

# Methylparaben chlorination in the presence of bromide ions and ammonia: kinetic study and modeling

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3	METHYLPARABEN CHLORINATION IN THE PRESENCE OF
4	<b>BROMIDE IONS AND AMMONIA: KINETIC STUDY AND</b>
5	MODELING
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#### 1 Abstract

The impacts of chlorination on methylparaben (MP) removal, as well as of bromide and ammonia 2 3 on the MP elimination kinetics were studied. Bromide and ammonia react with chlorine and are promptly transformed into bromine and chloramines, respectively. Rate constants of chlorine, 4 5 bromine and monochloramine with MP were determined under different pH conditions. At pH 8.5, the apparent second-order rate constants of MP reactions with chlorine and bromine were found to 6 be  $3.37(\pm 0.50) \times 10^1$  and  $2.37(\pm 0.11) \times 10^6$  M<sup>-1</sup>.s<sup>-1</sup> for k<sub>Chlorine/MP</sub> and k<sub>Bromine/MP</sub>, respectively, yet 7 there was low reactivity with monochloramine ( $k_{NH_2CI/MP} = 0.045 \text{ M}^{-1}.\text{s}^{-1}$ ). Regarding chlorination 8 9 and bromination, in order to gain further insight into the observed pH-dependence of the reaction, 10 the elementary reactions were considered and the corresponding second-order rate constants were 11 calculated. The experimental and modeled values were quite consistent under these conditions. Then chlorination experiments with different bromide and/or ammonia concentrations were 12 13 performed to assess the impact of inorganic water content on MP elimination and a kinetic model 14 was designed to assess MP degradation. Under these conditions, MP degradation was found to be 15 enhanced in the presence of bromide whereas it was inhibited in the presence of ammonia, and the 16 overall impact was pH dependent.

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## 18 Keywords: Methylparaben, chlorine, bromide, ammonia, modeling

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Abbreviations: pHBA, *p*-hydroxybenzoic acid; PCP, Personal care products; MP, Methylparaben;
PP, Propylparaben; WWTP, Wastewater treatment plant; THM, Trihalomethanes; EE2, 17αethynilestradiol; DOC, Dissolved organic carbon; HPLC, High performance liquid chromatography;
LOD, Limit of detection; LSODA, Livermore solver for ordinary differential equations; DPD, N,N
diethyl-p-phenylenediamine

#### 1 **1. Introduction**

Parabens are *p*-hydroxybenzoic acid (pHBA) esters with alkyl substituents belonging to methyl, butyl or benzyl groups (Jonkers et al. 2010). They were first introduced as antimicrobial preservatives in drug products in mid-1920s (Liebert 1984), while currently serving the same purpose in cosmetics, toiletries, pharmaceuticals and foods (Daughton and Ternes 1999). By 1987, over 7000 kg/year of parabens were used as additives in cosmetics and toiletries alone (Soni et al. 2005). That volume has increased over the last 20 years and parabens are nowadays found in approximately 80% of personal care products (PCP) (Brausch and Rand 2011; Pouillot et al. 2006).

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10 In the late 1990s, several studies confirmed the endocrine disrupting features of parabens as well as 11 their links with diseases such as breast cancer particularly when found in cosmetics and PCP (Darbe et al. 2004; Oishi 2001; Routledge et al. 1998). Studies on prenatal exposure of pregnant women to 12 13 parabens and potential impacts on anthropometric birth outcomes are ongoing (Jamal et al. 2019). 14 Moreover, recent research highlighted the occurrence of these molecules in human body fluids and 15 even breast milk, with methylparaben concentrations reaching 0.11-700 ng/mL (Dualde et al. 2019). 16 Despite their controversial effects, and the emergence of paraben-free products, parabens 17 (particularly methyl- (MP) and propylparaben (PP)) are still the most commonly used preservatives 18 in PCP. Recent concern has been focused on the risks involved in human exposure to parabens. The 19 industry estimated that adult and child exposure to parabens through the daily use of cosmetic 20 products that may contain this compound could amount to 17.76 g and 0.378 g, respectively (CIR 21 2008). In comparison to PCP parabens exposure, the daily intake of parabens from food was 22 estimated to be low, i.e. about 1 µg/kg body weight/day (mean) and 3 µg/kg body weight/day (95th percentile) (Liao et al. 2013). Finally, in addition to direct contact, humans may be exposed to 23 24 parabens in aquatic environments but also in swimming pools where parabens and their chlorinated 25 transformation products have been detected (Terasaki and Makino 2008).

