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# 1 Steady shear viscosity of blends of fresh and RAP binders with rejuvenator:

### 2 experimental and estimated results

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- 10

### 11 Abstract

12 This paper focuses on the influence of the RAP-extracted binder and rejuvenator contents on the

13 steady shear viscosity obtained as a linear viscoelastic property of different binder blends. One pure

fresh 50/70 binder, a RAP-extracted binder and a rejuvenator of vegetal origin were mixed in different dosages. Steady shear viscosity ( $\eta_0$ ) values at different temperatures (from 25°C to 85°C)

were determined from complex shear modulus results for all tested binders. In addition,  $\eta_0(T)$ 

values of all binder blends were estimated from  $\eta_0(T)$  values of base constituents by using two

18 different approaches. Good correspondences with experimental results were found.

19

20 Keywords: RAP binder; rejuvenator; steady shear viscosity; binder blends; estimations.

21

### 22 Highlights

- Viscoelastic properties (steady shear viscosity) of several binders were studied.
- Steady shear viscosity  $\eta_0$  at 85°C was determined from complex shear modulus results.
- $\eta_0(T)$  were calculated from  $\eta_0(T_{ref} = 85^{\circ}\text{C})$  and  $a_T$  shift factor at temperature T.
- 26  $\eta_0(T)$  of all binder blends were estimated with two different approaches.
- 27 28

## 29 **1. Introduction**

For economic and environmental reasons, the use of Reclaimed Asphalt Pavement (RAP) in the production of new bituminous mixtures HMA (hot-mix asphalt) [1], [2], [3], [4], [5] and WMA

(warm-mix asphalt) [6], [7] has become a common strategy for the construction and maintenance of
 roads.

Due to the long-term aging process, the physical and rheological properties as well as the chemical structure of the RAP-bitumen suffer irreversible changes [8], [9]. For these reasons, in order to achieve an adequate workability and good mechanical performance of a new bituminous mixture containing RAP material, a softer bitumen [10], [11] or some rejuvenators [12], [13], [14], [15], [16], [17] could be used.

Many studies showed the efficiency of using vegetal oils by evaluating the conventional properties (such as penetration, ductility, Fraass temperature, ring and ball temperature), fatigue or complex modulus of final blends produced with these products, different RAP binders and different base fresh binders [1], [18], [19], [20], [21], [22]. The binder has a very complex thermomechanical behaviour that is influenced by the temperature, the speed and the of the load level. In a width range of loading the behaviour can be considered as linear viscoelastic [23]. The linear viscoelastic response of a binder is commonly analysed in terms of complex shear modulus.

Di Benedetto and Corté (2005) indicated different behaviors of bituminous materials based on the temperature (T) and the amplitude of the deformation ( $|\varepsilon|$ ). As it can be observed in Figure 1, the following behaviors of binders can be distinguished: the brittle and the ductile domains, the linear elastic behavior (characterized by E and G), the linear viscoelastic (LVE) domain (characterized by E\* and G\*), the purely viscous Newtonian behavior (characterized by the viscosity  $\eta$ ), the fragile

52 rupture (characterized by the toughness K<sub>c</sub>) and the non-linear domain.



53

54 Figure 1. Binder behaviors as a function of T and  $|\varepsilon|$  [23].

55 The relation between temperature and viscosity is very important in the context of determining 56 and evaluating some characteristics such as adhesion, rheology, durability, etc. of binders.

57 Therefore, the characterization and the understanding of the viscoelastic behaviour of binders it 58 can be considered essential in the design process of a bituminous mixture due to the fact that the 59 binder has an important influence on the mechanical response of the bituminous mixture [7].

60 Complex shear modulus ( $G^*$ ) together with the steady and complex shear viscosities are the most 61 important rheological properties, used to characterize the linear viscoelastic behaviour of binders. 62 Viscosity is a fundamental characteristic property of binders and rejuvenators and it can be 63 determined by several methods [24], [25], [26].

64 The complex viscosity ( $\eta^*$ ) determined by oscillatory test is defined as the ratio between the 65 complex shear modulus  $G^*$  and the angular frequency  $\omega$ , multiplied by  $i(i^2=-1)$ .

66 Steady shear viscosity ( $\eta_0$ ) at a given temperature corresponds to the limit of the norm of the 67 complex viscosity  $|\eta^*|$  when angular frequency  $\omega$  tends towards zero.

68 The objective of this paper is to study the properties of several binder blends between one type 69 of fresh binder, a RAP binder with/without a rejuvenator of vegetal origin by evaluating the steady 70 shear viscosity at different temperatures ( $\eta_0(T)$ ). The experimental plan includes seventeen 71 binders. The materials used are specific for Romania.

In addition, steady shear viscosity values of all binder blends were estimated with two different approaches from values of  $\eta_0(T)$  of the base constituents. Correlation plots between the experimental and estimated results (with both approaches) were analysed in order to verify if these two estimation approaches are valid for these tested binders. Similar estimation methods were used in order to estimate the conventional properties of the same binder blends in [27].

77

### 78 2. Materials

Three base materials were used: one type of fresh binder (a 50/70 pen. grade binder), a RAP binder
(extracted and recovered from a RAP material) and one type of rejuvenator (a mixture of vegetal
oils).

The RAP material was classified and described by performing the tests required by EN 13108-8
[28]. Its measured binder content is 4.0%.

