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- **1** Experimental evaluation of the partial thermal energy compensation of hydrate
- 2 crystallization from cyclopentane-loaded porous activated carbon particles immersed in

3 brine

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11

12 Abstract

13 Hydrate-based desalination (HBD) is a potential water desalination technology that has been studied over the past decades. Recently, an HBD process based on hydrate formation from 14 cyclopentane (CP) loaded on porous activated carbon particles (PACP) was patented 15 ("Method for crystallizing clathrate hydrates, and method for purifying an aqueous liquid 16 using the clathrate hydrates thus crystallized", EP3153606, 2017). It is thought that the 17 crystallization of CP hydrates from CP adsorbed on PACP might cause partial thermal energy 18 19 compensation. Actually, the heat released by the exothermic hydrate crystallization should be partially balanced by the endothermic desorption of CP from the PACP. In order to 20 investigate this phenomenon, calorimetric and optical studies (heat flow and refractive index 21 22 measurements respectively) of hydrate formation in systems consisting of CP-saturated PACP immersed in brines (3.5 wt% NaCl and 8 wt% NaCl) were performed. Comparison of the 23 24 thermal energy measured directly (through the calorimetric study) - i.e. the energy produced by both hydrate crystallization and CP desorption - and the thermal energy measured 25

26	indirectly (deduced from the optical study) - i.e. the energy generated by hydrate
27	crystallization only - revealed a balanced energy ranging from 9 to 47 kJ/mol of
28	CP. Comparison of the latter with the differential enthalpy of CP desorption from PACP
29	suggests that the CP converted to hydrates was contained in the large pores of the PACP. It is
30	interesting to note that salinity had no significant impact on the degree of thermal energy
31	compensation obtained.
32	
33	Keywords: CP hydrates; CP-adsorption/desorption; activated carbon; energy
34	compensation; hydrate-based processes; desalination
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37	1. Introduction
38	
39	Hydrate-based desalination (HBD) is a potential water-desalination technology that was first
40	proposed by A. Parker in 1942 [1] and has received marked attention since the 1960s in order
41	to strengthen the water-energy nexus [2]. It is based on the formation of gas hydrates which,
42	once formed, are separated and dissociated to obtain desalinated water due to the fact that salt
43	ions do not participate in the hydrate structure [3]. Gas hydrates are ice-like compounds
44	formed by the association of water cages and small chemical compounds known as guests.
45	They generally form at relatively high pressures and low temperatures [4]. Some of them,
46	such as cyclopentane (CP) hydrates, can however form at atmospheric pressure. Hydrate
47	crystallization has been widely studied in the literature in different contexts such as natural
48	sediments [5–7], flow assurance [8–10] and hydrate-based processes [2,3,11–15]. A
49	significant number of water-guest systems and experimental set-up designs have been studied,
50	mainly to describe hydrate formation mechanisms [16,17] or hydrate crystal morphology [18-

51	20], to promote [21,22] or inhibit [8,23] hydrate formation, and to reduce the energy required
52	for hydrate crystallization [24–28]. The optimization of energy consumption for hydrate
53	crystallization, which is an exothermic reaction, has essentially been studied in the context of
54	an economically viable hydrate-based desalination process. In the studies published, the
55	authors generally tried to make the most of the endothermic energy produced by a reaction
56	which is exogenous to the system. For instance, He et al. (2018) and Babu et al. (2020)
57	attempted to make use of LNG regasification to cool the water to be desalinated [24,25]. He et
58	al. (2018) achieved a decrease in specific energy consumption of 27.42% and 24.61% for
59	3.5wt% NaCl and 7 wt% NaCl brines respectively [25].
60	The hydrate formation stage of a recently patented HBD process [29], which has the
61	particularity to use porous activated carbon particles (PACP) loaded with CP, was studied in a
62	previous paper [22]. The main results showed that the PACP act as both kinetic promoters and
63	a source of CP for hydrate formation. However, a relatively small amount of hydrates was
64	obtained (< 50% of the theoretical maximum amount of hydrates that could be formed) [22].
65	This was proven to be related to the fact that the CP found in the small pores of the PACP
66	remains trapped [30,31]. Based on this observation, PACP with predominantly large pores
67	were recommended for enhancing the process. In the present work, we focus on the energy
68	aspect of the hydrate formation stage in this HBD process, in which the energy supplied by
69	hydrate crystallization - exothermic reaction (-115.4 kJ/mol of CP [32]) - could possibly be
70	partially compensated by a reaction endogenous to the system, namely the desorption of CP
71	from the PACP, which is endothermic (+28 to +57 kJ/mole of CP [30]).
72	The main objective of the present work is to experimentally prove this partial thermal energy
73	compensation and determine its value. To do so, CP hydrates were crystallized from CP-
74	saturated PACP immersed in brines of 3.5 wt% NaCl and 8 wt% NaCl, at a subcooling
75	(difference between the hydrate equilibrium temperature and the experiment temperature) of

