

# **Nitro-Decorated Microporous Covalent Organic Framework (TpPa-NO 2 ) for Selective Separation of C 2 H 4 from a C 2 H 2 /C 2 H 4 /CO 2 Mixture and CO 2 Capture**

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## ARTICLE

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## **Nitro Decorated Microporous Covalent Organic Framework (TpPa-NO2) for Selective Separation of C2H<sup>4</sup> from C2H2/C2H4/CO<sup>2</sup> Mixture and CO<sup>2</sup> Capture**

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ABSTRACT: A nitro-decorated microporous covalent-organic framework (COF), TpPa-NO<sub>2</sub>, has been synthesized in gramscale with one-pot reaction. It can effectively selective separate  $C_2H_4$  from  $C_2H_2/C_2H_4/CO_2$  mixture and capture CO<sub>2</sub> from  $CO<sub>2</sub>/N<sub>2</sub>$  based on IAST calculations and transient breakthrough experiments. Theoretical calculations demonstrated that the hydrogen atom of imine bonds, carbonyl oxygen and nitro groups show high affinity toward  $C_2H_2$  and  $CO_2$  and play vital roles in the separation. The separation of the separation of the separation. The separation of  $\mathbf{r}$ 

In 2020, global energy demand is estimated to be 557.10 exajoules (EJ), and fossil fuel accounts for 83.152%. $^{1}$  The resultant global warming has led to sea level rise and more extreme weather events like heatwaves and heavy rainfalls. $^2$  Due to the COVID-19 pandemic and clean energy growing, the energy consumptions and carbon emissions have fallen by 4.5% and 6%, respectively. However, the rate of carbon emission decline is barely similar to what the world needs to do to meet the aims of the Paris Agreement. Two important methods for emission reductions are reducing energy consumption and carbon capture & sequestration. Statistics show that industrial separation processes, such as light hydrocarbon separation and carbon capture from flue gas, accounted for 10-15% of the world's total energy consumption in 2016. $^3$  Light hydrocarbon (LH) separation rely on the high energy demand process, distillation. Carbon capture using aqueous amine solutions strategy suffers not only high energy consumption, but also solvent distillation, water use, and equipment corrosion. Hence developing alternative LHs separation and efficient  $CO<sub>2</sub>$  capture techniques with low energy consumption and mild operating conditions would decrease the global energy demand and carbon emission.

Because its energy efficiency, high working capacity and high selectivity, physical sorption separation utilizing porous solids materials offers a promising alternative to the established energy intensive processes for LHs separation/purification and  $CO<sub>2</sub>$ 

capture. One of the most pressing issues for this technology is lack of low-cost and efficient physisorbents. The similar kinetic diameters and boiling points of  $C_2H_2$ ,  $C_2H_4$  and  $CO_2$ , make the design of robust physisorbents with simultaneously high uptake and selectivity extremely challenging. Porous materials such as porous silica<sup>4</sup>, activated carbons,  $5$  zeolites,  $6$  porous aromatic frameworks (PAFs),<sup>7</sup> metal-organic frameworks(MOFs), $8-11$  metal-organic cages  $(MOCs)$ ,  $12-14$  and covalent organic frameworks $(COFs)$ <sup>15-19</sup> etc. are potential candidates with excellent adsorption capacity and selectivity. Among them, COFs are a new type of crystalline framework materials built with strong covalent bonds between light elements (C, B, N, O, Si, B, etc.) using the design principles of 'reticular chemistry'.<sup>20</sup> They exhibited low density, remarkably high thermal stability, high surface area, readily adjustable pore size, and outstanding structural flexibility.<sup>21</sup> COFs have been widely investigated for applications in gas storage and separation,  $4, 17, 22, 23$ catalysis,<sup>24, 25</sup> clean energy conversion,<sup>26</sup> sensing,<sup>27, 28</sup> and energy storage.<sup>29, 30</sup> As porous framework materials, COFs have been regarded as an ideal physisorbents for LH separation and $^{17, 19, 31}$  CO<sub>2</sub> capture separation in the past decade.<sup>16, 23, 32, 33</sup> For example, Zhu and co-workers synthesized a COF (PAF-110) which exhibit selective adsorption of  $C_2H_2$  over  $C_2H_4$  as its carbonyl oxygen provided higher affinity for acetylene than ethylene.<sup>19</sup> Jiang's group introduced carboxylate groups onto the pore surface of COFs to increase the affinity towards  $CO_2$ .<sup>16</sup> Lai and co-workers synthesized CAA-COF-1 and CAA-COF-2. The former one contain electron-rich chlorine atoms and enhanced  $CO<sub>2</sub>$  adsorption capacity (by almost 28-44%) compared to the latter one.<sup>23</sup> Han and co-workers synthesized a perfluorinated covalent triazinebased framework (FCTF-1). Compared with the unfluorinated CTF-1, FCTF-1 displayed significantly reduced pore size, from microporous to ultramicroporous (0.5 nm), and resulted in improved  $CO<sub>2</sub>/N<sub>2</sub>$  selectivity in a mixed gas breakthrough test.<sup>32</sup> These researches show that introducing functional groups to the pore walls of COFs can increase the host-guest interactions to improve the adsorptive selectivity and facilitate the separation processes. Banerjee group reported

