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► **To cite this version:**

Z. Mohamad, F. Fardoun, F. Meftah. A review on energy piles design, evaluation, and optimization. Journal of Cleaner Production, 2021, 292, pp.125802. 10.1016/j.jclepro.2021.125802 . hal-03159204

**HAL Id: hal-03159204**

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Submitted on 8 Mar 2021

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# A Review on Energy Piles Design, Evaluation, and Optimization

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## Abstract

Integrating heat exchanger pipes with structural foundations in one system has created a new renewable solution for buildings' thermal loads. However, the interaction between thermal and geotechnical loads makes their design more complex and challenging. This review-study represents the current state of knowledge about the thermal and thermo-mechanical behaviors of energy piles. It also investigates the key parameters that affect their design concerning the piles' dimensions, the arrangement of pipes, concrete admixture, and fluid characteristics. It is found that the thermal efficiency improves significantly by increasing the number of pipes inside the piles and by adding thermally conductive materials to the concrete within acceptable limits. Besides, this paper reviews most of the studies conducted on optimizing vertical ground heat exchangers coupled with heat pumps. Objective functions, decision variables, design constraints, and optimization methods are specified and listed. It is concluded that a multi-objective optimization is highly recommended to enhance the dual performance of an energy pile system coupled with a heat pump using the 4E evaluation criteria (energy, exergy, economy, and environment) while ensuring the safety of the foundation under thermal cyclic loads.

**Keywords:** energy piles, thermo-mechanical behavior, design parameters, 4E-G evaluation criteria, optimization.

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## Table of Abbreviation

Nomenclature		Symbol	
BHE	Borehole heat exchanger	$s_p$	Pipes spacing
CFD	Computational fluid dynamics	$\lambda_g$	Thermal conductivity of grouting material
COP	Coefficient of performance	$\lambda_p$	Thermal conductivity of pipe material
DOF	Degree of freedom	$D_b$	Borehole diameter
EGN	Entropy generation number	$N_b$	Number of boreholes
EP	Energy pile	$N_p$	Number of pipes
FDM	Finite difference model	$R_e$	Reynolds number
FEM	Finite element model	$T_{in}$	Inlet fluid temperature
FLSM	Finite line source model	$T_{out}$	The outlet fluid temperature
FRSM	Finite ring source model	$m_f$	Mass flow rate
FSSM	Finite spiral source model	$r_b$	Borehole radius
FVM	Finite volume model	$\lambda_s$	Thermal conductivity of the soil
GA	Genetic algorithm	$r_p$	Pipe radius
GHE	Ground heat exchanger	$s_b$	Borehole spacing
GSHP	Ground source heat pump system	$s_p$	Pipes spacing
HJ	Hooke-Jeeves pattern search algorithm	$\Delta T$	Temperature change
HTF	Heat transfer fluid	$E$	Youngs modulus
ICSM	Infinite cylinder source model	$\alpha$	Thermal expansion coefficient
ILSM	Infinite line source model	$\sigma_{th}$	Thermal stress
IRSM	Infinite ring source model	$\varepsilon_{th}$	Thermal strain
ISSM	Infinite spiral source model	$\omega_z$	Vertical displacement
LCC	Life cycle cost		
MINLP	Mixed-integer Non-linear programming		
NM	The Nelder-Mead method		
NPV	Net present value		
PCM	Phase change material		
SCSM	Composite cylinder source model		
TAC	Total annual cost		

## 1. Introduction

Energy consumption of buildings has become a relevant international issue, and various design strategies have been developed to enhance energy saving in many countries. Today, Buildings' responsibility for approximately 40% of total energy consumption and over 30% of greenhouse gas emissions [1] has shifted global interest toward the so-called "Nearly zero energy buildings" (NZEB). The design of an NZEB has the purpose of constructing buildings with less energy consumption and low carbon emission. The development of energy geo-structures contributes to this goal as applying shallow geothermal energy in geo-structures for space cooling and heating of buildings. This environmentally friendly technology can be applied to all types of soil-embedded structures such as the diaphragm walls, tunnels, shallow foundations, and piles [2]. In the past years, an increasing number of energy geostructure projects have been implemented in many countries where they have achieved a cumulative share of carbon dioxide savings worldwide (Figure 1). The Laizer tunnel in Vienna (Austria), the Keble College in Oxford (UK), the Dock Midfield terminal at Zurich airport in Switzerland, and the Wuxi Guolian Tower in China are some applications for various types of energy geo-structures in the

world [2,3]. Among all these types, the energy pile remains the most common application for the ground heat exchange process. It takes advantage of the relative stability of underground temperature below a depth of 15m to 50m to extract or reject heat from/to the ground. The heat transfer is carried out in an energy pile through ground heat exchanger (GHE) pipes installed along their reinforcement cage, where the heat transfer fluid (HTF) circulates and exchanges heat with the surrounding. Despite the rapid spread of this technology, especially in the UK and Austria, energy piles' installation still faces considerable challenges due to the interaction between thermal and geotechnical design [4]. Many studies have been conducted or are ongoing to examine the performance of energy piles. Most of them are based on energy performance, but many recent studies have also been published to understand their thermo-mechanical behavior through in situ experiments, laboratory tests, and numerical analyses. Simultaneously, some authors have reviewed research studies in this field [5–15]. However, they do not address the optimization aspects of energy piles under thermo-mechanical interactions. This paper presents a comprehensive review of all energy piles' features: evaluation, design, and optimization. It interprets the complex performance of energy piles, expands knowledge on their evaluation criteria and design parameters, and provides design recommendations. It also attempts to develop an approach to optimize energy piles' design, considering thermal, economic, environmental, and mechanical perspectives.

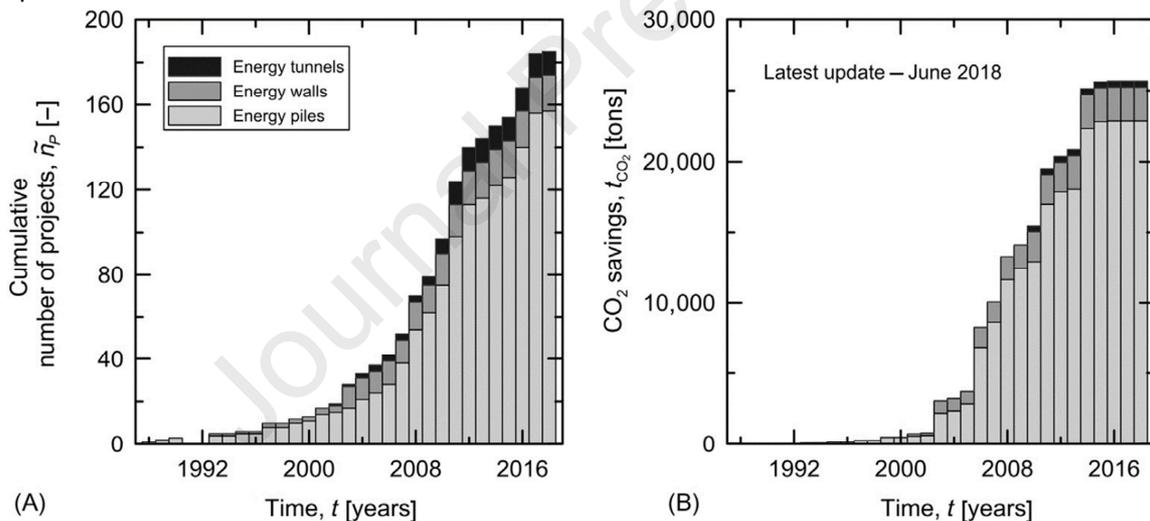


Figure 1. Cumulative number of (A) energy geostructure projects worldwide and (B) carbon dioxide savings worldwide [16].

## 2. Thermal behavior of energy piles

Understanding the heat transfer across energy piles is the first step in designing these systems. The thermal process goes in an energy pile, as in a borehole heat exchanger, in different stages: heat transfer through the ground, conduction through pile concrete and heat exchanger pipes, and convection in the fluid and at the interface with the inner surface of the pipes (Figure 2). Analytical and numerical studies have been conducted to analyze these systems' thermal performance (Table 1).

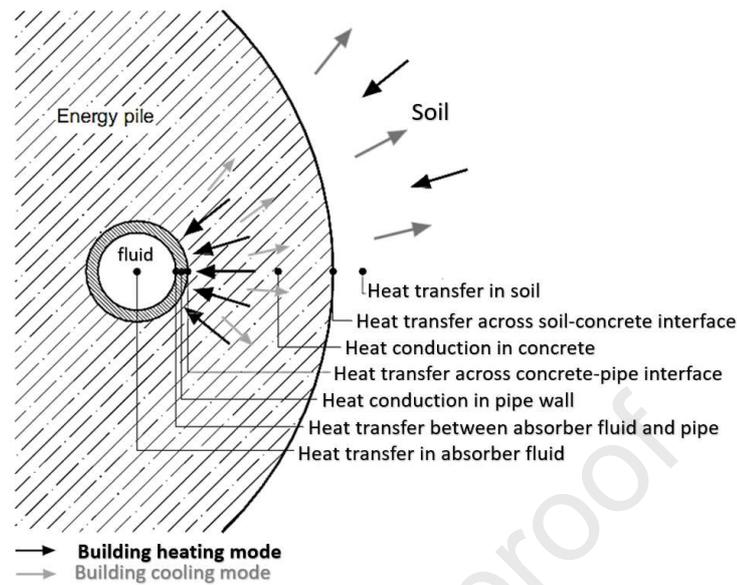


Figure 2. Heat transfer stages in an energy pile

Table 1. Recent studies on the thermal behavior of energy piles.

Reference	Pipe configuration	Pile size	Method and/or software	Numerical	Analytical	Experimental	Results
[17] Park et al.	5 U-tubes	D=1.5m	Engineering chart	✓	✓		The chart presents a good estimation of the rate of heat transfer compared to numerical analysis.
[18] Lei et al.	Spiral coil	—	hybrid analytical model		✓		Results with homogeneity assumption present acceptable errors.
[19] Cui and Zhu	U-tube	D=0.3m L=10m	3D FVM	✓			Reduction in soil temperature after a year of operation. Rapid soil temperature recovery with reduced volumetric heat capacity and high thermal conductivity of the soil.
[20] Rui et al.	U-tube	D=2.5m L=28m	1D FEM	✓			Steady-state is attained after 12–13 years of operation. 50% reduction in the energy consumption for GSHP after 30 years of service.
[21] Cui and Zhu	U-tube	D=0.3m L=10m	3D FVM CFD analysis	✓			The values of the CFD model deviate by 12% from the experimental results. The intermittent operation leads to higher COP values than continuous operations.
[22] Ghasemi-Fare and Basu	U-tube	D=110mm L=1.22m	Thermal loading tests FDM	✓		✓	Results show a higher pile-soil temperature gradient in saturated soil. The thermal conductivity at the wall of the pile= 50% and 63% of the thermal conductivity of soil measured in dry and saturated conditions.
[23] Dehghan B.	Spiral Coil	D=0.45m L=60m	COMSOL	✓		✓	Spiral ground heat exchangers have high efficiency and low costs. The recommended distance between piles is at least 6m.

[24] Li et al.	U-tube, double U- tube, W-tube	—	COMSOL	✓	✓	Concrete with graphite content of 25% results in a twice increase in thermal conductivity than cement concrete. Low heat transfer enhancement with graphite content of less than 10%.
[25] Cui et al.	—	—	the infrared thermal analysis system		✓	Increase in the thermal conductivity of concrete with alkali-activated slag (AAS) to cement paste. Reduction in compressive strength with increased graphite-modified PCM content in cement composite.
[26] Han and Yu	U-tube, W-tube, Spiral coil	D=1.2m L=30m	FEM	✓		Increase in energy extraction by integrating PCM into the concrete. High-cost materials.
[27] Huang et al.	cone helix- tube	D=1.2m L=1.5m	G-function, Laboratory test		✓	Higher heat transfer of energy pile with cone helix pipes compared to spiral coils. Better performance by setting a more significant cone angle.
[28] Zhang et al.	spiral coil	D=0.8m L=26m	the spiral line heat source model (SLSM)		✓	SLSM provides accurate results for the analysis of energy pile behavior with spiral pipes.
[29] Zhang et al.	spiral coil	—	2D advection G-function		✓	The study addresses the effect of groundwater flows in 2D directions on heat transfer.
[30] Lu et al.	U-tube, double U- tubes	L=30m, 60m	FLUENT 6.3	✓		35.4% Increase in Heat transfer per unit length with double U-tube compared to single U-tube. 33.6% Increase in Heat transfer per unit length with intermittent operation compared to continuous operations.
[31] Huang et al.	w-tube	D=1.5m L=60m	TRT test COMSOL	✓	✓	Twice heat exchange amount in the cooling operation compared to the heating operation. The tighter pipe layout reduces thermal performance.
[32] Zarrella et al.	Double U- tubes	D=0.62m L=20m	ILSM CaRM program	✓	✓	Underestimation of the pile length by 20% using ILSM compared to numerical analysis. 10% difference in SCOP between ILSM and the numerical model after ten years of operation.
[33] Zhang and Chen	3 U-tubes	D=0.6m L=28m	FEM CFD software	✓		The rate of heat transfer stabilizes at 60W/m after 20 days of operation. Results show a decrease in soil temperature by 0.03°C after one year of operation.
[34] Dehghan et al.	spiral coils	D=0.4m L=30m	COMSOL	✓		The recommended distance between piles is 7m. 100% change in pitch size and pipe diameter results in a 10% change in heat efficiency.

