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1 A multiparameter investigation of Syngas/diesel Dual-Fuel Engine performance and

2 emissions with various syngas compositions

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6 Abstract

Syngas, also known as producer gas or wood gas, is a gaseous biofuel produced by 7 8 gasification of biomass. It is mainly composed of hydrogen and carbon monoxide with a smaller share of methane, all diluted by nitrogen and carbon dioxide. Despite having carbon 9 in its composition, since it is made from biomass, it is considered low to zero-carbon and 10 being so makes it one candidate for reducing carbon emissions of internal combustion 11 engines. This work focuses on the effect of different syngas compositions on the performance 12 and the exhaust emissions of compression ignition engine with decane pilot injection as a 13 diesel surrogate. Results showed that thermal efficiencies over 39% are possible with a 14 variety of syngas with less than 10% energy contribution of decane. NO_x and soot emissions 15 were generally lowered by increasing the syngas/decane ratio, whereas CO and Total HC 16 emissions increased. Additionally, relations between engine performance/emissions and 17 fundamental properties of varying Syngas compositions were established. Further 18 investigation on other combustion properties, such as stretch sensitivity of the syngas/air 19 flame, are needed in order to better predict optimum operability. 20

Keywords: Syngas-fueled compression engine, diesel pilot injection, Dual-Fuel, syngas
 compositions, Performances, Emissions

23 **1 Introduction**

A considerable amount of pressure has been put on the energy sector to shift towards clean and renewable energy. In fact, to achieve the goal set by more than 100 countries of net-zero carbon emissions by 2050, all sectors of the economy will have to endure significant change[1]. While it might appear to most that, the only solution to achieve this goal, is a complete transition to a combustion-free energy sector, this might not be simple to accomplish.

Given the context presented above the use of biofuels presents itself as an alternative that 30 would reduce global CO₂ emissions with more affordable costs and simpler technologies. 31 Syngas, also known as producer gas and wood gas, is a general classification given to 32 33 flammable mixtures produced by the gasification of biomass. Gasification is a process that converts the molecules in the biomass (such as cellulose) to CO, H₂ and CO₂. It should not be 34 confused with biogas where the biomass is transformed mainly into CH₄ and CO₂ through 35 fermentation. As a waste-to-energy process, gasification competes with landfilling and 36 methanation, but the carbon footprint of the syngas scenario is higher than landfilling [2] and 37 can be in some case better than the biogas scenario [3]. The challenge when fueling an 38 internal combustion engine (ICE) with syngas is the inherent variability in composition that is 39 a result of several factors such as the biomass origin [4] and the gasification process [5]. 40 Typical values for H₂, CO and CH₄ contents stay between 10-20%, 13-24% and 0-7% in 41 volume respectively[5,6]. Moreover, regarding dilution, air-fed gasifiers typically produce 42 syngas that contains from 45 to 60% N₂ content and 10-20% CO₂. If oxygen or steam 43 gasification is used, N₂ content can be close to zero but these methods tend to be more 44 expensive[6]. 45

Nome	Nomenclature								
SI	Spark Ignition	<i>॑</i> V	Volumetric Flowrate						
CI	Compression Ignition	'n	Mass Flowrate						
HRR	Heat Release Rate	h	Heat Transfer Coefficient						
η	Efficiency	LHV	Lower Heating Value						
SOI	Start of Injection	Р	Pressure						
b	Cylinder Bore	Т	Temperature						
V_{cyl}	Diplaced Volume	ν	Piston linear speed						
CAD	Crank Angle Degree	CAX	X CAD where XX % of the fuel is burned						
IMEP	Indicated Mean Effective Pressure	IMEP	cov Coefficient of IMEP variation						
ATDO	C After Top Dead Center	BTDC Before Top Dead Center							
MPRR Maximum Pressure Rise Rate			Laminar Flame Speed						
RPM	Revolutions Per Minute	Total Hydrocarbons							

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47 Syngas can be used as fuel in ICE both in Spark Ignition (SI) [7,8] and Compression Ignition (CI) Engine [9–14]. Studies in SI engine are mainly focused on the auto-ignition propensity of 48 the syngas. Sridhar et al. [7] showed that, due to the auto-ignition resistivity of syngas, it was 49 possible to increase the compression ratio of SI engine with minimum knock risk thus 50 improving the efficiency. Arunachalam and Olsen [8] studied the knock propensity as a 51 function of different syngas compositions. Their work is noticeable since it compares "real" 52 compositions containing all the main components of the syngas namely H₂, CO, CH₄, CO₂ 53 and N₂. Regarding CI engines, Guo et al.[9] have investigated the effects of syngas energy 54 fraction, the reactive fuel injection timing and the load on emissions and efficiency for two 55 distinct simulated syngas compositions from air-fed gasifiers (48% N₂ and 13% CO₂ 56 concentrations) and one oxygen-fed gasifier composition (6% N2 only) in dual-fuel mode. The 57

effects of syngas substitution were a reduction in soot and NO_x emissions but higher CO 58 emissions for the two compositions with the highest N₂ content in syngas. Between these two 59 high-dilution compositions, the one with more CO and less H₂ produces more CO at the 60 exhaust and lower overall efficiencies. Some other studies used real syngas directly from a 61 gasifier. Rinaldini et al.[10] managed a maximum real syngas energy fraction of 60% at 50 62 N.m and 27% at 300 N.m of torque. Sharma and Kaushal[15] also tested real syngas from a 63 downdraft gasifier on a variable compression ratio CI engine. The result of increasing the 64 compression ratio from 12:1 to 18:1 was a reduction of CO and THC emissions with a 65 simultaneous increase in efficiency. Roy et al.[16] tested the effects of injection timing and 66 equivalence ratio on performance and emissions as a function of H₂ content in Syngas. Diesel 67 substitution levels of over 96 % under low or high H₂ content were achieved at an Indicated 68 Mean Effective Pressures (IMEP) of 14 bars but the highest H₂ content composition resulted 69 70 in a higher thermal efficiency. However, this also led to an increase in NO_x emissions.

