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# A novel laser-based method to measure the adsorption energy on carbonaceous surfaces

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## Abstract

The reactivity of carbonaceous surfaces bears a fundamental role in various fields, from atmospheric chemistry and catalysis to graphene and nanoparticles. This reactivity is mainly driven by the surface chemical composition and by the strength of the interaction between the adsorbates and the surface (physi-/chemisorption). While the surface composition of complex natural samples can be well characterized, adsorption energies (ergo, adsorption processes) of the corresponding adsorbate/adsorbent systems are often overlooked. We propose a novel laser-based method for measuring the adsorption energy of chemical species on various carbonaceous surfaces. The proof of concept of this original method has first been demonstrated by deriving adsorption energies of various systems consisting of polycyclic aromatic hydrocarbons and activated carbon. The great potential of this fast, spatially resolved, and surface-sensitive method, which can also act as a defect density probe at the mesoscale, has been further demonstrated through the study of systems of increasing complexity.

*Keywords:* Carbonaceous surfaces, Adsorption energy, Laser-induced thermal desorption, Mass spectrometry, Bayesian statistics

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## 1. Introduction

Carbonaceous materials are used in a wide range of applications including aerospace and defense, automotive, energy, construction, electronics, and sports. Their superior properties including excellent stiffness, high tensile strength, low thermal expansion, and good temperature tolerance [1, 2], make them versatile materials that can be shaped into various forms depending upon the use intended (*e.g.* carbon fibers, carbon nanotubes, graphene). Carbon-based materials can also be turned into metal-free catalysts and serve as a promising alternative to transform sustainable biomass into renewable energy systems [3].

Due to their excellent adsorption capacities, carbonaceous materials are widely employed as filtration media. Carbon nanotubes (CNT) show great

potential at revolutionizing water and gas treatment technologies [4] as they provide much higher surface areas, adsorption capacities, and faster kinetics than activated carbon, the currently prevailing filtration agent. The utility of the adsorptive fixation of organics in the gas and liquid phases for treating wastewaters and emission gasses is already showcased for a number of harmful compounds [5–8]. Another considerable advantage of carbon nanostructures is that their properties can be tailored to target certain chemical species (*e.g.* toxins, heavy metal ions) [4, 9, 10].

For carbonaceous materials, the downside of exhibiting high adsorptive capacities is that they will act as surface carriers. This can lead to adsorbed toxic species undergoing long-range transport in the atmosphere. This effect is commonly observed with combustion generated aerosols (soot), which consist of a carbonaceous matrix often coated with a plethora of organic species [11–13], many of them exhibiting a proven carcinogenic potential [14–16].

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39 This makes the impact of combustion generated  
40 particles on human health considerably greater, es-  
41 pecially since their inhalation can result in health  
42 problems beyond the lungs [17]. In fact, the pres-  
43 ence of combustion derived nanoparticles has been  
44 detected in the frontal cortex of autopsy brain sam-  
45 ples [18], urine of healthy children [19], and even in  
46 the fetal side of the placenta [20]. If transported  
47 to the fetus, these particles – as surface carriers for  
48 potentially toxic species – could significantly affect  
49 fetal health and development [20].

50 In this context, the benefit of identifying the ad-  
51 sorption mechanism on carbonaceous surfaces and  
52 its associated adsorption energy is threefold. It can  
53 provide necessary information to better compre-  
54 hend, and potentially minimize, the health impact  
55 of carbonaceous aerosols. It can help design bet-  
56 ter carbon-based materials for industrial use. And  
57 finally, it can offer some insights into the complex  
58 and still only partially understood soot formation  
59 mechanism since adsorption energies define whether  
60 the surface species (adsorbates) are chemisorbed or  
61 physisorbed, and therefore if the surface molecu-  
62 lar compounds result from surface chemistry (rem-  
63 nants of the soot formation) or physical condensa-  
64 tion [21].

65 Adsorption performances are governed by phys-  
66 ical and chemical parameters that greatly vary  
67 across adsorbate/adsorbent systems. Thus, a sys-  
68 tematic study needs to be undertaken in order to  
69 determine i) to what extent the adsorption energy  
70 depends on the nature and the size of the adsorbate,  
71 and ii) the type of interactions established between  
72 adsorbate and adsorbent. Depending upon the na-  
73 ture of the adsorbate (gas or liquid) and adsorb-  
74 ent (polycrystalline film, single-crystal, oxides, or  
75 nanoparticle surfaces, powders suspended in a liq-  
76 uid or loose powders) [22], various microcalorime-  
77 try techniques, such as single-crystal adsorption  
78 calorimetry (SCAC), isothermal titration calorime-  
79 try (ITC), and differential scanning calorimetry  
80 (DSC) [23, 24], or temperature-programmed des-  
81 orption (TPD) [25, 26] are commonly used to ei-  
82 ther measure directly the heat of adsorption (mi-  
83 crocalorimetry) [27–29], or infer the activation en-  
84 ergy for desorption (TPD). However, for systems  
85 exhibiting meso or macro scale (micrometer- or sub-  
86 millimeter sized) inhomogeneities or field-collected  
87 samples exhibiting small quantities of matter and  
88 complex compositions (*i.e.* with a multitude of  
89 co-adsorbed species), the use of these conventional  
90 techniques becomes at best arduous and at worst

91 impossible.

92 We propose here an original solution to over-  
93 come the restrictions encountered with more con-  
94 ventional techniques when determining adsorption  
95 energies. Our method relies on laser-induced ther-  
96 mal desorption (LITD) coupled with ultra-sensitive  
97 mass spectrometry detection. The principle of the  
98 method relies on the following stages: the carbona-  
99 ceous sample surface is very rapidly heated by a  
100 (visible) nanosecond laser pulse. The heating is lo-  
101 cal (scale of the laser beam diameter) and transient  
102 (initial temperature regained on a microsecond time  
103 scale). A fraction of the molecules adsorbed on  
104 the sample surface is therefore desorbed and subse-  
105 quently ionized by a second (UV) laser pulse before  
106 being mass-selectively detected by a time-of-flight  
107 mass spectrometer. Low desorption and ionization  
108 laser fluences are used to prevent fragmentation of  
109 the analytes or alteration of the adsorbent. The  
110 fraction of molecules desorbed from an irradiated  
111 spot depends on the laser fluence and the number  
112 of pulses it is exposed to. These relationships are  
113 specific to each adsorbate/adsorbent system and in-  
114 dicative of the interaction between the two compo-  
115 nents. The resulting experimental data can then be  
116 mathematically treated to derive the corresponding  
117 adsorption energy.

118 We present in this paper two distinct experimen-  
119 tal approaches, derived from the same LITD prin-  
120 ciple, along with two mathematical models (and  
121 associated statistical procedures) we developed to  
122 retrieve the adsorption energy from the recorded  
123 experimental data. The method is validated on  
124 well-controlled laboratory-synthesized samples, as-  
125 sociating several carbonaceous adsorbents and or-  
126 ganic/inorganic adsorbates at sub-monolayer con-  
127 centration, in a broad range of adsorption energies  
128 (0.2 – 1.5 eV).

## 129 2. Materials and Methods

### 130 2.1. Experimental approaches

131 Two distinct approaches based on the LITD prin-  
132 ciple were followed to collect experimental data for  
133 adsorption energy determination: the “signal de-  
134 cay” and the “fluence curve”.

#### 135 2.1.1. Signal decay

136 The principle of this first experimental approach  
137 is presented in Fig.1a-c: a region of the sample

(delimited by the laser spot on the surface) is irradiated with successive nanosecond laser pulses (10 Hz repetition rate) of constant (low) fluence. For each pulse, a fraction of desorbed molecules is ionized by a second nanosecond laser and further detected by a mass spectrometer. Mass spectra are so recorded for successive laser pulses and the signal corresponding to the adsorbate of interest is plotted as a function of the number of applied laser pulses (Fig. 1c). The pseudo-exponential decay observed simply illustrates a gradual “cleaning” of the irradiated spot by the successive desorption pulses. If this decay is “slow” (*i.e.* a high number of laser pulses is needed to “clean” the surface), then one can infer a strong interaction between the adsorbate and the surface. Conversely, a faster decay (in the same irradiation conditions) will be indicative of looser bonding of the adsorbate to the surface.

### 2.1.2. Fluence curve

The second approach relies on the variation of the desorption yield with the laser fluence, as illustrated in Fig. 1d-e. In this approach, multiple spots on the sample surface are irradiated with only one pulse each, but the pulses exhibit different fluences. Each measurement is performed on different spots of the sample, *i.e.* on a pristine surface that was not previously irradiated, to ensure that the initial concentration is always the same. The different fluences will lead to different temperature increase for each spot and, consequently to different desorption yields. Fitting the fluence variation of the desorption yield with the adequate equation (see below) allows retrieving the adsorption energy.

### 2.2. L2MS set-up

The experimental setup used in this work is based on the L2MS technique [11, 30, 31], which combines three key stages: laser desorption (LD), laser ionization (LI), and time-of-flight mass spectrometry (ToF-MS). The sample is mounted onto a copper holder maintained at constant temperature (170 – 190K in this study) by a regulating device consisting of a heating resistor and a liquid nitrogen closed loop. Initially developed for studies on ice samples [32, 33], this system has proved its efficiency in preventing volatile analyte evaporation at the working pressure ( $\sim 10^{-8}$  mbar) of the mass spectrometer on many combustion-related [11, 30, 34, 35] or PAH-containing [31, 36] samples.

The sample surface (placed vertically, Fig. 2) is irradiated at normal incidence by the 4 ns pulsed

beam of an Nd:YAG laser (Continuum Minilite, second harmonic,  $\lambda = 532$  nm). The desorption laser beam hits the surface with a quasi-top-hat profile of  $\sim 0.7$  mm diameter (measured with a Gentec Beamage-4M beam profiler). The quasi top-hat transverse intensity profile is obtained from the laser output beam by first enlarging it with a beam expander built around a set of convergent and divergent lenses, and then selecting the quasi-flat central region ( $\sim 5\%$ ) of the beam with a diaphragm, which is further image relayed onto the sample surface using a convergent lens.

The desorbed neutral molecules form a forward-peaked plume (*i.e.* narrow angular distribution around the revolution symmetry axis) which propagates at high speed [31, 37] from the sample surface toward the ionization zone. Neutral molecules from the desorbed plume are ionized following a two-photon ionization process [30, 38] using another 4 ns pulsed laser beam (Continuum Powerlite,  $\lambda = 266$  nm, 10 Hz repetition rate,  $\sim 1$  mm diameter, top-hat) propagating orthogonally ( $y$  direction, Fig. 2) to the desorption plume axis. The ionization laser beam intercepts the desorption plume in between the extraction electrodes of an 1 m long, reflectron time-of-flight mass spectrometer (RM Jordan, mass resolution  $m/\Delta m \sim 1000$ ) at  $d \sim 3$  cm from the sample surface. The delay between the desorption and ionization pulses is set to 100  $\mu$ s by a digital delay/pulse generator (SRS DG535).

The ions thus generated are extracted and accelerated ( $x$  direction) toward the free-field flight tube of the mass spectrometer. Mass spectra are recorded with a digital oscilloscope (LeCroy Waverunner 6200A) at a time resolution of 2 ns/point. Data acquisition is controlled by a dedicated routine developed in LabView (National Instruments). Experimental data points considered in this work and amenable to mathematical treatment represent integrated peak areas corresponding to a given analyte, which includes all the peaks associated with its isotopic distribution.