### 2.1. Analytical methods

Analytical models often use methods designed for borehole heat exchangers (BHE), while heat transfer within energy piles presents critical differences compared to BHE, especially for large diameter piles (Table 2). Many studies have examined the heat transfer within ground heat exchangers under steady-flux conditions. This process can be easily analyzed by introducing the concept of thermal resistance, similar to the concept of electrical resistance. Loveridge et al. [35] presented the principal methods developed on two-dimensional and three-dimensional scales to calculate the thermal resistance of GHE

pipes in the steady-state. However, the process of heat transfer within an energy pile is transient. So, the application of a time-independent approach can lead to an over-prediction of temperature changes underground and uncertainty regarding the system's thermal design [35]. Simultaneously, models derived from the G-function theory, such as line heat source models (LSM) and cylindrical heat source models (CSM), have been established to calculate the temperature change of a vertical heat source surrounded by a uniform ground [32,36,37] (Figure 3). These models have been widely used in practice to treat the behavior of boreholes and energy piles for their simplicity and low computational time. However, the simplifications assumed by these models can make errors in the analysis of energy piles. Wang et al. [38] investigated the limitation of the homogeneous analytical models for energy piles numerically. The results showed that the assumption of a homogenous domain could lead to an incorrect estimate of heat transfer, particularly in short-term operation, and for large diameter piles [39].

Furthermore, the models do not address the effect of the backfill material's thermal mass, while this aspect can be critical for energy piles of sizeable concrete volume. According to Park et al. [17], the concrete's thermal capacity has a dominant effect on the thermal performance of energy piles in short-term periods, even more than thermal conductivity. Therefore, thermal storage of heat within the pile concrete should be accurately specified, and its incorporation into analytical analysis and design software of energy pile needs to be considered. Man et al. enhanced the cylindrical source model to consider this aspect. The model showed a closer realistic analysis of pile heat exchangers compared to the classic models, especially at the long-term response, where the temperature curve tends to a steady-state distribution.

Nevertheless, it ignores the GHE geometry and applies uniform material properties for both concrete and ground. Some studies published analytical analysis for spiral heat exchangers. Cui et al. [40] developed the ring-coil heat source model (RSM) to analyze the transient thermal conduction around energy piles, including helical coils. The alternative model, based on the cylindrical heat source, simplifies the spiral tubes into separate rings but neglects the effect of the pile pitch. This assumption allows the temperature in each ring to tend to infinity, resulting in an unrealistic response to spiral pipes. Man et al. [37] overcome the gap of the ring model. They assumed the heat exchanger as a spiral line, where each pitch section releases heat. This spiral model with finite length can be considered a desirable tool for thermal analysis of spiral heat exchangers, as the model considers the radial dimension of the heat source and the heat capacity of the pile. However, the model still needs experimental and numerical validation.

Table 2.Aspects of differences between Boreholes and Energy piles

<b>Boreholes</b>	<b>Energy piles</b>
Aspect ratio from 500 to 2000	Aspect ratio from 15 to 50
Negligible thermal mass	large thermal mass
Symmetric geometry in the ground	geometry Constrained by foundation piles location
Neglected thermal axial effects	Significant axial effects at short-term
Thermal steady-state analysis	Thermal transient state analysis

Ignored short-term analysis

Significant short-term analysis

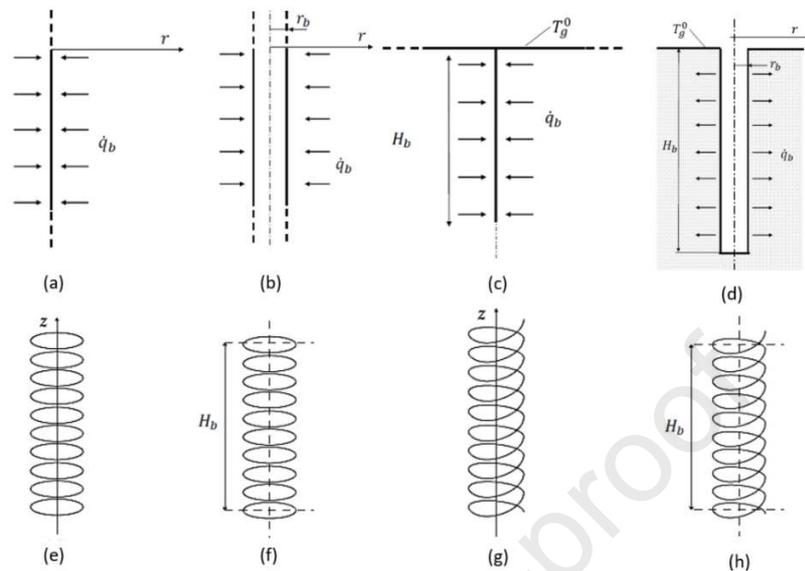


Figure 3. Schematic representation of the main analytical models for vertical GHE analysis: (a) ILSM, (b) ICSM, (c) FLSM, (d) SCSM, (e) IRSM, (f) FRSM, (g) ISSM, (h) FSSM

## 2.2. Numerical methods

Many numerical models have been developed in the past years to analyze energy piles' thermal performance, based mostly on finite element and finite volume methods [19,23,24,26,34]. Several reviews [5,6,41,42] showed that numerical models are precise and realistic to simulate energy piles. Their advantages come from defining each system component and describing various boundary conditions and configuration states. They can also simulate the fluid flow along the pipe, considering the temperature change with the pile depth. As well, they can introduce the groundwater movement in the soil, the various soil layers, and the thermal capacities of different pile elements. Some studies proposed 3D numerical models to detect the heat transfer performance of energy piles [31,43,44]. Cui and Zhu [21] found a difference of only 12% in pile temperature between the detailed numerical model and the experimental results. However, most numerical studies adopted simplifications to reduce the high computational time desired for the discretization of the complex numerical models [20,22,30,33,45]. Mixed 1D-3D approaches have also been developed to reduce the complexity of full 3D models [46,47]. They simulate the heat transfer in the piles and the surrounding based on 3D approaches, while they simulate the heat and fluid flow inside the pipes based on 1D approaches. Caulk et al. [47] checked the 1D-3D model and found good agreement with experimental data. Besides, Park et al. [17] proposed an engineering chart to assess the heat transfer in energy piles, based on the concept of thermal resistance and design factors, resulting from parametric studies. The authors verified the accuracy of the chart values by performing CFD models for energy piles with multiple U-tube and coil-tube configurations. The results revealed a maximum error of 9% compared to CFD simulations. However, the chart admits some limitations. It is recommended to address a larger number of design parameters to assess the overall thermal behavior of energy piles.

### 3. Thermo-mechanical behavior of energy piles

#### 3.1. State-of-the-art

Temperature changes associated with geothermal processes pose additional challenges to structural and geotechnical engineers. The application of heating/cooling cycles causes thermal expansion and contractions of piles, affects their bearing capacity, and produces stresses and strains in their section [48,49]. The review of experimental tests executed full and small scales energy piles and centrifuge models leads to develop a general understanding of the mechanical behavior of pile foundations under thermal loading. Energy piles under thermal loading are subject to thermal stresses related to the intensity of the temperature changes, to the pile-bearing behavior, and the end-restraint conditions [50] [3] (Figure 4). Heating energy piles, during the cooling season, increases the compressive stresses in the piles between 40 KPa/°C and 360 KPa/°C while cooling, during the heating season, induces a reduction in compressive stresses of approximately  $-15$  KPa/°C to  $-180$  KPa/°C [16]. Fang et al. [51] observed a double increase in total axial stresses under thermo-mechanical loading compared to mechanical loading only. Di Donna and Laloui [52] found that the compressive stresses generated in energy piles during heating are lower than the limit state. However, during the cooling phase, they decrease, leading to a zone of tensile stresses at the pile tip. This can be attributed to the high-restrained pile subjected to significant cooling loads. Besides, thermal loads can also mobilize the resistance of the shaft in both the upper-half and lower-half of energy piles, causing variations in their bearing capacity. The heating loads can increase the bearing capacity of energy piles ranging from 13% to 16.4% [53] [54] [51], but the cooling loads decrease it by 8.7% according to Wang et al. [54]. Thermally-induced strains along energy piles are often reversible, developed mainly during the first thermal cycle, and accumulated with time [55,56]. However, the increment of these strain accumulations decreases with the increase in thermal cycles, where at the end of cycles, these strains are within the elastic range [57]. Kalantidou et al. [58] studied the behavior of an axially loaded pile during cooling-heating cycles. They found that the displacement-temperature curve is reversible and varies similarly to the thermal expansion curve of the pile. However, when the applied mechanical loads exceed 40% of the ultimate resistance, the irreversible settlement appears at the pile's toe in sandy soil. Other studies have also revealed similar results [3,59]. Therefore, the effect of the mechanical loading rate on the thermally-induced stresses is critical and should be strongly accounted for when designing energy piles, especially for values greater than 40%.

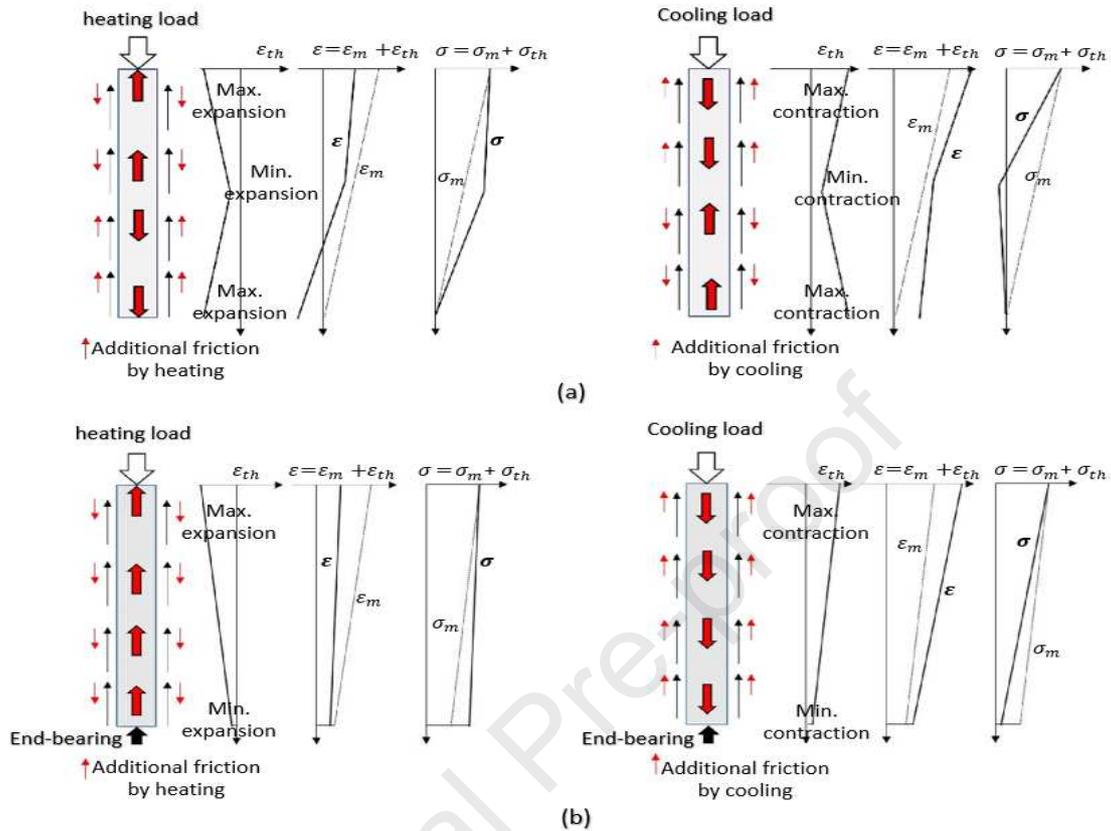


Figure 4. Thermo-mechanical performance of (a) friction pile and (b) end-bearing pile [60].

