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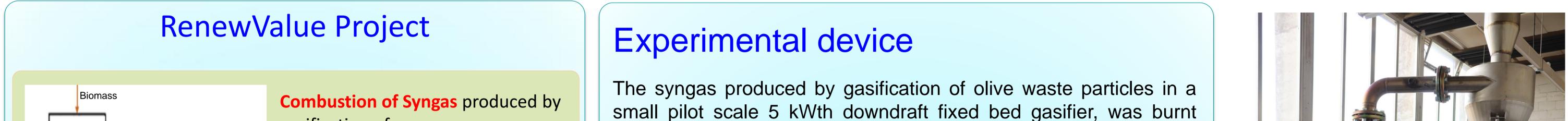
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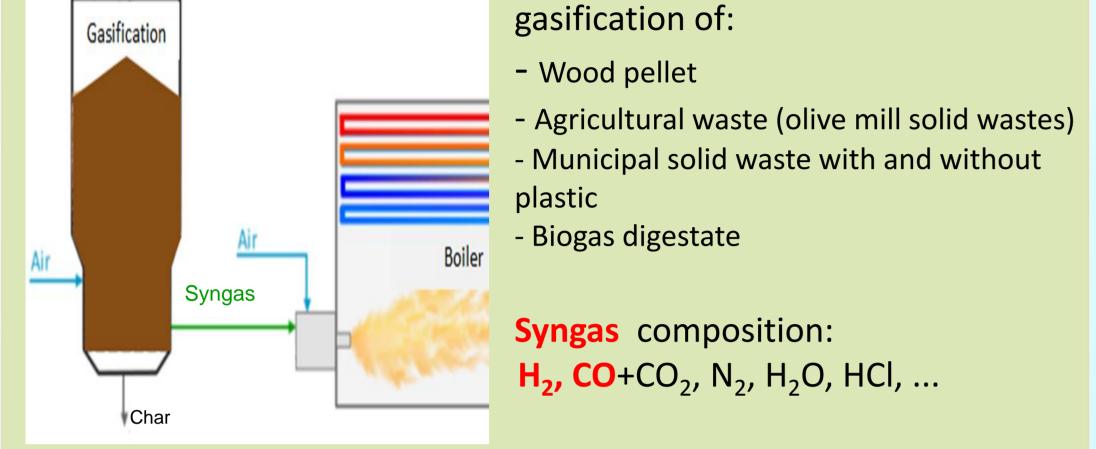
# Experimental study of combustion syngas released from gasification of agriculture waste in a downdraft gasifier

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#### European project: **ERANETMED2-72-169**

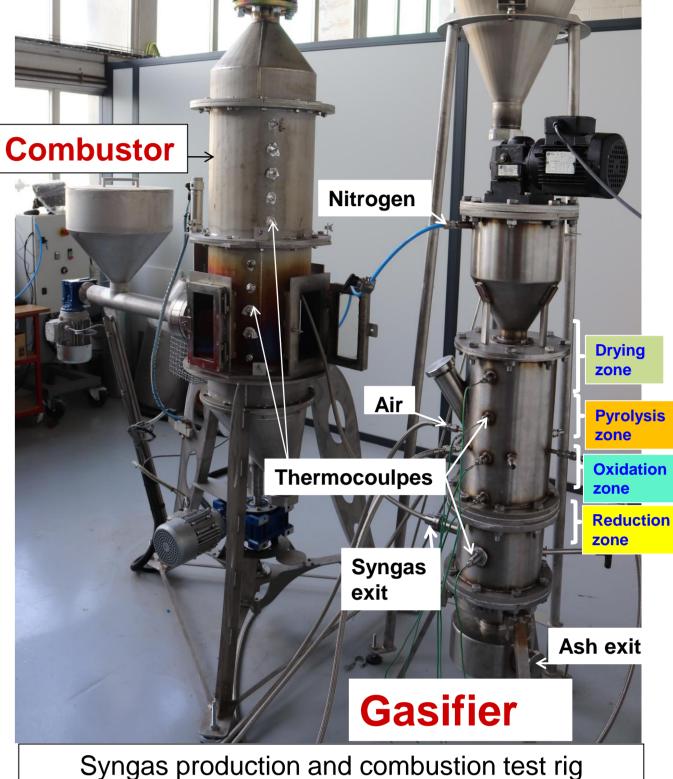
Subject: Local sustainable renewable energy supply for vulnerable communities in arid and semi-arid Mediterranean zones (MENA)

