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Delphine Doppler, Philippe Gondret, Thomas Loiseleux, Sam Meyer, M Rabaud. Relaxation dynamics of water-immersed granular avalanches. *Journal of Fluid Mechanics*, 2007, 577, pp.161-181. 10.1017/S0022112007004697 . hal-03865190

HAL Id: hal-03865190

<https://hal.science/hal-03865190>

Submitted on 14 Mar 2024

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Relaxation dynamics of water immersed granular avalanches

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(Received 20 October 2006 and in revised form ??)

We study water immersed granular avalanches in a long rectangular cell of small thickness. By video means, both the angle of the granular pile and the in-depth velocity profiles of the grains are recorded as a function of time. These measurements give access to the instantaneous granular flux. By inclining the pile at initial angles larger than the maximum angle of stability, avalanches are triggered and last for long time, up to several hours for small grains, during which both the slope angle and the granular flux relax slowly. We show that the relaxation is quasi-steady so that no inertia is to be considered: the relaxation at a given time is only controlled by the slope angle at this time. This allows us to adapt a frictional model developed recently for stationary conditions in either dry or water immersed granular flows. This model succeeds well in reproducing our unsteady avalanche flows, namely the flowing layer thickness, the granular flux and the time relaxation of the slope. When a water counter-flow is applied along the pile, the granular avalanches are slowed down and behave as if granular friction was increased

by an amount proportional to the water flow. All these findings are also well reproduced with the same friction model by taking into account the additional fluid force.

1. Introduction

If the flow equations for simple fluids are known for more than one century, this is not true for granular matter. This is why many experimental studies similar to those imagined in the past for water flows have been conducted these last years together with numerical studies in order to get insights and validate the different proposed theoretical approaches. Granular flow may sometimes resemble the one of a liquid but its detailed behaviour is much more complex, in particular the hysteretic behaviour that leads granular matter to switch from static to flowing state and vice versa.

A good knowledge of granular avalanche flows appears to be crucial in a large number of industrial and environmental problems. In all these practical configurations, the interstitial fluid can be a gas or a liquid. The influence of the interstitial fluid is certainly important in the granular avalanche process, as evidenced by the marked differences between the propagation of aeolian and submarine dunes: the flow may be continuous in the lee side of submarine dunes, but occurs by successive avalanches for aeolian dunes (Hunter (1985)). This is why two geologists in the early 1970's, Allen (1970) and Carrigy (1970), have made the first compared studies between dry and water immersed granular avalanches in a slowly rotating drum, focusing on the avalanche duration T and the avalanche amplitude $\Delta\beta = \beta_c - \beta_r$ that corresponds to the difference between the critical angle β_c at which an avalanche starts and the angle of repose β_r at which an avalanche stops. They concluded that the avalanche amplitude and the time duration of water

immersed granular avalanches are respectively smaller and larger when compared to the dry case.

During these last years, much attention has been paid to the dry case, and a review of numerous different studies can be found in the collective work of GDR MiDi (2004). It appeared from all the experimental and numerical results collected in this paper that a local rheology, with a dynamical friction coefficient μ depending on a dimensionless shear rate, correctly describes the steady avalanche flows down inclined planes. This dimensionless shear rate, named the inertial number and denoted I , arised from the work of da Cruz *et al.* (2005) on the steady plane shear configuration. The inertial number I can be viewed as the ratio of the typical falling time of one grain over its diameter (due to the confining external pressure or gravity) to the characteristic time of shear (GDR MiDi (2004)). Recently, the crucial role of side walls on steady granular surface flow on a heap has been investigated experimentally by Jop, Forterre & Pouliquen (2005): the strong localisation of the shear at the heap surface can be recovered by the same local rheology $\mu(I)$ provided that solid friction at the close walls is taken into account. Note that a similar local rheology has been developed in the mean time by Josserand, Lagree & Lhuillier (2004) with a slightly different point of view: the friction coefficient μ depends not only on I but also on the confining pressure while the local solid packing fraction ϕ is also a function of these two quantities. These two examples of local rheology appear to be able to reproduce many experimental observations for stationary conditions. These successes do not mean that the rheology is purely local since some non local behaviours, such as arching effects, are clearly pointed out (see e.g. in GDR MiDi (2004)) and that other non local modelling can also succeed in reproducing some of the experimental observations (Mills, Loggia & Texier (1999), Andreotti & Douady (2001), Rajchenbach (2003)).

Besides, some recent studies focused on the role of the interstitial fluid on dense granular flows. Courrech du Pont *et al.* (2003a) have systematically studied the avalanche duration and amplitude for different bead sizes, different bead and fluid densities, and different fluid viscosities in a slowly rotating drum. They put in light three different regimes depending on two dimensionless parameters: the grain/fluid density ratio r and the Stokes number St that corresponds to the ratio of grain inertia to fluid dissipation. In the ‘free-fall’ regime at large r and St values corresponding typically to solid grains immersed in a gas (e.g. the so-called dry case) the interstitial fluid can be neglected and the avalanche duration scales as a free-fall of one grain along the pile length L . Otherwise, the interstitial fluid controls the dynamics: at low St (case of small grains in viscous fluids, e.g. fine sand in water), the regime is ‘viscous’ as viscous forces are predominant, and the avalanche duration scaling corresponds to the pile length L covered by one grain at its terminal viscous Stokes velocity ; at low r and large enough St (case of large grains in liquids, e.g. coarse sand in water), the regime is ‘inertial’ as inertial fluid forces here dominate, and the avalanche duration scaling corresponds to the pile length L covered by one grain at its terminal inertial velocity. In a fast rotating drum, Jain, Ottino & Lueptow (2004) studied by particle tracking velocimetry (PTV) the steady flow of large steel beads in air, water or different water-glycerine mixtures and draw the main following conclusion: the velocity profile in the liquid case has a similar shape as in the dry case. By using an inclined recirculating flume, Armanini *et al.* (2005) tracked by a Voronoi imaging method the steady flow of PVC pellets in water. They found that the flow organises into different sublayers with either frictional or collisional behaviour. The transition between the frictional behaviour at low shear rate and the collisional behaviour at high shear rate appears to be controlled by the Stokes number, as this number has been shown to be the pertinent parameter that governs the liquid

immersed collision of grains (Davis, Serayssol & Hinch (1986); Joseph, Zenit, Hunt & Rosenwinkel (2001); Gondret, Lance & Petit (2002)). More recently Cassar, Nicolas & Pouliquen (2005) investigated experimentally the steady flow of glass beads in water down a rough inclined plane. They successfully analysed their results within the local rheology framework $\mu(I)$ developed initially in the dry case but adapted for the liquid immersed configuration: the falling time scale that enters in the definition of the inertial number I has to be here the viscous falling time already suggested by Courrech du Pont *et al.* (2003*a*). Finally, Loiseleux *et al.* (2005) studied the influence of a superficial water flow on the onset of granular avalanches: an upward water flow tends to increase the pile stability while the contrary stands for a downward water flow.

In this paper, we report results on the unsteady relaxation dynamics of a pile of small glass beads immersed in water in a long and thin inclinable channel, in the viscous avalanche regime defined by Courrech du Pont *et al.* (2003*a*). The paper is organised as follows. The experimental set-up and measurement methods are presented in § 2. The experimental results for the slope relaxation, granular flux, velocity profile and flowing layer thickness are presented and discussed in § 3, together with the influence of a water counter-flow. A modelling of our experimental configuration is then developed in § 4 by using the local rheology $\mu(I)$. At the end of § 4, we also implement the model to take into account the effect of a water counter-flow. All these model predictions are compared to the experimental data and discussed.

2. Description of the experiments

2.1. Set-up

The experimental set-up is composed of two 10 mm thick glass plates separated by a thin rubber sheet which defines the perimeter of the channel (length $L = 128$ cm and height

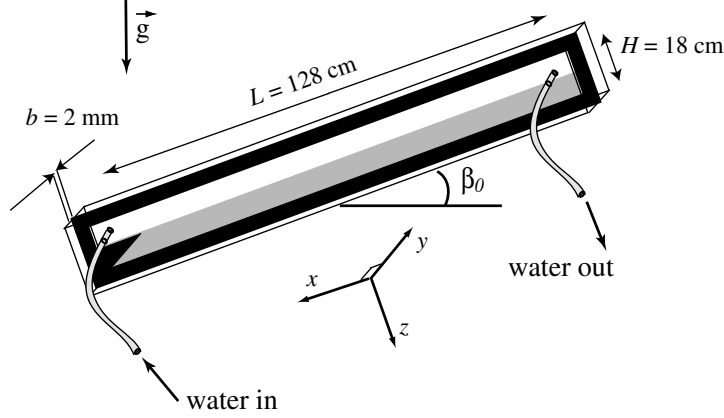


FIGURE 1. Sketch of the tiltable experimental Hele-Shaw cell.

