Nanoenergetic Materials for MEMS: A Review
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HAL Id: hal-03592682
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Submitted on 1 Mar 2022

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To link to this article:
URL : http://dx.doi.org/10.1109/JMEMS.2007.893519


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Traditional EMs (monomolecular or composite) are relatively easy to prepare (by mixing), and their performances can be predicted and tailored by adjusting the stoichiometry of the chemical reactants. For years, they have been widely used in military, mining, and demolition applications. For two decades, EMs have drawn a growing interest in the scientific community and civil industry since they are very attractive sources of onboard energy to generate gas, heat, and power. Typically, the combustion of propellant produces 5 MJ/kg, while a modern chemical lithium battery used in new laptops only stores 0.5 MJ/kg. Therefore, EMs could have a major impact on microenergetic field. Applications include microthrust [1]–[10], microinitiation [11]–[15], gases for actuation (including injection or moving fluid) [16]–[20], gases for chemical reaction [21]–[24], heating (power) and welding [25], and switching [26]. Various teams have successfully investigated chemical and technological ways to tailor EMs to the targeted applications either to produce gas, heat, or chemical compound. An important challenge that is not really addressed is the compatibility of the EMs with MEMS technologies. This implies two exigencies. First, the thin film of EMs must be grown or deposited at low temperature (below 250 °C). For some applications for which the EMs film is deposited in freestanding microstructures, its stress has to be controlled without any heat treatments. Some well-known semiconductor processing technique such as PVD followed by liftoff [27], [28], screen printing [1], or chemical reaction [13] have been already investigated to prepare and deposit EMs on silicon surface. The second exigency is to minimize heat losses which is one of the most challenging issues to be solved in MEMS applications.

Despite the significant improvements that have been performed through chemical formulation by combining known chemical compounds/molecules [29], the traditional composite and monomolecular EMs feature a relatively slow reaction rate for microscale applications [30]. For example, HMX deflagration will quench in steel tubes of several millimeters in diameter at atmospheric pressure. GAP/AP combustion will quench in glass tubes of 1.4 mm in diameter at atmospheric pressure [31]. To satisfy energy demanding systems of micrometer size, more reactive EMs than traditional ones are required. Significant efforts have been made to introduce metal powder with micro and nanosized particles into traditional EMs. Faster combustion velocities have been demonstrated [32]–[34]. However, difficulties in handling such powders and their incorporation into existing formulations have also been reported. Besides traditional EMs, inorganic energetic composite combining metal oxidizer and metal also called metastable intermolecular composite (MIC) are good candidates as well. They undergo a solid-state redox reaction that is rapid and very
exothermic (nearly twice that of the best monomolecular EM). First results demonstrated mainly empirically that the initiation and combustion properties of EMs are strongly influenced by their microscopical properties. They suggest that reducing the particle size to the nanoscale may result in reduction of the mass-transport rate and therefore would increase the burning rates making these nanoscale EMs (nEMs) attractive alternatives to monomolecular structures.

This paper presents a review of nEMs, a young but very active field of research. To begin, we introduce the recently synthesized nEMs and give the main performance reported by the authors. A section is dedicated to MIC: it is an important class of materials that combine excellent performances with interesting synthetic approaches for MEMS compatibility. While thermodynamic calculations of adiabatic flame temperature and reaction enthalpies are tools to help the choice of desirable EMs, they are not sufficient, in general, for the choice of good material for microscale application where thermal losses have to be taken into account. Section IV will discuss design considerations for nEMs for pyrotechnic systems of micrometer size. Section V will review the different approaches to the synthesis of nEMs. An analysis of the compatibility of the different synthesis routes with MEMS will be given. Lastly, some guidelines for future investigations are provided in the conclusions.

A list of abbreviations used in the review paper is given in Table I.

II. REVIEW OF EMs FOR MICROSCALE APPLICATION

The first route explored by researchers was to adapt traditional EMs to microscale combustion by incorporating nanoparticles of Al into traditional propellants or explosives. Doping composite propellant with thermal conductive nanoscale particles has demonstrated a slight enhancement in the reactivity of the mixture [31], [35]. Then, with the progress of nanotechnology, researchers preferred to combine or synthesize inorganic energetic nanocomposite composed of particles of oxidizer (typically metal oxide) and fuel (mainly Al) to produce MIC.

A. Nanoparticle-Doped Propellant

Nano-Al is the most widely used metallic doping particle for the following reasons.

1) Al is a common metal used in technology and is relatively low cost.
2) The formation of a thin oxide layer around each Al particle prevents Al powder from spontaneous combustion [33], [36].
3) Al can be easily produced in nanoparticles form (50–120 nm) and nano-Al is commercially available for example from NovaCentrix, formerly known as Nanotechnologies, Inc.
4) Al enhances the reactive power of the material by increasing the combustion velocity due to its high thermal conductivity.