### 3.2. Analysis approach

Full experiments reflect the actual behavior of energy piles subjected to thermal and mechanical loads [61]. However, when the in situ tests are not available, numerical studies can represent an alternative approach tool. These studies include two approaches of modeling: the first method uses load-transfer methods in a simplified one-dimensional model, where the second method uses the finite element method or the finite difference method in a complex three-dimensional model (Table 3).

#### 3.2.1. Load-transfer method

The load-transfer ( $t$ - $z$ ) methods are used to estimate the axial behavior of energy piles. They discretize the pile into rigid elements connected by springs. Bourne-Webb et al. [5] summarized and analyzed the studies carried out in the literature on the load-transfer methods. Their advantages come from their simplicity to use in the practical design application. However, the assumptions used in these methods can lead to necessary limitations on the accurate description of the real energy pile response. These models assume minor temperature changes in the ground, which can be critical for long-time analysis.

Additionally, they do not consider the effects of thermal loading on the mechanical properties of soils. It can be an acceptable approximation for granular and stiff ground, but it is not applicable in clayey soils, where thermal consolidation can occur due to heating loads. The thermo-mechanical study of Civelek [62] on silty clay revealed this issue and confirmed that clayey soils show a thermo-elastic response in

case of over-consolidation, where thermo-plastic response appears for the normally consolidated condition. Sutman et al. [63] compared three load-transfer approaches and found that they yield different results, although the same resistance, soil characteristics, and pile properties are assumed. The analysis of the (t-z) methods also showed a reduction in thermally-induced displacement compared to the actual behavior of the structure.

### 3.2.2. Numerical method

A full numerical thermo-hydro-mechanical model that considers all design aspects such as the mechanical boundary conditions, the behavior of each system element, the groundwater conditions, and material parameters is essential. However, the high computational time required for such analysis leads many authors to take simplifications regarding element modeling and boundary conditions [56,64–68]. A comprehensive review of Bourne-Webb et al. [14] highlighted a shortcoming of some simplifications that can cause a false prediction of pile restraint and thus introducing errors in the calculation of internal stresses and pile displacements. They noted that assuming steady-state and ignoring hydraulic coupling would result in more significant pile displacement and fewer stress changes in the pile response. Gawecka et al. [69] highlighted this effect and showed how these assumptions increase the displacement of the pile head and reduce the change of axial stresses over time. Therefore, further validation is required regarding the assumptions used in numerical models to assess their accuracy to detect the thermo-mechanical response of energy piles.

Table 3. Recent studies on the thermo-mechanical behavior of energy piles.

Reference	Temperature range	Soil type	Pile size	Method and/or software	Numerical	Analytical	Experimental	Results
[63] Sutman et al.	$\Delta T = 35^\circ\text{C}$	Clay	D=0.23m L=15.24m	load-transfer method CMOSOL	✓	✓		The load-transfer method miscalculates the thermally-induced displacement in the energy pile.
[64] Saggu	$\Delta T = 21^\circ\text{C}, 35^\circ\text{C}$	Sand	D= 0.5m, 1m L= 15m, 20m	FEM Abaqus, CASM	✓			The pile length and the soil density have significant effects on the pile behavior under thermal loading.
[61] Faizal et al.	T= $5^\circ\text{C}$ - $55^\circ\text{C}$	Sand	D= 0.6m L= 16.1m	Field test			✓	Thermal stresses in the radial direction are negligible compared to those in the axial direction. Ratcheting response appears during initial thermal cycles.
[54] Wang et al.	$\Delta T = 20^\circ\text{C}, 40^\circ\text{C}$	Sand, silty clay	D= 1.06m L= 25.8m	Field test FEM Abaqus	✓		✓	The bearing capacity decreases by 8.7% during cooling and increases by 13.2% during heating.
[70] Rotta Loria and Laloui	$\Delta T = 5^\circ\text{C} - 20^\circ\text{C}$	Multiple layers	D= 0.9m L= 28m	Field test FEM 3D CMOSOL	✓		✓	Increasing the number of activated energy piles increases the thermal strains and decreases the thermal stresses in the foundation.
[71] Ouyang et al.	T= $8^\circ\text{C} - 19^\circ\text{C}$	clay	D= 0.3m L= 25m	load-transfer method TRT		✓	✓	the experimental test showed thermally-induced cracks.
[72] Wu et al.	T= $5^\circ\text{C} - 45^\circ\text{C}$	NC Saturated clay	D= 23mm L= 550mm	Laboratory test			✓	The presence of the pile group and the pile cap reduces the irreversible pile head displacement.
[51] Fang et al.	T= $15^\circ\text{C} - 60^\circ\text{C}$	sandy clay	D= 0.6m L= 16.1m	Centrifuge test			✓	The bearing capacity of energy piles increases by 16.4% in the heating mode

								for $\Delta T = +29$ °C and by 30% for $\Delta T = +41$ °C.
[56] Bao et al.	T= 28°C - 50°C	Saturated Clay	D= 0.2m L= 1.25m, 0.95m	Laboratory Test 2D FE-FD	✓	✓		the pile settlement reduces during the pure heating cycle. Unrecoverable plastic deformation appears during the cooling cycle.
[53] Huang et al.	T= 5°C - 50°C	Saturated Sand	D= 50mm L= 1m	Laboratory Test	✓	✓		Plastic displacement appears after one heating cycle.
[66] Rammal et al.	T= 2°C - 26°C	Saturated Sand	D= 0.41m L= 12m	FDM FLAC3D	✓			Study the heating and the cooling cycles, independently, underestimates the pile displacement.
[68] Adinolfi et al.	T= 10°C - 28°C	Clay	D= 0.3m, 0.4m L= 23m, 11.4m	2D FEM COMSOL	✓			Ignoring daily thermal cycles can overestimate the heat transfer. The computational time of the numerical model is fifteen times longer than that of the simplified one.
[67] Xiao et al.	T= - 18°C - +20°C	NC Clay	D= 95mm	Thermal Borehole Shear Test			✓	Significant reduction in the shear strength at the pile/soil interface due to temperature and radial displacement under thermal cycles.
[73] Rotta Loria et al.				layer model continuous model 3D FEM	✓	✓		Higher accuracy of FEM compared to the load-transfer method to account for the interactions of energy pile groups.
[74] Nguyen et al.	T= 19°C - 21°C	Dry sand	D= 20mm L= 600mm	Laboratory test			✓	The increase in cycle number reduces the irreversible settlement. Higher axial force at the end of heating compared to cooling.
[55] Luo et al.	T= 10°C - 30°C	Sandy clay	D= 0.6m L= 18.5m	TRT			✓	The temperature change and the restraint condition affect the expansion and contraction of the energy piles. The deformation of energy piles is elastic.
[75] Wang et al.	T= 11°C - 55°C	Dry sand	D=104mm L= 1.6m	Laboratory test			✓	Thermal strains are higher for piles with W-tube compared to piles with spiral coil and U-tube.
[65] Alberdi-Pagola et al.	T= 4°C - 16°C	Sand	D= 0.15m L= 15m	3D FEM COMSOL	✓			No significant structural effects of thermal cycles on energy piles after one year of operation for temperature variation within 2°C.
[69] Gawecka et al.	T= -6°C - +56°C	Clay	D= 0.55m L= 23m	FEM ICFEP	✓			Considerable tensile axial stress appears in the pile during cooling mode. Overestimation of the pile behavior using the load-transfer method and when neglecting the transient state of the thermal loads.

### 3.3. Concrete behavior in energy piles

Understanding the accurate response of concrete under thermal loads is complex due to the non-linear and heterogeneous nature of concrete. The temperature changes can significantly affect the density, thermal diffusion, and compressive strength of concrete due to the change in permeability and porosity [50]. Besides, contraction and dilatation of cement can lead to thermal cracks in cement-based materials, resulting in reduced concrete durability. The effect of cracks becomes critical when tensile stresses occur in concrete and exceed its ultimate strength [71]. This behavior can pose a significant interaction problem between the mechanical and thermal performance of the geothermal system, especially for long-term operation. However, to the authors' knowledge, there is not yet a detailed

approach to integrate various properties of concrete into modeling to study their effects on the thermo-mechanical behavior of energy piles at different time scales.

### 3.4. Adjacent energy piles

The heat transfer capacity of a single pile is usually insufficient to cover the heating and cooling loads of a building. Thus, buildings require the activation of a group of piles to meet the thermal loads. In this regard, the load-transfer method has been modified to consider the interaction between adjacent piles [76]. The interaction factor method has also been reported in the literature to find the displacement response of pile groups exposed to cooling and heating. It consists of analyzing the interactions between two adjacent piles, then superimposing the individual impacts on a group. Rotta and Laloui [77] validated the interaction factor method by a 3D numerical model. However, the method is developed only for energy piles free of mechanical loads and free to move at their head where they are fully restricted at the tip. Therefore, using this method for floating pile groups can underestimate the vertical displacements.

On the other hand, some numerical models have been performed to investigate the effect of group action caused by thermally-activated piles [70,73,78]. The results showed that the increase in the number of energy piles decreases the pile stresses but increases the displacements of the foundation to critical values. Wu et al. [72] introduced the effect of the pile cap on the thermo-mechanical behavior of energy piles. They found that the pile cap poses additional restrains on the energy piles, resulting in smaller irreversible head displacements compared to that without the pile cap. The effect of the raft foundation appears more critical, as presented in the numerical study of Salciarini et al. [79]. The presence of a relatively rigid raft results in axial stresses in non-active piles in the same order as that of thermally active piles, even when the latter are relatively spaced, and the temperature variations in the non-active piles are small. The changes in strains and stresses of a pile group are related to various variables influencing the interaction between piles. The soil young's modulus ratio, the spacing between piles, the pile-soil stiffness ratio, the soil-pile thermal expansion coefficient ratio, and the pile slenderness ratio are reported [77] [80]. However, further information is still required to find the effect of these variables on both active and non-active pile behavior. Detecting the proper position and the number of active energy piles is also an essential problem that should be investigated.

## 4. Current Trends in energy piles design parameters

The efficiency of energy piles depends on the design parameters of the entire system (Figure 5). So, improving the thermal properties of each element leads to better thermal performance. The following section provides a broad review of most published parametric studies. It improves the heat transfer efficiency between GHE and the ground.

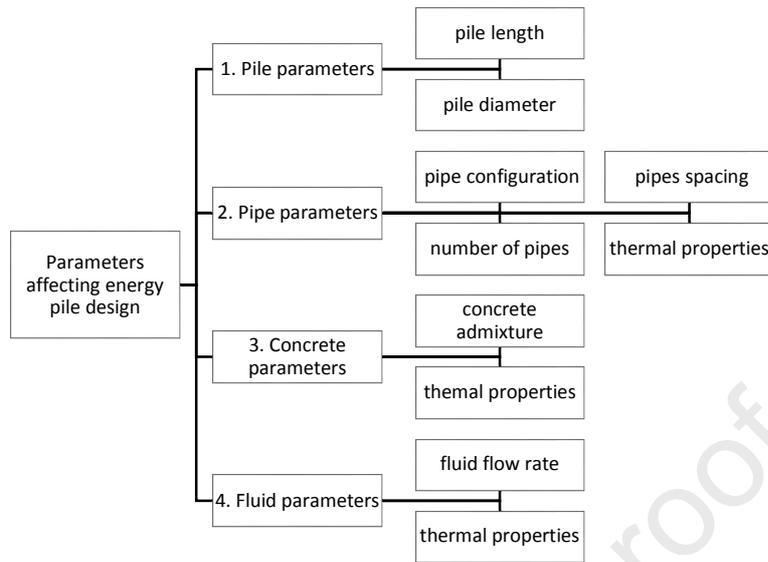


Figure 5. Parameters affecting energy piles design

#### 4.1. Pile design

The efficiency of heat transfer increases with longer piles (Figure 6). Using larger diameter piles also has a positive effect, as it allows more GHE pipes to be installed. It reduces the pile thermal resistance and so on increases the heat transfer, but on the condition of preventing pipe-to-pipe interactions [81]. However, from a mechanical perspective, the additional thermal loads, due to the improvement in thermal performance, can increase the axial stresses of the foundation. So, any change in the design of the energy piles should take the mechanical side-effects.

