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Performance analysis of proton exchange membrane fuel cell in automotive applications

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Abstract: *This paper deals with the performance analysis of a proton exchange membrane fuel cell in automotive applications and especially for start/stop phases. Start-Stop cycles are one of the main sources of degradation for fuel cell systems, embedded in the automotive applications, among other dynamic conditions as idling, load cycling or high power. In this study, polarization curves and electrochemical impedance spectra are used to analyze the degradation mechanisms inside fuel cell stack during start/stop cycling. Obviously, the carbon support of the catalyst layer is the main constituent that suffers performance degradation during the 2,600 successive cycles performed. The impedance measurement of a 5kW PEM fuel cell stack revealed that the ohmic resistance does not vary whereas the charger transfer and mass transfer resistances increase drastically depending on the number of cycle repetitions. The oxygen reduction reaction impact due to the fuel/air interface is also visible even if the reactants are consumed with a dummy load for the shutdowns.*

Keywords: *Proton exchange membrane fuel cell; start/stop cycling; durability; performance analysis; degradation mechanisms; oxygen reduction reaction.*

1. Introduction

Even if the smog pollution emission standards have been strengthened over time making the air substantially cleaner and healthier, NOx pollution is still a problem [1], [2]. Indeed, in the recent years,

there has been a steady overall reduction in greenhouse gas (GHG) emissions in the EU, except for the transport sector as its relative contribution to overall GHG emissions in Europe has become more significant [3], [4]. Therefore, actions are needed in order to meet emission reduction targets (nitrogen oxides (NO_x) and ultra-fine particles), especially in transport applications [5]. As given by the European Environment Agency (EEA), the projected trends suggest that the transport sector is unlikely to contribute to the emission reductions needed to achieve the EU's new targets for 2030 or to achieving climate neutrality by 2050 [6]. Therefore, further restrictive standards will be implemented for transport (i.e., Euro-7 standard) as road transport constitutes the highest proportion of overall transport emissions (around 71% in 2018). Decarbonized actions must be taken to move towards carbon neutrality. The Euro 7 emission standard proposed by the European Commission aims to ensure that a vehicle does not produce emissions throughout its life cycle, for all vehicles produced from 2025 [7], [8]. There are no precise figures yet, but the limits will be lower than those in the Euro 6 standard, which set NO_x emissions at 60mg/km for petrol vehicles and 80mg/km for diesel vehicles, as well as carbon monoxide emissions at 500 and 1,000mg/km, for petrol and diesel respectively. Other pollutants could complete the standards, including ammonia (NH₃). Less widely, there are also ultra-fine particles (PM<0.1), nitrogen oxide (N₂O) and even particles emitted by brakes.

Nowadays, hydrogen-energy and fuel cell systems appear as one relevant solution to face fuel dependency and GHG emissions [9]–[12]. Various studies consider hydrogen as a valuable option to face fossil fuel dependency and reduce global warming. In [13], Oldenbroek et al. addressed the question of the fuel cell electric vehicles and hydrogen balancing 100% renewable and integrated national transportation and energy systems for five countries in Europe. They assumed that hydrogen plays an important role in the transition toward a future- 100% renewable- energy and transport system. Other studies focused on the distribution system of hydrogen [14] as well as on the societal acceptability of this energy vector [15] [15]. Another point on which improvements are expected is the lifetime of the fuel cell system. In fact, the U.S. Department of Energy (DoE) requires a durability in automotive drive cycle of 8,000 hours with a performance loss of less than 10% of power [16]. An

additional aspect to take into account in the transport applications is the start-up/shutdown durability. Again, based on US DoE figures, the target is set at 5,000 start/stop cycles. It is important to know that the start-up and shut-down phases of a PEM fuel cell are one of the most degrading according to Pei et al. in [17]. They are therefore among the issues to be studied in order to drastically improve the lifetime of the electrochemical system. In [18], authors reviewed the start/stop experiments from literature and from developed models. It is observed that the range of degradation during the start/stop phases is between 15 and 65 μ V/cell/cycle with a mean degradation value determined as 25 μ V/cell/cycle. This degradation rate is twice as high as that encountered during the idling and high current phases for one hour of operation. Therefore, and obviously, it is necessary to optimize the duration and the frequency of these start/stop phases. Another tricky point when studying start/stop cycles is the method of purging the system when it stops. Oyarce et al. [19] compared PEMFC shutdown strategies to mitigate carbon corrosion of the catalyst support. The comparison is based on 1100 start/stop cycles with five different strategies including: without any purge, air purge, fuel consumption, air consumption and fuel purge. This comparative study shows that the best solution is to purge the cathode with fuel because the cathode is protected from high electrode potentials by hydrogen. However, two fuel/air fronts occur on both cathode and anode sides with the safety problems related to fuel/air mixture and the fuel could not be used as a gas purge in a transport framework. Thus, the oxygen consumption should be a good strategy for the shutdown process but it requires having a dummy load to consume oxygen at the cathode side. Lin et al. [20] also studied shutdown strategies to limit carbon corrosion and local starvation. Their method combines auxiliary load and air purge steps. Yang et al. [21] study the interest of using a dummy load to limit the degradation of the fuel cell during shutdown. The result shows that the dummy load can effectively reduce the duration of fuel/air interface, so that the reverse current effect is relieved. Zhang et al. [22] propose an extension of Yang's method with a two-phase dummy load strategy. The first main load declined at a certain linear rate, accompanied by the consumption of residual oxygen in the cathode

in order to avoid air starvation. Then, the following fixed dummy load aimed to consume the residual small amount of oxygen still located in the catalyst layer and gas diffusion layer.