The rejuvenator (Rej) was used in four dosages from 0% to 15% by mass of RAP binder (with a 5% increment) corresponding to 0.0%, 0.2%, 0.4% and 0.6% by mass of the RAP material.

The experimental campaign considers 17 binders: 15 blends (12 blends of the three base materials and 3 blends between the base RAP binder and the rejuvenator) and the two base binders (Table 1). It must be mentioned that different properties of the same binder blends were analysed in Forton et. al [27, 29].

Proportions of these three base components (RAP binder, fresh binder and rejuvenator) were calculated in order to reproduce real ratios within corresponding bituminous mixtures (having a total binder content 5.6%) containing 25%, 50%, 75% and 100% RAP material and different dosages of Rej. A summary table regarding the proportions for all binders is reported in Table 1.

To simplify, binder blends were named according to the penetration grade of the fresh bitumen (50/70), the dosage of RAP material used for the production of bituminous mixture (25%, 50%,

96 75%) and the dosage of the rejuvenator by the mass of RAP bitumen (5%, 10%, 15%).

97 Table 1. Weight proportion of the three base materials (fresh and RAP binders and the rejuvenator)

98 in tested binders [24]

	weight proportion in							
Bitumens	percent (%)							
	50/70	RAP	Rej					
50/70	100.0	-	-					
RAP	-	100.0	-					
RAP + 5% Rej	-	95.2	4.8					
RAP + 10% Rej	-	90.9	9.1					
RAP + 15% Rej	-	87.0	13.0					
50/70 + 25% RAP	82.1	17.9	-					
50/70 + 50% RAP	64.3	35.7	-					
50/70 + 75% RAP	46.4	53.6	-					
50/70 + 25% RAP + 5% Rej	81.4	17.7	0.9					
50/70 + 50% RAP + 5% Rej	63.1	35.1	1.8					
50/70 + 75% RAP + 5% Rej	45.22	52.17	2.61					
50/70 + 25% RAP + 10% Rej	80.7	17.5	1.8					
50/70 + 50% RAP + 10% Rej	62.1	34.5	3.4					
50/70 + 75% RAP + 10% Rej	44.1	50.8	5.1					
50/70 + 25% RAP + 15% Rej	80.0	17.4	2.6					
50/70 + 50% RAP + 15% Rej	61.0	33.9	5.1					
50/70 + 75% RAP + 15% Rej	43.0	49.6	7.4					

99 The procedures used to produce the studied binder blends were chosen in order to reproduce in 100 laboratory the actual production process of bituminous mixtures containing RAP material and 101 rejuvenator.

102 Therefore, the fresh and RAP binders were heated at 160°C in a thermostatic oven. The 103 rejuvenator was not heated before blending. All binder blends were produced in two steps. First, the 104 rejuvenator (at ambient temperature) was added to fresh binder (which was heated for 30 min) and 105 this preliminary blend was manually mixed for 5 minutes. This blend was than heated for 20 min at 106 160°C. Secondly, the RAP binder was added, and this final blend was manually mixed for 5
 107 minutes in order to produce a homogenous blend. The 160°C temperature was chosen with respect
 108 to the Romanian technical specifications for the production of bituminous mixtures.

#### 109 **3. Experimental campaign**

#### 110 3.1 Complex shear modulus test

111 A DSR apparatus with a 25 mm diameter plate-plate configuration with a 1 mm gap was used at 112 temperatures ranging from 25°C to 85°C and at frequencies ranging from 0.1 Hz to 10 Hz.

As all the tests, for all considered binder blends, were performed at intermediate and high temperatures, a 5% shear strain amplitude, which is the Linear Visco-Elastic domain according to Airey, Rahimzadeh & Collop (2003) [30], was imposed.

116 Tests were performed at 5% targeted shear strain amplitude ( $\gamma$ ), by imposing a sinusoidal shear 117 strain signal and measuring the corresponding shear stress. However, the torque limit of the 118 instrument was reached for strain amplitudes lower than the 5% targeted value during some tests at 119 the lowest temperatures and highest frequencies [29]. Therefore, these tests were performed at 120 strain amplitudes lower than 5%.

In order to highlight the influence of RAP binder and Rej content on the behaviour of the final blends, master curves of norm of complex shear modulus  $|G^*|$  were built for all blends at a reference temperature of  $T_{ref} = 85^{\circ}$ C. The Time–Temperature Superposition Principle (TTSP) was applied and verified for all binders, temperature shift factors  $(a_T)$  were obtained and the master curves were plotted for all binders according to equation 1 [9], [27], [31], [32], [33].

$$|G^{*}(T,f)| = |G^{*}(T_{ref}, a_{T} \cdot f)|$$
(1)

126 where T is the test temperature,  $T_{ref}$  is the reference temperature and f is the frequency.

127 Master curves of  $|G^*|$  and shift factors  $a_T$  at a reference temperature of 85°C for the two base 128 binders and RAP + Rej blends are shown in Figure 2 a and b, as an example. Data obtained at low 129 temperature/high frequency during cycles performed at variable strain amplitude  $\gamma$  (lower than the 130 targeted 5% value) are plotted with crossed (×).

131 The data presented in Black diagram (Figure 2 c) are located on a unique curve for each of the 132 considered blends. It means that the time temperature superposition principle (TTSP) is valid for all 133 tested binders. Then they are thermorheologically simple even when containing the rejuvenator.