76	6°C. These salt concentrations mimic those of seawater [33] and produced water [11]
77	respectively. The experiments were carried out using both differential scanning calorimetry
78	(DSC) and refractive index measurements.
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81	2. Experimental section
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83	2.1. Materials and Apparatus
84	
85	CP (purity of 97%) was supplied by Sigma Aldrich. Deionized water (resistivity of 18.2
86	$M\Omega$.cm) was produced by a Purelab laboratory water-purification system. Sodium chloride
87	(NaCl) (purity of 99.5%) was purchased from Acros Organics. A grade of PACP called BGX,
88	supplied by Chemviron SA (Belgium), was used for the hydrate formation experiments. BGX
89	is granular activated carbon with an average particle size of about 1 mm and a pore size
90	distribution that has the specificity of being developed in both the meso- and macroporous
91	regions in addition to the more standard microporous range (see SM-1 and SM-2). Their CP-
92	adsorption capacity is 0.96 ± 0.02 g of CP/g of BGX at 1°C (see SM-3). A closed vessel and a
93	set of resealable glass flasks with a 5-ml capacity were used for the CP-saturated PACP
94	preparation. Plastic syringes (3-mL capacity) and cellulose acetate syringe filters (0.8- μ m
95	mesh size), used to sample and filter the unconverted water at the end of the hydrate
96	formation experiments, were purchased from Sodipro.
97	A vacuum preparation apparatus called VacPrep™ (from Micromeritics) was used to purify
98	the PACP samples under primary vacuum at 200°C. The samples were weighed using an
99	ALC-110.4 balance (from Accurlab ®) with an uncertainty of 10 ⁻⁴ g. A universal convection
100	incubator (from Memmert®) was used to impose the chosen temperature on the closed vessel,

101	in which the PACP are placed to be saturated with CP (cf. paragraph 2.2.). Hydrate formation
102	was performed in the measurement cell (7-cm ³ capacity) of a Tian-Calvet BT2.15 calorimeter
103	(from Setaram Instrumentation). The uncertainty with regard to the measured energy is 4%
104	(see SM-4).
105	The refractive index nD (at a wavelength of 589.3 nm) of the water samples was measured
106	using an Abbemat 550 refractometer (from Anton Paar) with an accuracy of ± 0.00001 .
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108	2.2. Preparation of the CP-saturated PACP
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110	The saturation of PACP with CP was performed as follows: 0.54 g of BGX were purified at
111	200°C under primary vacuum for 12 hrs. Using a glass funnel, 0.500 ± 0.005 g of this hot
112	sample was immediately transferred to a resealable glass flask, which was then introduced
113	into the closed vessel partially filled with liquid CP (Fig. 1). This in turn was placed in the
114	incubator at $1.0 \pm 0.5^{\circ}$ C. The PACP were left in contact with saturating CP vapor for 48 hrs to
115	saturate their pores with CP.
116	