In 1997, Brown et al. [34] investigated the influence of the incorporation of microsized Sb particles into KMnO₄ and found that reducing particle size from 14 to 2 µm increased the burning rate by a factor of 4. Ivanov and Tepper [37] reported that by adding aluminium nanoparticles in a propellant formulation, the mixture burning rate could be enhanced by a factor of 5–10. Chiaverini et al. [38] demonstrated an increase of 70% in burning rate of HTPB-based solid propellant doped with 20% of nanoparticles of Al. Armstrong et al. [39] confirmed that the burning rate of the AP-based propellants increases when conventional Al powder is replaced by nano-Al. The burning rate increases from 1 to more than 100 mm/s when the aluminum particle size decreases from 10 µm to 100 nm. This tendency has been confirmed for several types of propellants (HTPB/AP, GAP/AP, and GAP/AN) by numerous authors and studies [31], [40]–[43]. The ignition time is also reduced when the propellant is doped with Al nanoparticles [41]. However, for explosives, the use of metallic nanopowder has not proven to be effective [43].

| TABLE I |
|-------------------------------|----------------------------------|
| ACRONYMS, ABBREVIATIONS, AND NOMENCLATURE |
| AFM | Atomic Force Microscope |
| ALD | Atomic Layer Deposition |
| AN | Ammonium Nitrate (NH₂NO₃) |
| AP | Ammonium Perchlorate (NH₄ClO₄) |
| CNT | Carbon Nanotube |
| CVD | Chemical Vapor Deposition |
| EM | Energetic Materials |
| GAP | Glycidyl Azide Polymer |
| HMX | Cyclotetramethylene-tetranitramine (C₄H₄N₂O₈) |
| HTPB | Hydroxyl-terminated Polybutadiene |
| MEMS | Microelectromechanical Systems |
| MIC | Metastable Intermolecular Composite |
| MO | Metal Oxide |
| PETN | Pentaaerythritol Tetryranitrate (C₁₁H₁₂N₄O₁₂) |
| PSi | Porous Silicon |
| PVD | Physical Vapor Deposition |
| RDX | Cyclotrimethylenenitramine (C₃H₃N₃O₆) |
| SEM | Scanning Electron Microscopy |
| TEM | Transmission Electron Microscopy |
| VD | Vapor Deposition |
| ZPP | Zirconium Perchlorate Potassium |
| α | Diffusivity (cm²/s) |
| Cp | Heat Capacity (J/kgK) |
| d | Particle Diameter (m) |
| k | Thermal Conductivity (W/mK) |
| m | Mass (kg) |
| ρ | Density (kg/m³) |
| r | Combustion Rate (mm²/s) |
| t | Time (s) |
| T₀d | Adiabatic Reaction Temperature (K) |
| ΔH | Heat of Reaction (cal/g) |
In conclusion, doping propellant with Al nanoparticles improves slightly its reactivity and ignition capability; the maximum burning enhancement seems to be reached when the Al content represents 20% of the propellant mass. However, recent studies reveal that the incorporation of nanosized metal particles into propellants does not increase the reaction temperature and burning rate sufficiently to compensate the thermal losses occurring in microscale devices. These nano-Al doped propellants suit mesoscale applications but are not applicable for microscale applications. The quenching diameter is around the millimeter, and the combustion is unstable in the centimeter scale. Furthermore, some authors have reported [40] that an AP-based propellant with pure nano-Al has unstable and nonreproducible combustion because of the difficulty to uniformly mix the ultrafine Al particles into the propellant. Other approaches have been therefore considered. One is the incorporation of carbon nanotubes (CNT), having very high thermal conductivity, into traditional propellant, and the other is developed by Pivkina et al. to produce nanopowder of AN and RDX. Very recently, Manaa et al. [44] presented a study of ignition and combustion of explosive-nanotube mixture. They incorporated single-wall CNT produced by Carbon Nanotechnologies, Inc. inside a PETN EM and demonstrated that the mixture (see Fig. 1) can burn rapidly with local temperature estimated between 1500 °C–2000 °C. Shock wave with an average speed of 6.8 km/s has been measured.

According to the authors, in a longer term, there is hope that CNTs could be used to encapsulate energetic ingredients/molecules to produce an EM that not only has good energetic performance but also has much improved handling and long-term storage capabilities.

An interesting vacuum codeposition technique was presented by Pivkina et al. to synthesize nanostructured AN, RDX, and AN/RDX composites [4], [45]. The typical process of synthesizing nano-RDX and AN/RDX consists of realizing nanopowder of the constituent (AN, RDX) by vacuum condensation of evaporated pure bulk substrates onto the cooled substrates to obtain AN and RDX powder with 50 nm in diameter. Conventional AN and RDX powder with 200 and 50 μm in diameter, respectively, have been compared with nano-AN and RDX powder with 50 nm in diameter. According to the results, the burning rate can be doubled for nanoscale RDX: 15.1 mm/s for the conventional RDX and 30 mm/s for the nanoscale one. Pure AN could not have a sustained combustion; only thermal analysis has been performed and showed that the temperature of maximum heat release for AN nanopowder is less than that for conventional one. Vasylykiv et al. [23], [24] proposed nanoreactors produced by nanoblasts impregnated with particles of C3H6N6O6. The described technique opens the door to the synthesis of a wide range of multimetal oxide ceramic and metal-ceramic composite nanopowders with precise stoichiometries and uniform morphologies.

B. Nanoscale Thermite Material or MIC

Thermite reaction is a highly exothermic reaction that involves a metal reacting with a metallic or a nonmetallic oxide to form a stable oxide and the corresponding metal or nonmetal of the reactant oxide [46]. This is a form of oxidation–reduction reaction that can be written as

\[
M + AO \rightarrow MO + A + \Delta H
\]

where \(M\) is a metal or an alloy, \(A\) is either a metal or a nonmetal, \(MO\) and \(AO\) are their corresponding oxides, and \(\Delta H\) is the heat of reaction. The thermite reactions exhibit fast reaction rates that make their use extremely energy efficient.

