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Selective reductive dimerization of CO₂ into

glycolaldehyde

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The selective dimerization of CO₂ into glycolaldehyde is achieved in a one-pot two-step process

via formaldehyde as a key intermediate. The first step concerns the iron-catalyzed selective

reduction of CO₂ into formaldehyde via formation and controlled hydrolysis of a bis(boryl)acetal

compound. The second step concerns the carbene-catalyzed C-C bond formation to afford

glycolaldehyde. Both carbon atoms of glycolaldehyde arise from CO₂ as proven by labelling

experiment with ¹³CO₂. This hybrid organometallic/organic catalytic system employs mild

conditions (1 atm of CO₂, 25 °C to 80 °C in less than 3 h) and low catalytic loadings (1 % and

2.5%, respectively). Glycolaldehyde is obtained in 53% overall yield. The appealing reactivity of

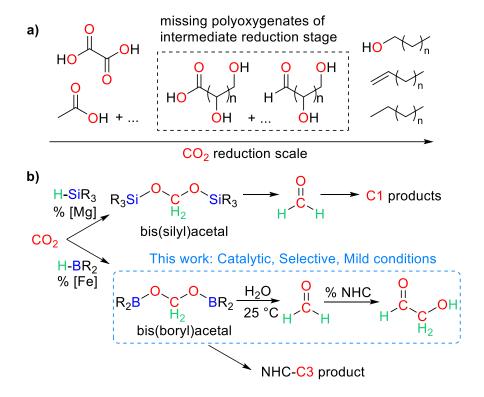
glycolaldehyde is exemplified i) in a dimerization process leading to C₄ aldose compounds and ii)

in a tri-component Petasis-Borono-Mannich reaction generating C-N and C-C bond in one process.

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INTRODUCTION

 CO_2 reductions to $C_{n>1}$ products are much less developed than to C_1 compounds, due to the intrinsic difficulty of combining two individually challenging steps in a single process: CO₂ reduction and C-C bond formation. As a consequence, further developments of CO₂ utilization as C_n source face two main issues: selectivity and limited scope of products. ¹⁻² Besides oxalate, acetate and related products,³ most of the obtained compounds are highly reduced products: aliphatic hydrocarbons, olefins and alcohols (Scheme 1a). In these electroreduction or hydrogenation systems, CO is considered as the key bifurcation point toward C_n products. Because of their high energy density, the synthesized products are of interest as energy carriers. However, if one wants to use CO₂ as a sustainable C_n source, less reduced polyoxygenated compounds would be highly desirable (Scheme 1a), because such compounds, featuring multiple alcohol, ketone and/or aldehydic functions, exhibit appealing molecular complexity leading to versatile reactivity. Their isolation from biomass is currently being explored for their use as new chemical feedstock.⁴ Finding a new access from CO₂, would offer a complementary sustainable alternative to biomass extraction. A thorough study on Cu-catalyzed electroreduction of CO₂ reported the detection of such C₂ and C₃ oxygenated compounds as minor species. ⁵ As indicated in the proposed mechanism and further complemented by an in-depth theoretical investigation, 6 these compounds cannot be accumulated because they are further reduced in situ (Scheme 1a) under the reaction conditions.



Scheme 1. a) C_n products obtained from electroreduction and hydrogenation of CO₂; b) Synthesis and utilization of 4e⁻ reduction products as C1 source from CO₂ hydrosilylation⁷ and as Cn source from CO₂ hydroboration.⁸

We believe that i) new pathways need to be developed for the generation and accumulation of these reactive intermediates, ii) homogeneous thermal transformations of CO₂ into C_n compounds would have a key role to play in this objective⁹ and iii) HCHO could be an alternative bifurcation point toward C_n products. Mild operating conditions should be pursued to favor in situ characterization and control of the reaction. In the field of CO₂ reduction, hydrosilane and hydroborane reductants enabled to use particularly mild conditions and make significant progress in mechanisms understanding as well as in the characterization and functionalization of reactive intermediates.¹⁰ More specifically, it enabled the development of reduction of CO₂ to the formaldehyde level with the selective generation of bis(silyl)¹¹ and bis(boryl)acetal¹² compounds

(scheme 1b). These reactive intermediates were proven particularly versatile for the synthesis of a large scope of different C₁ products.^{8, 11c, 12d, 12f, 13} While these acetal compounds were used as formaldehyde surrogates, it is only in a recent example, that Parkin et al. reported the actual release of formaldehyde from a bis(silyl)acetal compound by adding CsF at 25 °C or heating the solution to 120 °C in DMF.⁷ The in situ generated formaldehyde was then involved in C₁ transformations (Scheme 1b).