It is observed that with increasing Rej content in the blends, the master curves of RAP + Rej blends progressively approach the one of the pure bitumen. The same tendency was observed for the  $a_T$  shift factors, with blends RAP + 10% Rej and RAP + 15% Rej having even lower  $a_T$  values than fresh 50/70 binder. Shift factor values  $a_T$  at a reference temperature of 85°C for all binders are reported in Table A.1 (Appendix). Similar tendencies were observed in Forton et. al [27, 29] for the blends produced with fresh binder, 50% RAP and different amounts of rejuvenator at a reference temperature of 25°C.

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145 *3.2 Determination of steady shear viscosity at 85°C from DSR test results* 

146 Steady shear viscosity ( $\eta_0$ ) at a given temperature (85°C) corresponds to the limit of the norm of 147 the complex viscosity  $|\eta^*|$  when the angular frequency  $\omega$  tends towards zero (equation 2) [27].

$$\eta_0 = |\eta^*| = \frac{|G^*|}{\omega}, \omega \to 0$$
<sup>(2)</sup>

 $log|G^*| = log \,\omega + log|\eta^*| - logarithmic form of equation (2)$ (3)

As an example, Figure 3 ( $|G^*|$  vs.  $\omega$ , in a log-log scale) shows how  $\eta_0$  values were obtained, by highlighting the Newtonian behaviour by analysing the high temperature/low frequency part of the curves [27], for fresh binder, RAP binder and their blends. The obtained  $\eta_0$  values for all binders are shown in Table A.1 (Appendix).

As it can be observed in Figure 4,  $\eta_0$  values at 85°C increase with the increase of RAP binder content in the blends. Linear regressions (in logarithmic scale) could be performed on the obtained  $\eta_0$  values at different temperatures with good approximation. Moreover,  $\eta_0$  values decrease with the increase of rejuvenator content in the blends. These results were expected.





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#### 160 3.3 Determination of steady shear viscosity at different temperatures

161 In order to calculate  $\eta_0$  values for all binders at different temperatures equation (4) was used. In this 162 equation, the value of the steady shear viscosity at a temperature *T*,  $(\eta_0(T))$  is calculated from the 163 values of the steady shear viscosity at the reference temperature of 85°C,  $\eta_0(T_{ref} = 85^{\circ}C)$ , 164 multiplied by the temperature shift factor at temperature *T*,  $a_T$ . The same shift factors used to build 165  $|G^*|$  master curves are used.

$$\eta_0(T) = a_T \cdot \eta_0(T_{ref}) \tag{4}$$

166 The steady shear viscosity was calculated with equation (4) for all binders at temperatures from 167 25°C to 75°C. Results are reported in Table A.1 (Appendix) and in Figure 5.



Figure 5. Results of steady shear viscosity at different temperatures for all binders: (a)  $T = 25^{\circ}C$ ; (b)  $T = 35^{\circ}C$ ; (c)  $T = 45^{\circ}C$ ; (d)  $T = 55^{\circ}C$ ; (e)  $T = 65^{\circ}C$ ; (f)  $T = 75^{\circ}C$ .

171 As expected, values of  $\eta_0(T)$  decrease with the increase of temperature. Also,  $\eta_0(T)$  increase with 172 increasing RAP binder content in the blends and decrease with the increase of Rej content within 173 blends. Linear regressions in logarithmic scale as a function of RAP binder content were performed 174 with rather good approximation for all binders, at all considered temperatures. As it can be observed 175 in Figure 5 a and b and Table A.1 (Appendix), the values of  $\eta_0(T)$  at low temperatures (25°C and 176 35°C) of the blends containing 10% Rej (independently of the RAP binder content) are close to the results obtained for the base fresh binder. This observation is not valid at higher temperatures 177 178 (where  $\eta_0(T)$  increases with the increasing RAP bitumen content).

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#### 182 **4. Estimation of steady shear viscosity**

183 Two approaches were proposed in order to determine the estimated values of  $\eta_0(T)$  at different 184 temperatures (from 25°C to 85°C) of all produced binder blends. The obtained results were then 185 compared with the experimental values determined in Section 3.3. Similar estimation approaches 186 were used in the case of the conventional properties of same binder blends and both approaches 187 were considered valid (good correspondences were found between estimated and experimental 188 values of the European conventional parameters) [27].

#### 189 *4.1* 1<sup>st</sup> approach: two-way blending rule

190 The 1<sup>st</sup> approach considers the classical blending rule expressed in equation (5), which supposes 191 that  $\eta_0(T)$  values for fresh binder, RAP binder and blends of RAP + Rej (at the three different 192 dosages used in the study) are used as input values. For this approach,  $\eta_0(T)$  values for RAP + Rej 193 blends must be known from experimental tests, which is a drawback as these blends should be 194 tested for each of the three considered Rej contents (5%, 10% and 15%).

In the equation (5), known as log-log rule, [34], the estimated value of  $\eta_0$  of any of the 12 blends at a given temperature ( $\eta_{blend \, est. 1}(T)$ ) is determined from the experimental results of fresh binder  $\eta_0(T)_{(50/70)}$ , and RAP + Rej blends,  $\eta_0(T)_{(RAP+Rej)}$ , as a function of the relative mass concentration *a* of fresh binder in the blend.

$$\log \eta_{blend \ est. \ 1}(T) = a \cdot \log \eta_0(T)_{(50/70)} + (1-a) \cdot \log \eta_0(T)_{(RAP+Rej)}$$
(5)

### 199 *4.2* 2<sup>*nd*</sup> approach: three-way blending rule

200 The 2<sup>nd</sup> approach consists in the three-way blending rule expressed in equation (6), which requires 201 as input data only the values of  $\eta_0(T)$  for the three base materials used in this study.