$H = 18$ cm) and insures a constant gap $b = 2.0 \pm 0.1$ mm (figure 1). This Hele-Shaw cell is half filled with spherical glass beads (density $\rho_g = 2.5 \times 10^3$ kg/m³) manually sieved within the range $[125, 140]$ μm , with the mean diameter $d \simeq 132$ μm . As the ratio between the width of the channel and the diameter of the beads $b/d \simeq 15$ is not large and, due to solid wall friction, the two characteristic pile angles β_c and β_r are increased by a few degrees when compared to the values for non confined piles (Courrech du Pont *et al.* (2003b)). The particles are completely immersed in de-ionized water (density $\rho = 10^3$ kg/m³ and viscosity $\eta = 10^{-3}$ Pa.s). With such grains and fluid, one can calculate the Stokes velocity for one isolated falling grain $V_{St} = \Delta\rho g d^2 / 18\eta$ where $\Delta\rho = \rho_g - \rho$ is the density difference between grains and liquid, and calculate also the density ratio $r = (5\rho_g/3\rho)^{1/2}$ and the Stokes number $St = \rho_g^{1/2} d^{3/2} (\Delta\rho g)^{1/2} / 18\sqrt{2}\eta$ defined by Courrech du Pont *et al.* (2003a) for determining the avalanche regime: $V_{St} \simeq 14$ mm/s, $r \simeq 2$ and $St \simeq 0.4$. As $r < 5$ and $St/r < 2$, the avalanche regime will be viscous. The cell is connected to a hydraulic pump which, while imposing a pressure difference between the inlet and outlet of the cell, gives rise to a continuous steady laminar water flow above the granular bed. As the water flow rate through the porous granular bed is negligible (Beavers & Joseph (1967)), the mean water flow rate Q_f above the granular

bed is measured with a flow-meter. In a Hele-Shaw cell, Gondret *et al.* (1997) showed that, with flat and rigid walls, the velocity profile of the flowing liquid is parabolic in the transverse direction (y axis), and constant in the central (x, z) plane except for an exponential decrease near the top and bottom walls. Thus the water flow rate Q_f gives the mean velocity $\overline{U}_f \simeq Q_f/(bh_f)$ where h_f is the water height ($h_f \sim H/2$). The shear stress exerted by the fluid on the granular interface can finally be inferred by the relation $\tau_{xz} \simeq 3.26\eta\overline{U}_f/b$ (cf. appendix of Loiseleux *et al.* (2005)).

The particles are backlighted with a white LED box and video cameras are fixed to the channel. All the set-up, mounted on a motorised device, is tiltable in its (x, z) plane around the horizontal y axis from -60 to $+60^\circ$ without shocks with an angular velocity of about $10^\circ/s$. The angle between the longitudinal axis of the experimental cell Ox and the horizontal is measured with a digital inclinometer with a precision of $\pm 0.1^\circ$. More details about the set-up can be found in Doppler (2005).

2.2. Measurements

We restrict here our study to granular flows in quiet water, or with a weak water flow acting against gravity (counter-flow). The experimental procedure is the following. We first carefully prepare a flat granular interface by alternatively tilting the cell to large opposite angles, thus triggering avalanches in both directions. An experiment starts when the granular bed is tilted rapidly from slightly below β_r up to a fixed angle $\beta_0 > \beta_c$ within roughly 1 s. An avalanche starts and the pile slope relaxes slowly toward the angle of repose β_r . During the avalanche that can last few hours, the interface remains flat, and the avalanche dynamics is thus well characterised by the time evolution of the slope angle $\beta(t)$ from β_0 to β_r . When a water counter-flow is imposed, it is applied just before tilting the cell. In that case, the angles β_c and β_r are slightly larger as described in § 3.2.

The relaxation dynamics of the granular pile is studied experimentally using both global and local measurements.

- In a first global measurement technique, we focus on the time relaxation of the free surface of the pile with time. A CCD camera is placed at midlength and images are grabbed at a frequency of 1 Hz. As the channel is closed and contains a fixed grain quantity, the accumulation of particles at the base of the pile makes the downstream height to increase whereas the upstream height decreases but the interface remains flat during the avalanche. By image processing we extract the granular interface and then calculate its instantaneous mean slope $\beta(t)$. By mass conservation, the granular flux per unit width q_β at the center of the pile can be inferred from the evolution rate of the surface slope $d\beta/dt$ by the relation

$$q_\beta = -\frac{L^2}{8} \frac{d\beta}{dt}. \quad (2.1)$$

This granular flux q_β per unit width is related to the effective mass flow rate of the grains Q_m by $Q_m = \phi \rho_g b q_\beta$, where ϕ is the volume solid fraction of the granular packing.

- In a second local measurement technique, we measure the velocity field of the particles close to the wall with a Particle Image Velocimetry (PIV) method based on inter-correlation techniques between two successive images which provides valuable measures of grain velocity fields (Lueptow, Akonur & Shinbrot (1999)). For this, another camera with high image rates (from 100 to 1000 frames/s) is placed at mid-length of the cell. Video sequences of about 10 seconds are recorded, and then analysed with a commercial PIV software. We use interrogation windows (12×12 pixels) corresponding roughly to one grain size that gives the velocity field at the grain scale. To reduce noise, the velocity fields are averaged in the flow direction over the whole image width (typically 7 mm) and averaged in time over typically 50 successive images. The compromise between temporal and spatial resolutions as well as PIV parameters gives a final velocity accuracy

of about 0.1 mm.s^{-1} and an in-depth resolution of 0.1 mm corresponding to one grain diameter. Note that we observe the velocity field of the particles only at the wall and not in the bulk. However Courrech *et al.* (2005) showed that the dynamical evolution of the gap averaged velocities and wall velocities are comparable. With this PIV method we extract the in-depth grain velocity profiles $v(z)$ for different initial tilting angles β_0 with or without a water counter-flow, and we obtain by numerical integration the granular flux $q_{piv} = \int v(z)dz$ at the wall. The granular flux q_{piv} is measured at the wall and is therefore related to q_β by a coefficient that depends on the transverse profile of the velocity, more precisely on its exact form and slip velocity at the wall (§ 4.1.7). The two granular flux measurements q_β and q_{piv} will be compared in the following.

3. Experimental results

Results obtained without any imposed water counter-flow are detailed in § 3.1. The effect of a water counter-flow is then presented in § 3.2.

3.1. Quasi-steady granular flows

3.1.1. Slope relaxation

The time evolution of the pile slope $\beta(t)$ is presented in figure 2 for various initial tilt angles β_0 ranging roughly from the mean maximum angle of stability $\beta_c(\sim 31^\circ)$ up to 39° for which the system is far from equilibrium. In each case, the surface slope decreases in time but more and more slowly. The avalanches end after few hours at an angle of repose β_r . As it is usually observed for avalanches, the final slope angle differs slightly from one experiment to another: the angle of repose fluctuates by typically one degree around its mean value $\beta_r \simeq 29 \pm 1^\circ$. It is worthnoting that the time variation of the slope angle $\frac{d\beta}{dt}$ appears to be correlated to the slope angle β : it is larger for larger angle

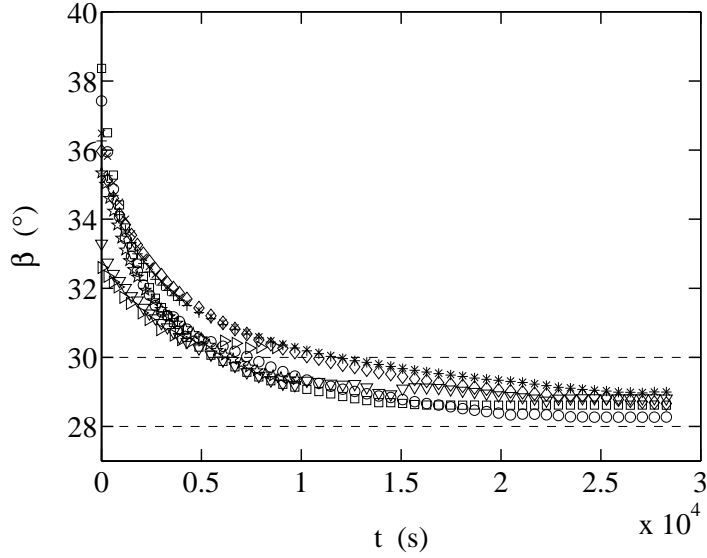


FIGURE 2. Time evolution of the pile slope β for different initial tilt angles β_0 : (\triangleright) $\beta_0 = 32.6^\circ$, (∇) $\beta_0 = 33.3^\circ$, (\star) $\beta_0 = 35.4^\circ$, (\diamond) $\beta_0 = 36.0^\circ$, (+) $\beta_0 = 36.3^\circ$, (\times) $\beta_0 = 36.5^\circ$, (\circ) $\beta_0 = 37.4^\circ$, (\square) $\beta_0 = 38.4^\circ$. (- -) limit values of $\beta_r = 29^\circ \pm 1^\circ$.

values. Note that for very large β_0 angles ($\beta_0 > 45^\circ$), the interface is no more flat with downward propagating waves and particles in suspension.