118 **Fig. 1.** Preparation of CP-saturated PACP

120 2.3. Investigation into the CP desorption-CP hydrate crystallization thermal energy 121 compensation

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CP hydrates were formed in systems composed of CP-saturated BGX immersed in brine (3.5 123 wt% NaCl and 8 wt% NaCl). In order to evaluate whether or not the thermal energy 124 consumed by CP desorption from the PACP partially compensates the thermal energy 125 released by hydrate crystallization, the thermal energy compensation was assessed by 126 127 comparing the thermal energy measured in the DSC hydrate formation experiments (referred 128 to as direct measurement) with the value deduced from the refractive index measurements of the unconverted water sampled at the end of the hydrate formation experiments (referred to as 129 indirect measurement). The former corresponds to the energy $E_{des+crys}$ generated by CP-130 desorption and hydrate crystallization, whereas the latter corresponds to the energy E_{crys} 131 generated by hydrate crystallization only. 132

For this experiment, 0.500 ± 0.005 g of CP-saturated BGX and 4.15 g (or 4.35 g) of 3.5 wt% 133 NaCl (or 8 wt% NaCl) solution were introduced into the measurement cell of the BT2.15 134 calorimeter along with a few CP-hydrate crystals prepared beforehand (see Fig.2). These 135 hydrate crystals were added to initiate hydrate crystallization by using the so called 136 137 "memory effect". Memory effect is a phenomenon resulting from the non-complete dissociation of hydrate structure which reduces the time required to initiate hydrate formation 138 139 [4]. The PACP, NaCl solution and cell were all precooled to the equilibrium temperature T_{eq} (5.5°C and 2.8°C for the 3.5 wt% NaCl and 8 wt% NaCl solutions respectively [22]). The cell 140 was then introduced into the calorimeter, which was set at a temperature 0.2°C above T_{eq} in 141 142 order to prevent (or at least limit) the added hydrate crystals from melting. The system was 143 maintained at this temperature for one hour (stage (a) in Fig. 3) so that the thermal signal (heat flow) caused by the introduction of the cell into the calorimeter should reach the 144 145 baseline and the added hydrate crystals should melt slowly. Then, the system temperature was decreased to the target temperature ($T_{eq} - 6^{\circ}C$), at a cooling rate of 1°C/min, and maintained 146 for 24 hrs (stage (b)). After 24 hrs of hydrate formation, the cell was removed from the 147 calorimeter, a sample of the residual (unconverted) NaCl solution was collected and filtered, 148 149 and its refractive index was measured (stage (c)).

150 $E_{des+crvs}$, deduced from the direct measurements, was obtained by integrating the thermal peak generated by subtracting the "blank" thermogram (obtained in a similar fashion but 151 without CP) from the "experiment" one (see Fig. 4). The "blank" thermogram (brown curve 152 in Fig. 4) only takes into account the heat flow deviations due to the temperature 153 154 programming and mass difference between the "measurement" and "reference" cells. Thus, the resulting thermogram "Experiment minus Blank" (blue curve in Fig. 4) only shows the 155 156 heat flows due to both the CP desorption from the PACP and the hydrate crystallization, and its integration gives $E_{des+crvs}$. 157

 E_{crys} , deduced from the indirect measurements, was obtained by first determining the salinity 158 [NaCl]_{24h} of the unconverted solution - concentrated with salt as hydrates formed - from the 159 160 measured refractive index and a previously generated "nD-[NaCl]" calibration curve (see SM-5). Based on this, the water-to-hydrate conversion (WHC) and the water-to-hydrate amount 161 (WHA) were determined using equations 1 and 2 respectively. The stoichiometric ratio of CP 162 to water in the CP hydrates (1 mole of CP:17 moles of water) served to determine the amount 163 of CP-to-hydrates obtained (CPHA) (equation 3). The hydrate formation energy was deduced 164 from the CP-hydrate dissociation enthalpy $(115,400 \pm 7,600 \text{ J/mole of CP} \text{ (Delroisse et al.,}$ 165 2018)) using equation 4. 166 $WHC(\%) = 100 - \frac{100 \cdot [NaCl]_i \cdot (100 - [NaCl]_{24h})}{(100 - [NaCl]_i) \cdot [NaCl]_{24h}}$ 167 (1) $WHA(g) = m_{iw} * WHC(\%)$ 168 (2)where $[NaCl]_i$, $[NaCl]_{24h}$ and m_{iw} are the initial water salinity (3.5 wt% NaCl or 8 wt% 169