The use of Syngas in a CI engine in dual-fuel mode has the advantage to have a flex-fuel 71 energy system, especially for off-grid stationary application. In dual-fuel mode, due to the 72 pilot injection of reactive fuel (as diesel fuel), there is the added complexity of the poorly 73 understood physicochemical interactions of the gaseous syngas combustion interactions with 74 75 the liquid pilot fuel spray. Currently, natural gas or methane dual-fuel operation are well covered by the literature [17–21] but syngas less. Moreover, to correctly optimize dual-fuel 76 syngas CI engines, the effects of its composition should be well understood. The challenge, 77 78 addressed in the present paper, when studying the influence of syngas composition on dualfuel engine performance is not fed the engine with real syngas but to control the compositions 79 that are representative of what is possible to produce from gasification, as an input parameter 80 and, in parallel, identifying the impact of each gas component on performance and emission 81 parameters. The novel approach chosen for this study is to consider three compositions that 82

represent the typical production of three gasifier types: Fluidized Bed, Fixed-bed Updraft and 83 Fixed-bed Downdraft (respectively indicated as Fluidbed, Updraft and Downdraft in 84 following), detailed in Table 1, and originally defined by Bridgwater[5] as well as to keep a 85 maximum syngas energy fraction(>60%). Indeed, the previous studies introduced above are 86 mainly conducted with a unique syngas composition or are numerical studies [12–14,22]. As a 87 new insight of syngas use in dual-fuel mode, the effect of syngas composition will be studied 88 as well as the contribution of each component of the syngas experimentally on an engine test 89 bench. It should be noted that the maximum laminar flame values for 3 Syngas compositions 90 displayed in Table 1 have been determined previously[23–25]. 91

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Table 1: Syngas Compositions.

	H ₂	CO	CO ₂	CH ₄	N ₂	Stoichiometric	LHV	Maximum
						Air/ Fuel ratio	(MJ/m³	laminar flame
	(%Vol)	(%Vol)	(%Vol)	(%Vol)	(%Vol)	(mol/mol)	of gas)	speed at 298K and
						(mass/mass)		1bar
								(cm/s)
Fluidbed	9	14	20	7	50	1.21 (1.25)	4.2	15.4
Updraft	11	24	9	3	53	1.12 (1.24)	4.4	30.7
Downdraft	17	21	13	1	48	1.00 (1.13)	4.8	36.7

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The global objective of this study is to identify what are the fundamental combustion and physical properties of syngas that determine engine performance and operating limits in dualfuel mode. For that, the effects of the pilot fuel quantity and equivalence ratio of premixed syngas/air on engine performance and emissions are analyzed for each composition. Moreover, to highlight the contribution of CH_4 and CO_2 contents, an additional analysis is carried out with ternary mixtures of $H_2/CO/N_2$.

100 2 Experimental Method

In this section the engine characteristics, experimental method and the post-processingmethod are described.

103 2.1 Experimental Setup

The experimental setup consists of a research PSA DW10 based engine test bench converted to single-cylinder operation with 3 cylinders not fueled. The engine speed, driven by an electric motor, is maintained at 1200 RPM. The engine speed for genset application is usually 1500 RPM. Unfortunately, it was not possible with our setup due to important vibrations of the intake/exhaust pipes and bench. The engine characteristics are described in Table 2.

Table 2: Engine Characteristics.

Displaced Volume	499 cm ³
Bore	85 mm
Stroke	88 mm
Rod length	145 mm
Compression Ratio	17:1
Piston Bowl Type	"Mexican hat"
Firing TDC position	0 CAD
Intake Valve Opening	351 CAD ATDC
Intake Valve Closure	157 CAD BTDC
Exhaust Valve Opening	140 CAD ATDC
Exhaust Valve Closure	366 CAD ATDC
Oil and Coolant Temperature	85 °C
Max Brake Power (for the commercial multi-cylinder engine)	120 kW @ 3750 rpm
Max Torque (for the commercial multi-cylinder engine)	340 N.m @ 2000 rpm

In order to obtain the desired intake charge compositions a series of mass flow meters, as specified in Table 3, are used. The resulting uncertainty for the premixed syngas/air equivalence ratio, $\phi_{premixed}$ (eq. 1) of the intake charge is ±2%. The mixing of the syngas/air charge is ensured by the intake plenum (visible in Fig. 1) which also enables to damper pressure oscillations at the intake port.

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Table 3: Mass Flow Controllers.

Gas Type	Flowmeter / Controller	Full Scale	Uncertainty
Air	Emerson F025S	1100 NL/min	±0.5%
N ₂	Brooks 5851S	100 NL/min	±0.9%
СО	Brooks 5851S	100 NL/min	±0.9%
H ₂	SLA5850	50 NL/min	±1,0 %
CO ₂	SLA5850	37 NL/min	±1.0%
CH ₄	SLA5850	5 NL/min	±1.0%

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The pilot injection is discharged by a Bosch CRI 2.2 six-holes common-rail injector operating at a reduced pressure of 200 bar to guarantee minimal injection quantities with sufficient injection duration. The injector was previously characterized by means of an IAV type-K flow rate analyzer to provide the injection rate profiles and injection quantities as a function of the injection duration. Decane ($C_{10}H_{22}$) was used as a surrogate for diesel fuel to facilitate future CFD simulations and kinetics one with Madison kinetic mechanism of Ren at al.[26] to determine fundamental combustion properties of syngas/decane/air mixtures.

The gaseous equivalence ratio, $\Phi_{premixed}$, is calculated as the O₂ volumetric flowrate required for stoichiometry divided by the real O₂ volumetric flowrate (Eq. 1). A global equivalence ratio (ϕ_{global}) can be also calculated as a function of the pilot fuel amount and the stoichiometric mass air/fuel ratio of decane (15.03) as indicated in Eq. 2.

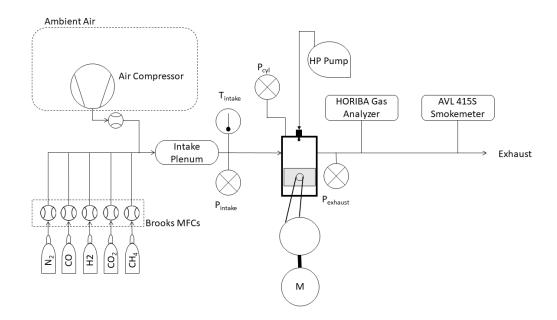
$$\phi_{premixed} = \frac{0.5\dot{V}_{CO} + 0.5\dot{V}_{H_2} + 2.0\dot{V}_{CH_4}}{0.21\dot{V}_{Air}} \#(1)$$
$$\phi_{global} = \phi_{premixed} + \frac{15.03}{\dot{m}_{air}/\dot{m}_{pilot}} \#(2)$$

Additionally, the energy share of the pilot fuel (decane) energy of the total supplied energy isdefined as follows:

$$E_{pilot} = 100 \cdot \frac{m_{inj} LHV_{C_{10}H_{22}}}{m_{inj} LHV_{C_{10}H_{22}} + \dot{m}_{syngas} LHV_{syngas}} \#(3)$$

A MEXA 7100D-EGR HORIBA gas analyzer is capable of measuring O_2 (magnetopneumatic detector), CO and CO₂, (non-dispersive infrared absorption analyzer), NO_x (chemiluminescence analyzer) and total unburnt Hydrocarbons (THC) (flame ion analyzer) concentrations with a precision of 1 ppm for all gases. These concentrations are converted to specific emissions. Additionally, an AVL 415S smoke-meter, with a detection limit of 0.02 mg/m³ is used to provide soot emission data. The full experimental setup is schematized in

140 Erreur ! Source du renvoi introuvable..



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Figure 1: Experimental Setup scheme.