The main contribution of this paper is to investigate the degradation rate of a PEM fuel cell stack, with a power of 5 kW dedicated to transport applications, undergoing a succession of start/stop cycles for 2,600 hours. Moreover, the PEM fuel cell shutdown strategy discussed in this paper is done without any purge. Both anode and cathode compartments are closed simultaneously so that they are no longer supplied with gas when the dummy load is connected. By adding this device, all residual amount of oxygen in the catalyst layer and gas diffusion layer are consumed quickly to limit the fuel/air interface as much as possible as explained in [22].

From this aim, this paper first introduces the experimental setup with PEMFC and test bench specifications and then the experimental protocol is described in detail in Section 2. The experimental results are given in Section 3 by considering the voltage degradation, the characterization measurements as well as the degradation rate observed on this automotive PEMFC short stack. Finally, results are discussed integrating degradation rates observed for start/stop cycles and long resting times. A conclusion is proposed in Section 4.

2. Experimental setup

2.1. Fuel cell stack specifications and test bench

In this study a 5 kW-PEMFC stack is devoted to start/stop duration tests. As it is a Symbio fuel cell stack, all values are normalized by cell in order to maintain the confidentiality of such sensitive data.

The nominal specifications are detailed in Table 1 and Figure 1 presents the general architecture of the dedicated test bench. Both gas lines are equipped with mass flow regulators and pressure regulators. The gases are humidified by passing through thermoregulated bubblers and they are saturated with water vapor. Condensates are evacuated thanks to gravity separators. Both gas lines are then heated until the fuel cell inlet with the help of self-regulating heating cables. The cooling system is composed of two circuits connected by a water/water heat exchanger. Gas and coolant temperature, pressure and relative humidity are measured at the inlet and the outlet of the fuel cell stack. The stack temperature is considered as the outlet coolant temperature. All fluidic, electric and thermal parameters are recorded all along the experiments at an acquisition frequency of 1Hz.

Table 1: Nominal fuel cell specifications

Nominal operating conditions	
Coolant	
Coolant Out Temperature = Stack Temperature [°C]	82
Coolant Inlet pressure [bar absolute]	2
Cathode	
Air Inlet Pressure [bar absolute]	confidential
Air Inlet Stoichiometry	confidential
Air Inlet Relative Humidity [%]	confidential
Air Inlet Temperature [°C]	70

Anode	
Hydrogen Inlet Pressure [bar absolute]	confidential
Hydrogen Inlet Stoichiometry	confidential
Hydrogen Inlet Relative Humidity [%]	confidential
Hydrogen Inlet Temperature [°C]	82

