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A self-consistent approach for the acoustical modeling of vegetal wools

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Abstract

Vegetal wools have the capacity to store atmospheric carbon dioxide, one of the main gases responsible for climate change. So, these insulating materials are used as key elements for green buildings. Moreover, vegetal wools present high sound absorption level performances contributing to the acoustic comfort of indoor living spaces. These properties are directly related to the morphology and the size of their vegetal fibres. Thus, to take their microstructural specificities into account for the modeling of their sound absorption properties, a micro-macro homogenization approach based on a cylindrical geometry is developed. This modeling method, based on a mix between Homogenization of Periodic Media (*HPM*) and Self-Consistent Method (*SCM*), is called *SCM_{cyl}*. The macroscopic behaviour laws of materials are rigorously obtained by using *HPM*. Then, the *SCM* leads to the establishment of two possible analytical solutions (a velocity approach v and a pressure approach p) under the fundamental assumption of the energy equivalence between a generic cylindrical inclusion, representative of the vegetal wools physical and geometrical properties at microscopic scale,

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9 and the homogeneous equivalent medium at the macroscopic scale. The two
10 modeling approaches developed in this paper, $SCM_{cyl} - v$ and $SCM_{cyl} - p$,
11 can be used to determine the sound absorption of fibrous materials using only
12 two parameters, an equivalent fibre radius value and the material porosity. Fi-
13 nally, these solutions are validated for the vegetal wools case by comparison
14 with experimental measurements.
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18 *Keywords:* Sound absorption coefficient, Self-consistent method,
19 Homogenization of Periodic Media, Fibrous materials, Vegetal wools
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22 23 **1. Introduction**

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Vegetal wools provide an innovative and sustainable response to human needs. Indeed, used as vegetal raw materials in green buildings insulation, they bring a significant storage of atmospheric carbon dioxide [1, 2]. In addition, these materials present high levels of performance in sound absorption [3, 4, 5, 6, 7] contributing significantly to the improvement of acoustic comfort inside buildings. Vegetal wools are characterized by the morphological and shape specificities of their fibres. They display a strong variability in fibre size distribution [5, 8]. Moreover, the organization of fibres in the materials leads to an anisotropic behaviour [9, 10]. These aspects of the fibrous microstructure of vegetal wools have a direct impact on their sound absorption performances at macroscopic scale [5, 8, 11, 12, 13] and it is necessary to take them into account when modeling sound absorption coefficient of vegetal wools. To do that, it seems particularly relevant to use real parameters related to fibre geometry and wool structure, such as fibre radius and porosity. Thus, empirical models dedicated to fibrous materials can be used. Some of them such as [14, 15] are approved and widely used in the literature. However, besides not being physically justified, these models historically developed for conventional fibrous materials seem to be less adapted to the high variability of vegetal fibres as shown in [8]. Moreover, they can lead to unphysical predictions as for example negative real parts of complex dynamic density especially at low frequencies [16]. Semi-phenomenological mo-

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dels, such as the Johnson-Champoux-Allard-Lafarge model (JCAL) [17, 18, 19], exist and have proven their efficiency for fibrous materials [5, 8] but they usually require five (or more) parameters related to pore configuration. Experimental characterization of some of these parameters such as viscous and thermal characteristic lengths or static thermal permeability is not always possible. So, the work carried out in [20] led to a model limited to three parameters if information on pore size distributions is available. However, semi-phenomenological models have been developed for the geometry of general pore networks and are not directly linked to the microstructural geometry of fibrous media such as fibre sizes which may be an accessible parameter for manufacturers of fibrous insulators. We can then focus on other approaches which are based on homogenization methods that link the properties of an heterogeneous medium at the microstructure scale to the properties of a macroscopic medium. One of the most widely used methods is the Homogenization of Periodic Media (HPM), initially developed by [21, 22]. This modeling method can be applied regardless of the periodic microstructure. However, it requires the implementation of important numerical simulations rather than analytical relationships. This approach has been adapted to the case of fibrous materials in [11, 23], where simplifying assumptions about the representative elementary volume (REV) had to be done in order to decrease the numerical calculations. Other micro-macro approaches are based on 3D modeling of the REV, requiring numerical simulations to determine the sound absorption properties [24]. In [25, 26] an hybrid approach is used on the basis of a numerical homogenization mixed with the JCAL model by numerical calculations related to the finite element method. This approach has been adapted to the case of porous media such as melamine foam in [27] and more recently to the special cases of a glass wool [28] and a vegetal fibrous materials (milkweed fibres) [29]. These methods have several advantages. Indeed, based on a relatively detailed REV, they lead to an accurate modeling of material acoustic properties. Moreover, it is possible to establish relationships between the characteristic parameters of the pore networks related to models such as JCAL and those describing the microstructure of materials. Nevertheless, as this hy-

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brid approach requires numerical resolutions, microstructure parameters are not directly related to the macroscopic properties of the materials through analytical relationships. In order to avoid tomography or SEM characterizations, it seems particularly relevant to have direct micro-macro analytical relationships to carry out rapid inverse analyses. To do this, it is possible to use a different but complementary homogenization approach, called Self-Consistent Homogenization (SCM) [30]. It is slightly different from the HPM method. Indeed, the microstructure is not identified with the same precision, but it is reproduced by generic heterogeneities. Also, it is specified in [31] that the fundamental hypothesis of this method is to consider that the material at the macroscopic scale and the microstructural parameters follow the same behaviour laws. In the case of a spherical geometry, coupled HPM-SCM approach has been developed in dynamics by [32, 33]. The HPM method is used to rigorously obtain the macroscopic behaviour laws of materials. The SCM approach is applied in a second step by relying on a two-component spherical inclusion (solid phase included in the fluid phase) in order to obtain relationships directly linking microstructural parameters such as spherical grain sizes and macroscopic properties. However, this method based on a spherical geometry is mainly dedicated to granular materials. For fibrous materials having a cylindrical geometry, Boutin’s work [34] has been limited to a static approach based on [35]. However, another SCM modeling approach has been developed in the literature, but without the fundamental self-consistent assumption, for example for a spherical geometry by [36]. For a cylindrical geometry, the Tarnow model is frequently used in the literature for modeling the sound absorption properties of fibrous materials [37, 38, 39]. Thus, in the light of all the above components and in order to directly relate both the fibre characteristic parameters and the material structure to their macroscopic properties, it seems particularly relevant to develop a cylindrical Self-Consistent Modeling approach in dynamic (SCM_{cyl}). Indeed, on the basis of the laws of macroscopic behaviour established by HPM, as in C. Boutin spherical approach, this SCM_{cyl} approach can lead to possible analytical solutions between specific parameters of fibrous microstructural media and macroscale sound absorption

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9 properties. Moreover, it can take the [anisotropic](#) nature of vegetal wools into
10 account, while respecting the fundamental hypothesis of [energy conservation](#).
11 Therefore, this paper is organised as follows : Section 2 describes very syntheti-
12 cally the determination of macroscopic behaviour laws by HPM approach. Then,
13 after presenting assumptions about the representative elementary volume, the
14 SCM_{cyl} approach is exposed. In Section 3, the SCM_{cyl} modeling approach is
15 validated by comparison with experimental data on two vegetal wools. Finally,
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2. Modeling

2.1. Macroscopic laws from the HPM

95 The description of this method is widely available in the literature, especially
for the general case of porous materials [32, 40, 41]. Thus, after a description
of the hypotheses and simplifications made in the present case for a fibrous
medium, the HPM main steps and results are recalled.

2.1.1. Basic hypothesis concerning the fibrous medium

100 We consider a biphasic fibrous medium composed by a solid phase (Ω_s) and
a fluid phase (Ω_f) saturating this medium. As a first approximation and to
take its anisotropic nature into account, the solid phase is represented by fibres
of constant cross-section over their entire length (which is considered large in
comparison with the cross-section size) [42]. Moreover, in our case, this medium
105 is represented by a regular layout of the fibres which are parallel to each other,
as shown by Fig. 1. In the general case, the solid phase is considered elastic [43],
[44]. Nevertheless, the work carried out in [45] defines a decoupling frequency
(f_d) above which it can be considered that only a compression wave propagates
in the fluid phase. Then, in this case, the hypothesis of a rigid solid phase is
110 acceptable. So, this assumption is used as a first approximation for the solid
phase. Moreover, this phase is considered impermeable and its thermodynamic

evolution is considered isothermal. The fluid phase is considered as a Newtonian
 viscous and compressible fluid of viscosity μ and thermal conductivity λ_f (air
 thermal conductivity). The porosity ϕ is considered to be open and the porous
 network is interconnected. Moreover, the case of a single porosity medium is
 chosen and wavelengths are considered large in comparison with the pore sizes
 in order to neglect diffraction effects.

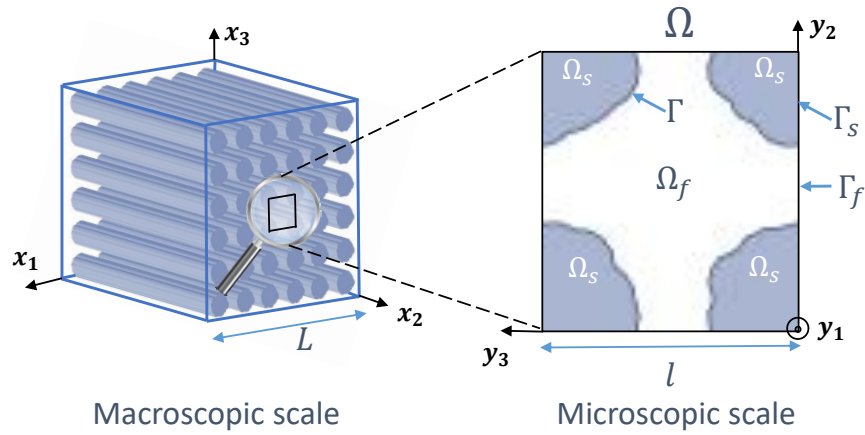


FIGURE 1: Schematic representation of a fibrous medium at macroscopic and microscopic scales by the periodic cell Ω . Ω_s and Ω_f correspond to volumes of the solid and fluid phases. Γ is the solid-fluid interface. Γ_s and Γ_f are the solid and fluid interfaces with the cell boundary Ω

Two specific orientations can be considered for the acoustic excitation. The first one is in a plane defined by $(\mathbf{x}_1, \mathbf{x}_3)$, perpendicular to the longitudinal axis (\mathbf{x}_2) of fibres. The second limit case corresponds to an acoustic excitation parallel to the longitudinal axis of the fibre (\mathbf{x}_2) . However, the parallel case does not correspond to a conventional use of insulation panels in buildings. Even though all orientations of the wave are possible between these two limits [9, 29], in this paper, only a specific focus is done on the perpendicular case which corresponds to most practical applications. To use a micro-macro homogenization method, two basic principles must be respected :

- the existence of a representative elementary volume (REV) ;

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9 — the scale separation between the medium macroscopic representation and
10 the microscopic characteristics of heterogeneities.