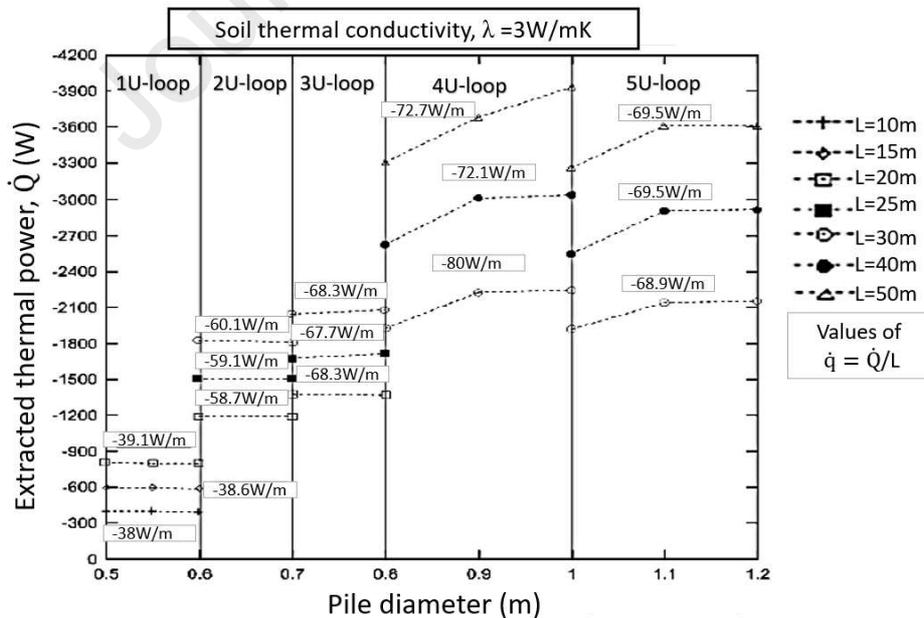


Figure 6. The effect of the diameter and length of the energy piles on their thermal performance [16]

## 4.2. Pipe design

### 4.2.1. Pipe configurations

The configurations of vertical GHE pipes installed in an energy pile, as in a borehole, can be classified based on their cross-sectional geometry and the pathway taken by the fluid in the flow channels to exchange heat with the ground (Figure 7).

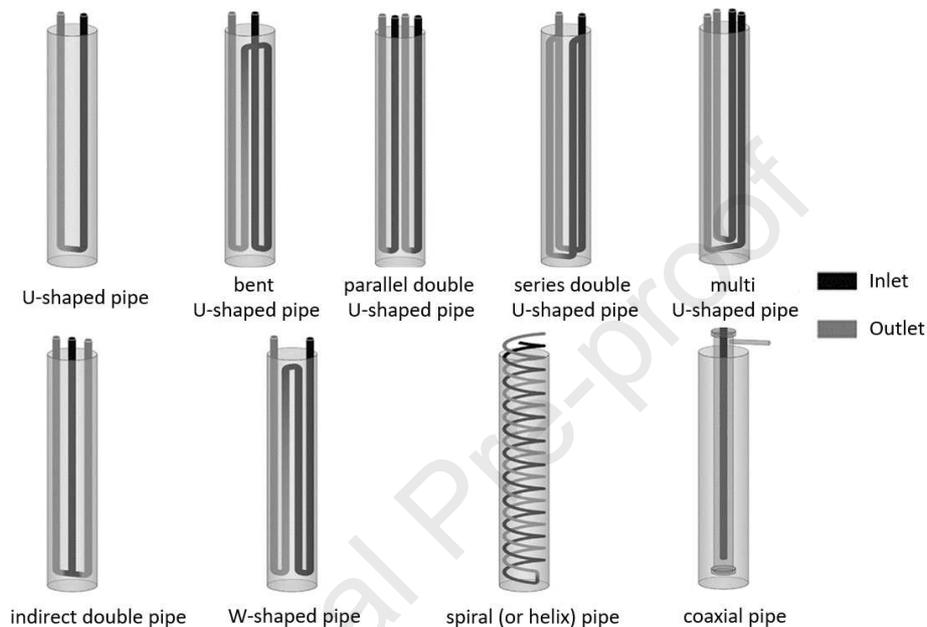


Figure 7. Pipe configurations for energy piles [16]

Changes in the pipe configuration play an essential role in thermal system performance. Generally, these pipes take the form of U, W, or spiral coils fixed to the reinforcement cage of an energy pile. For approximately thirty years, the single U-pipe has been the industry standard and the most commonly used for heat exchange in boreholes, as in energy piles. This popularity goes to the simplicity of U-tube design and ease of transport, as well as its ease of installation compared to other alternatives [82]. W-pipe heat exchangers have also been widely used in energy piles. However, although they have a higher thermal transfer capacity than those provided by U-pipes [3,83], the risk of air accumulation at the top of the W-tube [28] and its complicated installation compared to the U-tube can be the reasons for being less commonly used. The single U-tube and W-tube have been extended to double, triple, or multiple tubes to increase the effectiveness of heat exchange. The application of spiral (or helix) heat exchangers in energy piles has also attracted considerable attention. Providing high thermal efficiency, preventing airlock, and limiting thermal short-circuiting are the advantages that have led some studies to consider the spiral shape as the best configuration of the pile heat exchanger [23,84]. According to the thermal analysis done by Zarrella et al. [85] for short-timescales, the spiral coil provided a higher thermal transfer performance of 23% at the peak load than the pile with triple U-tube, but only a 9% increase in the normal state. Luo et al. [86] demonstrated that the spiral type after one year of operation achieved a thermal production of 90% and 96% compared with triple U- and double W- types, but it was 1.4 times

higher than double U-types (Figure 8). For the large-diameter energy piles, where more than 5-pairs of U-tubes can be installed, Park et al. [39] revealed that the heat exchanger pipes in helix shape have the optimal configuration, given the economic feasibility and the thermal performance. Nevertheless, the application of this shape is still limited because of the difficulties associated with its installation, especially in piles of small diameters [16].

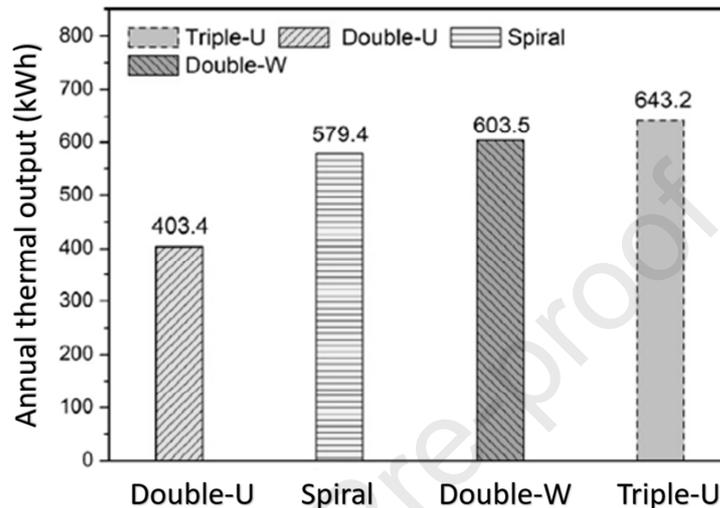


Figure 8. The effect of the pipe configuration on the thermal performance of energy piles [86]

Increasing the number of GHE pipes in an energy pile is advantageous. However, it becomes unfavorable when thermal interferences occur between the adjacent pipe loops [87]. Many studies emphasized the need to consider the effect of these interactions on heat transfer efficiency [12,43,47,81,88]. Lee and Lam [88] found that increasing the spacing between GHE pipes in an energy pile improves the thermal efficiency. However, the sensitivity analysis conducted by Caulk et al. [47] showed a gradual decrease in the rate of heat transfer per meter length after a certain distance (Figure 9). The study also showed lower thermal performance when the pipes are more plunged to the center of the pile. In this regard, Loveridge and Powrie [81] specified a typical range of pipe spacing from 250mm to 300mm to reduce heat transfer between GHE pipes and meet the thermal requirements. Therefore, to create an optimal geometry for heat exchangers in an energy pile with U-/W- configurations, it is recommended to install multiple GHE pipes with minimum shank spacing of 250 mm. Besides, ground heat exchangers should be attached to the pile reinforcement cage to minimize the impact of the concrete cover around the pipes.

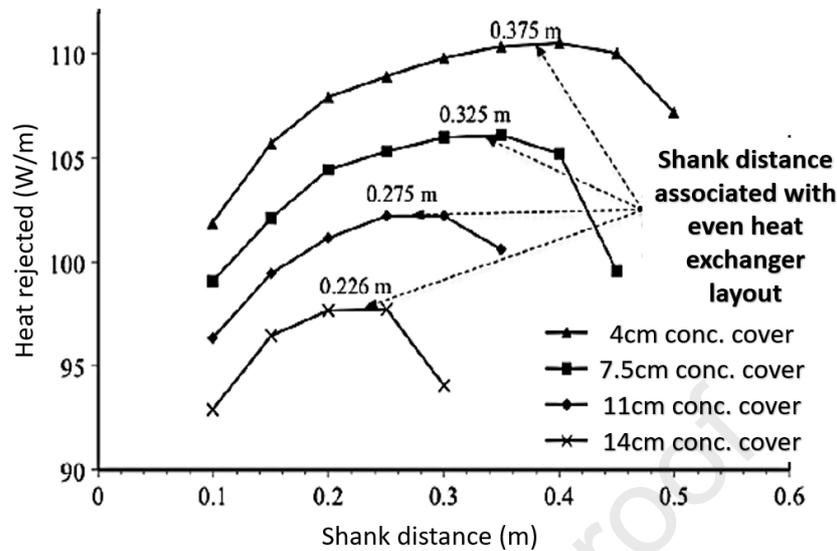


Figure 9. The effect of the shank distance and the concrete cover on the thermal performance of energy piles [47]

For helix heat exchangers, Zhao et al. [89] studied the effect of spiral pitch on the thermal behavior of energy piles. They proved that reducing the pitch size increases the heat transfer capacity. However, the use of smaller values less than 250mm can cause excessive pressure drops and significant thermal interferences [27,46]. To weaken these effects, Huang et al. [27] proposed a novel truncated cone helix energy pile. The laboratory investigations found a higher thermal efficiency of the novel energy pile than the conventional ones. They also showed better performance by setting a more significant cone angle. However, the complex constructability of this form seems impractical in reality. Alternatively, it needs further structural and economic feasibility analysis.

#### 4.2.2. Pipe characteristics

The pipes used in geothermal applications are subject to specific standards adopted during manufacturing. In general, they are polyethylene pipes [82], have a diameter ranging between 20mm (DN20) and 40mm (DN40) [90]. For GHE pipes deeper than 150m, DN40 is the most used. However, for shallow energy systems of depth less than 60m, such as energy piles, the use of large pipe diameters is sometimes unfeasible due to the additional amount of pumping power required to increase the flow rate [12]. Table 4 summarizes the general properties of the main pipe types used in practice.

Table 4. Properties of some plastic heat exchanger pipes [82]

Type	Outer diameter (mm)	Wall thickness (mm)	Thermal conductivity (W/(mK))	Thermal resistance (K/(W/m))
PE DN20 PN12	20	2.0	0.42	0.085
PE DN25 PN8	25	2.0	0.42	0.066
PE DN25 PN12	25	2.3	0.42	0.077
PE DN32 PN8	32	2.0	0.42	0.051
PE DN32 PN12	32	3.0	0.42	0.079
PE DN40 PN8	40	2.3	0.42	0.046
PE DN40 PN12	40	3.7	0.42	0.078

PE = polyethylene  
 DN = diameter - nominal  
 PN = pressure - nominal (in bars)

### 4.3. Concrete design

Providing high mechanical properties of concrete is one of the principal objectives to maintain the strength and durability required of the structure. For energy pile systems, the thermal properties of concrete are also important due to their positive impact on the efficiency of heat transfer between the GHE pipes and the surrounding soil. Concrete has thermal conductivity values from 1W/m. K to over 4W/mK, depending on the cement/aggregate ratio, aggregate type, and moisture content [91,92]. The high aggregate ratio improves the thermal conductivity of the concrete [93]. However, the high cement content required for high-strength concrete mixtures can reduce it. Besides, adding additive materials such as fly-ash to improve the workability and durability of concrete can have a supplementary negative impact on thermal conductivity degradation by over 20% [46,91]. Alternatively, Carotenuto et al. [46] found that the thermal performance of energy piles increases by 42% with an increase in the thermal conductivity of concrete from 1.2W/mK to 2.5W/mK. Therefore, many studies have proposed improvements for this parameter. Li et al. [24] suggested adding graphite powder to cement paste. The results of laboratory testing and numerical study exhibit a significant improvement in the heat transfer with increased graphite content under the same environmental temperature. Laing et al. [94] showed that mixing concrete with heat transfer materials such as graphite and aluminum can provide required heating and cooling with fewer pipe heat exchangers of shorter length. Yang et al. [95] proposed combining graphite with the phase change material (PCM) in concrete to benefit from the high thermal conductivity of graphite and the high heat storage capacity of PCM. However, the addition of a large amount of graphite to improve the thermal conductivity regardless of the study of their mechanical side-effects on the structure can be critical. Guo et al. [96] found an excessive reduction in compressive and flexural strengths of concrete by 50% when graphite was 5% of concrete content due to the increase in porosity and void volume (Figure 10). Therefore, some authors [11,97,98] proposed adding materials that have high strength and thermal conductivity, such as carbon fiber, copper slag, and steel fiber. In conclusion, adding thermally conductive materials to the concrete mix to improve the thermal properties of concrete is beneficial. Nevertheless, structural and economic feasibility studies are essential to maintain the compressive strength of concrete and to provide the cost-effectiveness of the structure.

