

Novel PDMS based Semi-Interpenetrating Networks (IPNs) for the extraction of phenolic compounds

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Abstract:

Four Semi-Interpenetrating Networks (semi-IPN) based on polydimethylsiloxane (PDMS) were developed for the sorptive extraction of polar phenolic compounds ($\log K_{ow} \leq 3$). Their preparation is based on the hydrosilylation crosslinking reaction of dihydrosilane terminated polydimethylsiloxane with its homologue divinyl, followed by the addition of inert various polyethylene oxide derivatives (PEO). The physico-chemical properties of the semi-IPN were controlled by Differential Scanning Calorimetry (DSC), Scanning Electronic Microscopy (SEM), RAMAN spectroscopy and contact angle measurements, showing the homogeneity of the semi-IPN and their higher hydrophilicity. Under optimum extraction conditions of phenolic molecules as target analytes and using liquid chromatography as analysis techniques, the novel modified PDMS phases showed good extraction rate against polar analytes with an excellent relative recovery average (69-100%) for phenolic molecules. The higher retention rates were obtained with 30% interpenetrated copolymer PEO/PPO in PDMS. Moreover, five adsorption/desorption cycles led to a loss of 5.8 % of the adsorption efficiency, showing a good stability of these PDMS-based IPN phases.

Keywords: PDMS phase, PEO derivatives, semi-IPNs, extraction, reusability, phenolic molecules.

Introduction

Organic pollutants which are originally derived from domestic, industrial and agricultural activities are increasingly released into the wastewater leading consequently to the contamination of the soil and the environment. Among the common contaminants which are strongly dispersed in aquatic environment, we can note phenolic compounds or pesticides namely known for their intolerable toxicity [1-3]. On the other hand, the continuous population growth and therefore the anthropogenic activity increase will result in much more important chemical and organic substances release into the environment which can critically threaten the fauna and flora and most specifically humans. For this purpose, the research community is more and more focused to develop robust, low cost and environmentally friendly processes capable of removing pollutants from water and at the same time to safeguard the health of affected populations.

Among various extraction technologies the extraction process based on solid adsorbents have been widely adopted [4] and is the most popular treatment up to date since it is known as an environmental friendly method compared to solvent-based extraction and also because of convenience, ease of operation and simplicity of design. Such process is based on specific solid phases since the removal performance of analytes relies on the affinity of both adsorbent phase and the own character of each contaminant. Phenolic compounds were extracted using different types of materials, especially for analytical purposes (coupled with ultra-high performance liquid chromatography (HPLC) or gas chromatography (GC) with different types of detectors). Solvent impregnated agarose gel was used for microextraction of phenols [5] and polyacrylate coated silica fibers were used for the extraction of chlorinated phenols and nitrophenols [6]. PDMS (polydimethylsiloxane) materials is the king of the adsorbent phases for solid-phase micro-extraction (SPME) and stir bar sorptive extraction (SBSE) formats [7,8]. The main choice of PDMS phase is intimately related to its exceptional properties: a high hydrophobicity, a high flexibility allowing a high deformation ability to easily adopt various shapes, an UV and thermal stability, a low toxicity, a versatile cross-linking chemistry and a high gas permeability [9-11]. The hydrophobicity of PDMS enables high extraction rate

of hydrophobic compounds. However, since the extraction of polar molecules is more difficult due to the strong interactions of these compounds with water molecules in aqueous solutions, therefore, the co-extraction of polar and non polar phenols by PDMS phases is challenging. Different chemical groups were introduced in the PDMS network to overcome the limitations of PDMS for the polar compounds: β -cyclodextrin [12], divinylbenzene [13], polyvinylalcohol [14]. In the present work, novel PDMS materials based on the insertion of various PEO (polyethylene oxide) derivatives were designed as novel solid adsorbents with better affinity for phenolic molecules. PMDS semi-IPN (inter-penetrating) phases were elaborated from two commercial PDMS chain precursors followed by the addition of various PEO (polyethylene oxide) derivatives as polymer modifiers (PM). After their physico-chemical characterization, the extraction efficiency of the novel PDMS compounds, grounded as a powder form (diameter < 1 mm) were determined for a series of phenolic target with different polarities ($\log K_{ow} \leq 3$). Their recyclability was also tested.

Experimental part:

1 – Research Methodology

A flowchart of the research methodology is presented in Figure 1.

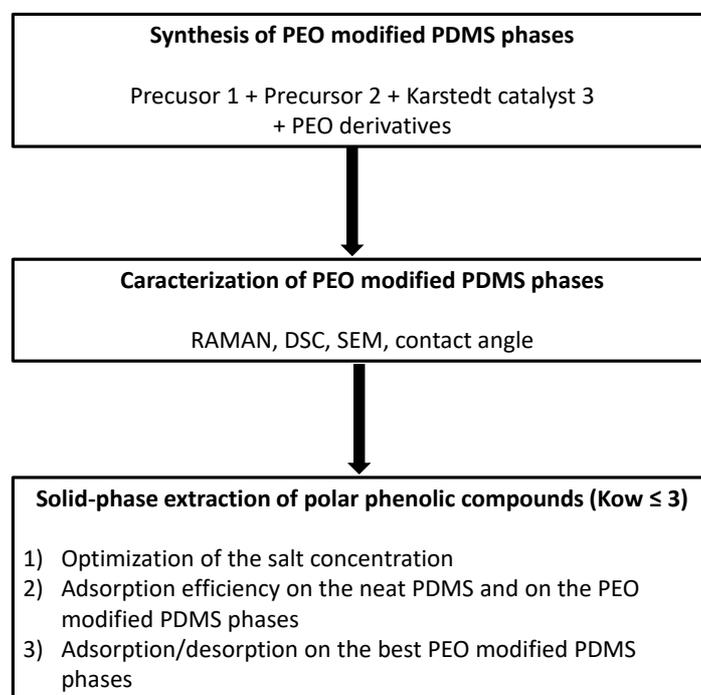
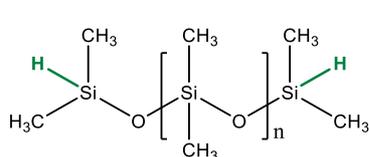


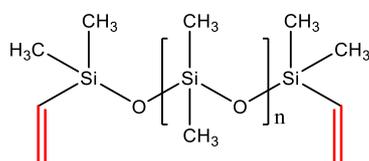
Figure 1. Flowchart of the research methodology

2- Reagents & Materials:

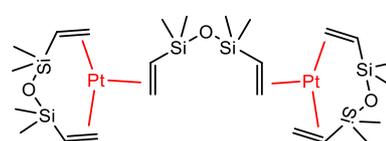
- Two kinds of PDMS precursors chains (RTV3428A & RT3428VB) were used in this study and supplied, from Elkem Silicones, in oil form. The composition and the chemical structural characterization of each precursor have been, previously, accomplished using several techniques (NMR, Maldi TOF, DSC and SEC) [15]. As shown below, the first transparent oil material RTVA (**Precursor 1**) is the dihydrosilane-terminated PDMS (average molecular weights or $M_n = 16.700$ g/mol, Polydispersity or $PD = 2.01$) and the second one with red rust color ($M_n = 18\ 200$ g/mol, $PD = 3.27$) is an oil composed from a combination between divinyl-terminated PDMS (**Precursor 2**) and **Karstedt catalyst 3** (0.5-1ppm) which is necessary for the crosslinking process.



