

Finite Element Solver for Thermo-Hydraulic Optimization of Architected Ceramics (NExT I-Site industrial partnership program: OPTHOCERA): project overview

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September 27-30, 2022 Albuquerque, NM, USA

28th SolarPACES Conference

Decarbonization of high-temperature industrial processes (T> 1,000°C)

- Stabilization of global warming¹→net-zero emission of CO₂ in human activities (industry, transpoirt, residential sector...)
- Industry accounts for 32 % of the final energy consumption with 74 % of this component is required for heat production of which 90 % is provided by burning fossil combustible (coal, oil, gas)
- 48 % of energy consumption for producing industrial heat is due to high-temperature processes (T > 400°C)



Production of fuels and chemical commodities



Zimmermann in Ullmann's Encyclopedia of Industrial Chemistry, Wiley-VCH, Weinheim, Germany, 2009



Metallurgical sector

¹⁾ Masson-Delmotte et al., In: Climate Change 2021 Contribution of Working Group I to the Sixth Assessment Report of the Intergovernmental Panel on Climate Change.

Interest of high-temperature concentrated solar heat

- Solar energy →abundant : 1% of the 3.8×10²⁴ joules of solar energy reaching the earth's surface every year → 40 times the electricity generated globally
- But dilute, geographically non uniform, temporally intermittent, variable
- Concentration²⁾ of solar radiation (paraboloid dishes and solar towers) →1,000°C (with incident fluxes > 1MW/m²)





 Development of high-temperature solar receivers with high solar-to-heat conversion efficiency and service life of 10,000 cycles under harsh conditions → thermal, mechanical, material challenges

²⁾ Romero, M., Steinfeld, A., 2012. Concentrating solar thermal power and thermochemical fuels. Energy Environ. Sci. 5, 9234–9245

Volumetric solar receivers = radiative-convective heat exchangers



Avila-Marin et al., Renewable and Sustainable Energy Reviews, 2019, 111 15

Conventional 3D geometries

Refractory porous ceramics (SiC, Al₂O₃,...)

- High solar absorptance
- Good thermal conductivity
- High volumetric surface
- Low thermal emittance
- High thermal shock resistance

New concepts based on additive manufacturing coupled with radiative transfer design → Improvement of the volume propagation of concentrated solar light, reduction of thermal emission

150 mm



Numerical design approach coupled with additive manufacturing



HEM : Homogeneous Equivalent Method \rightarrow continuous scale approach DS : Detailed Simulation \rightarrow pore scale approach

OPTHOCERA program (1 year)





Numerical design of 3D digitalized porous architectures (regular, pore size gradient) Conductiveradiative modelling→Temper ature and flux fields (HEM and DS)

Selected architectures according to Planck number → elaboration by stereolithography



Performance tests : solar-to-heat conversion (OPTISOL bench, PROMES Odeillo, France).



Radiative Transfer Equation : modelling of volume propagation of thermal and solar radiations

- Macro-porous ceramics \rightarrow semi-transparent media (absorption, scattering, emission)
- Valid if the medium is homogeneous, continous and weakly spatially correlated



 $\widehat{\Omega}. \nabla I_{\nu}(s, \widehat{\Omega}) + (\kappa_a + \kappa_s) - \kappa_s \int_{4\pi} I_{\nu}(s, \widehat{\Omega}) P(\widehat{\Omega}' \to \widehat{\Omega}) d\widehat{\Omega}' - \kappa_a I_{P\nu} = 0$



Chandrasekhar, Radiative Transfer, Dover, 1960

$$\nabla . \dot{q}''(s) = \int_{0}^{\infty} \kappa_{av} 4\pi I_{bv}(T) dv - \int_{0}^{\infty} \int_{4\pi} \kappa_{av} I_{v}(s, \hat{\Omega}) d\Omega dv$$

$$\rho c_{p} \frac{\partial T}{\partial t}(s) = \nabla . (k_{cond} \nabla T(s) - \dot{q}''(s))$$

Methods for solving the steady-state RTE



Use of the FEM solver for analyzing the coupling between conduction and radiation within a 1D slab sandwiched by a hot and a cold wall