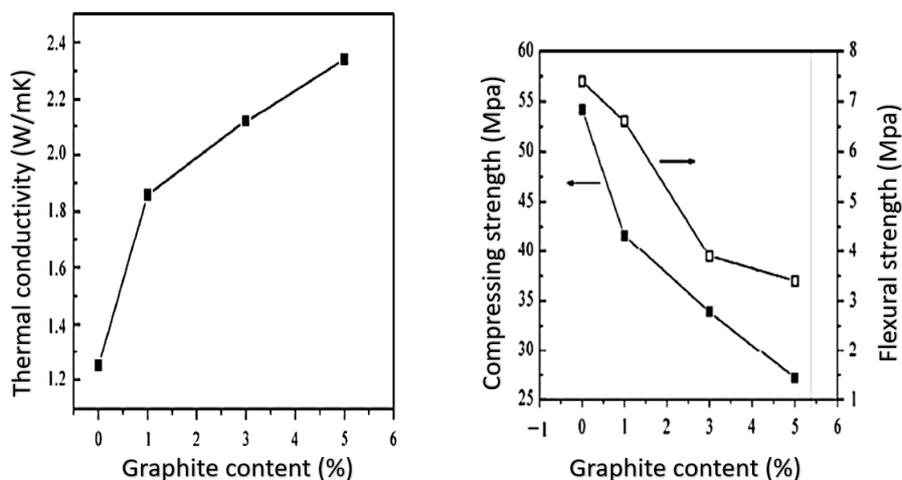


Figure 10. the effect of graphite content on thermal conductivity, compressive and flexural strength of concrete [96]

#### 4.4. Fluid design

##### 4.4.1. Fluid flow

The fluid flow behavior that is laminar or turbulent is an influential factor in the convective heat transfer efficiency between the fluid and the inner wall of GHE [99]. It is characterized by the Reynolds number ( $Re$ ), which increases by increasing the pipe diameter and fluid velocity or decreasing fluid viscosity [100]. Reynolds number values below 2300 produce laminar flow where values above 4000 produce turbulent flow. Using a turbulent flow rate improves the heat transfer rate per meter of length between the pipe and ground. It can also reduce the heat transfer between the upward and downward flow-pipes, and prevent the thermal short-circuiting that occurs at low laminar conditions [43,82]. However, according to Park et al. [17], excessive fast flow during full turbulence does not allow enough contact time for heat exchange and thus reduces thermal efficiency.

Moreover, increasing the pump performance to achieve turbulence leads to higher energy consumption by the heat pump and therefore increases the operational costs of the system[86]. Consequently, optimizing the fluid flow rate is necessary for both thermal performance and economic feasibility. Kavanaugh and Rafferty [90] recommended in the ASHRAE manual to use fluid flow rate in the transient conditions, for the Reynolds number between 2500 and 3000, which can be a compromise between thermal performance and power requirements of the heat pump.

##### 4.4.2. Fluid properties

Water is the primary fluid used in heat exchangers for heat transfer, but it can be mixed with an antifreeze solution such as propylene glycol and ethylene glycol to avoid freezing fluid when the temperature falls below zero in the heat exchanger tubes [101]. However, the increased concentration of the water-glycol mixture significantly increases the fluid viscosity and thus the laminar zone, decreasing heat transfer (Table 5). Therefore, the optimal proportion of any admixture should avoid freezing, prevent excessive viscosity, and improve thermal performance without significantly increasing operational costs.

Table 5. Properties of the heat transfer fluids [101]

Fluid	Freezing point (°C)	Normal boiling point (°C)	Viscosity at 20°C (centipoise)	Thermal conductivity (W/(mK))	The specific heat at 20°C (J/(Kg. K))
Water	0	100	1.01	0.609	4.19
Ethylene glycol	-13	197	20.9	0.258	2.19
Propylene glycol	-59	188	60.5	0.147	2.50
Methanol	-98	64	0.6	0.202	2.47

#### 4.5. Ground characteristics

One of the fundamental design aspects of energy geo-structures is ground characteristics. The determination of the total GHE length is related to the amount of heat exchanged with the surrounding and so on to the thermal properties and the temperature profile of the ground. Therefore, improper evaluation of these parameters can lead to an overestimation or underestimation of the GHE design, consequently affecting the overall performance of the system. This becomes more critical with

unbalanced heating and cooling loads [102]. The presence of groundwater flow also has a significant contribution in this direction due to convective heat transfer. The experimental study of You et al. [103] showed that groundwater flow not only increases the rate of heat transfer but also increases the soil thermal conductivity by 10%, for a water flow velocity of  $5 \cdot 10^{-8} m^2/s$ . Table 6 summarizes the thermal ground database for unconsolidated sediments and rocks obtained from literature, direct measurements, and the European Cheap GSHPs-project, which combines experimental and literature values.

Table 6. Review of ground thermal properties [104]

Material	From Literature Review				Directly measured			UNIPD-Cheap-GSHPs database				
	$\lambda$		$\rho c_p$	$\rho$	$\lambda$		$\rho c_p$	$\rho$	$\lambda$			
	$Wm^{-1}K^{-1}$		$MJm^{-3}K^{-1}$	$10^3 Kg m^{-3}$	$Wm^{-1}K^{-1}$		$MJm^{-3}K^{-1}$	$10^3 Kg m^{-3}$	$Wm^{-1}K^{-1}$			
	min	max			min	max	REC.			REC.		
Sandstone	0.72	6.50	1.8-2.6	2.2-2.7	1.03	4.54	2.00	2.06-2.28	2.43-2.66	0.72	6.50	2.60
Clay-mudstone	0.59	3.48	2.1-2.4	2.4-2.6	1.47	3.21	2.54	1.80-2.23	2.70	0.59	3.48	2.13
Limestone	0.60	5.01	2.1-2.4	2.4-2.7	2.42	4.41	2.88	1.81-2.22	2.35-2.80	0.60	5.01	2.50
Granite	1.49	4.45	2.1-3.0	2.4-3.0	2.02	3.68	3.13	1.80-2.12	2.66-2.73	1.49	4.45	2.74
Marble	0.98	5.98	2.0	2.5-2.8						0.98	5.98	2.50
Clean gravel, dry	0.13	0.9	1.3-1.6	1.8-2.2	0.14	0.55	0.33			0.14	0.9	0.4
Heteromeric gravel with sand, wet	0.18	3.00			0.94	1.33	1.08			0.2	3.00	1.08
Medium sand, dry	0.15	0.90	1.3-1.6	1.8-2.2	0.15	0.68	0.26	0.41-1.48		0.15	0.9	0.4
Medium sand, wet	1.00	2.60	2.2-2.8	1.9-2.3	1.44	2.45	1.86	1.53-2.27		1.0	2.6	1.9
Silty sand/sandy silt, wet	1.20	2.25			1.24	2.06	1.56	1.85-2.48		1.20	2.25	1.62
Silt, dry	0.26	1.09	1.5-1.6	1.8-2.0	0.25	0.82	0.50	1.37-1.52		0.25	1.09	0.55
Silt and clayey silt, wet	0.82	2.60	2.0-2.8	2.0-2.2	0.93	1.76	1.32	1.84-2.43		0.82	2.60	1.45
Clay, dry	0.25	1.52	1.5-1.6	1.8-2.0	0.25	1.22	0.64	0.49-1.38		0.25	1.52	0.64
Plastic clay, wet	0.60	1.90	2.0-2.8	2.0-2.2	0.87	1.39	1.03	0.62-2.67		0.60	1.90	1.10

## 5. Evaluation criteria of energy piles

The development of a sustainable energy pile system involves a comprehensive analysis that goes beyond the thermal efficiency. Environmental impact and cost, with the thermal efficiency of the energy system, are essential and influential factors in evaluating the feasibility of this system and optimizing it. The high level of sustainability for an energy system specifically refers to an efficient and economically viable system with the least negative impact on the environment. To date, few guidelines have provided a reference to the indicators to be used to assess the overall performance of an energy pile-operating system. The evaluation of energy piles, from a thermal perspective, deals with the multi-criteria analysis of the ground-source heat pump system (GSHP) associated with these heat exchangers: energy, exergy, economy, and environmental criteria (denoted by 4E criteria) [105]. From the structural view, the possibility of failure of an energy pile system due to excessive expansion or extraction resulting from thermal exchange needs to be checked. In this section, the 4E-G criteria relating to the design of energy piles, both thermally and mechanically, are reviewed (Table 7).

### 5.1. Energy criteria

Improving energy performance is the principal target in the feasibility study of geothermal systems. Providing the thermal needs for buildings in an abundance and sustainable manner is the base objective of these systems. Therefore, increasing the efficiency of energy systems is essential. The performance of a GSHP is evaluated by comparing the energy delivered for buildings with the electricity consumed to operate the system [106]. Many terms determine the efficiency of the system, where the coefficient of performance (COP) is the most used (Table 7).

### 5.2. Exergy criteria

Generally, the most commonly used measurement when evaluating the efficiency of heat pump systems is energy efficiency, as mentioned above. However, exergy analysis is also needed for a more accurate analysis of the actual system performance in a specified environment. The exergy criterion determines the quality of different energy flows in each subsystem of energy systems [107,108]. Therefore, exergy analysis can be used to identify the primary sources of thermodynamic irreversibility and to minimize entropy generation during the heat transfer process [109]. Exergy loss values can quantify the reduction in the system's ability to deliver thermal energy in individual subsystems and the overall one, allowing for a more comprehensive assessment of the system's efficiency than energy analysis [110,111].

### 5.3. Economic criteria

An economic study is essential before installing a GSHP system associated with borehole heat exchangers due to the high cost of drilling boreholes. In contrast, this feature is less critical for energy piles because ground heat exchangers are mainly built into the pile foundation. So, there is no additional cost for drilling. Nevertheless, the overall economic analysis of the system, which includes investment, operation, and maintenance, provides the opportunity to assess economic feasibility accurately, especially for large-scale projects. The net present value (NPV) is a fundamental criterion in the economy to analyze the life cycle cost of a system from the payback period [112]. Some studies used NPV to examine the economic values of energy piles for different pipe configurations. However, for an accurate assessment, it is suitable to conduct an economic analysis of the entire system of GSHP instead of a single element of equipment. Other economic criteria can be used, such as the savings-to-investment ratio (SIR), the life cycle cost (LCC), and the profitability index (PI) (Table 7).

### 5.4. Environmental criteria

Environmental concerns are an essential factor in sustainable development. Keeping a healthy environment preserves the system besides the surrounding environment. Operating a GSHP system without paying attention to this indicator can affect adjacent systems and the ecological environment with time. This aspect becomes critical with unbalanced heat exchange during the cooling and heating phases. In contrast, to date, none of the studies or references has provided indicators to assess this effect. However, some studies have used some factors that provided a general overview of the environmental impacts associated with the use of GSHP (Table 7).

### 5.5. Mechanical criteria

In most cases, the pile design is initially based on structural requirements. However, additional factors are required for energy piles to quantify heat extraction and injection. The thermal expansion and contraction of the pile caused by heating and cooling should be checked in addition to the mechanical deformations and displacements under the service limit state. Moreover, thermally-induced forces applied to energy piles due to compression and tension should not reach the ultimate pile capacity. The distribution of stresses and strains induced by imposed thermal loads highly depends on the degree of freedom of the pile (DOF). It goes from maximum strains ( $\varepsilon_{th,free} = -\alpha_{EP}\Delta T$ ) for completely free piles (DOF = 1) to maximum internal stresses ( $\sigma_{th,fixed} = E_{EP}\alpha_{EP}\Delta T$ ) for perfectly restrained piles (DOF = 0) [3,113]. Therefore, Soga and Rui [60] suggested considering the maximum thermal-induced displacement of a free pile ( $\omega_{th,free} = -\alpha_{EP}\Delta TL$ ) and the maximum thermal-induced stress ( $\sigma_{th,fixed}$ ) of a fully restrained pile as the primary design criteria to assess the serviceability and safety of the system. Bourne-Webb et al. [14] confirmed that  $\sigma_{th,fixed}$  can be a conservative limit to check the thermal-induced stresses of energy piles most times. However, they pointed out that  $\omega_{th,free}$  cannot be a safe limit for checking the pile movements, especially for a large soil-to-pile thermal expansion ratio. Besides, it cannot be applied to a group of piles, where the group movement is much higher than that of an unrestrained single pile. Alternatively, Rotta Loria et al. [114] showed a critical behavior of energy piles in the cases of development of tensile stresses during cooling and evolution of mechanical cyclic degradation in sandy soils. In these cases, the consideration of  $\sigma_{th,fixed}$  and  $\omega_{th,free}$  as boundary criteria cannot be conservative. Therefore, complex thermo-mechanical analysis is needed to provide more realistic responses for single energy piles and pile groups under the ultimate and service limit states, addressing critical design issues.

