results 166 obtained with the CV method, we have calculated a conver-167 sion factor by computing the average charge attributed to 168 the electrode atoms in the CV method. If we apply 1V, the 169

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Fig. 1. (a,b and c) Snapshots of the system showing ionic adsorption in different polarisation schemes upon steady state for the constant charge, the constant voltage and the chemistry driven charge localisation schemes respectively. (d) Pore size distribution of the electrodes. (e) structure of the local structure of the porous carbon electrode near adsorption sites. Colored surfaces are guides for the eyes to emphasizing the texture of the pores near the docked-ions. (f) density of Na (in blue) and Cl (in orange) for $\Delta_q = 0.02 e$ (1V) along the simulation cell axis, the two grey bands correspond to the electrodes position and thickness. (g) Calculation of the effective electrical potential acting on the ions in the solution for $\Delta_q = 0.02 e$ (1V). Effective potential acting on the ions in the simulation cell (in black). Due to the roughness, the position of the surface has to be defined arbitrarily, which has been done using the position of the most forward carbon atom of the electrode. Fit obtained using the Debye-Hückel formula (in red). The charge distribution follows a Debye-Hückel law due to the screening of the solution.

average excess/deficit charge is +/-0.02 e per carbon atom on
the anode/cathode respectively, which gives a voltage conversion factor of 0.02. In the CDCL approach, carbon defective
species have a nominative charge that reflects their local chemical environment and is in absolute value proportional to the
departure from the perfect sp2 state (equation 1) and the
applied voltage.

Recent CV atomistic simulations of CDCs carbon-based 177 porous structures have shown that solvated ions are adsorbed 178 in pores above 1nm in size; no fully dehydrated ions have been 179 observed implying that the subnanopores are still empty, in 180 agreement with what we observe in our CV simulations(42). 181 As demonstrated here below, it is important to note that the 182 CDCL approach is the only method that is able to predict at 183 the same time the adsorption of fully dehydrated ions inside 184 the subnanopores (less than 1 nm, Fig. 1(c)), partially or fully 185 hydrated ions on the external surface or in any other kind of 186 larger pores. All confinement environments were experimen-187 tally found to contribute to the overall capacitance of EDL 188 devices(2). 189

First, we investigate the adsorption of ions on the external 190 surface of the electrodes. The excess charge imposed additional 191 Coulombic forces on the ions of the system. The effective 192 voltage acting on the ions has been computed by extracting 193 the Coulombic forces on the ions with and without electric field 194 at the initial time of the simulation. The charge distribution, 195 in Fig. 1(g), shows that ions close to the external surface of the 196 electrodes are the ones experiencing larger attraction forces due 197

to the applied voltage compared to ions in bulk electrolyte away 198 from the electrode surface. Since it is related to a Coulombic 199 term, the force experienced by the ions is proportional to Δ_q 200 (see equation 1). The evolution of the effective potential is 201 characteristic of electrolyte solution and screening effect. Using 202 the Debye-Hückel formula (43), we can compare the Debye 203 length obtained from the simulation and that for a solution 204 with a uniform ion distribution for an ionic concentration 205 of $0.67 \text{ mol}.\text{L}^{-1}$ (corresponding to the salt concentration in 206 the inter-electrode void), with a dielectric constant of 80(44). 207 The agreement between the simulation and the Debye-Hückel 208 expression for the electric potential at the external surface 209 of the anode is remarkably good and gives a Debye length 210 around 0.2-0.3 nm in quantitative agreement with Debye length 211 obtained for this electrolyte type and concentration(44). 212

The number of effective ions adsorbed on and in both porous 213 electrodes is related to the capacitance of the system. The 214 capacitance has been calculated and is reported on Fig 2(a) for 215 each simulation with different Δ_q (the estimation of voltage is 216 given from the aforementioned conversion). There is a thresh-217 old at low voltage above which ions are being adsorbed on the 218 external surface of the electrodes (approximately $\Delta_a=0.0025$ 219 e corresponding to 0.125 V). For larger polarization voltages, 220 the amount of ions incorporated in the electrodes increases 221 quasi-linearly until it reached the maximum, hence, the capac-222 itance exhibits a peak shown in Fig. 2(a) in agreement with 223 the recent theoretical and simulation work of Verkholyak et 224 al.(45). Note that at voltages above about 1.8V, we consider 225

that the simulation is probably unrealistic since we do not 226 consider water splitting that happens at these voltages (46). 227 The capacitance is in agreement with the typical measured ca-228 pacitance of activated carbons (around 100 F/g with a specific 229 surface area at around 500 m^2/g for our carbon texture) (47). 230 The maximum capacitance we find, of about $20\mu F/cm^2$ is in 231 agreement with experimental values (2, 9, 10). Comparing the 232 results obtained with the CV and the CDCL on figure 2(a), we 233 can estimate that the contribution of the subnanopores to the 234 capacitance is about 20%, meaning that the supercapacitor 235 made of subnanoporous electrodes remains mostly a standard 236 EDL device with respect to aqueous electrolytes. 237

