SUPPLEMENTARY MATERIAL

Comparative kinetic analysis of redox flow battery electrolytes: from micro-fibers to macro-felts

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Figure S1: (a) 3D sketch and (b) photograph of the electrolysis cell for experiments with graphite felts





Figure S2: (a) Sketch of the microelectrode support : the red piece represents the copper wire while the black one is the carbon fibre (b) Photograph of a microelectrode carbon fibre (the fibre being located on the right-side and the connecting wire to the left side) and (c) optical microscope view of the carbon fibre.



Figure S3: Cyclic voltammograms for the different replication



Figure S4: Experimental Nyquist diagrams and their fits for all replications with porous graphite felts



Figure S5: Nyquist diagram at formal potential for the different replication of $(NH_4)_4Fe(CN)_6EIS$ measurement on SGL carbon felt (activated). Before and after translating the real part for d.c. resistance of all curves to match.



Figure S6: Nyquist diagram at different (E- E^{0} ') where E is the potential and E^{0} , is estimated formal potential, for one of the replications of $(NH_4)_4Fe(CN)_6EIS$ measurement on SGL carbon felt (non-activated)



c. (NH₄)₄Fe(CN)₆ on SGL not activated d. (NH₄)₄Fe(CN)₆ on SGL activated *Figure S7:* Experimental Nyquist diagrams and their fits for all replications with carbon fibre microelectrodes

Table S1: Optimized parameters' values for each replication and their average and standard deviation values for EIS experiments carried out on **non-activated** SGL carbon felt with TEMPO-based molecule at estimated formal potential of 0.66 V vs Ag/AgCl QRE.

		TEMPO-based				
		SC	GL GFD 4.6 n	.a.		
		#1	#2	#3	Average	Std Dev
R_{ohm}	$[\Omega]$	8.7	9.2	39.5	19.1	17.7
С	$[F cm^{-2} s^{\gamma-1}]$	1.05E-04	1.03E-04	9.83E-05	1.02E-04	3.51E-06
γ	[-]	0.97	0.97	0.97	0.97	0.002
k^{0}	$[cm s^{-1}]$	1.62E-03	1.61E-03	1.49E-03	1.57E-03	7.26E-05
l_p	[cm]	0.0011	0.0011	0.0010	0.0011	0.00003
S_c	$[cm^{2}cm^{-3}]$	327.2	333.3	334.9	331.8	4.1
f_p	[-]	2.93	2.83	3.28	3.01	0.24
φ	[-]	0.91^{*}	0.91^{*}	0.91^{*}	0.91 [*]	0.00

^{*}value fixed during optimization

Table S2: Optimized parameters' values for each replication and their average and standard deviation values for EIS experiments carried out on **activated** SGL carbon felt with TEMPO-based molecule at estimated formal potential of 0.66 V vs Ag/AgCl QRE.

		TEMPO-based				
		SO	GL GFD 4.6 a	ict		
		#1	#2	#3	Average	Std Dev
R_{ohm}	[Ω]	28.5	31.7	33.1	31.1	2.3
С	$[F cm^{-2} s^{\gamma-1}]$	8.55E-05	9.05E-05	1.11E-04	9.56E-05	1.34E-05
γ	[-]	1.00	0.99	0.99	0.99	0.01
k^0	$[cm s^{-1}]$	1.22E-02	8.59E-02	7.48E-02	5.77E-02	3.97E-02
l_p	[cm]	0.0020	0.0020	0.0021	0.0020	0.0001
S_c	$[cm^{2}cm^{-3}]$	303.8	295.6	259.8	286.4	23.4
f_p	[-]	1.32	1.10	1.20	1.21	0.11
φ	[-]	0.90^{*}	0.91^{*}	0.92^{*}	0.91 [*]	0.01

^{*}value fixed during optimization

Table S3: Optimized parameters' values for each replication and their average and standard deviation values for EIS experiments carried out on **non-activated** SGL carbon felt with ammonium hexacyanoferrate at estimated formal potential of 0.25 V vs Ag/AgCl QRE.