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12 130 So, as shown by Fig. 1, the REV is related to the microscopic length (l) and the
13 fibrous medium is associated to the macroscopic length (L). Both lengths are
14 related to the scale ratio $\varepsilon = \frac{l}{L} \ll 1$. The acoustic solicitation is represented by
15 the propagation of a harmonic plane wave of velocity c_0 and of unit amplitude
16 in the fibrous medium. Then, this wave is subjected to dissipation phenomena
17 related to both visco-inertial and thermal effects. It is possible to establish local-
18 135 level relationships for each of these phenomena.
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24 2.1.2. Basic equations related to visco-inertial and thermal effects

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26 An acoustic wave propagates through the fluid phase. The wave is considered
27 harmonic ($e^{j\omega t}$ dependency is supposed, with $j^2 = -1$ and $\omega = 2\pi f$ is the
28 angular frequency, f being the frequency in hertz), so the linearized Navier-
29 Stokes equation governing the fluid phase is written :
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$$32 \mu \Delta \mathbf{v} - \nabla p = j\omega \rho_0 \mathbf{v} \quad (1)$$

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34 with μ the dynamic viscosity, \mathbf{v} the local speed of the fluid, p the pressure and
35 ρ_0 the fluid phase bulk density at rest.
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38 The local form of the linearized mass conservation equation is given by the
39 following relationship :
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$$41 j\omega \rho + \rho_0 \nabla \cdot \mathbf{v} = 0 \quad (2)$$

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44 140 with ρ the bulk density.

45 At the local scale, the temperature variation is governed by the linearized
46 heat equation, which is expressed by the relation :
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$$49 \lambda_f \Delta T - j\omega \rho_0 C_p T = -j\omega p \quad (3)$$

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51 with λ_f the thermal conductivity of the fluid phase, T the temperature and C_p
52 the heat capacity at constant pressure.
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9 *2.1.3. Scale separation condition*

10 The next step of HPM is the scale separation condition. It consists in scaling
11 each term of the linearized equations (Eqs. 1 to 3). To do that, we define the
12 variable \mathbf{X} . It can be related to the variable $\mathbf{x} = \frac{\mathbf{X}}{L}$ at macroscopic scale and
13 to the variable $\mathbf{y} = \frac{\mathbf{X}}{l}$ at microscopic scale. \mathbf{x} and \mathbf{y} are related to ε by the
14 following relationship : $\mathbf{x} = \varepsilon\mathbf{y}$. Then, each vector and scalar field, \mathbf{v} , p , ρ and
15 T can be expressed as an asymptotic development in powers of ε as follows :
16 $f(\mathbf{x}, \mathbf{y}) = \sum_{i=0}^{\infty} \varepsilon^i f^i(\mathbf{x}, \mathbf{y})$. The gradient (∇), divergence ($\nabla \cdot$) and Laplacian (Δ)
17 operators are approximated by the following relationships : $\nabla \simeq \nabla_{\mathbf{x}} + \varepsilon^{-1}\nabla_{\mathbf{y}}$;
18 $\nabla \cdot \simeq \nabla_{\mathbf{x}} \cdot + \varepsilon^{-1}\nabla_{\mathbf{y}} \cdot$; $\Delta \simeq \Delta_x + 2\varepsilon^{-1}\nabla_{\mathbf{x}} \cdot \nabla_{\mathbf{y}}$. After injecting the asymptotic
19 developments into the equations relating to viscous and thermal dissipation
20 phenomena, terms of the same order can then be identified. At the order $o(\varepsilon^{-1})$,
21 we obtain the following relationships :

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$$\nabla_{\mathbf{y}} p^0 = 0 \tag{4}$$

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32 The pressure is uniform in the pores at the first order. So, it can be expressed
33 by : $p^0 = p^0(\mathbf{x}) = P$. We also find the hypothesis of incompressibility of the
34 fluid, in the first order, at the pore scale :

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$$\nabla_{\mathbf{y}} \cdot \mathbf{v}^0 = 0 \tag{5}$$

39 At the order $o(1)$, we obtain the following relationships :

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41 — Visco-inertial effects

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$$\begin{cases} \mu \Delta_{\mathbf{y}} \mathbf{v}^0 - \nabla_{\mathbf{y}} p^1 - \nabla_{\mathbf{x}} p^0 = j\omega \rho_0 \mathbf{v}^0 & (6) \\ j\omega \rho^0 + \nabla_{\mathbf{y}} \cdot \mathbf{v}^1 + \nabla_{\mathbf{x}} \cdot \mathbf{v}^0 = 0 & (7) \end{cases}$$

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45 — Thermal effects

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$$\{ \lambda_f \Delta_{\mathbf{y}} T^0 - j\omega \rho_0 C_p T^0 = -j\omega p^0 \tag{8}$$

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53 **145** *2.1.4. Variational formulation resolution and [energy conservation condition](#)*

54 The resolution of the previous set of equations is traditionally realized in the
55 literature using a variational formulation. This mathematical operation consists
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9 in performing the scalar product of each terms by a \mathbf{w} field belonging to the
10 vector space W , defined by : $W = \{\mathbf{w}, \Omega - \text{periodic} / \nabla_{\mathbf{y}} \cdot \mathbf{w} = 0, \mathbf{w}_{/\Gamma} = \mathbf{0}\}$.
11 Equations are then integrated over Ω_f . For the **visco-inertial** effects, based on
12 Eq. 6 we can express the following relationship :
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$$15 \quad - \iiint_{\Omega_f} \nabla_{\mathbf{y}} p^1 \cdot \mathbf{w} d\Omega + \mu \iiint_{\Omega_f} \Delta_{\mathbf{y}} \mathbf{v}^0 \cdot \mathbf{w} d\Omega - \iiint_{\Omega_f} \nabla_{\mathbf{x}} p^0 \cdot \mathbf{w} d\Omega = \iiint_{\Omega_f} j\omega \rho_0 \mathbf{v}^0 \cdot \mathbf{w} d\Omega \quad (9)$$

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19 To simplify Eq. 9, we use the flow-divergence theorem showing an equality between
20 the integral on a given volume (V) of the vector field (\mathbf{F}) divergence and
21 the flow of this field through the surface (dS) representing the volume boundary
22 (∂V). By associating a scalar field (g) to the vector field (\mathbf{F}), we can write this
23 theorem :
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$$26 \quad \iiint_V (\mathbf{F} \cdot \nabla g + g (\nabla \cdot \mathbf{F})) dV = \oint_{\partial V} g \mathbf{F} \cdot \mathbf{dS} \quad (10)$$

27
28 Based on this theorem, as well as the periodicity properties of the functions
29 belonging to the vector space W and assuming that $\vec{w} = \vec{\mathbf{v}}^0$, the conjugate of
30 the velocity \mathbf{v}^0 , we obtain the following relation :
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$$34 \quad \iiint_{\Omega_f} \nabla_{\mathbf{y}} \mathbf{v}^0 \cdot \nabla_{\mathbf{y}} \vec{\mathbf{v}}^0 d\Omega + j \frac{\omega \rho_0}{\mu} \iiint_{\Omega_f} \mathbf{v}^0 \cdot \vec{\mathbf{v}}^0 d\Omega = -\frac{1}{\mu} \nabla_{\mathbf{x}} P \iiint_{\Omega_f} \vec{\mathbf{v}}^0 d\Omega \quad (11)$$

35
36 This relationship demonstrates the **energy conservation** between the microscopic
37 and macroscopic descriptions of the fibrous medium, which is a fundamental
38 assumption of homogenization models. Then, the solution is classically written :
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$$42 \quad \mathbf{v}^0(\mathbf{x}, \mathbf{y}, \omega) = -\frac{[\pi(\mathbf{y}, \omega)]}{\mu} \nabla_{\mathbf{x}} P(\mathbf{x}, \omega) \quad (12)$$

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44 $\pi(\mathbf{y}, \omega)$ represents the local permeability tensor. By integrating $\mathbf{v}^0(\mathbf{x}, \mathbf{y}, \omega)$ over
45 Ω , we get the macroscopic velocity of the equivalent homogeneous medium :
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$$49 \quad \langle \mathbf{v}^0 \rangle_{\Omega} = -\frac{[\Pi(\omega)]}{\mu} \nabla_{\mathbf{x}} P(\mathbf{x}, \omega) \quad (13)$$

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51 This equation corresponds to the **Generalized Darcy's Law**, where $[\Pi(\omega)]$
52 is the dynamic permeability tensor related to the dynamic density ρ with the
53 following relation : $\rho(\omega) = \frac{\mu}{j\omega \Pi(\omega)}$.
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For the thermal effect, applying the same procedure as for visco-inertial effects, Eq. 8 leads to the following relationship :

$$\lambda_f \iiint_{\Omega_f} \nabla_{\mathbf{y}} T^0 \cdot \nabla_{\mathbf{y}} \overline{T^0} d\Omega + j\omega\rho_0 C_p \iiint_{\Omega_f} T^0 \overline{T^0} d\Omega = j\omega P \iiint_{\Omega_f} \overline{T^0} d\Omega \quad (14)$$

This relationship represents the [energy conservation](#) for heat dissipation effects between the local scale represented by the terms on the left and the equivalent homogeneous medium, macroscopic scale, represented by the right term. The solution of the variational formulation process is expressed according to the following relationship where $\xi(\mathbf{y}, \omega)$ represents the thermal permeability at the local scale :

$$T^0(\mathbf{x}, \mathbf{y}) = \frac{\xi(\mathbf{y}, \omega)}{\lambda_f} j\omega P(\mathbf{x}, \omega) \quad (15)$$

The relation governing the macroscopic temperature variation of the equivalent homogeneous medium is obtained by integrating over Ω :

$$\langle T^0 \rangle_{\Omega} = \frac{\Xi(\omega)}{\lambda_f} j\omega P(\mathbf{x}) \quad (16)$$

Eq. 16 is equivalent to Darcy's law for visco-inertial effects. $\Xi(\omega)$ is the dynamic thermal permeability of the equivalent homogeneous medium. It is related to the bulk modulus K with the following relation : $K(\omega) = \frac{\gamma P_0 / \phi}{\gamma - j(\gamma - 1) \frac{\Xi(\omega)}{\delta_p^2 \phi}}$.

Using the HPM approach, relationships can be established between the local velocity, pressure and temperature fields and their macroscopic shape related to the equivalent homogeneous medium. However, the HPM is used independently of the morphology of the elementary cell and the implementation of numerical resolutions is necessary to determine solutions. Thus, in order to determine possible analytical solutions, a coupling of the HPM and the SCM homogenization is performed. To do that, SCM is used on the basis of the equations governing the laws of behaviour on a macroscopic scale that have been established in this section and on the fundamental hypothesis of [energy conservation](#).