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*Electronic supplementary information (ESI) available: Experimental details, materials synthesis, additional structural figures, crystallographic refinement details, PXRD, TGA curves, gas adsorption results. See DOI: 10.1039/x0xx00000x*

### **ARTICLE Journal Name**

 $\text{TPPa-NO}_2$ , which possesses imine backbone and  $\text{-NO}_2$  group functionalized pore walls. TpPa-NO<sub>2</sub> was first synthesized by means of a twin screw extruder, $11$  which is difficult to obtain for common lab and unsuitable for small amount synthesis. In 2020, Luo and coworkers synthesized  $TpPa-NO<sub>2</sub>$  by solvothermal method at milligram-scale using solvethermal method.<sup>34</sup> However, the synthesis scale was too small to produce samples for transient column breakthrough separation.

Herein, we report the gram-scale synthesis of  $\text{TpPa-NO}_2$  using onepot reflux method, and investigation of its performance in  $C_2H_4$ selective separation from  $C_2H_2/C_2H_4/CO_2$  mixture as well as  $CO_2$ capture from flue gas. Structure simulation and powder X-ray diffraction (PXRD) pattern demonstrate that the scale up synthesis produced crystalline and pure  $TpPa-NO<sub>2</sub>$  in AA packing mode. Single component gas adsorption experiments and theoretical calculations certify that introduction of -NO<sub>2</sub> can improve the adsorption selectivity and enhance the adsorbate−adsorbent interaction. The transient breakthrough experiments prove that  $TpPa-NO<sub>2</sub>$  can separate  $C_2H_4$  from binary ( $C_2H_2/C_2H_4$ ) and ternary ( $C_2H_2/C_2H_4/CO_2$ ) mixtures while it can also effectively capture  $CO_2$  from  $CO_2/N_2$ (15:85) mixture simulating flue gas. The excellent  $C_2H_4$  and  $CO_2$ adsorption selectivity is attributed to the -NO<sub>2</sub> groups and the hydrogen atoms of the imine bonds based on theoretical calculations. Moreover, the outstanding durability, easy regeneration, and excellent thermal and chemical stability of TpPa- $NO<sub>2</sub>$  suggest that it can be applied to industrial  $C<sub>2</sub>H<sub>4</sub>$  purification process and  $CO<sub>2</sub>/N<sub>2</sub>$  separation.



Figure 1. a) Synthetic scheme of  $TpPa-NO_2$ . Graphic view of the slipped AA stacking structure of  $T$ pPa-NO<sub>2</sub> (b, along a/b axis; c, along c axis) Hydrogen atoms are omitted for clarity. Color scheme: pink, Pa-NO<sub>2</sub>; blue, Tp; turquoise, –NO<sub>2</sub> groups.