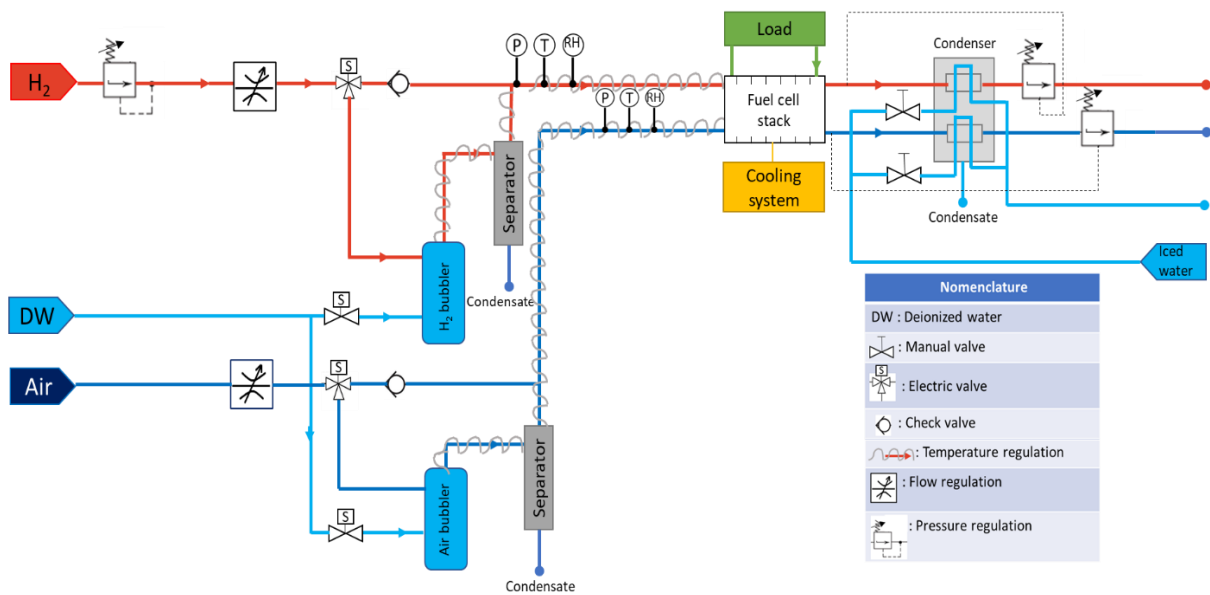


Figure 1: Test bench architecture

2.2. Experimental protocol

The aim of this paper is to consider specific phases relative to vehicle operating conditions. Here, start and stop case is mainly studied as well as the relative degradation aspect. Thus, the start-up and shutdown phases of the fuel cell shall be carried out successively and repeated as many times as possible until the end-of-test criterion, defined as a minimum voltage of 0.3V for a single cell, is reached.

One start and stop cycle takes one hour with the first 30 minutes for the stop state without nitrogen purge but with reactant consumption and the last 30 minutes for the start state, including preheating

the stack coolant. The maximal reaching load during the startup step is set at $1.5\text{A}/\text{cm}^2$. The dummy load allows the consumption of residual oxygen in the cathode, which avoided air starvation.

The start-up and shut-down repetition (2,600 cycles) was carried out with the following steps:

1. The fuel cell is running at a current density of $1.5\text{A}/\text{cm}^2$. The relative humidity, the pressure and stoichiometry at anode and cathode sides are both regulated and fixed for the needs of the fuel cell stack. The stack temperature is 82°C . After at least 30 minutes of stabilization under these operating conditions, the shutdown procedure can start.
2. The load is shut off as well as the reactants supply. The pressure, gas temperature and humidity regulations are also shut off. The coolant flow is maintained, and the stack temperature decreased until reaching the ambient temperature (approx. 25°C). When ambient temperature is reached, the cooling system is shut off. Both gas inlet solenoid valves are closed to limit the oxygen suction from the pipe located between the valves and the stack inlet and hence, the oxygen diffusion to the anode side. After that, the dummy load is connected with constant current density of $0.02\text{A}/\text{cm}^2$. The cell voltages dropped under 0.1V indicating a primary depletion of the oxygen in the cathode side. This step of air consumption with the dummy load is repeated 3 times to avoid the restrike of the cell voltages by consuming the residual small amount of oxygen still located in the catalyst layer and gas diffusion layer, as well as in the pipes upstream of the stack inlet (which have a significant length). The fuel cell remains in these shutdown conditions for 30 minutes.
3. For the startup phase, a pre-heating step is advised just in order to discriminate damages due to cold starts from damages due to start/stop cycling. The stack temperature is set to 82°C , the gas temperature and humidity are shut on. A minimum reactants flow corresponding to a current density of $0.3\text{A}/\text{cm}^2$ is set. Then, the pressure regulation is turn on and the load is increase stepwise (with a $0.2\text{A}\cdot\text{cm}^{-2}\cdot\text{s}^{-1}$ ramp) until gas flows and load reached the setpoint of $1.5\text{A}/\text{cm}^2$. The operating conditions are stabilized for 30 minutes.

The procedures are summarized on Figure 2. It is important to note that no nitrogen was used for purging the fuel cell stack as it is the case inside a vehicle application. A 3 seconds-delay is also fixed between the gas supply and the load demand.

Once a week, a polarization curve is performed following by 3 electrochemical impedance spectra (EIS) for 3 cells (extreme cells and mid-cell) and stack at 3 current densities of 0.5, 1 and 1.5A/cm². The nature of the applied signal is galvanostatic with an amplitude of the AC signal set at ±10% of the DC current and the sweeping frequency ranged comprised between 0.1Hz and 6kHz (46 data points, 10 points per decade of frequency). EIS were measured in order to study the change of the resistances, including ohmic resistance, charge transfer resistance for the oxygen reduction and mass transfer resistance.