Precursor 1

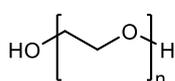


Precursor 2

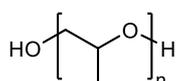


Karstedt catalyst 3

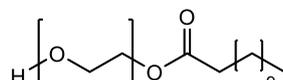
- Four types of poly(ethylene oxide) (**4-7**) (PEO derivatives) were supplied from Sigma Aldrich as polymer modifiers.



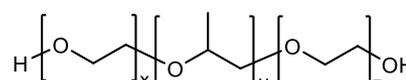
PEO (400 g.mol⁻¹)
4



PPO (400 g.mol⁻¹)
5



PEO Laurate (400 g.mol⁻¹)
6



Breaker 2 (1750 g.mol⁻¹)
7

- p-hydroxy benzoic acid ($\geq 99\%$), caffeic acid ($\geq 95\%$), ferrulic acid ($\geq 98\%$), benzoic acid ($\geq 99.5\%$), anisic acid ($\geq 98\%$), toluic acid ($\geq 98\%$), p-chlorobenzoic acid (99%), eugenol (99%), t-anethol (99%) were used as target analytes (phenols's class) and were purchased from Sigma Aldrich, France. Phosphoric acid ($\geq 85\%$), HPLC grade acetonitrile and methanol were also purchased from Sigma Aldrich, France. Sodium Chloride (99.9%) was purchased from Fischer Scientific (France).

Characterization methods

Raman Rxn1 spectrometer (Kaiser Optical Systems, Ann Arbor, USA), equipped with a thermoelectrically cooled CCD detector, was used in combination with a fiber optic sapphire immersion probe. The laser wavelength was 785 nm. All spectra were recorded at a resolution

of 4 cm¹ in the spectral window from 150 to 3480 cm¹. Data collection was controlled using the HoloGRAMS™ software. Acquisition time was 5 s and five spectra were cumulated. For each sample analyzed, spectra acquisition was reiterated 3 times.

Differential Scanning Calorimetry (DSC) thermograms were obtained by using a METTLER TOLEDEO DSC882e Differential Scanning Calorimetry. The scanning temperature was performed from -140 °C to 50 °C using a heating rate of 10 °C/min under nitrogen atmosphere.

Scanning electron microscopy (SEM) images were realized by using a VEGA TESCAN SEM.

Water contact angle (WCA) measurements were carried out using a Dataphysics Digidrop contact angle meter equipped with a CDD2/3 camera with the sessile drop method and by using Milli-Q quality water as probe liquid. The tabulated results are the average of at least five measurements on different parts of each sample.

3- Preparation of solid phases based on PDMS material

3-1- Neat PDMS phase 8 (conventional PDMS phase)

Neat networks were prepared based on the formulation provided by Elkem silicones with a ratio of (10:1) of dihydrosilane terminated PDMS **1** as bifunctional linear network chain and divinyl-terminated PDMS **2** as a crosslinker. The hydrosilylation reaction was catalyzed by a platinum complex (Karstedt catalyst) **3** which is already diluted on divinyl-PDMS **2** as received. These precursors were thoroughly mechanically mixed for 10 min at 110°C until caking and then the mixture was kept for curing for 24 h at 110 °C. The resultant neat PDMS **8** was obtained as a rigid elastic material with color of red rust.

3-2- Novel modified PDMS phases 9-12

The novel modified PDMS phases **9-12** were prepared through a reaction mixture of **1** and **2** with a ratio of (10 :1), as for phase 8, by the addition of different percentages (10, 20 and 30%) of polymers modifiers **4-7** (Table 1). To ensure the total interpenetration of these polymers modifiers through the crosslined chains, the synthesis was carried out as follows: the PEO derivative was firstly diluted in the dihydrosilane terminated PDMS **1** and homogenously mixed together at 110°C for nearly 10 min. After cooling at room temperature, the second crosslinker **2** was added to the precursors and the mixture was manually mixed at 110°C until caking. The resulting materials named as semi-interpenetrating polymer networks

(semi-IPNs) were allowed to cure at 110°C for 24 h. All of them provided rigid elastic networks **9-12** with red rust colors.

Table 1: Composition of the neat PDMS and the modified PDMS phases

Neat PDMS	1+2+3			
PM	4	5	6	7
Modified PDMS	9	10	11	12

3-3- Homogeneity and miscibility study

Before testing the prepared semi IPN phases as adsorbents, it is crucial to verify the complete polymerization of the PDMS, regardless the nature of the PM; this point was verified by RAMAN spectroscopy and by GPC. The miscibility of the resulting networks was verified by DSC and by SEM. In fact, The immiscibility between Polymer Modifier (PM) and the PDMS can lead to PM aggregates which is obviously not the required result. In fact, it was reported that Differential Scanning Calorimetry (DSC) is the most frequently and widely used technique to investigate the miscibility of polymer modifier inside the semi-IPN [16-18]. A widely accepted criterion of miscibility in a polymer blend is the disappearance of the glass transition temperature of the two peaks corresponding to both phases (i.e the polymer modifier and the original PDMS) present in the blends.

4- Shaping of PDMS phases (8-12)

The neat PDMS 8 as well as the semi-IPNs PDMS 9-12 were ground to the required size (<1 mm, selected through a stainless steel sieve with diameter of 1.00 mm) using a Cryogenic Grinders, in order to maximize the contact surface with pollutants on further analysis and extraction experiments (Figure 2(b)).