170 NaCl), the final water salinity (after 24 hrs.) and the initial pure-water mass respectively.

171
$$CPHA(g) = \frac{WHA*(17*18)}{70.13}$$
 (3)

172
$$E_{crys}(J) = \frac{CPHA*115400}{70.13}$$
 (4)

The uncertainties as regards $E_{des+crys}$ were determined as the sum of experiment repetition and calibration-control deviations, whereas the uncertainties as regards E_{crys} were calculated from the experiment-repetition deviation, the calibration curve deviation, the refractometer accuracy, and the uncertainty regarding the dissociation enthalpy.



Fig. 2. Preparing the system for the hydrate formation experiment in the calorimetric cell of
the BT2.15 apparatus. 1) The measurement cell, 2) hydrate seed, 3) CP-saturated PACP, and
4) brine

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187 3. Results and discussion

- 189 Fig. 4 shows the resulting thermal peak (green curve) obtained after subtracting the "blank"
- 190 thermogram (brown curve) from the "experiment" one (blue curve) for both NaCl solutions.
- 191 The superposition of the thermal peaks obtained in experiments 1 and 2 shows a good

192 reproducibility for each salinity (Fig. 5). The average values of $E_{des+crys}$ obtained by



Fig. 4. Thermal energy peak (green curve) generated by subtracting the "blank" thermogram
(brown curve) from the "experiment" thermogram (blue curve) for the 3.5 wt% NaCl solution
(left) and 8 wt% NaCl solution (right)

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Fig. 5. Comparison of the thermal energy peak obtained in two repeated experiments with the 3.5 wt% NaCl solution (left) and the 8 wt% NaCl solution (right). The values of $E_{des+crys}$ were obtained by integrating the peaks.

The thermal energy values E_{crys} deduced from the indirect measurements for the same systems are given in Table 1. The refractive indexes (nD) measured after 24 hrs of hydrate formation in experiments 1 and 2 are in good agreement which indicates a good reproducibility (difference of less than 0.002%).

209

		3.5 wt% NaCl	8 wt% NaCl
nD	Exp. 1	1.340402	1.348213
at $t = 24 h$	Exp. 2	1.340376	1.348220
	Average	1.340390 ± 0.00001	1.34822 ± 0.00001
[NaCl] _{24h} (wt%)		4.23 ± 0.01	8.71 ± 0.01
WHC (%)		18.0 ± 0.4	8.70 ± 0.25
WHA (g)		0.72 ± 0.02	0.35 ± 0.01
CPHA (g)		0.160 ± 0.004	0.080 ± 0.002
E_{crys} (J)		271 ± 24	131 ± 12

210 **Table 1.** Indirect measurement of hydrate formation energy

211

As can be seen in Table 2, $E_{des+crys}$ is lower than E_{crys} . The difference in energy (E_{crys} – 212 $E_{des+crys}$) is in fact the balanced energy. Since the PACP are initially saturated with CP, 213 meaning that the CP is found only within the pores, the balanced energy can thus be fully 214 attributed to CP desorption. While assuming that all the CP desorbed from the PACP is 215 converted to hydrates (i.e. the desorbed-CP amount is equal to CPHA), the balanced energy 216 value, calculated as the ratio of $(E_{crys} - E_{des+crys})$ to CPHA (in mol), is between 9 (=28-19) 217 kJ/mol of CP and 47 (=28+19) kJ/mol of CP. The balanced energy can be compared to the 218 differential enthalpy of CP desorption (the opposite of the differential enthalpy of CP 219 adsorption on PACP), which ranges from 28 to 57 kJ/mol of CP. The differential enthalpy of 220

- CP desorption was measured in a previous paper for two different activated carbons (see SM6) [30] using the calorimetric-manometric technique [34]. The similarity of the curves
 indicates a general range of values for CP adsorbed on an activated carbon. For the sake of
 comparison, the balanced energy range and the differential enthalpy of CP desorption from
 PACP are plotted in the same figure (Fig. 6).