TpPa-NO<sub>2</sub> was synthesized using the one-pot reflux method by solvothermal reaction modified from the literature. $34$  2,4,6triformylphloroglucinol (Tp) and 2-nitor-1,4-phenylenediamine (Pa-NO<sup>2</sup> ) were dissolved in 1,4-dioxane and 1,3,5-trimethylbenzene with p-toluenesulfonic acid monohydrate as the template. The reaction mixture was refluxed under nitrogen protection at 120 $\degree$ C for 72 hours (Figure 1a). The condensation produced scarlet powder in 87% isolation yield. The infrared (IR) spectrum of TpPa-NO<sub>2</sub> shows that the stretching vibration bands of C=N and C=O at 1617 and  $1640 \, \text{cm}^{-1}$ ,<sup>35, 36</sup> respectively, proving the success of the aldoamine condensation reaction (Figure S1 in the Supporting Information). The morphology of  $TpPa-NO<sub>2</sub>$  was examined by scanning electron microscopy (SEM), which shows a large quantity of uniform nanofibers, thus implying its phase purity (Figure S2b). The structural simulation predicted that  $\text{TPa-NO}_2$  in AA packing mode has one-dimensional channels along the c-axis with a diameter of 15 Å while the layers stack with an interlayer distance of 3.46 Å (Figure 1). The framework of TpPa-NO<sub>2</sub> is stable in ambient air and retains its crystallinity after heating to 300  $^{\circ}$ C in air (Figure S3-4). It is also stable after soaking in a variety of organic solvents, concentrated acid (12 M HCl & 2 M  $H_2SO_4$ ), or hot water (85 $^{\circ}$ C) for one week. while it can stay in basic aqueous solutions (2 M NaOH) for 48 hours (Figure S5). The specific surface area was determined to be 398  $m^2 g^{-1}$  from N<sub>2</sub> sorption isotherms at 77K, lower than the literature reported value (850  $m^2$   $g^{-1}$ ). Pore size distribution calculated by using the quenched solid density functional theory (QSDFT) method resulted in a pore size of 1.5 nm (Figure S6 & S7), matching the simulated AA-packing mode structure model.

Intrigued by its high crystallinity, microporous channels, excellent chemical and thermal stability, imine porous backbone, polar functional groups  $(-NO_2)$ ,<sup>37</sup> we expect that TpPa-NO<sub>2</sub> has high adsorption affinity for  $CO<sub>2</sub>$  and can make gas molecules diffuse differently, suitable for separation industrial gases with similar kinetic diameter such as  $CO_2(3.3 \text{ Å})$ , N<sub>2</sub>(3.64 Å), C<sub>2</sub>H<sub>2</sub>(3.3 Å), C<sub>2</sub>H<sub>4</sub> (4.16 Å).



Figure 2.  $C_2H_2$ ,  $C_2H_4$ ,  $CO_2$  and  $N_2$  adsorption isotherms of TpPa-NO<sub>2</sub> at a) 273 and b) 298 K, respectively. c) Isosteric heat of  $C_2H_2$ ,  $C_2H_4$ and  $CO_2$ , adsorption  $(O_{st})$  of TpPa-NO<sub>2</sub> as a function of surface coverage. d) IAST selectivity of TpPa-NO<sub>2</sub> for different binary gas mixture at 298 K.

Single component adsorption isotherms of  $C_2H_2$ ,  $C_2H_4$ ,  $CO_2$  and N<sub>2</sub> for TpPa-NO<sub>2</sub> were collected at 273 and 298 K, respectively (Figure 2a & b). The isosteric heat of adsorption  $(Q_{st})$  plots were calculated using the Clausius-Clapeyron equation (Figure 2c Figure  $S(8-10).$ <sup>38, 39</sup> As expected, TpPa-NO<sub>2</sub> shows excellent CO<sub>2</sub> uptake under 273 K (78.3cm<sup>3</sup>  $g^{-1}$ ) and 298 K (49.52cm<sup>3</sup>  $g^{-1}$ ) at 1bar, similar