1 Widespread production and use of parabens has led to their dissemination into the aquatic 2 environment through direct input in lakes, rivers or seawater when rubbed off bathers' skin during 3 recreational activities, or indirectly via effluents released from wastewater treatment plants (WWTP). Parabens have actually also been detected in WWTP at concentrations ranging from 13 4 5  $\mu$ g/L in influents to 0.085  $\mu$ g/L in effluents (Benjits et al. 2004; Canosa et al. 2006; Lee and Peart. 6 2005). In surface waters, the occurrence of parabens and their concentrations were found to be 7 highly season dependent, with maximum concentrations correlated with low flow conditions 8 (Loraine and Pettigrove 2006; Peng et al. 2008). Concentrations around 400 ng/L and 69 ng/L were 9 reported for methylparaben and propylparaben, respectively, in European rivers, whereas higher 10 methyl, ethyl, propyl and n-butylparaben concentrations of up to several µg/L were detected in 11 Chinese and Brazilian rivers (Peng et al. 2008; Kasprzyk-Hordern and Dinsdale, 2008; González-12 Mariño et al. 2009; Galinaro et al. 2015). Finally, reports concerning drinking water have been 13 contradictory, with some authors confirming their presence in tap water at 17 ( $\pm$  4) ng/L 14 concentration, while others have denied this issue (Loraine and Pettigrove, 2006; Casas Ferreira and 15 Möder 2011). A recent study evaluating the amount of parabens in mineral and treated water 16 samples indicated methylparaben levels below 0.242 µg/L, with 10 ng/g detected in drinking water 17 treatment sludge (Marta-Sanchez et al. 2018).

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19 Chlorination is used in drinking water treatment and swimming pool disinfection. Studies on 20 parabens chlorination would now be warranted since traces of parabens have been detected in 21 swimming pool water and in surface waters that serve as water resources for drinking water 22 production. Several studies have already shown that halogenated by-products can be generated 23 during the chlorination of parabens, some of which have been found in wastewaters, rivers and 24 swimming pools (Canosa et al. 2006; Terasaki and Makino 2008; González-Mariño et al. 2011; Terasaki et al. 2012). Similarly, some kinetic parameters associated with the parabens chlorination 25 26 have been described (Canosa et al. 2006; Terasaki et al. 2012; Mao et al. 2016; Yoom et al. 2018).

1 Yet, in most studies only direct reactions of chlorine with parabens have been assessed while 2 overlooking the impact of constituents of the water matrix. Natural waters actually contain 3 dissolved organic matter along with various ions (bromide, ammonia, etc.) that could be involved in chlorine consumption during disinfection steps. Bromide ions (Br-) have been detected in fresh 4 5 water environments at concentrations ranging from ~ 10 to > 1000  $\mu$ g/L (Heeb et al. 2014). Moreover, ammonia is found in waters with concentrations around 0.3 mg/L. Bromine and 6 7 haloamines (particularly monochloramine (NH<sub>2</sub>Cl)) can be formed as a result of Br<sup>-</sup> and ammonia 8 reactions with chlorine during chlorination steps in water treatment plants. Monochloramine is less 9 reactive than chlorine with organic compounds, whereas bromine is a highly reactive oxidant that 10 could contribute to organic compound degradation. According to published findings, the THM 11 formation rate and yield could actually be significantly increased during chlorination in the 12 presence of Br<sup>-</sup> (Symons et al. 1993).

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14 The impact of chlorination on the elimination of one of the most common paraben PCP additives (methylparaben (MP)) during disinfection steps was assessed in this study. This compound is found 15 16 in 48% of cosmetics and PCP (Masten 2005). Here we focused on the impact of Br<sup>-</sup> and ammonia 17 on MP removal during chlorination. Chlorination, bromination and chloramination of 18 methylparaben were studied at different pH levels. MP chlorination experiments were also 19 conducted in the presence of various Br and ammonia concentrations and for different pH levels. 20 Under these conditions, a kinetic model was designed and a comparison between the simulation 21 data and our experimental findings was performed. The impacts of Br<sup>-</sup> and ammonia on MP 22 removal during chlorination steps were discussed with respect to MP, chlorine, Br<sup>-</sup> and ammonia 23 concentrations commonly found during the drinking water production process.

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#### 1 **2. Material and methods**

#### 2 2.1. Chemical reagent

3 Methylparaben (MP) (98% purity) and 17 $\alpha$ -ethynilestradiol (EE2) (98% purity) were from Sigma 4 Aldrich and phenol was from ProLabo. Commercial sodium hypochlorite solution (13%) was 5 obtained from Acros Organics. Analytical grade phosphate buffers, sodium thiosulfate, and 6 colorimetric agents were from Sigma Aldrich or Acros Organics.

7

8 Pure water from a MilliQ water purification system was used to prepare all stock solutions (18.2 9  $M\Omega$ .cm and DOC < 0.1 mg/L). Bromine stock solutions were obtained by adding 0.55 mM of 10 potassium bromide (KBr) to a 0.5 mM ozone solution at pH 4 (10 mM phosphate) and at a 11 temperature of 5°C. NaOH was then used to adjust the storage solution pH to 11. Free chlorine was 12 slowly added to an ammonium chloride solution (NH<sub>4</sub>Cl) (2 mol/mol nitrogen-to-chlorine ratio) in a 13 well-stirred reactor at pH= 8.5 to prepare the daily monochloramine stock solutions.