Comparison between HEM model/exact solution from Viskanta





- $\tau = 0.9 (+36 \%)$
- ightarrow @T=700 K , + 252 K
- low κ_e : for a given p, high d_{nom} (low PPI)



Typical values of *N* for real ceramic-based open cell foams (T=1,300 K)

0,000	size =	size =	size =	size =	80 %, cell size =	@1000°C	material
0.02456	4mm 0.04913	0.09826	0.04913	0.09826	0.19652	~6.8	alumina
0,01156	0,02312	0,04624	0,02312	0,04624	0,09248	~3.2	mullite
0,00542	0,01084	0,02167	0,01084	0,02167	0,04335	~1.5	cordierite
0,18062	0,36124	0,72249	0,36124	0,72249	1,44497	~50	silicon carbide
	size = <u>4mm</u> 0,04913 0,02312 0,01084 0,36124	size = 2mm 0,09826 0,04624 0,02167 0,72249	size = 8mm 0,04913 0,02312 0,01084 0,36124	size = 4mm 0,09826 0,04624 0,02167 0,72249	size = 2mm 0,19652 0,09248 0,04335 1,44497	@1000°C [W/(m.K)] ~6.8 ~3.2 ~1.5 ~50	alumina mullite cordierite silicon carbide

Interest for semi-transparent porous ceramics with high p and high d_{nom}

Comparison of the Rosseland↔HEM model and of the HEM↔DS model



331 860 tetrahedral elements for the solid phase and 1 753 680 elements for the fluid phase ; 62 processors, 128 directions

Thermal behaviour of 4 fictitious alumina-based Kelvin Cell Foams exposed to a collimated concentrated solar beam (10⁶ W.m²)



Porosity = 91 %, \emptyset = 5 cm, h= 5 cm	
--	--

	d _{nom} =0,004 m without coating Case 1	d _{nom} =0,008 m without coating Case 2	d _{nom} =0,004 m with coating Case 3	d _{nom} =0,008 m with coating Case 4
$eta_{eff}(m^{-1})$	108	54	108	54
κ_{eff} (m ⁻¹)	33.7	12,7	79	33
σ_{eff} (m ⁻¹)	74.3	41.3	29	21
E _{eff}	0.31	0.24	0.73	0.61
λ_{eff} (W.m ⁻¹ .K ⁻¹)	0,33	0,33	0,33	0,33
$N_{P,\beta_{eff}}$	0,04422	0,02211	0,04422	0,02211
ω_{eff}	0.67	0.76	0.27	0.39
$ ho_{eff}$ (kg.m³)	330	330	330	330
$C_{P,eff}$ (J. Kg ⁻¹ K ⁻¹)	1200	1200	1200	1200
$h_{x_{min}} = 10h_{x_{max}}$ (W. m ⁻² .K ⁻¹)	10	10	10	10

Addition of an absorbing coating on the alumina ligaments

Thermal behaviour of porous alumina ceramics exposed to a collimated concentrated solar beam (10⁶ W.m²)



Mora Monteros et al., Ceramics International 46 (2020) 2805-2815

ceramics exposed to artificial concentrated

 $N_{P,\beta_{eff}}(1,3) = 2N_{P,\beta_{eff}}(2,4) \rightarrow$ volume radiation effect more important $\omega_{eff}(1,2) < \omega_{eff}(3,4) \rightarrow$ volume radiation effect more important $\varepsilon_{eff}(1,2) < \varepsilon_{eff}(3,4) \rightarrow$ decreasing of the radiative losses at the front face

From the numerical design of porous ceramics up to elaboration thanks to stereolithography



Improvement of the solar absorptance of the alumina skeleton with a commercial refractory black coating



Numerical computations of the Kelvin cell foams emissivities with genMat



Parallelized Monte Carlo Ray-Tracing code

Absorption length of the incident collimated beam : effect of d_{nom}



Impact d_{nom} on the absorption of the incident radiative flux and the position of T_{max}

2000



Radiation transport is stopped at the first rank of cell : after conductive (convective) heat transfer