3.1.2. Granular flux

The time evolution of the granular flux q_{piv} obtained from PIV measurements is presented for short times in figure 3a. Data show that in the first seconds of the avalanche the granular flux increases before rapidly saturating at a plateau value. The granular flux, that can be viewed as saturated at short times when the slope angle does not change significantly, decreases in fact slowly in time at larger time as the avalanche goes on and the angle slowly relaxes (figure 3b). The time duration of the short acceleration stage is about 5 s, and does not vary significantly with β_0 , whereas the avalanche lasts typically few hours. Two time scales can thus clearly be distinguished: the granular flux adapts itself in about 5 s to any β variation and after this transient, the granular flux appears to

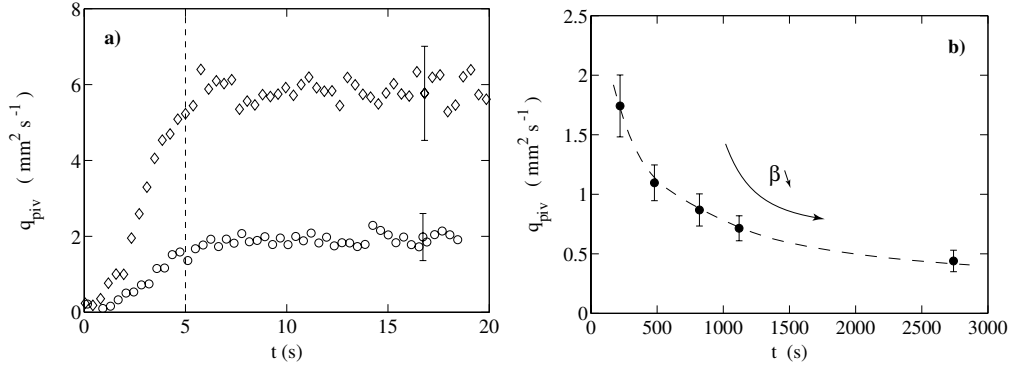


FIGURE 3. Time evolution of the granular flux q_{piv} measured by PIV means at short (a) and long times (b). Experimental data are averaged over 40 images: data points correspond to mean values and error bars to typical standard deviations. (a) $\beta_0 = 31.2^\circ$ (\circ), $\beta_0 = 33.0^\circ$ (\diamond); (b) $\beta_0 = 31.6^\circ$ (\bullet). Dashed lines are guide for the eyes.

be correlated to the instantaneous pile slope β . We can then conclude that after the quick rise transient the avalanche flow is quasi-steady without inertia effects. This result is not surprising as we are in the viscous regime defined by Courrech du Pont *et al.* (2003a). For different initial pile angles β_0 , we measure the maximum saturated granular flux q_{piv} (figure 4). As one could guess from the time decrease of β (figure 2) and q_{piv} (figure 3b), the measurements of 4 show that q_{piv} increases with β .

3.1.3. Velocity profiles

The in-depth velocity profiles $v(z)$ measured in the quasi-steady flow regime for various pile slopes β are shown in figure 5a. Whatever the pile slope is, the velocity is maximum at the pile surface ($z = 0$) and decreases toward zero at increasing depth. Data show that only a thin surface layer, roughly 1 to 2 mm thick, flows significantly. The surface velocity increases with the pile slope, taking values up to 55 mm/s, of the same order as the values found by Cassar *et al.* (2005) in the inclined rough plane configuration. These values can be larger than the Stokes velocity $V_{St} \simeq 14$ mm/s of a single falling isolated grain since the avalanche corresponds to a collective motion. Our profiles are

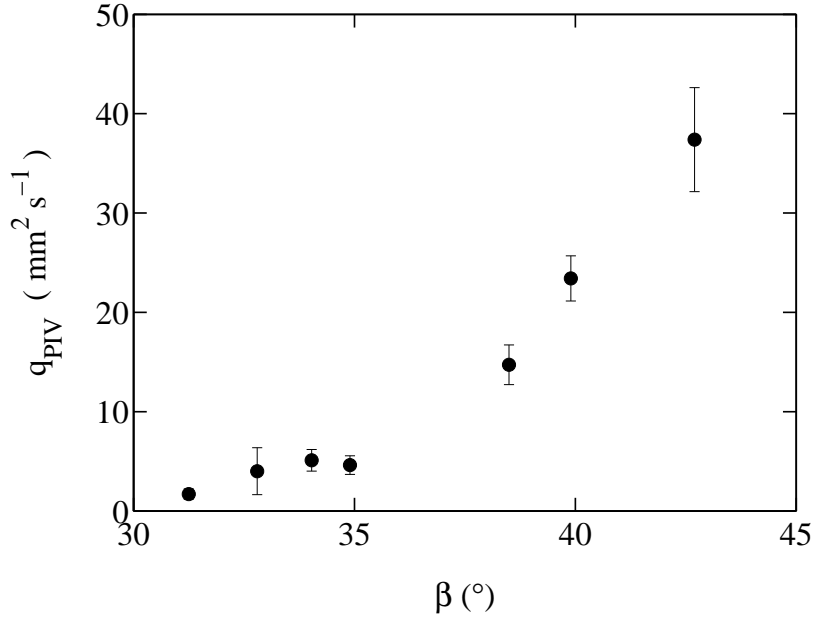


FIGURE 4. Granular flux q_{piv} as a function of the pile angle β . Data points correspond to mean values and error bars to standard deviations.

similar to those already observed for steady surface flows in the dry case (Bonamy *et al.* (2002); GDR MiDi (2004)) or liquid immersed case (Jain *et al.* (2004)). By shifting each velocity profile in z by a value z^* depending on the slope angle β , all data of figure 5a collapse rather well on a single curve as evidenced in figure 5b. As shown by Bonamy *et al.* (2002), GDR MiDi (2004), this master curve presents roughly a linear part near the surface and an exponential tail further in the depth. During the slow quasi-steady slope relaxation, the grain velocity is slowly decreasing and the velocity profile therefore describes a smaller and smaller part of the master curve. In particular, for $\beta < \beta_c$, the velocity profiles is only exponential as shown by Courrech *et al.* (2005) for dry natural avalanches.

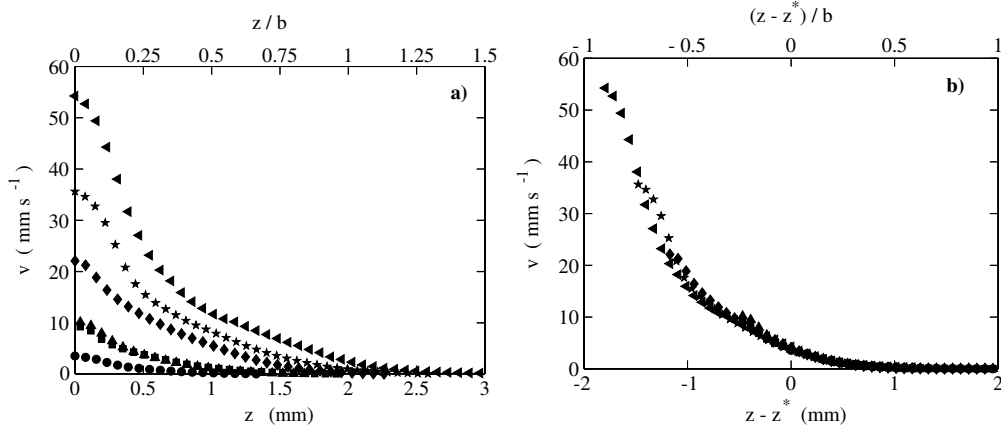


FIGURE 5. a) Grain velocity profiles in the depth z for different pile angles β : (\bullet) $\beta = 31.3^\circ$, (\blacksquare) $\beta = 34.3^\circ$, (\blacktriangle) $\beta = 34.9^\circ$, (\blacklozenge) $\beta = 38.5^\circ$, (\blackstar) $\beta = 39.9^\circ$, (\blacktriangleleft) $\beta = 42.7^\circ$. b) Same data shifted in-depth by a quantity z^* such as $v(z^*) = 4 \text{ mm/s}$.

3.1.4. Flowing layer thickness

From the velocity profiles, we define the thickness h of the flowing layer as the depth where the velocity is larger than a cut-off velocity ($\sim 0.1 \text{ mm/s}$ corresponding to the less precise measurement). The measurements of h for various experiments are reported in figure 6 as a function of the tilt angle. This figure shows that the flowing layer thickness h increases linearly with $\tan \beta$. Similar results are found for larger values of the cut-off velocity. Such a result has already been observed by Taberlet *et al.* (2003) and Jop *et al.* (2005) for steady dry granular flows with a continuous feeding, and has been attributed to wall effects. In our case, the measured flowing layer thickness varies roughly from 1 to 3 mm (5 to 20 grain diameters) which is of the order of the gap thickness $b = 2 \text{ mm}$. Note that no data is reported below the angle of repose β_r as no flow occurs then. Thus a non-zero flowing layer thickness may exist at the flowing/static transition, here $h_r \simeq 0.7 \text{ mm}$ at $\tan \beta_r \simeq 0.55$.

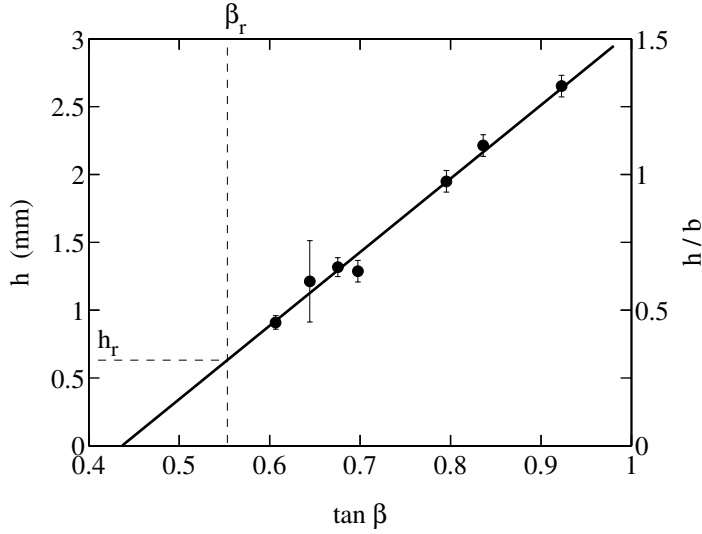


FIGURE 6. Flowing layer thickness h as a function of the pile slope β . (●) Experimental data together with error bars corresponding to standard deviation. The solid line corresponds to the linear fit h (mm) = $5.4(\tan \beta - 0.43)$.