Nano-Al is most widely used as the fuel for the reasons detailed in Section II-A plus additional advantages for thermite reactions.

1) Al has low vapor pressure: Al, unlike calcium or magnesium, does not require a pressure-tight reaction vessel for the reaction.

2) Al melting temperature is low (approximately 660 °C) resulting in a low ignition temperature.

Among a large number of possible oxidizers [52], only a few have been investigated by different teams: \(\text{Fe}_2\text{O}_3\), \(\text{MoO}_3\), \(\text{K Mn}_2\text{O}_4\), \(\text{CuO}, \text{NiO}, \text{Mn}_3\text{O}_4, \text{WO}_3, \text{SnO}_2, \text{and SiO}_2\).

In 1995, Aumann et al. [33] produced \(\text{MoO}_3/\text{Al}\) MIC being 20–50 nm in diameter. When the mixture is stoichiometric, the energy density reached 16 kJ/cm³, and the mixture can burn 1000 times faster than macroscale thermite material. Bockmon et al. [47] compared different samples of \(\text{Al/MoO}_3\) MIC fabricated using ultrasonic mixing where nano-Al was used. The measured average combustion velocity increases from approximately 685 to 990 m/s when the Al particle size is decreased from 121 to 44 nm. As a comparison, micrometer scale \(\text{Al/MoO}_3\) burns at 10 mm/s [34]. Authors also note that the reaction rate becomes independent of Al particle diameter below a critical diameter, which is 40 nm in their case. This could be explained by the fact that, when the Al particle diameter decreases, the proportion of \(\text{Al}_2\text{O}_3\) over Al increases resulting in a reduction of the volume of active material and possible inhibition of the thermite reaction.

Granier and Pantoya [48], [49] observed that the burning rate of nano-Al/\(\text{MoO}_3\) MIC is enhanced by a factor of 10 when the average Al particle size decreases from 20 000 to 50 nm. Moreover, they noted that by decreasing the Al particle size from micrometer to nanometer scale in the composite consistently decreases the ignition time by up to two orders of magnitude (from 6 s down to 20 ms) and improves the
repeatability of the composite’s response to ignition. The increased sensitivity to ignition may be explained by the reduction in melting temperature associated with nanoparticles. Sun et al. [50] studied the reactions of nano-Al with O₂ with the average Al particle diameters ranging from 30 to 160 nm. It was shown that Al/O₂ reacts below the Al melting temperature. The heat released by the reaction (approximately 10 kJ/g) is below the theoretical one (25 kJ/g). Bhattacharya et al. [51] investigated the burning rate of nanoscaled CuO/Al and Bi₂O₃/Al. The burning rate reaches the average values of 440 and 150 m/s for nanoscaled CuO/Al and Bi₂O₃/Al, respectively.

Results of empirical studies reported in Section II establish clearly that the initiation temperature, reaction properties, and propagation rate are strongly influenced by the microscopical properties of the EMs, including the size of constituents and intimacy of the contact.

III. STRATEGY TO DESIGN nEMs FOR MICROSCALE APPLICATION

Basically, the synthesis of EMs and the choice of molecules or compounds are mainly guided by molecular modeling and thermochemical codes. This approach has proven its efficiency for traditional EMs and macroscale/mesoscale applications, and significant improvements have been performed through chemical formulation, i.e., combining known chemical compounds/molecules. However, for microscale applications, besides the optimization of energy density given by thermochemical codes, other considerations have to be taken into account to design novel nEMs.

1) The rate of reaction has to be enhanced to minimize heat losses, not only by increasing the heat of reaction.
2) The technological process has to be controlled to adapt the stoichiometry of reactants, the size of particles, the purity of the final mixture, and the intimacy of the contact between the fuel/oxidizer.
3) The contribution of the mass diffusion rate has to be evaluated since it could limit the combustion rate.

For the first point, we propose a theoretical evaluation that is based on the diffusivity parameter, to guide the selection of any EMs for microscopic application. The second point, which is related to the structural control of the material, is very difficult to be theoretically predicted yet, and it is mainly investigated empirically by numerous research teams. Main results will be presented and discussed in Section IV. For the third point, a simple intuitive reasoning can estimate the scale of the particle size below which diffusion process can be neglected. For that, we consider a spherical particle coated with a thin oxide layer that burns from the external surface to the center, as shown in Fig. 2. The diameter of the particle decreases over the time as follows

\[ \pi \times d^2 = r \times t \]

with \( r \) as the combustion rate (mm²/s), and \( d \) as the particle diameter. Therefore, with \( r = 1.5 \text{ mm}^2/\text{s} \) (which is the low limit), particles of 100 nm in diameter would be consumed in 0.01 μs. This time is sufficiently short compared to mass diffusion delay \(^1\) to consider the mass diffusion process negligible for particles having diameter lower than 100 nm.

For the rest of the section, the mass diffusion phenomena will be neglected, and three parameters will be considered to propose a classification of nEMs: the thermal diffusivity \( \alpha \), the heat of reaction \( \Delta H \), and the adiabatic temperature \( T_{ad} \).