Table 7. 4E-G evaluation criteria summary for GSHP system with energy piles

Criterion	Term	Symbol	Equation	Suitable value	Reference
Energy	Coefficient of performance	COP	$\frac{\text{Heat output}}{\text{Electrical energy input}}$	>3.5	[90] [106–108]
	Heating Season Performance Factor	HSPF	$\frac{\text{Total seasonal heating output}}{\text{electrical energy input}}$	>6.8	
	Seasonal Energy Efficiency Ratio	SEER	$\frac{\text{total seasonal cooling output}}{\text{electrical energy input}}$	8-10	
	Energy Efficiency Ratio	EER	$\frac{\text{cooling capacity}}{\text{electrical energy input}}$	>10	
	heat exchanger effectiveness	$\theta^a$	$\frac{T_{in} - T_{out}}{T_{in} - T_g}$		
Exergy	Exergy efficiency	$\psi$	$\frac{\text{exergy output}}{\text{total exergy input}}$		[107,108,110,111,115]
	Exergetic coefficient of performance	$COP_{ex}$	$\frac{\text{exergy input} - \text{exergy output}}{\text{electrical energy input}}$		
	Exergy loss	$\Delta \dot{E}_X$	Exergy input - exergy output		
	entropy generation number	$Ns^a$	$\frac{S_{gen}}{Q} + \frac{A}{\pi R_e} + 0.0195\pi(1+\Phi) \frac{B}{\theta_m} Re^{21/4}$		[116]
Economy	Net present value	$NPV^b$	$\sum_{t=0}^n \frac{Bt}{(1+r)^t} - \sum_{t=0}^n \frac{Ct}{(1+r)^t}$ (Annual savings) $\frac{(1+r)^n - 1}{r} - \text{initial cost}$	>0	[102,117–120]
	Internal rate of return	IRR	$\sum_{t=0}^n \frac{C_t^e - C_t^i}{(1+IRR)^t} = 0$		
	Simple payback period	SPP	$\sum_{t=0}^n C_t^e - C_t^i = 0$	2-10 years	
	Discounted payback period	DPP	$\sum_{t=0}^n \frac{C_t^e - C_t^i}{(1+r)^t} = 0$		
	Savings-to-investment ratio	$SIR^c$	$\frac{\sum_{t=0}^n \frac{St}{(1+r)^t}}{\sum_{t=0}^n \frac{It}{(1+r)^t}}$	>1	

	Profitability index	PI	$\frac{\sum_{t=0}^{n-1} \frac{St}{(1+r)^t} - \sum_{t=0}^{DPP} \frac{St}{(1+r)^t}}{\sum_{t=0}^{DPP} \frac{St}{(1+r)^t}}$	
	Life cycle cost	LCC	$\sum_{t=0}^n \frac{C_t}{(1+r)^t}$	
	total annual cost	TAC <sup>d</sup>	$C + C_{inv}$	
Environment	CO <sub>2</sub> emission factor	Y <sup>e</sup>	$n \cdot E_{annual} \cdot \frac{EF}{1000}$	[102,121,122]
	Total Equivalent Warming Impact	TEWI <sup>f</sup>	$(n \cdot L \cdot m \cdot GWP) + (n \cdot E_{annual} \cdot EF) + (L_{demolition} \cdot n \cdot GWP)$	
	Environmental prevention cost	Cp <sup>g</sup>	$\sum_{i=1}^k PC_i E_i$	
Geostructure	Total strain	$\varepsilon^h$	$\varepsilon_m + \varepsilon_{th}$	[16]
	Vertical displacement	$\omega_z$	$\varepsilon_z * L$	
	Total stress	$\sigma^i$	$\sigma_m + \sigma_{th} = E_{EP}(\varepsilon_m + \varepsilon_{th} + \alpha_{EP} \Delta T)$	

<sup>a</sup>  $T_{in}$ : inlet fluid temperature,  $T_{out}$ : outlet fluid temperature,  $t_g$ : undisturbed ground temperature.

<sup>b</sup>  $S_{gen}$ : the total entropy generation rate due to the pressure drop  $\Delta P$  and the temperature difference  $\Delta T$ ,  $T_{f,m}$ : the logarithmic average fluid temperature of the GHE with U-tube,  $Q$ : the heat transfer rate,  $\Theta_m = \frac{QR_B}{T_{f,in} L}$ ,  $A = \frac{Q}{\mu C_f T_{f,in} r_i}$ ,  $\Phi =$  scale factor of pressure,  $B = \frac{\rho_f v^3 R_B}{T_{f,i}^2}$ ,  $\nu$ : dynamic viscosity,  $\rho_f$ : fluid density,  $C_f$ : fluid specific heat,  $r_i$ : inner pipe radius.

<sup>c</sup>  $n$ : the period of life cycle analysis;  $B_t$ : the GSHP benefits in year  $t$ ;  $C_t$ : operating cost in year  $t$ ;  $r$ : real discount rate;  $C_t^e$ : operating cost in year  $t$  for the existing system;  $C_t^f$ : operating cost in year  $t$  for the alternative system.

<sup>d</sup>  $S_t$ : the savings in year  $t$ ;  $I$ : the investment in year  $t$ .

<sup>e</sup>  $C$ : Annual operating cost,  $C_{inv}$ : The initial investment cost for yearly system operation.

<sup>f</sup>  $E_{annual}$ : annual energy use in kWh/year;  $EF$ : emission factor driving energy in kg CO<sub>2</sub>/kWh.

<sup>g</sup>  $L$ : annual leakage rate (%),  $m$ : refrigerant charge in kg,  $GWP$ : global warming potential in kg CO<sub>2</sub>/kg refrigerant,  $L_{demolition}$ : refrigerant losses during demolition (%).

<sup>h</sup>  $E$ : emission amount for a type of pollution;  $PC$ : prevention cost for a type of pollution.

<sup>i</sup>  $\varepsilon_m$ : the strain induced by the mechanical loads,  $\varepsilon_{th}$ : the observed strain induced by the thermal loads.

<sup>j</sup>  $\alpha_{EP}$ : the thermal expansion coefficient of an energy pile,  $E_{EP}$ : the young's elastic modulus of an energy pile.

## 6. Optimization of energy piles

Optimization is vital for an optimized GSHP with energy piles as it can increase the thermal efficiency of the system and simultaneously decrease the system cost while maintaining system-induced stresses and strains within acceptable limits. All GSHP optimization studies associated with energy piles mainly focus on improving heat exchanger parameters to provide better thermal performance. However, the development of a complete strategy for the design optimization of these systems is still needed. Full coverage of existing optimization studies (which have mainly been published for borehole heat exchangers), including a review of objective functions, decision variables, design constraints, and optimization methods, is presented and discussed in this section.

### 6.1. Objective function

Generally, the design optimization of a thermal system is a process that involves improving system components and design parameters based on minimizing or maximizing single or multiple design objectives according to specific constraints [109]. For GSHP, it aims to optimize one or more objectives that are derived from the 4-E evaluation criteria described in Table 7.

#### 6.1.1. Single-objective optimization

Many studies have developed a single-objective optimization in the geothermal field [123–125]. Major works include thermal and economic analysis to improve the design and operation of GSHP systems. For instance, Robert et al. [126] developed a new optimization design method of BHE to minimize the total cost of the GSHP system, including the initial costs of drilling, heat pump, excavation, and the cost of electricity. Li et al. [127] established a single-objective optimization method to minimize entropy generation in a U-tube heat exchanger, and they found the optimal parameters of BHE. Huang et al. [128] developed an optimization methodology for BHE design to improve the thermodynamic

performance of the GSHP system. The optimization strategy minimizes the entropy generation number (EGN), and it is based on defining the critical design parameters and design constraints as a first step, then devising the optimization solution, including the development of the objective function, the selection of the performance model and the optimization technique. The proposed method was validated using TRNSYS and achieved a 12.2% reduction in EGN. However, the economic analysis of the borehole system based on optimized design parameters showed an increase in energy consumption of the heat pump compared to the base system design. The results reveal that optimizing one objective function of a system can deviate from the full effective design optimization.

### 6.1.2. Multi-objective optimization

Unlike single-objective optimization, multi-objective optimization considers multiple objective functions simultaneously. They overcome the shortcoming of single-objective design optimization techniques by providing comprehensive information on the impact of different objective functions on decision-making and helping to find appropriate optimized solutions [129]. According to Dinçer et al. [130], the multi-objective optimization problem is to find the appropriate design variable vector  $X\{x_1, x_2, \dots, x_n\}$ , which minimizes or maximizes the objective functions of  $f_1(X)$ ,  $f_2(X)$ , ...  $f_N(X)$ , subjected to certain constraints. Few studies have been published on the multi-objective optimization of GSHP systems in the past years, with a significant focus on the thermo-economic approaches. Sayyaadi et al. [131] conducted a multi-objective design optimization study of a vertical ground-source heat pump system by examining thermodynamic and thermo-economic analysis simultaneously and considered eight decision variables for optimization. Huang et al. [116] applied a multi-objective design optimization for vertical GHE pipes to minimize both the cost of the system and the thermodynamic irreversibility induced by the entropy generation in-ground heat exchangers. The effectiveness of the proposed method was validated based on small-scale and large-scale case studies of GSHP systems implemented in Australia and China. Park et al. [132] presented their optimization study for borehole sizing based on thermal and economic aspects. The proposed method takes the life cycle cost and the entering fluid temperature to the heat pump as objective functions. The results showed a reduction in the total required length of BHE by 30%. However, it remains only useful for the early design stage.

### 6.1.3. Scalarization and Pareto solutions

Two conventional approaches have been used to solve multi-objective optimization problems. The first one uses the weighted sum function to simplify the multiple objectives into a single-objective problem [133]. However, multi-objective optimization looks for tradeoffs between objectives that are in conflict rather than a single solution, considering the interferences between them [134,135]. The Pareto approach is the second solution used by most of the studies for multi-objective optimization. This trade-off optimization consists of the development of a set of feasible non-dominated solutions called Pareto Front (or Pareto Frontier) to improve the objective function without ignoring another one [132]. The objective function values of the Pareto front refer to the set of all non-dominated optimal decision variables called the "Pareto optimal set" [136]. Figure 11 illustrates a typical example of Pareto solutions for a two-objective minimization problem where Pareto Front bounds non-dominated solutions. According to Cao et al. [137], Pareto-based algorithms benefit from the diversity of solutions. However, they exhibit problems of efficiency, such as slow convergence to the optimal front and low performance

on the problems with many objectives. Li et al. [138] propose a bi-criterion evolution framework of Pareto and non-Pareto criteria to apply it in the evolutionary algorithms to overcome weaknesses in each evolution. The proposed framework was validated, experimentally, on 42 test problems with various characteristics. However, this new solution needs to be implemented and validated for GSHP systems.

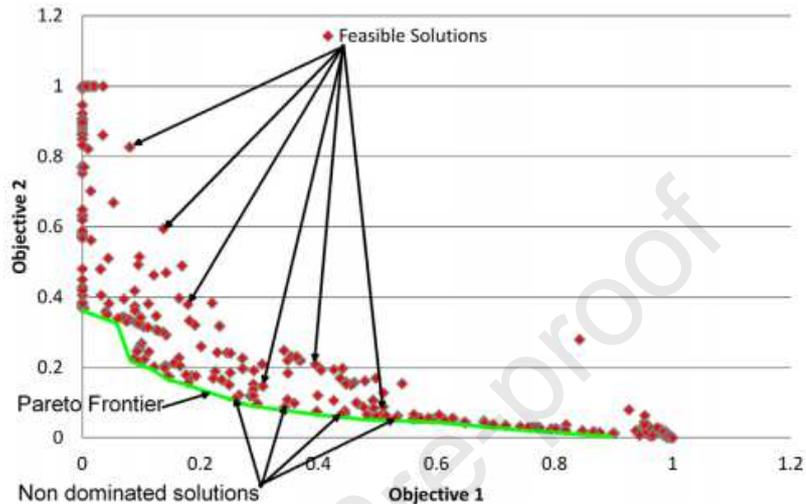


Figure 11. An example of Pareto Front for two-objective functions [134]

#### 6.1.4. Decision- making

Analyzing a multi-objective optimization problem can result in a set of solutions based on the Pareto front, which can be a potential solution. However, selecting the ultimate optimal solution for all various objective functions at the same time needs decision-making [135]. Generally, decision-making is a problem-solving process that chooses the optimal solution among the available solutions of Pareto front based on the priority of each objective concerning other objectives for a specific design case [134]. The stability of the selected point and its sensitivity for input system parameters are also essential criteria for decision-makers [139]. GSHP optimization studies based on decision-making have received little attention in the literature. Therefore, further development in this area is recommended.