		$(NH_4)_4Fe(CN)_6$				
		SC	GL GFD 4.6 n	.a.		
		#1	#2	#3	Average	Std Dev
R_{ohm}	$[\Omega]$	8.3	91.1	92.5	64.0	48.2
С	$[F cm^{-2} s^{\gamma-1}]$	5.38E-05	4.49E-05	5.95E-05	5.27E-05	7.34E-06
γ	[-]	1.00^{*}	1.00^{*}	1.00^{*}	1.00	0.00
k^0	$[cm s^{-1}]$	2.60E-03	1.87E-03	2.14E-03	2.20E-03	3.70E-04
l_p	[cm]	0.0010	0.0008	0.0010	0.0010	0.00009
S_c	$[cm^{2}cm^{-3}]$	289.3	288.8	305.7	294.6	9.6
f_p	[-]	6.70	7.15	5.47	6.44	0.87
φ	[-]	0.79	0.81	0.84	0.81	0.02

^{*}value fixed during optimization

Table S4: Optimized parameters' values for each replication and their average and standard deviation values for EIS experiments carried out on **activated** SGL carbon felt with ammonium hexacyanoferrate at estimated formal potential of 0.25 V vs Ag/AgCl QRE.

		$(NH_4)_4$ Fe $(CN)_6$				
		S	GL GFD 4.6 a	ict		
		#1	#2	#3	Average	Std Dev
R_{ohm}	[Ω]	55.3	90.0	8.2	51.2	41.1
С	$[F cm^{-2} s^{\gamma-1}]$	9.15E-05	8.79E-05	9.19E-05	9.04E-05	2.21E-06
γ	[-]	1.00	0.99	0.99	1.00	0.00
k^0	$[cm s^{-1}]$	1.21E-02	5.69E-02	2.91E-02	3.27E-02	2.26E-02
l_p	[cm]	0.0018	0.0019	0.0019	0.0019	0.00004
S_c	$[\mathrm{cm}^2\mathrm{cm}^{-3}]$	314.6	276.4	243.3	278.1	35.7
f_p	[-]	1.29	1.53	1.11	1.31	0.21
φ	[-]	0.92^{*}	0.90^{*}	0.91^{*}	0.91 [*]	0.01

^{*}value fixed during optimization

Table S5: Optimized parameters' values for each replication and their average and standard deviation values for EIS experiments carried out on carbon fibre microelectrode drawn from **non-activated** SGL carbon felt with TEMPO-based molecule at estimated formal potential of 0.66 V vs Ag/AgCl QRE.

		TEMPO-based				
		SC	GL GFD 4.6 n	.a.		
		#1	#2	#3	Average	Std Dev
R _{ohm}	[Ω]	387.5	723.9	491.6	534.4	172.2
Y_0	$[F.cm^{-2}.s^{\gamma-1}]$	2.48E-06	2.30E-06	3.26E-06	2.68E-06	5.10E-07
γ	[-]	0.97	0.96	0.96	0.96	0.01
k^{0}	$[cm s^{-1}]$	1.09E-03	7.42E-04	8.68E-04	9.00E-04	1.75E-04
D	$[cm^2 s^{-1}]$	3.98E-06	3.33E-06	6.09E-06	4.47E-06	1.44E-06

Table S6: Optimized parameters' values for each replication and their average and standard deviation values for EIS experiments carried out on carbon fibre microelectrode drawn from activated SGL carbon felt with TEMPO-based molecule at estimated formal potential of 0.66 V vs Ag/AgCl QRE.

		TEMPO-based				
		SC	GL GFD 4.6 a	ıct		
		#1	#2	#3	Average	Std Dev
R _{ohm}	[Ω]	399.2	496.8	6918.9	2605.0	3736.3
Y_0	$[F cm^{-2} s^{\gamma-1}]$	2.18E-05	1.20E-05	4.29E-05	2.56E-05	1.58E-05
γ	[-]	0.83	0.89	0.80	0.84	0.04
k^{0}	$[\mathrm{cm \ s}^{-1}]$	3.66E-03	3.76E-03	1.00E-02	5.81E-03	3.63E-03
D	$[cm^2 s^{-1}]$	3.43E-06	4.50E-06	3.70E-06	3.88E-06	5.59E-07

Table S7: Optimized parameters' values for each replication and their average and standard deviation values for EIS experiments carried out on carbon fibre microelectrode drawn from **non-activated** SGL carbon felt with ammonium hexacyanoferrate at a potential of 0.6 V vs Ag/AgCl QRE.