1) Diffusivity: \( \alpha = k/(\rho \times C_p) \) where \( k \) is thermal conductivity, and \( \rho \times C_p \) is the volumetric heat capacity. Substances with high thermal diffusivity conduct heat quickly. Tables II and III give the calculated diffusivity for well-known organic EMs and seven thermite EMs: Al/Fe₂O₃, Al/MoO₂, Al/CuO, Al/NiO, Al/SnO₂, Al/SiO₂, and Al/TiO₂.

2) Heat of reaction: for each thermite couple, thermodynamic calculations of heat of reaction (\( \Delta H \)) and adiabatic flame temperature (\( T_{ad} \)) are given in Table IV. The values of \( T_{ad} \) are from [52]. For the purpose of comparison, the values of \( \Delta H \) are from COACH [53], which is an in-house code, and [52], respectively.

3) The adiabatic reaction temperature given in Tables II and IV is the temperature that results from a complete combustion process that occurs without any heat transfer or changes in kinetic or potential energy.

A. Calculation of the Diffusivity of Thermite Materials

We suppose that the aluminum (Al) and metallic oxide (MO)\(^2\) are mixtures of nanoscale powders with \( d_{Al} \) and \( d_{MO} \) being the Al and MO particle diameter. We also assume that the Al-to-MO mass ratio (\( m_{Al}/m_{MO} \)) is the stoichiometric one for each reaction. The thermal conductivity of Al/MO MIC at 300 K is a function of the diameter of the Al and MO particles as well as thermal conductivities of both Al and MO. In a first approximation, we suppose that the MIC that is composed of Al and MO particles in intimate contact can be modeled as an Al/MO bilayer material. The Al and MO layer thickness would be equal to the Al and MO particle diameter.

The resulting bilayer thermal conductivity can be therefore calculated as the following:

\[ k_{Al/MO} = \frac{k_{Al}k_{MO}}{k_{Al} \left( \frac{1}{d_{Al}} + \frac{1}{d_{MO}} \right)} \]

\(^1\)Mass diffusion time of a particle of Al of 100 nm in diameter: hundreds of microns.

\(^2\)MO is Fe₂O₃, MoO₂, CuO, NiO, SnO₂, SiO₂, TiO₂.
TABLE II
DIFFUSIVITY, HEAT OF REACTION, AND ADIABATIC TEMPERATURE FOR THREE DIFFERENT ORGANIC EMs

<table>
<thead>
<tr>
<th>Organic EMs</th>
<th>Diffusivity at 300 K $\alpha$ (cm$^2$/s)</th>
<th>Heat of reaction $\Delta H$ (cal/g)</th>
<th>Adiabatic reaction Temperature $T_{ad}$ (K)</th>
</tr>
</thead>
<tbody>
<tr>
<td>PETN</td>
<td>$1.29 \times 10^{-3}$</td>
<td>1435</td>
<td>4140</td>
</tr>
<tr>
<td>HMX</td>
<td>$0.77 \times 10^{-3}$</td>
<td>1350</td>
<td>3255</td>
</tr>
<tr>
<td>NC</td>
<td>$10^{-3}$</td>
<td>960</td>
<td>3000</td>
</tr>
</tbody>
</table>

TABLE III
DIFFUSIVITY FOR SEVEN DIFFERENT MICs CALCULATED FOR THREE FUEL-OVER-METALLIC OXIDE DIAMETER RATIOS

<table>
<thead>
<tr>
<th>MIC</th>
<th>Diffusivity at 300K $\alpha$ (cm$^2$/s)</th>
<th>Diffusivity at 300K $d_d=0.1d_{MO}$ $\alpha$ (cm$^2$/s)</th>
<th>Diffusivity at 300K $d_d=10^{-3}d_{MO}$ $\alpha$ (cm$^2$/s)</th>
</tr>
</thead>
<tbody>
<tr>
<td>Al/MnO$_2$</td>
<td>$31.64 \times 10^{-3}$</td>
<td>$17 \times 10^{-3}$</td>
<td>$16.1 \times 10^{-3}$</td>
</tr>
<tr>
<td>Al/CuO</td>
<td>$60 \times 10^{-3}$</td>
<td>$33 \times 10^{-3}$</td>
<td>$30 \times 10^{-3}$</td>
</tr>
<tr>
<td>Al/Fe$_2$O$_3$</td>
<td>$85 \times 10^{-3}$</td>
<td>$49 \times 10^{-3}$</td>
<td>$45 \times 10^{-3}$</td>
</tr>
<tr>
<td>Al/FeO</td>
<td>$61 \times 10^{-3}$</td>
<td>$35 \times 10^{-3}$</td>
<td>$32 \times 10^{-3}$</td>
</tr>
<tr>
<td>Al/SnO$_2$</td>
<td>$190 \times 10^{-3}$</td>
<td>$116 \times 10^{-3}$</td>
<td>$107 \times 10^{-3}$</td>
</tr>
<tr>
<td>Al/SiO$_2$</td>
<td>$16.5 \times 10^{-3}$</td>
<td>$9 \times 10^{-3}$</td>
<td>$8.3 \times 10^{-3}$</td>
</tr>
<tr>
<td>Al/TiO$_2$</td>
<td>$48.5 \times 10^{-3}$</td>
<td>$27.3 \times 10^{-3}$</td>
<td>$25 \times 10^{-3}$</td>
</tr>
</tbody>
</table>