143 2.2 Post-processing method

From the averaged in-cylinder pressure, calculated over 100 consecutive cycles that are measured by a Kistler 6043A piezo-electric pressure transducer (accuracy of \pm 2.0 %), the gross Heat Release Rate (HRR) is estimated with the following equations:

$$HRR (J/CAD) = \frac{\gamma}{\gamma - 1} P dV + \frac{1}{\gamma - 1} V dP + dQ_{wall} \# (4)$$
$$dQ_{wall} (J/CAD) = h.S. (T - T_{wall}) \# (5)$$
$$h (J.K^{-1}.m^{-2}) = 3.26b^{-0.2}P^{0.8}T^{-0.55}v^{0.8} \# (6)$$

The heat transfer coefficient *h* is determined using the correlation proposed by Woschni [27]. The integrated value of $dQ_{combustion}$ is used to determine the mass of fuel burnt (MFB). Cylinder wall temperature, T_{wall} , is estimated at 423 K. The calculation is first done with a constant heat capacity ratio, γ , to obtain a first MFB. Then γ is reassessed from the MFB with the mole fractions of all six components (N₂, O₂, CO, H₂, CO₂, CH₄) for the unburnt gases and with the emissions data for the burnt gases using NASA polynomials equation. Equations 4-6 are then recalculated with this variable γ and the definitive MFB value is obtained.

154 The thermal efficiency is calculated with the following equation:

$$\eta_{thermal} = \frac{IMEP * V_{cyl} * \dot{m}_{total}}{LHV_{C0} \cdot \dot{m}_{C0} + LHV_{H_2} \cdot \dot{m}_{H_2} + LHV_{CH_4} \cdot \dot{m}_{CH_4} + LHV_{C_{10}H_{22}} \cdot \dot{m}_{C_{10}H_{22}}} \#(7)$$

The combustion efficiency is calculated by doing the oxygen balance between intake and exhaust related to the total equivalence ratio:

$$\eta_{combustion} = \frac{0.21\dot{m}_{air-intake} - \dot{m}_{O_2-exhaust}}{\dot{m}_{O_2-theoretically burning}} \#(8)$$

157 **3 Results and discussion**

158 3.1 Effect of premixed equivalence ratio

To study the effect of syngas/air equivalence ratio, the injection duration was kept constant at 500 μs (i.e. 0.61 mg) with an increase of syngas amount in the intake charge. The start of injection (SOI) was optimized to guarantee maximum IMEP. Premixed equivalence ratio $\phi_{premixed}$ was varied to 0.3, 0.5, 0.7 and 1.0 for all three compositions except for Fluidbed for which $\phi_{premixed} = 1.0$ induced very unstable combustion, i.e. IMEP_{cov} >10%. In this section, increasing $\phi_{premixed}$ leads to a syngas mass flowrate increase but an air mass flowrate decrease in order to keep a constant intake pressure (i.e. 1 bar).

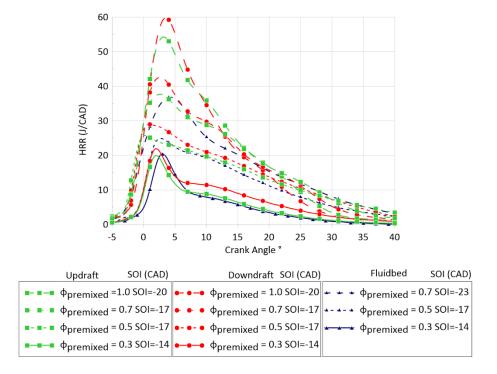




Figure 2: Evolution of Heat Release Rate for all premixed equivalence ratios and the
 three compositions (1200 RPM, P_{intake} = 1 bar, T_{intake} = 300K).

In Figure 2 the HRR traces show that, for all compositions, the increase of $\phi_{premixed}$ induces 169 170 a transition from a two-phase to a single-phase combustion evolution. This could be linked to a reduction in the ignition delay of the syngas/air mixtures with $\phi_{premxed}$ so, in practice, 171 instead of having the first auto-ignition of the decane charge followed by a slow flame of 172 syngas/air mixture, both fuels start burning simultaneously. When the pilot injection occurs, 173 i.e 20 CAD BTDC, the liquid fuel is atomized and has enough time to mix with the nearest 174 surrounding syngas/air premixed mixture. Therefore, the ignition of the liquid pilot spray will 175 176 also ignite the surrounding premixed charge of syngas especially if the syngas is in sufficient quantity as for the stoichiometric syngas/air case. When $\phi_{premixed}$ is lower, the decane is 177 178 introduced later, so less mixing with syngas/air, and less syngas is available. Therefore, the

decane will first ignite before the ignition of the premixed syngas charge. It should also be 179 noted that the maximum HRR increases with $\phi_{premixed}$ but the delay does not seem to be 180 affected after $\phi_{premixed} \ge 0.5$ for downdraft and updraft. Higher H₂ concentrations in the 181 syngas composition induce higher peak of HRR. This is consistent with the findings of Dhole 182 et al.[28] and Roy et al.[16]. For same equivalence ratio, the overall shape of the profiles is 183 not affected by the Syngas composition as also highlighted by the In-Cylinder Pressure in 184 Figure 3. The In-Cylinder Pressure shows that the $\phi_{premixed}$ increase leads to a higher peak 185 pressure and a longer combustion tail for downdraft. The major change is when increasing 186 from 0.3 to 0.5 after that the pressure traces show similar envelope. For the composition 187 effect, Updraft and Downdraft present the same pressure trace while the peak pressure is a bit 188 lower for Fluidbed as expected due to its lower energy content. The differences, between both 189 190 compositions, in terms of start of combustion are highlighted in Figure 3b (in-cylinder pressure traces of Updraft and Fluidbed are available as supplementary materials). It can also 191 192 be noted from Figures 3 that SOI remains between -14 and -20 CAD for Updraft and Downdraft and that the range is a bit wider for Fluidbed, i.e. down to -23 CAD. Moreover, in 193 order to get maximum IMEP with minimum IMEP_{cov}, the SOI is advanced with the increase 194 195 of $\phi_{premixed}$.