to those of C<sub>2</sub>H<sub>2</sub> (79.03 cm<sup>3</sup> g<sup>-1</sup> at 273 K and 49.92 cm<sup>3</sup> g<sup>-1</sup> at 298 K), respectively. The  $Q_{st}$  for CO<sub>2</sub> was 37.83 kJ mol<sup>-1</sup> at the zero coverage, and higher than that of  $C_2H_2$  (33.42 kJ mol<sup>-1</sup>). For most porous materials the adsorption capacity and  $Q_{st}$  of  $C_2H_2$  is always higher than those of CO<sub>2</sub>.<sup>10, 37</sup> Due to the larger kinetic diameter (4.16 Å) and smaller quadrupole moment  $(1.50 \times 10^{26} \text{ e}^2 \text{ s})$  of  $C_2H_4$ compared with of  $CO<sub>2</sub>$  (3.3 Å and  $4.30 \times 10^{26}$  esu cm<sup>2</sup>),<sup>40</sup> the adsorption capacity of C<sub>2</sub>H<sub>4</sub> (50.57 cm<sup>3</sup> g<sup>-1</sup> at 273 K and 20.74 cm<sup>3</sup> g<sup>-</sup> <sup>1</sup> at 298 K) is much lower than that of CO<sub>2</sub> and C<sub>2</sub>H<sub>2</sub>. N<sub>2</sub> keeps its consistent behavior of not being adsorbed under 273/298 K. To our surprise, the adsorption capacity of  $C_2H_4$  seems to be more susceptible to temperature changes than  $C_2H_2$  and  $CO_2$  gases.

Increasing temperature can obviously reduce the uptake of  $C_2H_4$ (Figure 2a & b), which implied that  $C_2H_4$  may have the highest  $Q_{st}$ . Subsequent  $Q_{st}$  calculation (60.22 kJ mol<sup>-1</sup>) certified this speculation (Figure 2c). The adsorption selectivities of  $\text{TPPa-NO}_2$  for binary mixtures of  $CO_2/N_2$  (15:85 v/v),  $C_2H_2/C_2H_4$  (1:99 v/v),  $C_2H_2/CO_2$ (10:90 v/v), and  $CO_2/C_2H_4$  (10:90 v/v) were calculated using the ideal adsorption solution theory (IAST) based on the single component adsorption data (Figure 2d).<sup>38, 39</sup> From 0.01 to 1 bar at 298 K, TpPa-NO<sub>2</sub> presents excellent  $CO<sub>2</sub>/N<sub>2</sub>$  selectivity (477.33-128.92), while its selectivity of  $C_2H_2/C_2H_4$  (1:99 v/v),  $C_2H_2/CO_2$  (10:90  $v/v$ ) and  $CO_2/C_2H_4$  (10:90 v/v) were 27.15-8.22, 2.40-1.48 and 8.64-4.71, respectively.



Figure 3. Transient breakthrough curves and cycling tests of TpPa-NO<sub>2</sub> for a/d) C<sub>2</sub>H<sub>2</sub>/C<sub>2</sub>H<sub>4</sub>(1:99 v/v), b/e) C<sub>2</sub>H<sub>2</sub>/C<sub>2</sub>H<sub>4</sub>/CO<sub>2</sub> (1/90/9, v/v/v), and  $c/f$ ) CO<sub>2</sub>/N<sub>2</sub> (15/85, v/v) mixture at 298K and 1bar, respectively.  $(C/C_0,$  outlet concentration/feed concentration)