In the last 10 years, we developed 4e- reductions of CO₂ with hydroboranes¹⁴ and applied it to C₁ chemistry. We aimed at using this process for the transformation of CO₂ into C_n products. A first example of the synthesis of a C₃ compound was reported from the stoichiometric reaction of an N-Heterocyclic Carbene (NHC) with a bis(boryl)acetal compound. However, the coupling step was not catalytic and the yield (30%) remained modest. Herein, we present the first catalytic system enabling to generate selectively glycolaldehyde from the CO₂ reductive dimerisation in 62% yield from a bis(boryl)acetal compound.

RESULTS AND DISCUSSION

Step 1: Formaldehyde release from bis(boryl)acetal

As reported earlier, bis(boryl)acetal **1** is generated from the selective 4e⁻ reduction of CO₂ with 9-BBN using mild conditions (25°C, 1 atm of CO₂, 45 min.) and 1 mol% of the iron complex Fe(H)₂(dmpe)₂ (Scheme 2).^{12f} The first objective was to find a pathway to generate formaldehyde from bis(boryl)acetal **1** under mild and compatible conditions for the subsequent organo-catalyzed coupling step (vide infra). While partial release of HCHO was mentioned in the literature from a bis(boryl)acetal featuring pinacolboryl moieties, ^{12d, 14b, 16} no system actually reported quantitative generation of HCHO from bis(boryl)acetal compound as in Parkin's example from a related bis(silyl)acetal.⁷ In this context, compound **1** was subjected to 1, 2 and 10 equivalents of water

(Scheme 2). While 1 and 2 equiv. led to partial release of formaldehyde in 24 and 72% yield, respectively (even after 24 h), the use of 10 equiv. afforded formaldehyde in 94% yield within 30 min. Formaldehyde was detected by ¹H NMR analysis both as free formaldehyde (singlet at 9.58 ppm) and as hydrated or oligomeric formaldehyde (broad signals at 4.5-5.5 ppm). Both sets of resonances were measured against an internal standard to calculate the yield in formaldehyde (see Table S2 and Figure S1 in ESI for details).

Scheme 2: Step 1: Release of HCHO from reactivity of 1 with D₂O.

Step 2: Carbene-catalyzed formose reaction of HCHO in the presence of water

We then turned our attention to the formation of short chain carbohydrates from HCHO. The so-called formose reaction corresponds to the oligomerization of formaldehyde into carbohydrate compounds. While this powerful transformation was discovered in the 19th century, ¹⁷ it suffers from numerous side reactions leading to mixtures of up to 30 different products when catalyzed by inorganic bases. ¹⁸ Net improvements in controlling side reactions and chain growth were achieved with the use of NHC-type catalysts, notably with thiazolium and triazolium precursors. ¹⁸⁻¹⁹ In these studies, it is clear that formose outcome is very sensitive to the reaction conditions (solvent, NHC, reaction time), however i) beyond the accepted general mechanism via Breslow intermediate, more defined rationales to explain such variations are lacking ^{19c-e} and ii) THF and H₂O are two solvents that have been sparingly used. ^{19e, 20}

Table 1. Step 2: Formose reaction in DMF, THF and THF/H₂O media with catalyst 2 and 3.^a

| $\begin{array}{c} 2 \text{ or } 3 \\ H \end{array} \begin{array}{c} \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\$ | | | | | | | |
|---|------|-----|-----------------------------------|---------|-----------------------------|---------|------------------|
| Entry | Time | NHC | Solvent | C_2^b | $\mathbb{C}_3^{\mathrm{b}}$ | C_4^b | Total yield % |
| | min | | | % | % | % | |
| 1 | 10 | 2 | DMF | 33 | - | - | 33 |
| 2 | 30 | 2 | DMF | 62 | 34 | - | 96 |
| 3 | 60 | 2 | DMF | 38 | 28 | 34 | 100 |
| 4 | 10 | 2 | THF | 16 | - | - | 16 |
| 5 | 30 | 2 | THF | 16 | - | 72 | 88 |
| 6 | 60 | 2 | THF | 17 | 5 | 78 | 100 |
| 7 | 30 | 2 | THF+H ₂ O ^c | 27 | 18 | 11 | 56 |
| 8 | 30 | 2 | THF+H ₂ O ^d | 31 | - | - | 31 |
| 9 | 30 | 2 | THF+H ₂ O ^e | 17 | - | - | 17 |
| 10 | 30 | 2 | THF+MeOH ^f | 37 | 3 | - | 40 |
| 11 | 30 | 3 | THF | 12 | 67 | 4 | 93 |
| 12 | 30 | 3 | THF+H ₂ O ^c | - | - | - | 0 |

^a Reaction conditions: 0.5 mmol of paraformaldehyde, 0.0025 mmol of carbene, 5 mL of THF (0.1 M), 80 °C. ^b GC yields obtained after derivatization reactions. ^c 10 equiv. of water were added relative to HCHO amount. ^d 20 equiv. of water were added relative to HCHO amount. ^e 40 equiv. of water were added relative to HCHO amount. ^f 1 equiv. of MeOH was added relative to HCHO amount.