The estimated values of steady shear viscosity at a given temperature for any of the 15 blends  $(\eta_{blend \ est. \ 2 \ (T)})$  were calculated from the experimental results of fresh binder  $(\eta_0(T)_{(50/70)})$ , RAP binder  $(\eta_0(T)_{(RAP)})$  and from equivalent values of the rejuvenator  $(\eta_0(T)_{(Rej)})$ .

$$\log \eta_{blend\ est.\ 2}(T) = a \cdot \log \eta_0(T)_{(50/70)} + b \cdot \log \eta_0(T)_{(RAP)} + c \cdot \log \eta_0(T)_{(Rej)}$$
(6)

where a, b and c are the relative mass concentrations of the three base materials, respectively (a + b + c = 1).

Equation (6) could be rewritten as equation (7), considering that *a* and *c* could be calculated as functions of *b* and of the percentage of Rej by the mass of RAP binder,  $r (c = r \cdot b)$ .

$$\log \eta_{blend\ est.\ 2}(T) = [1 - b \cdot (1 + r)] \cdot \log \eta_0(T)_{(50/70)} + b \cdot \log \eta_0(T)_{(RAP)} + b \cdot r \cdot \log \eta_0(T)_{(Rej)}$$
(7)

In order to obtain the equivalent values for the rejuvenator of  $(\eta_0(T)_{(Rej)})$  at a given temperature, it was necessary to optimize the correlation between experimental results and estimated values of blends  $(\eta_{blend \ est. \ 2\ (T)})$ . The least square method was used by maximizing the R<sup>2</sup> value of the estimated vs. experimental correlation in order to obtain  $\eta_0(T)_{(Rej)}$ . It should be mentioned that these equivalent  $\eta_0(T)_{(Rej)}$  values were used only for this second estimation approach, which is valid only for rather small Rej content (up to 15%). This equivalent viscosity is not equal to the viscosity of the rejuvenator used for this study.

In Figure 6, the experimental results of  $\eta_0$  at different temperatures for RAP + Rej blends are plotted as a function of the rejuvenator content, together with the equivalent values of  $\eta_0(T)_{(Rej)}$ determined for the rejuvenator. Linear regressions could be performed with excellent approximation at all considered temperatures. It was observed that all the regression lines can be obtained with the same R<sup>2</sup> (influence only on the 4<sup>th</sup> decimal) when considering that all lines intersect a unique point: 35% Rej content and 0.038 Pa·s. Figure 6 gives an overview of these results.

- 222 These results led to the idea of a "temperature-independent constant content-viscosity couple"
- 223 for the rejuvenator which is expressed in Equations (8) and (9), where viscosity is expressed in Pa.s.
- 224 Equation (8) is in fact equation (6) in which the amount of the fresh binder is equal to zero and
- 225  $\eta_{blend \, est. 2}(T) = \eta_{RAP+35\% Rei} = 0.038 \, Pa \cdot s.$  Equation (7) can then be rewritten as in equation (10), consisting in the final form of the  $2^{nd}$  approach when viscosity is expressed in Pa.s. 226

$$\log 0.038 = 0.65 \log \eta_0(T)_{(RAP)} + 0.35 \log \eta_0(T)_{(Rej)}$$
(8)

$$\log \eta_0(T)_{(Rej)} = \frac{\log 0.038}{0.35} - \frac{0.65}{0.35} \log \eta_0(T)_{(RAP)}$$
(9)

 $\log \eta_{blend\ est.2}(T) = \left[1 - b(1+r)\right] \log \eta_0(T)_{(50/70)} + b\left(1 - \frac{0.65}{0.35}r\right) \log \eta_0(T)_{(RAP)} + \frac{b \cdot r}{0.35} \log 0.038$ (10)



227



#### 4.3 Analysis of results 230

Plots of the estimated results obtained from the 1<sup>st</sup> approach and the 2<sup>nd</sup> approach versus the 231 experimental results are and shown in Figure 7. Estimated results of  $\eta_0(T)$  of all blends are reported 232 233 in Table A.2 and Table A.3 (Appendix).

The coefficient of determination  $(R^2)$  was calculated for each plot with respect to the equality 234 235 line.

In order to calculate  $R^2$  for the 1<sup>st</sup> approach, steady shear viscosity values of the base constituents (fresh 50/70 binder, RAP binder and the three RAP + Rej blends, for a total of five binders) were not taken into account. Regarding the 2<sup>nd</sup> approach, R<sup>2</sup> was calculated without considering the steady shear viscosity values of the base constituents: fresh 50/70 binder, RAP binder and the 'temperature-independent constant content-viscosity couple' for the rejuvenator. These values are not considered because they correspond to input data, which are perfectly estimated.



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As it can be observed in Figure 7, the estimated results ( $\eta_{blend est. 1}(T)$ ,  $\eta_{blend est. 2}(T)$ ) of all binder blends are close to the corresponding experimental results. It can be noticed that with the decrease of temperature (from 85°C to 25°C) R<sup>2</sup> values decrease but they are still satisfactory (always higher than 0.960).