Due to the ionic docking in the subnanometric pores, the 238 capacitance estimated from the CDCL method is larger than 239 that the one obtained with the CV method (dots, see Fig. 2(a)). 240 There is a positive correlation between the capacitance and 241 the specific surface area as measured with BET experiments 242 (48). In fact the large value of the specific surface area reflects 243 both the amount of subnanopores and chemical defects on the 244 carbon backbone. Chloride and sodium contribute differently 245 to the capacitance (orange and blue dashed lines, see Figs. 246 247 2(a)). The adsorption sites are different due to the ionic size, as shown by the radial distribution function in Fig 2(b). 248 This leads to an asymmetric loading and charge unbalanced 249 electrodes, which is a direct consequence of the ion docking 250 into the subnanometric pores (while the simulation cell overall 251 charge remains neutral at all times in the simulation). The 252 capacitance being the sum of the charges divided to the voltage, 253 254 the peak can be explained with the less and less efficient ion docking upon voltage increase, this will be discussed hereafter. 255

In more detail, Figs. 3(a) and (b) show the number of 256 adsorbed ions on the surface, inside the subnanopores of the 257 electrodes during polarization simulations and the total ionic 258 loading during charge and discharge simulations with $\Delta_q =$ 259 0.01e (see S.I. video). At the voltage corresponding to the max-260 imum capacitance, the total adsorption is larger for Cl⁻ than 261 Na^+ . Comparing Figs. 3(a) and (b), one can see that Na^+ is 262 mostly adsorbed at the external surface whereas Cl⁻ is equally 263 adsorbed inside and at the external surface of the electrodes. 264 We observe that half of the sodium ions are adsorbed; the rest 265 remains in the solution in-between the electrodes. Similarly, 266 2/3 of the chloride ions are adsorbed and 1/3 remain in the 267 electrolyte solution. 268

Fig. 3(c) shows the number of adsorbed ions (i) on the sur-269 face, (ii) inside the nanopores and (iii) in total for different po-270 larizations. Cl⁻ ions are partially adsorbed on the surface and 271 inside the electrode nanopores following a monotonous increase 272 until $\Delta_q = 0.01e$ (0.5V) and then it reaches a plateau. Na⁺ is 273 adsorbed in larger quantity than Cl^- at voltages larger than 274 $\Delta_q = 0.01e$ (0.5V). Interestingly, as the voltage increases, we 275 observe a transition from an external surface adsorption only 276 (from $\Delta_q=0.0025e$ to $\Delta_q=0.01e$) to a dual inside-pore dock-277 ing/surface adsorption for the sodium ions above $\Delta_q = 0.01e$ 278 (0.5V). This is due to the fact that surface adsorption involves 279 hydrated ions whereas inside-pore docking involves bare ions. 280 Low voltages do not provide enough energy to loosen the hy-281 dration shell of Na⁺ leading to external surface adsorption of 282 hydrated ions (2). 283

The process of ion adsorption in nanopores is accompanied with a change in the solvation shell of the ions. In bulk water, sodium ions have a first solvation shell made of approximately 6



Fig. 2. (a) Capacitance due to sodium and chloride ions adsorbed inside and onto the electrodes at steady state with a maximum additional charge Δ_q (the added/subtracted charge is maximal on defective (non-sp2) sites). Note that the carbon atoms at the vicinity of the pores are not necessarily the non-sp2 carbons. The x-axis represents the excess of charge on each carbon atom of the positive electrode with respect to Δ_q . The dots correspond to the calculated value with the CV method. The simulated capacitance value is in the ball park of experimental values (100 F/g) for supercapacitors based on porous carbons with specific surface area around 500 m²/g (which is the value of our simulated porous carbon) (b) Radial distribution functions for C-Na and C-Cl distances at steady state for $\Delta_q = 0.01e$.

water molecules (49), which is also observed in our simulations before charging the electrodes. An ion and its first layer hydration shell are of about 0.7 nm in diameter and, therefore, can only access the largest pores in our system.