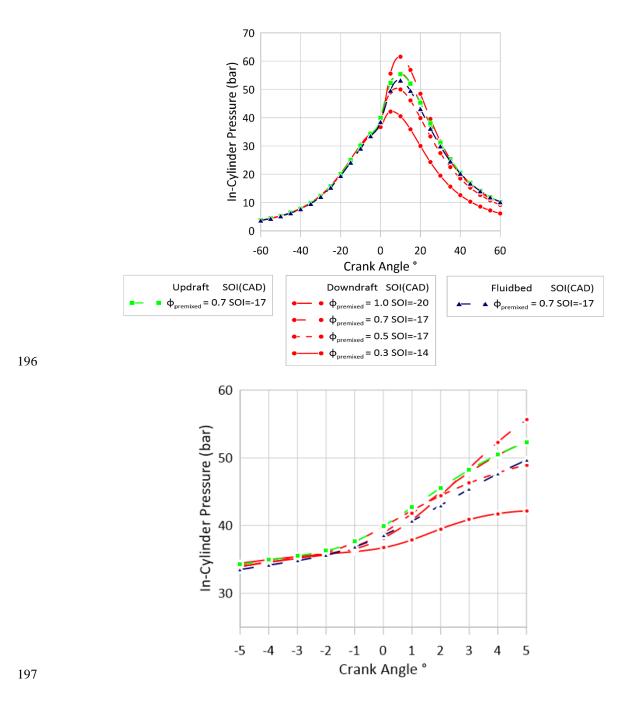


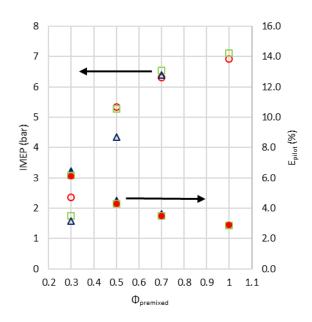
Figure 3. (a) Evolution of In-Cylinder Pressure for all premixed equivalence ratio for Downdraft and only at $\phi_{premixed} = 0.7$ for Updraft and Fluidbed, (b) zoomed between

-5 and 5 CAD. (1200 RPM, Pintake = 1 bar, Tintake= 300K)

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Figure 4a displays the corresponding IMEP and energy share of the pilot E_{pilot} . First, in agreement with HRR and in-cylinder pressure traces, IMEP increases with $\phi_{premixed}$ since more energy is introduced. Then it is worth noticing that, in all cases, the energy share of the

pilot stays below 21% of the total energy amount. Since the injected quantity of decane is 204 maintained constant, the pilot energy share decreases with $\phi_{premixed}$. Figure 4b shows the 205 IMEP_{cov} as well as the MPRR as a function of $\phi_{premixed}$. It can be seen that for premixed 206 equivalence ratio greater than 0.5, the combustion is quite stable for all compositions, i.e. 207 IMEPcov below 6%, except for Fluidbed (8% for IMEPcov). For $\phi_{premixed} = 0.3$, the 208 combustion is more likely to be unstable (up to 13% of IMEPcov for Downdraft) but it 209 remains possible to operate the engine. Regarding combustion noise, the maximum pressure 210 rise rate (MPRR) increases with $\phi_{premixed}$ because of energy input increase and H₂ content in 211 the syngas composition. The syngas compositions can be ranked, Fluidbed, Updraft, 212 213 Downdraft from lower to higher maximum pressure gradient. For Downdraft and Updraft at stoichiometric premixed equivalence ratio, it should be mentioned that the MPRR is at the 214 limit of excessive combustion noise (4 bar/CAD) [29]. 215



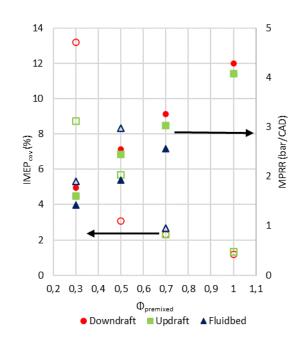
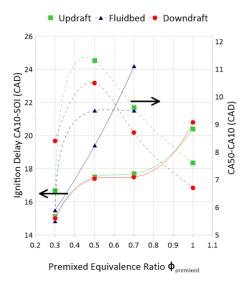




Figure 4. a) IMEP (empty symbols) and Epilot (filled symbols) and b)IMEPcov (empty symbols) and MPRR (filled symbols) as function of φ_{premixed}

In Figure 5, both the ignition delays from the pilot injection timing and the first part of the 220 combustion development are plotted as a function of the equivalence ratio. First, it can be 221 noted that the increase in premixed equivalence ratio also increases the ignition delay. It is 222 probably explained by the fact that the start of injection (SOI) is advanced with the increase in 223 premixed equivalence ratio. Indeed, it should be reminded that SOI is advanced in order to 224 keep a maximum IMEP and therefore a relatively constant CA50. This is especially verified 225 for the Fluidbed composition, for which the increase is more linear and stronger than for the 226 Downdraft and Updraft ones. This is probably explained by the higher CO_2 content (20%) of 227 228 Fluidbed composition that contributes to delay the autoignition. Yet, the duration of the first half of the combustion, represented by CA50-CA10, strongly decreases from $\phi_{premixed} = 0.5$ 229 230 onwards. This is due to the increased reactivity of the premixed charge and the increase of the flame propagation speed. 231



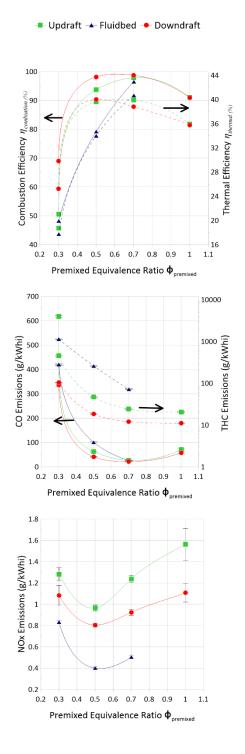
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Figure 5: Effect of premixed equivalence ratio on ignition phasing (continuous lines) and first half of combustion (dotted lines) (1200 RPM P_{intake} = 1 bar T_{intake} = 300K).