14

#### 15 2.2. Kinetic experiments

16 Duplicate kinetic experiments were performed at room temperature  $(20 \pm 2^{\circ}C)$  in aqueous solutions 17 in the presence of phosphate salts (ionic strength 2 x  $10^{-3}$  M), in the pH 6 to 11 range (pH variation 18 < 0.1 under these conditions).

19

20 Chlorination kinetic experiments were conducted in the presence of excess free chlorine 21 ([Chlorine]<sub>T,0</sub> > 10 [MP]<sub>T,0</sub>) under pseudo-first-order conditions using HPLC-UV to measure the 22 decrease in MP concentration. Chlorine concentration variations were found to be less than 5% 23 throughout the reaction time under these conditions. Batch reactors (1 L) were used in these 24 experiments. Chlorine stock solution ([Chlorine]<sub>T,0</sub> > 15  $\mu$ M) was added to the solution containing 25 MP (1  $\mu$ M) to start the kinetic runs. Then, 1.5 mL of solution was sampled at different time 26 intervals (0 to 60 min), and placed in vials containing 20  $\mu$ L of sodium thiosulfate (100 g/L). 1 Residual chlorine was quenched and the reaction stopped under these conditions. The first-order 2 kinetics relative to chlorine were confirmed by varying the chlorine concentration under different 3 pH conditions. The monochloramine reactivity with MP was assessed using the same kinetic 4 method. The experiments were conducted in batch reactors (1 L) containing monochloramine stock 5 solutions (2 mM) and the kinetic runs were started by adding MP stock solution ([MP]<sub>T,0</sub> = 1  $\mu$ M). 6 At different time intervals (0 to 300 min), samples were withdrawn and placed in vials containing 7 20  $\mu$ L of sodium thiosulfate (100 g/L) to quench residual monochloramine.

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9 Bromination experiments were also performed to determine the rate constants of bromine with MP 10 in the light of the fact that chlorine reacts with Br<sup>-</sup> to yield bromine (Kumar and Margerum 1987). 11 For these experiments, the competitive kinetic method was used since bromine is much more reactive than chlorine with organic compounds. This competitive method was conducted using two 12 13 reference compounds based on their similar reactivity with bromine, i.e. phenol and  $17\alpha$ -14 ethynilestradiol (EE2). Different bromine doses (0 to 4.5 µM) were added in 50 mL batch reactors 15 containing equimolar quantities of MP and reference compound (1 µM) in our experiments. HPLC-16 UV was used to analyse the remaining MP and competitor (phenol or EE2) concentrations after 24 17 h to confirm complete bromine consumption. The k<sub>Oxidant/MP</sub> rate constants were calculated based on 18 previously reported k<sub>Oxidant/C</sub> (k<sub>Oxidant/EE2</sub> or k<sub>Oxidant/phenol</sub>) values (Gallard et al. 2003; Lee and von 19 Gunten 2009).

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# 22 2.3. Chlorination experiments and kinetic modeling in the presence of Br and/or ammonia

All chlorination experiments conducted in the presence of Br<sup>-</sup> and/or ammonia were carried out in batch reactors (1 L) buffered with phosphate salts to pH 7 and 8.5 at initial chlorine and MP concentrations of 10  $\mu$ M and 2  $\mu$ M, respectively. Concentrations ranging from 0 to 10  $\mu$ M were used for Br<sup>-</sup> and ammonia. For the kinetic modeling, all possible reactions in the presence of chlorine and Br<sup>-</sup> and/or ammonia
at pH 7 and 8.5 were considered and the LSODA deterministic simulation method was used in the
Copasi software environment (Hoops et al. 2006). The model simulations were subsequently
compared to the experimental results obtained at pH 7 and 8.5.

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# 7 2.4. Analytical methods

8 Chlorine in commercial and stock solutions was quantified by iodometry (Rodier et al. 2009). 9 Concentration in the bromine stock solution was determined by measuring absorbance at 329 nm ( $\epsilon$ 10 = 332 M<sup>-1</sup>cm<sup>-1</sup>) with a VARIAN Cary 50 UV/VIS spectrophotometer (Troy and Margerum, 1991). 11 During the chlorination experiments, the DPD colorimetric method (Rodier et al. 2009) was 12 followed for chlorine concentration determination and an SAFAS spectrophotometer was used to 13 measure the absorbance at 510 nm ( $\epsilon$  = 14550 M<sup>-1</sup>cm<sup>-1</sup>; LOD = 0.5 µM). pH measurements were 14 obtained using a MeterLab pH-meter fitted with a Radiometer Analytical combination pH electrode. 15

16 MP, phenol and EE2 were analyzed with an Alliance Waters 2695 HPLC system (pump and 17 autosampler) combined with a UV Visible Waters 2487 detector and by using a C18 Kromasil 18 column (250 mm x 4.6 mm, 5  $\mu$ m). The eluent used at 1 mL/min flow rate for HPLC analysis had a 19 methanol/purified water ratio of 55/45 for MP and phenol or had a 0.1% acetic acid 20 methanol/purified water ratio of 70/30 for EE2. The injection volume for each sample was 100  $\mu$ L 21 and the UV detection wavelength was set at 254 nm for MP, 255 nm for phenol and 270 nm for 22 EE2.