from a burner inserted in a combustor.

Gasifier and burner are made of stainless steel. The gasifier has a height of 0.682 m and an inner diameter of 0.190 m, lined with insulator thickness of 20 mm. The throat diameter is 0.047 m. The oxidizing agent is air, regulated via a mass flow controller. The syngas is regulated by high temperature vortex flow meter.

The nozzle exit inner burner diameter is 25 mm. The fuel nozzle consists of a center body fuel injector, a radial air swirler, and a mixing area. The burner is placed in the combustion chamber (Combustor).

For the temperature, 5 type-K thermocouples were used for recording temperature profile at different parts of the gasifier.



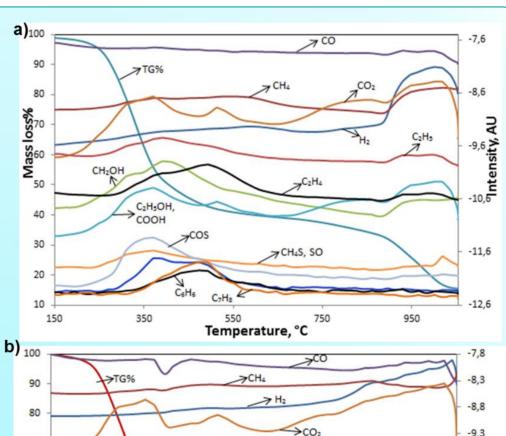
# **Feedstock materials**

The agricultural waste used in this work came from a traditional Moroccan olive oil extraction unit.

the Netzsch (STA 449 F3 Jupiter) thermal analyzer (TG-DTG) coupled with a quadruple (QMS 403D Aëolos) MS was used for thermogravimetric analysis of olive waste. The TG tests were carried out in ambient argon, oxygen and steam to estimate the pyrolysis, combustion and gasification characteristics.

# Thermogravimetry and mass spectrometry results

Thermal analysis of samples were performed at different heating rate over temperature range of 150-1050 ° C.



Moisture	7.5
Volatile Matter	69.5
Fixed Carbon	20.2
Ash	2.8

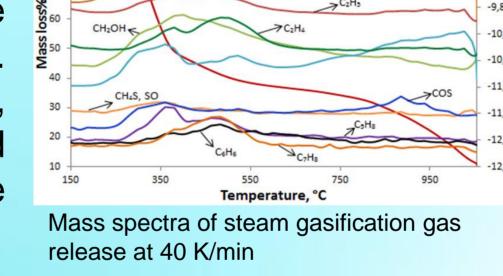
bon	50.69
drogen	6.08
agan	1 7 2

Carl

The calorific value was measured using a Parr 1351 adiabatic bomb calorimeter. The high heating value HHVs is 20 MJ/kg  $\pm$  2.4%.

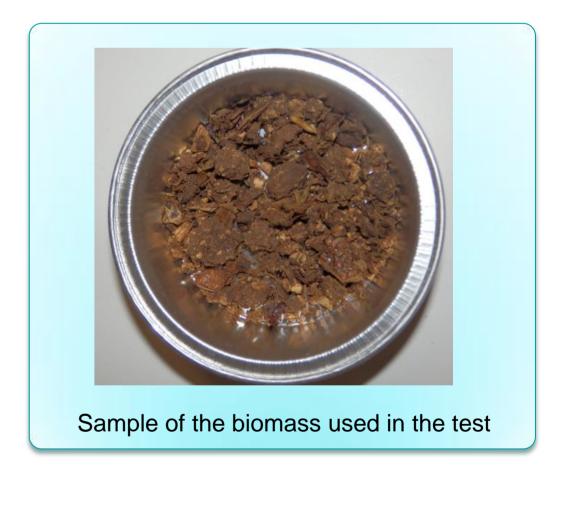
The ultimate and proximate analysis are summarized in Table 1.