Solar-to-heat performances : OPTISOL bench





Mey-Cloutier et al., Solar Energy 136 (2016) 226-235

Qualitative agreement but some experiments must still be explained

$$\begin{split} \eta_{ST,1} &< \eta_{ST,2} \leftrightarrow N_{P,\beta_{eff},1} > N_{P,\beta_{eff},2} \\ \eta_{ST,4} &< \eta_{ST,3} \text{ but } N_{P,\beta_{eff},3} > N_{P,\beta_{eff},4} \end{split}$$

 $\eta_{ST,4} < \eta_{ST,3} \leftrightarrow \omega_{eff,3} < \omega_{eff,4}$

Modification of the front face for case 4 ? Heat exchange coefficient?

d _{nom} =0,004 m without coating					
: case 1					
DNI	q air	T out	η_{ST}		
(W/m²)	(g/s)	(° C)			
1017	3	219	0,39		
1020	2	270	0,33		
1022	1	387	0,24		
d_{not}	m=0,004 m	i with coat	ing		
	: ca	se 3			
DNI	q air	T out	η_{ST}		
(W/m²)	(g/s)	(° C)			
1014	3	423	0,82		
1024	2	574	0,75		
1014	1	838	0,57		
d_{nom} =0,008 m without coating					
: case 2					
DNI	q air	T out	η_{ST}		
(W/m²)	(g/s)	(° C)			
1027	3	307	0,56		
1028	2	368	0,46		
1024	1	490	0,32		
d_{nom} =0,008 m with coating :					
case 4					
DNI	q air	T out	η_{ST}		
(W/m²)	(g/s)	(° C)			
1022	3	382	0,72		
1034	2	507	0,64		
1034	1	731	0,48		

Experimental data

$$\begin{split} N_{P,\beta_{eff}} &= 0.04422\\ \omega_{eff} &= 0.67 \end{split}$$

 $N_{P,\beta_{eff}} = 0,04422$ $\omega_{eff} = 0.27$

 $N_{P,\beta_{eff}} = 0,02211$ $\omega_{eff} = 0.76$

$$\begin{split} N_{P,\beta_{eff}} &= 0.02211\\ \omega_{eff} &= 0.39 \end{split}$$

Conduction-toradiation number



Conclusions & outlook

- Fast and robust FEM solver for conduction-radiation heat exchange modelling through HEM and DS method
- Validation of HEM-DS ↔ Viskanta model (hot and black wall) for a porous structure with a regular lattice (cubic cells)
- Volume propagation of radiation locally increases $T \rightarrow$ interest for developing VSR
- Numerical design and elaboration of 4 based-alumina VSR (\emptyset = 5 cm, h= 5 cm) with stereolitography
- Performance tests with the OPTISOL bench
- Best VSR : porosity 91 %, nominal pore diameter 4 mm with a coating of high solar absorptance
- Planck number not sufficient for following volume propagation within VSR : need to introduce a trapping effect number.

	International Journal of Heat and Mass Transfer 197 (2022) 123274	_	Velocity_3D U_exact
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Finite eleme within heter S. Ouchtout, B. Nantes Université, CNRS, I	ent framework for modeling conducto-radiative transfers rogeneous media at both discrete and continuous scales Rousseau, Y. Favennec ⁴ aboracoire de thermique et finergie de Nautes ITEN, UMR 6607, Nautes F-44000, France	Chaos for spitial	Market and the second sec

- Coupling with fluid transport (Darcy-Forchheimer HEM/ Navier-Stokes DS) \rightarrow ANCRE SdBE FATHERCASE program (2022-2023) with IFPEN and GeM
- PRC ANR ORCHESTRA (2022-2026) with LTeN-GeM-IFPEN-IRCER
- Topology optimization \rightarrow
- Thermal shock resistance modelling
- Elaboration of SiC lattice with binder jetting...



Thank you for your attention ! benoit.rousseau@univ-nantes.fr



Influence of the anisotropy factor

From macro-scale to meso-scale





S. Guévelou et al., Journal of Quantitative Spectroscopy and Radiative Transfer, 2017, 189, 329-338



Influence of the albedo