23

# 24 **3. Results and discussion**

25 *3.1. Kinetic study: reaction of chlorine, bromine and monochloramine with MP and pH dependence* 

1 All chlorination and chloramination experiments were conducted in the presence of an excess oxidant concentration. Under these conditions, apparent second-order rate constants ranging from 2  $1.90 (\pm 0.10) \times 10^{-1}$  to  $4.60 (\pm 0.10) \times 10^{1} \text{ M}^{-1} \text{ s}^{-1}$  were obtained in the 6 to 10 pH range during 3 4 chlorination, whereas we observed low chloramine reactivity with MP with a second-order rate constant of 0.045 M<sup>-1</sup>.s<sup>-1</sup> at pH 8.5. This latter result was in the same order of magnitude as those 5 obtained previously for phenolic compounds (Abdallah et al. 2015; Cimetière et al. 2009). No other 6 7 pH level was tested during chloramination due to this low reactivity with MP. Regarding bromine, 8 experiments based on the competitive kinetic method were performed and apparent second-order rate constants between 2.26 ( $\pm 0.14$ ) × 10<sup>4</sup> and 3.35 ( $\pm 0.11$ ) × 10<sup>6</sup> M<sup>-1</sup>.s<sup>-1</sup> were found in the 6 to 11 9 10 pH range.

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Fig. 1 shows the variations obtained in the apparent second-order rate constants of chlorine 12 13 (k<sub>Chlorine/MP</sub>) and bromine (k<sub>Bromine/MP</sub>) as a function of the pH. Similar profiles are obtained for both 14 oxidants, with maximum koxidant/MP values noted at pH 8 for chlorination and pH 8.6 for 15 bromination. These pH profiles could be explained by taking the ionized and neutral MP species and the different chlorine or bromine forms into account. Accordingly, a kinetic model was 16 17 designed to predict variations in k<sub>Chlorine/MP</sub> and k<sub>Bromine/MP</sub> apparent rate constants according to the 18 pH. Table 1 gives a list of HOX and XO<sup>-</sup> reactions with neutral and ionized forms of MP that were 19 considered in the model simulations. In this Table, X represents Cl or Br, respectively, for chlorination or bromination experiments. For both oxidants, X<sub>2</sub>O and X<sub>2</sub> reactivity was neglected 20 21 since the chlorination reaction did not differ from a first-order reaction relative to chlorine, and 22 chlorine and bromine had high rate constants (Heeb et al. 2014; Sivey et al. 2010). Under these 23 conditions, since MP has second-order reactions with chlorine and bromine, and following a similar 24 rationale as that outlined in Abdallah et al. (2015), k<sub>Oxidant/MP</sub> could be formulated as follows:

25 
$$k_{\text{Oxidant/MP}} = \frac{k_1[H^+]^2 + k_2K_{a2}[H^+] + k_3[H^+]K_{a1} + k_4K_{a1}K_{a2}}{([H^+] + K_{a2})([H^+] + K_{a1})}$$
(1)

1 For each oxidant, the rate constants of elementary reactions 3 to 6 (i.e.  $k_1$ ,  $k_2$ ,  $k_3$  and  $k_4$ ) were 2 determined via non-linear least-square regression of the experimental data using the Sigma Plot 3 11.0 software package. The thus obtained elementary rate constants are shown in Table 1. For these 4 rate constants, the experimental and modeled values were closely correlated for both chlorination 5 and bromination, as shown in Fig. 1, thus validating the proposed reaction system. Under these conditions, for a pH range between 7 and 9, the overall reaction seemed to be mainly controlled by 6 7 the elementary reaction between the ionized form of MP and the protonated form of the oxidant 8 (HOX), leading to a maximum apparent rate constant for  $pH = (pKa_1+pKa_2)/2$ . This trend was in 9 line with previously reported findings on phenolic compound chlorination and bromination 10 (Abdallah et al. 2015; Deborde and von Gunten, 2008). Moreover, as previously observed by Yoom 11 et al. (2018), we found that bromine was four orders of magnitude more reactive with MP compared 12 to chlorine at pH 7. Fig. 1c shows the half-life patterns according to pH for the  $[Oxidant]_T = 14 \mu M$ ([Chlorine]<sub>T</sub> = 1 mg/L; [Bromine]<sub>T</sub> = 2.2 mg/L) constant values. Under these conditions, the half-13 14 lives of 32.5 min and 0.27 s at pH 7 were calculated for chlorination and bromination, respectively.