		$(NH_4)_4Fe(CN)_6$				
		SC	GL GFD 4.6 n	.a.		
		#1	#2	#3	Average	Std Dev
R _{ohm}	[Ω]	373.6	747.1	586.2	569.0	187.4
Y_0	$[\mathrm{F}\mathrm{cm}^{-2}\mathrm{s}^{\gamma-1}]$	2.63E-06	2.28E-06	5.99E-06	3.64E-06	2.05E-06
γ	[-]	0.97	0.97	0.95	0.96	0.02
k^{o}	$[cm s^{-1}]$	1.05E-05	1.91E-05	2.31E-05	1.76E-05	6.44E-06
D	$[cm^2 s^{-1}]$	7.47E-06	1.19E-05	1.86E-05	1.26E-05	5.58E-06
m_O	$[\mathrm{cm \ s}^{-1}]$	9.82E-04	8.50E-04	1.18E-03	1.00E-03	1.63E-04

Table S8: Optimized parameters' values for each replication and their average and standard deviation values for EIS experiments carried out on carbon fibre microelectrode drawn from activated SGL carbon felt with ammonium hexacyanoferrate at estimated formal potential of 0.25 V vs Ag/AgCl QRE.

		(.	NH ₄) ₄ Fe(CN)			
		S	GL GFD 4.6 a			
		#1	#2	#3	Average	Std Dev
R _{ohm}	[Ω]	2379.8	410.6	3480.9	2090.4	1555.5
Y_0	$[F cm^{-2} s^{\gamma-1}]$	6.09E-05	9.23E-05	1.70E-04	1.08E-04	5.63E-05
γ	[-]	0.82	0.80	0.77	0.79	0.02
k^{o}	[cm s ⁻¹]	4.48E-03	3.06E-03	1.03E-02	5.95E-03	3.84E-03
D	$[cm^2 s^{-1}]$	3.60E-06	4.15E-06	5.39E-06	4.38E-06	9.17E-07

Parameters symbols and u	Values	
n	[-]	1
α	[-]	0.5
Т	[°C]	25
Scan rate	[mV s ⁻¹]	10
С	$[mol L^{-1}]$	10 ⁻⁴
D	$[cm^2 s^{-1}]$	$3.8 \ 10^{-6}$
$E^{0'}$	[V vs ref]	0.25
R_{Ohm}	[Ω]	10
Intervals of distribution function	[-]	10
Cylinders per mm ²	[-]	722
Carbon fibre radius	[µm]	4.5

Table S9: Input parameters kept constant for the simulation of Cyclic Voltammetry in Polarographica

Expression of Paasch, Micka and Gersdorf model as a function of formal potential

Defining the electrode potential E (Defined as \tilde{E} in the original paper) within porous electrode as the difference between solid phase electrical potential ϕ_1 and liquid phase electrical potential ϕ_2 , and starting with equation (2) from Paasch, Micka and Gersdorf paper [15]. Convention for the sign of the current was kept American (positive current for reduction) in order to limit possible confusion.

$$E = \phi_1 - \phi_2 d \tag{S.1}$$

$$AS_{c}C\frac{\partial E}{\partial t} = -\frac{A}{\rho_{2}}\frac{\partial^{2}\phi_{2}}{\partial x^{2}} + AS_{c}nFk^{0}C_{0}^{*1-\alpha}C_{R}^{*\alpha}\left[e^{-\frac{\alpha nF}{R_{g}T}(E-E_{n})} - e^{\frac{(1-\alpha)nF}{R_{g}T}(E-E_{n})}\right]$$
(S.2)