3.2. Effect of a counter-flow

We now report the effect of a water counter-flow imposed along the granular pile on the avalanches. The water flow rate is chosen below the threshold corresponding to the onset for bed-load motion. Loiseleux *et al.* (2005) have shown that this onset corresponds to a critical value θ_c of the Shields number $\theta = \tau_{xz}/(\Delta\rho gd) = 3.26\eta\overline{U_f}/(\Delta\rho gbd)$, that compares the fluid forces acting on a surface grain to its apparent weight. When both avalanche and counter erosion processes take place simultaneously, Loiseleux *et al.* (2005) mentioned also that non-linear structures quickly grow. In all the present experiments, the θ value will thus be kept below the critical value 0.1 to avoid any erosion process and formation of structures that would modify drastically the avalanche flow. We also restrict our study to water counter-flow as it is rapidly difficult for water co-current flows to distinguish between erosion and avalanche granular motions (Loiseleux *et al.* (2005)).

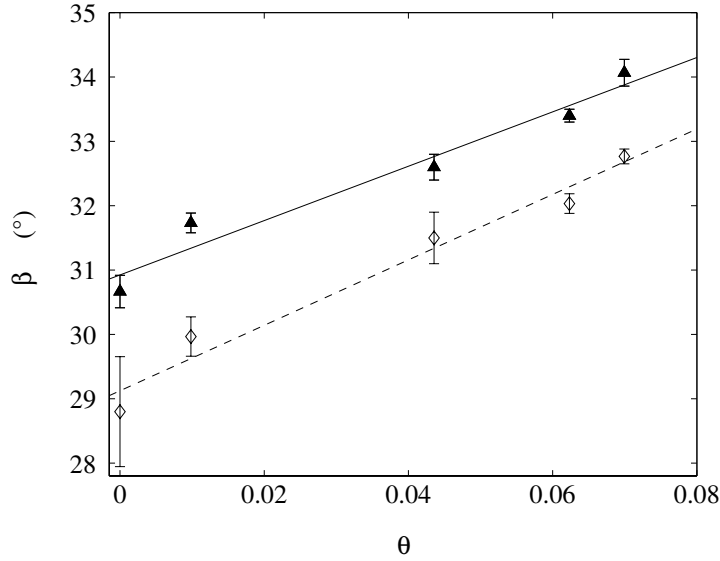


FIGURE 7. Experimental maximum angle of stability β_c (\blacktriangle) and angle of repose β_r (\diamond) as a function of the Shields number θ for water counter-flows ($\theta > 0$), with best linear fits $\beta_c(\theta) = 30.9 + 42.2\theta$ (—), $\beta_r(\theta) = 29.1 + 50.8\theta$ (- - -).

3.2.1. Angles of stability

The water flow modifies the force equilibrium acting on the pile and thus the two characteristic angles β_c and β_r . For different flow rates, i.e. different values of the Shields number, we measured the corresponding maximum angle of stability β_c and angle of repose β_r . The influence of the Shields number θ on both angles is presented in figure 7 for the grain diameter studied here ($d \simeq 132 \mu\text{m}$). As observed for various other diameters (Loiseleux *et al.* (2005)), both β_c and β_r increase linearly with θ by a few degrees, typically from 31° to 34° for β_c and from 29° to 33° for β_r .

3.2.2. Avalanche dynamics

When a water counter-flow is imposed along the pile, the relaxation process of the pile angle is slowed down but is similar to the configuration without any water flow. We find that the time needed for the granular flux to reach a steady state is the same without or

with a counter-flow (Doppler (2005)). More strikingly, it is observed that velocity profiles measured in the quasi-steady regime, without or with a counter-flow, present similar shapes, as illustrated in figure 8a. For a given slope angle β , *e.g.* $\beta = 42.6^\circ$ ($\tan \beta = 0.92$) in figure 8a, the water counter-flow tends to slow down the grains. However, as evidenced in figure 8a, velocity profiles coincide for the same deviation from the maximum angle of stability $\tan \beta - \tan \beta_r(\theta)$, *e.g.* $\tan \beta - \tan \beta_r(\theta) = 0.28$ in figure 8a. Such a collapse is observed for various data sets.

When one focuses on the thickness h of the granular flowing layer, it appears from figure 8b that h increases also linearly with $\tan \beta$ when a counter-flow is applied (open symbols). For a given angle β , h is however reduced when a water counter-flow is applied. Again, this is due to the resisting effect of the counter-flow that slows down the avalanche. As the slope of the two linear fits of figure 8b is the same, the h reduction is only due to a larger intercept with the horizontal axis corresponding to a larger static friction coefficient (see § 4), here $\mu_s(\theta) = 0.51$ for $\theta = 0.08$ when compared to the no water flow case, $\mu_s(0) = 0.43$ for $\theta = 0$. Note that the difference $\mu_s(\theta) - \mu_s(0) \simeq 0.08$ for the friction coefficient appears to be the same as the difference $\tan \beta_r(\theta) - \tan \beta_r(0) \simeq 0.08$ for the angle of repose β_r . Thus, the deviation $\tan \beta - \tan \beta_r(\theta)$ or $\tan \beta - \mu_s(\theta)$ appears to be the control parameter of the dynamics of water immersed granular avalanches, which characterizes the out of equilibrium state of the system. This will be understood in the modelling presented in next section.

4. Modelling the avalanche.

Let us now present the modelling of our experimental configuration. This modelling is based on the analysis developed for steady dense flows of dry granular matter in GDR MiDi (2004), and adapted recently either for dry confined flows by Jop *et al.* (2005) or

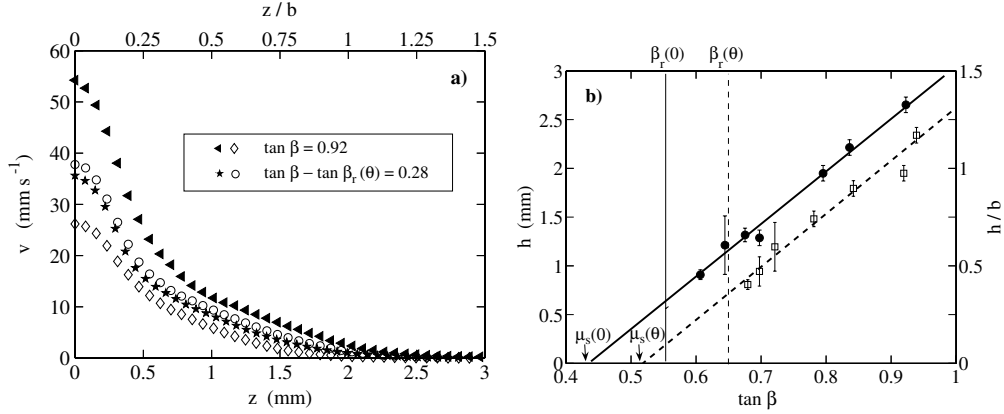


FIGURE 8. a) In-depth velocity profile for different values of β with the counter-flow $\theta = 0.08$ ($\beta = 42.6^\circ$ (\diamond), $\beta = 43.2^\circ$ (\circ)) or without any counter-flow ($\beta = 39.9^\circ$ (\star), $\beta = 42.7^\circ$ (\blacktriangleleft)). b) Flowing layer thickness h as a function of the pile angle β with the counter-flow $\theta = 0.08$ (\square) or without any counter-flow (\bullet). Best linear fits give $h(\theta) = 5.4(\tan \beta - 0.51)$ with the counter-flow $\theta = 0.08$ (- - -) and $h(0) = 5.4(\tan \beta - 0.43)$ without any counter-flow (—) .

for water immersed grains by Cassar *et al.* (2005). The key point is that for a granular material exhibiting a simple shear with the shear rate γ and the confining granular pressure $\tau_{zz} = P_g$, the shear stress τ_{xz} obeys a Coulomb relation

$$\tau_{xz} = \mu(I)P_g, \quad (4.1)$$

where the friction coefficient μ depends on a single dimensionless parameter I and where the solid volume fraction ϕ is supposed to be the same all over the flowing layer. The inertial number I can be viewed as the ratio of two time scales: the typical flow time scale $1/\gamma$, and the typical falling time scale for one grain from the top of an underneath grain to the next hole. The typical falling time scale is the free fall time $t_{ff} \sim d(\rho_g/P_g)^{1/2}$ for dry grains of diameter d and density ρ_g , but corresponds to the viscous falling time $t_{vf} \sim \eta/(\alpha P_g)$ for grains immersed in a viscous liquid of viscosity η (Cassar *et al.* (2005)). The coefficient α relates the permeability k of the corresponding granular medium to the grain diameter d : $\alpha = k/d^2$. Whatever the regime is, the dependence of the friction

coefficient μ with the parameter I is well fitted by the relation (Cassar *et al.* (2005))

$$\mu(I) = \mu_s + \frac{\mu_m - \mu_s}{1 + I_0/I}. \quad (4.2)$$

The coefficient μ varies continuously from the lower asymptotic value μ_s for slow flows with low shear rate γ (*i.e.* for $I \ll 1$) towards the maximum asymptotic value μ_m for rapid flows with high shear rate γ (*i.e.* for $I \gg 1$). Note that this kind of analysis does not catch the complex static/flowing transition of granular matter, as for instance the hysteretic behaviour of granular piles between the two characteristic avalanche angles β_c and β_r .