### 2.3. Surface evolution upon irradiation

The desorption fluence is carefully adjusted to be in the low, pre-ablation regime [11, 30], which ensures the desorption of neutral species from the surface of the sample without affecting the underlying carbonaceous matrix. Upon irradiation, the sample surface undergoes temperature variations of large magnitude (1500–2000 K) over a

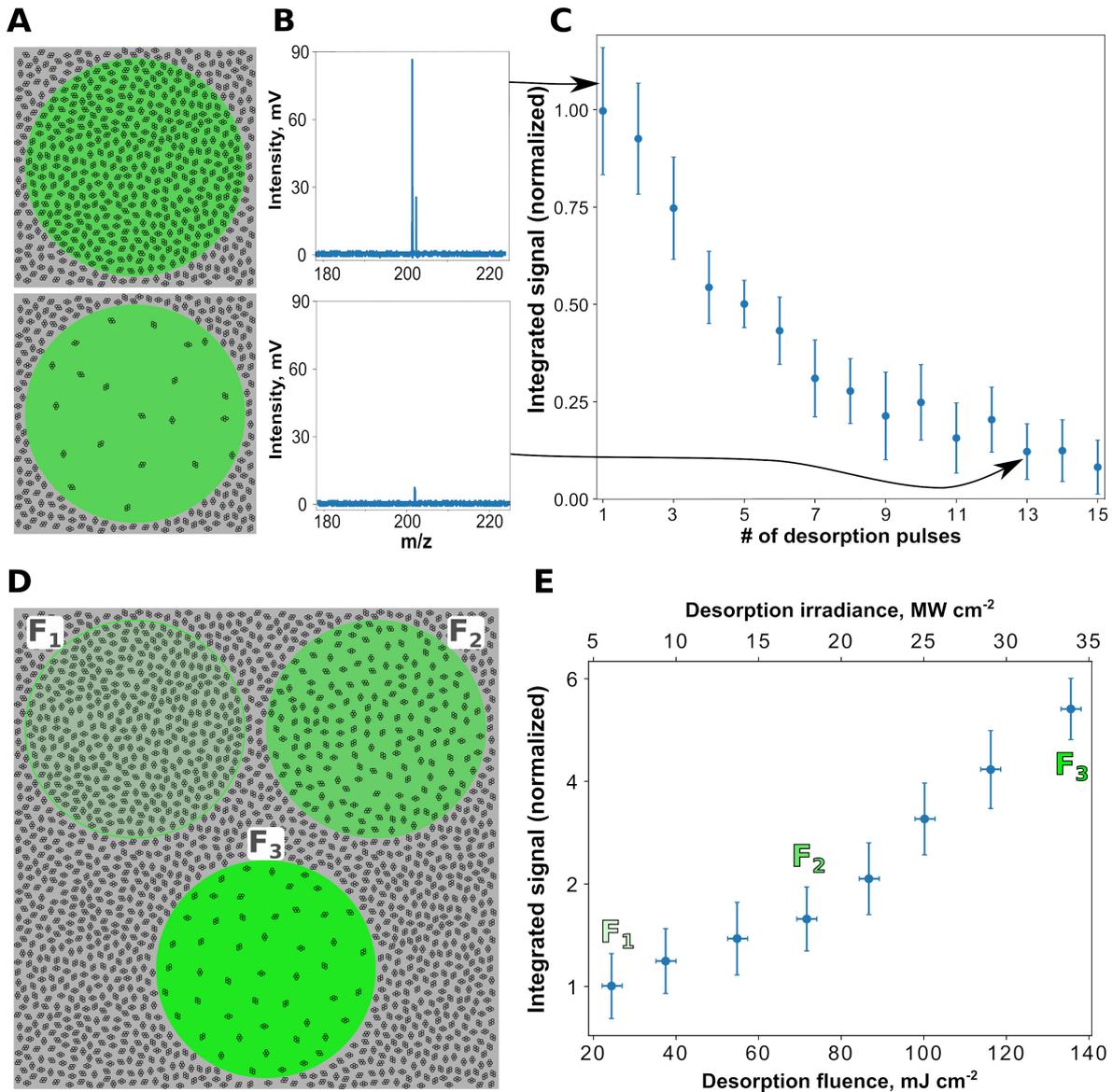


Figure 1: The top and bottom rows describe the “signal decay” and the “fluence curve” experimental approaches, respectively, used to obtain the two distinct datasets from which adsorption energies were subsequently derived. (a) Schematics of the adsorbate coverage evolution upon successive laser pulses of constant fluence applied on the same spot on the sample surface, (b) recorded mass spectra corresponding to two distinct desorption laser pulses (top – 1<sup>st</sup> pulse, bottom – 13<sup>th</sup> pulse), and (c) recorded signal decay. (d) Schematics of the “fluence curve” approach – different spots of the sample irradiated with single laser pulses of various fluences, (e) recorded “fluence curve” signal.

238 very short period of time (the surface typically re- 246  
 239 gains its initial temperature in about 1  $\mu$ s). De- 247  
 240 spite the high temperature reached by the surface 248  
 241 (for only nanoseconds), it was demonstrated that 249  
 242 such a fast-transient process, when generated with 250  
 243 low fluence pulses as performed here, does not ab- 251  
 244 late the adsorbent [11]. Moreover, our fluence op- 252  
 245 timization procedure shows that mass spectra are 253

devoid of any fragments originating from the ad-  
 sorbate throughout the whole fluence regime used  
 in this work. Therefore, our measurements demon-  
 strate that such fluence regime prevents the frag-  
 mentation of the desorbed molecules and precludes  
 ablation of the adsorbent.

In regards to possible adsorbent nanostructure  
 rearrangement upon fast-transient heating, previ-

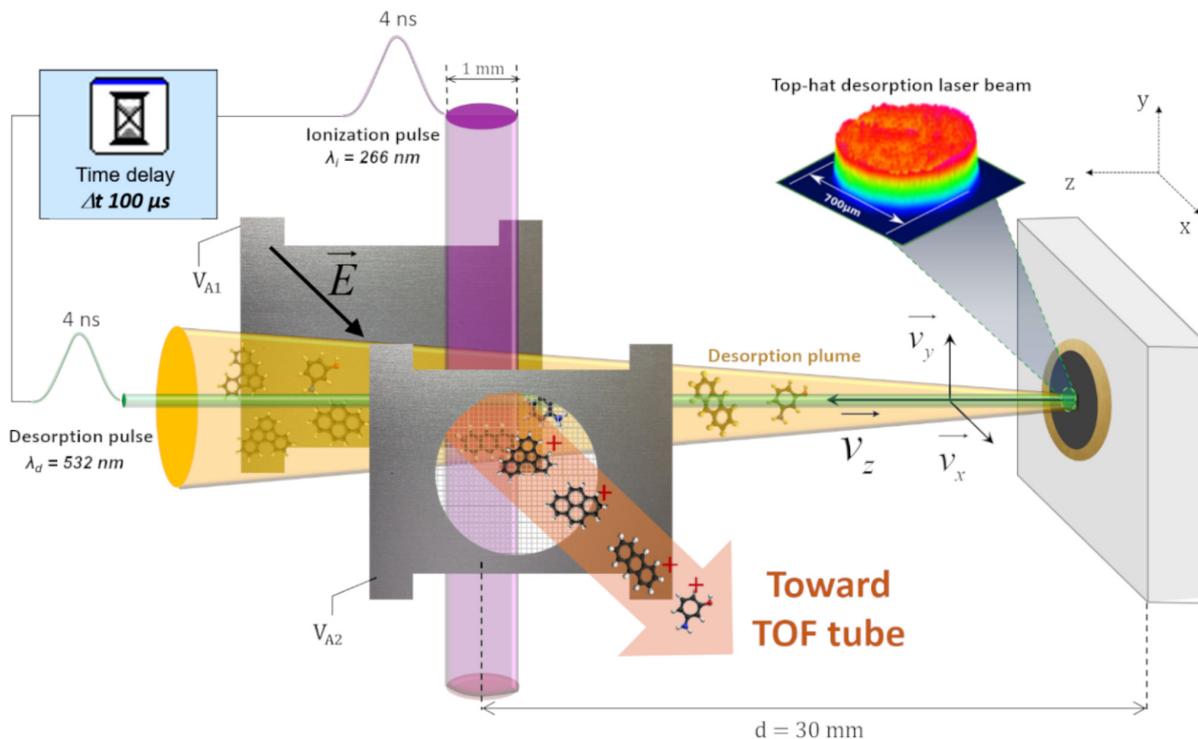


Figure 2: Schematic representation of the laser desorption / laser ionization / ToF-MS experimental arrangement. The desorption laser beam (green) with a top-hat transverse beam profile forms a  $700 \mu\text{m}$  spot on the sample surface. The desorbed neutral molecules form a “plume” (dark yellow) which propagates from the sample surface ( $z$  axis) toward the ionization region situated in between the extraction electrodes of the ToF-MS. A pulsed UV ionization laser beam (purple,  $y$  axis) intersects the desorption plume  $100 \mu\text{s}$  after the desorption beam hits the surface. The obtained ions are then extracted and accelerated ( $x$  axis) toward the field-free flight tube of the ToF-MS.

ous works on amorphous carbon films [39] or black carbon nanoparticles [40] irradiated by nanosecond Nd:YAG laser pulses showed that no significant change in the sample structure was induced in the low fluence regime (typically  $< 50 \text{ mJ cm}^{-2}$ ). In the work of Abrahamson et al. [40], multi-wavelength pyrometry was used to measure transient surface temperatures of more than  $2000^\circ\text{C}$ , while no notable difference in carbon nanostructure was observed by transmission electron microscopy (*i.e.* no rearrangement).

In the first (“signal decay”) experimental approach followed in our work, when a single region of the surface (adsorbent) is irradiated with successive nanosecond laser pulses resulting in the gradual desorption of the adsorbate, it is worth noting that the changing adsorbate surface concentration upon subsequent irradiations does not affect the thermal and optical properties of the system as long as the chemical species are transparent to the desorption

pulse ( $\lambda_d = 532 \text{ nm}$ ) and as the system exhibits a very low surface coverage (both conditions met in this work). As the L2MS technique involves the fast removal of species from the vicinity of the sample [31, 37], re-adsorption of desorbed species is negligible. In addition, any lateral diffusion of molecules across the surface that could potentially replenish the laser spot in between two consecutive desorption laser pulses ( $100 \text{ ms}$ ) can be neglected. For instance, it would take minutes for a pyrene molecule to travel a distance of  $1 \mu\text{m}$  on a carbon surface [41]. Therefore, the physical characteristics of the sample will not change with the increasing number of desorption pulses and thus not influence the desorption process.

#### 2.4. Sample preparation

The development and validation of a method for adsorption energy determination requires well characterized samples. Moreover, the reproducibility of

the method could be assessed only if the characteristics of the sample are held constant. As this work focuses on desorption from carbonaceous surfaces, combustion-generated particles (soot) would have been an appealing candidate as object of study, however, they usually exhibit a very high variability, as their characteristics (*e.g.* specific surface, porosity) depend highly on the combustion conditions. In this context, laboratory-prepared “synthetic soot” [11] represents an interesting alternative as it exhibits a structure akin to that of real soot but has a known and controllable surface chemical composition.