TABLE IV
STOICHIOMETRIC MASS RATIO, HEAT OF REACTION ($\Delta H$), AND ADIABATIC TEMPERATURE ($T_{ad}$) FOR SEVEN DIFFERENT MICs

<table>
<thead>
<tr>
<th>MIC</th>
<th>Stoichiometric mass ratio (Al/MO)</th>
<th>Heat of reaction $\Delta H$ (cal/g)</th>
<th>Adiabatic reaction temperature $T_{ad}$ (K)</th>
</tr>
</thead>
<tbody>
<tr>
<td></td>
<td>COACH</td>
<td>Ref. [52]</td>
<td>without phase change</td>
</tr>
<tr>
<td>4Al + 3MnO$_2$</td>
<td>1 / 2.417</td>
<td>1146</td>
<td>1159</td>
</tr>
<tr>
<td>2Al + 3CuO</td>
<td>1 / 4.422</td>
<td>987.8</td>
<td>974.1</td>
</tr>
<tr>
<td>2Al + Fe$_2$O$_3$</td>
<td>1 / 2.959</td>
<td>952.0</td>
<td>945.4</td>
</tr>
<tr>
<td>2Al + 3NiO</td>
<td>1 / 4.154</td>
<td>855.1</td>
<td>822.3</td>
</tr>
<tr>
<td>4Al + 3SnO$_2$</td>
<td>1 / 4.189</td>
<td>686.8</td>
<td>686.8</td>
</tr>
<tr>
<td>4Al + 3SiO$_2$</td>
<td>1 / 1.670</td>
<td>515.0</td>
<td>513.3</td>
</tr>
<tr>
<td>Al + TiO$_2$</td>
<td>1 / 2.221</td>
<td>379.8</td>
<td>365.1</td>
</tr>
</tbody>
</table>

with $k_{Al}$ and $k_{MO}$ as the thermal conductivities at 300 K of Al and MO, respectively, and $d_{Al}$ and $d_{MO}$ as the diameters of Al and MO particles, respectively.

The heat capacity at 300 K of Al/MO can be calculated as the following:

$$C_{PAI/OMO} = \frac{m_{Al} \times C_{PAI} + m_{MO} \times C_{PMO}}{m_{Al} + m_{MO}}$$

with $m_{Al}$ and $m_{MO}$ as the masses of Al and MO contained in the MIC, respectively, and $C_{PAI}$ and $C_{PMO}$ as the heat capacitances of Al and MO, respectively.

B. Results and Comments

In Fig. 3, it can be clearly shown that the Al/MO thermite diffusivities decrease when the MO-to-Al particle diameter ratio increases. In consequence for the rest of the study, $d_{Al}$ is taken which is equal to $d_{MO}$.

Fig. 4 classifies the different EMs in a 2-D diagram: heat of reaction in $y$-axis and diffusivity in $x$-axis. The graph indicates that any EMs placed in the left bottom corner of the graph could not suit microscale application because of too low heat of reaction and insufficient diffusivity. However, the EMs in the upper right parts of the diagram are considered to be well adapted to MEMS because they release high amount of heat, and the rate is expected to be high. To conclude this short study, among investigated MICs, the best...
Fig. 3. Example of diffusivity evolution as a function of the MO-to-Al diameter ratio for three MICs: Al/Fe$_2$O$_3$, Al/NiO, and Al/MnO$_2$.

Fig. 4. Classification of EMs in a 2-D diagram ($\Delta H$, $\alpha$).

ones are: Al/MnO$_2$, Al/Fe$_2$O$_3$, and Al/NiO. From Fig. 4, MICs appear to be a promising category of nEMs that could be a good candidate to realize thin layer of EMs for microscale applications since they have excellent diffusivity, and they can be very reactive compared with traditional organic EMs, and also, they can exhibit high exothermicity. For organic EMs, the best one appears to be PETN that nevertheless presents poor diffusivity.

IV. SYNTHESIS OF nEMs FOR MICROSCALE APPLICATIONS

There are different approaches to synthesize nanosized thermit composite or MIC. Basically, they can be classified into traditional approaches, which include MEMS compatible approaches, nanopatterning, and “bottom-up” or molecular engineering approaches. In traditional approaches, the nanoparticles of fuel and oxidizer are first synthesized or purchased and then mixed together, i.e., powder mixing. In MEMS compatible approaches, the fuel/oxidizer molecules or particles are synthesized and put together in a single process such as sol–gel chemistry and vapor deposition (VD) techniques. In molecular engineering approaches, the atoms or molecules of fuel and oxidizer are first synthesized and then combined using molecular engineering in solution or via a polymer chain. The “bottom-up” approaches are mainly investigated with the aim at developing a fundamental understanding of the evolution of the EMs properties with the size and intimacy of the constituents. The main synthesis approaches of MIC are presented and discussed in the following.

A. Powder Mixing

The easiest method is the physical powder mixing. In recent works, the ultrasonic mixing is mostly employed to combine nano-Al and oxidizer powder [40], [47]–[50], [54]–[56]. Typically, the nano-Al and oxidizer are dispersed in solvents (e.g., hexane) and mixed together with ultrasonic wave. The sonication process is used to break up agglomerates and mix both constituents. After sonication, the mixture is heated to evaporate the solvent. The mixture is often passed through a fine mesh to break any agglomerates formed during the evaporation process and produce submicronic powder. Fig. 5 is a representative SEM image of the Al/MoO$_3$ MIC which, thus, obtained mixture.