5- Preparation of the aqueous solutions of the phenolic compounds:

The aqueous solutions containing the phenolic molecules were prepared in distilled water at concentration 1 ppm (1 mg/L). Doped solution containing the target polyphenols: After weighing the exact mass of each solid phenolic compound in aluminum capsules, it was successively introduced into a vial of 1L and then filled with distilled water. The pH of the aqueous solution was adjusted to 2 by the addition of 2 mL of phosphoric acid. The mixture was kept under agitation for 24 h in order to ensure a total dissolution of all solid phenols.

6- Extraction procedure

In order to test the extraction efficiency of each developed PDMS phase, we firstly started by studying the optimum conditions for a maximum recovery of the target molecules. For this purpose, several doped aqueous solutions (phenols) with the addition of salt (as matrix modifier) and the elaborated PDMS phases (with various percentages of PM) were prepared.

- Preparation of samples used for the salting-out effect study:

The corresponding solutions were prepared as follows: in a vial of 20 mL, 60 mg of neat PDMS phase **8** was introduced with the addition of 10 mL of solutions containing the target phenolic compounds and different percentages of sodium chloride: 0%, 10% and 30%, respectively. All solutions were deposited on a magnetic multistirrer and kept under constant agitation (900 rpm) for different durations: 1 hour, 5 hours and 24 hours. After each time interval, a sample volume of 0.5 mL was taken from each solution and filtered with a 0.45 μm PTFE filter and subsequently analyzed by HPLC /DAD technique (wavelength: 210 nm). The HPLC system and the analytical conditions were described in more detail in previous work [19]. The adsorption efficiency is calculated according to Equation 1.

$$\text{Adsorption efficiency} = \left(\frac{C_i - C_t}{C_i} \right) * 100 \quad (1)$$

Where C_i : initial concentration (mmol l^{-1}), C_t : the residual concentration of the pollutant at time t .

Results and discussion

1- Preparation of novel solid adsorbent phases based on PDMS

In this work, it is intended both: to prepare a PDMS network **8** (Neat PDMS) to be used as adsorbent phase for extraction process and to incorporate polymer modifiers (PEO derivatives **4-7**) into the PDMS network to obtain novel PDMS solid adsorbents phases. The neat PDMS as well as the novel elaborated phases will be tested as adsorbents and the added value of the PM will be studied.

The most important reason for the use of PEO derivatives **4-7** as polymer modifiers is due to their polarity which can ensure a higher affinity to polar analytes. However, the mass of the modifying polymer is a crucial parameter involved in the extraction efficiency of the

adsorbent phase. Therefore, an optimization study was carried out based on an optimum of extraction of several modified PDMS phases elaborated using different percentages (10 %, 20 % and 30 %) of each PEO derivatives.

The incorporation of these linear PM into the PDMS network have been performed in-situ, as it was detailed in the experimental part, leading to a new class of PDMS semi-Interpenetrating Networks. The obtained materials **9-12** can be described as a polymeric network consisting on cross-linked chains having nodes originated from the hydrosilylation reaction [20-22] of the vinyl end with the hydrosilane end of the corresponding PDMS precursor (**1**) between which linear chains of PEO derivatives **4-7** are interpenetrated as schematically illustrated in Figure 2(a). [23-25]. The disappearance of the Si-H bond was monitored by RAMAN spectroscopy. The corresponding band at 2120 cm^{-1} (Si-H terminal) decreases during 120 min at 20°C and then stabilizes (Figure 3), regardless the percentage of PM. The reaction time decreases when the temperature is higher.

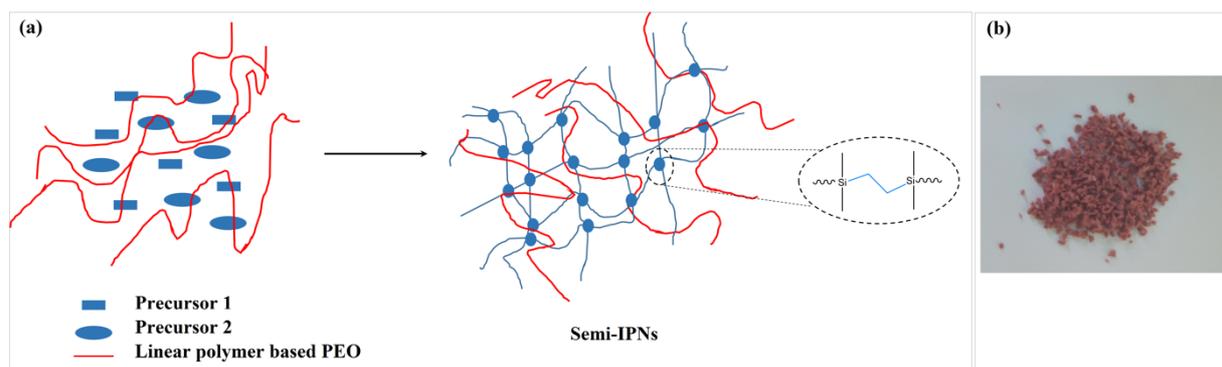


Figure 2. (a) Schematic presentation of PDMS Semi-IPNs (b) The resulting powder after (diameter <1mm)

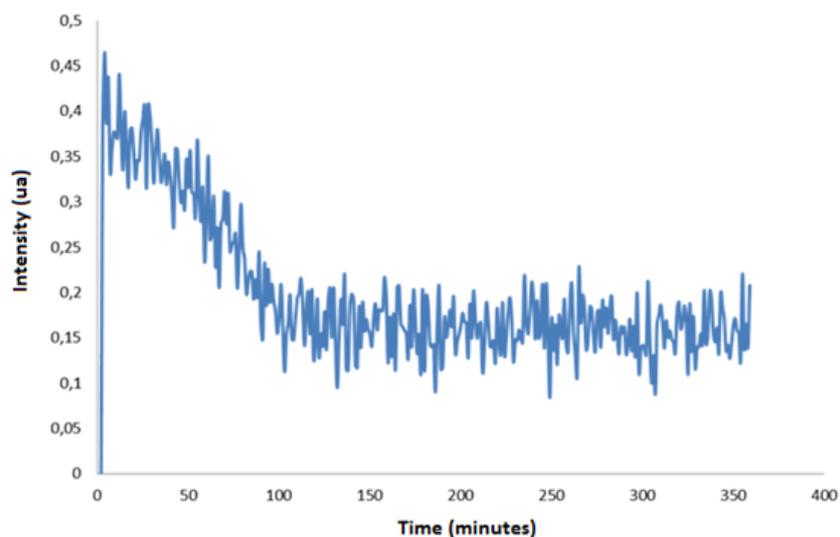


Figure 3. Monitoring of the terminal Si-H bond by Raman spectroscopy.