2.2. SCM with cylindrical geometry (SCM_{cyl}) adapted to fibrous media

This method has been used in static for the determination of ρ , for fibrous materials by [35] and for granular materials (spherical SCM) by [34]. Subsequently, work carried out in [32] and [33] led to the determination of ρ and of

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165 the bulk modulus K in dynamic, but only in the case of the granular materials
with spherical geometry. To apply this method, it is first necessary to develop a
generic inclusion of simplified geometry and to establish the equations governing
the behaviour of the velocity, local pressure and temperature fields. Then, under
the constraint of an homogeneous macroscopic force, differential equations are
170 obtained and solved to determine solutions for the three characteristic quantities
within the fluid phase. Then, the establishment of boundary conditions makes
it possible to propose two families of possible solutions for ρ and K , which can
be used for the modeling of fibrous materials acoustic properties.

2.2.1. *Cylindrical generic inclusion for a fibrous medium*

The selected generic inclusion (Ω) is a biphasic inclusion described by a
cylinder of radius (R) and surface (∂R). The solid phase, representative of a
fibre of volume (Ω_s), has a radius (βR) constant along its entire length (Z)
considered, in first approximation, large in comparison with the cylinder cross-
section ($\frac{Z}{r} = \varepsilon \ll 1$). The solid phase is included in an air cylinder (fluid phase)
with a hole in the middle. Its external radius is R and its internal radius is βR ,
as shown in Fig. 2. Thus, we can express the porosity ϕ from the solid phase
radii βR and the inclusion R . $\phi = 1 - \left(\frac{\beta R}{R}\right)^2 = 1 - \beta^2$. The macroscopic stress
materialized by a pressure gradient $\nabla \mathbf{P}$, has been represented in Fig. 2 in a plane
defined by $(\mathbf{e}_r, \mathbf{e}_\theta)$, perpendicular to the longitudinal axis (\mathbf{e}_z) of the fibres. As
indicated in section 2.1.1, only this special limit case is investigated. To simplify
the writing of the acoustic pressure force, $\nabla \mathbf{P}$ is replaced by a force noted
 $\mathbf{G} = \nabla \mathbf{P}$. So, at macroscopic scale in the equivalent homogeneous medium,
generalized Darcy law for the visco-inertial effects and equivalent Darcy law for
the thermal effects are expressed through the following relationships :

$$\langle \mathbf{v} \rangle = \mathbf{V} = -\frac{\Pi}{\mu} \nabla \mathbf{P} = -\frac{\Pi}{\mu} \mathbf{G} \tag{17}$$

$$\langle T \rangle = \frac{\Xi}{\lambda_f} j\omega P \tag{18}$$

175 In the fluid phase of the cylindrical inclusion for $\beta R < r < R$:

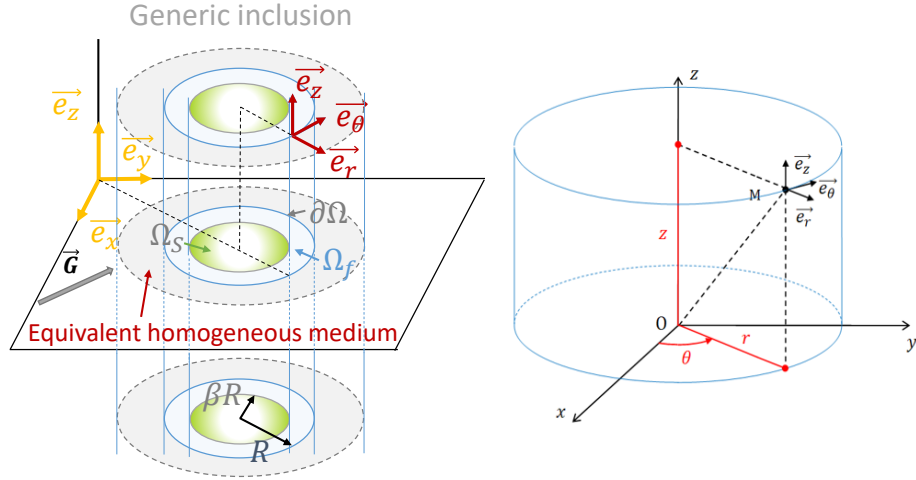


FIGURE 2: Schematic representation of a fibrous medium at macroscopic and microscopic scales by the periodic cell Ω . Ω_s and Ω_f correspond to volumes of the solid and fluid phases. Γ is the solid-fluid interface. Γ_s and Γ_f are the solid and fluid interfaces with the cell boundary Ω

- local fluid movements are governed by the linearized Navier-Stokes equation. For convenience, it is expressed as :

$$-\nabla p - \frac{1}{\delta_v^2} \mu \mathbf{v} + \Delta(\mu \mathbf{v}) = \mathbf{0} \quad (19)$$

with $\delta_v = \sqrt{\frac{\mu}{j\rho_0\omega}}$ the viscous boundary layer thickness ;

- based on Eq. 5 the fluid phase is considered as incompressible at the first order :

$$\nabla \cdot \mathbf{v} = 0 \quad (20)$$

- **no slip** condition between the solid phase and the fluid phase is zero :

$$\mathbf{v}|_{\Gamma} = \mathbf{0} \quad (21)$$

- temperature field variations in the fluid phase are governed by the linearized heat equation which is expressed as follows :

$$\Delta T - \frac{1}{\delta_t^2} T + \frac{j\omega P}{\lambda_f} = 0 \quad (22)$$

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With $\delta_t = \sqrt{\frac{\lambda_f}{\rho_0 C_p \omega}}$ the thermal boundary layer thickness ;
 — the temperature condition at the solid/fluid interface is zero :

$$T/\Gamma = 0 \tag{23}$$

2.2.2. *The pressure field*

In a first approximation and based on [46] works, which is also used in [32], it is possible to expressed the pression field (p) as a function of both \mathbf{G} and a function denoted h (which has to be determined) depending on r by the following relationship :

$$p = \mathbf{G} \cdot \nabla \mathbf{h}(r) \tag{24}$$

Using the divergence operator ($\nabla \cdot$) on the linearized Navier-Stokes equation (Eq. 19), we get :

$$\nabla \cdot \nabla p - \frac{1}{\delta_v^2} \mu \nabla \cdot \mathbf{v} + \omega (\mu \nabla \cdot \mathbf{v}) = 0 \tag{25}$$

However, as the fluid is considered incompressible at the local scale (Eq. 20), the previous expression (Eq. 25) can be simplified and we can write it :

$$\Delta p = 0 \tag{26}$$

By combining Eqs. 24 and 26, we obtain :

$$\Delta (\mathbf{G} \cdot \nabla \mathbf{h}(r)) = \mathbf{G} \cdot \nabla (\Delta h(r)) = G_r \frac{\partial (\Delta h(r))}{\partial r} = 0 \tag{27}$$

Then, it leads to the following differential equations :

$$\Delta h(r) = c_0 \tag{28}$$

Finally, the expression of h function can be obtained by the following relationship :

$$h(r) = c_0 \ln(r) + \frac{c_1 \cdot r^2}{4} \tag{29}$$

The constant term is taken equal to zero because it has no physical meaning and it does not participate in the establishment of boundary conditions.

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9 *2.2.3. The velocity field*

10 As for the case of the scalar field p , it is possible to rely on [32, 46] to express
11 the local velocity vector field in the following form :

$$12 \quad \mu \mathbf{v} = \mathbf{G} [\nabla \otimes \nabla f(r) + g(r)I] \quad (30)$$

13
14 with \otimes representing the tensor product operator and I the identity matrix. Ap-
15 plying the divergence operator to Eq. 30, we obtain the following relationship :

$$16 \quad \mathbf{G} \cdot \nabla \cdot [\nabla \otimes \nabla f(r) + g(r)I] = \mu \nabla \cdot \mathbf{v} = 0 \quad (31)$$

17 Then, Eq. 31 can be written in the following form :

$$18 \quad \mathbf{G} \cdot \nabla [\Delta f(r) + g(r)] = G_r \left(\frac{\partial(\Delta f(r) + g(r))}{\partial r} \right) = 0 \quad (32)$$

19 Thus, we can write that $\Delta f(r) + g(r) = a_0$, or $g(r) = -\Delta f(r) + a_0$ with a_0 a
20 constant. By injecting the $g(r)$ expression into Eq. 30, we obtain the following
21 relationship :

$$22 \quad \mu \mathbf{v} = \mathbf{G} [\nabla \otimes \nabla f(r) - \Delta f(r)I + a_0I] \quad (33)$$

23 On the other hand, we can include the term $-\frac{a_0}{2}r^2$ in the $f(r)$ function in order
24 to remove the term a_0I . Eq. 30 is finally written :

$$25 \quad \mu \mathbf{v} = \mathbf{G} \cdot [\nabla \otimes \nabla f(r) - \Delta f(r)I] \quad (34)$$

26 Now, we can replace both $\mu \mathbf{v}$ and p terms in the linearized Navier-Stokes equa-
27 tion (Eq 19) by their respectively expressions given by both Eq 24 and Eq 34.
28 Thus, we obtain the following relationship :

$$29 \quad -\nabla \cdot (\mathbf{G} \cdot \nabla h(r)) - \frac{1}{\delta_v^2} \mathbf{G} \cdot [\nabla \otimes \nabla f(r) - \Delta f(r)I] + \Delta (\mathbf{G} \cdot [\nabla \otimes \nabla f(r) - \Delta f(r)I]) = \mathbf{0} \quad (35)$$

30 This expression can also be written in the following simplified form :

$$31 \quad -\mathbf{G} \cdot \Delta h(r)I + \mathbf{G} \cdot [\nabla \otimes \nabla - I\Delta] \left[-h(r) + \Delta f(r) - \frac{1}{\delta_v^2} f(r) \right] = \mathbf{0} \quad (36)$$

32 To further simplify Eq. 36, a m function is introduced. It is expressed by :
33 $m(r) = \left[-h(r) + \Delta f(r) - \frac{1}{\delta_v^2} f(r) \right]$. Moreover, the h function is replaced by its

expression given by Eq. 29. So, $\Delta h(r) = \frac{1}{r} \frac{\partial}{\partial r} (r \frac{\partial h}{\partial r}) = c_1$. Finally, Eq. 36 can be written :

$$\mathbf{G} \cdot [-c_1 I + \nabla \otimes \nabla m(r) - I \Delta m(r)] = \mathbf{0} \quad (37)$$

$$\text{with } \nabla \otimes \nabla m(r) = \begin{bmatrix} \frac{\partial}{\partial r} \left(\frac{\partial m(r)}{\partial r} \right) & 0 & 0 \\ 0 & \frac{1}{r} \frac{\partial m(r)}{\partial r} & 0 \\ 0 & 0 & 0 \end{bmatrix} \text{ and } \Delta m(r) = \frac{1}{r} \frac{\partial m(r)}{\partial r} + \frac{\partial^2 m(r)}{\partial r^2}.$$

Eq. 37 can thus be written in matrix form as follows :

$$\mathbf{G} \cdot \begin{bmatrix} -c_1 - \frac{1}{r} \frac{\partial m(r)}{\partial r} & 0 & 0 \\ 0 & -c_1 - \frac{\partial^2 m(r)}{\partial r^2} & 0 \\ 0 & 0 & -c_1 - \frac{\partial^2 m(r)}{\partial r^2} - \frac{1}{r} \frac{\partial m(r)}{\partial r} \end{bmatrix} = \mathbf{0} \quad (38)$$

So, $\frac{\partial m(r)}{\partial r} = -c_1 r$. Thus, we can express the m function by the following expression :

$$m(r) = -h(r) + \Delta f(r) - \frac{1}{\delta_v^2} f(r) = -c_0 \ln(r) - \frac{c_1}{4} r^2 + \Delta f(r) - \frac{1}{\delta_v^2} f(r) = -\frac{c_1}{2} r^2 \quad (39)$$

Finally, for the function f , we obtain a second degree differential equation with non-constant coefficients and with a second member. It is expressed by the following relation :

$$\frac{\partial^2 f(r)}{\partial r^2} + \frac{1}{r} \frac{\partial f(r)}{\partial r} - \frac{1}{\delta_v^2} f(r) = c_0 \ln(r) - \frac{c_1}{4} r^2 \quad (40)$$

The solution is :

$$f(r) = \delta_v^2 \left(-c_0 \ln r + \frac{c_1}{4} r^2 - c_1 \delta_v^2 \right) + c_2 I_0(r/\delta_v) + c_3 K_0(r/\delta_v) \quad (41)$$

With I_0 and K_0 , modified Bessel functions of the first species.