Fig. 3(d) shows the evolution of the hydration shells of the 291 adsorbed Na⁺ and Cl⁻ ions together with the total number of 292 adsorbed ions at $\Delta_q = 0.01e (0.5V)$. The adsorbed Na⁺ ions are 293 surrounded on average by 4-5 water molecules, whereas the 294 Cl⁻ ions carry 2-3 water molecules. All adsorbed ions have lost 295 either partially or totally their hydration shell, when adsorbed 296 on the surface of the electrodes, or their whole hydration shell 297 when entering the subnanopores. Fig. 3(e) shows the hydration 298 number of Cl⁻ ions before adsorption and after adsorption 299 inside the nanopores. The hydration shell becomes loose at 300 the surface and then the ions can enter either bare or with at 301 most one water molecule in the subnanopores. Note that we 302 observed the formation of anion-cation ionic pairs only in the 303 solution outside of the electrodes. 304



Fig. 3. (a) Evolution of the number of sodium ions in the electrode during the loading, adsorbed in the pore network (blue) or on the surface of the electrode (red) while imposing a voltage corresponding to a Δ_q =0.01e (0.5V) (total in black) and during unloading (in green) for Δ_q =0. To determine the adsorption, a cutoff of 4.0 Å and 5.0 Å have been used for Na-C and Cl-C distances respectively, corresponding to the first minimum in the radial distribution functions. (b) Evolution of the number of chloride ions in the electrode. (c) Number of (blue) sodium ions and (orange) chloride ions adsorbed (diamond) in total, (squares) inside the electrodes, (circles) at the surface. (d) Evolution of the surface (d) Evolution of the standard deviation. Evolution of the quantity of adsorbed Na (blue) and Cl(orange). (e) Hydration number of several ions versus Δ time (each color corresponds to a different Na⁺ ion), where Δ time is the time difference to the moment where the ion enters into the electrode. The values reported are the running average over 100 steps.

Focusing now on the role of water in porous electrodes at full saturation, we observed that in polarized electrodes that few water molecules adsorb in the pores of the electrodes (50). The ratio for the amount of water inside the electrode is less than 15%. The carbon structure is rather hydrophobic as indicated by radial distribution functions (shown in S.I.), the shortest C-water distance being about 3.5 Å.

Corrected for the effective accessible pore volume, the sub-312 nanopores are just large enough to accommodate one bare ion 313 314 (diameter for sodium and chloride equal 0.1nm and 0.18nm) respectively) in agreement with the conclusions of Simon and 315 Gogotsi(2). While the electrodes are being charged, the den-316 sity of water inside the electrodes slightly increases. This 317 indicates that the adsorption of ions into the carbon electrodes 318 make the structure less hydrophobic in a similar fashion as 319 the clay interlayer void is hydrophilic only because the pres-320 ence of cations compensating the overall clay layer negative 321 charge. The clay basal planes per se are rather hydrophobic 322

as they carry no OH surface groups immediately in contact with adsorbed water; the ions act as water pump inside a polarized porous carbons or in-between clay layers charged through isomorphic substitutions (51).

Regarding the desorption process, the ions that are ad-333 sorbed deep in the core of the electrode will more likely remain 334 trapped upon discharge. At voltage set back to zero, about 335 10% of the formerly docked Na⁺ ions (about 3% of the to-336 tal number of cations) and 30% of the adsorbed Cl⁻ (about 337 10% of the total number of anions) are still trapped inside 338 the electrodes (after 1 ns of unloading, 2 Na^+ and 6 Cl^- are 339 inside the electrodes, see S.I.). Note that desorption, which is 340

simulated under a null voltage, takes place over a longer time 341 than ion docking (see Figs. 3(a and b)). The trapped ions may 342 not participate to the current unloading cycle but they could 343 move to a nearby pore during the cycling and become again 344 345 available for storage. The trapped ions upon depolarization 346 is compatible with the hysteretic behavior observed in the supercapacitor I-V characteristic curve. More specifically, the 347 ions that are being desorbed at zero voltage are only the ions 348 that have an easy path to exit the porous material. Other 349 ions, that are in small pores or in tortuous porous network, 350 are not easily extracted from the media. Being smaller ion, 351 Na⁺ is often trapped more deeply in the porous network at 352 larger voltages. Three adsorption/desorption cycles has been 353 performed in this work and we have observed that after the 354 first cycle, the amount of ions irreversibly docked inside the 355 electrode nanoporosity remains constant. 356

2. Conclusion 357

We propose a new approach to describe the charge and dis-358 charge process in subnanoporous carbon made electrodes, in a 359 supercapacitor setting, that we call chemically driven charge 360 localisation model (CDCL). Despite its mean-field charac-361 ter, the CDCL approach is an improvement of the current 362 standard methods to simulate charged devices at the atomic 363 scale, namely the constant charge and the constant voltage 364 methods that are ineffective to correctly describe ionic dock-365 ing in subnanopores. Informed from DFT calculations, the 366 CDCL method consists in localising charges on defective non-367 sp2 carbon sites, including chemical or topological defects. 368 By contrast to the standard methods, this allows simulat-369 ing both adsorption on the electrodes external surfaces and 370 371 in-subnanopore docking.