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16 The highest rate constants observed for elementary reactions with the ionized species of MP ( $k_2 > k_1$ 17 and  $k_4 > k_3$  for HOX and XO<sup>-</sup> respectively) could be attributed to the higher electron donor feature of 18 the phenolate function that is conducive to electrophilic attack of chlorine or bromine. As 19 previously shown with regard to various phenolic compounds, this could be illustrated by 20 comparing the elementary rate constant k<sub>2</sub> to the Hammett constants of the substituents that reflect 21 the electronic density of the aromatic ring (Heeb et al. 2014; Gallard et al. 2003; Lee and von 22 Gunten 2009; Abdallah et al. 2015; Duirk and Bridenstine 2013; Deborde and von Gunten 2008; 23 Guo and Lin 2009; Rebenne et al. 1996). Fig. 2 shows these correlations based on the reactivity of 24 protonated forms of chlorine and bromine (HOCl and HOBr) versus Hammett constants ( $\sigma_{o,m,p}$ ) for 25 various mono- and di-substituted phenols according to Duirk et al. (2013) and Heeb et al. (2014). In 26 this Figure,  $\sigma_{o,m,p}$  were calculated on the basis of previously reported values (Hansch and Leo 1995;

1 Hansch and Leo 1991), while the kinetic data were obtained from various studies (Gallard et al. 2 2003; Abdallah et al. 2015; Deborde and von Gunten 2008; Rebenne et al. 1996; Gallard and von 3 Gunten 2002; Pattison and Davies 2004; Echigo 2002; Acero et al. 2005). The negative slope 4 plotted for both oxidants (chlorine and bromine) was consistent with the electrophilic substitution 5 mechanism. Concerning chlorination, two different correlations were obtained for substituted phenols and dihydroxybenzenes, indicating that for the same  $\sum \sigma_{(o,m,p)}$  values, the substituted 6 7 dihydroxybenzene rate constants were more than one order of magnitude higher than those of 8 substituted phenols, as expected from the higher sensitivity of dihydroxybenzenes towards HOCl 9 substitution (Deborde and von Gunten 2008; Gallard and von Gunten 2002). There was close 10 agreement between the k2 rate constants obtained for MP chlorination and bromination and 11 Hammett-type correlations for phenolic compound chlorination and bromination, as shown in Fig. 2. Accordingly, it was assumed that there was a similar mechanism based on electrophilic 12 13 substitution on the ortho positions to the phenol during MP chlorination or bromination. The 14 formation of mono and dihalogenated derivatives was thus expected. Such transformation products 15 were previously reported by Canosa et al. (2006), Terasaki and Makino (2008), González-Mariño et al. 2011, Teraski et al. (2012 and Yoom et al. (2018). 16

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### 18 3.2. Impacts of Br/ammonia on MP chlorination and kinetic modeling

19 Chlorination experiments were conducted in the presence of Br<sup>-</sup> and/or ammonia at pH 7 and 8.5. The results are illustrated in Fig. 3 for pH 7 and Fig. 4 for pH 8.5. Kinetic modeling was undertaken 20 21 using Copasi software (Hoops et al. 2006) to simulate the experimental results for MP removal 22 under these conditions. The 12 reactions listed in Table 2 were considered in this modeling. First 23 transformation product reactions with chlorine and bromine were taken into account since they can 24 lead to oxidant consumption. In the case of monochloramine, reactions with the transformation products were overlooked based on its low reactivity with phenolic compounds. Similarly, reactions 25 26 of other haloamines with MP (and the transformation products) were assumed to be negligible as

1 previously noted by Abdallah et al. (2015). For these haloamines, low concentrations were actually expected according to Luh and Mariñas model (Luh and Mariñas 2014) (i.e. < 10<sup>-7</sup> M for 2 dichloramine, trichloramine and bromamines, at pH 7 for [Chlorine]<sub>T,0</sub> = 10  $\mu$ M and [NH<sub>4</sub><sup>+</sup>] = [Br<sup>-</sup>] 3 4 = 1  $\mu$ M). In addition, these species were generated slowly under our experimental conditions. 5 Finally, BrCl and BrOCl reactions were overlooked since the concentrations of these species were 6 several orders of magnitude lower than those of HOBr under our pH conditions, and regarding the 7 high HOBr reactivity with MP (Heeb et al. 2014). Calculations were conducted considering the 8 Hammett correlations described previously in Fig. 2 in order to determine the k<sub>2</sub> elementary rate 9 constants for halogenated MP products (Heeb et al. 2014; Duirk et al. 2013). The apparent rate 10 constants at pH 7 and 8.5 were obtained from the simplified equation 1, while considering the HOX 11 reaction with the ionized species of each compound as being the major reaction yet without 12 including the other reactive forms over the considered pH range (7-8.5).