2.2.4. The temperature field

By analogy with visco-inertial effects and by using the equations previously established for heat dissipation in Section 2.1.4, the temperature T can be expressed as a function of local scale thermal permeability by the following relationship :

$$T(r) = \xi(r) \frac{j\omega P}{\lambda_f} \quad (42)$$

By injecting this T expression into Eq. 22, we obtain the following relationship :

$$\Delta\xi(r) - \frac{1}{\delta_t^2}\xi(r) + 1 = 0 \quad (43)$$

By expressing $\Delta\xi(r)$ in cylindrical coordinates, we finally obtain the following differential equation :

$$\frac{\partial^2\xi(r)}{\partial r^2} + \frac{\partial\xi(r)}{\partial r} - \frac{1}{\delta_t^2}\xi = -1 \quad (44)$$

The solution of this equation is :

$$\xi(r) = \delta_t^2 + c_4 I_0(r/\delta_t) + c_5 K_0(r/\delta_t) \quad (45)$$

The expressions of the functions relating to the pressure, velocity and temperature fields have been expressed locally. It is now necessary to determine the five constants used in these functions. To do that, we can use the boundary conditions of the problem. First, concerning the velocity, boundary conditions can be expressed at the solid-fluid boundary as well as at the inclusion boundary. Then, concerning the pressure, strains on generic inclusion at the inclusion boundary should also be expressed. In addition, concerning the temperature, boundary conditions can be expressed at the solid-fluid interface too. Finally, it is necessary to take the [energy conservation](#) condition between inclusion, at the local scale, and the equivalent homogeneous medium into account for both visco-inertial and thermal effects.

2.2.5. Boundary conditions at the solid-fluid interface

At the solid-fluid interface, $r = \beta R$, [no slip](#) condition (Eq. 21) leads to a zero velocity, $\mathbf{v}(\beta R) = \mathbf{0}$ and the temperature variation condition (Eq. 23) also leads to zero. This condition concerning the temperature variation allows us to easily and quickly establish the first boundary condition. Indeed, it can be expressed by the following relationship :

$$\xi(\beta R) = 0 \quad (46)$$

Concerning the velocity, based on both the cylindrical geometry and the hypothesis of a perpendicular flow (in the plane $(\mathbf{e}_r, \mathbf{e}_\theta)$), it can be written $\mathbf{v} =$

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$v_r \mathbf{e}_r + v_\theta \mathbf{e}_\theta$. Thus, based on Eq. 34, the velocity can be written as the following relationship :

$$\begin{pmatrix} \mu v_r \\ \mu v_\theta \\ 0 \end{pmatrix} = \begin{pmatrix} G \cos \theta \\ G \sin \theta \\ 0 \end{pmatrix} \begin{bmatrix} -\frac{1}{r} \frac{\partial f(r)}{\partial r} & 0 & 0 \\ 0 & -\frac{\partial^2 f(r)}{\partial r^2} & 0 \\ 0 & 0 & -\frac{1}{r} \frac{\partial f(r)}{\partial r} - \frac{\partial^2 f(r)}{\partial r^2} \end{bmatrix} \quad (47)$$

Thus, we obtain two relationships for the velocity vector at the local scale, projected on $(\mathbf{e}_r, \mathbf{e}_\theta)$:

— On the \mathbf{e}_r axis :

$$\mu v_r(r) = -G \cos \theta \frac{1}{r} \frac{\partial f(r)}{\partial r} \quad (48)$$

— On the \mathbf{e}_θ axis :

$$\mu v_\theta(r) = -G \sin \theta \frac{\partial^2 f(r)}{\partial r^2} \quad (49)$$

In combination with **no slip** condition and Eqs. 48, 49, we obtain the second and the third boundary conditions :

$$-\frac{1}{\beta R} \frac{\partial f(\beta R)}{\partial r} = 0 \quad (50)$$

$$-\Delta f(\beta R) = 0 \quad (51)$$

To summarize, the three boundary conditions for local velocity and temperature are given by Eqs.46, 50 and 51.

200 2.2.6. Boundary conditions at the inclusion frontier

It is also possible to express a boundary velocity condition between the generic inclusion and the equivalent homogeneous medium ($r = R$). Indeed, the mean velocity within the inclusion is equal to the macroscopic velocity given by the Darcy relation expressed by Eq. 17. This equality leads to the following relationship :

$$\mathbf{V}(r) = \frac{1}{\Omega} \iiint_{\Omega_f} \mathbf{v}(r) d\Omega \quad (52)$$

It is possible to rewrite Eq. 52 as the following expression :

$$\iiint_{\Omega_f} \mathbf{v}(r) d\Omega = \iiint_{\Omega_f} (\mathbf{v} \cdot \nabla r \mathbf{e}_r + r \mathbf{e}_r (\nabla \cdot \mathbf{v}(r))) d\Omega \quad (53)$$

Indeed, $\nabla r \cdot \mathbf{e}_r = 1$ and $\nabla \cdot \mathbf{v} = 0$ (Eq. 20). Then, we can simplify this expression by using the relation of the flow-divergence theorem exposed earlier by Eq. 10 :

$$\iiint_{\Omega_f} \mathbf{v}(r) d\Omega = \iint_{\partial\Omega} r \mathbf{e}_r \cdot \mathbf{v}(r) \cdot \mathbf{dS} \quad (54)$$

for $r = R$, $\mathbf{dS} = R d\theta dz \mathbf{e}_r$. Finally, by solving the surface integral, the mean velocity can be obtained :

$$\mathbf{V}(r) = \frac{1}{\mu R} \frac{\partial f(R)}{\partial r} \mathbf{G} \quad (55)$$

By identifying $\mathbf{V}(r)$ with the Generalized Darcy Equation 17, we can write a third boundary condition for $r = R$ as a function of the permeability Π , by the following relationship :

$$-\frac{1}{R} \frac{\partial f(R)}{\partial r} + \Pi = 0 \quad (56)$$

The normal fluid velocity $v_r(r)$ is expressed as a function of $\frac{\partial f(r)}{\partial r}$. So, this boundary condition means that radial velocities are equal at any point on the frontier surface between the inclusion and the equivalent homogeneous medium. Thus, we can write the following relation :

$$v_r(R) = V_r(R) \quad (57)$$

Now, on the basis of [32, 33], we can express the stress on generic inclusion at the inclusion boundary. So, it is physically possible to implement an equality between the pressure P in the equivalent homogeneous medium and the inclusion stress, which can be expressed as $-p\mathbf{I} + 2\mu \underline{\mathbf{D}}(\mathbf{v}(r))$ with $\underline{\mathbf{D}}(\mathbf{v}(r))$ the tensor of the deformation rates depending on the local velocity. This condition can be written :

$$\iint_{\partial\Omega} [-(p - P)\mathbf{I} + 2\mu \underline{\mathbf{D}}(\mathbf{v}(r))] \cdot \mathbf{dS} = 0 \quad (58)$$

At the inclusion frontier, $r = R$, $\mathbf{dS} = R d\theta dz \mathbf{e}_r$. The integral of the three terms forming Eq. 58 can be calculated separately. The first term is $\iint_{\partial\Omega} -p\mathbf{I} \cdot \mathbf{dS}$. Using the expression for p given by Eq. 24, we can write $\iint_{\partial\Omega} -p\mathbf{I} \cdot \mathbf{dS} = \iint_{\partial\Omega} -\mathbf{G} \cdot \nabla h(r) \cdot \mathbf{I} \cdot \mathbf{dS}$. So, the result is given by the following relationship :

$$\iint_{\partial\Omega} -p\mathbf{I} \cdot \mathbf{dS} = -\pi R Z \frac{\partial h(R)}{\partial r} G \quad (59)$$

with Z the cylindrical inclusion height which will later vanish. Now, to resolve the second integral, we can use the flow-divergence theorem presented by Eq. 10. Thus, $\oint_{\partial\Omega} P \mathbf{I} d\mathbf{S} = \iiint_{\Omega_f} (\mathbf{I} \cdot \nabla P + P \nabla \cdot \mathbf{I}) d\Omega$. With $\nabla \cdot \mathbf{I} = 0$, $\nabla P = \mathbf{G}$ and $d\Omega = r dr d\theta dz$. So, the result is given by the following relationship :

$$\oint_{\partial\Omega} P \mathbf{I} d\mathbf{S} = \pi R^2 Z G \quad (60)$$

Finally, to obtain the third term of Eq. 58, it is necessary to use the tensor $\underline{\mathbf{D}}(\mathbf{v}(r))$ based on the expressions of $v_r(r)$ (Eq. 48) and $v_\theta(r)$ (Eq. 49). The expression of $2\mu \underline{\mathbf{D}}(\mathbf{v}(r))$ is given by the following relationship :

$$2\mu \underline{\mathbf{D}}(\mathbf{v}(r)) = \begin{bmatrix} -2(\mathbf{G} \cdot \mathbf{e}_r) \frac{\partial}{\partial r} \left(\frac{1}{r} \frac{\partial f(r)}{\partial r} \right) & (\mathbf{G} \cdot \mathbf{e}_\theta) \left(\frac{1}{r} \frac{\partial^2 f(r)}{\partial r^2} - \frac{\partial^3 f(r)}{\partial r^3} \right) & 0 \\ (\mathbf{G} \cdot \mathbf{e}_\theta) \left(\frac{1}{r} \frac{\partial^2 f(r)}{\partial r^2} - \frac{\partial^3 f(r)}{\partial r^3} \right) & -2(\mathbf{G} \cdot \mathbf{e}_r) \frac{1}{r^2} \frac{\partial f(r)}{\partial r} & 0 \\ 0 & 0 & 0 \end{bmatrix} \quad (61)$$

for $r = R$, $d\mathbf{S} = dS \mathbf{e}_r = R d\theta dz \mathbf{e}_r$. So, we can write :

$$\oint_{\partial\Omega} 2\mu \underline{\mathbf{D}}(\mathbf{v}(R)) \cdot \mathbf{e}_r dS = \oint_{\partial\Omega} 2\mu D_{rr} dS + \oint_{\partial\Omega} 2\mu D_{r\theta} dS \quad (62)$$

with

$$\begin{cases} 2\mu D_{rr} = -2G \cos \theta \frac{\partial}{\partial r} \left(\frac{1}{r} \frac{\partial f(r)}{\partial r} \right) & (63) \\ 2\mu D_{r\theta} = G \sin \theta \left(\frac{1}{r} \frac{\partial^2 f(r)}{\partial r^2} - \frac{\partial^3 f(r)}{\partial r^3} \right) & (64) \end{cases}$$