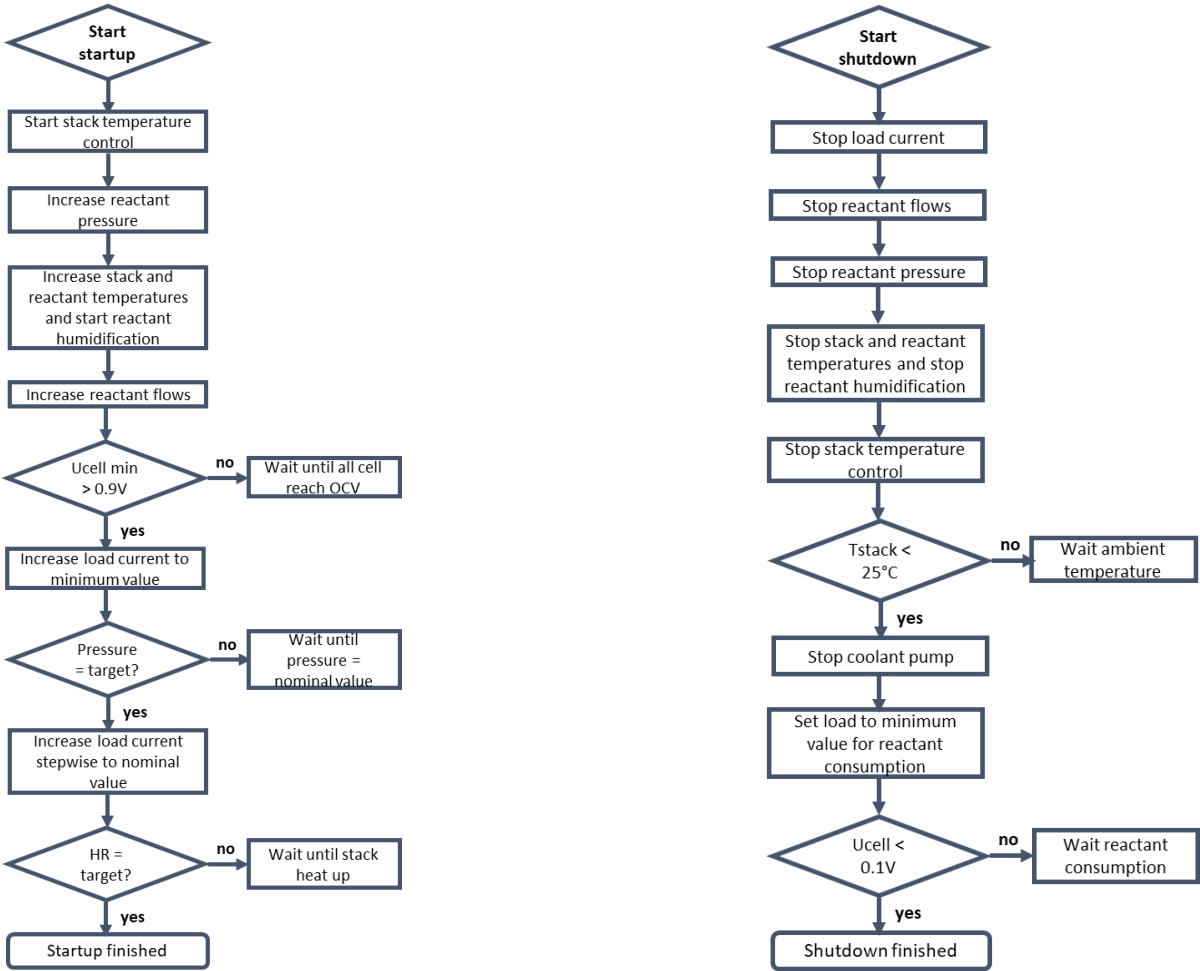


Figure 2: Experimental protocols for both startup and shutdown phases

3. Experimental results and discussion

3.1. Performance degradation of the fuel cell with start/stop cycles – Voltage vs. current analysis

Figure 3 shows the evolution of the performance degradation, over 2,600 start/stop cycles, representing approx. 4 months of cumulative tests. Figure 4 is complementary to figure 3 and presents the cumulative voltage loss along with start/stop cycles. The stack voltage degradation is represented for five current densities: 0, 0.5, 1, 1.5 and 1.9A/cm². The voltage is determined on the polarization curves performed during the experiment and corresponds to a date and hence, a number of cycles.

Generally, the trend is similar regardless of the current density, even if a bit higher for the two highest current densities. Furthermore, during the first 500 hours, the voltage decreases drastically (55 mV/cell lost at the maximal current density). This degradation could be attributed to an incomplete conditioning phase of the fuel cell performed before the start/stop cycles. During the conditioning phase, fuel cell performance increases, until reaching a performance plateau [23]. However, if this plateau is not achieved, the performance decreases drastically instead of increasing. So, during the first 500 hours, the membrane hydration seems not satisfying as well as the catalyst layer is not completely activated when start/stop cycling began. Moreover, during the break-in the platinum migrate in the catalyst layer and the particle coalescence continues during the first few hundred hours of vehicle operation, which results in a gradual performance drop. The migration of the catalyst seems to be not finished too. These are the start/stop cycles that end the activation of the stack.

From 500 hours of functioning, the performance increasing, and the degradation trend are less important than during the first 500 hours. The mean cell voltage loss is 0.1V, at the maximal current density, in 2,000 cycles compared to 1V in the first 500 cycles. Figure 4 clearly shows the two main trends (for the first 500 hours and from 500 hours).