Mixing nanopowders of fuel with oxidizer is a simple method. Nevertheless, it presents limitations. First, one is the difficulty to mix intimately ultrafine powder, the second one is the difficulty to obtain a homogeneous distribution of oxidizer and fuel nanoparticles, and thirdly, the manipulation of some powder can be dangerous, and the deposition in thin film or into a microsystem is difficult [30].

B. Sol–Gel/Aerogel Process

A wide variety of glass or glass–ceramic monoliths and nanostructured powders are synthesized through sol–gel technique, since it has the advantages of low temperature processing, high chemical homogeneity, etc. Researchers at Lawrence Livermore National Laboratory have first introduced the use of the sol–gel chemistry to synthesize nEMs [57], [58].

The sol–gel process involves reactions in solution to produce dispersion of nanoparticles in a liquid phase, called “sol” (colloidal solution). By condensation, the sol gives a 3-D solid network, called a “gel,” with the open pores being occupied by the solvent. Solvent removal by evaporation produces the collapse of the open pore structure of the gel and leads to a xerogel. Supercritical drying allows removing the solvent without collapsing the gel structure. This leads to a highly porous and lightweight material called aerogel, with excellent uniformity given that the particles and the pores are both in nanoscale. The sol–gel process is illustrated in Fig. 6.

Tillotson et al. [58] reported about successful sol–gel synthesis of Fe$_2$O$_3$/Al MIC. It consists of clusters of Fe$_2$O$_3$
the aerosol–gel chemistry was also employed to synthesize reaction performance. of the sample mass leading to a significant reduction of the mixture often has organic impurities that can reach up to 10% inhibition of self-sustaining reaction; Second is that sol–gel a separation between the fuel and oxidizer and, therefore, the random distribution of the particles that can lead to locally the process. However, two disadvantages can be noted: First is and properties due to the high porosity. Sol–gel process can also offer could represent 10% in mass of the sample.

The sol–gel chemistry provides process advantages over mixing methods: it is MEMS compatible, low cost, safe, and can potentially produce nEMs with interesting and special properties due to the high porosity. Sol–gel process can also offer good opportunity to tailor the nEMs properties by controlling the process. However, two disadvantages can be noted: First is the random distribution of the particles that can lead to locally a separation between the fuel and oxidizer and, therefore, inhibition of self-sustaining reaction; Second is that sol–gel mixture often has organic impurities that can reach up to 10% of the sample mass leading to a significant reduction of the reaction performance.

Besides the sol–gel chemistry used in [57], [58], and [60], the aero-sol–gel chemistry was also employed to synthesize nano-KMnO₄, CuO, Fe₂O₃, and the corresponding MICs with nano-Al as the fuel [55], [61]–[63]. Clapsaddle et al. [63], for example, reported that the particle size and properties of the aerogel preparation can be tailored easily by controlling the epoxide addition procedure.

Prakash et al. [64] reported a novel aerogel-based process to create a pure nanosized MIC core-shell nanostructure that is obtained by coating a strong oxidizer nanoparticle with a thin layer of relatively mild oxidizer. The authors use a two-temperature aerosol spray-pyrolysis method, as shown in Fig. 8. The core is KMnO₄, and the shell is Fe₂O₃. In this process, an aqueous solution of Fe(NO₃)₃·9H₂O and KMnO₄ is sprayed into droplets (1 μm in diameter). The environment is dried. The aerosol is then thermal cured. First, it is maintained above the decomposition temperature of iron nitrate (typically 120 °C), and then, the temperature is increased to about 240 °C (approximately melting point of permanganate). The 0.6-μm composite particles are then collected on a filter. At 120 °C, iron nitrate decomposes into Fe₂O₃ enrobing with intimately the solid permanganate. At 240 °C, the permanganate melts, and the Fe₂O₃ aggregates around the KMnO₄ particles. The resulting composite nanoparticle of KMnO₄ (150 nm in diameter) coated with Fe₂O₃ (4-nm thick) is shown in Fig. 9. Authors performed reactivity experiments and announced that the reactivity can be moderated over a relatively large range by changing the thickness of the iron oxide. Besides the resulting intimate contact between the reactants, the oxide coating thickness on each nanoparticle is nanoscale and could be precisely controlled to lower the ignition temperature and also not to inhibit the thermit reaction.

Prakash’s process is interesting to precisely investigate the influence of the nEMs structural properties (oxide thickness for example) on its reactivity. However, it is complex and not currently applicable for mass production process.

### C. Vapor Deposition

An alternative route to sol–gel/aerogel chemistry is to deposit alternatively a nanolayer of oxidizer and fuel under vacuum by vapor deposition or sputtering. VD is a chemical process often used in the semiconductor industry for the deposition of thin films of various materials. In a typical VD process, the substrate is exposed to one or more volatile precursors, which react and/or decompose on the substrate surface to produce the desired deposition. Basically, the resulting layer’s thickness ranges from 20 nm to 2 μm. Sputtering is a physical process whereby atoms in a solid target material are ejected into the gas phase due to bombardment of the material by energetic ions. It is also commonly used for thin-film deposition.