Synthetic soot is prepared here following the protocol described in our previous work [11]. Briefly, polycyclic aromatic hydrocarbons (pyrene and coronene, Sigma Aldrich, 98% purity) are dissolved into dichloromethane (Sigma Aldrich, 99% purity) to make mother (stock) solutions of known concentrations. To these stock solutions are added activated carbon particles (Pureblack 100 Carbon, average particle diameter 80 nm, specific surface area 80–150 m<sup>2</sup>g<sup>-1</sup>) and the resulting mixtures are magnetically stirred for 2 hours. The mixtures are then filtered using a vacuum filtration system employing a quartz fiber filter (Pall Tissuquartz QAT- UP 2500). This filtration step yields, on the one hand, a quartz fiber filter covered by a sub-millimeter thick soot layer infused with the stock solution, and, on the other hand, a filtered solution whose remaining concentration in PAHs can be determined by UV-Vis absorption spectroscopy and subsequent comparison with the stock solution (see Figure S1a). Specifically, as the measured absorbance and the molar concentration are directly proportional in the concentration range studied here, molar concentrations can be estimated knowing the molar extinction coefficient of the solution at a given wavelength and path length. From absorbance measurements of stock solutions of known concentrations can thus be deduced the molar concentrations of the filtered solutions. Therefore, by comparing the absorbance of the stock solution and that of the filtered solution (Figure S1b), it is possible by difference to retrieve the concentration of PAHs remaining on the filter, assuming volatility losses during the preparation steps are negligible [11]. Finally, the surface concentration of PAHs adsorbed on activated carbon particles is calculated knowing the PAH concentration and the specific surface of the particles deposited on the filter.

Three different samples containing either organic

or inorganic species were prepared using the described procedure (Table 1). This included systems containing either a single or two co-adsorbed compounds. Pyrene and coronene were chosen here as adsorbates because of the well-known presence of polycyclic aromatic hydrocarbons (PAH) on the surface of soot particles sampled from real combustors [11, 12]. Additionally, Pb – a heavy metal commonly found in industrial wastewater and usually removed using various carbonaceous materials [9, 10], was used to validate the method for inorganic species. A similar protocol (but a different solvent – ultra-pure deionized water, Purelab Option-Q) was used for the preparation of the lead samples from PbCl<sub>2</sub> salt (Sigma Aldrich, 98%) and Pureblack activated carbon.

Table 1: List of the samples synthesized for adsorption energy measurements. The surface coverage  $\theta$  (in monolayers, ML) was determined from UV-Vis extinction measurements.

Sample	$\theta$ , ML
Pyrene / activated carbon	$2 \cdot 10^{-3}$
(Pyrene + coronene) / activated carbon	$8 \cdot 10^{-3}$ (pyrene) $1.2 \cdot 10^{-2}$ (coronene)
Pyrene / graphite sheet	$\lesssim 10^{-3}$
Pyrene / HOPG	$\lesssim 10^{-3}$
Pb / activated carbon	$\lesssim 10^{-3}$

In order to study the influence of the surface defect density on the retrieved adsorption energy, two more samples based on (mm-thick) graphite sheet and highly oriented pyrolytic graphite (HOPG) adsorbents were prepared in a similar way as the synthetic soot, with the exclusion of the vacuum filtration step. Graphite (Alfa Aesar, graphite sheet) and HOPG (Sigma Aldrich) exhibit significantly lower specific surface areas compared to activated carbon. The resulting adsorbate surface concentration is therefore at the limit of detection of the spectrophotometric method [11]. For this reason, only upper coverage limits ( $\sim 10^{-3}$  ML) are provided in Table 1.

Considering the low coverages and the preparation protocol used in this work, we can assume first that no lateral interaction between adsorbate molecules is present, and second that the coverage is homogeneous across the surface. A low coverage also reduces the possibility of adsorbates forming islands of stacked molecules [42] and thus ensures that the only interaction probed is between adsorbates and the adsorbent surface. Moreover, under these experimental conditions any lateral diffusion

385 of molecules across the surface that could poten- 432  
386 tially replenish the irradiated spot between desorp- 433  
387 tion laser pulses can be neglected [41]. 434

### 388 2.5. Repeatability 435

389 To account for possible experimental fluctuations 436  
390 (mainly due to desorption and ionization lasers), 437  
391 several equivalent measurements are performed in 438  
392 different zones of the same sample. The ana- 439  
393 lyzed regions are chosen not to overlap and there- 440  
394 fore all measurements are considered self-contained. 441  
395 Specifically, for the first experimental approach 442  
396 (signal decay), four signal decays are recorded for 443  
397 the same laser set-point, each decay in a pristine 444  
398 sample zone. For the second experimental approach 445  
399 (*i.e.* fluence curve), four experimental data points 446  
400 per desorption fluence value are acquired on four 447  
401 distinct (pristine) zones of the sample (*e.g.* for 448  
402 pyrene, seven desorption fluence values are utilized 449  
403 which results in 28 experimental datapoints in total). 450  
404 As all measurements are performed in differ- 451  
405 ent spots on the sample, each datapoint is fully 452  
406 independent. Therefore, different combinations of 453  
407 these points can be made to build distinct “fluence 454  
408 curves”. Among all possible combinations, a total 455  
409 of 10 distinct fluence curves are constructed by 456  
410 randomly combining experimental datapoints. 457

## 411 3. Theory 458

### 412 3.1. Background 459

413 When a pulsed laser beam hits a sample surface, 465  
414 a part of its energy (determined by the physical 466  
415 properties of the irradiated material) is passed on 467  
416 to the sample and induces a temperature jump that 468  
417 may i) trigger the desorption of adsorbates possibly 469  
418 present on the surface, ii) alter the surface (nanos- 470  
419 tructure changes), or even iii) ablate micro-volumes 471  
420 of sample. This study is performed in the frame- 472  
421 work of the first effect, known as laser-induced ther- 473  
422 mal desorption (LITD). The pulsed laser-induced 474  
423 heating increases the temperature of surfaces at 475  
424 high rates (up to  $\sim 10^{11}$  K s<sup>-1</sup> with a nanosecond 476  
425 laser [43]), otherwise unattainable with traditional 477  
426 methods (*e.g.* resistive or electron bombardment 478  
427 heating), and is therefore appealing for application 479  
428 to desorption studies. Early studies showed efficient 480  
429 desorption of H, CO, and CO<sub>2</sub> molecules from a 481  
430 variety of surfaces irradiated by pulsed laser beams 482  
431 [44], phenomenon interpreted as a purely thermal 483

effect. This effect was later used to study the ad-  
sorption and desorption kinetics of these species  
by means of relaxation methods [45]. LITD was  
also used to examine the desorption of Na and  
Cs atoms with a sub-monolayer surface concentra-  
tion from Ge (100) substrates [46], of H<sub>2</sub> from Ni  
(100), (110) and (111) [45], of CO from Fe [47] and  
of benzene from Pt (111) surfaces [48]. However,  
none of these studies addressed the determination  
of the adsorption energies from LITD data, as they  
typically used a single high-fluence laser pulse to  
desorb all the adsorbed species from the surface,  
thereby completely “cleaning” the irradiated spot  
of the sample with only one laser pulse. On the  
other hand, when a lower desorption laser fluence  
is used, not all the molecules are desorbed by a  
single laser pulse and multiple, consecutive pulses  
can be applied to the same surface spot [49]. Since  
after each desorption pulse the surface concentra-  
tion of molecules reduces, the amount of desorbed  
compounds decreases after each subsequent laser  
pulse, thus resulting in a pseudo-exponential varia-  
tion of both surface coverage and desorbed amount.  
This variation was first linked to the energetics of  
the adsorbate-adsorbent interaction by Specht and  
Blades [21], who suggested that the decay obtained  
for pyrene desorbing from charcoal corresponds to  
molecules that are weakly bound to the surface,  
while the relatively constant signal that followed  
was associated with molecules having a stronger in-  
teraction with the carbonaceous surface. The ob-  
served decay, however, was not used by the authors  
to derive the strength of the pyrene-surface inter-  
action.

A similar decay was reported by our laboratory  
in a previous work [11] which focused on the cal-  
culation of the detection limit of the two-step laser  
mass spectrometry (L2MS) technique. Although  
the energetics of the analyte-surface bond was not  
studied, we demonstrated at that time that a sin-  
gle form of interaction between the analyte and the  
carbonaceous surface (in this case physisorption)  
can be achieved on surrogate soot samples. A dif-  
ferent approach was proposed by Dreisewerd et al.  
[50] to derive the activation energy of desorption  
from sinapic acid and bovine insulin thick layers  
deposited on stainless steel, based on the evolution  
of the desorbed amount of molecules with the irra-  
diation laser fluence.

The present study builds on this previous works  
and proposes for the first time a complete experi-  
mental, theoretical, and data treatment methodol-

ogy to derive adsorption energies from LITD/L2MS experiments. Moreover, by developing a theoretical model describing LITD, an extra step was taken toward better understanding fast processes occurring at the sample surface.

### 3.2. Desorption of physisorbed species

In the kinetic approach, the desorption is described in terms of the desorption rate – the number of molecules that desorb from a unit of surface per unit of time. Assuming that all adsorbed atoms or molecules occupy identical sites, the desorption rate can be expressed by the Polanyi-Wigner equation [51]:

$$-\frac{d\theta}{dt} = \nu\theta^n \exp\left(-\frac{E_{des}}{k_B T}\right) \quad (1)$$

where  $n$  is the order of the desorption kinetics (usually  $n = 1$  for physisorption),  $E_{des}$  is the activation energy for desorption,  $T$  is the surface temperature, and  $k_B$  the Boltzmann constant. As said above, at the low adsorbate coverages used here ( $10^{-3}$ – $10^{-2}$  monolayers) any interaction between neighbouring adsorbed molecules can be neglected [52], and thus the  $E_{des}$  will be characteristic of the adsorbate-adsorbent interaction only. The first-order pre-exponential factor  $\nu$  (measured in  $\text{s}^{-1}$ ), related with the vibration of the adsorbate-adsorbent bond along the reaction coordinate associated with desorption, is also called attempt frequency and is on the order of the atomic frequency of the crystal lattice ( $\sim 10^{13} \text{ s}^{-1}$ ) [53]. For the atom or molecule to leave the surface it needs to overcome the activation barrier for desorption. Since physisorption is a reversible process, the activation energy of desorption is equal to the adsorption energy:  $E_{ads} = E_{des}$ , and therefore these two terms will be used interchangeably hereafter.

As seen in Eq. (1), the driving force of desorption is the surface temperature. Therefore, to calculate the rate of desorption and subsequently estimate the adsorption energy, one should first determine the temperature variation. A precise calculation of the temperature temporal and spatial variation involves quite a heavy mathematical apparatus. Therefore, some authors [50, 54, 55] have used a simplified LITD description, a steady-state process involving an “effective” temperature that would be reached upon laser irradiation and at which the desorption occurs.

Although a more elaborated, space- and time-resolved model was developed in this study, we also

present here this simplified approach for the sake of comparison with previous works.

### 3.3. “Effective temperature” model

The advantage of this simplified, steady-state approach is that all optical and thermal properties of the sample are expressed by a single factor, thus making it easier to retrieve when fitting experimental data. Moreover, the temperature profile of the sample is not required which significantly reduces the computational time needed by the model. Within this approximation, the number of molecules  $N$  desorbed after a laser pulse can be expressed as [50, 54, 55]:

$$N \approx A \cdot \exp\left(\frac{-E_{ads}}{k_B (T_0 + BF)}\right) \quad (2)$$

where  $A$  is proportional to the surface coverage,  $B$  is a factor that describes the conversion of the deposited energy into the surface temperature increase and is associated (for the low coverage used here) solely with the adsorbant properties,  $T_0$  is the initial temperature,  $F$  the desorption laser fluence at the surface. In this model,  $(T_0 + BF)$  is seen as an “effective” sample temperature which would be reached upon laser irradiation and at which the desorption occurs.