To further confirm the separation performance of TpPa-NO<sub>2</sub>, transient breakthrough experiments for  $C_2H_2/C_2H_4$  (1:99 v/v),  $C_2H_2/C_2H_4/CO_2$  (1/90/9, v/v/v) and  $CO_2/N_2$  (15/85, v/v) mixtures were carried out at 298 K (Figure 3). Firstly, binary gas mixtures  $C_2H_2/C_2H_4$  (1:99 v/v) was tested.  $C_2H_4$  broke through the packed bed and yielded purity  $C_2H_4$  (>99.9%) at first only need 20 minutes after the start, whereas after 42 minutes  $C_2H_2$  slowly eluted and reached equilibrium at 70 minutes (Figure 3a). For further examining the separation ability of TpPa-NO<sub>2</sub> in more complex gas mixture systems, ternary mixture was used. The outlet time of  $C_2H_4$  (15 min) and  $C_2H_2(30 \text{ min})$  maintained while CO<sub>2</sub> eluted as the second gas at 25 min (Figure 3b). The capture capacity of  $C_2H_4$ ,  $CO_2$  and  $C_2H_2$  were 1,39, 0,231 and 0.0416 mmol, respectively, Hence  $C_2H_4$  can still be separated from the ternary mixtures. For simulated carbon capture in flue gas  $(CO_2/N_2:15/85, v/v)$ , N<sub>2</sub> eluted first as a result of weak adsorbate−adsorbent interaction; whereas  $CO<sub>2</sub>$  was captured in the column until its saturated sorption and then breakthrough, with the  $CO<sub>2</sub>$  capture capacity of 0.51 mol  $g<sup>-1</sup>$  (Figure 3c). Furthermore, cycling breakthrough experiments on TpPa-NO<sub>2</sub> were carried out under the same conditions. The breakthrough curves for  $C_2H_2/C_2H_4$ ,

 $C_2H_2/C_2H_4/CO_2$ , and  $CO_2/N_2$  mixtures in 3 cycles tests were consistent, manifesting that  $TpPa-NO<sub>2</sub>$  has good stability and regenerability.

To understand the separation mechanism, first-principle density functional theory (DFT) calculations were employed to investigate the gas adsorption sites and host-guest interactions of  $\text{TPPa-NO}_2$ . Generally, the gases are held by the weak van der Waals (vdW) force (the C…H, O…H and C…O interactions) at the channel aperture. As shown in Figure 4, the strongest interaction of  $C_2H_2$  comes from the O...H interaction (2.27 Å) between the C<sub>2</sub>H<sub>2</sub> and the carbonyl oxygen of TpPa-NO<sub>2</sub> (Figure 4a). For  $C_2H_4$ , except the C...H interactions (2,83 Å) between the  $C_2H_4$  and imine backbone, the O...H interactions (3.22 Å & 3.56 Å) provided by -NO<sub>2</sub> and carbonyl oxygen of TpPa-NO<sub>2</sub> also contribute to holding the  $C_2H_4$  (Figure 4b).  $CO<sub>2</sub>$  was held by the O...H interactions (2.79 $\approx$ 3.1 Å) between the H atoms of imine backbone and  $CO_2$ , and the C...O interaction (2.97 Å) between the carbonyl oxygen of TpPa-NO<sub>2</sub> and carbon atoms of  $CO<sub>2</sub>$ (Figure 4c).

### **Conclusions**

In summary, we have successfully achieved the gram-level synthesis of COF (TpPa-NO<sub>2</sub>) in one-step synthesis using the one-pot reflux method. Its  $C_2H_4$  selective separation and  $CO_2$  capture performance has been systematically studied. TpPa-NO<sub>2</sub> exhibit high IAST selectivity of 8.22 and 128.92 for  $C_2H_2/C_2H_4$  (1:99) and  $CO<sub>2</sub>/N<sub>2</sub>$  (15:85) at 298 K and 1 bar, respectively. Breakthrough experiments further confirmed that TpPa-NO<sub>2</sub> can separated  $C_2H_4$ from  $C_2H_2/C_2H_4$  and  $C_2H_2/C_2H_4/CO_2$  mixtures while it can also effectively capture  $CO_2$  from  $CO_2/N_2$ . DFT calculations revealed that the H of imine group, carbonyl oxygen and -NO<sub>2</sub> imposed the strong influence for  $CO_2$ ,  $C_2H_2$  and  $C_2H_4$ . The outstanding durability, easy regeneration, excellent thermal and chemical stability of TpPa-NO<sub>2</sub> offer a promising application potential for high value-added light hydrocarbons separation & purification and carbon capture.



Figure 4. DFT-calculated TpPa-NO<sub>2</sub> binding configurations: a)  $C_2H_2$ , b)  $C_2H_4$ , c)  $CO_2$ . Double dotted-lines, H...O; dotted-lines, C...H interaction; sold line, C…O interaction.

## **Author Contributions**

The manuscript was written through contributions of all authors.

### **Conflicts of interest**

The authors declare no competing financial interest.

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