227	Table 2. Determination of the balanced energy per mole of Cl	Р
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	3.5 wt% NaCl	8 wt% NaCl
E _{des+crys} (J)	204 ± 16	100 ± 7
E _{crys} (J)	271 ± 24	131 ± 12
CPHA (g)	0.16	0.08
	$(2.3 \ 10^{-3})^*$	(1.1 10 ⁻³)*
Balanced energy (J)	67 ± 40	31 ± 19
Balanced energy (kJ/mol CP)	29 ± 17	28 ± 19

^{*}value of CPHA in mol

Fig. 6. Comparison of the balanced energy obtained in the case of hydrate formation from CPsaturated PACP (green area), and differential enthalpy of CP desorption from PACP (blue and
black dots) [30]

234

235 As can be seen in Figure 6, the former (green area) does not cover the entire range of the latter (dots), which confirms that part of the CP did not desorb from the PACP (and therefore did 236 237 not participate in the formation of hydrates). The high enthalpy values (48 to 57 kJ/mol of CP) of the uncovered dots correspond to the filling of pores at the lowest pressures (0 < P_{eq}/P_{sat} <-238 0.02) [30] *i.e.* the smallest pores, mainly micropores, where the prevailing interactions are 239 240 fluid-solid. The non-desorbed CP was therefore trapped in these pores. The enthalpy values of 241 the covered dots (28 to 48 kJ/mol of CP) correspond to medium-to-high-pressure filling of the meso- and macropores (~ $0.02 < P_{eq}/P_{sat} < 1$) [30]. Hence, CP that desorbed from the PACP to 242 243 form hydrates was contained in these pore ranges where the prevailing interactions are solidfluid-fluid and fluid-fluid interactions. One can see that the balanced energy range obtained 244 was almost the same for both salinities (3.5 wt% NaCl and 8 wt% NaCl), suggesting no 245 significant effect of salt on this phenomenon. This result makes sense since the balanced 246 energy was found to be related to the CP-desorption energy. The balanced energy (+9 to +47 247 248 kJ/mol of CP) implied a thermal energy compensation of between 8% and 40% of the energy supplied by hydrate crystallization. The (positive) balanced energy (+9 to +47 kJ/mol of CP) 249 implied a thermal energy compensation of the (negative) energy supplied by the hydrate 250 251 crystallization (-115.4 kJ/mol of CP). Its value, calculated as the ratio of the balanced energy to the dissociation enthalpy of CP hydrates, is between 8% (=100×9:115.4) and 40% 252 (=100×47:115.4). 253

The investigation into the thermal energy compensation together with the assumption that (some) water molecules can enter the pores of PACP [16,31] lead us to propose a mechanism

for CP-hydrate formation from CP-saturated PACP (Fig. 7). In the smallest pores, the fluidsolid interactions prevent CP from desorbing and thus from participating in hydrate formation.
In larger pores, the prevailing interactions (solid-fluid-fluid and fluid-fluid interactions) allow
the desorption of CP (or at least part of it). In this case, hydrate formation can occur outside
and/or inside the pore.

It should be noted that the surface chemistry of the PACP is reported to impact (promote or inhibit) hydrate crystallization [8,16,35]. However, in the case of our investigated system, the low-size pores of PACP, where the specific surface is significant and thus also the surface chemistry effects could be, do not participate to hydrate formation as previously explained. Therefore, the role of surface chemistry is probably not critical compared to that of pore size.