Figure 6 presents the thermal and combustion efficiencies and emissions as a function of 235 premixed equivalence ratio for the three Syngas compositions. Both combustion and thermal 236 efficiencies are bell-shaped reaching peak values around 98% and 39% respectively for 237 Downdraft and Updraft compositions. For Fluidbed, efficiencies continuously increase but the 238 curves start to bend. Since premixed stoichiometric equivalence ratio was not achievable, it is 239 240 not possible to forecast for which equivalence ratio efficiencies will start to decrease. The lowest combustion efficiency, reached for the ultra-lean premixed charge, induces, as 241 expected, the highest CO and THC emissions. The minimum CO and THC emissions are 242 obtained when $\phi_{premixed}$ is between 0.5 - 0.7 and as expected where efficiencies are the 243 highest ones. Overall, this effect of the premixed equivalence ratio on the CO and THC 244 emissions confirms the ones observed by Roy et al.[16]. For NO_x emissions, also the lowest 245 values are obtained at $\phi_{premixed} = 0.5$, with the highest ones reached at the stoichiometric 246 syngas/air mixture. This evolution is not expected as the NOx emission peak is reached in 247 lean side in classical SI engine. It is indeed surprising to observe that minimum NOx 248 coincides with minimum CO, but since syngas is a highly diluted fuel (about 50% N_2 , 10 to 249

 $20 \ \% CO_2$), its combustion temperature is very low leading to low NOx levels even in lean mixtures where CO emission is also minimum. Similar trends were observed numerically for NOx emission but not for CO one (Kousheshi et al. [30]). For all operating conditions, soot emissions were below the detection limit of the measurement device.

254



256	Figure 6:	Efficiencies and	exhaust gases	emissions as a	function of	premixed	equivalence
						r	1

257 ratio for the three Syngas compositions (1200 RPM, $P_{intake} = 1$ bar, $T_{intake} = 300$ K,

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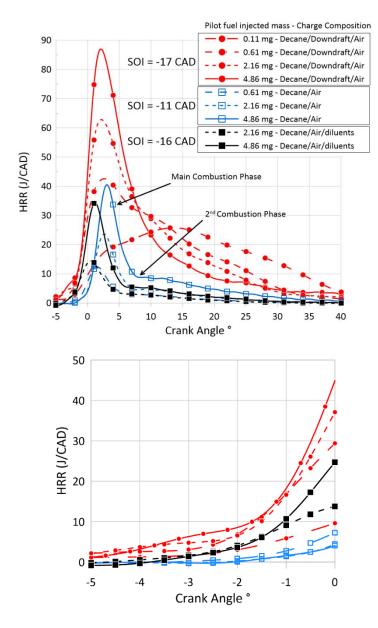
Optimum SOI).

259 3.2 Effect of pilot fuel injection quantity

In the previous section, since the optimal premixed equivalence ratio was found to be around $\phi_{premixed} = 0.7$, the effect of the pilot injection was evaluated at this particular value, while the injection duration was varied from 250 μs to 1000 μs , i.e. corresponding to 0.11 to 4.86 mg of decane injected per cycle (see Table 4). First, to evaluate the contribution of the pilot amount in the combustion development, the pilot fuel is first injected in air (without syngas) and then in air plus 5%_{vol} CO₂ and 20%_{vol} N₂ concentrations (equivalent charge dilution as the downdraft case).

Case	Injection Duration (µs)	Decane injected mass (mg)	ϕ_{global}	Pilot fuel energy share (%)	IMEP (bar)	SOI (CAD) ATDC	
	250	0.11	0.71	0.6	5.7		
Downdraft/Air	500	0.61	0.74	3.3	6.3	-17	
	750	2.16	0.83	10.9	6.8		
	1000	4.86	1.0	21.7	7.4		
	500	0.61	0.02		0.4		
Air	750	2.16	0.08		1.2	-11	
	1000	4.86	0.17	100	2.8		
Air/Diluents	750	2.16	0.1	0.1		-16	
	1000	4.86	0.22		2.0		

267	Table 4: Experimental conditions to study the effect of pilot fuel injection quantity.



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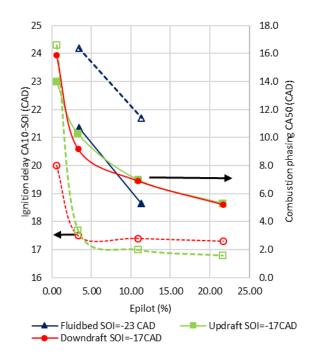


Figure 7(a): Heat release rate from the fuel pilot injection in air and air with diluents compared to downdraft dual-fuel. ($\phi_{premixed} = 0.7$) and (b)zoom between -5 and 0

CAD

In Figure 7, it can be clearly seen that the ignition delay of the reactive fuel, decane from pilot injection, is similar in air with diluents as with the presence of syngas. However, it can be noted that for the highest quantity of liquid pilot injection, i.e. 4.86 mg, an earlier heat release can be observed between -5 and -2 CAD before TDC, smaller than the major rise in HRR that follows – when decane is injected in premixed syngas/air. This low-temperature heat release

could indicate a two-stage ignition process that does not occur when the decane injection is done in non-reactive medium (i.e. air or air/diluent). In these cases, the combustion occurs in two phases: the main combustion phase due to the premixing of decane with air and a second one, slower due to the diffusion-controlled combustion. The distinction between the phases is less clear when syngas is premixed with the intake charge but there is still an inflexion point after the peak in HRR for 0.61 and 2.16 mg quantity injected at around 7 and 9 CAD ATDC respectively.

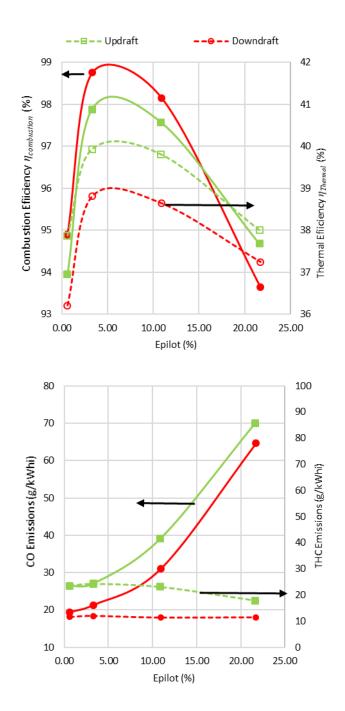


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Figure 8: Effect of pilot fuel energy share on ignition delay (empty symbols, dashed lines) and combustion phasing CA50 (filled symbols, continuous lines) for three Syngas compositions (1200 RPM, $P_{intake} = 1$ bar, $T_{intake} = 300K$, $\phi_{nremixed} = 0.7$).