DSC was used to control the miscibility of polymer modifier inside the semi-IPN. The glass transition temperatures obtained for the PEO-derivatives (4-7), neat PDMS (8) and semi-IPNs (9-12) are presented in Table 2.

Table 2. Glass transition temperatures (T_g) of Neat PDMS (8), semi-IPNs phases and their corresponding polymer modifiers

PM and Semi-IPNs phases	T _g (°C)
A) PDMS (8)	-117
PM (4)	-63
Semi IPNs (9)	-81
B) PDMS (8)	-117
PM (5)	-75
Semi IPNs (10)	-97
C) PDMS (8)	-117
PM (6)	-76
Semi IPNs (11)	-99
D) PDMS (8)	-117
PM (7)	-67
Semi IPNs (12)	-85

From the results presented in Table 2, neat PDMS presents a thermal transition temperature at $-117\text{ }^{\circ}\text{C}$, which is close to the experimental value reported in the literature [26]. For the modifier polymers, the T_g values of the PEO (4), PPO (5), PEO-monolaurate (6) and Breaker (7) are found to be at -63 , -75 , -76 and $-67\text{ }^{\circ}\text{C}$, respectively. These values are in accordance with the T_g reported in the literature [26-27].

In addition we have observed that the T_g value of the neat PDMS is different and lower than the values of T_g s obtained from DSC results of the semi-IPNs phases (9-12). An effective entrapment of PEO derivatives chains in PDMS network might inhibit their mobility in the structure. Therefore, the segmental motion of polymer chains is inhibited leading to increase glass transition temperature [28]. Therefore, the presence of a single T_g indicates the perfect miscibility and homogeneity between PDMS and the PEO-derivatives polymers. These clearly confirm that these results arose from the existence of homogenous, miscible and highly crosslinked three dimensional semi-interpenetrating networks.

SEM images of neat PDMS and of modified PDMS phase 12 are presented in Figure 4. A total homogeneity of the surface of both PDMS phases, without any agglomeration in modified PDMS phase 12.

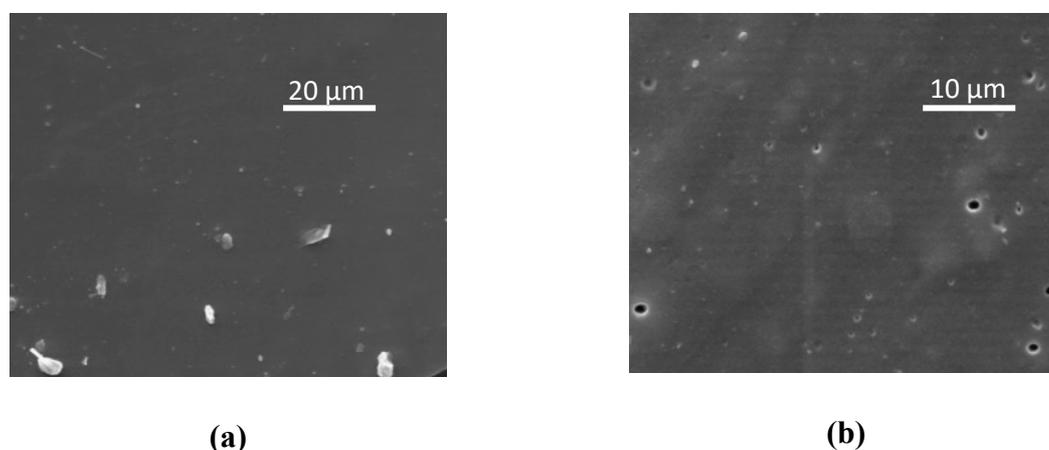


Figure 4. SEM images of (a) neat PDMS (b) modified PDMS phase 12

The contact angles measured with water, on neat PDMS and on modified PDMS phase 12 surfaces are presented in Figure 5. The wettability of the modified PDMS phase 12 is highly improved by the insertion of Beaker 2 (30%) which will then improve the adsorption of more polar phenol compounds.

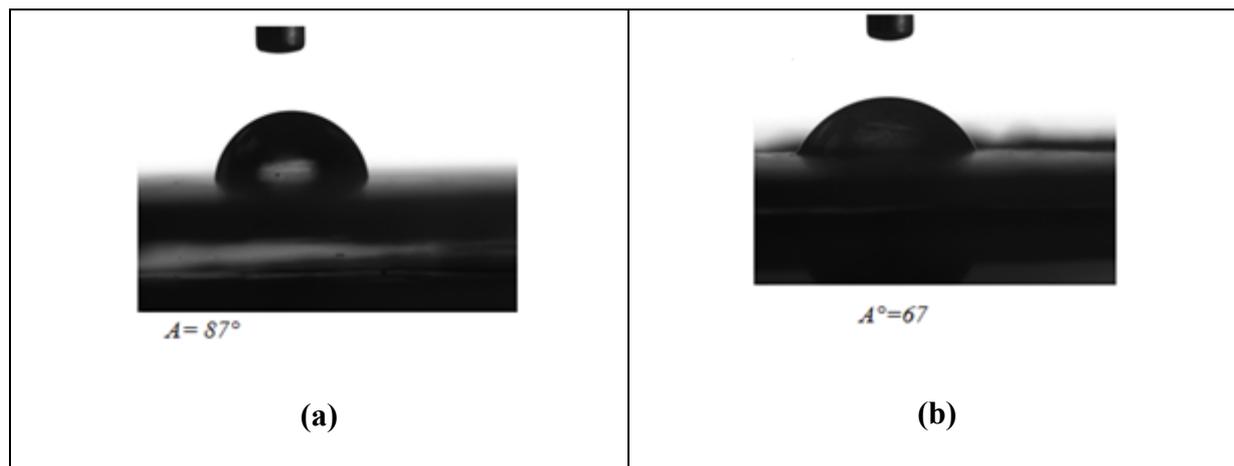


Figure 5. Contact angle measurements of water on (a) neat PDMS (b) modified PDMS phase 12 surfaces.

2- Extraction procedures

The high polarity of specific contaminants in water is considered as the main problem of a limited extraction capacity of conventional extraction techniques (eg, SBSE or SPME techniques) basing on neat PDMS [8]. As it can be seen in Figure 6, series of phenols compounds; as target analytes, (used for the preparation of doped aqueous solutions) the decreasing of the logarithm of the octanol/water partition coefficient (Log Kow) indicates a more hydrophile character of these molecules (eg, 4-hydroxybenzoic acid, caffeic-acid) and consequently an opposite affinity with PDMS solid phases.