Another point to raise is about the impact of the calendar aging. During this experiment, a long-closed time (7 weeks) took place between the third and fourth characterization. On restart, a performance

loss is observed in comparison with the third polarization after approx. 400 cycles. This could be due to the impact of calendar aging and the drying conditions [24], [25] that lead to non-optimal operating conditions even after a stabilization step at $1A/cm^2$ for 1 hour and a polarization curve. To validate this assumption, two new polarization curves are performed 2 days later and 5 days later, interspersed with start/stop cycles, to observe the performance evolution. It turns out that the fuel cell performance is recovered after one additional characterization even better than before the long shutdown. Thus, the effect of the aging was mitigated by an extended stop and a testing in well-humidified conditions. Another possible way is that the conditioning phase is achieved that reveals the best performance of the electrochemical device, after membrane hydration, porosity increasing of the catalyst layer and catalyst migration [26]. The following polarization curve (5 days later) is quite similar with little improvement on stack voltage at low current densities ($j < 0.6A/cm^2$). It is important to specify that the humidity and temperature conditions of the test cell are controlled and monitored even during the resting times.

There are some other periods without running the fuel cell due to unavoidable shutdowns and/or maintenances, for instance at 1,000 cycles. There are two points for the same abscissa, corresponding to two polarization curves separated by several days of calendar aging. The results show that the device is extremely sensitive to this non-operating time. After 200 additional start/stop cycles, the performance joined those before the experiment interruption.