Butler-Volmer contribution to the equation can be replaced with classic i-E expression as a function of formal potential E^0 , and surface concentrations:

$$AS_{c}C\frac{\partial E}{\partial t} = -\frac{A}{\rho_{2}}\frac{\partial^{2}\phi_{2}}{\partial x^{2}} + AS_{c}nFk^{0}\left[C_{O}^{s}e^{-\frac{\alpha nF}{R_{g}T}\left(E-E^{0}\right)} - C_{R}^{s}e^{\frac{(1-\alpha)nF}{R_{g}T}\left(E-E^{0}\right)}\right]$$
(S.3)

Applied potential during impedance measurement can be expressed as a function of the average potential \overline{E} around which oscillation with time ΔE :

$$E = \overline{E} + \Delta E \tag{S.4}$$

Equation (S.3) can therefore be rearranged as:

$$AS_{c}C\frac{\partial\Delta E}{\partial t} = -\frac{A}{\rho_{2}}\frac{\partial^{2}\phi_{2}}{\partial x^{2}} + AS_{c}nFk^{0}\left[M_{O}e^{-\frac{\alpha nF}{R_{g}T}\Delta E} - M_{R}e^{\frac{(1-\alpha)nF}{R_{g}T}\Delta E}\right]$$
(S.5)

Where the expressions of M_O and M_R are given below:

$$M_{O} = C_{O}^{s} \exp\left(-\alpha \frac{nF}{R_{g}T} (\bar{E} - E^{0'})\right)$$
(S.6)

$$M_R = C_R^s \exp\left((1-\alpha)\frac{nF}{R_g T} \left(\bar{E} - E^{0'}\right)\right)$$
(S.7)

The classic assumption of small amplitudes allows to linearize the exponential terms with a first order Taylor expansion:

$$AS_{c}C\frac{\partial\Delta E}{\partial t} = -\frac{A}{\rho_{2}}\frac{\partial^{2}\phi_{2}}{\partial x^{2}} - \frac{AS_{c}n^{2}F^{2}k^{0}}{R_{g}T}[\alpha M_{0} + (1-\alpha)M_{R}]\Delta E + AS_{c}nFk^{0}(M_{0} - M_{R})$$
(S.8)

Assuming a Nernstian system and substituting surface concentrations with their expressions according to Nernst equation given in **equations (8)** and **(9)** (in the paper) allows to further elucidate M_O and M_R :

$$M_{O} = (C_{O}^{*} + C_{R}^{*}) \cdot \frac{\exp\left((1 - \alpha)\frac{nF}{R_{g}T}(\bar{E} - E^{0'})\right)}{1 + \exp\left(\frac{nF}{R_{g}T}(\bar{E} - E^{0'})\right)} = M_{R}$$
(S.9)

Hence in the case where surface concentrations are assumed to be equal to Nernst concentrations, M_O is equal to M_R , simplifying equation (S.8) into equation (S.10):

$$AS_{c}C\frac{\partial\Delta E}{\partial t} = -\frac{A}{\rho_{2}}\frac{\partial^{2}\phi_{2}}{\partial x^{2}} - \frac{AS_{c}n^{2}F^{2}k^{0}(C_{o}^{*}+C_{R}^{*})e^{\frac{(1-\alpha)nF}{R_{g}T}\left(\bar{E}-E^{o'}\right)}}{R_{g}T\left(1+e^{\frac{nF}{R_{g}T}\left(\bar{E}-E^{o'}\right)}\right)} \cdot \Delta E$$
(S.10)

Although this equation might seem complicated, it is virtually the same equation as equation (9) from the original paper, with exchange current density replaced by M_R which depends on available parameters. Symmetrically a similar development is made for equation (10) from Paasch team's original paper, and their equation (11) is obtained, only with a new expression for k which was presented here in **equation (4)** of our paper. Integration of this equation strictly gives the same analytical solution for complex impedance, but with a different value for k.