R<sup>2</sup> values obtained in the case of the  $2^{nd}$  approach are always higher than 0.969 and greater than the values obtained with the  $1^{st}$  approach. Considering the goodness of the correlation with experimental points and the reduced number of input data necessary, the  $2^{nd}$  approach can be considered more advantageous than the  $1^{st}$  approach.

As a general comment, with the 2<sup>nd</sup> approach a total of 105  $\eta_0$  values were estimated, at seven different temperatures for 15 blends, using as input data the experimental results of  $\eta_0$  obtained at a reference temperature of 85°C,  $\eta_0(T_{ref} = 85^{\circ}C)$ , for fresh and RAP binders and the 'temperatureindependent constant couple' for the rejuvenator. A global correlation plot between all these estimated values obtained by applying the 2<sup>nd</sup> approach and the experimental values of the 15 blends is shown in Figure 8. A satisfactory global R<sup>2</sup> was found (0.977).



Figure 8. Global correlation plot of estimated (2<sup>nd</sup> approach) vs. experimental results of  $\eta_0(T)$  at temperatures from 85°C to 25°C for the 15 blends of fresh 50/70, RAP binders and rejuvenator (Rej).

#### 263 **5. Conclusions**

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The objectives of the presented work were to study the influence of the addition of a rejuvenator of vegetal origin on the steady shear viscosity of binder blends of fresh and RAP binders and to propose two approaches in order to estimate  $\eta_0$  of all blends from experimental results obtained for the base constituents.

Three base materials were used in this study: one type of pure bitumen (50/70), a RAP bitumen and a rejuvenator, which were blended in different proportions, producing 17 binders (including the two base bitumens).

271 Complex shear modulus tests were performed on all binders at temperatures from 25°C to 85°C 272 and at frequencies from 0.1 Hz to 10 Hz. The Time-Temperature Superposition Principle was validated for all tested binders. Steady shear viscosity ( $\eta_0$ ) at 85°C was obtained as the norm of 273 complex viscosity at high temperature/low frequency in the domain of Newtonian behaviour of 274 binders.  $\eta_0$  values at temperatures from 75°C to 25°C were calculated from the experimental values 275 of  $\eta_0$  at the reference temperature of 85°C, ( $\eta_0(T_{ref} = 85^{\circ}C)$ ), multiplied by the shift factors. Two 276 different estimation approaches were proposed and  $\eta_0$  values were estimated for all produced 277 278 binder blends at all temperatures from 25°C to 85°C, from  $\eta_0$  values of base constituents.

From the obtained results it can be concluded that, for all temperatures,  $\eta_0$  values are increasing with the increase of RAP binder content and with the decrease of Rej content in the blends. The addition of the rejuvenator was observed to counterbalance the stiffening effect of the RAP binder in the blends. These effects that were expected are clearly quantified and well estimated by the two proposed approaches.

Slightly better correspondence was found between estimated  $\eta_0$  values obtained with the 2<sup>nd</sup> approach, which is an original input of this work, and experimental values (R<sup>2</sup> values always higher than those found with the 1<sup>st</sup> approach, which is based on the classical log-log rule). Moreover, the

287 2<sup>nd</sup> approach has also the great advantage to need only one data for each of the three base 288 constituents when the dosage if fixed.

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## <u>Appendix</u>

Table A.1. $a_T$ shift factors values at a reference temperature of 85°C and experimental results of steady shear viscosity, $\eta_0(T)$ , at different temperatures for a	all
tested binders.	