In Figure 8, the effect of decane addition on the ignition timing and the combustion phasing (CA50) is presented for the 3 syngas compositions. For the Fluidbed composition, stable combustion could not be achieved at the lowest and highest pilot fuel injection durations therefore only two data points are presented. This behavior can be attributed to the high CO_2 concentrations of Fluidbed combined with the comparatively low H_2 and CO contents. For

updraft and downdraft ones, the ignition delay seems to stabilize once enough decane is 295 injected (over 10% of the total available energy). But, the combustion phasing is monotically 296 advanced with the addition of decane, as expected from the HRR profiles presented in Figure 297 7 for the Downdraft composition. Basically, increasing the energy share from the more 298 reactive fuel will reduce the ignition delay of the whole fuel charge as observed on CA10-299 SOI, the decane being easier to auto-ignite. This will lead to a shift of the CA50 and globally 300 of the whole combustion earlier in the cycle. For Downdraft, IMEP_{cov} decreases from 2.4 301 down to 1.08 % and MPRR increases from 1.2 up to 6.9 bar/CAD as E_{pilot} increase. For 302 Updraft, the trends and values are very similar to Downdraft. However, for Fluidbed, IMEP_{cov} 303 decreases from 2.6 down to 2 % and maximum pressure gradient increases from 2.6 up to 4.8 304 bar/CAD with E_{pilot} increases. Hence, and as expected, ranking in terms of combustion 305 stability and noise is the same as the one observed in the previous section. 306





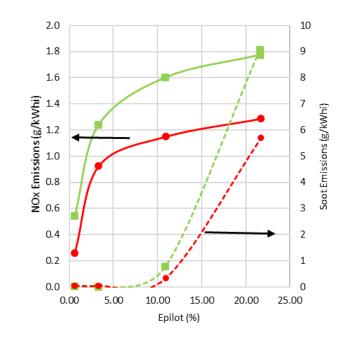


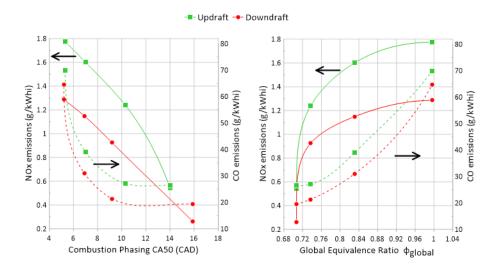


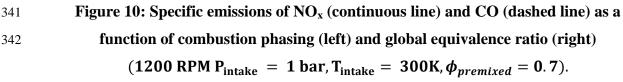
Figure 9: Efficiencies and emissions as a function of decane energy share for the three
 Syngas compositions. Filled symbols/continuous lines : Combustion efficiency, CO and
 NOx emissions for a,b and c respectively. Empty symbols/Dashed lines: Thermal
 Efficiency, THC and Soot emissions for a, b and c respectively

314 (1200 RPM, $P_{intake} = 1 \text{ bar}, T_{intake} = 300 \text{ K}, \phi_{premixed} = 0.7$).

315 In Figure 9, for Updraft and Downdraft compositions, the combustion and thermal efficiencies are bell shaped with a maximum value, reached around 10% pilot fuel energy 316 share. Fluidbed results are not plotted as only two conditions provide stable combustions. It 317 has to be noted that the Updraft composition induces a lower combustion efficiency than 318 Downdraft but a better thermal one. This is despite the fact that CA50 is very similar between 319 the two compositions for the same pilot fuel amount (Figure 8). Due to the higher H2 content, 320 Downdraft has a greater flame speed (Table 1) thus leading to a better consumption of fresh 321 gases. On the other hand, this higher H2 content could lead to higher combustion temperature 322 323 and therefore more heat losses thus depleting the thermal efficiency as highlighted numerically by Kousheshi et al. [30]. The emissions data show that CO and soot emissions are 324

negatively affected by the increase in decane quantity, without any bell or inverse bell shape: 325 more diesel type fuel induces more unburnt carbonaceous exhaust gases except THC, i.e. a 326 slight reduction seems to occur with decane addition for the updraft composition. The level of 327 soot was so low than no value could be measured, for fuel amount lower than 12% energy 328 share similarly to what was observed by Papagiannakis et al. [17] with methane/diesel dual-329 fuel. Yet when reaching 20% for E_{pilot}, soot emissions rise up to significant value of 6-9 330 g/kWh. It is also clear that NO_x emissions strongly increase as a function of decane amount, 331 due to the increase of in-cylinder temperatures. It is interesting to notice, both CO and NOx 332 are minimum for the same E_{pilot} and rises with E_{pilot} increase. The syngas is globally a low 333 NOx fuels, its combustion temperature is very low compare to other fuels. Moreover since the 334 equivalence ratio stays poor in the whole study the CO and HC are also low. Yet, when 335 increasing decane quantity both NOx and CO rise simultaneously because it will induce a 336 combustion temperature increase leading to higher NOx and an increase of liquid quantity that 337 338 leads to a poorer mixing and evaporation that leads to higher CO and HC. The effects of CO₂ on NO_x emissions will be discussed further on the final part of this work. 339





In Figure 10, NO_x and CO emissions are presented as a function of CA50 and ϕ_{global} . 343 Regarding the relationship between emissions and combustion phasing it is clear that, for this 344 premixed equivalence ratio, CO emissions reach a plateau for CA50 > 9 CAD ATDC while 345 NO_x emissions decrease almost linearly with CA50, as the in-cylinder temperature is higher 346 for shorter combustion. The NOx emissions as function of the global equivalence ratio 347 follows the decane share, and seems to reach a plateau when the global equivalence ratio 348 tends to 1. Meanwhile, the increase in CO emissions seems not to reach a plateau as usually in 349 SI engines: CO increases with the global equivalence ratio increase. 350

351 3.3 Effect of CH₄ and CO₂ concentration

To give further insight on the roles of CH₄ and CO₂ on performance and emissions, 352 complementary measurements were performed with the composition variations as in Table 5. 353 The variation consists of maintaining H₂ and CO volume fractions constant while adjusting 354 the N₂ volume fraction to compensate CO₂ or CH₄ variations. The variations are designated by 355 356 the composition (FB, UD, DD for Fluidbed, Updraft, Downdraft respectively), from which the H₂ and CO content is kept, followed by an index that refers to the CO₂ or CH₄ content. The 357 variation FB-20_{CO2} is greyed out as no stable operation could be obtained. The Madison 358 kinetics mechanism[26] was selected in combination with the PREMIX and EQUIL 359 CHEMKIN ANSYS PRO codes to estimate laminar flame speed and flame temperature 360 respectively, by considering initial conditions equal to those in the cylinder at the start of 361 injection (864 K and 30 bar, $\phi = 0.7$). This mechanism was validated for this purpose in a 362 previous study[25]. Premixed equivalence ratio was kept constant at 0.7 and the injection with 363 a duration of 400 μs (i.e. 0.32 mg corresponding to $E_{pilot} \approx 1.65\%$) started at -18 CAD BTDC. 364 365