Development of quasi-reversible model

General expression of Fick's second law of diffusion for species O (the oxidant) is:

$$\frac{\partial C_o}{\partial t} = D_o \nabla^2 C_o \tag{S.11}$$

In cylindrical geometry for an infinitely long cylinder and under steady state assumption, this equation resumes to:

$$\frac{d^2 C_0}{dr^2} = -\frac{1}{r} \cdot \frac{dC_0}{dr}$$
(S.12)

This differential equation can be solved taking, as first boundary condition the flux continuity at the electrode surface using Faraday's law, and as second boundary condition the concentration equal to bulk electrolyte concentration at a distance δ of the electrode's walls (finite diffusion). The solution is as follows[36]:

$$C_O(r) = C_O^* + \frac{r_0 I_{ss}}{nFAD_O} \ln\left(\frac{\delta}{r}\right)$$
(S.13)

This solution is true for a radius comprised between electrode's radius r_0 and Nernst diffusion layer δ . Surface concentration is obtained for $r = r_0$:

$$C_O^s = C_O^* + \frac{r_0 I_{ss}}{nFAD_O} \ln\left(\frac{\delta}{r_0}\right)$$
(S.14)

And similarly, for the reductant R:

$$C_R^s = C_R^* - \frac{r_0 I_{ss}}{nFAD_R} \ln\left(\frac{\delta}{r_0}\right)$$
(S.15)

Assuming the same value of diffusion coefficient for O and R, one may identify mass transfer coefficient m_O :

$$m_0 = \frac{D}{r_0 \ln\left(\frac{\delta}{r_0}\right)} \tag{S.16}$$

Surface concentration expressions may then be substituted in classic i-E expression, just as Bard and Faulkner demonstrated for planar diffusion [31]:

$$I_{ss} = nFAk^{0} \left[\left(C_{R}^{*} - \frac{I_{ss}}{m_{0}} \right) \exp\left(\frac{(1-\alpha)nF}{R_{g}T} (E-E^{0}') \right) - \left(C_{0}^{*} + \frac{I_{ss}}{m_{0}} \right) \exp\left(-\frac{\alpha nF}{R_{g}T} (E-E^{0}') \right) \right]$$
(S.17)

Rearranging this equation permits obtaining an i-E relation as a function of bulk electrolyte concentrations:

$$I_{ss} = \frac{nFAk_0 \left[C_R^* e^{\frac{(1-\alpha)nF}{R_g T} \left(E - E^{0'} \right)} - C_0^* e^{-\frac{\alpha nF}{R_g T} \left(E - E^{0'} \right)} \right]}{1 + \frac{k_0}{m_0} \left[e^{\frac{(1-\alpha)nF}{R_g T} \left(E - E^{0'} \right)} + e^{-\frac{\alpha nF}{R_g T} \left(E - E^{0'} \right)} \right]}$$
(S.18)

Substituting I_{ss} in equations (S.14) and (S.15) finally allows obtaining surface concentrations as a function of bulk concentrations, mass transfer coefficient and charge transfer kinetic constant:

$$C_{R}^{s} = \frac{C_{R}^{*} + (C_{R}^{*} + C_{O}^{*}) \frac{k^{0}}{m_{O}} e^{-\frac{\alpha n F}{R_{g} T} \left(E - E^{0'}\right)}}{1 + \frac{k^{0}}{m_{O}} \left[e^{-\frac{\alpha n F}{R_{g} T} \left(E - E^{0'}\right)} + e^{\frac{(1 - \alpha) n F}{R_{g} T} \left(E - E^{0'}\right)} \right]}$$
(S.19)

$$C_{O}^{s} = \frac{C_{O}^{*} + (C_{R}^{*} + C_{O}^{*}) \frac{k_{0}}{m_{O}} e^{\frac{(1-\alpha)nF}{R_{g}T} (E-E^{0'})}}{1 + \frac{k_{0}}{m_{O}} \left[e^{-\frac{\alpha nF}{R_{g}T} (E-E^{0'})} + e^{\frac{(1-\alpha)nF}{R_{g}T} (E-E^{0'})} \right]}$$
(S.20)