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# Turbulent combustion with oxygen enrichment and capture of CO<sub>2</sub> in industrial boilers of medium power

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# CO2 EnergiCapt project

- ✓ **Period**: 2010-2015
- Support: ANR French National Research Agency
- ✓ ANR grant: 1 261 469€
- ✓ Subject: Integration of oxygen-enriched air combustion and CO<sub>2</sub> capture for existing boilers: development industrial demonstrator

#### **Project partners**

metropolis

- ✓ **ICARE CNRS**, specialist in combustion
- **LRGP CNRS**, specialist in capture of CO<sub>2</sub>
- ✓ LLT «Leroux et Lotz Technologies», manufacturer of industrial equipments ✓ **Polymem**, manufacturer fiber
- membranes for fluid treatments **CPCU**, operator of boilers of the Paris
  - dedicated to district heating heat production units and validate it on an industrial site

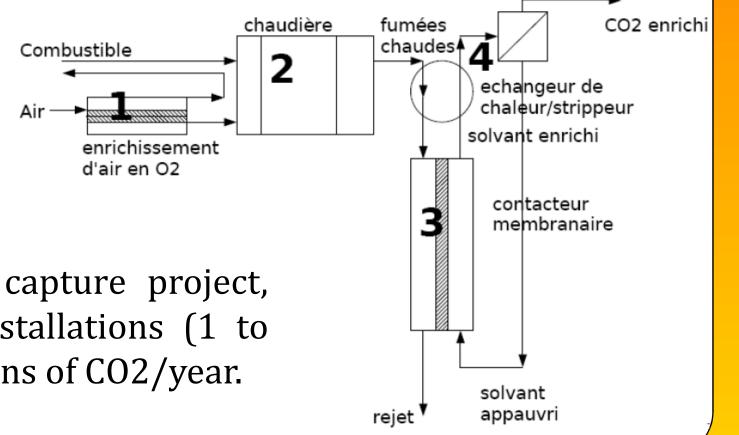
#### **Objective**

- **Optimization of industrial boilers** by the combination of combustion air enriched with oxygen and reducing CO<sub>2</sub> by a membrane capture.
- ✓ Development of a **CO**<sub>2</sub> capture pilot unit

# Description of CO2 EnergiCapt project

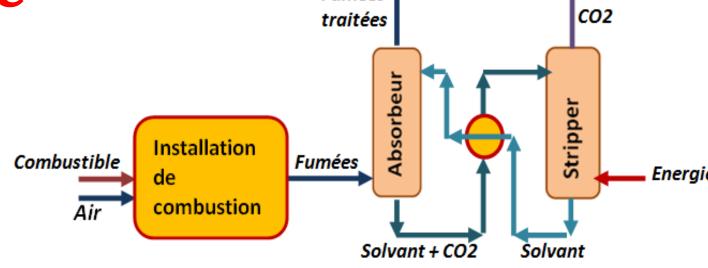
- 1 Oxygen Enriched Air
- 2 Combustion
- 3 CO<sub>2</sub> capture
- **4** Exchanger for CO<sub>2</sub> separation

✓ CO2 EnergiCapt is an innovative  $CO_2$  capture project, intended primarily for medium-power installations (1 to 100 MW), i.e. emitting 25,000 to 100,000 tons of CO2/year.



### Post-combustion CO<sub>2</sub> capture

Step 1 - Absorption: This step consists in putting the flue gas in contact with a solvent having a chemical affinity with CO<sub>2</sub> in order to combustible absorb it. The flue gas are then evacuated without the initial carbon dioxide.



**Step 2 - Desorption**: this step consists of providing energy to break bonds between the CO<sub>2</sub> and the solvent. The latter is then regenerated and reused to absorb CO<sub>2</sub> in step 1. The CO<sub>2</sub> is evacuated from the process.

#### Originality and application

- ✓ Technology: efficient, compact and competitive
- ✓ **Application**: medium power plants (1 to 100 MW). This range of facilities (9% of overall  $CO_2$  production) are almost ignored by CCS projects.
- ✓  $O_2$  enriched combustion: improved combustion  $\Rightarrow$ better thermal efficiency.
- **✓ Thermal integration** of the solvent regeneration process.
- ✓ Intensification of mass transfer and capture by membrane contactors ⇒ better mass transfer.
- ✓ Conception and realization a pilot: test and installation on a real boiler.