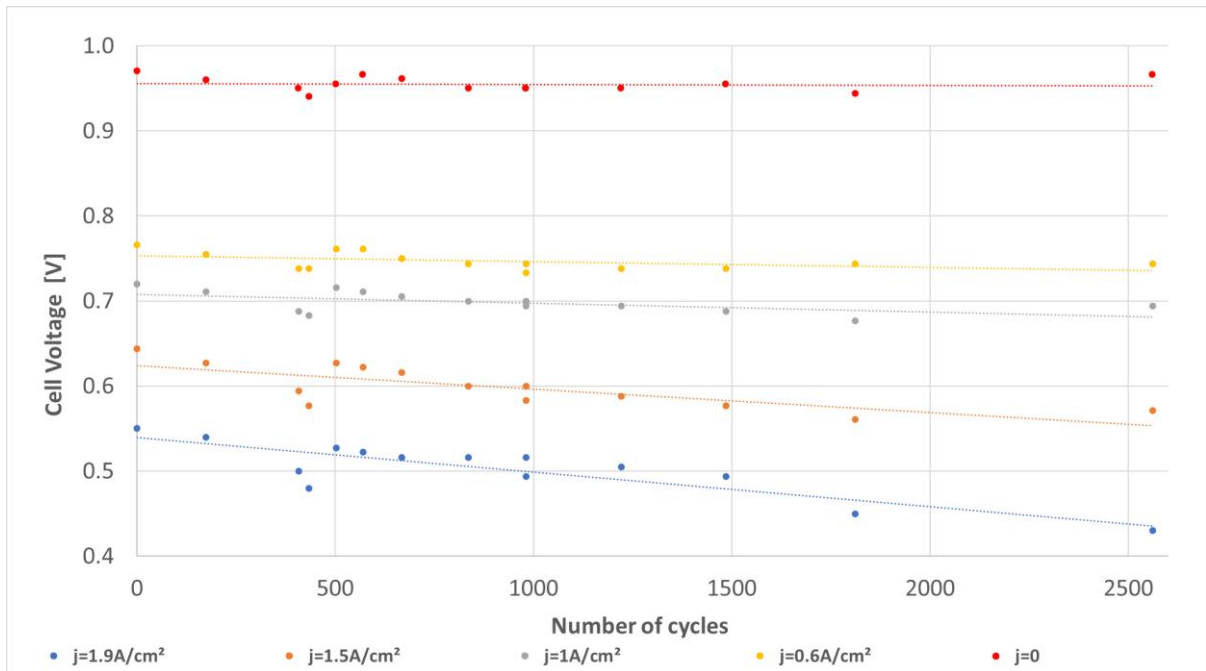


Figure 3: Evolution of the cell voltage with the number of start/stop cycles

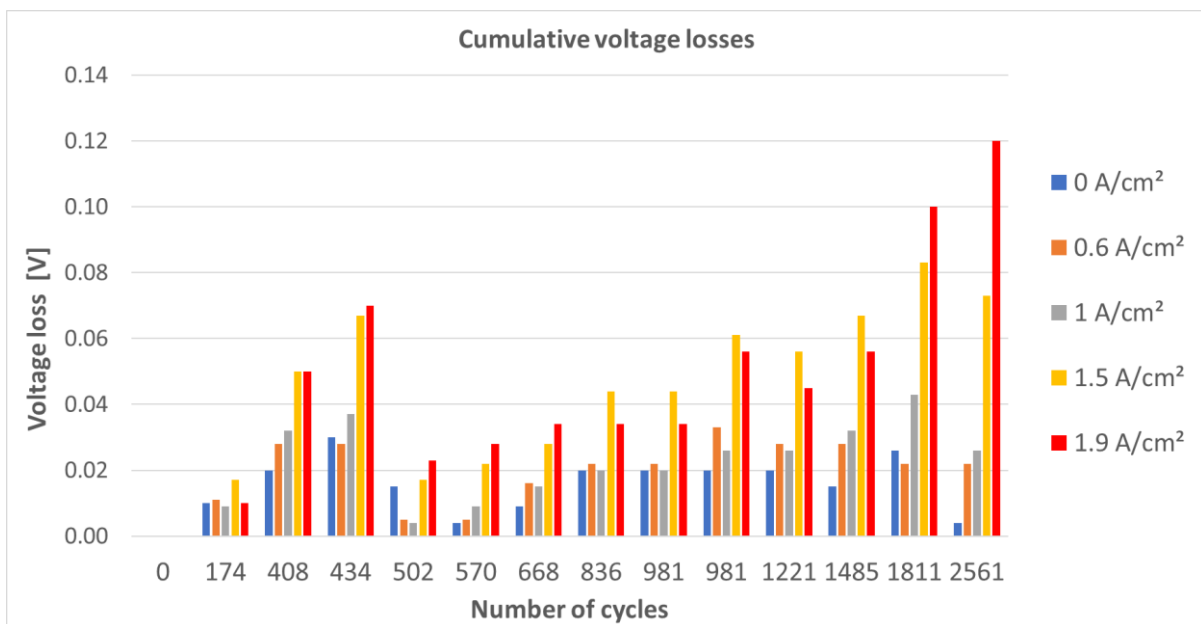


Figure 4: Cell voltage degradation with the number of start/stop cycles for five current densities

An additional test is performed to evaluate the performance loss during non-operating periods. Thus, at the end-of-test, the fuel cell is purged with nitrogen and the reactants are consumed. The stack is kept connected to the bench during one month without running. As a result of this, the trend of the

polarization curve is lower than one month before. The influence of the calendar aging is thus clearly visible on Figure 5.

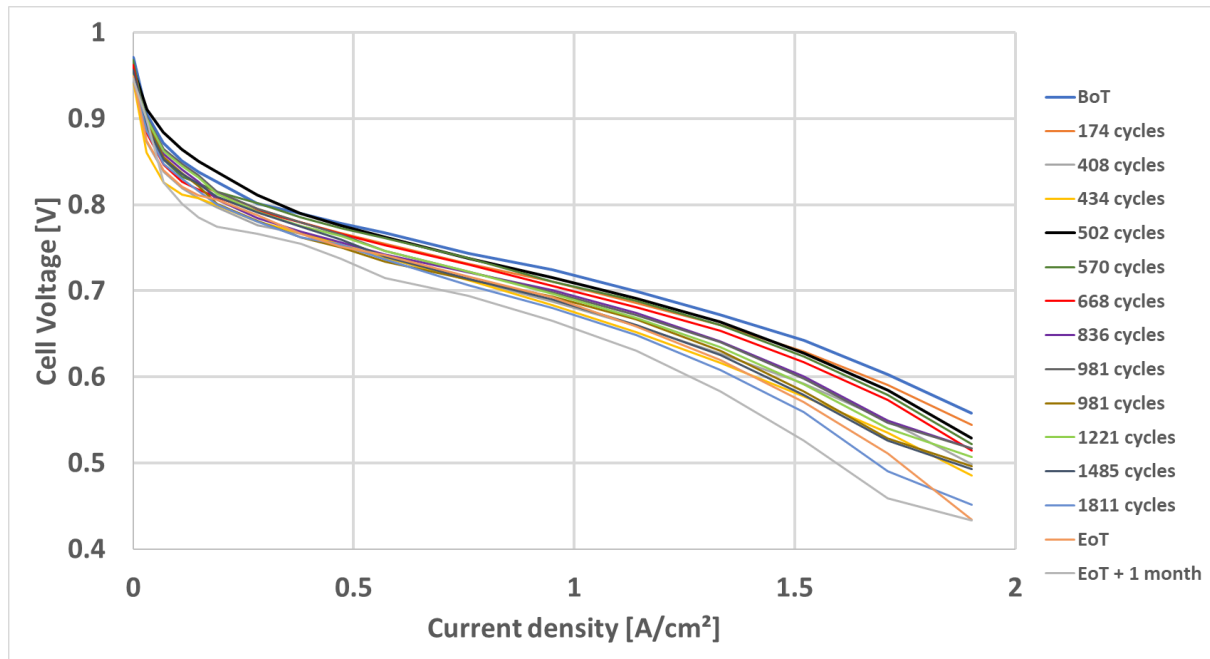


Figure 5: Comparison between polarization curves along start/stop cycles

Based on Figure 3, the degradation rate can be calculated to Equation 1.

$$\text{Degradation rate } [\mu\text{V}/\text{cell}/\text{h}] = \frac{\text{voltage at EoT } [\mu\text{V}] - \text{voltage at BoT } [\mu\text{V}]}{\text{Time [h]} / \text{Number of cells}} \quad (1)$$