13

14 Fig. 3a and 3c illustrate the findings of the experiments conducted at pH 7 in the presence of Br<sup>-</sup> or 15 ammonia. Faster MP degradation occurred in the presence of Br<sup>-</sup>, due to the higher rate constants of 16 bromination compared to chlorination. After a 10 min reaction time, the MP concentration 17 decreased by 21% in the absence of Br<sup>-</sup> compared to approximately 50%, 75% and 100% in the 18 presence of 1, 2 and 5 µM Br<sup>-</sup>, respectively. However, in the presence of ammonia, a decrease in 19 MP elimination during chlorination was observed with increasing ammonia concentrations due to chlorine reaction with ammonia, thus yielding chloramines which are known to have lower 20 21 reactivity. Total inhibition of MP elimination was observed in the presence of high ammonia 22 concentrations (10 µM). With the proposed reaction system and rate constants, there was close 23 agreement between the experimental data and the model simulations (Fig. 3a and 3c). The kinetic 24 model was therefore also used to simulate the oxidant variation patterns during the chlorination 25 experiments conducted in the presence of Br<sup>-</sup> or ammonia. As seen in Fig. 3b, the increase in Br<sup>-</sup> concentrations led to a decrease in free available chlorine concentration due to the reaction between 26

1 HOCl and Br<sup>-</sup>. At pH 7, rapid bromine formation was noted followed by its elimination due to its reaction with phenolic compounds (MP and transformation products). An increase in bromine 2 3 concentration was then expected when substantial MP removal was observed ([Br-] =  $5 \mu$ M; t = 2 4 min). Fast initial chlorine consumption leading to chloramine formation was observed in the 5 presence of increasing ammonia concentrations (without Br; Fig. 3d). Monochloramine decomposition was slow, as reflected by the low reactivity of monochloramine (NH<sub>2</sub>Cl) with MP. 6 7 All chloramine decomposition reactions were not considered in Table 2. However, complementary 8 modeling tests were conducted by taking into account complete chloramine decomposition reaction 9 systems according to Luh and Mariñas (2014) and Vikesland et al. (2001). The results obtained 10 under these conditions were in line with those shown in Fig. 3.

11

12 Fig. 4a 4b, 4c and 4d represent MP chlorination experiments performed in the presence of Br<sup>-</sup> or 13 ammonia at pH 8.5. Results similar to those obtained at pH 7 were obtained in both experiments in 14 the presence of Br<sup>-</sup> or ammonia, i.e. an increase in MP elimination in the presence of Br<sup>-</sup> and a 15 decrease in MP decay in the presence of ammonia. However, at pH 8.5, a lower rate constant for the chlorine reaction with Br<sup>-</sup> ( $k_{HOCl/Br}$ <sup>-=</sup> 153 M<sup>-1</sup>.s<sup>-1</sup> at pH 8.5 versus 1200 M<sup>-1</sup>.s<sup>-1</sup> at pH 7) and a 16 17 higher bromine reactivity with MP (and transformation products) lead to slower bromine formation and faster consumption during the experiments performed at pH 8.5 in the presence of Br. 18 19 Consequently, lower bromine concentrations were expected compared to those predicted at pH 7 20 and an increase in bromine concentration was expected only when significant MP elimination was 21 achieved ( $[Br^-] = 5 \mu M$ ; t = 10 min). In parallel, in the presence of ammonia, there was more rapid 22 monochloramine formation at pH 8.5 due to the higher rate constant of the reaction between chlorine and ammonia ( $k_{HOCl/NH_3}$ =1.33 ×10<sup>4</sup> M<sup>-1</sup>.s<sup>-1</sup> at pH 7 compared to 4.58 × 10<sup>4</sup> M<sup>-1</sup>.s<sup>-1</sup> at pH 23 8.5). 24

1 Finally, Fig. 3e, 3f, 4e and 4f show results obtained for experiments performed in the simultaneous 2 presence of ammonia and Br-. Under these conditions, a good correlation that supported the 3 proposed reaction system was obtained between the experimental data and the model simulations 4 for both studied pH levels. For a given Br<sup>-</sup> concentration, the inhibitory effect due to chlorine 5 consumption and chloramines formation was progressively observed as the ammonia concentration increased, regardless of the considered pH. However, in the presence of ammonia, the promoting 6 7 effect of bromine formation on MP degradation was more or less favored according to the pH level 8 (Fig. 3e and 4e). Accordingly, in the presence of equal quantities of Br<sup>-</sup> and ammonia, the overall 9 effect on MP elimination was pH dependent. After 10 min reaction time in the presence of  $[Br^-] =$ 10  $[NH_4^+] = 10 \mu M$ , MP removal was close to 50% at pH 7 whereas only 10% MP removal was observed at pH 8.5. Hence, the promoting effect of Br<sup>-</sup> was more marked at pH 7 while ammonia 11 12 had a predominant inhibitory effect at pH 8.5. The higher rate constant of the chlorine-bromide reaction at pH 7, leading to a faster bromine formation ( $k_{Chlorine/Br}$  = 1200 M<sup>-1</sup>.s<sup>-1</sup> at pH 7 versus 13 153 M<sup>-1</sup>·s<sup>-1</sup> at pH 8.5), together with the slight decrease of the rate constant of the chlorine-ammonia 14 reaction at pH 7 compared to pH 8.5 ( $k_{Chlorine/NH_2} = 1.33 \times 10^4 \text{ M}^{-1} \text{.s}^{-1}$  at pH 7 versus  $4.58 \times 10^4 \text{ M}^{-1}$ 15 <sup>1</sup>.s<sup>-1</sup> at pH 8.5), could partially explain this phenomenon (as shown in Fig. 3f, 4f). 16

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18 MP decay after 10 min chlorination in the presence of different Br<sup>-</sup> and ammonia concentrations 19 was estimated in Fig. 5 based on the reactions reported in Table 2. These results showed that, for 20 given Br<sup>-</sup> and ammonia concentrations, the overall impact could differ significantly according to the 21 pH considered. At pH 7, the promoting effect of Br prevailed over the inhibitory effect of 22 ammonia. Consequently, MP removal by bromine was favored during chlorination in the presence of Br- under water treatment conditions, which could lead to the formation of brominated 23 24 transformation products. These latter compounds are usually more toxic than chlorinated by-25 products (Chisholm et al. 2008; Sharma et al. 2014; Zhai et al. 2014).