4.1. *Confined submarine avalanches*

4.1.1. *Model equations*

Let us apply this theoretical framework to our experimental configuration in a quasi-steady regime. The equilibrium of a slice of immersed grains of solid packing fraction ϕ between the upper surface and the depth z confined between two parallel solid walls separated by the gap width b can be written as

$$0 = \tan \beta - \mu_w \frac{z}{b} - \mu(I). \quad (4.3)$$

The first term of the right hand side corresponds to the driving gravity force whereas the two other terms correspond to resisting friction forces: the solid friction at the lateral walls with the friction coefficient μ_w , and the friction at the bottom of the slice due to the shear in the granular pile. Note that this last term depends on the vertical position z as the shear rate γ (and then I) varies in the depth z of the granular pile. As stated above, the parameter $I = \eta\gamma/(\alpha P_g)$ writes for liquid immersed grains flowing under gravity

$$I(z) = \frac{\eta\gamma(z)}{\alpha\phi\Delta\rho g z \cos \beta}, \quad (4.4)$$

as $P_g = \phi\Delta\rho g z \cos \beta$ is the normal stress due to the buoyant weight of the grains.

4.1.2. *Flowing layer thickness*

The thickness h of the flowing layer can be determined by considering the depth where $\gamma(h) = 0$, so that $I(h) = 0$. In such a case, the last term of equation (4.3) tends towards μ_s , and (4.3) leads to

$$\frac{h(\beta)}{b} = \frac{\tan \beta - \mu_s}{\mu_w}. \quad (4.5)$$

Note that this last condition does not depend on the precise expression chosen for the dynamical friction coefficient $\mu(I)$ but just on the non zero friction coefficient μ_s at low shear. Equation (4.5) predicts a linear dependence for the thickness of the flowing layer with $\tan \beta$ as observed experimentally in figure 6. The best linear fit of our data gives $\mu_w \simeq 0.37 \simeq \tan 20.3^\circ$ and $\mu_s \simeq 0.43 \simeq \tan 23.3^\circ$. Although both these values depend on the precise criterion chosen to measure experimentally the flowing layer thickness, similar values can be found in the literature (Jop *et al.* (2005); Taberlet *et al.* (2003); Cassar *et al.* (2005)). Note that this modelling does not describe the static/flowing transition, so that (4.5) does not predict the angle of repose β_r neither the corresponding avalanche thickness h_r that are found experimentally to be $\beta_r \simeq 29^\circ$ ($\tan \beta_r \simeq 0.55$) and $h_r \simeq 0.7$ mm.

4.1.3. *Granular flux*

Equation (4.3) together with (4.2) and (4.4) also allows to deduce the in-depth profile of the shear rate $\gamma(z)$, thus the velocity profile $v(z)$ and the grain flux per unit width q by successive integration as

$$\begin{cases} \gamma(z) &= \gamma^* \frac{z}{b} \cos \beta \left(\frac{\mu_m - \mu_s}{\tan \beta - \mu_w \frac{z}{b} - \mu_s} - 1 \right)^{-1}, \\ v(z) &= \int_h^z \gamma(z) dz, \\ q &= \int_h^0 v(z) dz, \end{cases} \quad (4.6)$$

where $\gamma^* = \alpha\phi I_0 \Delta\rho gb/\eta$. In the following, we will use the velocity scale $v^* = \gamma^* b$ and the granular flux scale $q^* = \gamma^* b^2$.

From the set of equations (4.6) we can calculate the granular flux q for a given angle β provided β is smaller than the upper limit value $\arctan \mu_m$. In figure 9, the normalized granular flux q/q^* is plotted by using for q^* the same parameter values of $\phi = 0.55$, $\alpha = 0.01$ and $I_0 = 1$ used by Cassar (2005). The other friction parameters have been determined by the fit of our h data ($\mu_w = 0.37$ and $\mu_s = 0.43$, see § 4.1.2) except μ_m . This last parameter will be determined by the fit of our q data. The experimental data for the granular flux q_β are obtained by averaging the time derivative of the slope relaxations of figure 2. The numerical calculation of q for $\mu_m = 0.9, 1$ and 1.1 are plotted on figure 9. The curve for $\mu_m = 1$ fits the experimental data well. This value is a little higher than the range $(0.82, 0.87)$ of μ_m found in Cassar (2005). The granular flux increases non linearly with β since both the surface velocity and the flowing layer thickness h increase with β . As $\cos \beta$ does not vary so much in the explored range of angles, this non linear variation corresponds roughly to $q/q^* \sim (\tan \beta - \mu_s)^4$ as demonstrated in the appendix (A 3) for small enough flowing layer thicknesses and thus small enough pile angles. Such an analytical scaling (thick dashed line in figure 9) is close to the complete numerical calculation at small angles but deviates significantly at larger angles by about 25 percent at $\beta \simeq 37^\circ$. For even higher angles, the analytical scaling underpredicts even more the q values as the complete calculation diverges when β approaches $\arctan \mu_m \simeq 45^\circ$ from below. Note that Jop *et al.* (2005) found a similar scaling of the granular flux $q \sim (\tan \beta - \mu_s)^{7/2}$ for dry confined steady flows, with a slightly different exponent. This slight difference arises from the differences in the velocity profiles between the dry case and the liquid immersed case, as the inertial parameter I has not the same expression in the two cases. Note also that by integrating (4.6) q is supposed to tends toward 0 when

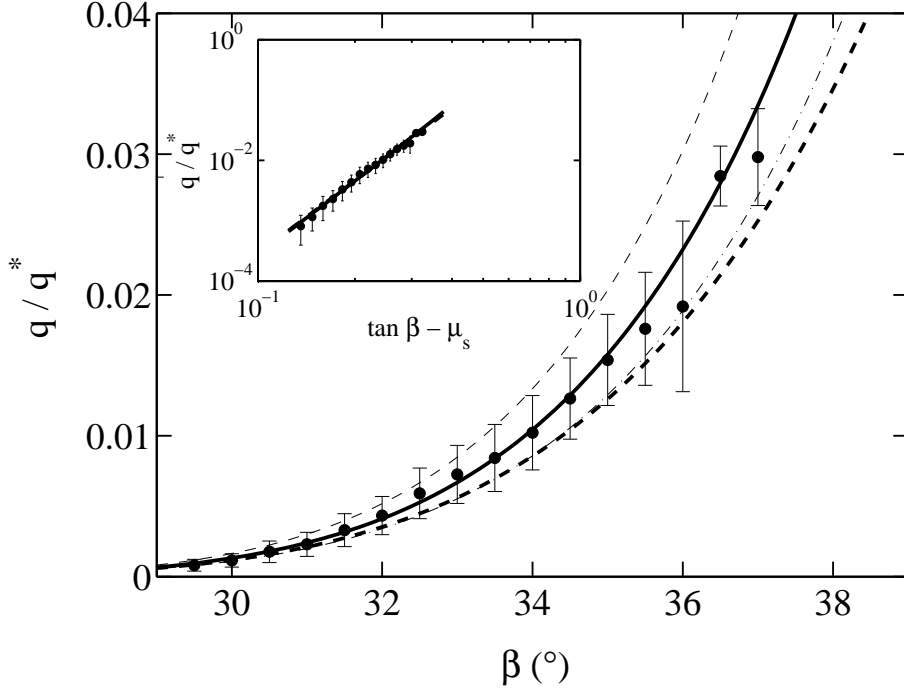


FIGURE 9. Normalized granular flux q/q^* as a function of the pile angle β . Data points (\bullet) correspond to the mean values of the experiments of figure 2 and error bars are the corresponding standard deviations. Lines come from the modelling by set of equations (4.6) with $\mu_w = 0.37$, $\mu_s = 0.43$, and $\mu_m = 1$ (—), $\mu_m = 0.9$ (---), $\mu_m = 1.1$ (- · -), and by the approximate power law (Eq. A 3) $q/q^* \sim (\tan \beta - \mu_s)^4$ (· · ·), with $\mu_m = 1$. Same data are shown in the insert, using a log-log representation.

β tends toward $\arctan \mu_s \simeq 23.3^\circ$ but the flow experimentally stops at an angle of repose $\beta_r > \arctan \mu_s$, for which the modelling predicts a weak but non-zero value of q .

4.1.4. Slope relaxation

Since the time derivative of the pile angle β is related to the granular flux q by equation (2.1), we can calculate by numerical integration any $\beta(t)$ curve starting from a given initial value $\arctan \mu_s < \beta_0 < \arctan \mu_m$. Each experimental curve $\beta(t)$ of figure 2 can thus be fitted by the model with the same parameter values except slightly different μ_s values: $\mu_s = 0.434 \pm 0.013$, that correspond closely to the μ_s value 0.43 found previously

with the flowing layer thickness measurements. All the data $\beta(t)$ can be seen in the normalized plot of figure 10 together with the full master numerical curve (solid line). For this, each experimental curve has to be shifted by a time lag τ_d depending on the corresponding initial angle β_0 (τ_d increases for decreasing β_0). One can see in figure 10 that the data are very close to the model except that the avalanches stop experimentally at an angle of repose larger than $\arctan \mu_s$: the experimental curves then deviate from the model curve with a plateau after the avalanche stop. The dispersion in the plateau values corresponds to the experimental fluctuation of the angle of repose. The slope relaxations $\beta(t)$ do not correspond to an exponential decrease but roughly to a power law. Indeed, as detailed in the appendix, analytical calculations are possible under some restrictions. The key point is that the slope relaxation corresponds to the scaling $((t + \tau_d(\beta_0))/\tau_c)^{-1/3}$ (A 5), where τ_c is a characteristic time proportional to L^2/q^* (A6). This scaling (dashed line in figure 10) is very close to the complete calculation (solid line). The τ_c values can be inferred from the previous fitting μ_s values: $\tau_c = 29.9 \pm 0.07$ s.