# Experiments and CO<sub>2</sub> capture results

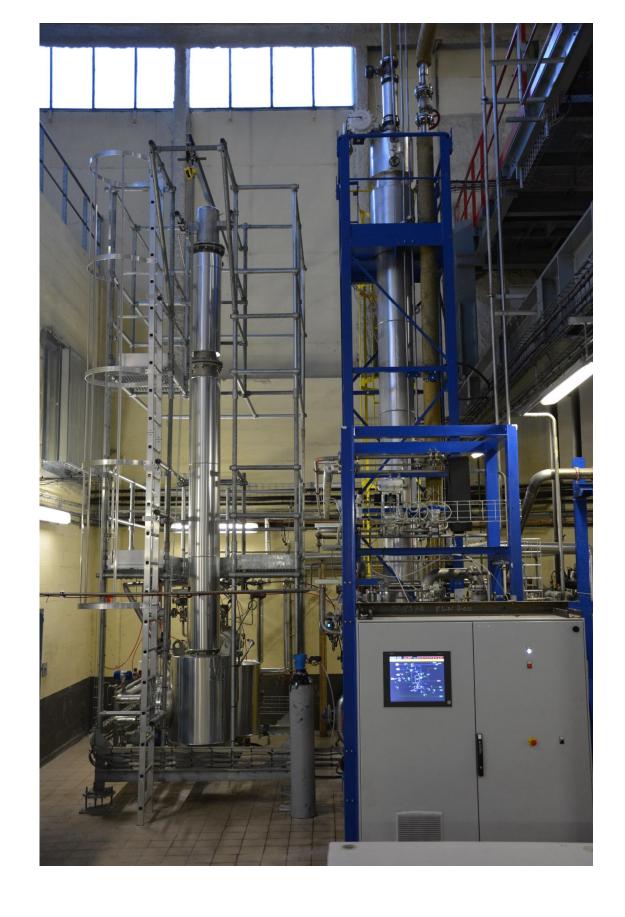
- ✓ Experiments in real conditions allowed to **validate** the performances of the membrane contactor and to capture CO<sub>2</sub> in the CPCU boiler by the CO<sub>2</sub> EnergiCapt pilot developed.
- ✓ Results are **very promising** in terms of CO<sub>2</sub> capture efficiency and the **robustness** of the pilot in terms of startup and **reactivity**.
- Tests on 10 and 50 m<sup>2</sup> contactors showed that the demonstrator has a CO<sub>2</sub> abatement rate of about 90% (with or without MEA regeneration) for flue gas flows of 12 and 150 Nm<sup>3</sup>/h, respectively.

CO<sub>2</sub> capture unit **is currently marketable** by LLT. The unit is **easily** integrated into an existing installation without the need for retrofit.

CO2 EnergiCapt has won two national trophies:

- Trophy for public research on Energy-climate-environment, 2015.
- Energy Transition Trophy in Technology category, 2017.

CO2-EnergiCapt demonstrator installed at the CPCU (LLT ®)



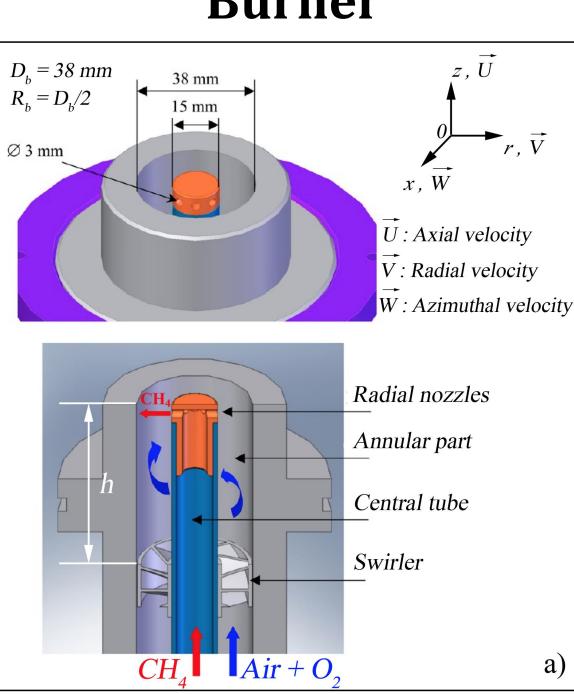
#### **ICARE-CNRS** research results

#### **Combustion chamber**



Combustion chamber with the OH\* Chimiluminescence system and gas analyzers. Dimensions 0.5x0.5x1 m<sup>3</sup> Power 25 kW.