Applied to a realistic texture of nanoporous carbon, we 372 could unravel the fundamental processes underlying the capac-373 itive effect of a subnanoporous carbon-based supercapacitor 374 device in operation. We show in particular that subnanomet-375 ric pores constitute about 20% of the capacitance of such a 376 device using a standard aqueous electrolyte. The simulated 377 value of the capacitance of about 100 F/g (or 20 μ F/cm²) 378 is in good agreement with the experimental values measured 379 on activated carbon based supercapacitors. In more details, 380 we show that the docking of ions in pores is preceded by an 381 assymptical desolvation at the vicinity of the external pore 382 surface. The ion adsorption density profile on the electrodes 383 external surfaces is in agreement with the Debye-Hückel theory 384 with a Debye length of 0.2-0.3nm. The desolvation process 385 is actually different for sodium and for chloride ions as the 386 hydration shell of sodium is tighter than that of chloride. Once 387 ions are desolvated, they can access nanopores; subnanopores 388 being mostly populated with bare ions in agreement with in 389 situ X-rays experiments (6). Due to the difference in their 390 ionic size, the docking mechanism of sodium and chloride ions, 391 leads to an unbalanced electrode charging. Upon discharge, we 392 found that a significant amount of ions (10%) of the cations and 393 30% of the anions) remains trapped in the subnanopores due 394 to the pore network tortuosity right after the first charge that 395 is compatible with the typical I-V curve of supercapacitors. 396

The current CDCL method allows exploring how doping 397 with elements such as N, S, etc. influence the ion adsorption 398 and the in-pore docking (54). Furthermore, the current CDCL 39 method could be coupled with a constant voltage approach in 400

order to take into account the variation of the substrate defects 401 charge upon ionic thermal movement. This will allow studying 402 the ageing of the electrodes texture upon charge-discharge 403 cycling.

3. Methods

A super-capacitor composed by porous carbon layers (of 22Å thick-406 ness), separated with a water solution containing electrolytes, has 407 been simulated with a fully atomistic approach. The electrodes has 408 been generated using a liquid quench MD method (55) using the 409 reactive force field ReaxFF (56) to obtain a micro-porous carbon 410 containing hydrogen (0.3 H/C). The charges due to defects in the 411 carbon structure are compensated by H atoms. This structure has 412 been relaxed at 293 K and 1 atm, then, cut in half in order to add 413 a phase of bulk of water replacing the other half. The cut leads 414 to unstable atoms at the interface due to broken bonds. Thus, we 415 performed a relaxation with an MD run at a higher temperature 416 (1500 K) to force water molecules to react with the unstable carbon 417 atoms, stabilize the structure and diffuse within the structure. Then, 418 we have duplicated the system one time toward the orthogonal di-419 rection of the cut surface. Each electrode contains 5440 atoms. It 420 has a connected pore network and a density of 1.45 g.cm^{-3} . 421

In order to study the charge of the capacitor with ions we have 422 built a model in which pure water solution has been enriched with 423 60 Na^+ and 60 Cl^- ions. We have investigated the adsorption of 424 the ions in the porous carbon structure that has been described 425 previously. Since ReaxFF is not well suited for simulating systems 426 with electric fields, the potential used for the charge and discharge 427 simulations is the COMPASS potential (39, 40) to describe the 428 electrodes-water interactions and the SPC/E (57) potential to de-429 scribe water molecule interactions which is well-known for it's good 430 description of polar liquids. The interactions cutoff has been set to 431 12Å. In this work, considering the complexity of the electrodes and 432 therefore of finding a relevant force field to simulate the motion of 433 the atoms of the electrodes, the electrodes were kept rigid. This is 434 an approximation that could slightly influence the quantity of ions 435 that can be adsorbed (in a flexible system, one can imagine that 436 the pores will slightly adapt to the presence of ions). In further 437 studies, the use of reactive force fields such as ReaxFF should be 438 considered in order to assess the stability of the structure and the 439 durability of the pore network due to the ion adsorption. Since 440 such a reactive potential relies on the calculation of charges at each 441 step of the dynamics, the CDCL method should be implemented 442 as a post-calculation to add the charge excess/deficit after the 443 electronegativity equalization method algorithm. 444

Ewald summation has been used for the long range interactions. The PPPM scheme, which is well suited for large systems (in this work over 30 000 atoms), as implemented in LAMMPS has been used with a threshold on the forces of 10^{-4} . Periodic boundary conditions have been imposed to the simulation cell. The electrodes are symmetrical and the simulation cell is electroneutral.

For the dynamics, we have used a time step of 0.2 fs, in agreement with the frequency of the O-H stretching modes in water. The system has been thermostated using Nosé-Hoover thermostats. Before adding the electric field, the system has been equilibrated during 300ps at 300K. As discussed in S.I., we have not observed any increase of temperature under electric field contrarily to the results published in a recent work by Merlet et al. (26) the authors attribute to a macroscopic dipole moment, which is an artifact of the simulation.

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