4.1.5. *Avalanche time duration*

As the modelling predicts an avalanche slope relaxation toward the low limit value $\arctan \mu_s$ with a vanishing granular flux, the asymptotic value $\arctan \mu_s$ would be reached for an infinite time. However, since the slope relaxation stops experimentally at the angle of repose $\beta_r > \arctan \mu_s$, the experimental avalanche time duration should be finite, with the scaling (A 8)

$$T = \tau_c \left[\frac{1}{(\tan \beta_r - \mu_s)^3} - \frac{1}{(\tan \beta_0 - \mu_s)^3} \right]. \quad (4.7)$$

The present expression is much more complex than the one already proposed by Courrech du Pont *et al.* (2003a) as their scaling $T \sim L/V_{St}$ was independent of the avalanche amplitude. However, Courrech du Pont *et al.* (2003a) report results on natural avalanches

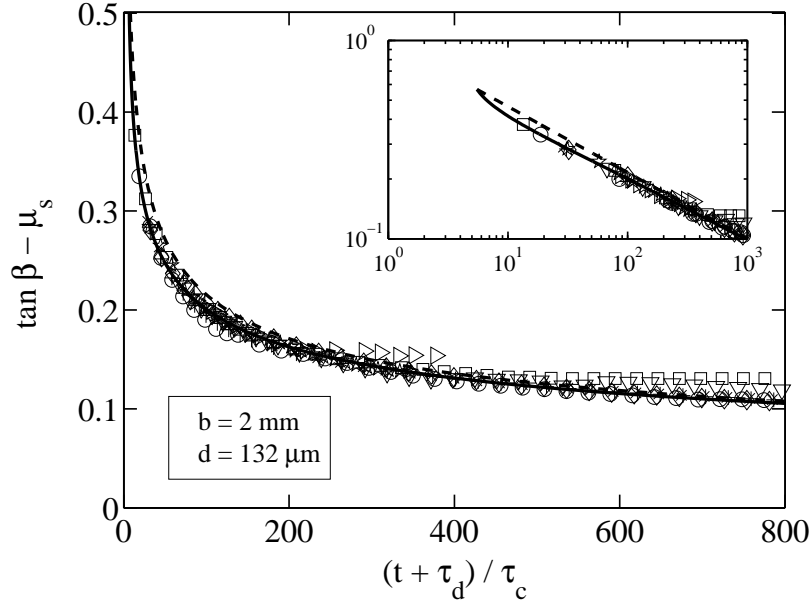


FIGURE 10. Normalized time variation of the pile angle β . Experimental data (same symbols as in figure 2) are rescaled using best fitting values of $\mu_s = 0.434 \pm 0.013$ and $\tau_c = 29.9 \pm 0.07$ s. Numerical modeling (—) by set of equations (4.6) with same parameter values as in figure 9, and analytical approximation (- - -) by equation (A5): $\tan \beta(t) = \mu_s + [\tau_c / (t + \tau_d)]^{1/3}$. The insert corresponds to the log-log plot of the same data.

of small amplitude from β_c to β_r contrarily to the present case where the system is driven far from equilibrium. One interesting point in the present study is that the avalanche duration increases with the starting angle β_0 . At large initial angle β_0 , T is supposed to tend towards the asymptotic value $T = \tau_c (\tan \beta_r - \mu_s)^{-3} = (5 \pm 1)$ hours which corresponds closely to the measured experimental time duration $T = (5.5 \pm 1)$ hours.

4.1.6. Influence of the gap thickness and grain diameter

In the modelling, we can see that the granular flux q per unit width is proportional to b^3 and independent of the grain size (A 3). The flux increase with b is intuitive as one can easily imagine that wall friction is less important for wider gap cell. The b dependence (b^4 for the total flux) that comes from the strong localisation of the flowing layer on the

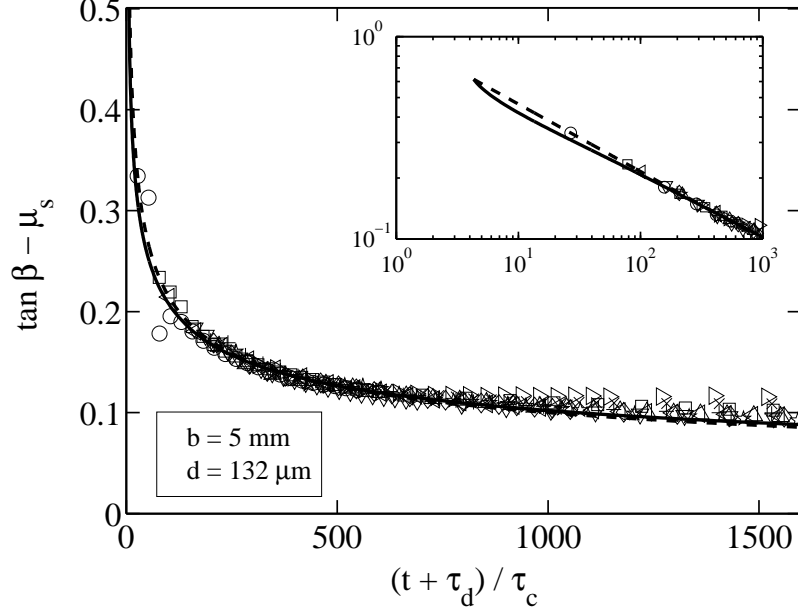


FIGURE 11. Normalized time variation of the pile angle β , with the same glass beads as in figure 10 ($d = 132\mu\text{m}$), but with a wider gap $b = 5$ mm. Experimental data are rescaled using best fitting values of $\mu_s = 0.385 \pm 0.007$ and $\tau_c = (1.91 \pm 0.02)$ s for the different curves starting from $\beta_0 = 27.7^\circ$ (\times), $\beta_0 = 27.8^\circ$ (\triangleright), $\beta_0 = 28.9^\circ$ ($+$), $\beta_0 = 29.1^\circ$ (Δ), $\beta_0 = 29.2^\circ$ (\diamond), $\beta_0 = 29.5^\circ$ (\star), $\beta_0 = 29.8^\circ$ (∇), $\beta_0 = 30.9^\circ$ (\triangleleft), $\beta_0 = 31.5^\circ$ (\square), $\beta_0 = 35.5^\circ$ (\circ). Numerical modeling (—) by set of equations (4.6) and analytical approximation (- - -) by equation (A5). The insert corresponds to the log-log plot of the same data.

scale b resembles the one of the Hagen-Poiseuille law for the flow of a classical viscous fluid in a duct of transverse size b . As in the Hagen-Poiseuille law where there is an equilibrium between the driving pressure gradient and the resisting viscous forces of the fluid, there is here an equilibrium between the driving pressure forces of gravity and the resisting viscous and granular friction forces. The non d dependence of q (Eqs. A2 and A3) is not intuitive as one could imagine that larger grains would flow faster as for a single falling grain or a classical sedimenting suspension. This surprising result comes from the fact that the time scale used in the present model is $t_{vf} \sim \eta/(\alpha P_g)$ independent

of the grain diameter as the granular pressure P_g is proportional to the depth and thus to the cell gap b . We have thus made other experiments by varying the cell gap b and the grain diameter d to test the predictions of the model. The results are plotted in figure 11 for the avalanche slope relaxations in a larger cell of gap thickness $b = 5$ mm. The model fits again the experimental data quite well with the following values $\mu_s = 0.385 \pm 0.07$ giving $\tau_c = 1.91 \pm 0.02$ s. This value is 15.7 times smaller than the τ_c value found for $b = 2$ mm and, very close to the $(5/2)^3 \simeq 15.6$ predicted factor. Note that for this larger gap, the experimental angle of repose $\beta_r = 25.7^\circ \pm 0.4^\circ$ is smaller (Courrech du Pont *et al.* (2003b)) due to smaller wall effects and the experimental curves $\beta(t)$ explore thus angle values closer to $\arctan \mu_s$ in a longer normalized time $(t + \tau_d)/\tau_c$. The measured time duration of avalanches is here $T = (80 \pm 30)$ min, a little larger than the predicted values $T = (40 \pm 20)$ min.