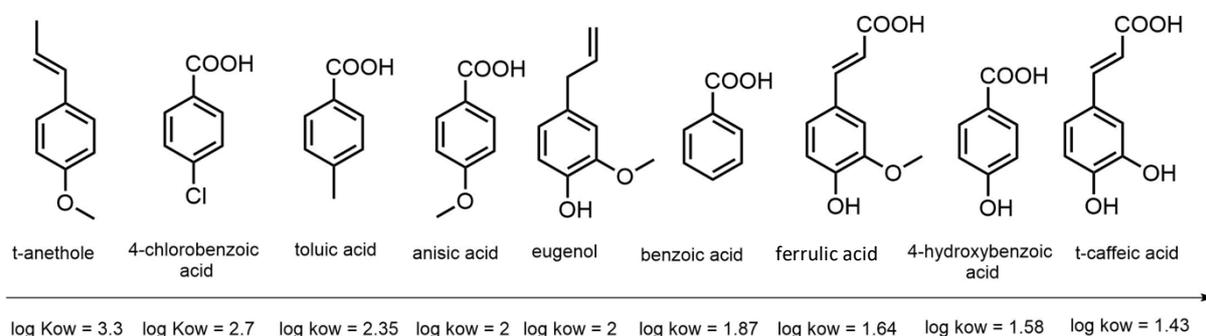


Figure 6. Chemical structures and log Kow values of the targeted phenolic analytes.

HPLC-DAD was used for the detection of these phenolic compounds with an initial concentration of 1 ppm. The figure of merit for all the target molecules is the following one: LOD 0.1 ppm, LOQ 0.5 ppm, linear range 0.1 ppm to 200 ppm, RSD 1 %.

2-a- Extraction of the phenolic compounds as target molecules:

Effect of the salting out of the phenolic compound solutions on the extraction rate

The salting-out effect is commonly used to maximize the extraction efficiency in analytical procedures by adding salt to water samples [29]. In fact, the addition of inert salts would enhance the transfer of polar analytes towards the acceptor phase by decreasing the solubility of these analytes in the aqueous sample solution. This study of the salting-out effect on the prepared solutions of the phenolic compounds with higher polarities (Figure 6) was conducted with the neat PDMS (phase 8).

A first extraction test was carried out using solutions without sodium chloride as reference. Then two subsequent extraction tests were performed following the addition of 10% and 30% NaCl, respectively. After repeating 3 times each extraction experiment, an RSD was found to be 5%.

The results, shown in Figure 7, indicate that the adsorption efficiency, obtained for salt free solution, of polar molecules (p-hydroxy, caffeic, ferrulic, and benzoic acids) does not exceed 10% compared to non-polar ones which can reach nearly a yield of 100% (t-anethol). However, the addition of 10% of sodium chloride slightly increased the adsorption efficiency of both polar and non polar molecules. Moreover, the addition of 30% of sodium chloride can improve remarkably the adsorption efficiency which reached up to 60 % for the ferrulic acid case whereas it was less than 20% with the addition of 10% of NaCl.

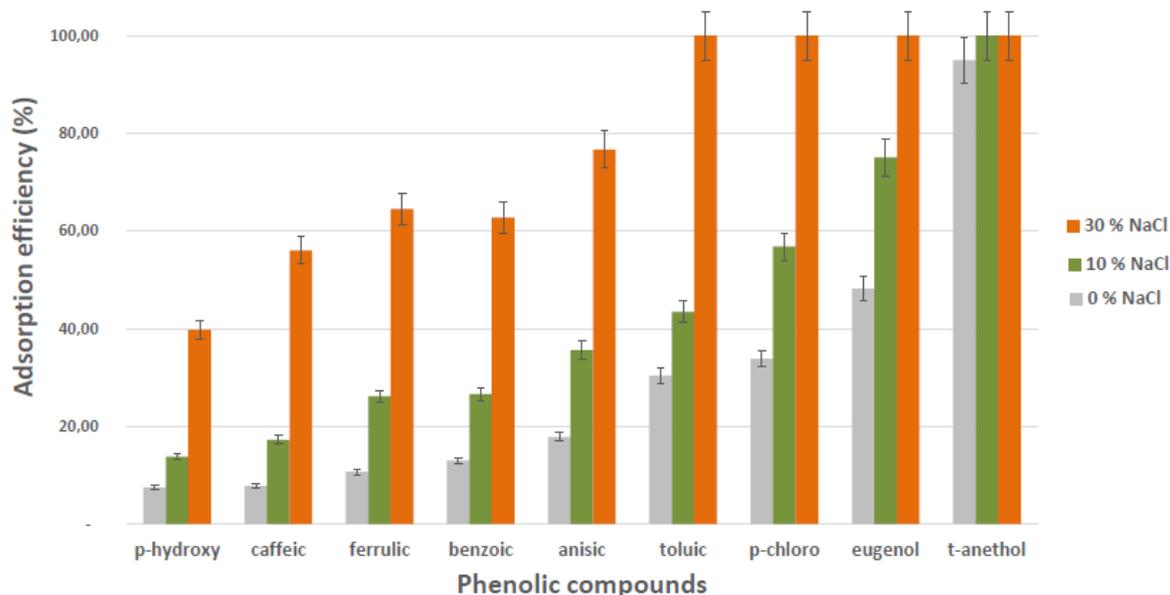


Figure 7. Salting-out effects obtained in NaCl solutions with PDMS (8) – Time of equilibration: 5 h

From the salting-out effect study, it can be concluded that even though the use of the neat PDMS **8** (solid phase), the addition of 30% of sodium chloride has allowed a significant modification of the ionic strength of the solutions resulting in a reduced solubility of these components in water and consequently an efficient transfer of polar analytes from the aqueous solution to the sorptive phase. All the following extraction experiments will be performed using the different phases, the phenolic compound solutions will contain 30% NaCl in order to maximize the adsorption efficiency of the polar molecules as it was revealed previously.

Effect of the structure and of the percentage of PM on the adsorption efficiency

An extraction optimization was carried out for all prepared PDMS solid phases: **8** (neat PDMS phase considered as reference) and **9-12** (table 1), neat PDMS with the addition of diverse amounts of polymer modifiers (20% and 30%). A kinetic study was carried out by varying the equilibrium durations from 1 h up to 24 h. After repeating 3 times each extraction experiment, the RSD was found to be 5%. The adsorption efficiency of these novel PDMS phases and the determination of the optimum parameters were assessed by calculating the recoveries from aqueous solutions doped with the target compounds. From the preliminary results of phenol adsorption (Table 3) it has been marked that:

- The highest adsorption efficiency of the phenol molecules was obtained with the addition of 20 and 30% of PM in the PDMS phase. However a further increase in the amount of the PM

does not improve the adsorption efficiency and, on the other hand, the linear PEO chains are found to be excluded from the network.