### 1 **4. Conclusion**

2 Chlorine was shown to be an efficient oxidant for MP elimination, with apparent rate constants of up to 33.7 M<sup>-1</sup>.s<sup>-1</sup> at pH 8.5. In the presence of Br<sup>-</sup> and ammonia (e.g. under water treatment 3 4 conditions), chlorine is consumed as a result of Br<sup>-</sup> producing bromine or of ammonia producing 5 chloramines. Bromine was shown to be highly reactive with MP, with an apparent rate constant of 2.37 x 10<sup>6</sup> M<sup>-1</sup>.s<sup>-1</sup> at pH 8.5, whereas low monochloramine reactivity was noted. Accordingly, 6 7 during chlorination in the presence of Br, MP elimination could be induced by bromine and the 8 formation of brominated transformation products-assumed to be more toxic-could potentially be 9 observed. In the presence of ammonia, partial or total inhibition of MP elimination could occur. 10 Finally, in the presence of both Br<sup>-</sup> and ammonia (e.g. under water treatment conditions) the overall 11 impact is pH dependent. For given Br and ammonia concentrations, a more relevant inhibiting impact of ammonia at pH 8.5 is observed due to the fast chlorine consumption, compared to a more 12 13 pronounced promoting effect of Br<sup>-</sup> which resulted in rapid bromine formation at pH 7. In this 14 study, a kinetic model considering the different possible reactions was designed to predict 15 methylparaben removal during chlorination in the presence of Br<sup>-</sup> and ammonia. This model could 16 be used to assess other alkyl parabens which include alkyl substituents with similar electronic 17 effects. Based on Hammett-type correlations, the method described in this study could also be used 18 to estimate the removal of other phenolic compounds during the water chlorination steps.

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Fig. 1 Variation in the apparent second-order rate constants for MP reaction with chlorine (a) and bromine (b) as a function of the pH level. Symbols show measured data and solid lines are the obtained modeled values of koxidant/MP using non-linear least squares (c) Comparison between chlorination and bromination rate constants and half-lives calculated by considering  $[Oxidant]_T = 14 \mu M$  ([Chlorine]\_T = 1 mg/L and [Bromine]\_T = 2.2 mg/L)

regression.



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Fig. 2 Correlations between the second order rate constants for phenoxide ions reactions with
chlorine (a) and bromine (b) and the Hammett constants according to Duirk et al. (2013), Heeb et
al. (2014)



**Fig. 3** MP chlorination in the presence of Br<sup>-</sup> and/or ammonia at pH 7 ([MP]<sub>T,0</sub> = 2 ( $\pm$  0.2)  $\mu$ M, [Chlorine]<sub>T,0</sub> = 10 ( $\pm$ 1)  $\mu$ M ; and T= 20  $\pm$  2°C). Symbols show experimental data and solid lines are the modeling simulations obtained using Copasi software (Hoops et al. 2006)



**Fig. 4** MP chlorination in the presence of Br<sup>-</sup> and/or ammonia at pH 8.5 ([MP]<sub>T,0</sub> = 2 (± 0,2)  $\mu$ M, [Chlorine]<sub>T,0</sub> = 10 (±1)  $\mu$ M ; and T = 20 ±2°C). Symbols are experimental data and solid lines represent the modeling simulations obtained using Copasi software (Hoops et al. 2006)



**Fig. 5** Modeling of MP removal during chlorination in the presence of different Br<sup>-</sup> and ammonia concentrations (t = 10 min [MP] = 2  $\mu$ M, [Chlorine]<sub>T</sub> = 10  $\mu$ M). (a) pH = 7; (b) pH = 8.5



**Table 1** List of elementary reactions considered for MP chlorination and bromination (X = Cl or Br)

Reactions			Chlorination	Bromination			
1	$HOX \leftrightarrows XO^- + H^+$	pKa <sub>1</sub>	7.54 <sup>a</sup>	8.89 <sup>c</sup>			
2	$MP \ \leftrightarrows MP^- + H^+$	pKa <sub>2</sub>	8.4 <sup>b</sup>				
3	$HOX + MP \rightarrow products$	$\mathbf{k}_1$	$1.46 \ (\pm 0.25) \times 10^1 \ M^{-1}.s^{-1}$	6.48 (±11.8) × $10^3$ M <sup>-1</sup> .s <sup>-1</sup>			
4	$HOX + MP^- \rightarrow products$	$k_2$	$5.60 (\pm 0.43) \times 10^2  \text{M}^{-1}.\text{s}^{-1}$	$3.11 (\pm 0.77) \times 10^6 \mathrm{M}^{-1}.\mathrm{s}^{-1}$			
5	$XO^- + MP \rightarrow products$	k <sub>3</sub>	negligible	negligible			
6	$XO^- + MP^- \rightarrow \text{products}$	<b>k</b> 4	negligible	$1.03 (\pm 0.26) \times 10^6 \mathrm{M}^{-1}.\mathrm{s}^{-1}$			