Thus, we obtain the following result :

$$\oint_{\partial\Omega} 2\mu \underline{\mathbf{D}}(\mathbf{v}(r)) \cdot \mathbf{e}_r dS = \pi R Z G \left(-\frac{\partial^3 f(R)}{\partial r^3} + \frac{1}{R} \frac{\partial^2 f(R)}{\partial r^2} - 2 \frac{\partial}{\partial r} \left(\frac{1}{R} \frac{\partial f(R)}{\partial r} \right) \right) \quad (65)$$

Finally, we can write the solution by the following relationship :

$$\oint_{\partial\Omega} 2\mu \underline{\mathbf{D}}(\mathbf{v}(r)) \cdot \mathbf{e}_r dS = \pi R Z G \left(-\frac{\partial}{\partial r} (\Delta f(r)) \right) \quad (66)$$

So, by combining Eqs. 59, 60 and 66 with Eq. 58, we obtain the following relationship :

$$\pi R Z G \left(R - \frac{\partial h(R)}{\partial r} - \frac{\partial}{\partial r} (\Delta f(r)) \right) = 0 \quad (67)$$

We finally obtain a fifth boundary condition :

$$R - \frac{\partial h(R)}{\partial r} - \frac{\partial}{\partial r} (\Delta f(R)) = 0 \quad (68)$$

To summarize, at the inclusion frontier, we have set two new boundary conditions. First for velocity which is given by Eq.57 and the second for the stress on the inclusion which is given by Eq. 68.

2.2.7. Boundary conditions related to the *energy conservation*

Boundary conditions related to the *energy conservation* are determined for both visco-inertial and thermal effects. A preliminary operation is performed on the Navier-Stokes Equation 19 which governs the fluid's movements on local scale. For practical reasons, it is written in the following useful form :

$$\mu \Delta \mathbf{v}(r) - j\omega \rho_0 \mathbf{v}(r) = \nabla p \quad (69)$$

Then, the variational formulation method used previously in Section 2.1.4 is applied to Eq 69. However, instead of performing the scalar product by a \mathbf{w} field, the local velocity conjugate $\bar{\mathbf{v}}$ is used. Thus the following relationship is obtained :

$$\mu \iiint_{\Omega_f} \Delta (\mathbf{v}(r)) \cdot \bar{\mathbf{v}}(r) d\Omega - j\omega \rho_0 \iiint_{\Omega_f} \mathbf{v}(r) \cdot \bar{\mathbf{v}}(r) d\Omega = \iiint_{\Omega_f} \nabla p \cdot \bar{\mathbf{v}}(r) d\Omega \quad (70)$$

Now, it is possible to simplify Eq. 70 by using the flow-divergence theorem (Eq. 10) and by replacing $(\nabla \cdot \mathbf{v}(r))$ with $2\mathbf{D}(\mathbf{v}(r))$. Thus, the first term of Eq. 70 can be written :

$$2\mu \iiint_{\Omega_f} (\nabla (\mathbf{D}(\mathbf{v}(r))) \cdot \bar{\mathbf{v}}(r) + \mathbf{D}(\mathbf{v}(r)) \cdot \mathbf{D}(\bar{\mathbf{v}}(r))) d\Omega = 2\mu \oint_{\partial\Omega} \mathbf{D}(\mathbf{v}(r)) \bar{\mathbf{v}}(r) \cdot \mathbf{dS} \quad (71)$$

The right-hand term of Eq. 70 can be written as :

$$\iiint_{\Omega_f} \nabla p \cdot \bar{\mathbf{v}}(r) d\Omega = \oint_{\partial\Omega} p \bar{\mathbf{v}}(r) \cdot \mathbf{dS} \quad (72)$$

Now, Eq. 70 can be written as follows :

$$\begin{aligned} & 2\mu \iiint_{\Omega_f} \mathbf{D}(\mathbf{v}(r)) \cdot \mathbf{D}(\bar{\mathbf{v}}(r)) d\Omega + j\omega \rho_0 \iiint_{\Omega_f} \mathbf{v}(r) \cdot \bar{\mathbf{v}}(r) d\Omega \\ & = - \oint_{\partial\Omega} p \bar{\mathbf{v}}(r) \cdot \mathbf{dS} + 2\mu \oint_{\partial\Omega} \mathbf{D}(\mathbf{v}(r)) \bar{\mathbf{v}}(r) \cdot \mathbf{dS} \end{aligned} \quad (73)$$

Eq. 73 can be related to Eq. 11 established previously by the HPM method. In order to adapt it to the SCM_{cyl} case, it can be written again by the following relation :

$$2\mu \iiint_{\Omega_f} \underline{\mathbf{D}}_{\mathbf{y}}(\mathbf{v}(r)) \cdot \underline{\mathbf{D}}_{\mathbf{y}}(\bar{\mathbf{v}}(r)) \, d\Omega + j\omega\rho_0 \iiint_{\Omega_f} \mathbf{v}(r) \cdot \bar{\mathbf{v}}(r) \, d\Omega = -\frac{1}{\mu} \nabla_{\mathbf{x}} P \iiint_{\Omega_f} \bar{\mathbf{v}}(r) \, d\Omega \quad (74)$$

This relationship depicts the [energy conservation](#) between the local scale inclusion (left-hand terms) and the equivalent homogeneous medium at the macroscopic scale (right-hand term). By analogy between Eqs. 73 and 74, the following relationship can be established :

$$-\oint_{\partial\Omega} p \bar{\mathbf{v}}(r) \cdot \mathbf{dS} + 2\mu \oint_{\partial\Omega} \underline{\mathbf{D}}(\mathbf{v}(r)) \bar{\mathbf{v}}(r) \cdot \mathbf{dS} = -\nabla P \iiint_{\Omega_f} \bar{\mathbf{v}}(r) \, d\Omega \quad (75)$$

By using the flow-divergence theorem on the right-hand term of Eq. 75, we finally obtain the following relationship :

$$-\oint_{\partial\Omega} p \bar{\mathbf{v}}(r) \cdot \mathbf{dS} + 2\mu \oint_{\partial\Omega} \underline{\mathbf{D}}(\mathbf{v}(r)) \bar{\mathbf{v}}(r) \cdot \mathbf{dS} = -\oint_{\partial\Omega} P \bar{\mathbf{v}}(r) \cdot \mathbf{dS} \quad (76)$$

In order to express the energy equivalence between the inclusion and the same volume of the equivalent homogeneous medium, the approach previously used for boundary stress conditions is implemented. So, $\bar{\mathbf{V}}(R)$ is defined as the conjugate of the mean velocity at the frontier between the inclusion and the equivalent homogeneous medium. Then, the energy equivalence at $r = R$ can be written by the following relationship :

$$-\oint_{\partial\Omega} [(P - p) + 2\mu \underline{\mathbf{D}}(\mathbf{v}(R))] \cdot [\bar{\mathbf{v}}(R) - \bar{\mathbf{V}}(R)] \, dS \mathbf{e}_r = \mathbf{0} \quad (77)$$

By doing the scalar product with \mathbf{e}_r , we get two relationships :

$$\left\{ \begin{array}{l} -\oint_{\partial\Omega} [(P - p) + 2\mu D_{rr}] [\bar{v}_r(R) - \bar{V}_r(R)] \, dS \\ = 0 \end{array} \right. \quad (78)$$

$$\left\{ \begin{array}{l} -\oint_{\partial\Omega} 2\mu D_{r\theta} [\bar{v}_\theta(R) - \bar{V}_\theta(R)] \, dS = 0 \end{array} \right. \quad (79)$$

$$\left\{ \begin{array}{l} -\oint_{\partial\Omega} 2\mu D_{r\theta} [\bar{v}_\theta(R) - \bar{V}_\theta(R)] \, dS = 0 \end{array} \right. \quad (80)$$

We saw previously that $\bar{v}_r(R) = \bar{V}_r(R)$, so Eq. 79 does not lead to the [energy conservation](#) conditions. On the other hand, Eq. 80 allows two possible condi-

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9 tions. Indeed, either $[\overline{v_\theta}(R) - \overline{V_\theta}(R)]$, or $2\mu D_{r\theta} = 0$. In the first case, by expres-
10 sing $v_\theta(R)$ from Eq. 49 and $V_\theta(R)$ from generalized Darcy equation (Eq. 17),
11 we get the following relationship :
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$$13 \quad v_\theta(R) - V_\theta(R) = -\frac{\partial^2 f(R)}{\partial r^2} \frac{\mathbf{G} \cdot \mathbf{e}_\theta}{\mu} + \Pi \frac{\mathbf{G} \cdot \mathbf{e}_\theta}{\mu} \quad (81)$$

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17 So, we obtain :

$$18 \quad \frac{\partial^2 f(R)}{\partial r^2} = \Pi \quad (82)$$

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20 Combining this result with the velocity boundary condition at the inclusion fron-
21 tier, given by Eq.57, we finally obtain a sixth boundary condition relationship :
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$$24 \quad -\frac{1}{2} \Delta(f(R)) + \Pi = 0 \quad (83)$$

25
26 In this case, at the frontier between the inclusion and the equivalent homoge-
27 neous medium, the fluid phase velocity is equal to the velocity of the equiva-
28 lent medium (radial and orthoradial components). On the other hand, there
29 is no equality between the pressure in the inclusion and the pressure of the
30 equivalent homogeneous medium. This kind of configuration has been named
31 *flow approach* [32], it is noted hereafter with the v index. In the second case,
32 by using the $D_{r\theta}$ expression, given by Eq. 64, we get an alternative boundary
33 condition related to the [energy conservation](#). It can be written by the following
34 relationship :
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$$37 \quad \frac{\partial^3 f(R)}{\partial r^3} = \frac{1}{R} \frac{\partial^2 f(R)}{\partial r^2} = 0 \quad (84)$$

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44 **205** In this case, the shear stress is cancelled. Thus, the stress $(-p\mathbf{I} + 2\mu \underline{\mathbf{D}}(\mathbf{v}(R)))$ on
45 the inclusion is equal to the pressure P in the equivalent homogeneous medium.
46 However, at the frontier between the inclusion and the equivalent homogeneous
47 medium the orthoradial velocities of the fluid phase and the homogeneous me-
48 dium are not equal. This configuration is called *pressure approach* and it is
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52 **210** written with the p index.