- The obtained adsorption efficiency after 24 h were similar to those found at 5h, therefore, only the two equilibrium durations: 1 h and 5 h were reported. This leads to conclude that equilibrium duration of 5 hours is sufficient.

Table 3: Effect of the modified PDMS phases on the adsorption efficiency (%) of the phenolic compounds for two different duration times of equilibration (1 h and 5 h)

According to the adsorption efficiency values of both polar and non-polar molecules and independently on the required time or the composition of each PDMS phase, a distinct difference can be noticed. In fact, it can be observed that in the case of the extraction of t-anethol (non polar) that its adsorption efficiency is in the range of 80-100% compared to the p-hydroxybenzoic acid (polar phenol) which shows an adsorption efficiency ranging from 4 up to 70%. In fact, this result can be expected and the non-polar molecules tend to be easily removed since they have the same affinity with the surface of the PDMS phase.

On the other hand, and focusing on the reactivity of the novel modified PDMS phases (**9-12**), it was observed that the lowest extraction rates (4-20%) were reported while using neat PDMS solid phase **8** particularly for the most polar ones (eg, p-hydroxybenzoic, caffeic, ferrulic and benzoic acids). Nevertheless, the novel PDMS phases (**9-12**) have shown a noticeable improved adsorption efficiency since their selectivity towards polar molecules were reinforced by the polar character of PEO chains. Moreover, the increase of the adsorption efficiency depends on the PM percentage added to the conventional PDMS. Indeed, in all cases the rate of the extracted phenolic compounds increases with time, however, a duration of five hours represents the optimal time which allows a maximal adsorption efficiency of all these entities to be reached. It was shown that the increase of the percentage of the PM can result in an increase of the adsorption efficiency. Thus, a presence of 30% of PM in the neat PDMS phase can allow a higher adsorption efficiency than it can be obtained by 20% of PM (**Table 3**). In order to reveal how each PM (**4-7**) added to the PDMS solid phase affects the extraction procedures, the adsorption efficiency of the various phenolic molecules were calculated under the following optimal conditions: 30 % NaCl, 5h, 30 % PM and are presented in Figure 8.

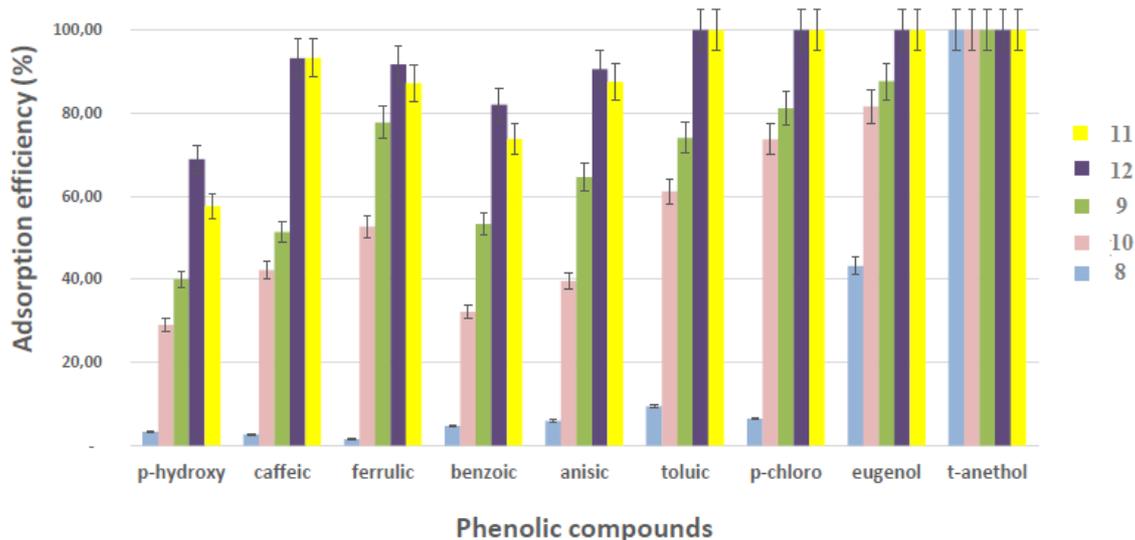


Figure 8. Adsorption efficiency of the phenolic compounds on PDMS (8) and the different modified PDMS phases (9,10,11,12) for 5 h of equilibration time.

As previously mentioned, all novel solid PDMS phases (9-12), showed a clear enhancement of the extraction of the polar and non-polar pollutants against conventional PDMS phase 8. This is mainly due to the polar character of PEO chains which can allow a better ability to extract the most polar molecules. However, if we compare the phenol adsorption efficiency of phase 9 and phase 10, respectively, it can be noted that the highest adsorption efficiency was observed when using phase 9 (with PEO as PM 4). As for example, in the case of ferrulic acid, the recovery yield obtained using phase 10 was 70 % whereas it was increased to 80% with the solid adsorbent phase 9. Although both PMs PEO 4 and PPO 5 share the same molar mass of $400 \text{ g}\cdot\text{mol}^{-1}$, their effects on adsorption efficiency was different. This difference might result on the chemical structure of the repeating unit of PPO 5 which contains a pendant methyl group responsible of its reduced polarity compared to PEO 4 leading, thus, to a lower adsorption efficiency. Based on these results, a combination of the hydrophobic character of 5 and polar character of 4 to obtain a copolymer matrix (**Breaker 2: PM7**) and its addition in PMDS phase 12 as a polymer modifier (7), was suggested. Finally, for the case of the adsorption efficiency of phase 11, using alkyl polyethylene oxide (6) as polymer modifier, this latter has in turn a similar extraction effect as 12 since they have both aliphatic and alkoxy segments which confer to the PDMS phase a most suitable affinity for polar and non-polar molecules.