The energy deposited into the sample unit volume is determined by the incident laser fluence, and accounts for the reflectivity  $R$  and the optical absorption coefficient  $\alpha(\lambda_0)$  of the sample at the desorption laser wavelength  $\lambda_0$ . This is expressed through the  $B$  parameter, as follows [50]:

$$B = (1 - R) \frac{\alpha(\lambda_0)}{\rho c} \quad (3)$$

where  $c$  is the specific heat capacity of the sample and  $\rho$  is the sample density. The value of the  $B$  parameter can considerably change depending on the actual sample characteristics; however, a good initial estimation can be obtained with values reported in the literature. Alternatively,  $B$  can be determined by measuring the required physical parameters of the sample prior to the adsorption energy determination. However, this is not always possible in the case of field-collected samples since characterizing micrograms of material can be challenging and adds extra preparation steps that can potentially damage and/or contaminate the sample (often being very expensive to obtain and/or unique). Therefore, the developed model should be

576 able to determine the adsorption energy based on  
 577 only an ‘initial guess’ for the  $B$  parameter. The  $B$   
 578 parameter values calculated for two different adsorbent  
 579 materials used in this work (nano-porous soot  
 580 and graphite), along with the physical constants  
 581 used in their calculation, are presented in Table 2.  
 582 Note that the  $B$  values presented in this table can  
 583 be only seen as estimates, sufficiently close to the  
 584 real values to be used by the fitting algorithm as  
 585 ‘initial guess’.

Table 2:  $B$  parameters calculated from Eq. (3) for activated  
 carbon particles and graphite, along with physical parameters  
 sourced from the literature and used in the calculation.

Parameter	Carbonaceous surface	
	Activated carbon particles	Graphite
R	0.2 <sup>a</sup>	0.1 <sup>b</sup>
$\alpha$ , $10^7 m^{-1}$	1.0951 <sup>c,d</sup>	3.4385 <sup>b</sup>
$\rho$ , $10^3 kg m^{-3}$	0.4 <sup>c</sup>	1.9 <sup>d</sup>
$c$ , $J K^{-1} kg^{-1}$	840 <sup>c</sup>	970 <sup>d,e</sup>
B, $J^{-1} K m^2$	26.0	16.2

<sup>a</sup>Ref. [56], <sup>b</sup>Ref. [57], <sup>c</sup>Ref. [11], <sup>d</sup>Ref. [58], <sup>e</sup>Ref. [59]

586 The surface concentration of adsorbed species de-  
 587 creases after each desorption pulse, changing the  $A$   
 588 factor in Eq. (2). The first laser pulse will give  $N_1$   
 589 desorbed molecules:

$$N_1 = p \cdot s \cdot Q_0 \cdot \exp\left(-\frac{E_{ads}}{k_B(T_0 + BF)}\right) \quad (4)$$

590 where  $Q_0$  is the initial adsorbate surface concentra-  
 591 tion,  $s$  is the surface area of the irradiated spot,  
 592 and  $p$  a proportionality constant. The number of  
 593 molecules left on the irradiated surface spot will  
 594 progressively decrease after each subsequent laser  
 595 pulse.

596 Considering that for the low coverages used here  
 597 the adsorption energy does not change with the sur-  
 598 face concentration (see Section 2.4) and the phys-  
 599 ical properties of the sample surface do not change  
 600 upon irradiation with successive laser pulses (see  
 601 Section 2.3),  $N_j$  molecules will be desorbed on the  
 602  $j^{th}$  desorption pulse:

$$N_j = p \cdot s \cdot Q_0 \left(1 - p \cdot \exp\left(-\frac{E_{ads}}{k_B(T_0 + BF)}\right)\right)^{j-1} \cdot \exp\left(-\frac{E_{ads}}{k_B(T_0 + BF)}\right) \quad (5)$$

The  $S_j$  signal recorded by the detector will there-

fore be:

$$S_j = m \cdot N_j = m \cdot p \cdot s \cdot Q_0 \left(1 - p \cdot \exp\left(-\frac{E_{ads}}{k_B(T_0 + BF)}\right)\right)^{j-1} \cdot \exp\left(-\frac{E_{ads}}{k_B(T_0 + BF)}\right) \quad (6)$$

603 where  $m$  is a proportionality factor accounting for  
 604 the ionization efficiency, transfer function of the  
 605 mass spectrometer, and detector efficiency.

The variation of the recorded signal can also be  
 607 expressed as a function of the desorption fluence  
 608 – a “fluence curve” that can be obtained with the  
 609 second experimental approach (see Section 2.1.2):

$$S(F) = m \cdot p \cdot s \cdot Q_0 \cdot \exp\left(-\frac{E_{ads}}{k_B(T_0 + BF)}\right) \quad (7)$$

The proposed model can be used to derive the ad-  
 sorption energy of a given analyte from experimen-  
 tal data recorded by the mass spectrometer. The  
 adsorption energy of an analyte can be retrieved by  
 fitting experimental data either with Eq. (6) (sig-  
 nal decay induced by successive laser pulses applied  
 on the same surface spot) or Eq. (7) (signal vari-  
 ation with fluence). The fitting algorithm requires  
 an “initial guess” – a starting point relatively close  
 to the actual values. The initial guess for the  $B$   
 parameter was calculated using literature data (Table  
 2). The initial value for the adsorption energy was  
 also sourced from the literature (*e.g.* 0.98 eV for  
 pyrene [60, 61]). We note however that fitting the  
 signal decay and fluence curves with Eq. (6) and  
 (7), respectively, can be challenging as they contain  
 two highly correlated parameters. Since the “ef-  
 fective” temperature reached by the surface upon  
 laser irradiation is significantly higher than its ini-  
 tial temperature (*i.e.*  $BF \gg T_0$ ), the adsorption  
 energy  $E_{ads}$  and the  $B$  parameter are highly corre-  
 lated. Therefore, fitting the proposed model to ex-  
 perimental data requires a specific algorithm which  
 is detailed below in Section 3.5 and Appendices A  
 and B.

### 3.4. Transient temperature model

#### 3.4.1. Pulsed laser surface heating

The effective temperature desorption model is  
 only a crude approximation of the laser-induced  
 thermal desorption and to fully model this pro-  
 cess the fast variation of the sample temperature

641 should be taken into account. A variety of stud-  
642 ies addressed the fast heating of solid samples ex-  
643 posed to lasers, describing the processes occurring  
644 at different wavelengths, laser irradiances, pulse  
645 lengths and on various target materials [11, 49, 62–  
646 66]. The approach commonly followed is to de-  
647 scribe laser–solid interactions at a macroscopic  
648 scale using the heat conduction equation (although  
649 some studies treated this phenomenon at an atom-  
650 istic/molecular level, but on a limited timescale  
651 [54]). For low-fluence nanosecond laser pulses, the  
652 energy passed on to the sample does not lead to  
653 its melting nor its evaporation, therefore no phase  
654 transition terms are needed in the equations [64].  
655 Most of the studies focus on the temperature vari-  
656 ation in the sample volume (*i.e.* along the  $z$  depth  
657 axis) and not radially on the surface. Moreover,  
658 the laser pulse is often considered as a surface heat  
659 source ( $z=0$ ), which does not take into account its  
660 propagation into the sample volume as described by  
661 the Beer-Lambert law [11].

662 To calculate sample temperature variations upon  
663 laser irradiation, the sample was considered as a  
664 medium characterized by continuous specific heat  
665 capacity  $c_p$ , thermal conductivity  $k$  and density  $\rho$ .  
666 Considering a continuum is the approach adopted  
667 in all previous studies and is justified by the di-  
668 mension of the probed zone (0.7 mm laser diame-  
669 ter in our case), which is much larger than possi-  
670 ble nanoscale heterogeneities, even for nanoporous  
671 media as the synthetic soot samples studied here.  
672 Space- and time-resolved temperature profiles were  
673 calculated with the 3D heat conduction equation:

$$\begin{aligned} \rho(T) \cdot c_p(T) \frac{\partial T(x, y, z, t)}{\partial t} = k(T) \left( \frac{\partial^2 T(x, y, z, t)}{\partial x^2} + \right. \\ \left. + \frac{\partial^2 T(x, y, z, t)}{\partial y^2} + \frac{\partial^2 T(x, y, z, t)}{\partial z^2} \right) + q_H(x, y, z, t) \end{aligned} \quad (8)$$

674 where  $T$  is the local sample temperature as a func-  
675 tion of the time  $t$  and position  $(x, y, z)$ . The term  
676  $q_H(x, y, z, t)$  describes the heat source which, in this  
677 case, is the desorption laser pulse. To match the  
678 characteristics of the laser pulse used in the ex-  
679 periments, the heat source is represented as a flat  
680 space profile (equivalent to a top-hat laser profile)  
681 in the calculations. In the temporal domain, the  
682 laser beam is represented as a Gaussian pulse. The  
683 energy of the laser pulse is absorbed by the sample  
684 according to the Beer-Lambert law, therefore:

$$q_H(x, y, z, t) = \alpha I_0 (1 - R) \cdot f(x, y) \cdot g(t) \cdot e^{-\alpha z}$$

$$f(x, y) = \begin{cases} 1, & \sqrt{x^2 + y^2} \leq r_{des} \\ 0, & \text{otherwise} \end{cases} \quad (9)$$

$$g(t) = \frac{1}{\sigma\sqrt{2\pi}} \cdot \exp \left[ -\frac{1}{2} \left( \frac{t - t_0}{\sigma} \right)^2 \right], \quad (10)$$

with  $\sigma = \frac{\tau_{des}}{2\sqrt{2 \ln 2}}$

685 where  $R$  is the sample surface reflectivity,  $\alpha$  is the  
686 adsorption coefficient at the desorption wavelength  
687 (532 nm),  $I_0$  is the pulse peak irradiance. The  
688  $f(x, y)$  and  $g(t)$  functions define the space and  
689 time profiles of the pulsed laser beam of radius  $r_{des}$  (top-  
690 hat) and duration  $\tau_{des}$  (full width at half maximum,  
691 Gaussian). Previous studies conducted by multi-  
692 wavelength pyrometry [40] showed no change in the  
693 structural or optical properties of similar carbona-  
694 ceous surfaces for a laser-induced transient temper-  
695 ature increase of more than 2000°C, which is above  
696 the maximum temperatures reached here. Accord-  
697 ingly, the  $R$  and  $\alpha$  parameters were kept constant in  
698 the calculations. The same approach is sometimes  
699 adopted for simulating the laser-induced incandes-  
700 cence (LII) of soot nanoparticles, where even higher  
701 temperatures (4000 K) are reached [67]. Moreover,  
702 Eqs. (8) and (9) do not include any terms account-  
703 ing for phase transitions or surface alteration (*e.g.*  
704 photo/thermal-bleaching) [68] as these do not occur  
705 at the low desorption fluence values studied here.  
706 The boundary conditions required to solve Eq. (8)  
707 are:

$$\begin{cases} T(x \rightarrow \infty, y \rightarrow \infty, z \rightarrow \infty, t) = T_i \\ T(x, y, z, t = 0) = T_i \end{cases} \quad (11)$$

708 where  $T_i$  is the initial temperature of the sample.

The thermal conductivity of nonporous samples  
(*e.g.* graphite) can be found in the literature [58].  
For porous materials, such as nano-porous soot  
(*nps*), the thermal conductivity  $k_{nps}$  strongly de-  
pends on the porosity as the efficiency of phonon  
propagation is related to the number of contact  
points between the nanoparticles forming the sam-  
ple. In this case, the thermal conductivity  $k_{nps}$  of

the  $nps$  layer can be expressed as [69]:

$$k_{nps}(T) = k_{graph}(T) \left[ (1 - \xi)^{3/2} + \xi^{1/4} \frac{k_{air}(T)}{k_{graph}(T)} \right] \quad (12)$$

where  $k_{graph}$  is the thermal conductivity of bulk graphite [58] and  $k_{air}$  is the conductivity of the air filling the pores. The layer porosity  $\xi$  is given by:

$$\xi = 1 - \frac{\rho_{nps}}{\rho_{graph}} \quad (13)$$

where  $\rho_{nps}$  and  $\rho_{graph}$  are the densities of nano-porous soot and graphite, respectively.