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54 As for the visco-inertial case, the first step for the determination of the
55 boundary condition related to thermal effect consists in applying the variational
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formulation to the heat equation (Eq 22). To do that, \bar{T} is used. So, the following relationship is obtained :

$$-\lambda_f \iiint_{\Omega_f} \Delta T(r) \bar{T}(r) d\Omega + j\omega \rho_0 C_p \iiint_{\Omega_f} T(r) \bar{T}(r) d\Omega = j\omega P \iiint_{\Omega_f} \bar{T}(r) d\Omega \quad (85)$$

By applying the flow-divergence theorem to the first term of Eq. 85, we get the following relationship :

$$\begin{aligned} \lambda_f \iiint_{\Omega_f} \nabla T(r) \cdot \nabla \bar{T}(r) d\Omega + j\omega \rho_0 C_p \iiint_{\Omega_f} T(r) \bar{T}(r) d\Omega - \lambda_f \iint_{\partial\Omega} \nabla T(r) \bar{T}(r) d\mathbf{S} \\ = j\omega P \iiint_{\Omega_f} \bar{T}(r) d\Omega \end{aligned} \quad (86)$$

At the inclusion frontier ($r = R$), by identifying the Eq 86 with the previously established Eq. 14, we get the following relationship :

$$\lambda_f \iint_{\partial\Omega} \nabla T(R) \bar{T}(R) d\mathbf{S} = 0 \quad (87)$$

It can also be written :

$$\lambda_f \frac{\partial T(R)}{\partial r} \bar{T}(R) \int_0^Z dz \int_0^{2\pi} d\theta = 0 \quad (88)$$

The first possibility is $\bar{T}(R) = 0$, but it is an artificial term used to apply the variational formulation, so that does not make physical sense. The second solution is $\frac{\partial T(R)}{\partial r} = 0$. Taking the T expression given by the Eq 42, we can finally write the boundary condition for the [energy conservation](#) of the thermal dissipation effects by the following relationship :

$$\frac{\partial \xi(R)}{\partial r} = 0 \quad (89)$$

Now, it is possible to determine all the constants for both pressure p and velocity v approaches. For each of them, we have 7 unknown constants $c_0, c_1, c_2, c_3, c_4, c_5$ and Π (v or p) for 7 equations. To summarize, the both equation systems are related to the following relationships :

- v -approach : Eqs. 46, 50, 51, 57, 68, 83 and 89 ;
- p -approach : Eqs. 46, 50, 51, 57, 68, 84 and 89.

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9 *2.2.8. Solutions for the SCM_{cyl} modeling method*

10 The solving of these systems leads to the expressions of both visco-inertial
11 and thermal permeabilities. To simplify the writing of the equations, four adi-
12 220 dimensional parameters are defined $p = \frac{r}{\delta_v}$, $q = p\beta$, $p' = \frac{r}{\delta_t}$ and $q' = p'\beta$. To
13 solve the equation systems, a formal calculation software has been used. So,
14 the visco-inertial permeabilities for both v and p approaches are given by the
15 following relationships :

16 — v -approach :

$$17 \Pi_v = \delta_v^2 \left(\frac{R^2 \phi A_0 + 2\delta_v R(\beta A_1 + A_2)}{R^2(1 - \phi)A_0 + 2\delta_v(-2R\beta^2 A_3 + R\beta A_4 + RA_2 + 8\beta\delta_v A_5)} \right) \quad (90)$$

18 with A_0, A_1, A_2, A_3, A_4 and A_5 functions expressed by the following
19 relationships :

$$20 \left\{ \begin{array}{l} A_0 = I_0(p)K_0(q) - I_0(q)K_0(p), \quad (91) \\ A_1 = I_0(p)K_1(q) - I_0(q)K_1(q) + I_1(q)K_0(p) - I_1(q)K_0(q), \quad (92) \\ A_2 = I_0(p)K_1(p) - I_0(q)K_1(p) + I_1(p)K_0(p) - I_1(p)K_0(q), \quad (93) \\ A_3 = I_0(q)K_1(p) + I_1(p)K_0(q), \quad (94) \\ A_4 = I_0(p)K_1(q) + I_0(q)K_1(q) + I_1(q)K_0(p) + I_1(q)K_0(q), \quad (95) \\ A_5 = -I_1(p)K_1(q) + I_1(q)K_1(p) \quad (96) \end{array} \right.$$

21 — p -approach :

$$22 \Pi_p = \delta_v^2 \left(\frac{R^3 \phi A_3 + R^2 \delta_v(2\beta A_5 - \phi A_0) + 2\delta_v^2 R(\beta A_1 - A_2)}{\phi R^3 A_3(R^2 + 4\beta^2 \delta_v) - R^2 \delta_v(2 - \phi)A_0 - 2R\delta_v^2(A_2 + \beta A_4) - 2\beta\delta_v(R^2 + 4\delta_v^2)A_5} \right) \quad (97)$$

23 The A_0, A_1, A_2, A_3, A_4 and A_5 functions are the same as for v -approach.

24 There are expressed by Eqs. 91, 92, 93, 94, 95 and 96.

25 The thermal permability is given by the following relationship :

$$26 \Xi(\omega) = \delta_t^2 \left(1 - \frac{2\delta_t^3}{R\phi A_6} [A_7 - A_8] \right) \quad (98)$$

27 with A_6, A_7 and A_8 functions expressed by the following relationships :

$$28 \left\{ \begin{array}{l} A_6 = I_0(q')K_1(p') + K_0(q')I_1(p'), \quad (99) \\ A_7 = K_1(p')(\beta I_1(q') - I_1(p')), \quad (100) \\ A_8 = I_1(p')(\beta K_1(q') - K_1(p')), \quad (101) \end{array} \right.$$

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9 Then, by associating each dynamic visco-inertial permeability (Π_v or Π_p) with
10 the thermal permeability (Ξ), it is possible to get both parameter couples :
11 (ρ_v, K) or (ρ_p, K). Finally, we can get two possible sound absorption coefficients
12 α_v or α_p . To summarize, based on both a mean fibre radius and a porosity value,
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230 the SCM_{cyl} method developed in this paper leads to two possible solutions :

- v -approach $\Rightarrow (\Pi_v, \Xi) \Rightarrow (\rho_v, K) \Rightarrow \alpha_v$
- p -approach $\Rightarrow (\Pi_p, \Xi) \Rightarrow (\rho_p, K) \Rightarrow \alpha_p$.

21 3. Validation and discussion

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24 In this section, the SCM_{cyl} method is validated by comparison with experi-
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26 235 mental measurements. Two vegetal wools are characterized at microscopic scale
27 to obtain modeling approach input parameters as well as at macroscopic scale
28 to measure their sound absorption properties. Finally, the approach developed
29 in this paper is discussed.
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32 3.1. Materials

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35 240 Both materials used for the validation of the SCM_{cyl} modeling approach are
36 thermobonded vegetal wools manufactured as [a single panel with one kind of](#)
37 [vegetal fibres over its entire thickness](#). The first one is a flax wool (referred as
38 "Flax") and the second one is a hemp wool (referred as "Hemp"). These both
39 types of fibrous materials have been chosen because they are among the most
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43 245 widely used biobased insulation materials in green buildings. The both vegetal
44 wools are shown in FIG 3. As shown in Table 1, the both materials have relatively
45 different thickness and bulk density values to lead to different sound absorption
46 coefficients. These wools characteristics are based on 5 measurements for every
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49 4 samples of each material.
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51 3.2. Methods

52 3.2.1. Fibre size distribution

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55 Microstructure pictures of the wools have been realized using a FEI Quanta
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57 400 Scanning Electron Microscope (SEM) in secondary electron (SE) imaging
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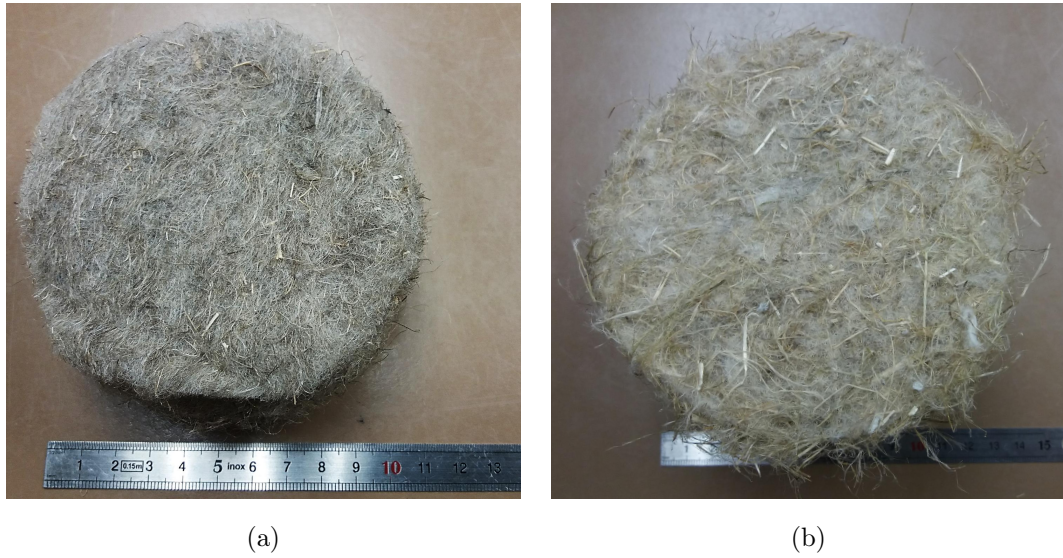


FIGURE 3: The materials, (a) "Flax", (b) "Hemp"

mode in low vacuum. Then, these pictures are analysed to characterize the
255 [vegetal fibre specificities](#). As shown in FIG 4 (a), vegetal fibres are present either
in the form of a single fibre or fibre bundles. [However, due to the 2D nature of the](#)
images and the great variability in the vegetal fibre shapes and morphologies,
it is generally difficult to really distinguish them. Thus, in the following of
this paper, as a first approach, all characterized elements will be assimilated to
260 fibres and represented by a fibre radius value. Although fibres are not perfectly
circular, it is assumed that they can be considered as cylinders of constant radius
over their entire length, as shown in FIG 4 (a). This hypothesis is corroborated
by the results carried out in [47] for which the circularity of flax fibres had been
estimated at 0.907. To determine the fibre radii distribution, we rely on the works
265 carried out in [8, 13, 48, 49]. So, using Mesurim © software, the measurements
are performed by drawing a transversal segment to the longitudinal axis of the
fibre, as shown in Fig. 4 (b).