#### 6.2. Decision variables

For a given optimization problem, the decision variables are the system parameters that affect the objective functions. So, analysis of these parameters is necessary to minimize or maximize these functions. For a GSHP system, various parameters affect its thermal optimization at different levels, including the building level, the heat pump level, and the GHE level. The latter is the most energy-saving part, as GHE has the minimum exergy efficiency and the maximum contribution to the installation cost of GSHP systems [110]. Some parameters can be changed and adjusted, while others are constrained either by installation conditions or by structural conditions. Therefore, identifying the decision variables that critically affect the performance of GSHP is vital for the optimization process. Experimental analysis can be used for optimization problems involving a limited number of parameters. However, in the case of GHE, numerical analysis is strongly recommended [140]. Many parametric studies have been published in the past years to investigate the most influential parameters of ground heat exchangers

[140–145]. Fernández et al. [143] proved that the use of sensitivity analysis is effective for determining which parameters should be optimized. They also revealed a reduction in the number of iterations required for the optimization process by approximately 89%. Huang et al. [128] carried out a global sensitivity analysis based on the Sobol method to determine the design variables of vertical heat exchangers.

The results showed a slight effect on the pipe thermal conductivity, the pipe shank distance, and the distance between the boreholes. Sivasakthivel et al. [140] observed that the heating load, the fluid inlet temperature, and the fluid flow rate have remarkable influences on COP and borehole thermal resistance. Cecinato and Loveridge [146] found that the number of GHE pipes is the most influential design parameter. For energy piles with spiral heat exchangers, the pitch size is the most critical factor affecting the heat transfer [23,40,44]. Batini et al. [13] studied the thermo-mechanical effects of many design parameters. They found that the configuration of tubes as U-, double U- or W-shape is the most important factor in both the thermal and mechanical performance of energy piles. They also found that the aspect ratio of the pile strongly affects the thermo-mechanical behavior. However, the mass flow rate of the circulating fluid affects only the thermal performance of the foundation. As well, the water antifreeze mixtures did not have a noticeable effect in this context. The design parameters used in the reviewed studies to optimize the vertical heat exchangers have thermal effects, not structural parameters (Table 8). Jelušič and Žlender [147] fill this gap in their new study to optimize the cost of energy piles. The vertical loads, the number of reinforcing steel bars, and the young soil modulus are the decision variables studied. However, wide-ranging research is still needed to detect decision variables by studying more thermal and structural parameters.

Table 8. A summary of the decision variables detected in some previous studies.

Reference	type	Method	GHE geometry					Material parameters			Operating conditions	
			$N_p$	$N_b$	$L_b$	$D_p$	$D_b$	$s_p/pitch$	$\lambda_p$	$\lambda_g$	$\lambda_s$	$m_f$
[142]	BHE	RSM				✓						✓
[128]	BHE	SOBOL		✓	✓				✓			✓
[144]	BHE	numerical			✓					✓		✓
[148]	BHE	numerical			✓				✓			✓
[140]	BHE	Taguchi			✓	✓	✓		✓	✓		✓
[149]	BHE	Taguchi					✓		✓			
[150]	BHE	Review			✓		✓		✓	✓		✓
[13]	EP	numerical	✓		✓		✓					✓
[145]	EP	numerical	✓			✓			✓	✓		✓
[146]	EP	Taguchi	✓						✓			
[81]	EP	numerical	✓						✓			
[86]	EP	TPT	✓			✓						
[151]	EP	numerical	✓						✓			
[47]	EP	numerical	✓					✓				✓
[34]	EP	numerical				✓		✓				
[46]	EP	numerical	✓			✓		✓		✓		
[11]	EP	review	✓						✓	✓		✓

### 6.3. Constraints

In optimization problems, design variables do not take arbitrary values but are restricted by some specified boundaries and conditions called design constraints [3]. Constraints for GSHP systems can be classified into levels, such as geometrical constraints related to the configuration and geometry of GHE, constraints associated with the material properties and the operational parameters of the system, and temperature constraints [90,128]. Typical thermal constraints applied to the design of ground heat exchangers can be reported in the literature. Some guidelines highlighted the effect of fluid freezing on the performance of energy piles. They, therefore, recommended maintaining the fluid temperature above zero with a safety margin of 2°C [5,6]. They also suggested that this temperature does not exceed 40°C because of the negative effect of high temperature on the efficiency of the heat pump [91]. However, unlike boreholes, energy piles are primarily designed to meet structural purposes and, therefore, parametric optimization must be controlled to avoid exceeding the limits of the structure. The stresses, strains, and the displacement of the pile should be below the allowable limits to avoid system failure resulting from temperature changes [91,147]. Determining the pile end conditions that can be unrestrained, fully restrained, or partially restrained also plays an essential role in the evolution of the foundation constraints. Therefore, mechanical restrictions can be a key target that should be introduced in the optimization study of energy piles.

### 6.4. Optimization methods

Various computational methods have been used to optimize energy systems. The selection of a technique depends on the type of problem being faced, the computational cost for models, and the time available for a project [134], [141]. Therefore, applying the appropriate one can significantly decrease the simulation run time and provides accurate optimum results. Brief details of the optimization algorithms used to optimize ground heat exchangers are listed below, including the genetic algorithm, other derivative-free optimization methods, and hybrid algorithms where more than one optimization algorithm is integrated (Table 9).

#### 6.4.1. Genetic algorithm (GA)

The genetic algorithm (GA) is the most widely used optimization method in energy systems. It relies on evolutionary techniques combining selection, crossover, and mutation operators to find the best solution to a problem. The process begins with a population of randomly generated candidate solutions called individuals, where each individual is evaluated. During each generation, GA selects the right individuals who are adjusted through mutation to form a new population. The process is repeated until the algorithm reaches the maximum number of generations or the satisfactory level of fitness for the population. In the end, the algorithm converges to the best individual, which represents the optimal solution to the given problem [152]. Genetic algorithms have many advantages for finding optimal values [153]. They are easy to understand, simple to implement, and less sensitive to initialization [61]. Compared to traditional optimization methods, GAs have less computing time, good convergence, and higher robustness with no need for differentiable or continuous search space. However, they can have some disadvantages, such as long convergence time for large and complex problems, problems of inaccuracy, and the possibility of proposing inaccurate solutions [154]. Several studies have used genetic algorithms for the optimization of GSHP systems with vertical GHE pipes [128,131]. Zeng et al. [155]

used the GA algorithm with 500 generations and 40 individuals. Sanaye and Niroomand [156] selected the GA characteristics as 1000 generations, 100 individuals in each population, with a 10% mutation probability. However, Park et al. [132] only used ten generations and 40 individuals for their multi-objective optimization study. These small values can be attributed to the limited number of variables designed in the study. Pu et al. [157] presented an alternative method of multi-objective optimization (MOGA) based on the non-dominate sorting genetic algorithm (NSGA-II). The GSHP system showed higher performance with the optimized parameters of the MOGA method compared to that of the screening method.

#### 6.4.2. Artificial Neural Network (ANN)

Artificial Neural Network (ANN) is a non-linear method that uses brain processing as a basis for developing algorithms used to model complex patterns and optimization problems. It acts as a black box that uses training data to link processing elements, called artificial neurons, to find the relationship between the input and output without requiring detailed information about the system [158]. ANN can handle a large number of data sets. It can implicitly detect non-linear, distributed, and parallel interactions between variables, even for complex problems. Afram et al. [154] proposed using ANN-based heuristic algorithms for optimization where the application of linear algorithms is unfeasible. Their proposal consists of transforming the objective functions into a new function by training neural networks, which allows the generation of a polynomial equation to solve the optimization problem. In the geothermal field, some authors have used the neural network to assess the performance of GSHP systems [148,158–160]. However, it is still not applied as a method of optimization for ground heat exchangers.

#### 6.4.3. The Nelder-Mead method (NM)

Nelder-Mead (NM) is a numerical optimization method used to find the optimum solution for functions of N variables by comparing function values at the three vertices of a triangle. The process generates a series of triangles with different dimensions in which the worst vertex that has the most significant function values is rejected and replaced with a new vertex. The process continues as long as function values are reduced at the vertices until the minimum is found. This method can represent good convergence due to its rapid calculation time. However, in many cases, it fails to obtain the optimal values due to the non-equality constraints of design parameters [134]. Sanaye and Niroomand [156] overcome this shortcoming by modifying the algorithm to enable it to work with inequality constraints. Then, they used the modified NM to obtain the optimum design parameters of a vertical ground coupled heat pump system. The optimal parameters obtained from NM were compared with those obtained from the genetic algorithm, and the results found a good agreement between the two methods.

#### 6.4.4. Mixed-integer Non-linear programming (MINLP)

Mixed-integer non-linear programming (MINLP) is a mathematical optimization methodology that addresses non-linear problems in objective functions and constraints [135]. Decision variables are constrained in this method either by integers or non-integer ranges. One study on the use of MINLP to optimize GSHP systems was detected. Retkowski and Thöming [161] used the Generalized Reduced

Gradient algorithm (GRG2) based on MINLP to optimize the main design parameters of a vertical ground heat exchanger. The total annual costs and the COP are both objective functions included in the model for detecting economic and thermodynamic aspects. They found that the GRG2 approach has higher stability and less computing time than evolutionary algorithms (EA). An overall annual cost improvement of over 10% was also detected using MINLP.

#### 6.4.5. Hooke-Jeeves pattern search algorithm (HJ)

The pattern search algorithm developed by Hooke and Jeeves is a type of derivative-free optimization method that can optimize non-continuous and non-differentiable functions. It finds the best match by tracking the behavior of the objective function using a series of exploratory moves as a point-to-point transition without starting from scratch at each new point [134]. Pattern search algorithm benefits from low computational time compared to other algorithms. Khan and Spitler [162] applied the Hooke-Jeeves search algorithm to optimize the design of a GSHP system using the GenOpt tool. Zhang et al. [163] also used it for this purpose. They found that the optimization methodology using HJ can suitably provide an appropriate tool to achieve the best BHE design parameters in GSHP. However, it is still less effective than other derivative methods. A comparison of the Hooke-Jeeves algorithm with the genetic algorithm showed better performance for GA in all comparison cases [135]. Nevertheless, Machairas et al. [37] pointed to the higher robustness of HJ compared to noisy functions when analytical derivatives are not available; or when finite difference approximations for the gradient are unreliable.

#### 6.4.6. Taguchi's method

The Taguchi method is a new technique of optimization. It is based on the design of experiments to determine the best combination of parameters [140]. This method uses a set of orthogonal arrays to arrange the variable parameters at different levels with a minimum number of experiments. The signal-to-noise ratio (S/N) is evaluated during the process for all parameter levels, where the maximum S/N value indicates the optimal level. Taguchi is one of the best tools to improve an objective, especially in product development and industrial engineering fields [164]. However, its disadvantage comes from its limitation to improve multi-objective functions [140]. A limited number of studies on Taguchi's method for improving GSHP design parameters have been reported [140,149,165].

Table 9. Summary of studies focused on the optimization of vertical heat exchanger design.