The parameters required to calculate the temperature profile of the studied sample were either taken from the literature [11, 26, 58, 63, 69, 70] or calculated from the values for graphite while accounting for the porosity of the sample (Eqs. (12), (13)). The temperature variations of all parameters required for solving Eq. (8) are presented in Fig. S2 of the Supplementary Material. Physical parameters for the graphite sheet and HOPG samples used in this work are nearly identical which allows us to use the same physical characteristics for these two sets of samples.

Eq. (8) was solved with the COMSOL Multiphysics simulation platform using finite element methods. The temporal and spatial temperature evolutions calculated for nano-porous soot and graphite (Fig. 3) show a fast increase with a maximum value reached at  $t = 5.5$  ns in the center of the irradiated surface, followed by a slower cooling toward the initial sample temperature (on microsecond timescale). The heat-affected sample depth is in the range of  $100 \mu\text{m}$  (Fig. 3b), which is significantly lower than the thickness of the samples used in this study. We note that the obtained depth and temporal profiles follow the same trend as the ones reported by previous similar studies [49, 63, 64], although a direct, quantitative comparison is not possible, as the temperature profiles reported in the literature were computed for different materials and desorption laser characteristics (*e.g.* wavelength, pulse duration, fluence).

### 3.4.2. Time- and space-resolved desorption

Once the temperature profile  $T(x, y, z, t)$  is calculated, a space- and time-resolved desorption mathematical model, including the time-dependence of the desorption rate, the number of molecules desorbed per unit of surface, and the total number of

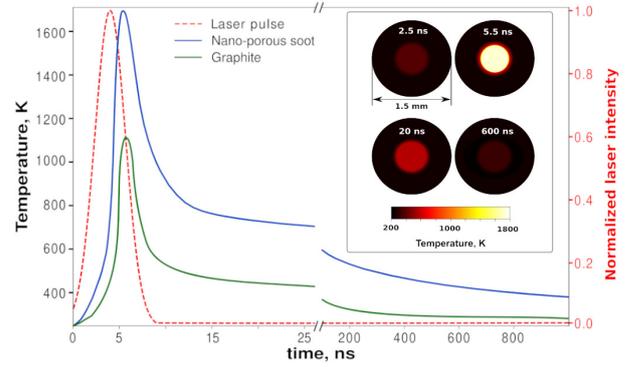


Figure 3: Temporal evolution of the temperature in the center of the irradiated spot ( $T(x = 0, y = 0, z = 0, t)$ ) calculated for nano-porous soot (blue lines) and graphite (green lines) obtained for  $F_{des} = 32 \text{ mJ cm}^{-2}$ . The temporal profile of the desorption laser is plotted for comparison (red dashed line). Snapshots of the radial distribution of the temperature at various delays after the laser pulse are presented in the inset.

molecules desorbed after each desorption pulse can be formulated.

The number of molecules desorbed from the surface after the first laser pulse can be therefore expressed as follows:

$$N_1 = \iint_{-\infty}^{+\infty} Q_0(x, y) \cdot \left( 1 - \exp \left( -\nu \int_0^{\frac{1}{f}} \exp \left( -\frac{E_{ads}}{k_B T(x, y, z = 0, t)} \right) dt \right) \right) dx dy \quad (14)$$

where  $Q_0$  is the initial adsorbate surface concentration and  $f$  is the repetition rate of the desorption laser. The number of molecules desorbed on the  $j^{th}$  desorption pulse can thus be determined with the following relationship:

$$N_j = \iint_{-\infty}^{+\infty} Q_{j-1}(x, y) \cdot \left( 1 - \exp \left( -\nu \int_0^{\frac{1}{f}} \exp \left( -\frac{E_{ads}}{k_B T(x, y, z = 0, t)} \right) dt \right) \right) dx dy \quad (15)$$

$Q_{j-1}(x, y)$  represents the analyte surface concentration after the  $(j - 1)^{th}$  desorption pulse (*i.e.* before the  $j^{th}$  desorption pulse). Since the surface concentration of the analyte decreases after each desorption pulse, the number of desorbing molecules is progressively reduced.

Once a proportionality factor  $m$  is introduced to take into account the overall detection efficiency, the equation can be used for experimental data fitting and adsorption energy retrieval:

$$S_j = m \cdot N_j = m \cdot \iint_{-\infty}^{+\infty} Q_{j-1}(x, y) \cdot \left( 1 - \exp \left( -\nu \cdot \int_0^{\frac{1}{f}} \exp \left( -\frac{E_{ads}}{k_B T(x, y, z=0, t)} \right) dt \right) \right) dx dy \quad (16)$$

where  $S_j$  is the signal recorded by the detector for the  $j^{th}$  desorption pulse. The only unknowns in this equation are the pre-exponential factor  $\nu$ , the adsorption energy  $E_{ads}$ , and the proportionality factor  $m$ . Similarly to the “effective temperature” model, the adsorption energy is determined by fitting the experimental data, in this case with Eq. (16). Compared to the “effective temperature” model, the correlation between the unknown parameters in this equation is much lower which facilitates the fitting procedure. Initial adsorption energy values were sourced from the literature and were the same as in the effective temperature model fits (see above). The initial value for the pre-exponential parameter was taken in accordance with literature recommendations [42, 53, 71] as  $\nu = 10^{12} \text{ s}^{-1}$ .

### 3.5. Data fitting

Fitting the experimental data can be challenging as some of the unknown parameters (*e.g.*  $E_{ads}$  and  $B$  in the “effective temperature” model) are highly correlated. Least-square fitting with functions that contain highly correlated parameters and/or multiple exponential functions can be very unstable, as the outcome of the fit is highly dependent on the initial guess. A *search method* [72] could be used in this case – an algorithm relying on multiple least-square fits of the data performed with different initial values (in user-defined ranges) of the unknown parameters. However, this method is characterized by a rather long convergence time and relatively wide posterior distribution of the retrieved values, and thus was not used here. Instead, we adopted a Markov chains Monte Carlo (MCMC) fitting approach (described in Appendix A) in a Bayesian statistics framework. Starting with initial values for fitted parameters sourced from literature (or calculated based on literature data), several hundred thousands fits are generated to match the experimental data using both the steady-state and transient models. This procedure will return posterior distributions for the fitted parameters. The mode

of these distributions will represent the most probable fit for the given dataset and the confidence intervals will reflect the precision of determination of the unknown parameters from the fit. An illustration is given in Fig.4 for the signal decay of pyrene adsorbed on activated carbon nanoparticles (experimental data averaged over four desorption spots on the same sample,  $2\sigma$  error bars) fitted with the steady-state and the transient temperature models. We notice that both models fit equally well the experimental data, however it is important to emphasize that the red (steady-state model) and green (transient model) dashed lines in Fig. 4a reflect two distinct mathematical concepts. The former results from a severe approximation in that the desorption process occurs at a constant (“effective”) surface temperature, whereas the latter more closely represents the physical reality in that the surface temperature evolves in time and space during the desorption process. The 95% credibility intervals highlighted on the  $E_{ads}$  posterior distributions displayed in Fig. 4b clearly reflect the much lower correlation of the fitted parameters in the transient model with respect to the steady-state one. However, these intervals cannot be used directly to derive “physically-significant” error bars for the adsorption energy, as the developed MCMC fitting algorithm could not converge in a reasonable number of steps (500 000) when large error bars are specified for the experimental data. To derive physically-significant error bars of the fitted parameters, we fitted multiple individual datasets generated from the same sample in the same experimental conditions (see Section 2.5) and further applied an “aggregation of estimators” procedure (see Appendix B) to the fitted parameters values and variances.

## 4. Results

### 4.1. Polycyclic aromatic hydrocarbons on activated carbon nanoparticles

The experimental approaches and the associated mathematical models are first tested using “synthetic soot” samples synthesized in the laboratory (Section 2.4) by (co)adsorbing polycyclic aromatic hydrocarbons on activated carbon nanoparticles at well-controlled, sub-monolayer surface coverages. Pyrene ( $C_{16}H_{10}$ ) and coronene ( $C_{24}H_{12}$ ) were chosen as representative PAHs as they are both known

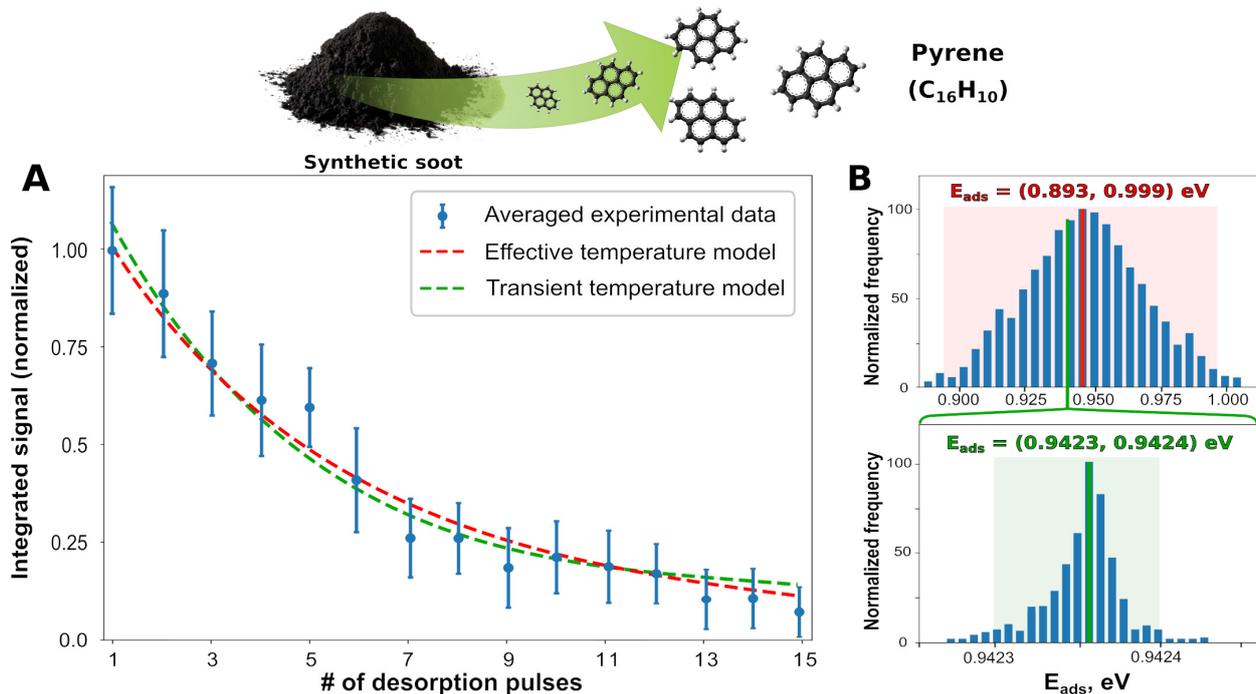


Figure 4: (a) Steady-state (red dashed line) and transient (green dashed line) models fitted to the signal decay curve (four-zone average experimental datapoints) of pyrene desorbing from activated carbon ( $F_{des} = 32 \text{ mJ cm}^{-2}$ ). The plotted fits correspond to the maximum (mode) of the Bayesian posterior distributions shown in (b) – top: steady state, bottom: transient. Shaded areas represent the 95% credibility intervals of  $E_{ads}$ .