Reusability cycling

Stability and reproductibility are noteworthy features of the sorbents, then it is necessary to study their regeneration and reusability. Regeneration experiments were performed by a series of successive extractions. Then, a desorption process using methanol as washing solvent, due to its polarity, low volatility and its capacity to dissolve the pollutants, was conducted. When the equilibrium was reached after 5 h of contact with the pollutants, the PDMS phases (**11** or **12**) were washed with 10 mL of methanol for 40 minutes, at room temperature. It was then washed with deionized water and dried to be reused for the next cycle. **Table 4** shows the reusability study of the two most efficient PDMS phases (**11** and **12**), for 10 consecutive cycles (adsorption/desorption).

Table 4. Adsorption /desorption cycles with the PDMS phases 11 and 12 after 5 hours of contact with the pollutants and washed with 10 mL of methanol for 40 minutes and then 5 hours of contact with the target polyphenols

The data showed that phase 11 exhibits a good stability for 6 cycles, the removal efficiency decreased 10 % compared to cycle 1 for the most hydrophilic pollutants. Although, it does not decrease for the hydrophobic ones. After 10 cycles, the adsorption efficiency of the phase 11, was not completely regenerated under the chosen regenerating conditions, especially for the most hydrophilic pollutants. However, the adsorption efficiency decreased slightly with number of cycles for the most hydrophobic pollutants from 100% to 91 or 79 % whereas it decreased more significantly for the hydrophilic molecules: it decreased from 96% to 42% for caffeic acid after 10 cycles. Nevertheless, the results presented in Table 3, show that the phase 12 exhibits a good recyclability after 10 cycles. However, the adsorption efficiency was reduced by 10 percent from the 1st cycle to the 10th cycle for all hydrophylic and hydrophobic tested pollutants.

Comparison of the adsorption efficiency of the prepared PDMS phases with those of published polymeric phases.

Table 5. Comparison of the adsorption efficiency of the prepared PDMS phases with those of published polymeric phases.

Polymeric phase	Pollutant	Adsorption efficiency	References
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		Cycle 1	Cycle 5	
Silica grafted with CTABr	4-hydroxybenzoic acid	56%		[30]
poly(ether pyridine) based on BPA	4-hydroxybenzoic acid	26%		[31]
poly(ether pyridine) based on isosorbide	4-hydroxybenzoic acid	96%	63%	[31]
PDMS	4-hydroxybenzoic acid	7 %		This work
PDMS + 30% Breaker	4-hydroxybenzoic acid	69 %	65%	This work

As presented in Table 5, 4-hydroxybenzoic acid ($\log K_{ow} = 1.58$) presents higher adsorption efficiency on 30% Breaker modified PDMS (69%), compared to neat PDMS (7%), as shown in this work. Higher adsorption efficiency was found for a biosourced poly(ether pyridine) (96%) compared to BPA based poly(ether pyridine) (26%) [31]. Lower adsorption efficiency was found for silica grafted with CTABr (cetyltrimethylammonium bromide) (56%) [30] than for a biosourced poly(ether pyridine) and for 30% PEO/PPO modified PDMS.

About the recycling of the adsorbent phases, a lost of 5.8 % of the adsorption efficiency was observed after 5 adsorption/desorption cycles for 30% PEO/PPO modified PDMS whereas a lost of 34% was observed 5 cycles for a biosourced poly(ether pyridine) [31].

Conclusion :

In this work a new class of polymer for adsorption process application based on PDMS semi-IPNs by the versatile hydrosilylation crosslinking reaction was successfully developed. They present a high homogeneity and a more hydrophilic character than neat PDMS. Under the optimal extraction conditions the novel solid adsorbent phases showed an excellent extraction performance for removing polar phenolic analytes from standard aqueous solutions. The highest adsorption efficiencies were reached with modified PDMS phases containing 30% of PM and an extraction duration of 5 h. One of the more polar compound 4-hydroxybenzoic acid was found to present an adsorption efficiency of 69% on 30% PEO/PPO modified PDMS whereas it was only 7% for neat PDMS. Moreover five adsorption/desorption cycles led to a

lost of 5.8 % of the adsorption efficiency, showing a good stability of these PDMS-based IPN phases. These phases could then be used as new solid phases suitable for SBSE and SPME devices.

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Table 3: Effect of the modified PDMS phases on the adsorption efficiency (%) of the phenolic compounds for two different duration times of equilibration (1 h and 5 h)

PDMS phases % PM (4-7)*	8**		9**				10**				11**				12**				
	-		4 (20%)		4 (30%)		5 (20%)		5 (30%)		6 (20%)		6 (30%)		7 (20%)		7 (30%)		
Extraction Time (hours)	1	5	1	5	1	5	1	5	1	5	1	5	1	5	1	5	1	5	
p-hydroxybenzoic acid	4.21 ± 0.21	6.99 ± 0.35	24.66 ± 1.23	24.24 ± 1.21	34.13 ± 1.71	34.14 ± 1.71	18.39 ± 0.92	27.04 ± 1.35	32.18 ± 1.61	33.7 ± 1.69	41.4 ± 2.07	47.31 ± 2.37	46.46 ± 2.32	50.79 ± 2.54	44.35 ± 2.22	60.38 ± 3.02	50.02 ± 2.50	68.91 ± 3.45	
t- caffeic acid	10.25 ± 0.51	12.75 ± 0.64	49.54 ± 2.48	54.9 ± 2.75	51.61 ± 2.58	61.69 ± 3.08	30.72 ± 1.54	49.98 ± 2.50	47.38 ± 2.37	58.92 ± 2.95	52.11 ± 2.61	58.14 ± 2.91	66.88 ± 3.34	96.06 ± 4.80	64.33 ± 3.22	93.04 ± 4.65	70.02 ± 3.50	93.24 ± 4.66	
ferrulic acid	17.56 ± 0.88	19.55 ± 0.98	71.63 ± 3.58	71.79 ± 3.59	79.7 ± 3.99	81.43 ± 4.07	50.84 ± 2.54	62.88 ± 3.14	64.81 ± 3.24	69.80 ± 3.49	65.67 ± 3.28	73.21 ± 3.66	71.36 ± 3.57	91.70 ± 4.59	78.29 ± 3.91	92.63 ± 4.63	77.49 ± 3.87	91.72 ± 4.59	
benzoic acid	14.11 ± 0.71	15.96 ± 0.80	42.12 ± 2.11	51.86 ± 2.59	56.8 ± 2.48	67.27 ± 3.36	33.07 ± 1.65	45.11 ± 2.26	39.08 ± 1.95	47.06 ± 2.35	64.16 ± 3.21	66.99 ± 3.35	65.53 ± 3.28	77.97 ± 3.90	75.73 ± 3.79	79.97 ± 4.00	75.49 ± 3.77	82.04 ± 4.10	
anisic acid	49.36 ± 2.47	55.87 ± 2.79	52.18 ± 2.61	66.19 ± 3.31	67.53 ± 3.38	80.28 ± 4.01	38.73 ± 1.94	57.03 ± 2.85	48.78 ± 2.44	91.96 ± 4.60	78.55 ± 3.93	81.99 ± 4.10	78.31 ± 3.92	85.99 ± 4.30	86.55 ± 4.33	89.79 ± 4.49	83.69 ± 4.18	90.57 ± 4.53	
toluic acid	47.01 ± 2.35	49.21 ± 2.46	64.23 ± 3.21	82.26 ± 4.11	76.79 ± 3.84	91.04 ± 4.55	62.55 ± 3.13	81.35 ± 4.07	68.96 ± 3.45	92.12 ± 4.61	92.89 ± 4.64	94.7 ± 4.74	88.00 ± 4.40	100 ± 5.00	91.59 ± 4.58	100 ± 5.00	90.69 ± 4.53	100 ± 5.00	
p-chlorobenzoic acid	51.42 ± 2.57	54.57 ± 2.73	73.59 ± 3.68	88.85 ± 4.44	84.53 ± 4.23	95.05 ± 4.75	74.56 ± 3.73	94.88 ± 4.74	79.86 ± 3.99	93.86 ± 4.69	93.86 ± 4.69	100 ± 5.00	88.93 ± 4.45	100 ± 5.00	94.72 ± 4.74	100 ± 5.00	92.78 ± 4.64	100 ± 5.00	
eugenol	78.91 ± 3.95	81.77 ± 4.09	82.04 ± 4.10	98.41 ± 4.99	88.1 ± 4.41	100 ± 5.00	84.99 ± 4.25	98.41 ± 4.92	84.84 ± 4.24	100 ± 5.00	100 ± 5.00	100 ± 5.00	98.83 ± 4.94	100 ± 5.00	100 ± 5.00	100 ± 5.00	97.60 ± 4.88	100 ± 5.00	
t-anethol	96.32 ± 4.82	97.53 ± 4.88	100 ± 5.00	100 ± 5.00	100 ± 5.00	100 ± 5.00	100 ± 5.00	100 ± 5.00	100 ± 5.00	100 ± 5.00	100 ± 5.00	100 ± 5.00	100 ± 5.00	100 ± 5.00	100 ± 5.00	100 ± 5.00	100 ± 5.00	100 ± 5.00	100 ± 5.00