Gasification behavior of the sample was conducted in steam atmosphere. During the char gasification process, CO, CO<sub>2</sub> and H<sub>2</sub> gases are released with a small amount of  $CH_4$  (see figure).



Sulphur Oxygen	0 35.14
HHV (MJ/kg)	20.2
Oil content (%)	6

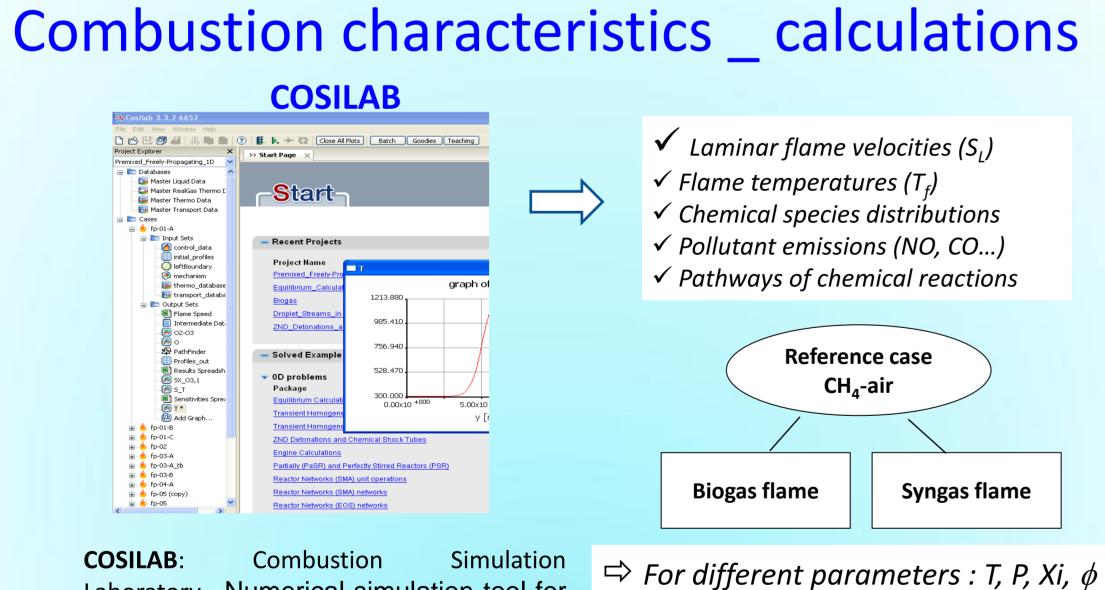
Table 1: Proximate and ultimate analysis for the biomass sample



## Next steps

Tests with different biomass (pellet wood, olive waste, municipal solid waste)