853 to be present on combustion generated soot parti- 876  
 854 cles [11–13, 30] and, at the same time, exhibit signifi- 877  
 855 cantly different adsorption energies, which makes 878  
 856 them perfect candidates to test the  $E_{ads}$  recovery 879  
 857 method. Two sets of samples were synthesized, the 880  
 858 first one with a single adsorbed PAH (pyrene), the 881  
 859 second one with both PAHs co-adsorbed on the 882  
 860 same surface. The proposed method allows mea- 883  
 861 suring adsorption energies of co-adsorbed species, 884  
 862 as the signal of multiple mass peaks can be simulta- 885  
 863 neously monitored by time-of-flight mass spectrom- 886  
 864 etry.

#### 865 4.1.1. Pyrene

866 Multiple signal decay and fluence curve datasets 890  
 867 are recorded from the pyrene / activated carbon 891  
 868 surface following the approach described in Sec- 892  
 869 tion 2.5 and the MCMC fitting procedure is ap- 893  
 870 plied to these individual datasets for both steady- 894  
 871 state and transient models. The  $E_{ads}$  initial value 895  
 872 was taken as 0.98 eV from the literature [60] and 896  
 873 this parameter was allowed to vary in the 0.6– 897  
 874 1.2 eV interval for both models. For the steady- 898  
 875 state model, an initial  $B$  value of  $26 \text{ J}^{-1} \text{ K m}^2$  (Ta- 899

ble 2) is used, with an allowed variation interval 15–30  $\text{J}^{-1} \text{ K m}^2$ . In the transient model, a  $10^{12} \text{ s}^{-1}$  initial value is considered for the pre-exponential parameter  $\nu$  in accordance with literature recommendations [53, 71], along with the allowed variation interval  $10^{11}$ – $10^{13} \text{ s}^{-1}$ . Starting with these values, a maximum of 100 000 fits are generated to match the individual datasets with the steady-state and transient models. Both models converge before reaching the maximum number of allowed fits, typically in  $\sim 50\,000$  steps each. The posterior distributions of the  $E_{ads}$ ,  $B$ , and  $\nu$  parameters returned by individual fits are aggregated following the procedure described in Appendix B to calculate the average values and associated error bars ( $1\sigma$ ) listed in Table 3. The obtained data is then used to reconstruct the signal decay and fluence curves, as illustrated in Fig. S3 of the Supplementary Material.

We notice an excellent agreement between the adsorption energies found in both experimental approaches (both signal decay and fluence curve) and by both models. These results are also well in line with the literature value measured for pyrene ad-

900 sorbed on soot particles using thermal desorption 951  
901 kinetics (0.986 eV) [60]. For the “effective temper- 952  
902 ature” model the  $B$  parameters returned by the 953  
903 two approaches ( $B_{decay} = 23.9 \pm 3.4 \text{ J}^{-1} \text{ K m}^2$  and 954  
904  $B_{fluence} = 21.3 \pm 2.1 \text{ J}^{-1} \text{ K m}^2$ ) are in good agree- 955  
905 ment with each other and slightly smaller than 956  
906 the initial estimation ( $26 \text{ J}^{-1} \text{ K m}^2$ ) calculated us- 957  
907 ing literature values. For the transient tempera- 958  
908 ture model, the retrieved pre-exponential factor  $\nu$  959  
909 ( $1.56 \cdot 10^{12} \text{ s}^{-1}$ ) is also close to the initial guess.  
910 Beside validating the analytical method proposed  
911 here, the good agreement with previous works also  
912 confirms that the analyzed samples mimic well soot  
913 samples described in the literature.

#### 914 4.1.2. Pyrene and coronene co-adsorbed

915 Having demonstrated functionality with a single 965  
916 PAH adsorbed onto activated carbon, this adsorp- 966  
917 tion energy calculation method is then put to test 967  
918 using a system consisting of two different polycyclic 968  
919 aromatic compounds co-adsorbed onto the same 969  
920 adsorbant but in such low amount ( $10^{-3} - 10^{-2}$  970  
921 monolayer) that any lateral interactions between 971  
922 them can be neglected. In this configuration, the 972  
923 same laser pulse applied to the surface will lead to 973  
924 the desorption of both molecules, but each with its 974  
925 own kinetics (determined by its adsorption energy 975  
926 value). Signals associated with both molecules are 976  
927 simultaneously recorded by the mass spectrometer 977  
928 to generate individual datasets which are further 978  
929 subjected to the fitting procedure described above, 979  
930 leading to the results displayed in Table 3. 980

931 For the adsorption energy of pyrene, we observe 981  
932 again a very good agreement between the values 982  
933 retrieved by the various experimental / theoretic- 983  
934 al approaches and also with the values determined 984  
935 above, when pyrene was the sole analyte adsorbed 985  
936 onto activated carbon. For coronene, the adsorp- 986  
937 tion energy values determined from various ap- 987  
938 proaches are in excellent agreement with each other 988  
939 and in line with those experimentally determined 989  
940 via temperature programmed desorption measure- 990  
941 ments for coronene adsorbed on carbon nanofibers 991  
942 ( $1.31-1.50 \text{ eV}$ ) [42]. The signal decay and fluence 992  
943 curves of both pyrene and coronene reconstructed 993  
944 from parameters presented in Table 3 overlaid on 994  
945 experimental data are illustrated in Fig. S4 of the 995  
946 Supplementary Material. The  $B$  parameters (char- 996  
947 acteristic of the adsorbent) determined from the 997  
948 two fits of the binary adsorbate / activated carbon 998  
949 sample are in close agreement with each other and 999  
950 also with the ones retrieved for the previous single

adsorbate system (pyrene / activated carbon) shar-  
ing the same adsorbent. Similarly, the  $\nu$  parame-  
ter for pyrene agrees well between the two systems.  
Coronene shows a higher  $\nu$  value (with respect to  
pyrene), as expected from theoretical calculations  
[53, 71]. These results demonstrate the robustness  
of the adsorption energy calculation method from  
LITD experiments and allow us to conceive its ex-  
tension to other adsorbate/adsorbent systems.

#### 960 4.2. Pb on activated carbon nanoparticles

961 Heavy metal ions (*e.g.*  $\text{Pb}^{2+}$ ) are common con- 962  
963 taminants of industrial wastewater and are usu- 964  
965 ally removed using various carbonaceous materials  
966 [9, 10]. Thus, the study of the interaction between  
967 heavy metals, proven to be carcinogenic even at low  
968 concentration, and materials used for their removal  
969 from water (*e.g.* activated carbon) is of great im-  
970 portance. Detection of lead on soot particles (pre-  
971 sumably coming from combustion of leaded gaso-  
972 line) was already shown to be possible with laser-  
973 based mass spectrometry (*e.g.* Particle Analysis  
974 by Laser Mass Spectrometry, PALMS) employing  
975 UV ionization of desorbed species [73, 74].  $\text{PbCl}_2$   
976 salt was dissolved in deionized water and the re-  
977 sulting solution was used to impregnate the acti-  
978 vated carbon nanoparticles. Mass spectra recorded  
979 upon sample irradiation with the 532 nm laser and  
980 ejecta ionization with the 266 nm laser exhibited  
981 the characteristic isotopic distribution of  $\text{Pb}^+$  in the  
982  $m/z$  204–208 range, presented in Fig. S5 of the Sup-  
983plementary Material. No  $\text{Pb}^{2+}$  signal was present  
984 in the mass spectra. Moreover, experiments per-  
985 formed with the ionization laser switched off gave  
986 no signal in the mass spectra, *i.e.* ionized lead is not  
987 directly sampled from the surface. This may seem  
988 surprising, as  $\text{Pb}^{2+}$  ions may be formed in the aque-  
989 ous solution and be further transferred onto the ad-  
990 sorbent surface. Our explanation for this is twofold.  
991 First, the desorption fluence employed (limited by  
992 the carbonaceous surface ablation threshold) might  
993 be too low for desorbing these ions from the sur-  
994 face. Second, the formation of  $\text{Pb}^{2+}$  in the aqueous  
995 solution is only one of many other possibilities, as  
996  $\text{Pb-Cl}$  is not a “pure” ionic bond ( $\Delta\chi_{\text{Pb-Cl}} < 1.7$ ).  
997 Furthermore, in aqueous solution the formation of  
998 an array of (partially) solvated ions is to be ex-  
999 pected. All these ions can then adsorb onto acti-  
vated carbon via different mechanisms (adsorption,  
surface precipitation, ion exchange, sorption, etc.)  
[10, 75–79], and participate to further acid/base,

Table 3: Main parameters derived with the “effective” and transient temperature models. Mean values and error bars are computed using the procedure described in Appendix B. The small number of experimental points for the fluence curve of the pyrene/HOPG system prevented a reliable derivation of the adsorption energy from its fluence curve.

Absorbate	Sample	“Effective temp.” model				Transient temp. model	
		Signal decay		Fluence curve		Signal decay	
		$E_{ads}, \text{eV}$	$B, \text{J}^{-1} \text{K m}^2$	$E_{ads}, \text{eV}$	$B, \text{J}^{-1} \text{K m}^2$	$E_{ads}, \text{eV}$	$\nu, 10^{12} \text{s}^{-1}$
Pyrene	Pyrene / activated carbon	$0.949 \pm 0.049$	$23.9 \pm 3.4$	$0.968 \pm 0.041$	$21.3 \pm 2.1$	$0.965 \pm 0.014$	$1.56 \pm 0.21$
	(Pyrene + coronene) / activated carbon	$0.961 \pm 0.054$	$20.4 \pm 2.8$	$0.983 \pm 0.038$	$22.4 \pm 2.5$	$0.958 \pm 0.018$	$1.31 \pm 0.34$
	Pyrene / graphite sheet	$0.681 \pm 0.019$	$14.1 \pm 1.9$	$0.662 \pm 0.015$	$15.1 \pm 1.4$	$0.696 \pm 0.010$	$1.24 \pm 0.18$
	Pyrene / HOPG	$0.476 \pm 0.021$	$13.5 \pm 1.9$	–	–	$0.508 \pm 0.011$	$1.38 \pm 0.13$
Coronene	(Pyrene + coronene) / activated carbon	$1.519 \pm 0.022$	$22.8 \pm 2.4$	$1.508 \pm 0.024$	$23.1 \pm 1.1$	$1.513 \pm 0.013$	$2.46 \pm 0.15$
Pb	Pb / activated carbon	$0.226 \pm 0.024$	$20.6 \pm 2.3$	$0.206 \pm 0.015$	$21.1 \pm 2.1$	$0.243 \pm 0.011$	$7.46 \pm 0.26$

redox or coordination reactions on the particle surface. A thorough investigation of such a complex surface chemistry is well beyond the scope of the present work.

Both experimental approaches (signal decay and fluence curve) were applied to study the desorption of lead from activated carbon particles. For the signal decay approach, the recorded signal vanishes in fewer desorption pulses compared to aromatic species adsorbed on the same adsorbent (Fig. S6, Supplementary Material). Fitting both models to the experimental data resulted in values for the adsorption energy ( $E_{ads}^{steady} = 0.226 \text{ eV}$  and  $E_{ads}^{transient} = 0.243 \text{ eV}$ , Table 3) close to that found in the literature (0.21 eV for Pb(II) adsorbed on carbon particles obtained from bio waste) [10]. A similar value ( $E_{ads}^{fluence} = 0.206 \text{ eV}$ ) was also determined from the fluence curve (Fig. S6, Table 3). The adsorption energy of lead to carbonaceous surfaces is therefore much lower compared to that of aromatic species [10]. The  $B$  parameter (which is only related to the adsorbent material) is in good agreement (within the limits of the error bars) with the values returned by the steady-state fits on the other samples involving activated carbon (see Table 3). The pre-exponential factor determined from the transient model fit ( $\nu = 7.5 \cdot 10^{12} \text{ s}^{-1}$ ) is in line with theoretical values calculated for small adsorbates [53]. To the best of our knowledge, no  $\nu$  experimental value for this system is reported in the literature.