<sup>a</sup> Morris 1966, <sup>b</sup> Tammilehto and Büchi 1968, <sup>c</sup> Lee and von Gunten 2009

#### Table 2 Different reactions and apparent rate constants at pH 7 and 8.5 considered for kinetic modeling of MP removal during chlorination in the 1

#### presence of Br- and ammonia 2

N°	D (1	Transformation	$\sum \sigma_{o,m,p}$	pKa <sup>f</sup>	$k (M^{-1}.s^{-1})^b$	Apparent rate constant (M <sup>-1</sup> .s <sup>-1</sup> )	
	Keactions	Products				рН 7	pH 8.5
1	HOC1 + MP-	CIMP-	0.45 <sup>i,j</sup>	8.4 <sup>h</sup>	$5.60 \times 10^{2 a}$	$4.30 \times 10^{1  a}$	$3.37 \times 10^{1 a}$
2	HOC1 + C1MP-	Cl <sub>2</sub> MP-	0.60 <sup>i,j</sup>	7.0 <sup>g</sup>	$1.23 \times 10^{2}$ c	$4.77 \times 10^{1  e}$	$1.18 \times 10^{1 e}$
3	HOCl + Br-	HOBr + Cl <sup>-</sup>		_	$1.55 \times 10^{3} \mathrm{m}$	$1.20 \times 10^{3 e}$	$1.53 \times 10^{2} e$
4	HOBr + MP-	BrMP <sup>-</sup>	$0.45^{i,j}$	8.4 <sup>h</sup>	$3.11 \times 10^{6 a}$	$1.25 \times 10^{5 a}$	$2.37 \times 10^{6  a}$
5	HOBr + BrMP-	Br <sub>2</sub> MP <sup>-</sup>	0.60 <sup>i,j</sup>	7.2 <sup>g</sup>	$5.01 \times 10^{5  d}$	$1.91 \times 10^{5 e}$	$3.39 \times 10^{5  e}$
6	HOC1 + BrMP-	BrClMP <sup>-</sup>	0.60 <sup>i,j</sup>	7.2 <sup>g</sup>	$1.23 \times 10^{2  d}$	$3.69 \times 10^{1  e}$	$1.16 \times 10^{1  e}$
7	HOBr + ClMP-	BrClMP-	0.60 <sup>i,j</sup>	7.0 <sup>g</sup>	$5.01 \times 10^{5  d}$	2.47 × 10 <sup>5</sup> e	3.45 × 10 <sup>5</sup> e
8	HOCl + NH <sub>3</sub>	$NH_2Cl + H_2O$	_	9.25	$3.07 \times 10^{6  k}$	$1.33 \times 10^{4} e$	$4.58 \times 10^{4 e}$
9	$NH_2Cl + H_2O$	$NH_3 + HOC1$	_	_	$2.11 \times 10^{-5 \text{ k}}$		
10	$HOC1 + NH_2C1$	$NHCl_2 + H_2O$	_	_	$1.50 \times 10^{21}$	$1.20 \times 10^{2 e}$	$1.53 \times 10^{1  e}$
11	$NHCl_2 + H_2O$	$NH_2Cl + HOCl$	-	_	$6.39 \times 10^{-71}$		-
12	NH <sub>2</sub> Cl + MP <sup>-</sup>	products	0.45 <sup>i,j</sup>	8.4 <sup>h</sup>	_	<0.045ª	0.045 <sup>a</sup>

<sup>a</sup> This study, <sup>b</sup> Correspond to the rate constant k<sub>2</sub> of the oxidant (HOCl or HOBr) with the deprotonated form in the case of reagents with pKa value, <sup>c</sup> k<sub>2</sub> calculated using the Hammett correlation 34567 for monohydroxybenzene chlorination (Duirk 2013), <sup>d</sup>k<sub>2</sub> calculated using the Hammett correlation for bromination of monohydroxybenzene (Heeb et al. 2014), <sup>e</sup> Apparent rate constant k<sub>Oxidant/P</sub> calculated by considering the reaction between HOX and the deprotonated form as the major reaction; <sup>f</sup> pKa values correspond to the compound reacting with the oxidant (HOCl or HOBr); <sup>g</sup> Calculated using Marvin Sketch®; h Tammilehto and Büchi 1968, i Hansch et al. 1991, J Jonsson et al. 1993, k Qiang and Adams 2004, Margerum et al. 1978, m Kumar and Margerum 1987