Reference	Objective function		Design variables	Constraints		Optimization method/software		
				Parameter	Min		Max	
Sanaye and Niroomand [156] <sup>a</sup>	Single	TAC	$D_p$	$T_{in}$ (heating mode)	0°C		NM, GA/ optiGA tool	
			$T_{in}$	$T_{evap}$ (heating mode)	-50°C			
			$T_{out}$	$T_{evap}$ (cooling mode)	-50°C			
			$T_{evap}$	$T_{wi} - T_{evap}$	10°C			
			$T_{cond}$	$T_{cond} - T_{wi}$	10°C			
Khalajzadeh et al. [142]	multiple	$\eta$	$L_b$	$\frac{L_b}{D_b}$	120	600	—/Design-Expert software	
			$\theta$	$D_p$	$\frac{D_p}{D_b}$	0.2		0.3334
			$T_{in}$	$\frac{T_{in}}{T_g}$	1.75	2.5		
			Re	Re	3200	9600		
Li and Lai [127]	Single	EGN	$L_b$	—			Calculation based/—	
Bayer et al.	Single	Change in	$N_b$	—			linear programming /—	

[124]		ground temperature	$s_b$	Thermal loads			
Robert and Gosselin [126] <sup>a</sup>	Single	LCC	$L_b$	$L_b$	45m	105 m	Fast Fourier Transform/MATLAB
			$s_b$	$s_b$	3m	8m	
			$N_b$	P	60%	90%	
			size of HP	$\frac{Q_{field-peak}}{N_b L_b}$	30	130	
Huang et al. [128]	Single	EGN	$N_b$	$N_b$	1		GA/ MATLAB
			$L_b$	$L_b$	50m	200 m	
			$r_b$	$r_b$	0.0325m	0.1 m	
			$r_p$	$r_p$	0.012m	0.022m	
			$m_f$	$m_f$	0.1 kg/s	1 kg/s	
				$\lambda_g$	0.5 w/mk	2.5 w/mk	
				$\lambda_p$	0.2 w/mk	0.6 w/mk	
				$\lambda_s$	0.5 w/mk	2.5 w/mk	
				Initial soil temperature	10°C	20°C	
Retkowski and Thöming [161]	Single	$\frac{TAC}{COP}$	$N_b$	—			MILP/ Excel
			$L_b$				
			$m_f$				
			Type of HP				
			Number of HP				
Sivasakthivel et al. [140]	Single	$L_b$	$r_b$	—			Taguchi method, utility concept/ —
		COP	$r_p$				
		$R_b$	$s_p$				
			$\lambda_g$				
			$\lambda_p$				
			$m_f$				
			$T_{in}$				
			Heating load				
GAMAGE et al. [123] <sup>c</sup>	Single	NPV	$N_b$	$N_b$	4	144	Monte-Carlo model/—
			$L_b$	DR	1	9	
			$s_b$	$\frac{s_b}{L_b}$	0.05	1	
				$\ln \frac{t}{t_s}$	-2	3	
Huang et al. [116]	Multiple	EGN	$N_b$	$N_b$	1		GA/ MATLAB
		Initial cost	$L_b$	$L_b$	50 m	200 m	
			$r_b$	$r_b$	0.0325m	0.1 m	
			$r_p$	$r_p$	0.012m	0.022m	
			$m_f$	$m_f$	0.1 kg/s	1 kg/s	
				$\lambda_g$	0.5 w/mk	2.5 w/mk	
				$\lambda_p$	0.2 w/mk	0.6 w/mk	
				$\lambda_s$	0.5 w/mk	2.5 w/mk	
				Initial soil temperature	10°C	20°C	
Zhang et al. [163]	Single	Temperature function	$L_b$	$L_b$	45 m	105m	HJ/—
			$s_b$	$s_b$	3 m	8 m	
			$N_b$	$N_b L_b$	$\frac{Q_{field-peak}}{130}$	$\frac{Q_{field-peak}}{30}$	
Park et al. [132]	multiple	LCC	$L_b$	$L_b$	85 m	200 m	NSGA-II/ Multiopt2
		Temperature function	$s_b$	$s_b$	4m	7m	
			$N_b$	$N_b$	35	45	
Ma and Xia [125]	Single	Energy consumption	$T_{out}$	$T_{out}$ (cooling mode)	6°C		—/ model-based approach
				$T_{out}$ (heating mode)	20°C		
Pu et al. [157] <sup>d</sup>	Multiple	EGN	$D_b$	$\frac{D_p}{D_b}$	$\frac{1}{15}$	$\frac{4}{15}$	MOGA/ TRNSYS
		IEF	$D_p$	$\frac{s_p}{D_b}$	$\frac{1}{6}$	$\frac{1}{3}$	
			$s_p$	$\frac{T_{in}}{T_g}$	1.75	2.5	
			$m_f$	Re	994	39769	

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$$\frac{T_{in}}{Re}$$

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$$v$$

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<sup>a</sup> $T_{wi}$ : the inlet temperature to the heat pump from the building;  $T_{cond}$ : condensation temperature;  $T_{evap}$ : evaporation temperature.

<sup>b</sup> $P$ : Percentage of the building peak load.

<sup>c</sup> $DR$ : distribution ratio= the number of boreholes in the longer direction over the number of boreholes in the other direction,  $t_s$ : the characteristic time  $L^2/9\alpha$  where  $\alpha$ : the thermal diffusivity of soil.

<sup>d</sup> $IEF$ : integrated evaluation factor,  $v$ : inlet flow velocity.

## 6.5. Developed optimization scheme

Figure 12 summarizes the steps of the proposed design strategy for energy piles basing on a global optimization approach.

Journal Pre-proof

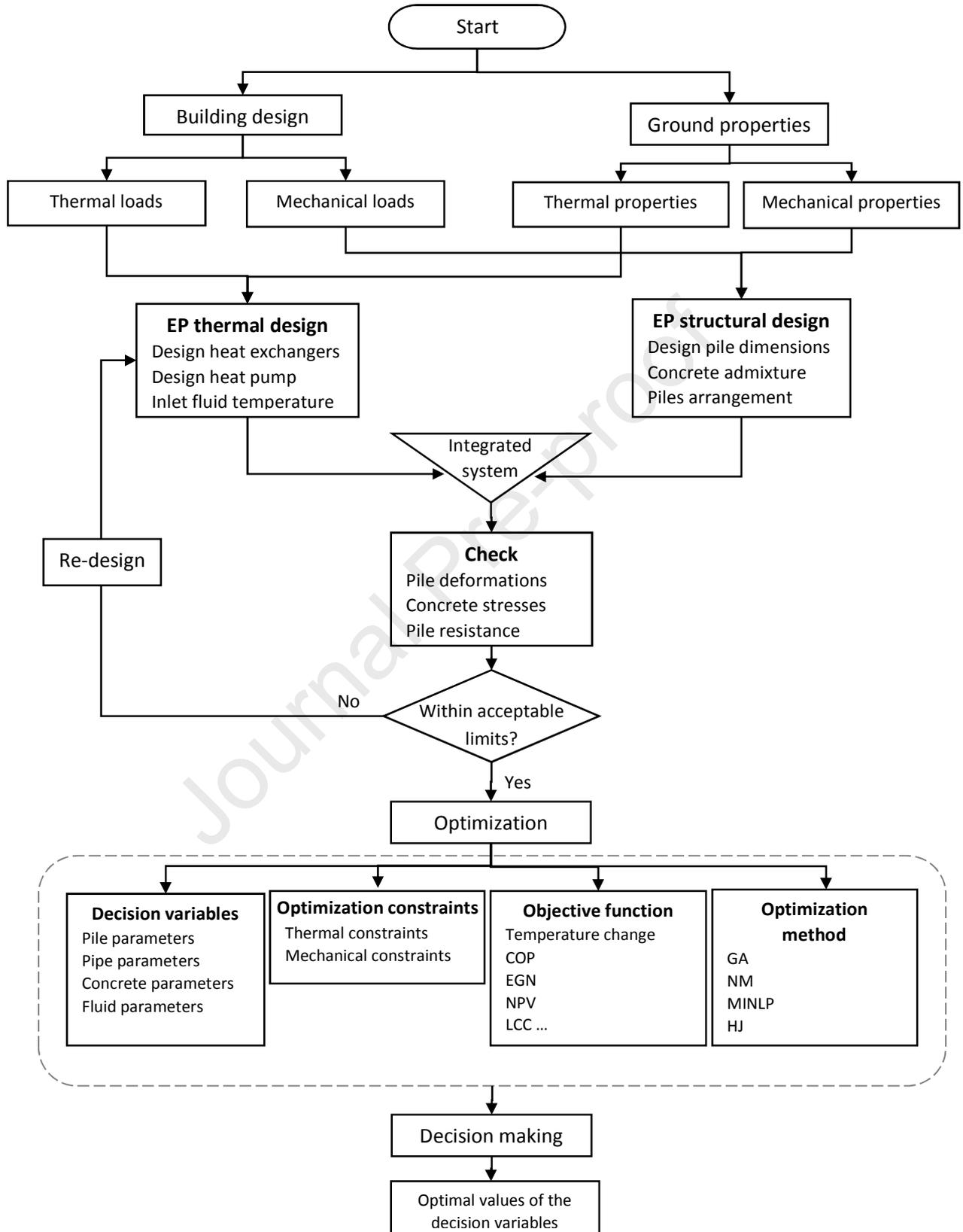


Figure 12. The developed optimization approach for energy piles design

## 7. Conclusions

While the thermal analysis of borehole heat exchangers is specified, and their design and dimensions can be controlled to meet thermal requirements and establish the optimal system, the design of energy piles is a complex matter derived from the interaction between thermal and mechanical loads. A comprehensive understanding of all design aspects of energy piles is required, and developing an optimization strategy is still needed. This review has the purpose of filling the gaps regarding these aspects. It represents the current state of knowledge about the analysis methods used for energy piles, investigates the thermal and thermo-mechanical behaviors of these systems, summarizes the 4E-G evaluation criteria, and presents an overview of optimization methods that can be applied to such systems. Finally, it proposes a comprehensive strategy for design and optimization of energy piles, considering thermal, economic, environmental, and mechanical perspectives. Some important conclusions can be stated:

- Numerical modeling is recommended to simulate energy piles due to their high accuracy in detecting the thermal and thermo-mechanical response of these systems. However, experimental and numerical benchmarking validations are necessary for the assumptions and simplifications used in the literature to reduce the high computational time taken by a full numerical model. The heat flow should also be addressed to consider the actual thermal behavior of energy piles.
- The thermally-induced changes of stresses and strains in energy piles depend strongly on the pile fixity and can reach critical values if the restraint conditions are not correctly defined. Therefore, integrating the real restraint conditions into the modeling is still necessary to detect the actual design of energy piles at different restraint levels. They also depend on the percentage of mechanical loads applied to the foundation where irreversible settlement can occur for axial mechanical loads exceeding 30%–40% of the ultimate resistance.
- The maximum internal stresses of perfectly restrained piles can be a conservative limit to check the thermally-induced stresses of a single energy pile. However, the maximum displacement of completely free piles is not a safe constraint to check pile movements, especially where the soil-to-pile thermal expansion ratio is large. For a group of piles, the use of these limits is not useful. A complex thermo-mechanical analysis is therefore required to provide safe criterion constraints for single energy pile and pile groups under the ultimate and service limit states.
- The response of a group of energy piles depends on various variables influencing the interaction between piles, such as pile spacing, the soil-to-pile thermal expansion coefficient ratio, and the pile stiffness. However, more information is still needed to determine the effect of these variables on the behavior of both active and non-active piles. Besides, detecting the best positions and number of active energy piles in a foundation is an important target that should be investigated.
- The heterogeneity of the concrete mixture can have a sensitive effect on the thermal cracks induced in cement-based materials due to the contraction and expansion of energy piles. A mesoscopic approach is therefore recommended integrating the thermally-induced cracks of concrete into modeling to study their effects on the real mechanical behavior and the long-term thermal performance of energy piles.

- The efficiency of heat transfer in an energy pile depends on the design parameters concerning the characteristics of the pile, pipe, concrete, fluid, and ground. The configuration of heat exchanger pipes is found to be the most influential parameter. Adding thermally enhanced materials to the concrete mix can also improve the thermal performance of concrete by 40%. However, it should be accompanied by structural and economic feasibility studies to maintain the typical compressive strength of concrete and to ensure the cost-effectiveness of the structure.
- To create an optimal geometry for heat exchangers in an energy pile with U-/W- or spiral configuration, it is recommended to set a minimum shank spacing/pitch size of 250 mm to prevent thermal interactions between the adjacent pipe loops. It is also recommended to attach the GHE pipes to the pile reinforcement cage, which minimizes the high thermal resistance of the concrete cover.
- The development of an optimal energy pile system involves complex analyzes. It comprises the selection of objective functions, the detection of decision variables and system design constraints, then the best optimization method. GA proves to be the most popular optimization method, but MINLP proves to be more efficient, more stable, and faster than GA.
- The number of heat exchanger pipes, the mass flow rate, the thermal conductivity of grouting material, and the inlet fluid temperature are the most common decision variables reviewed in previous studies. However, a wide-ranging study on structural parameters is also suggested.
- Multi-objective optimization of energy piles, including the 4E-G assessments (energy, exergy, economy, environment, and geo-structure) can be a vital objective for future studies.

## Acknowledgments

The authors would like to thank the Association of Specialization and Scientific Guidance (ASSG), the Agence Universitaire de la Francophonie (AUF), the National Council for Scientific Research of Lebanon (CNRS-L), and the Erasmus+ Programme for their financial support.

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**Declaration of interests**

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

The authors declare the following financial interests/personal relationships which may be considered as potential competing interests:

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