#### 4.3. Toward the systematic exploration of adsorption energies as a function of adsorbent properties

In order to expand the adsorption energy calculation method to systems of much greater chemical or structural complexity, it is first necessary to explore various adsorbate/adsorbent systems ex-

hibiting significantly different adsorption energies. This can be realized by testing either distinct adsorbates on the same adsorbent or, conversely, the same adsorbate on distinct adsorbents, the latter being studied here. The adsorption energy retrieved corresponds to the average energy of all desorbed molecules. If the irradiated surface contains different types of adsorption sites, each one characterized by a different adsorption energy, then the measured  $E_{ads}$  can be expressed as a weighted average of all possible energy values (*i.e.* energies that correspond to all existing sites). The change in the proportion of adsorption sites of a given type will modify the average and hence the measured (desorption spot averaged) adsorption energy.

Various surface defects can act as adsorption sites (*e.g.* vacancies, impurities) and most of them are present and abundant on the surface of synthetic (and real) soot particles. The adsorption energy of aromatic compounds on adsorbents exhibiting defect-rich surfaces is higher than that expected when the same compounds are adsorbed on a defect-free carbon lattice [80–83]. Accordingly, as the surfaces of materials such as graphite and HOPG contain a much smaller density of defects compared to activated carbon, the adsorption energy of *e.g.* pyrene, on such adsorbents is expected to be substantially lower.

As predicted, the shape of the signal decay curve and the adsorption energy of pyrene desorbed from a graphite sheet and HOPG are noticeably different (Fig. 5). Since the adsorption energy is lower, a smaller number of laser pulses are required to desorb all molecules present on the irradiated spot, hence a shorter signal decay curve is observed. The adsorption energies obtained from the fits performed with the two models (steady-state and transient) are, once again, very similar. Adsorption en-

ergies obtained for pyrene adsorbed on HOPG (Table 3) are in line with values resulting from ab initio calculations (0.42 – 0.5 eV) [80, 81]. To the best of our knowledge, no experimental measurement for either system (pyrene/HOPG or pyrene/graphite sheet) is reported in the literature. When the adsorbent is graphite sheet, the adsorption energy value obtained for pyrene ranges between the ones retrieved for activated carbon and HOPG, which is expected since the surface contains an intermediate number of defects compared to HOPG (fewer defects) and activated carbon (more defects). It is also possible to obtain “fluence curves” for pyrene desorbing from graphite and retrieve the adsorption energy and  $B$  parameter from this approach (Table 3). The values for  $E_{ads}$  and  $B$  (0.681 eV and  $14.1 \text{ J}^{-1} \text{ K m}^2$ , respectively) are also in line with the values obtained from the signal decay. Moreover, the obtained  $B$  values are close to that calculated with literature parameters ( $16.2 \text{ J}^{-1} \text{ K m}^2$ , Table 2).

Across the various adsorbate-adsorbent systems investigated here (Table 3), the values obtained and trends followed for  $B$  and the pre-exponential  $\nu$  parameters are in accordance with what should be expected in regards of their relationship with either the adsorbate or the adsorbent. Specifically, as the  $B$  parameter is associated with adsorbent properties (for low adsorbate coverages as studied here), its retrieved value should be comparable for all systems featuring the same adsorbent. This is indeed what is observed in Table 3, since a similar  $B$  value was obtained with two different experimental approaches for all cases where desorption from the same adsorbent is studied (*e.g.*  $20.4 - 23.9 \text{ J}^{-1} \text{ K m}^2$  for activated carbon, Table 3). In contrast, as the pre-exponential factor  $\nu$  is related to the vibration of the adsorbate-adsorbent bond along the reaction coordinate associated with desorption [53], its value should be largely affected by the adsorbate properties. In accordance, Table 3 shows that the value of this parameter significantly varies for systems based on the same adsorbent but different adsorbates (*e.g.*  $1.56 \cdot 10^{12} \text{ s}^{-1}$  for pyrene adsorbed on activated carbon and  $7.46 \cdot 10^{12} \text{ s}^{-1}$  for lead adsorbed on activated carbon). Such variation with distinct adsorbates was previously reported [42, 53]. Table 3 also confirms that the pre-exponential factor  $\nu$  values obtained for desorption events involving the same adsorbate are similar ( $1.24 - 1.56 \cdot 10^{12} \text{ s}^{-1}$  for pyrene). Finally, beside the consistent evolution of the retrieved  $\nu$  values across the systems studied here, they are also in good agreement with

pre-exponential factors previously reported in the literature.

## 5. Discussion

While it is possible using microcalorimetry to directly appraise the heat of adsorption of a sorbate on various surfaces with a limit of detection (femtomole) akin to ours, performing measurements on such distinct samples (loose powder to highly oriented surfaces) using a single calorimetric technique can be challenging. A direct comparison with microcalorimetry may be impeded by the fact that we do not study adsorption events taking place from a liquid solution nor directly measure the heat of adsorption of a dose of gaseous molecules onto a powder or a surface, but instead monitor the desorption of ‘dry’ adsorbates. Temperature-programmed desorption (TPD) measurements can provide reliable estimates for adsorption energies in experimental conditions close to ours (PAHs already adsorbed on the surface, high vacuum pressure conditions). This technique is thus better suited for comparison purposes. The adsorption energies retrieved using our method are in good agreement with the values reported in the literature from TPD measurements or ab initio calculations. To the best of our knowledge, no adsorption energy values determined via (micro/nano)calorimetry techniques are reported in the literature for the adsorbate/adsorbent systems investigated in this work.

The unique features of the new laser-based method proposed here offer some distinct advantages with respect to the more conventional techniques cited above. First, this method can be applied to systems exhibiting micrometer or sub-millimeter heterogeneities. Specifically, it can be utilized to recover the mean adsorption energy of analytes present in distinct areas of a sample as the lateral resolution is defined by the diameter of the laser spot. The smaller the beam diameter, the better the lateral resolution. Second, our method requires no sample preparation prior to analysis (*e.g.* extraction of material) and necessitates only micrograms of materials to operate. It is hence directly applicable to pristine field-collected and natural samples, for which collecting as much as micrograms of material can be challenging (*e.g.* sampling of aircraft engine [34] or on-road vehicle internal combustion engine emissions [12]). This is particularly important when the focus is on size-selected particles [84, 85] as small as 10 nm, for which the

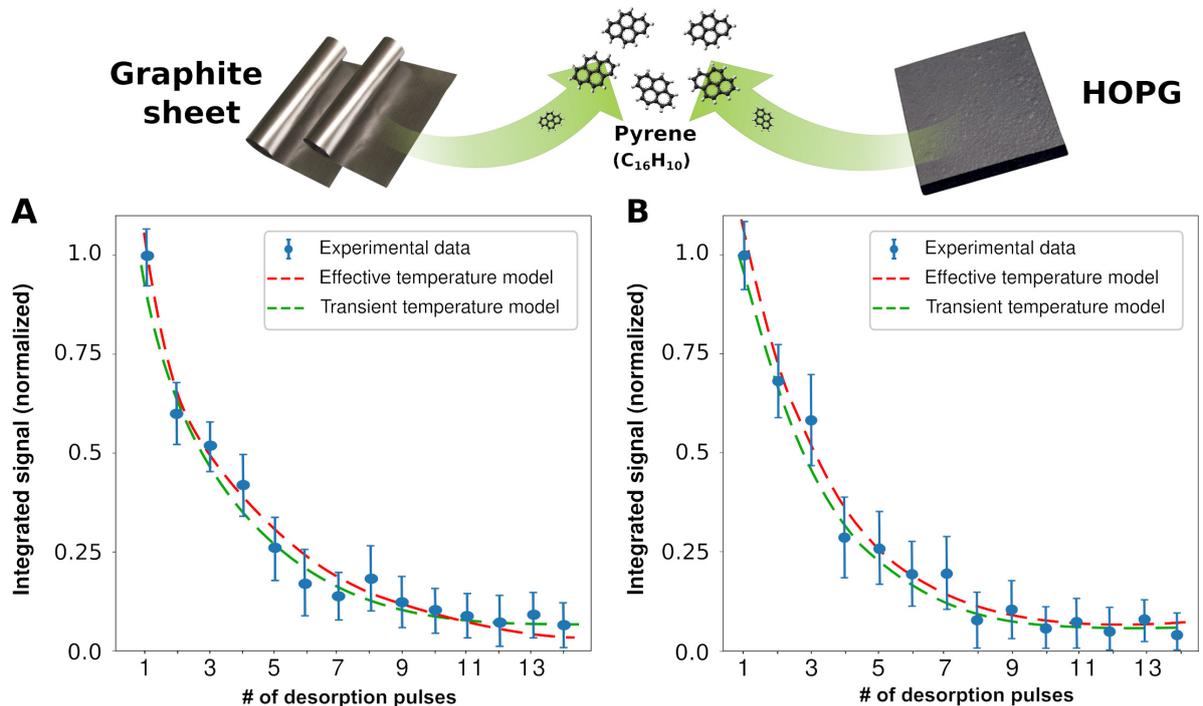


Figure 5: Experimental datapoints (four-zone average) recorded with the “signal decay” approach for pyrene desorbing from (a) graphite sheet ( $F_{des} = 50 \text{ mJ cm}^{-2}$ ) and (b) HOPG ( $F_{des} = 61 \text{ mJ cm}^{-2}$ ). Steady-state (red dashed line) and transient (green dashed line) decay curves calculated with parameters from Table 3.

1178 particle mass lies within the range of attograms. 1202  
 1179 Third, it allows the simultaneous study of one or 1203  
 1180 several analytes coadsorbed on the same surface, 1204  
 1181 which is particularly adapted to real-world complex 1205  
 1182 mixtures. Finally, these particular characteristics, 1206  
 1183 in conjunction with the very low limit of detection 1207  
 1184 (sub-femtomole) that our method provides, consti- 1208  
 1185 tute a valuable solution when more conventional 1209  
 1186 techniques cannot be utilized. 1210

1187 The method we present is sensitive enough to 1211  
 1188 show how the structure of the adsorbent (*e.g.* num- 1212  
 1189 ber of defects) can significantly change the mean 1213  
 1190 adsorption energy. As expected, the adsorption en- 1214  
 1191 ergies derived from our experiments increase with 1215  
 1192 the number of surface defects. This method could 1216  
 1193 act as a surface defect probe and monitor defect 1217  
 1194 densities of various adsorbate/adsorbent systems by 1218  
 1195 following a dedicated and systematic experimen- 1219  
 1196 tal procedure. Different adsorption energies aver- 1220  
 1197 aged over defined zones of a sample surface or 1221  
 1198 between distinct samples can further be related to 1222  
 1199 the disorder/heterogeneity characteristics using, for in- 1223  
 1200 stance, micro-Raman mapping, where deconvoluted 1224  
 1201 Raman maps can be superimposed on adsorption 1225

energy maps of the sample surface probed with the 1202  
 laser. While currently limited to sub-millimeter 1203  
 scale heterogeneities, the lateral resolution could 1204  
 be improved by reducing the diameter of the des- 1205  
 orption laser spot size. The high sensitivity of the 1206  
 technique (ensured by the mass spectrometric de- 1207  
 tection) can be used to finely map spatial variations 1208  
 of physi/chemisorption interactions across hetero- 1209  
 geneous samples, possibly containing small surface 1210  
 inclusions (regions with a distinct composition). 1211

The capabilities of the proposed novel method 1212  
 open perspectives of application in various fields. 1213  
 First, it can serve as a benchmark for adsor- 1214  
 bate/adsorbent systems against which other meth- 1215  
 ods (*e.g.* ab initio calculations) can be compared. 1216  
 On a technological level, it can also encourage the 1217  
 development of advanced materials specially de- 1218  
 signed to selectively target and capture dangerous 1219  
 compounds such as toxins or heavy metal ions [86]. 1220  
 Beyond the obvious interest for catalytic or en- 1221  
 ergy storage materials [87], this method can also 1222  
 be used to characterize thin films grown by phys- 1223  
 ical (pulsed laser deposition, magnetron sputter- 1224  
 ing) [88] or chemical vapor deposition [89] pro-

cesses, which can (depending on the deposition geometry, substrate etc.) exhibit quite large heterogeneities [90, 91] in their adhesion/adsorption properties. The local character of our technique (defined by the laser beam diameter) in conjunction with a fast mathematical treatment (as the simplified effective temperature model) can help in implementing a real-time, spatially-resolved probe directly in the technological process line. Finally, in the combustion field, our method can help shed light on the formation process of soot particles [92, 93] by identifying the origin of the aromatic species present on the surface (i.e. remnants of the nucleation/growth process or condensation from the gas phase).