We have also made other experiments varying now the grain diameter d . The results for the avalanche slope relaxations are plotted in figure 12 for the thickness $b = 5$ mm but with larger grains of diameter $d = (360 \pm 40)$ μm . Again, the agreement with the model is quite good with the following fitting parameters $\mu_s = 0.444 \pm 0.005$ giving $\tau_c = (1.88 \pm 0.02)$ s. This value of τ_c is very close to the value $\tau_c = (1.91 \pm 0.02)$ s found previously for the smaller grains ($d = 132 \mu\text{m}$) in the same gap cell, meaning that the avalanche process is indeed independent of the grain size as predicted by the model. The measured time duration of avalanches is much shorter here, $T = (6 \pm 1)$ min, which is close to the predicted value $T = (7 \pm 3)$ min. Note that even if the characteristic time values τ_c are the same for the two different grain diameters in the same cell gap, the avalanche time duration is smaller for the larger grains as the angle of repose is larger ($\beta_r = 31.5^\circ \pm 1^\circ$) due to larger wall effect.

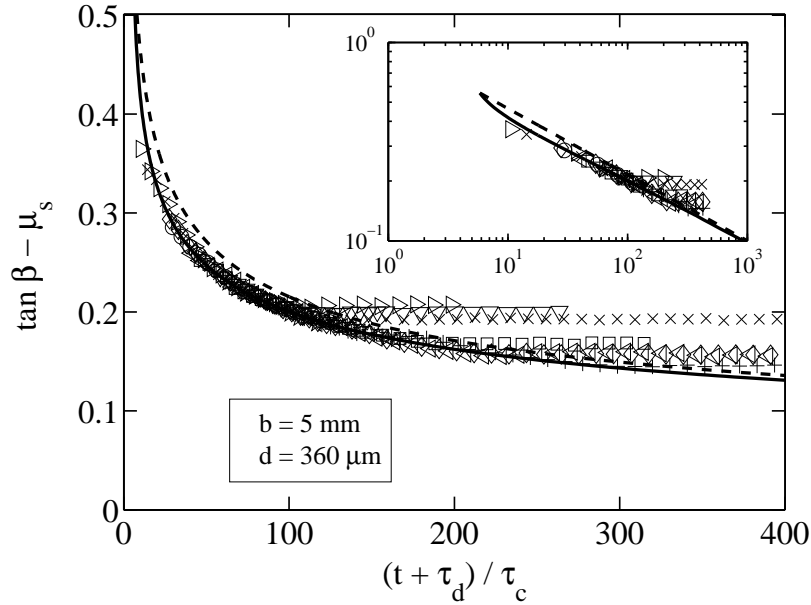


FIGURE 12. Normalized time variation of the pile angle β , for the same gap $b = 5$ mm as in figure 11 but with a larger grain diameter $d \simeq 360\mu\text{m}$. Experimental data are rescaled using best fitting values of μ_s ($\mu_s = 0.444 \pm 0.005$) and $\tau_c = (1.88 \pm 0.02)$ s for the different curves starting from $\beta_0 = 33.1^\circ$ (+), $\beta_0 = 34.0^\circ$ (∇), $\beta_0 = 34.2^\circ$ (\star), $\beta_0 = 34.7^\circ$ (\square), $\beta_0 = 35.4^\circ$ (\triangleleft), $\beta_0 = 36.0^\circ$ (\circ), $\beta_0 = 36.3^\circ$ (\diamond), $\beta_0 = 38.4^\circ$ (\times), $\beta_0 = 39.2^\circ$ (\triangleright). Numerical modelling (—) by set of equations (4.6) and analytical approximation (- - -) by equation (A5). The insert corresponds to the log-log plot of the same data.

4.1.7. Velocity profiles

The velocity profiles in the depth of the granular pile can also be calculated by set of equations (4.6). An example of such a profile for the pile angle $\beta = 34.3^\circ$ together with the experimental data are reported in figure 13. If the qualitative trend is the same, i.e. a maximal velocity at the free surface ($z = 0$) and a decreasing velocity in the depth, there is a quantitative mismatch. Indeed, the model predicts that the velocity is strictly zero at the precise depth $z = h$ ($h/b \simeq 0.67$ in figure 13) whereas the experimental data decrease smoothly towards zero with an exponential tail. Again, this mismatch shows that the modelling fails in reproducing the complex and hysteretical ‘liquid-solid’

transition. As a matter of fact, the experimental tail observed also for dry granular avalanches on piles and often referred as ‘creeping flow’ is not well understood for the moment. Another mismatch between theoretical and experimental velocity profiles is observed at the vicinity of the free surface: if the maximum normalised velocity is not so badly evaluated (0.035 instead of 0.03), the modelling predicts $\gamma = 0$ at the free surface $z = 0$ whereas it is not the case for the experimental data (figure 8a). However, the experimental data show clearly an inflexion point and a decrease of the shear rate close to the free surface. Note that the velocity profiles are measured experimentally at the wall when the velocity profiles calculated in the modelling arise from an averaging over the entire width. This may explain why the measurements are quite below the model, and can also introduce some distortion as we check experimentally that the global granular flux q_β measured by the angle variation is different from the granular flux q_{piv} measured by PIV means at the wall: the ratio q_β/q_{piv} increases roughly from 1 for $\beta \sim \beta_r$ to 5 for $\beta \sim \arctan \mu_m$. This means that the velocity profile $v(z)$ varies in the width of the channel, with a slip velocity at the wall that depends on the pile angle. This behaviour is clearly not well described by our width averaged modelling.

4.1.8. Initial transient regime

Let us come back now on the initial transient regime. Starting from the initial angle β_0 with a zero granular flux, the granular flux increases quickly toward its saturated value $q(\beta)$ that we have already determined. This transient phase can be modelled by adding the acceleration term in the left hand side of equation (4.3). The calculation shows a transient rise time for the granular flux of the order of 0.1 s instead of the few seconds observed experimentally (see figure 3). If the model fails to reproduce correctly the very first instants of the avalanche dynamics, we can however plot the avalanche path in the $(\beta, d\beta/dt)$ plane, since $d\beta/dt$ is directly related to the granular flux q . Starting

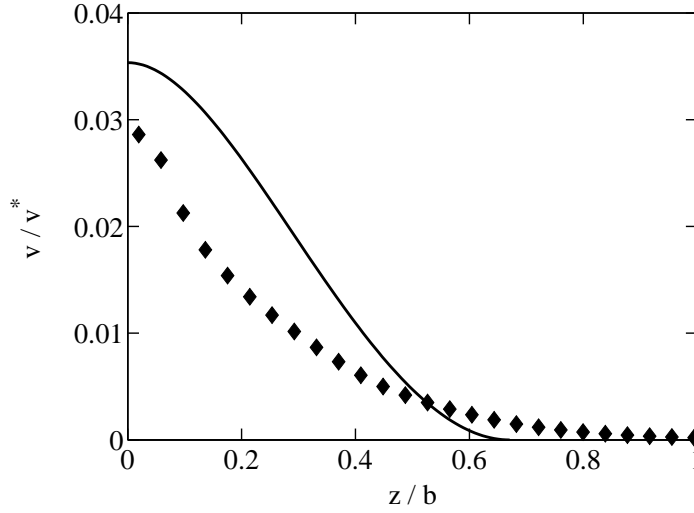


FIGURE 13. Normalised granular velocity profile for the pile angle $\beta = 34.3^\circ$. Experimental data (\blacklozenge) and modelling (—) by set of equations 4.6.

from a given angle β_0 , the granular flux and then $d\beta/dt$ increase quickly with almost no variation of β along the vertical dotted line sketched in figure 14, until they reach their saturated value at the solid line. Then the pile slope β slowly decreases in a quasi-steady way following the solid line.

4.2. Influence of a water counterflow

When a water counter-flow characterised by the Shields number θ is applied along the granular pile, the fluid forces have to be added to the force balance. In our Hele-Shaw configuration, these fluid forces have been shown to be of two origins (Loiseleux *et al.* (2005)):

- the shear stress $\tau_{xz} = \Delta\rho g d \theta$ related to the water shear at the water/grains interface,
- the longitudinal pressure gradient $\partial\tau_{xx}/\partial x \simeq 3.7(\Delta\rho g d \theta/b)$ existing in the porous phase and which is also constant along the cell (independent of x position).

The equilibrium of a slice of material of thickness z writes then:

$$0 \simeq \tan \beta - \mu_w \frac{z}{b} - \mu(I) - \theta d \frac{1 + 3.7 \frac{z}{b}}{\phi z \cos \beta}, \quad (4.8)$$

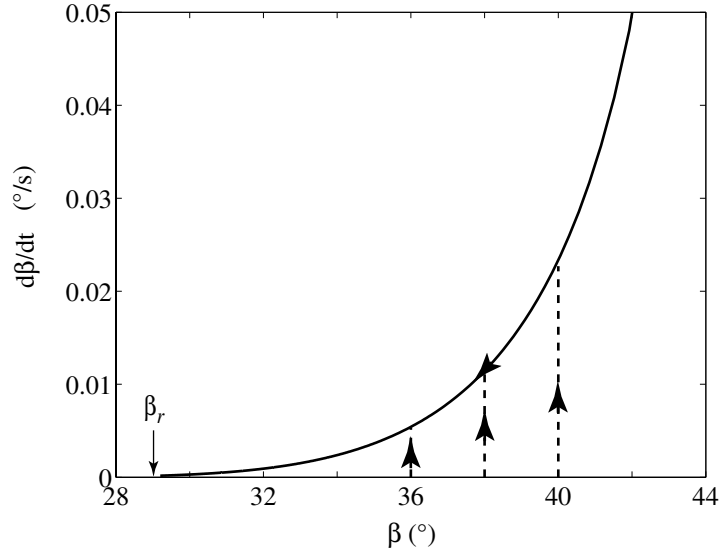


FIGURE 14. Schematic evolution of $d\beta/dt$ versus β for different avalanches of different initial angles β_0 . Dotted lines are for the transient parts.