The voltage at $0.5\text{A}/\text{cm}^2$ decreased from $0.76\text{V}/\text{cell}$ to $0.74\text{V}/\text{cell}$, with the degradation rate of $10\mu\text{V}/\text{cell}/\text{h}$. For the nominal current density at $1\text{A}/\text{cm}^2$, the voltage decreased from 13V to 12.4V that leads to a degradation rate of $13\mu\text{V}/\text{cell}/\text{h}$. While at $1.5\text{A}/\text{cm}^2$, the rate is $28\mu\text{V}/\text{cell}/\text{h}$ and $49\mu\text{V}/\text{cell}/\text{h}$ for the maximal current density of $1.9\text{A}/\text{cm}^2$. As one might expect, the degradation is higher at a high current density than at a lower current density as the MEA could not provide enough active sites for electrochemical reaction at high current density [27].

3.2. Performance degradation of the fuel cell with start/stop cycles – EIS analysis

Figure 6 presents the results of the electrochemical impedance spectra (EIS) performed, at the beginning-of-test (BoT) and at the end-of-test (EoT), on the whole stack and for three current densities. With increasing number of start/stop cycles, the real and the imaginary parts of the impedance plots increase at the same time.

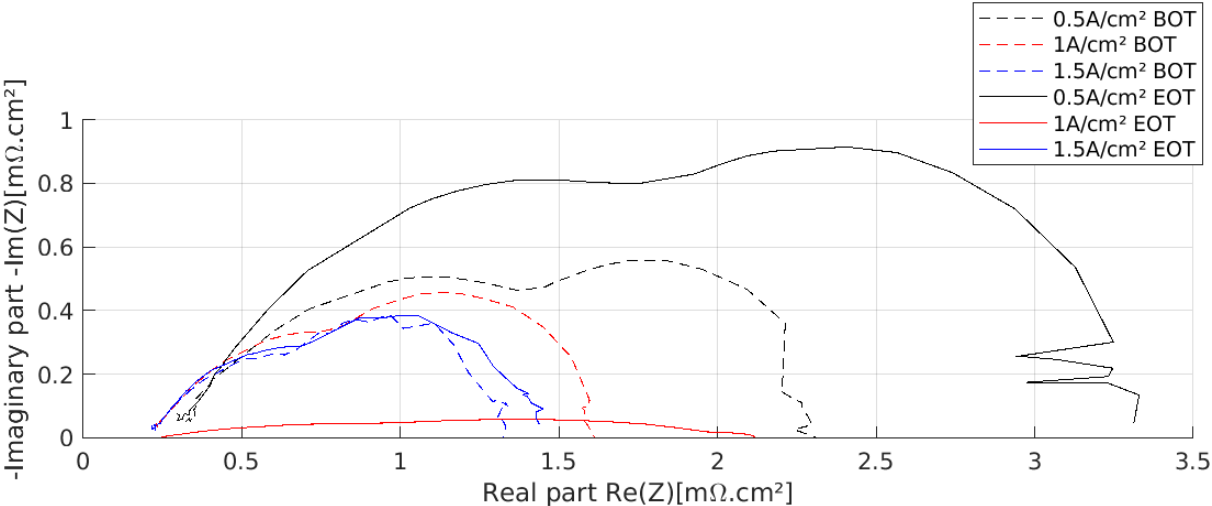


Figure 6: Comparison between the electrochemical impedance spectra on the fuel cell at the beginning-of-test (BOT) and the end-of-test (EOT) measured at 0.5A/cm², 1A/cm² and 1.5A/cm² from 100mHz to 6kHz (46 frequencies)

Based on an equivalent circuit (Figure 7), the ohmic, charge transfer, diffusion and polarization resistances are defined. The results are presented in Table 2. *R_{ohm}* is the ohmic resistance related to losses that are caused by the passage of ions through the membrane and the electrical resistances of the electrodes and connections. *R_{ct}* is the charge transfer resistance that model the resistance due to the passage of charges in electrode/electrolyte interface. It is also referring to the diameter of the first semi-circle of the impedance spectra. *R_{diff}* is the diffusion resistance which considers the mass transport losses and is representing by the diameter of the second semi-circle. *R_{pola}* is the polarization resistance including all resistive parts.

Table 2: Resistance values extracted from the impedance spectra

Resistance values [mΩ]	Current density [A/cm ²]		
	0.5 (BoT / EoT)	1 (BoT / EoT)	1.5 (BoT / EoT)
<i>R_{ohm}</i>	0.29 / 0.31	0.23 / 0.23	0.22 / 0.22
<i>R_{ct}</i>	1.48 / 2.13	0.94 / 1.16	0.61 / 0.72
<i>R_{diff}</i>	1.22 / 2.05	1.11 / 1.5	0.88 / 1
<i>R_{pola}</i>	2.27 / 3.27	1.6 / 2.1	1.33 / 1.44