In this context, NHC 2 and 3 were selected for initial tests with commercial para-formaldehyde in DMF, THF and THF/H₂O media (Table 1). Results reported by Teles et al. in DMF were first

reproduced with catalyst 2, showing that 30 and 60 min were necessary to reach full conversion. Glycolaldehyde (C₂) was the main product after 30 min while a mixture of C₂-4 carbohydrates was observed after 60 min with 0.5 mol% catalyst loading (Table 1, entries 1-3). 19e Two formose reactions were reported in THF with triazolium precursors, slightly different from 2, leading to the favored formation of glycolaldehyde in 62% and 46% yields. 19e, 19f We thus explored the reaction in THF with catalysts 2 and 3. The reaction was almost complete after 30 min: 88% and 93% total yield with 2 and 3, respectively (Table 1, entries 5 and 11). Interestingly, 3 favored the dihydroxyacetone (C₃ ketose) with a measured 67% yield after 30 min, and 2 favored the C₄ aldoses (erythrose and threose) with combined yields of 72% and 78% after 30 and 60 min, respectively. C₄ ketoses were never detected. To the best of our knowledge, these latter results are the best yields and selectivity reported for C₄ aldoses. Teles et al. indeed reported two reactions in DMF in which the C₄ carbohydrates were the major products with yields of 50% and 16% with triazolium and imidazolium precursors as catalyst, respectively. 19e, 19f We then probed the impact of the addition of H₂O which was reported detrimental for the reaction yield and the selectivity in DMF/H₂O thiamine-based catalysis.²⁰ In accordance with these data, we observed a general negative impact of H₂O on the yield. However, while the addition of 10 equiv. of water completely shut down any conversion with catalyst 3 (Table 1, entry 12), we were pleased to observe a 56% total yield of C₂₋₄ aldose products with catalyst 2 after 30 min in the same conditions. The addition of 20 and 40 equiv. of water or 1 equiv. of methanol afforded lower total yields (Table 1, entries 8-10). With these positive results from HCHO in presence of water in hands, we then decided to explore this transformation from CO₂.

Synthesis of glycolaldehyde from CO₂

We combined the two reactions developed above in a one-pot system. The conditions deduced from these independent studies are as follow: bis(boryl)acetal 1 generated *in situ* in THF was hydrolyzed with 10 equiv. of water at 25°C in 1 h. 0.5% of NHC 2 was then added to catalyze the formose reaction at 80 °C in 30 min (Scheme 3). To our delight, glycolaldehyde was generated in 37% yield under these standard conditions. The yield is the average yield of 4 runs with a measured maximum deviation (Δmax) of 7%. C3 and C4 carbohydrates were detected in 0.4 and 0.6% yield, respectively. The reaction was thus particularly selective since no other carbohydrate was detected, although the yield remained modest. The reaction took place only in the presence of carbene catalyst 2 or its triazolium precursor 6. Their absence or the use of carbenes 3-5 did not afford any detectable C2, C3 or C4 products.²¹ Future work will be dedicated to understand the specificity of carbene 2 in protic media, keeping in mind recent questioning about organo-catalyzed umpolung reactions.²²

Scheme 3. One-pot system under initial standard conditions with catalyst **2-6**.

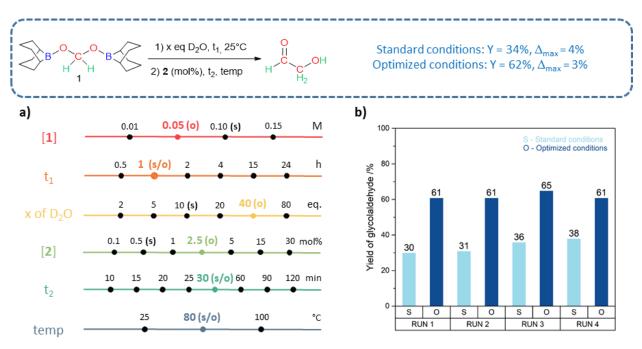
In order to improve glycolaldehyde yield, reaction conditions were optimized using catalyst 2. The optimization was conducted in two stages: i) variation of one parameter at a time (Scheme 4a), and ii) combination of optimal conditions and careful comparison of the obtained yields between standard (s) and optimized (o) conditions (Scheme 4b).