# Burner

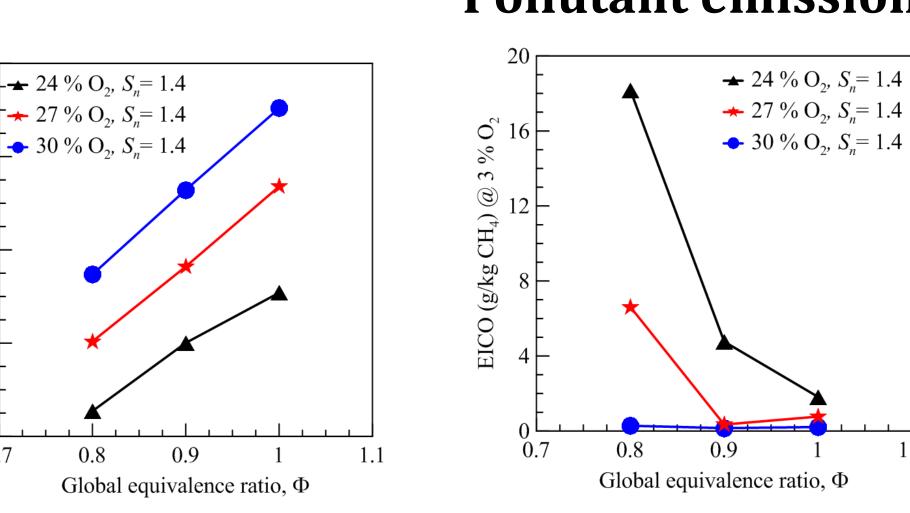


Two concentric tubes with a **swirler** in the annular part

**Example** of flame



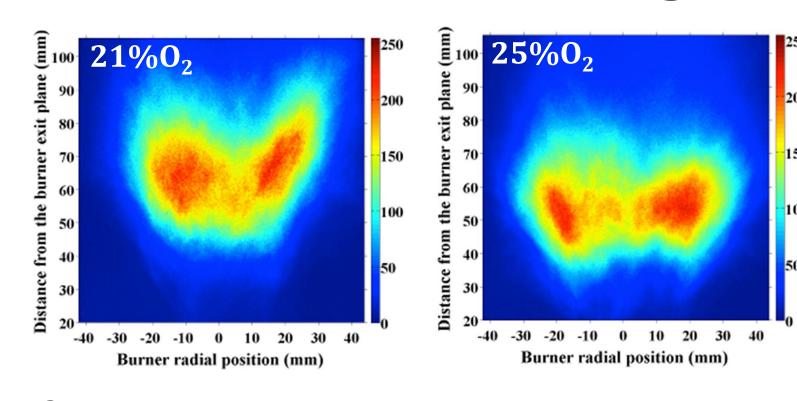
#### **Pollutant emissions**



With O<sub>2</sub> enrichment: CO<sub>2</sub> increases, CO decreases, NOx increases

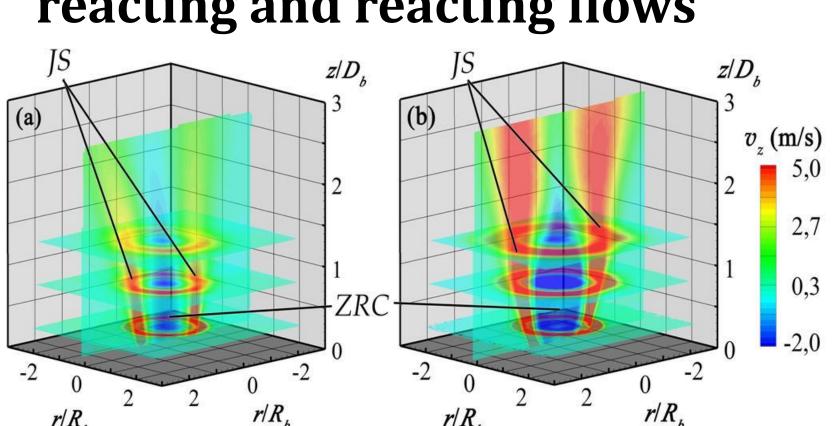
 $+24\% O_2$ ,  $S_n = 1.4$  $\star$  27 % O<sub>2</sub>,  $S_n = 1.4$ • 30 %  $O_2$ ,  $S_n = 1.4$ Global equivalence ratio,  $\Phi$ 

#### **Instantaneous OH\* images**



**⇒ Flame stability** is **enhanced** with oxygen addition even for low oxygen enrichment rates.

#### Velocity mean fields of non reacting and reacting flows



→ Recirculation zone at the flow center, and the swirling jet in the peripheral flow