## 6. Conclusions

Employing laser-induced thermal desorption in conjunction with an adequate mathematical framework, we successfully determine the adsorption energy of distinct adsorbates deposited onto various carbonaceous surfaces. We first formulate and then apply two different mathematical equations modeling the desorption phenomena observed experimentally. The first model describes the desorption process as a steady state phenomenon, using an “effective” sample temperature. This model, while greatly simplifying the calculations, also only constitutes a rough approximation of the desorption process. Advantageous when computational speed is required, it can be used in conjunction with real-time chemical mapping to better characterize the zone of interest. The second model accounts for the fast variation of surface temperature triggered by the absorption of the laser pulse energy. This transient temperature model is more complex but mathematically describes a scenario much closer to physical reality, and also benefits from very little correlation between the variables. Both models fit our experimental data well and provide results close to the values reported in the literature. The adsorption energy is determined for two organic molecules (pyrene and coronene) as well as for an inorganic adsorbate (lead). This approach is also able to retrieve the energy of different compounds co-adsorbed on the same sample (from the same measurements). This serves as a good “proof of concept” for the method, demonstrating that laser-induced desorption combined with our mathematical formulations can be used to study adsorption mechanisms. The novelty and the advantages of

the proposed technique over more traditional approaches in some specific cases along with several new perspectives opened by the developed method were discussed.

Supplementary figures Fig. S1 – S6 can be found in the Supplementary Material at [URL will be inserted by publisher].

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Author contribution: DD, CF, AF, MZ conceptualized the experimental and theoretical method. DD, MV, YC executed the experiments, DD, CPirim, YC, CF discussed the results, DD, CPirim, CF wrote the initial version of the manuscript, DD, CPirim, CF, CPreda developed and validated the mathematical model and the statistical approach. All authors revised and approved the manuscript.

## Appendix A. Markov chains Monte Carlo data fitting

Fitting experimental data with models involving highly correlated parameters requires the use of Bayesian statistics [94–96], which provide powerful tools for estimating complex models where the maximum likelihood-based estimation methods fail. In this framework, several approaches can be followed. Initial tries with the “conventional” *search method* [72] resulted in rather long convergence times and wide posterior distributions of the retrieved parameters (*e.g.*  $E_{ads}$ ,  $B$ ). In this context, we adopted a Markov chains Monte Carlo (MCMC) approach which converges at a much faster pace.

The MCMC method is designed to estimate the joint posterior distribution of a parameter of interest by random sampling in the probability

1321 space. Many problems described by models containing a large number of free parameters, making them expensive to compute with regular methods (e.g. problems in cosmology and astrophysics that deal with low signal-to-noise measurements [94–96]), have benefited from MCMC. One of the most important benefits of Bayesian data analysis is the ability to minimize the impact of nuisance parameters [96] – parameters that are required to model the studied process but otherwise are not the main objective of the fit. Most uses of the MCMC are based on the Metropolis-Hastings (M-H) method [94–96] or its derivatives and consist of three main parts:

- 1335 • Monte Carlo simulations generating random steps to model complex systems.
- 1336
- 1337 • Markov chains - sequences of events that are probabilistically related to one another. Each event originates from a set of outcomes and each outcome determines the next one, in accordance with a fixed set of probabilities.
- 1338
- 1339
- 1340
- 1341
- 1342 • The acceptance-rejection sampling – an iterative algorithm that generates parameter values from their unknown theoretical posterior distribution.
- 1343
- 1344
- 1345

1346 MCMC allows to generate a data subset covering many possible outcomes of a given system in order to obtain an estimate of the theoretical posterior distribution that can be used to extract statistical measures as mean, median or standard deviation. The simulation process is based on a Markov behavior of the iterative algorithm [95, 96]. An example of a model that can benefit from the use of the MCMC algorithm is the laser-induced thermal desorption, e.g. Eq. 6 of the “effective temperature” model that contains a product of two exponential functions and two highly correlated parameters ( $E_{ads}$  and  $B$ ). The performance of the M-H sampler can be very sensitive to the initial choice of parameters. The result of the MCMC fit will be more reliable for longer chains. For this reason, the first values of the Markov chain are usually dropped. Thus, to determine optimal parameters in a data-driven way, a lengthy “burn-in” period must be used. The burn-in allows to start the MCMC procedure with parameters chosen for convenience that might be located in low probability regions, Fig. A.1a. Once the chain has entered the high-probability region, its states become more representative of the correct distribution (the convergence is achieved). All

the values after the convergence are then used to retrieve the distributions and mode values of all parameters, Fig. A.1b.

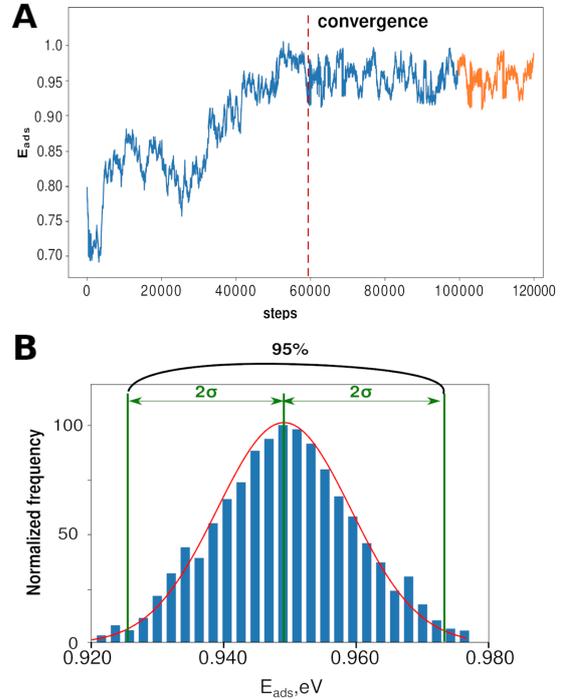


Figure A.1: (a) Example of a Markov chain obtained during fitting of experimental data. The convergence of the fit is depicted with a red dashed line. The last portion of the chain (orange line) is used to determine the posterior distribution of the fitted parameter (b). The distribution is then used to identify the most probable value and the variance of the determined parameter.

## Appendix B. Average value and error bar calculation by estimator aggregation

Individual fits performed on multiple independent datasets generated as described in Section 2.5 return estimated values and associated variances for all parameters of interest through the posterior distributions. As an example, Fig. B.1 illustrates the individual fits of four signal decays recorded in the same experimental conditions (the solid lines represent the “most probable fit” (mode) of the Bayesian posterior distribution for each dataset). In order to account for the measurement variability and determine “physically-significant” average values and error bars associated with the fitted parameters (called “estimators” henceforth), the “inter-

1390 nal” (*i.e.* inside one individual dataset) and “exter- 1410  
 1391 nal” (*i.e.* between different datasets, such as A, B, 1411  
 1392 C, D zones in the signal decay approach, Fig. B.1) 1412  
 1393 variances must be combined in an “estimator ag- 1413  
 1394 gregation” methodology [97, 98]. 1414

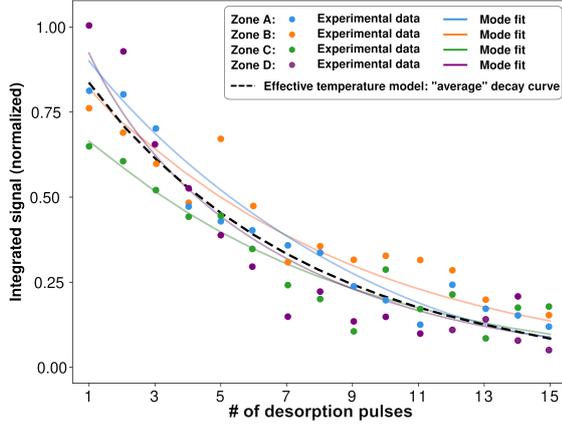


Figure B.1: Symbols: pyrene molecule signal recorded in the same experimental conditions ( $F_{des} = 32 \text{ mJ cm}^{-2}$ ) from four different zones (A, B, C, D) of the same pyrene / activated carbon sample (homogeneous coverage). Solid lines: most probable (mode) fits returned by the Bayesian posterior distribution for each individual dataset. Dashed line: effective temperature model decay curve generated with average parameter values (Table 3).

1395 For a given parameter  $\hat{\beta}$ , let  $\hat{\beta}_i$  be the estima- 1438  
 1396 tors obtained from data collected in the zone  $i$ , 1439  
 1397  $i \in A, B, C, D$ . Then, the best linear-combination 1440  
 1398 estimator for the  $\hat{\beta}$  parameter with respect to the 1441  
 1399 mean squared error will be: 1442

$$\hat{\beta} = \sum_{i=1}^n \omega_i \hat{\beta}_i \quad (\text{B.1})$$

1400 where  $\omega_i = \frac{\text{Var}^{-1}(\hat{\beta}_i)}{\sum_j \text{Var}^{-1}(\hat{\beta}_j)}$  is the weight associated 1450  
 1401 with each estimator, retrieved from fitting individ- 1451  
 1402 ual datasets (either signal decays or fluence curves). 1452  
 1403 Considering the independence of data recorded in 1453  
 1404 different zones of the sample, the standard devia- 1454  
 1405 tion of the  $\hat{\beta}$  parameter is given by: 1455

$$\sigma(\hat{\beta}) = \sqrt{\text{Var}(\hat{\beta})} = \sqrt{\sum_i \omega_i^2 (\text{Var}(\hat{\beta}_i) + (\hat{\beta}_i - \hat{\beta})^2)} \quad (\text{B.2})$$

1406 The first term in Eq. (B.2) represents the “inter- 1464  
 1407 nal” variance of each dataset, while the second term 1465  
 1408 represents the “external” variance (*i.e.* between 1466  
 1409 datasets). 1467

The average values and error bars were calculated for the parameters of interest with the described method and reported in Table 3 in the form  $\hat{\beta} \pm \sigma(\hat{\beta})$ . The validity of the method can be verified with the “average” fitting curve (*i.e.* average for all datasets) calculated with the average values for the required parameters. An example of such a curve obtained with the “effective temperature” model is presented in Fig. B.1 (dashed line).

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