						Adiabatic	
Variation	H2	СО	CO2	CH4	N2	Equilibrium	Laminar Flame
v arration	$(\%_{\rm vol})$	$(\%_{\rm vol})$	$(\%_{\rm vol})$	$(\%_{\rm vol})$	(% _{vol})	Flame	Speed (cm/s)
						Temperature (K)	
FB – 0 _{CO2-CH4}		14	0	0	77	1868	32.3
FB – 10 _{CO2}			10	0	67	1834	24.3
$FB - 20_{CO2}$	9		20	0	57	1802	14.9
FB - 2.5 _{CH4}	-		0	2.5	74.5	1955	33.0
$FB - 5_{CH4}$			0	5	72	2016	35.0
FB - Reference			20	7	50	2004	26.4
$UD - 0_{CO2-CH4}$	11 24		0	0	65	2092	61.5
UD - 10 _{CO2}		24	10	0	55	2059	51.1
UD - 20 _{CO2}			20	0	45	2028	41.9
UD – 2.5 _{CH4}			0	2.5	62.5	2131	59.5
UD – 5 _{CH4}			0	5	60	2160	58.2
UD - Reference			9	3	53	2112	51.1
DD – 0 _{CO2-CH4}	OCO2-CH4		0	0	62	2120	83.0
DD - 10 _{CO2}			10	0	52	2088	69.1
DD - 20 _{CO2}	17	21	20	0	42	2057	57.9
DD - 2.5 _{CH4}	11		0	2.5	59.5	2154	75.4
DD - 5 _{CH4}			0	5	57	2178	71.2
DD – Reference			13	1	48	2095	62.7

367 In Figure 11, the effect of CO_2 and CH_4 content on HRR is highlighted. CO_2 addition to

368 Syngas delays the onset of combustion and extends the combustion duration. This effect has

been well described by Xiang et al.[31] and Halter et al.[32] for CH₄/CO₂/Air mixtures where 369 370 the dilution, thermal and chemical contributions of CO₂ to the reduction of laminar flame speed have been quantified. Since the total dilution amount, i.e. N₂ + CO₂ quantity, is kept 371 constant, the effect seen here is both related to the thermal (increased heat capacity of the 372 charge \rightarrow reduction of charge temperature) and chemical effects. Moreover, the two 373 combustion stages present for downdraft and updraft without any CO_2 (DD – $0_{CO2-CH4}$ and UD 374 $-0_{\text{CO2-CH4}}$ respectively), are less evident with CO_2 addition. On the other hand, the addition of 375 CH₄ advances the start of combustion and makes it easier to distinguish the two combustion 376 phases. This could indicate that the H₂ in the syngas might be consumed first, contributing to 377 the initial rise in HRR, followed by the slower-burning CO and CH₄. 378

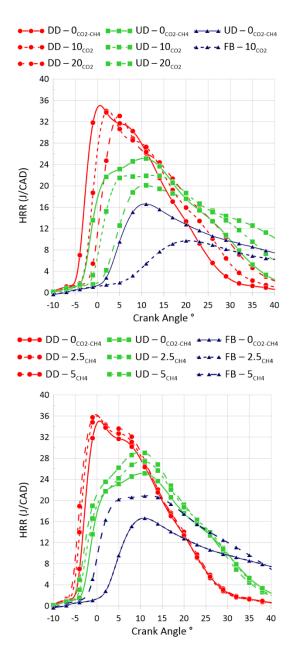




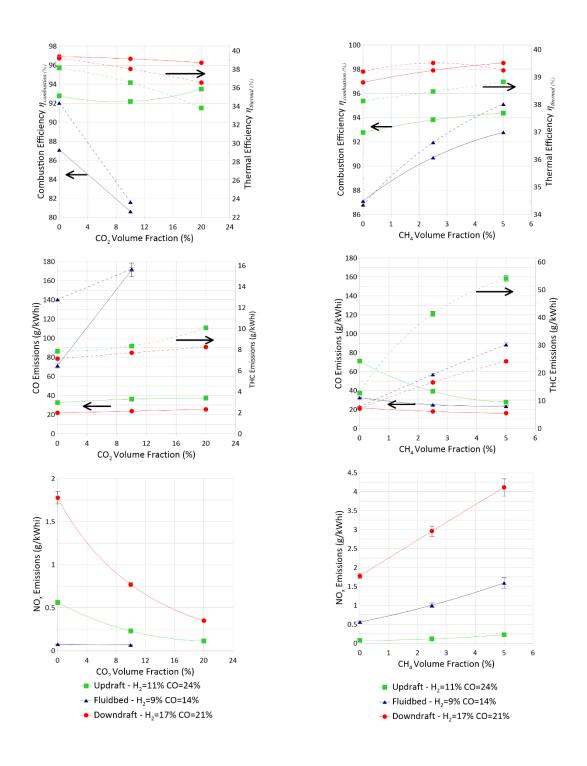
Figure 11: Heat Release Rate profiles for varying CO₂ (top) and CH₄ (bottom) contents (1200 RPM P_{intake} = 1 bar, T_{intake} = 300K, $\phi_{premixed} = 0.7 SOI =$

382

-18 CAD BTDC).

The resulting efficiencies and emissions from the variations tested are presented in Figure 12. Soot emissions are not presented because they are always under the detection limit. By replacing N_2 with CO₂, the decrease of combustion efficiency induces CO and THC increase

- but a reduction of NO_x emissions, due to the delay of the combustion phasing as the start of
- 387 injection was maintained constant and not optimized.



a) Effect of CO2 content

b) Effect of CH4 content

Figure 12. Effect of Syngas components a) CO2 and b) CH4 on engine efficiencies and

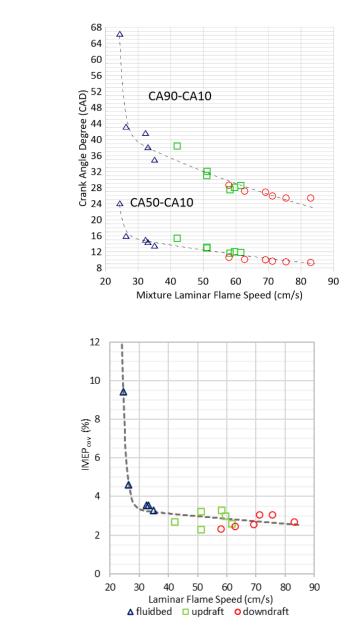
exhaust emissions (1200 RPM,
$$P_{intake} = 1 \text{ bar}$$
, $T_{intake} = 300 \text{ K}$, $\phi_{premixed} =$

-17 BTDC).