- The extraction rates were calculated as the difference between the concentration of the phenolic solution before extraction to the concentration of the phenolic solution after extraction

- *: 4, 5, 6 and 7 are the polymer modifiers

- **: 8 is the neat PDMS, 9, 10, 11 and 12 are the mixture of (8+4); (8+5); (8+6) and (8+7) respectively.

Table 4. Adsorption /desorption cycles with the PDMS phases 11 and 12 after 5 hours of contact with the pollutants and washed with 10 mL of methanol for 40 minutes and then 5 hours of contact with the target polyphenols

CYCLES	C1		C2		C3		C4		C5		C6		C7		C8		C9		C10	
PDMS Phases	11	12	11	12	11	12	11	12	11	12	11	12	11	12	11	12	11	12	11	12
p-hydroxybenzoic acid	51 ± 3	69 ± 3	48 ± 2	67 ± 3	46 ± 2	65 ± 3	44 ± 2	64 ± 3	45 ± 2	65 ± 3	42 ± 2	64 ± 3	36 ± 2	63 ± 3	34 ± 2	60 ± 3	31 ± 2	58 ± 3	25 ± 1	57 ± 3
<i>t</i> - caffeic acid	96 ± 5	93 ± 5	94 ± 5	91 ± 5	93 ± 5	91 ± 5	90 ± 5	89 ± 4	89 ± 4	89 ± 4	85 ± 4	87 ± 4	74 ± 4	88 ± 4	61 ± 3	85 ± 4	55 ± 3	82 ± 4	42 ± 2	80 ± 4
ferrulic acid	91 ± 5	92 ± 5	90 ± 5	91 ± 5	89 ± 4	90 ± 5	88 ± 4	89 ± 4	86 ± 4	87 ± 4	83 ± 4	88 ± 4	71 ± 4	85 ± 4	59 ± 3	84 ± 4	53 ± 3	81 ± 4	44 ± 2	82 ± 4
benzoic acid	78 ± 4	82 ± 4	74 ± 4	80 ± 4	75 ± 4	81 ± 4	72 ± 4	82 ± 4	71 ± 4	80 ± 4	68 ± 3	79 ± 4	64 ± 3	77 ± 4	57 ± 3	74 ± 4	51 ± 3	73 ± 4	45 ± 2	71 ± 4
anisic acid	86 ± 4	90 ± 5	82 ± 4	90 ± 5	81 ± 4	88 ± 4	79 ± 4	86 ± 4	77 ± 4	85 ± 4	75 ± 4	84 ± 4	67 ± 3	85 ± 4	55 ± 3	83 ± 4	50 ± 3	79 ± 4	45 ± 2	80 ± 4
toluic acid	100 ± 5	100 ± 5	100 ± 5	100 ± 5	99 ± 5	97 ± 5	95 ± 5	99 ± 5	94 ± 5	96 ± 5	93 ± 5	95 ± 5	89 ± 4	94 ± 5	85 ± 4	91 ± 5	81 ± 4	90 ± 5	79 ± 4	89 ± 4
p-chlorobenzoic acid	100 ± 5	100 ± 5	100 ± 5	100 ± 5	98 ± 5	100 ± 5	97 ± 5	98 ± 5	95 ± 5	96 ± 5	92 ± 5	94 ± 5	89 ± 4	95 ± 5	83 ± 4	93 ± 5	82 ± 4	92 ± 5	80 ± 4	90 ± 5
eugenol	100 ± 5	100 ± 5	100 ± 5	100 ± 5	100 ± 5	100 ± 5	100 ± 5	100	100 ± 5	100 ± 5	100 ± 5	100 ± 5	98 ± 5	100 ± 5	96 ± 5	100 ± 5	97 ± 5	100 ± 5	91 ± 5	99 ± 5
t-anethol	100 ± 5	100 ± 5	100 ± 5	100 ± 5	100 ± 5	100 ± 5	100 ± 5	100 ± 5	100 ± 5	100 ± 5	100 ± 5	100 ± 5	100 ± 5	100 ± 5	99 ± 5	100 ± 5	99 ± 5	100 ± 5	97 ± 5	100 ± 5