where the last extra term in comparison with equation (4.3) represents the fluid resisting forces of two origins mentioned above. For a given slope angle β and a given Shields number θ , the thickness h of the flowing layer is determined by the quadratic relation

$$0 \simeq \tan \beta - \mu_w \frac{h}{b} - \mu_s - \theta d \frac{1 + 3.7 \frac{h}{b}}{\phi h \cos \beta}. \quad (4.9)$$

For large angle values β , the flowing layer h is thick enough ($h \sim b$) so that the fluid force term reduces to its longitudinal pressure gradient origin. The flowing layer thickness h can thus be approximated by

$$\frac{h}{b} \simeq \frac{\tan \beta - (\mu_s + 3.7 \frac{\theta d}{\phi b \cos \beta})}{\mu_w}. \quad (4.10)$$

As $\cos \beta$ does not vary so much around the value $\cos 35^\circ \simeq 0.8$, the predicted flowing layer thickness h depends quasi-linearly on $\tan \beta$ which satisfactorily reproduces the experimentally found linear variation (figure 8b). All is as if the limit friction value μ_s had to be increased by a value proportional to the Shields number θ : $\mu_s(\theta) \simeq \mu_s + 4.6\theta d/\phi b$. In the same way (4.3) leads to set of equations (4.6) for $\theta = 0$, (4.8) leads to a similar

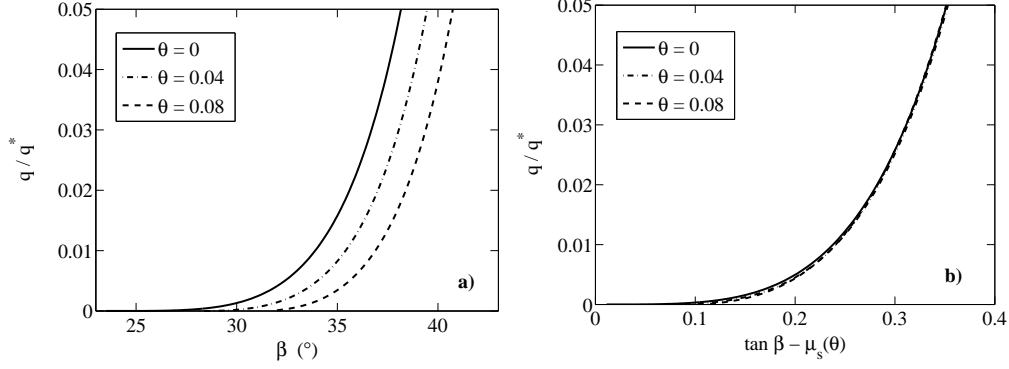


FIGURE 15. a) Normalized granular flux q/q^* as a function of the pile angle β for different water counter-flows of Shields number $\theta = 0$ (—), $\theta = 0.04$ (- · -) and $\theta = 0.08$ (- - -). b) Same data plotted as a function of $\tan \beta - \mu_s(\theta)$ with $\mu_s(0) = 0.434$, $\mu_s(0.04) = 0.48$ and $\mu_s(0.08) = 0.51$. set of equations that allows for $\theta \neq 0$ the successive calculations of the shear rate $\gamma(z)$, the velocity profile $v(z)$, and the granular flux q per unit width. The numerical results for q are shown in figure 15a for two different values of the Shields number $\theta = 0.04$ and $\theta = 0.08$, together with the no flow case $\theta = 0$. Numerical data show that q decreases with increasing θ for a given slope angle β , meaning that the water counter-flow slows down the avalanche. This is clearly due to the added resisting effect of the fluid. As for the flowing layer thickness, the granular flux q appears to be governed by $\tan \beta - \mu_s(\theta)$ as the different curves collapse in the plot of figure 15b. Thus the parameter $\tan \beta - \mu_s(\theta)$ appears to be the control parameter of the system that characterizes its out of equilibrium state. As we already found experimentally that the deviation $\mu_s(\theta) - \mu_s(0)$ between the values of the friction coefficient is roughly the same than the deviation $\tan \beta_r(\theta) - \tan \beta_r(0)$ between the values of the angle of repose (figure 8b), this explains why the experimental velocity profiles coincide (figure 8a) for same values of $\tan \beta - \tan \beta_r(\theta)$, which can be viewed also as a good experimental control parameter.

5. Conclusion

In this paper, we have presented experimental results concerning water immersed avalanches of small grains (in the so-called viscous regime) in a long and narrow channel of gap b , with or without a water counter-flow. Whatever the initial pile angle, even much larger than the maximum angle of stability, the slope relaxation corresponds to a quasi steady motion after a short transient. The pile slope β has been shown to be the sole control parameter for the granular flow. When a water counterflow characterized by the Shields number θ is imposed, the dynamics of the granular flow is slowed down, but all the results are similar if one considers the deviation of the pile angle from the corresponding angle of repose $\beta_r(\theta)$. These results have been well modelled using a unique granular friction coefficient depending on the local shear rate, together with taking into account the solid friction due to the lateral walls and also the fluid friction due to the possible water flow. Calculations have led to a granular flux scaling $q \sim (\tan \beta - \mu_s)^4$, which agrees satisfactorily with the experimental data. A consequence of this power law scaling of q is that the pile slope evolves in time as $t^{-1/3}$. Another key point is that the granular flux increases non linearly with the gap thickness of the cell ($q \sim b^3$) and seems to be independent of the grain diameter. The characteristic time of large amplitude avalanches on water immersed granular piles of small grains driven far from equilibrium decreases thus non linearly with the gap cell ($\sim b^{-3}$) and is independent of the grain diameter.

The authors are grateful to Olivier Pouliquen and Daniel Lhuillier for fruitful discussions. Frédéric Moisy, Raphaël Fischer and Sylvain Courrech du Pont are also acknowledged for their assistance concerning the use of PIV technique. This work has been supported by the ACI Jeunes Chercheurs 2114 of the Ministère Français de la Recherche.

Appendix

For the sake of convenience, let us introduce the parameter $h_m = b(\mu_m - \mu_s)/\mu_w$ corresponding to the maximal flowing layer thickness obtained for the largest slope angle $\beta = \arctan \mu_m$, beyond which the rheology is no longer valid. Integrating equation (4.6) twice with the boundary conditions $\gamma(h) = 0$ and $v(h) = 0$, one gets the following analytical expression for the granular flux q per unit width:

$$q(h) = q^* \cos \beta \frac{h_m^3}{b^3} \left[-\frac{h}{h_m} \left(\frac{1}{3} \left(\frac{h}{h_m} \right)^2 - \frac{3}{2} \frac{h}{h_m} + 1 \right) - \left(1 - \frac{h}{h_m} \right)^2 \ln \left(1 - \frac{h}{h_m} \right) \right]. \quad (\text{A } 1)$$

where $q^* = \alpha \phi I_0 \Delta \rho g b^3 / \eta$.

For small enough flowing layer thickness h (when compared to the maximal thickness h_m) corresponding to a moderate value of the pile angle, (A 1) can be developed at first order as

$$q(h) = q^* \frac{\cos \beta}{12b^3 h_m} h^4 + O(h^5). \quad (\text{A } 2)$$

The granular flux q appears to be a power function of h . As the flowing layer thickness h is proportional to $\tan \beta - \mu_s$ as shown by (4.5), the granular flux may be written as

$$q(\beta) \simeq \frac{q^* \cos \beta}{12\mu_w^3 (\mu_m - \mu_s)} (\tan \beta - \mu_s)^4. \quad (\text{A } 3)$$

Since the time derivative of the pile angle β is related to the granular flux q by equation (2.1) and considering a quasi-steady process, we can calculate the elementary angle variation $d\beta$ in the elementary time variation dt by

$$-\frac{d\beta}{\cos \beta (\tan \beta - \mu_s)^4} \simeq \frac{2q^*}{3\mu_w^3 (\mu_m - \mu_s) L^2} dt. \quad (\text{A } 4)$$

As $\cos \beta$ does not vary so much in the explore range of plie angles, (A 4) can be integrated.

Given an initial slope β_0 , the time evolution of β may thus be approximated by

$$\tan \beta(t) \simeq \mu_s + \left(\frac{\tau_c}{t + \tau_d(\beta_0)} \right)^{1/3}, \quad (\text{A } 5)$$

with the two time constants

$$\tau_c = \frac{\mu_w^3 (\mu_m - \mu_s) L^2 \overline{\cos \beta}}{2q^*}, \quad (\text{A } 6)$$

$$\tau_d(\beta_0) = \frac{\tau_c}{(\tan \beta_0 - \mu_s)^3}. \quad (\text{A } 7)$$

The parameter $\tau_d(\beta_0)$ is the time lag by which each $\beta(t)$ curve for a given initial slope β_0 has to be shifted in order to fit the main curve (which starts at $\arctan \mu_m$), whereas τ_c is an intrinsic time of the granular flow. This modelling predicts a decrease of β toward the asymptotic value $\arctan \mu_s$ in an infinite time. If one defines the time duration T of the avalanche as the time needed for the pile to relax from β_0 to the angle of repose β_r , the expression for T is

$$T \simeq \frac{\tau_c}{(\tan \beta_r - \mu_s)^3} - \tau_d(\beta_0). \quad (\text{A } 8)$$

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