First stage (Scheme 4a): 6 parameters were optimized: the initial concentration of compound 1 in THF, the time t_1 of the hydrolysis, the number of equivalents of D_2O added for hydrolysis, the

catalyst loading in 2, the time (t_2) and temperature (temp) of formose reaction. For each parameter, standard (s) and determined optimal (o) condition are indicated among the different conditions tested (in black color). Details on observed trends for each parameter are described hereafter in the order indicated in Scheme 4a while detailed yields are given in ESI. A significant yield improvement of about 10% was observed when the initial concentration of 1 in THF was divided by half ([1] = 0.05 M). This observed trend is consistent with the common observation of lower chain length selectivity with lower concentration of formaldehyde in formose reaction. 19b, 19c, 19e The hydrolysis time of the acetal $\mathbf{1}$ (t_1) had a negligible impact on the yield when it was varied from 30 min to 24 h. It indicates that compound 1 is readily hydrolyzed in these conditions. However, we observed improved yields in glycolaldehyde when 40 equiv. of water were used instead of 2, 5, 10, 20 or 80. Since the hydrolysis of the acetal 1 (t₁) had no impact on the yield, we believe that the increased yield with 40 equiv. of H₂O was not due to a better hydrolysis process but rather to a dilution factor. Adding 40 equiv. of H₂O indeed led to a decrease of the concentration by about half which was shown to be beneficial above. We confirmed this assumption by varying the amount of equiv. of H_2O added while maintaining [1]. In this case, yield improvement was attenuated, but still in favor of the addition of 40 equiv. of H_2O . Although the observed +4% increase is marginal, we kept 40 equiv. of H₂O as an optimized condition, while maintaining concentration [1] = 0.05 M. When catalyst loading [2] was varied from 0.1 to 30 mol%, a narrow variation of 10% was observed between the highest and the lowest yields. 2.5 mol% catalyst loading was found optimal. It first indicates that the catalyst is very active under these conditions. It also shows that if H₂O has a detrimental impact, its excess compared to the amount of catalyst (3 to 4 orders of magnitude) is too large to be compensated by a 10-fold increase of the catalyst loading. Finally, the standard conditions for formose reaction time and temperature

 $(t_2 = 30 \text{ min, temp} = 80 \,^{\circ}\text{C})$ are also the optimal conditions, in accordance with the literature. $t_2 = 25 \,\text{or } 30 \,\text{min}$ enabled to record the best yields, while shorter or longer reaction time had a negative impact. We confirmed that the reaction took place at $100 \,^{\circ}\text{C}$ but with a slightly lower yield, while expectedly, it did not proceed at room temperature.

Second stage (Scheme 4b): The presented general optimization methodology relies on a classical one-factor-at-a-time method. Although this is a classical method, combinations of effect are then not considered. In order to properly assess the impact of the optimized conditions, the given yields are the average of 4 runs. In each of them, the solution containing the *in situ* generated 1, was split into two containers which were then subjected in parallel to the standard conditions (s) for one container and to the optimized conditions (o) for the other one. With these experiments, a 34% yield (Δ max = 4%) was measured under the standard conditions, in the same range as that initially obtained (i.e. 37%, Δ max = 7%). Gratifyingly, the yield obtained under the optimized conditions is calculated to be 62% with a maximum deviation of 3%. The optimization study thus led to almost doubling the product yield. Considering the system including the CO₂ reduction step, we developed herein a hybrid one-pot organometallic/organic system transforming CO₂ into glycolaldehyde in an overall 53% yield based on hydroborane used, under mild conditions in less than 3h.



Scheme 4. Optimization for the synthesis of glycolaldehyde: **a)** one-factor-at-a-time study over 6 parameters, (s) indicates the standard condition, (o) indicates the optimal condition; **b)** comparison of yields between standard and optimized conditions.