Binders	$a_T$ (-) at T <sub>ref</sub> = 85°C					$\eta_0(T)$ , (Pa·s)								
Diliders	85°C	75°C	65°C	55°C	45°C	35°C	25°C	85°C	75°C	65°C	55°C	45°C	35°C	25°C
50/70	1	$2.87 \times 10^{0}$	$9.65 \times 10^{0}$	$3.95 \times 10^{1}$	$2.08 \times 10^{2}$	$1.51 \times 10^{3}$	$1.67 \times 10^{4}$	$1.32 \times 10^{1}$	$3.79 \times 10^{1}$	$1.27 \times 10^{2}$	$5.22 \times 10^{2}$	$2.74 \times 10^{3}$	$1.99 \times 10^{4}$	$2.21 \times 10^{5}$
RAP	1	$4.14 \times 10^{0}$	$2.05 \times 10^{1}$	$1.26 \times 10^{2}$	$9.96 \times 10^{2}$	$1.09 \times 10^{4}$	$1.77 \times 10^{5}$	$3.39 \times 10^{2}$	$1.41 \times 10^{3}$	$6.96 \times 10^3$	$4.26 \times 10^{4}$	$3.38 \times 10^{5}$	$3.69 \times 10^{6}$	$6.01 \times 10^{7}$
RAP + 5% Rej	1	$3.33 \times 10^{0}$	$1.30 \times 10^{1}$	$6.17 \times 10^{1}$	$3.72 \times 10^{2}$	$3.02 \times 10^{3}$	$3.59 \times 10^{4}$	9.36×10 <sup>1</sup>	$3.12 \times 10^{2}$	$1.22 \times 10^{3}$	$5.78 \times 10^{3}$	$3.48 \times 10^{4}$	$2.83 \times 10^{5}$	$3.36 \times 10^{6}$
RAP + 10% Rej	1	$2.70 \times 10^{0}$	$8.40 \times 10^{0}$	$3.09 \times 10^{1}$	$1.41 \times 10^{2}$	$8.33 \times 10^{2}$	$6.97 \times 10^{3}$	$2.90 \times 10^{1}$	$7.84 \times 10^{1}$	$2.44 \times 10^{2}$	$8.97 \times 10^{2}$	$4.08 \times 10^{3}$	$2.42 \times 10^{4}$	$2.02 \times 10^{5}$
RAP + 15% Rej	1	$2.35 \times 10^{0}$	$6.24 \times 10^{0}$	$1.94 \times 10^{1}$	$7.30 \times 10^{1}$	$3.52 \times 10^{2}$	$2.35 \times 10^{3}$	$1.27 \times 10^{1}$	$2.99 \times 10^{1}$	$7.96 \times 10^{1}$	$2.47 \times 10^{2}$	$9.30 \times 10^{2}$	$4.49 \times 10^{3}$	$3.02 \times 10^{4}$
50/70 + 25% RAP	1	$3.14 \times 10^{0}$	$1.16 \times 10^{1}$	$5.28 \times 10^{1}$	$3.08 \times 10^{2}$	$2.47 \times 10^{3}$	$3.01 \times 10^4$	$2.31 \times 10^{1}$	$7.27 \times 10^{1}$	$2.69 \times 10^{2}$	$1.22 \times 10^{3}$	$7.11 \times 10^{3}$	$5.71 \times 10^{4}$	$6.95 \times 10^{5}$
50/70 + 25% RAP + 5% Rej	1	$2.96 \times 10^{0}$	$1.03 \times 10^{1}$	$4.38 \times 10^{1}$	$2.39 \times 10^{2}$	$1.81 \times 10^{3}$	$2.10 \times 10^4$	$2.16 \times 10^{1}$	$6.39 \times 10^{1}$	$2.22 \times 10^{2}$	$9.45 \times 10^2$	$5.17 \times 10^{3}$	$3.91 \times 10^4$	$4.54 \times 10^{5}$
50/70 + 25% RAP + 10% Rej	1	$2.90 \times 10^{0}$	$9.83 \times 10^{0}$	$4.07 \times 10^{1}$	$2.16 \times 10^{2}$	$1.58 \times 10^{3}$	$1.76 \times 10^{4}$	$1.36 \times 10^{1}$	$3.93 \times 10^{1}$	$1.34 \times 10^{2}$	$5.52 \times 10^{2}$	$2.93 \times 10^{3}$	$2.14 \times 10^{4}$	$2.39 \times 10^{5}$
50/70 + 25% RAP + 15% Rej	1	$2.84 \times 10^{0}$	$9.45 \times 10^{0}$	$3.82 \times 10^{1}$	$1.97 \times 10^{2}$	$1.40 \times 10^{3}$	$1.50 \times 10^{4}$	$1.14 \times 10^{1}$	$3.24 \times 10^{1}$	$1.08 \times 10^{2}$	$4.35 \times 10^{2}$	$2.25 \times 10^{3}$	$1.59 \times 10^{4}$	$1.71 \times 10^{5}$
50/70 + 50% RAP	1	$3.37 \times 10^{0}$	$1.34 \times 10^{1}$	$6.54 \times 10^{1}$	$4.09 \times 10^{2}$	$3.51 \times 10^{3}$	$4.51 \times 10^{4}$	$4.17 \times 10^{1}$	$1.40 \times 10^{2}$	$5.59 \times 10^{2}$	$2.72 \times 10^{3}$	$1.71 \times 10^{4}$	$1.46 \times 10^{5}$	$1.88 \times 10^{6}$
50/70 + 50% RAP + 5% Rej	1	$3.01 \times 10^{0}$	$1.06 \times 10^{1}$	$4.55 \times 10^{1}$	$2.48 \times 10^{2}$	$1.84 \times 10^{3}$	$2.04 \times 10^{4}$	$2.32 \times 10^{1}$	$7.00 \times 10^{1}$	$2.47 \times 10^{2}$	$1.06 \times 10^{3}$	$5.76 \times 10^{3}$	$4.28 \times 10^{4}$	$4.74 \times 10^{5}$
50/70 + 50% RAP + 10% Rej	1	$2.82 \times 10^{0}$	$9.28 \times 10^{0}$	$3.70 \times 10^{1}$	$1.88 \times 10^{2}$	$1.31 \times 10^{3}$	$1.37 \times 10^{4}$	$1.47 \times 10^{1}$	$4.15 \times 10^{1}$	$1.37 \times 10^{2}$	$5.46 \times 10^{2}$	$2.77 \times 10^{3}$	$1.93 \times 10^{4}$	$2.03 \times 10^{5}$
50/70 + 50% RAP + 15% Rej	1	$2.72 \times 10^{0}$	$8.62 \times 10^{0}$	$3.29 \times 10^{1}$	$1.59 \times 10^{2}$	$1.05 \times 10^{3}$	$1.03 \times 10^{4}$	$1.21 \times 10^{1}$	$3.31 \times 10^{1}$	$1.05 \times 10^{2}$	$4.00 \times 10^{2}$	$1.94 \times 10^{3}$	$1.27 \times 10^{4}$	$1.25 \times 10^{5}$
50/70 + 75% RAP	1	$3.57 \times 10^{0}$	$1.51 \times 10^{1}$	$7.87 \times 10^{1}$	$5.28 \times 10^{2}$	$4.86 \times 10^{3}$	$6.69 \times 10^4$	$8.05 \times 10^{1}$	$2.88 \times 10^{2}$	$1.22 \times 10^{3}$	$6.34 \times 10^{3}$	$4.25 \times 10^{4}$	$3.91 \times 10^{5}$	$5.39 \times 10^{6}$
50/70 + 75% RAP + 5% Rej	1	$3.17 \times 10^{0}$	$1.18 \times 10^{1}$	$5.32 \times 10^{1}$	$3.04 \times 10^{2}$	$2.35 \times 10^{3}$	$2.66 \times 10^4$	$4.01 \times 10^{1}$	$1.27 \times 10^{2}$	$4.74 \times 10^{2}$	$2.13 \times 10^{3}$	$1.22 \times 10^{4}$	$9.42 \times 10^{4}$	$1.07 \times 10^{6}$
50/70 + 75% RAP + 10% Rej	1	$2.64 \times 10^{0}$	$8.02 \times 10^{0}$	$2.88 \times 10^{1}$	$1.28 \times 10^{2}$	$7.50 \times 10^2$	$6.22 \times 10^3$	$2.13 \times 10^{1}$	$5.63 \times 10^{1}$	$1.71 \times 10^{2}$	$6.15 \times 10^2$	$2.74 \times 10^{3}$	$1.60 \times 10^4$	$1.67 \times 10^{5}$
50/70 + 75% RAP + 15% Rej	1	$2.53 \times 10^{0}$	$7.31 \times 10^{0}$	$2.51 \times 10^{1}$	$1.06 \times 10^{2}$	$5.93 \times 10^{2}$	$4.74 \times 10^{3}$	$1.44 \times 10^{1}$	$3.64 \times 10^{1}$	$1.05 \times 10^{2}$	$3.61 \times 10^{2}$	$1.53 \times 10^{3}$	$8.54 \times 10^{3}$	$6.82 \times 10^4$