Investigate the operating conditions

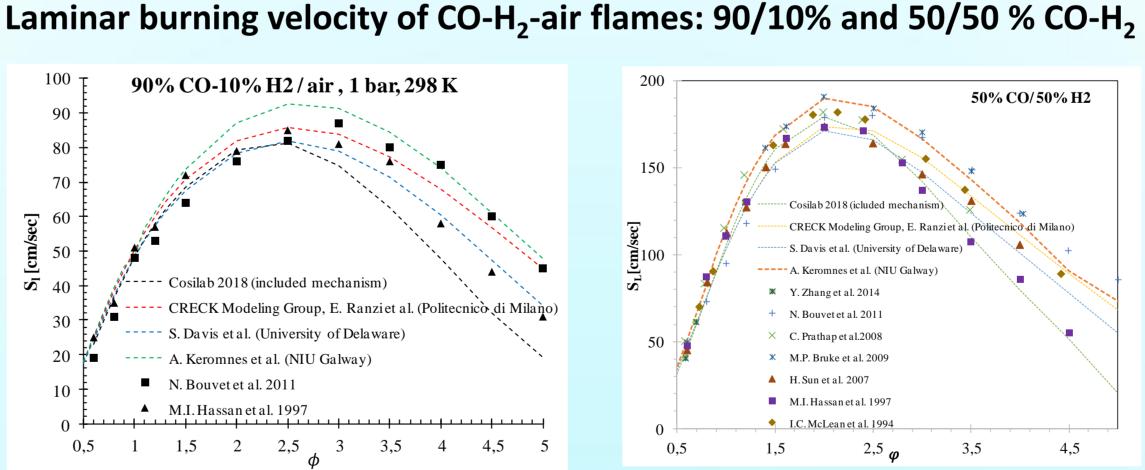


**COSILAB:** Combustion Simulation Laboratory. Numerical simulation tool for laminar combustion problems 0D, 1D and recently 2D. Here, calculations of flame 1D (RUN 1DL)

### **Case of CH**<sup>₄</sup>-air flame

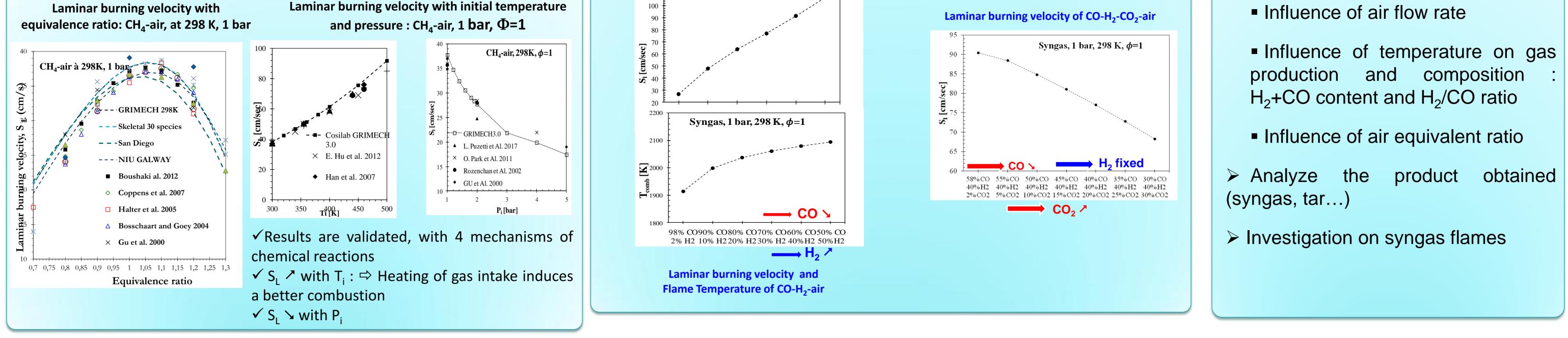
⇒ With different mechanisms of

reactions



Syngas flame calculations

✓ Results are compared and validated with experimental results
✓ With +H<sub>2</sub>: S<sub>L</sub> max at Φ = 2.5 (CH<sub>4</sub>-air: at Φ = 1.05)
✓ + H<sub>2</sub> ⇔ S<sub>L</sub> ≯; S<sub>Lmax</sub>: 190 at 50% of H<sub>2</sub>, 90 at 10%H<sub>2</sub> against 38 cm.s<sup>-1</sup> CH<sub>4</sub>-air
✓ + H<sub>2</sub> : higher reactivity, higher flammability limits, higher velocity, higher T





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Syngas, 1 bar, 298 K, φ=1

110