Synthesis of ¹³C-labeled glycolaldehyde

As a mean to prove that glycolaldehyde is indeed formed from the reductive coupling of two molecules of CO₂ and to generate valuable 13 C-labeled glycolaldehyde, we conducted the reaction using 13 CO₂. The multiple forms adopted by glycolaldehyde in solution (monomeric, symmetrical and unsymmetrical oligomeric and hydrated forms) complexify its NMR analysis (see ESI). $^{5, 24}$ We present herein the characterization of the simple monomeric aldehydic form in the crude THF- d_8 /D₂O mixture. In 13 C 1 H 1 NMR analysis, this species is characterized at δ 203.3 (d, 1 J_{C-C} = 41.1 Hz) and 69.7 (d, 1 J_{C-C} = 41.1 Hz). The two carbon centers correlate with the aldehydic and methylenic protons characterized at δ 9.60 (dd, 1H, 1 J_{H-C} = 173.2 Hz, 3 J_{H-C} = 26.9 Hz) and 4.01 (dd, 2H, 1 J_{H-C} = 140.9 Hz, 3 J_{H-C} = 4.0 Hz), respectively. Figure 1 discloses the stacking of 1 H NMR analysis as well as the selective and broad band 1 H 13 C 13 S spectra of the selected areas. It enables

to visualize that each proton correlates with both carbon nuclei of the molecule with observed 1J and 3J scalar couplings, the selective 13 C decoupling further highlighting these correlations. Importantly, no 12 C-labeled glycolaldehyde was detected in the crude mixture by 1 H NMR, indicating that every molecule of glycolaldehyde quantified by GC analyses arises from CO₂ reductive coupling.

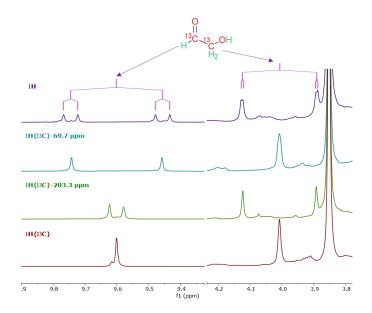


Figure 1. Selected areas of ¹H and ¹H{¹³C} NMR analyses of the crude mixture obtained from the developed ¹³CO₂ reductive coupling process.

In situ transformation of glycolaldehyde

Carbohydrates and glycolaldehyde in this instance are attractive species because of their reactive nature. 4e, 25 In order to exemplify this feature, glycolaldehyde *in situ* generated from CO₂ was engaged in two reactions depicted in Scheme 5a) and b). The tri-component Petasis-Borono-Mannich reaction was conducted in water to afford compound 7, isolated in 37% yield in aqueous solution. The dimerization of glycolaldehyde was then conducted with Zn(L-Pro)₂ as catalyst. Increasing the reaction temperature to 50 °C enabled to generate erythrose (8, 40%) and threose (9, 24%) for a total GC yield of 64 % of C₄ aldoses.

a)
$$\frac{1}{1}$$
 $\frac{1}{1}$ \frac

Scheme 5. Reactivity of *in situ* generated glycolaldehyde: a) Synthesis of **7** by Petasis Borono-Mannich reaction; b) Synthesis of C₄ carbohydrates.

CONCLUSIONS

In the present publication, the selective dimerization of CO₂ into glycolaldehyde is reported for the first time. To achieve such transformation, particularly mild conditions (1 atm of CO₂, 25 °C to 80 °C in < 3 h) and low catalytic loadings (1% and 2.5%, respectively) were employed with a hybrid organometallic/organic catalytic process. Key aspects of the presented work rely on the quantitative release of formaldehyde from the hydrolysis of a bis(boryl)acetal compound compatible with the C-C coupling step. Intensive optimization led to the generation of glycolaldehyde in 62% yield from compound 1 and in 53% overall yield from CO₂ based on the amount of hydroborane engaged. The ultimate proof of CO₂ being the sole source of carbon was obtained with labelling experiment using ¹³CO₂. This homogeneous thermal CO₂ process shows that i) bis(boryl)acetal obtained from mild CO2 reduction enables a selective and mild access to formaldehyde, ii) acetal compounds can be involved in the generation of C_n compounds and iii) carbohydrates such as glycolaldehyde are valuable reactive feedstocks to be synthesized from CO₂. ^{4e, 25} On a broader perspective, the presented strategy highlights that formaldehyde offers an appealing new synthetic access to C_n products of intermediate reduction stage. Although, in the present case, the boron-based reductant system is not sustainable and the formose control only

applies to the smallest carbohydrate, we believe that the strategy presented herein could stimulate different fields of CO₂ reduction.

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Author Contributions

The manuscript was written through contributions of all authors. All authors have given approval to the final version of the manuscript.

ASSOCIATED CONTENT

Supporting Information.

The supporting information are available free of charge. It includes experimental details, compounds synthesis and characterization and description of the optimization procedure.

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