Blends	$\eta_0$ - Steady shear viscosity (Pa·s)							
	$T = 25^{\circ}C$	$T = 35^{\circ}C$	$T = 45^{\circ}C$	T = 55°C	$T = 65^{\circ}C$	T = 75°C	T = 85°C	
50/70 + 25% RAP	$6.01 \times 10^5$	$5.06 \times 10^4$	$6.48 \times 10^3$	$1.15 \times 10^{3}$	$2.60 \times 10^2$	$7.23 \times 10^{1}$	$2.36 \times 10^{1}$	
50/70 + 25% RAP + 5% Rej	$3.66 \times 10^5$	$3.26 \times 10^4$	$4.40 \times 10^{3}$	$8.16 \times 10^2$	$1.94 \times 10^{2}$	$5.60 \times 10^{1}$	$1.90 \times 10^{1}$	
50/70 + 25% RAP + 10% Rej	$2.17 \times 10^{5}$	$2.07 \times 10^{4}$	$2.96 \times 10^{3}$	$5.79 \times 10^{2}$	$1.44 \times 10^{2}$	$4.36 \times 10^{1}$	$1.54 \times 10^{1}$	
50/70 + 25% RAP + 15% Rej	$1.48 \times 10^{5}$	$1.48 \times 10^{4}$	$2.21 \times 10^{3}$	$4.49 \times 10^{2}$	$1.16 \times 10^{2}$	$3.61 \times 10^{1}$	$1.31 \times 10^{1}$	
50/70 + 50% RAP	$1.63 \times 10^{6}$	$1.28 \times 10^{5}$	$1.53 \times 10^{4}$	$2.51 \times 10^{3}$	$5.32 \times 10^{2}$	$1.38 \times 10^{2}$	$4.21 \times 10^{1}$	
50/70 + 50% RAP + 5% Rej	$6.02 \times 10^5$	$5.29 \times 10^{4}$	$6.99 \times 10^3$	$1.27 \times 10^{3}$	$2.93 \times 10^{2}$	$8.23 \times 10^{1}$	$2.72 \times 10^{1}$	
50/70 + 50% RAP + 10% Rej	$2.13 \times 10^{5}$	$2.14 \times 10^{4}$	$3.19 \times 10^{3}$	$6.41 \times 10^2$	$1.63 \times 10^{2}$	$4.99 \times 10^{1}$	$1.78 \times 10^{1}$	
50/70 + 50% RAP + 15% Rej	$1.01 \times 10^{5}$	$1.11 \times 10^{4}$	$1.80 \times 10^{3}$	$3.90 \times 10^2$	$1.06 \times 10^{2}$	$3.46 \times 10^{1}$	$1.30 \times 10^{1}$	
50/70 + 75% RAP	$4.45 \times 10^{6}$	$3.27 \times 10^{5}$	$3.62 \times 10^4$	$5.52 \times 10^{3}$	$1.09 \times 10^{3}$	$2.63 \times 10^{2}$	$7.52 \times 10^{1}$	
50/70 + 75% RAP + 5% Rej	$9.80 \times 10^5$	$8.51 \times 10^{4}$	$1.10 \times 10^{4}$	$1.95 \times 10^{3}$	$4.39 \times 10^{2}$	$1.20 \times 10^{2}$	$3.86 \times 10^{1}$	
50/70 + 75% RAP + 10% Rej	$2.10 \times 10^{5}$	$2.22 \times 10^{4}$	$3.42 \times 10^{3}$	$7.06 \times 10^2$	$1.83 \times 10^{2}$	$5.69 \times 10^{1}$	$2.05 \times 10^{1}$	
50/70 + 75% RAP + 15% Rej	$7.07 \times 10^4$	8.15×10 <sup>3</sup>	$1.48 \times 10^{3}$	$3.41 \times 10^{2}$	$9.74 \times 10^{1}$	$3.31 \times 10^{1}$	$1.29 \times 10^{1}$	