Figure 12 b) indicated that CH₄ addition increases both thermal and combustion efficiencies 391 resulting in lower CO emissions. Despite the overall higher combustion efficiencies, THC 392 emissions increase with CH₄ addition due to the increase of unburned CH₄ itself. Even if the 393 amount of CH4 added remains low, the increase of CH4 % induces an increase of NOX 394 emissions, mainly due to higher in-cylinder temperatures, as predicted the higher adiabatic 395 temperature values in Table 5. Due to the higher H_2 content, Downdraft provides a greater 396 combustion development speed thus leading to a better consumption of fresh gases. On the 397 other hand, this higher H₂ content could lead to higher combustion temperature and therefore 398 more heat losses thus depleting the thermal efficiency. 399

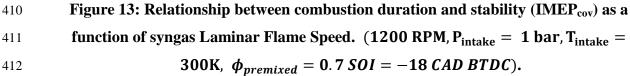
400 3.4 Relationship between fundamental composition properties and engine operation

In order to predict the effect of syngas composition, it is important to highlight the relationship between the fundamental properties of the composition (such as laminar flame speeds, LFS, or adiabatic flame temperature, T_{ad}) and the resulting engine performance and emissions. For that, empirical correlations are suggested in Figure 13 and 13 to identify the effect of properties variations in Table 5 to the combustion durations and stability and NO_x, THC and CO emissions.





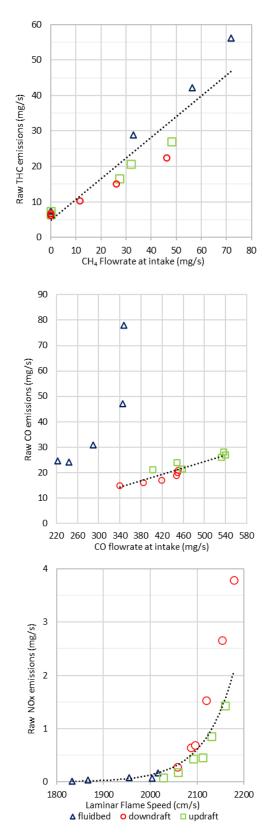




First flame development stage duration (CA50-CA10) and total combustion duration (CA90-CA10) clearly decrease with the laminar flame speed with a clear transition when the flame speed goes under a certain level probably due to the combustion instabilities linked to the low value of LFS in the case of fluidbed. A similar behavior was observed by Lhuillier et al.[33] for NH_3/H_2 mixtures in a SI engine. Nevertheless, while the trend is clear for the whole of the 17 compositions tested, locally, the experimental points seem to group together as a function of H₂/CO contents. In Figure 13b, one can note that when the composition of a syngas/air mixture induces a laminar flame speed lower than 40 cm/s, as it is for fluidbed composition, IMEP_{cov} rises sharply. Yet, for LFS > 40 *cm/s*, the stability is not affected by any laminar flame speed change.

In Figure 14a, total hydrocarbon (THC) emissions increase with the addition of CH_4 , as the number of HC increase, indicating that the part of intermediate CH due to the decane oxidation (or to crevice trapping) is lower. In the case of CO emissions (Figure 14.b), same linear dependency can be noted of Downdraft and Updraft compositions but the exhaust CO values are less than 10 times the CO quantity introduced, due to the oxidation of the CO during the combustion process. Yet, the high IMEP_{cov} for Fluidbed induces higher combustion instabilities leading to high CO emissions even if the CO flowrate at the intake is lower.

As the main source of NOx for these fuels is due to the thermal mechanism, NO_x production 430 rate increases exponentially with the adiabatic flame temperatures as shown in Figure 14.c. 431 The increase of H₂ contents as in Downdraft induces higher NOx emissions: exponential 432 evolution as a function of adiabatic temperature is accurate but with different coefficients, 433 dependent to the syngas compositions. Notably, for very similar adiabatic flame temperatures, 434 the Downdraft compositions produce more NO_x than the Updraft compositions. Last, as 435 highlighted by Rakopoulos et al. [34], the oxygen content has a significant effect on 436 performances and emissions. When comparing updraft and fluidbed, they exhibit very similar 437 H2 content but CO and therefore oxygen content is much higher for updraft. Rakopoulos et al. 438 showed that NO emissions increase with the degree of oxygenation which could explain the 439 higher NOx levels for updraft mixtures compared to fluidbed. 440









444 Figure 14: Relationship between THC emissions and intake CH4 (a), Exhaust and



Intake CO (b), NOx and T_{ad} (c).

446 (1200 RPM $P_{intake} = 1 \text{ bar } T_{intake} = 300 \text{ K}, \phi_{premixed} = 0.7 \text{ SOI} =$ 447 -18 CAD BTDC).

448 **4** Conclusion

In this study, the effects of the syngas composition on engine operation parameters and emissions are presented and discussed as a function of the syngas/air equivalence ratio in the intake charge and the more reactive fuel pilot injected mass. The main conclusions from these results are the followings:

- With minimal tuning and no engine geometry optimization, indicated thermal efficiencies of over 38% were obtained with all compositions with syngas representing almost 90% of the total energy supplied to the engine.
- Heat release rate profiles showed a strong influence of syngas H₂ content on
 combustion duration and phasing.
- CO₂, present on most of syngas compositions, plays an important role in reducing
 NO_x emissions in dual-fuel operating mode. While this can be interesting for
 complying with emission regulations, too much CO₂ on Syngas can lead to poor
 combustion efficiency requiring more reactive fuel in the pilot injection in order to
 ensure stable engine operation but increase of soot emissions is the consequence.
- The development of the in-cylinder combustion can be empirically predicted based 463 • only on known fundamental properties of the syngas composition as the laminar 464 flame speed. The emissions also can be predicted as a function of the different 465 components in the syngas. This could be useful for live tuning of the engine's control 466 strategy to as a function of the composition fluctuations of the gasifier product gas. 467 Accurate predictions would require a better knowledge of secondary chemical and 468 physical effects of varying syngas compositions such as stretch sensitivity or 469 chemical pathways and species rate of production. 470

Finally, further studies on optical engine would be necessary to give a better understanding on different combustion steps (as diffusion phase, premixed or cool flame due to pre-ignition) and flame propagation as it relates to the different compositions and their respective fundamental combustion properties.

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