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269 Fig. 7. Proposed prevailing mechanisms of hydrate formation from CP-saturated PACP

- 270 immersed in water
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- 272
- **4. Conclusions**
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In this work, the partial thermal energy compensation that may occur during hydrate 275 276 formation from CP adsorbed in PACP was investigated in brines with salt concentrations 277 typical of seawater (3.5 wt% NaCl) and produced water (8 wt% NaCl). A combination of differential scanning calorimetry and refractive index measurements were used to determine 278 279 the thermal energies released by both the hydrate crystallization and CP desorption from the PACP ($E_{des+crvs}$), and by the hydrate crystallization alone (E_{crvs}). The balanced energy 280 $(E_{crys} - E_{des+crys})$ was found to range between 9 and 47 kJ/mol of CP for both salinities, 281 which means that it might be possible to save 8% to 40% of the energy required by hydrate 282 crystallization in hydrate-based desalination processes. This energy can be attributed to the 283 desorption of CP from the large pores of the PACP. This result demonstrates that the CP 284 converted to hydrates was contained by the largest pores of the PACP, and that the part of CP 285 adsorbed in the smallest ones remained trapped. In the light of these results, a mechanism of 286 hydrate formation in these types of CP-saturated PACP has been proposed. 287

288

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404 Supplementary Material

Quantachrome IQ)

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408

- 406 SM-1
- 407 Fig. S1. PSD and cumulative PV determined using gas porosimetry (Ar isotherms at 87K on

411 SM-2

412 Fig. S2. cumulative PV determined using mercury intrusion porosimetry (Micromeritics

413 Autopore IV)

417 <u>Determination of the CP-adsorption capacity of BGX</u>

418 To perform CP-adsorption capacity measurements, the PACP were purified at 200° C for 12

419 hrs under primary vacuum. Using a glass funnel, the hot purified sample was directly

420 transferred into a small closable flask (5-mL capacity), which was then weighed and

421 introduced into the CP adsorption chamber (closed-vessel partially filled with a flask of liquid

422 CP). The PACP were only in contact with CP vapor (cf. Figure S1). The CP adsorption

423 chamber was placed in the incubator at $1.0 \pm 0.5^{\circ}$ C. After 48 hrs of adsorption, the flask was

424 weighed again and the CP-adsorption capacity of the PACP was determined. The experiment

425 was repeated 3 times to check the results.

426

427 **SM-4**

Fig. S3. dissociation of ice used to determine the uncertainties associated with the DSCmeasurements

The calibration curve [NaCl] vs. nD was obtained by measuring the refractive index (nD) of previously prepared NaCl solutions of known concentrations [NaCl]. The linear regression of the [NaCl] vs the nD plot gave the following equation: $[NaCl] = 573.044 \times nD - 763.87$. The uncertainties regarding the slope and the offset were determined using the DROITEREG

function method ($\Delta a = 0.18704$; $\Delta b=0.25096$). The uncertainties Δ [NaCl] and Δ WHC

regarding the salinity determined and the water-to-hydrate conversion (WHC) respectively,

442 were obtained by differentiating the calibration equation and equation 1. Finally, ΔE_{crvs} was

obtained in a similar fashion after determining Δ WHA, Δ CPHA from the differentiation of

- equations 2 and 3.
- 445
- 446 SM-6

447 Gbac and ChemA are the notation used for G-BAC-G70R and Chemviron-A, which are two

different PACP manufactured by Keruha Gmbh and Calgon, respectively. The differential

enthalpies of CP-adsorption on these PACP were measured in a previous work [30], and they

450 showed almost the same values despite their different origins and characteristics. The

similarity of the obtained results indicates a general range of values for CP adsorption on

- 452 activated carbons.
- 453 Table S1. Origin and characteristics of Gbac and ChemA

	Gbac	ChemA
Origin	Petroleum pitch	Coconut
Particle size (µm)	700	<177
Principal pore size (nm)	5.5 ; 0.79	5.5 ; 0.79; 1.3

454