In order to comply with these work recommendations, for each material,
at least 300 fibre diameters are recorded from a minimum of 20 pictures. The

Material	Thickness (mm)	Bulk density ($kg.m^{-3}$)	Porosity (%)	Mean fibre radius (μm)
Flax	48 ± 1	26.6 ± 1.1	98.4 ± 0.2	11.8 ± 1.6
Hemp	107 ± 2	40.8 ± 2.7	97.4 ± 0.2	16.7 ± 1.7

TABLE 1: Experimental characteristics of the vegetal wools obtained under a thermal condition of $T = 25 \pm 0.8^\circ C$ and a relative humidity of $RH = 40 \pm 2\%$. Data are presented with mean value \pm standard deviation.

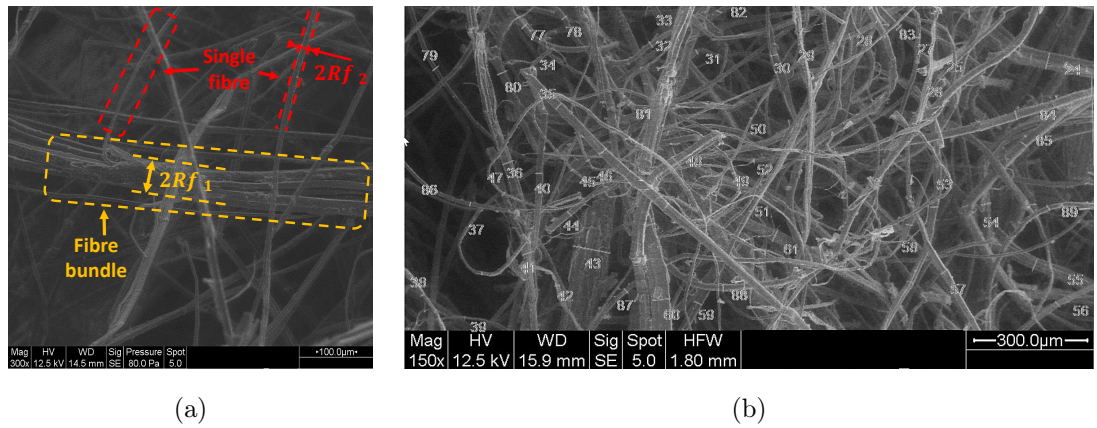


FIGURE 4: Analysis and exploitation of SEM pictures, (a) flax single fibres and fibre bundle, (b) radius measurements of hemp wool fibres with Mesurim © software

270 measured fibre radius distributions for flax and hemp wools are represented
 275 by bar charts as shown in Fig. 5. The smallest measured fibres have radii of
 approximately $3\mu m$. For the biggest ones, radii values are around $80\mu m$ for
 the hemp fibres and around $90\mu m$ for the flax fibres. Although the bar charts
 are relatively similar, the distribution of hemp fibre radii shows more elements
 above $30\mu m$. On the other hand, as shown in Fig. 5, these are log-normal laws
 which better correspond to the vegetal fibre radii distributions. Nevertheless, as
 the SCM_{cyl} modeling approach is based on an equivalent fiber radius value, in
 a first approach, we choose a single radius value corresponding to the mean of
 the fibre radii [3, 8, 13, 48]. In [23, 28] the fibre radius is weighted according

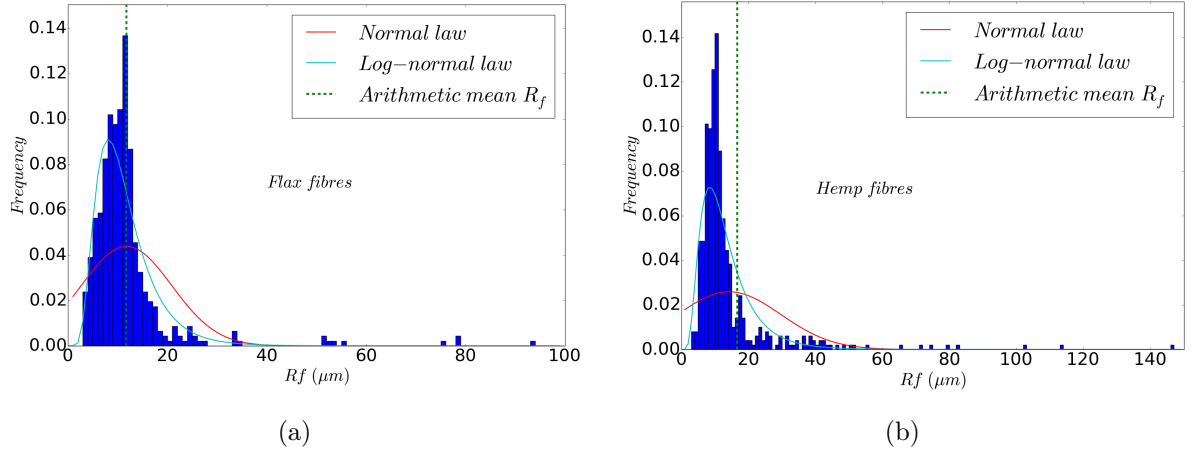


FIGURE 5: Bar charts of fibre radii distributions, (a) flax wool, (b) hemp wool

280 to its corresponding fibre volume. This typically shifts the single fibre radius towards larger values. However, in our case, as the length of the fibres is not known, it is not possible to apply this correction. Moreover, as shown in Fig. 5, for both distributions, the arithmetic mean fibre radii value is greater than the mean radii value related to the log-normal laws. Indeed, the arithmetic mean
 285 better takes the influence and the presence of large size elements into account.

The results are presented in Table 1.

3.2.2. Porosity

The porosity was experimentally characterized using the air volumes comparison method described in [50]. This method leads to the determination of the porosity directly accessible by air. It corresponds to the open porosity of materials by determining directly the volume of their solid phase. Both the inter-fibre
 290 porosity and the open intra-fibre porosity can be considered as the accessible porosity of vegetal wools. Nevertheless, works carried out in [5] have estimated that the intra-fibre porosity is lower than 0.2% of the total porosity for this type
 295 of material. So, as a first approach, it can be neglected.

The results presented in Table 1 were obtained from five measurements on both materials.

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3.2.3. Sound absorption coefficient

A B&K © type 4106 standing wave tube with an inner diameter of 100
300 mm, was used to experimentally characterize the sound absorption coefficient
of the both sides of four samples for each vegetal wool. These measurements
were carried out at normal incidence according to standard ISO 10534-2 [51].
Taking the configuration of the impedance tube and the distance between the
two microphones located upstream of the sample (7.5 cm) into account, the
305 standard ISO 10534-2 leads to a validity limit value for low-frequency measure-
ments of 226Hz. The validity limit of high-frequency measurements is estimated
to be around 2000Hz. The three position method without cavity, based on the
work carried out in [52] and adapted by [53] for microphones located outside
the tube, was used. This method leads to the determination of intrinsic material
310 parameters, the bulk modulus (K) and the dynamic density (ρ).

3.3. Modeling validation

In a first step, the both dynamic density SCM_{cyl} modeling, ρ_v and ρ_p , are
compared to the experimental ones. Then, in the same way, the bulk modulus
(K_{exp} and K_{SCM}) obtained by both experimental measurements and SCM_{cyl}
315 modeling method are analyzed. Finally, the sound absorption coefficients (α_v
and α_p) based on materials thickness, dynamic densities and bulk modulus are
modelized and compared to the experimental measurements.

3.3.1. Dynamic densities

For visco-inertial effects, the real and the imaginary parts of the normalized
320 dynamic density (ρ/ρ_0) of the experimental measurements and both SCM_{cyl}
modeling approaches for the both vegetal wools are shown in Fig. 6. As ex-
pected for the both materials, Fig. 6 shows that both approaches give values
of the real part of the dynamic density close to 1 regardless of the frequency.
For the imaginary part, in a classic way, both modeling approaches of mate-
325 rials follow a trend in $-\frac{\sigma}{\omega}$ for low frequency and close to 0 when the frequency
increases, as shown by Fig. 6. It should be noted that the differences between ex-

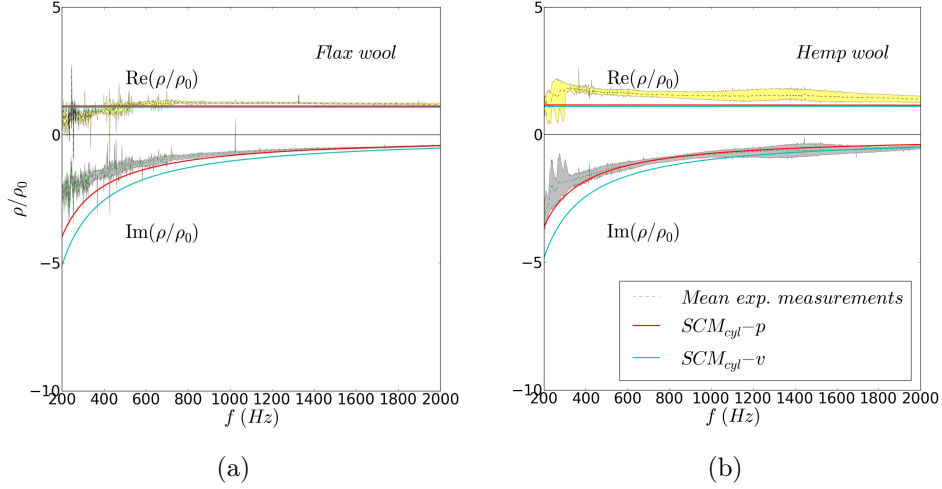


FIGURE 6: Experimental characterisation and SCM_{cyl} modeling of the normalised dynamic density as a function of frequency for (a) the flax wool and (b) the hemp wool

experimental and modeling results in the low-frequency regime for the imaginary part of the normalized dynamic density are slightly larger for flax wool than for hemp wool. This is confirmed by the airflow resistivity values determined by the low-frequency limit from both experimental measurements and SCM_{cyl} modeling. Indeed, for flax wool we obtain $\sigma_{exp} = 4161N.m^{-4}.s$, $\sigma_p = 5008N.m^{-4}.s$ and $\sigma_v = 6432N.m^{-4}.s$, while the differences are smaller for hemp wool with $\sigma_{exp} = 3993N.m^{-4}.s$, $\sigma_p = 4611N.m^{-4}.s$ and $\sigma_v = 6062N.m^{-4}.s$. For these both materials, no significant limp behaviour was observed. If so, the SCM modeling could have been mixed with the dynamic density related to a limp behaviour [54, 55]. However, a difference is observed between the curves of the both approaches. Indeed, for both materials, the flow approach is slightly further away than the pressure approach. This trend follows the same behaviour already observed for spherical modeling. The cause of the differences between the results of the flow and pressure approaches requires further investigation.