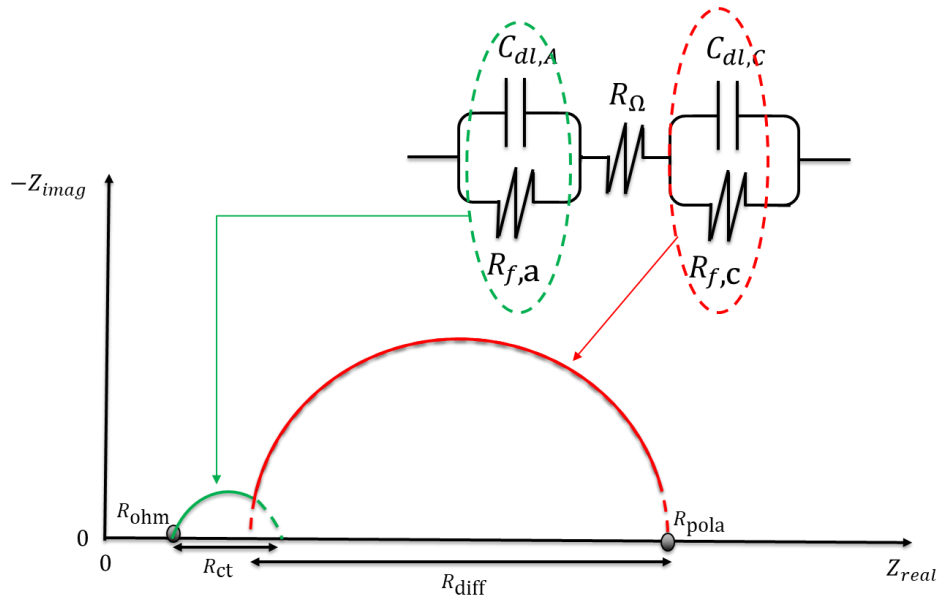


Figure 7: Equivalent circuit model for electrochemical impedance spectra

The ohmic resistances stay quite similar separately from the number of cycles. However, the results show a stronger cathode degradation mainly due to sluggish oxygen reduction reaction [28], [29]. During the startup phase, the anode is temporarily supplied with hydrogen so, a mix between H₂ and air appears at the anode side. Consequently, the potential increases to reach ~1.4V, at the cathode side. At this potential, water, carbon and/or platinum are oxidized. This phenomenon is so called

“reverse current decay mechanism” [28], [30], [31]. During start/stop phase, the fuel cell degradation is related with the high open circuit voltage which implies that the main degradation is related to the corrosion of the carbon support [18], [32]. The polarization resistance is higher at low current density because of the limiting gas flows that increase the charge transfer resistance (first semi-circle) and the diffusion resistance because the produced water is far less evacuated with the aging. It was found that carbon corrosion reduced the hydrophobicity of the pores in the catalytic layer, making it more prone to flooding [33].

4. Conclusion

This study deals with a long duration tests of a PEMFC stack under start/stop cycling. The main purpose is to propose a scientific analysis of the impact of such repetitive cycles on the fuel cell performance. The study rests on several measurements such as voltage, polarization curve, impedance spectra and also the degradation rate calculation depending on the number of cycles and the current density. It is shown that startup and shutdown phases clearly impact the MEA and especially the carbon support which is exposed to corrosion during air/fuel boundaries. This leads to an increase of the global resistance (R_{pola}) of 50% at the lower current density. Another phenomenon observed during this experiment is the aging due to long resting time. During these periods, the fuel cell is drying out, which is leading to a performance loss at the restart. The performance recovery is achieved after several operating hours and a remoisturing of the membrane. Indeed, the performance after 2,600 start/stop cycles remains in the degradation ranges obtained in the literature [18], with 5% and 10% loss of performance versus fresh MEA, respectively for a nominal current density of $1A/cm^2$ and $1.5A/cm^2$ (maximal current during start phase). Moreover, the Fuel Cell Technical Team Roadmap defined by the US DoE [34] targeted several degradation rates when considering unmitigated start/stop durability protocol with:

- less than 5% change for a voltage at $1.2A/cm^2$;
- less than 5% change for the high frequency resistance (R_{ohm}) at $1.2A/cm^2$;

- less than 10% change for the low frequency resistance (R_{pola}) at $1.2A/cm^2$.

In our experiment, no information is collected for a current density of $1.2A/cm^2$. However, both points at $1A/cm^2$ and $1.5A/cm^2$ can be considered as they are very close to $1.2A/cm^2$. Our results showed that the voltage loss at $1A/cm^2$ is 3.6% change, the resistance R_{ohm} has not changed at either $1A/cm^2$ or $1.5A/cm^2$, while R_{pola} is 8% change at $1.5A/cm^2$. All these results concur to say that the degradation levels respect the target degradations given by the US DoE.

Apart from start/stop cycles, 1,300 hours of operation have been performed, corresponding to the cumulative start phases (30 minutes for each). As future work, further investigations need to be achieved in order to be able to decorrelate the degradations related to the starts and stops, to OCV phases and load demand states.

5. Acknowledgment

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