Table A.2. Estimated values of steady shear viscosity at different temperatures from the 1<sup>st</sup> approach for all tested binder blends. 1<sup>st</sup> approach

	$\eta_0$ – Steady shear viscosity (Pa·s)							
Blends								
	$T = 25^{\circ}C$	T = 35°C	$T = 45^{\circ}C$	T = 55°C	$T = 65^{\circ}C$	T = 75°C	T = 85°C	
RAP + 5% Rej	$3.37 \times 10^{6}$	$3.03 \times 10^{5}$	$3.84 \times 10^4$	$6.41 \times 10^3$	$1.34 \times 10^{3}$	$3.36 \times 10^2$	$9.85 \times 10^{1}$	
RAP + 10% Rej	$2.45 \times 10^{5}$	$3.11 \times 10^4$	$5.30 \times 10^{3}$	$1.14 \times 10^{3}$	$2.99 \times 10^2$	$9.15 \times 10^{1}$	$3.20 \times 10^{1}$	
RAP + 15% Rej	$2.25 \times 10^4$	$3.90 \times 10^3$	$8.71 \times 10^2$	$2.37 \times 10^{2}$	$7.62 \times 10^{1}$	$2.79 \times 10^{1}$	$1.14 \times 10^{1}$	
50/70 + 25% RAP	$6.01 \times 10^5$	$5.06 \times 10^4$	$6.48 \times 10^3$	$1.15 \times 10^{3}$	$2.60 \times 10^2$	$7.23 \times 10^{1}$	$2.36 \times 10^{1}$	
50/70 + 25% RAP + 5% Rej	$3.67 \times 10^5$	3.31×10 <sup>4</sup>	$4.49 \times 10^{3}$	$8.33 \times 10^{2}$	$1.98 \times 10^{2}$	$5.69 \times 10^{1}$	$1.92 \times 10^{1}$	
50/70 + 25% RAP + 10% Rej	$2.24 \times 10^{5}$	$2.16 \times 10^4$	$3.11 \times 10^{3}$	$6.06 \times 10^2$	$1.50 \times 10^{2}$	$4.48 \times 10^{1}$	$1.56 \times 10^{1}$	
50/70 + 25% RAP + 15% Rej	$1.40 \times 10^5$	$1.43 \times 10^{4}$	$2.18 \times 10^{3}$	$4.46 \times 10^2$	$1.15 \times 10^{2}$	$3.56 \times 10^{1}$	$1.28 \times 10^{1}$	
50/70 + 50% RAP	$1.63 \times 10^{6}$	$1.28 \times 10^{5}$	$1.53 \times 10^{4}$	$2.51 \times 10^{3}$	$5.32 \times 10^{2}$	$1.38 \times 10^{2}$	$4.21 \times 10^{1}$	
50/70 + 50% RAP + 5% Rej	$6.04 \times 10^5$	$5.43 \times 10^4$	$7.26 \times 10^3$	$1.32 \times 10^{3}$	$3.03 \times 10^{2}$	$8.48 \times 10^{1}$	$2.77 \times 10^{1}$	
50/70 + 50% RAP + 10% Rej	$2.29 \times 10^{5}$	$2.35 \times 10^4$	$3.52 \times 10^{3}$	$7.02 \times 10^2$	$1.76 \times 10^{2}$	$5.29 \times 10^{1}$	$1.85 \times 10^{1}$	
50/70 + 50% RAP + 15% Rej	$9.07 \times 10^4$	$1.06 \times 10^4$	$1.76 \times 10^{3}$	$3.84 \times 10^{2}$	$1.04 \times 10^{2}$	$3.37 \times 10^{1}$	$1.25 \times 10^{1}$	
50/70 + 75% RAP	$4.45 \times 10^{6}$	$3.27 \times 10^{5}$	$3.62 \times 10^4$	$5.52 \times 10^{3}$	$1.09 \times 10^{3}$	$2.63 \times 10^{2}$	$7.52 \times 10^{1}$	
50/70 + 75% RAP + 5% Rej	$9.81 \times 10^5$	$8.83 \times 10^4$	$1.16 \times 10^4$	$2.06 \times 10^{3}$	$4.62 \times 10^2$	$1.25 \times 10^{2}$	$3.97 \times 10^{1}$	
50/70 + 75% RAP + 10% Rej	$2.35 \times 10^{5}$	$2.56 \times 10^4$	$3.97 \times 10^{3}$	$8.11 \times 10^{2}$	$2.06 \times 10^2$	$6.21 \times 10^{1}$	$2.17 \times 10^{1}$	
50/70 + 75% RAP + 15% Rej	$5.98 \times 10^4$	$7.84 \times 10^3$	$1.42 \times 10^{3}$	$3.33 \times 10^{2}$	$9.49 \times 10^{1}$	$3.18 \times 10^{1}$	$1.22 \times 10^{1}$	

Table A.3. Estimated values of steady shear viscosity at different temperatures from  $2^{nd}$  approach for all tested binder blends.  $2^{nd}$  approach