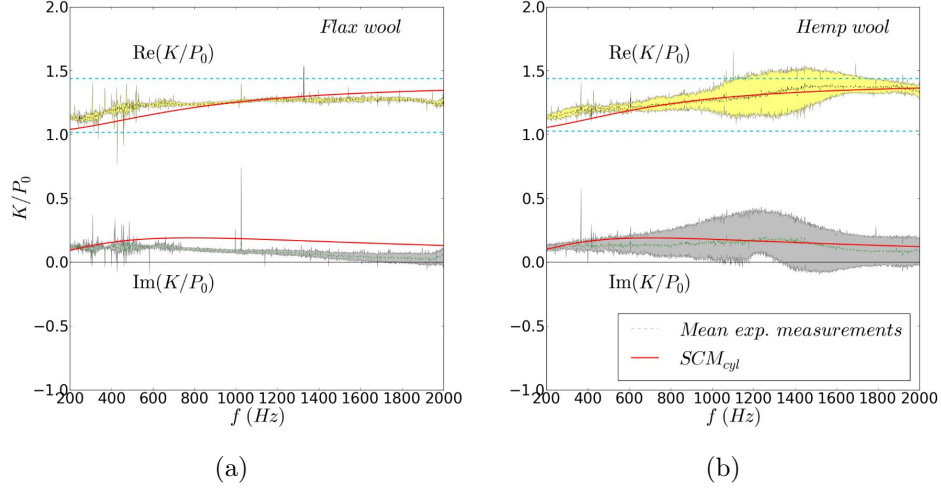


FIGURE 7: Experimental characterisation and SCM_{cyl} modeling of the normalized bulk modulus as a function of frequency for (a) the flax wool and (b) the hemp wool

3.3.2. Bulk modulus

For thermal effects, Fig. 6 shows both real and imaginary parts of the normalized bulk modulus (K/P_0) obtained by the experimental measurements and the SCM_{cyl} modeling approach for the both wools. For the real part of this parameter, the modeling method remains between the two physical limit values corresponding to $\text{Re}(K/P_0) \simeq 1/\phi$ in low frequency (isothermal regime) and $\text{Re}(K/P_0) \simeq \gamma/\phi$ in high frequency (adiabatic regime). Thus, it is verified that when the frequency is low ($f \rightarrow 0$), the real part of the normalized bulk modulus from SCM_{cyl} modeling tends towards $1/\phi$. Concerning the imaginary part of the normalized bulk modulus, as expected, at low frequency we have $\lim_{f \rightarrow 0} \text{Im}(K/P_0) = 0$. Then it increases to the thermal transition frequency before decreasing again to zero. For both materials, as shown by Fig. 7, the SCM_{cyl} modeling approach is relatively close to the experimental measurements.

3.3.3. Sound absorption coefficient

The results of the SCM_{cyl} modeling, shown in Fig. 8, are relatively close to the experimental measurements for both materials. In both cases, the pressure

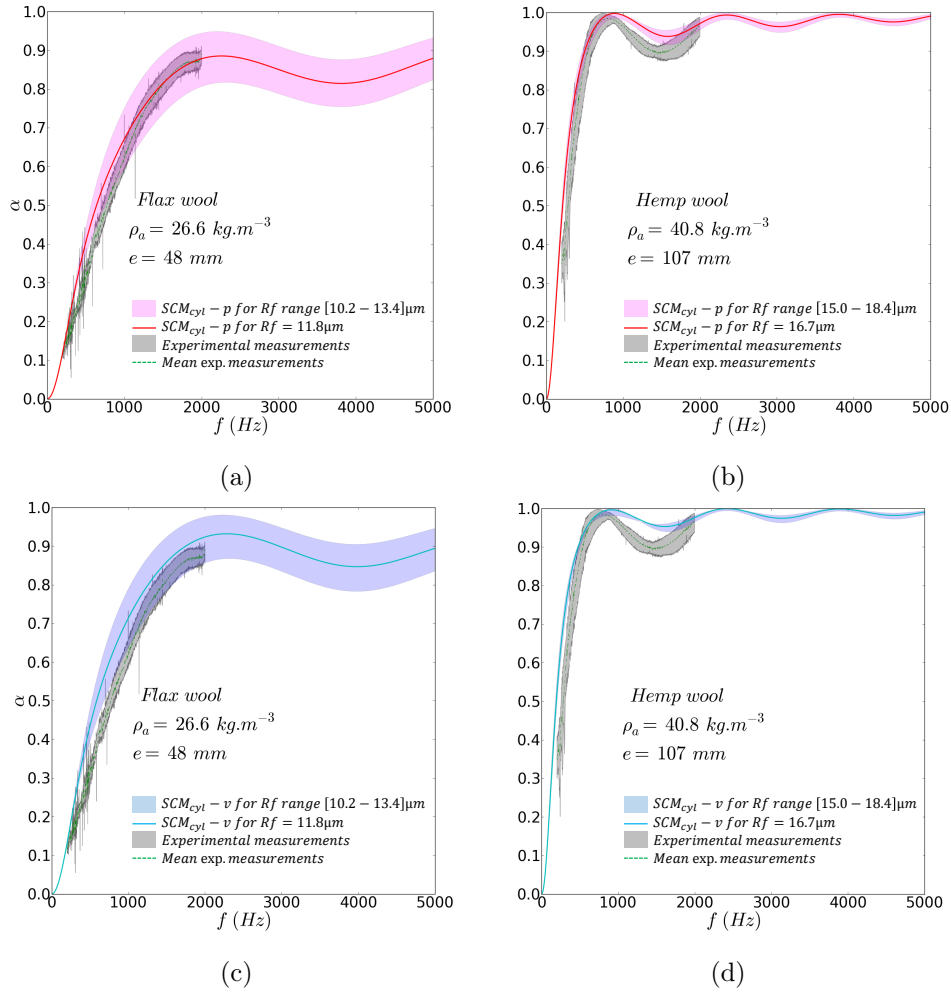


FIGURE 8: Experimental characterisation and modeling of the sound absorption coefficient as a function of frequency for (a) the flax wool and the $SCM_{cyl} - p$ modeling, (b) the hemp wool and the $SCM_{cyl} - p$ modeling, (c) the flax wool and the $SCM_{cyl} - v$ modeling and (d) the hemp wool and the $SCM_{cyl} - v$ modeling

approach has a lower mean relative deviation than the experimental relative deviation, as shown in Table 2. Indeed, both values are less than 10%. In the both cases, the flow approach is slightly further away than the pressure approach. As shown in Table 2, for the hemp wool, the relative deviation is less than 10%, but for the flax wool, it is higher but remains close to the experimental mean

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9 deviation.

Material	Mean relative deviation (%)		
	Exp. mean relative deviation (%)	p	v
Flax	11.8	9.4	16.1
Hemp	11.7	6.4	8.9

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19 TABLE 2: Relative deviation of the experimental measurements and mean relative deviation
20 between SCM_{cyl} modeling and mean experimental values.
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23 So, both $SCM_{cyl} - p$ and $SCM_{cyl} - v$ modeling approaches developed in
24 this paper can be validated in order to determine sound absorption coefficient
25 of vegetal wools.
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28 On the other hand, the sound absorption deviation as a function of fibre radii
29 dispersion (values are indicated in Table 1) is shown in Fig. 8. It gives an over-
30 view of the SCM_{cyl} modeling sensitivity regarding the fiber radius value, which
31 is a key input parameter, in these two particular cases. The results are similar
32 for both pressure and flow approaches, but are different for each material. In
33 our case, where the both materials have equivalent airflow resistivities, the sensi-
34 tivity decreases as the thickness of the material increases. However, this result
35 would require a more systematic study in order to better understand the rela-
36 tionship between the modeling sensitivity and parameters such as fibre radius,
37 porosity, airflow resistivity, material thickness etc. Finally, by using both sound
38 absorption coefficient and porosity values, both of these modeling approaches
39 can also be used to obtain an equivalent fibre radius for a fibrous material or
40 more precisely, a range of fibre radii to be consistent with the previous result.
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49 3.4. Limits and outlooks about the SCM_{cyl} approaches

50 A huge benefit of the SCM_{cyl} method developed here is that it is based on
51 only two parameters, a porosity value and a mean fibre radius. However, vegetal
52 wools are often made up of other fibre types that may have different radii. So, to
53 take a second fibre type into account, it is possible to mix the SCM_{cyl} modeling
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9 method with a composite modeling approach as in [8]. This modeling approach
10 has been elaborated to describe materials including two types of microstructures.
11 In the case of vegetal wools, the material is considered as a mixture of two fibrous
12 media represented by a volume fraction of polymer fibres within vegetal ones.
13 Moreover, in order to better model the behaviour of vegetal wools, it might also
14 be relevant to take the variability of vegetal fibre distributions into account,
15 using the whole size distribution of materials. Indeed, it could lead in extreme
16 cases to double porosity effects as shown in [56] for hemp particles. In this paper,
17 the choice has been done to develop the SCM_{cyl} modeling with a focus only on
18 the specific case of a perpendicular sound propagation. However, it would also be
19 relevant to take a mix of both perpendicular and parallel sound propagation into
20 account in the modeling approach. Indeed, during the manufacturing process,
21 the fibres are not always arranged in regular parallel layers and may have a
22 low inclination. Finally, the SCM_{cyl} modeling method has been validated for a
23 frequency range specific to the building field. Nevertheless, it also seems relevant
24 to study the low and high frequency limits of both visco-inertial and thermal
25 permeabilities (Π and Ξ) using the SCM_{cyl} relationships. It would then be
26 possible to relate the SCM_{cyl} modeling approaches to the specific parameters
27 of the fluid-equivalent models used for porous materials.
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41 **4. Conclusion**

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43 In this paper, a self-consistent modeling approach for the sound absorption
44 properties of fibrous materials has been developed. It is called SCM_{cyl} . By
45 using *HPM*, it is based on the rigorous establishment of macroscopic behaviour
46 laws for fluid flow relating to the dissipation phenomena of visco-inertial and
47 thermal effects. In order to establish analytical relationships between specific
48 microscale fibrous parameters with their macroscopic properties, assumptions
49 are made to represent the microstructure as a generic cylindrical inclusion (a
50 solid phase included in a fluid phase) which is close to the fibre morphology. So,
51 the development of the SCM_{cyl} modeling led to equations for both the dynamic
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9 density ρ and the bulk modulus K . For ρ two possible solutions are obtained : a
10 velocity approach $\rho - v$ and a pressure approach $\rho - p$. Finally, both $SCM_{cyl - v}$
11 and $SCM_{cyl - p}$ approaches lead to a useful sound absorption modeling based on
12 415 and $SCM_{cyl - p}$ approaches lead to a useful sound absorption modeling based on
13 only two input parameters : a porosity value (ϕ) and a mean fibre radius (Rf).
14 These approaches has been validated for the vegetal wools case by showing
15 a fit between both $SCM_{cyl - v}$ and $SCM_{cyl - p}$ modeling predictions with
16 experimental measurements. It is also possible to reverse the SCM_{cyl} modeling
17 420 in order to obtain an equivalent fibre radius value by using a porosity and a
18 sound absorption coefficient values. Nevertheless, it is necessary to take the
19 dispersions related to the used parameters into account in this inversion. In
20 order to extend the field of use, the modeling approaches developed here can
21 be applied to other fibrous materials and even to the case of materials that
22 can be represented by cylindrical geometries and subjected to flow propagation.
23 425 Finally, future work may also investigate the possibility of joint approaches
24 with SCM modeling methods developed for the determination of the fibrous
25 materials thermal properties.
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