VD technique has been employed to deposit PETN thin film by Tappan et al. [27], [28]. Vine et al. [65] reported the VD of Ti/C and Ti/Al multilayers. An increase in the burning rate has been found for multilayered composition compared with the conventional one. Blobaum et al. [66] carried out a study on Al/CuOx multilayer nanofoils deposited by magnetron sputtering onto silicon substrates. The process of deposition is simple: a CuO target is RF sputtered on silicon in alternance with Al target. To avoid metal interdiffusion, the silicon wafer is cooled down during the deposition process. The deposited compositions exhibit a layered structure Al (0.3 μm)/CuOx (0.7 μm), as shown in Fig. 10. The measured heat of reaction of the fabricated nanofoils is 3.9 ± 0.9 kJ/g that is similar to that calculated for the reaction of Al and CuO, as listed in Table IV.
An important dependence of the burning rate with the layer thickness and intermixing conditions has been noticed.

Gavens et al. in 1999 [67] has proposed Al/Ni nanofoils deposited using high vacuum dc and RF sputtering. The total thickness of the multilayers foils is 11 µm. Each layer thickness ranges from 12.5 to 200 nm. Then, the foils are annealed to intermix the fuel and the oxidizer by atomic interdiffusion. The rate and heat of reaction are measured for different bilayer thicknesses and intermixing conditions. The 200-nm-thick bi-layer has a burning rate of 1 m/s. Authors mention that when the bilayer thickness decreases, the burning rate increases and then drops to zero. For a thick layer (200 nm), the intermixing conditions are negligible, whereas for a thin layer, the reaction rate is controlled by the thickness of the intermixed region.

In a fuel/oxidizer multilayer foil deposited by vapor deposition method, the diffusion distances between fuel and oxidizer are reduced 10–1000 times compared to powders, thereby enhancing atomic mixing and reactivity. The presence of impurities and Al oxidation are much smaller in multilayer foils than in sol–gel or powder mixing process because the foils are deposited in high vacuum.

D. Nanostructuring

1) Atomic Layer Deposition (ALD): Among investigated nanostructuring methods, ALD is an ideal process to deposit ultrathin films with high conformal uniformity and precise thickness control. ALD utilizes sequential precursor gas pulses to deposit a film one layer at a time. ALD has been already utilized to deposit many metal oxides as WO$_3$ [68], Co$_3$O$_4$ [69], and NiO [70]. The maximum thickness is a few tens of nanometers. Ferguson et al. [71] employed it to deposit SnO$_2$ oxidizer coatings on nanoparticles of Al. The Al/SnO$_2$ MIC prepared by ALD process is shown in Fig. 11. The first experimentations on the Al−SnO$_2$ samples show a quick and violent reaction despite the low Sn percent by mass and low Al/O molar ratio.

2) Nanoporous Silicon With Oxidizer: Porous silicon (PSi) has been known as a reactive material when McCord et al. [72] discovered a combustion reaction of PSi immersed in nitric acid. The exothermic reactions of PSi with liquid oxygen and gadolinium nitrate were then presented in [73] and [74]. The PSi pores (2–10 nm) are filled with a liquid oxidizer. Because of these findings, PSi-based nEMs were proposed for industrial applications as a component of an airbag initiator [13], [14].

The PSi (Fig. 12) can be produced by electrochemical etching of bulk silicon in solutions containing fluoride (e.g., HF) and H$_2$O$_2$ [75]. The porosity and the structure size of the PSi can be adjusted from 2 to 1000 nm by selecting suitable etching parameters such as fluoride concentration, current density, treatment duration, and starting material [14]. The nanopores are then filled with a liquid oxidizer (Ca(ClO$_4$)$_2$, KClO$_4$, NaClO$_4$, Sulfur, etc.). To enhance the intimacy between
the Si and O$_2$, the PSi matrix can also be filled with the oxidizer by CVD and PVD. The activation energy of the PSi/O$_2$ reaction can be tailored by controlling the SiO$_2$ native layer before the oxidizer loading. The results are very promising: Laucht et al. [13] tested PSI/Ca(ClO$_4$)$_2$ and PSI/Na(ClO$_4$)$_2$ in a calorimetric bomb. Authors noted heats of reaction of 8.6 kJ/g and 9.2 kJ/g for PSI/Ca(ClO$_4$)$_2$ and PSI/Na(ClO$_4$)$_2$, respectively, which are well above that of ZPP (6.3 kJ/g).

One particular advantage of PSi-based nEMs is that silicon is one of the base materials for MEMS. Therefore, the nEMs can be conveniently incorporated into silicon-based MEMS devices. This provides the advantage of low cost production and MEMS compatibility. In particular, the PSi-based nEMs can be easily integrated into semiconductor circuitries.

3) Other Approaches: Menon et al. [76] realized Al/Fe$_2$O$_3$ MIC by embedding an array of Fe$_2$O$_3$ nanowires inside a thin Al film, as described in Fig. 13(a). The process started with electrochemical anodization of Al foil to form nanoporous alumina templates [77], [78]. Then, Fe nanowire was fabricated inside the nanopores by electrochemical deposition. After partial etching of the alumina walls from the top, Fe nanowires were revealed and then oxidized. Finally, the remaining alumina walls were etched away, and at this stage, all of the Fe nanowires were converted into Fe$_2$O$_3$ nanowires by annealing. A typical SEM image of a high-density nanowire array embedded in Al film is shown in Fig. 13(b). The diameter of a single nanowire is about 50 nm, and the density of nanowires for all observed specimens is about $10^{10}$ wires/cm$^2$.

The main advantage of this approach is the precise control of oxidizer and fuel dimensions at nanoscale. The method avoids both the incorporation of impurities and the oxidation of the Al at the fuel-oxidizer interface prior to ignition.

E. Molecular Engineering or “Bottom-Up” Approaches

Molecular engineering has been investigated very recently by only a few teams to control the fuel/oxidizer interfacial contact area and improve the homogeneity of the final material.

One interesting technique is the molecular self-assembly. It means that the fuel nanoparticles will arrange by themselves or enhanced by external forces, in a controlled manner around the oxidizers or vice versa. Fuel or oxidizer molecules can be arranged in inorganic solution or manipulated by using a polymer. Kim and Zachariah [79] presented a method to synthesize MIC in which the Al and Fe$_2$O$_3$ self-assembly is controlled by the electrostatic forces which exist between charged aerosol particles. The authors compared the reactivity of resulting Al/Fe$_2$O$_3$ with a randomly assembled Al/Fe$_2$O$_3$. As shown in Fig. 14(b), the nano-Al particles surround perfectly the surface of Fe$_2$O$_3$ particles and the contact between Al and Fe$_2$O$_3$. The typical SEM shows a high density of Al/Fe$_2$O$_3$ MIC nanowires, where the diameter of a single nanowire is about 50 nm, and the density of nanowires for all observed specimens is about $10^{10}$ wires/cm$^2$.
Fe$_2$O$_3$ is intimate. Fig. 14(a) is a TEM image of nano Al/Fe$_2$O$_3$ synthesized by random Brownian assembly. It can be seen that nano-Al particles form linear chains in contact with the Fe$_2$O$_3$ particles. The authors' results showed that Al/Fe$_2$O$_3$ MIC materials electrostatically assembled are more powerful than those produced via random assembly due certainly to the enhanced fuel/oxidizer interfacial surface. The total measured heat of reaction is 1.8 kJ/g against 0.7 kJ/g for a random assembly that remains lower than the theoretical heat of reaction of Al/Fe$_2$O$_3$ MIC (3.9 kJ/g).

Subramaniam et al. [80] employed a polymer chain on which the nanoparticles (CuO and Al) are binded, as shown schematically in Fig. 15. The polymer is therefore a structural link for the nanoparticles assembly process. In a typical process, CuO nanorods are first prepared from a chemical route (by surfactant templating method). Then, the CuO nanorods are coated with the poly(4-vinyl pyridine) polymer from Aldrich in a sonic bath. After that, the CuO nanorods are removed from the solution, washed, dried, and mixed with nano-Al particles (80 nm in diameter with 2 nm of passivation layer). The resulting Al/CuO MIC is shown in Fig. 16. The highest burning rate measured by the authors is 2000 m/s for Al/CuO MIC (3.9 kJ/g).

V. Conclusion

The R&D of nano-EMs is a quite young field but is very active, and promising results could lead to interesting breakthrough in the field of microenergetic devices. For years, different synthesis approaches to enhance the performances of EMs and make them applicable to microscopic systems have been investigated and reported in this review.

The first approach consists of doping traditional EMs (HTBP, PETN, RDX, ...) with nanoparticles of Al and, more recently, CNT. The results are quite interesting but suffer from two main disadvantages. Besides the difficulty to get a final homogeneous mixture, the procedure of elaboration can be hazardous, and the finally obtained material has to be manipulated and reported on the initiator which is, if possible, very difficult.

The second approach widely investigated consists of elaborating MICs that exhibit very powerful reaction mainly because of its high redox capability and high thermal diffusivity. Different nano-based processes have been investigated to reduce the diffusion distances between reactant species and increase the surface-over-volume ratio. These MICs can be synthesized in different ways.

Powder mixing is a widely used method but not really applicable to microenergetic applications. Sol–gel is an interesting approach mainly because it presents process advantages in terms of homogeneity, cost, and safety. Fabrication of the nano-PSi-based EM is also very innovative and promising because it is totally integratable into standard semiconductor technologies. In particular, the nano-PSi-based EMs can be easily integrated on a silicon chip.

Modern technologies as nanopatterning provide nice opportunities to get a new class of tailored EMs. The elaboration of energetic multilayer nanofoils from PVD or sputtering is also a promising approach for the integration of nano-EMs within microsystems because of the compatibility with mass production process, the good quality of the fabricated layer, and the possibility to control precisely each metal and oxide thickness layer and interdiffusion region. More recently, a couple of “bottom-up” approaches have been investigated and seem to provide a good means to better understand the structural mechanisms governing the EMs thermal and dynamic properties. This “bottom-up” route would enable molecularly manipulated energetic substances and formulations having tailored chemical and physical properties, high performance, low sensitivity, and multifunctional capabilities [16], [21], [81]. This is a good route to access to a fundamental understanding of the evolution of the EMs properties with the size and intimacy of the constituents.
Although there has been considerable success in formulating new MIC with enhanced energy-release rates, the subject of achieving a precise control over the reactivity of nEMs is an opportunity for further research. To achieve a better understanding of nEMs properties, progress in computational method and tools is requested to assess the reactivity to predict the stability of these new classes of nEMs. Fundamental computations aimed toward the simulation of the behavior of nEMs are in the primary stage.

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