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Manuel Théodet, Cyril Quilfen, Cristina Martínez, Cyril Aymonier. Continuous supercritical synthesis of unsupported and high specific surface area catalyst precursors for deep-hydrodesulfurization. *Journal of Supercritical Fluids*, 2016, 117, pp.252-259. 10.1016/j.supflu.2016.07.002 . hal-03113987

**HAL Id: hal-03113987**

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Submitted on 24 Nov 2023

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This paper must be cited as:

Theodet, M.; Quilfen, C.; Martínez, C.; Aymonier, C. (2016). Continuous supercritical synthesis of unsupported and high specific surface area catalyst precursors for deep-hydrodesulfurization. *Journal of Supercritical Fluids*. 117:252-259.  
doi:10.1016/j.supflu.2016.07.002.



The final publication is available at

<http://dx.doi.org/10.1016/j.supflu.2016.07.002>

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Additional Information

# Continuous supercritical synthesis of unsupported and high specific surface area catalyst precursors for deep-hydrodesulfurization

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**Abstract:** Unsupported and high specific surface area ( $S_{\text{BET}}$ ) catalyst precursors for deep-hydrodesulfurization (deep-HDS) are obtained using an environmental friendly, continuous and fast synthesis process in supercritical water/alcohol mixtures. This approach offers an access to high production rate and upscaling. Two mixed oxides were synthesized:  $\text{NiMoO}_4$ , which is the preferred material when deep-HDS is investigating, and  $\text{CoMoO}_4$  preferred for simple HDS. The role of the water/alcohol mixture on the resulting specific surface area has been studied and allows a controlled adjustment of the resulting specific surface area. The obtained  $\text{NiMoO}_4$  material consists of the highly active hydrate  $\text{NiMoO}_4 \cdot 0.75\text{H}_2\text{O}$  phase with a controlled composition and specific surface area up to  $200 \text{ m}^2 \cdot \text{g}^{-1}$ . Resulting materials have shown great performances when tested in deep-HDS catalytic tests.

## Introduction

Due to increasingly stringent environmental regulations in sulfur limits for distillates fuels, production of ultra-low sulfur content fuels is required to reach the limits of 10 ppm in the European Union <sup>1</sup> and Japan <sup>2</sup> and 15 ppm in North America<sup>3,4</sup>. Moreover, remaining available crude oils resources contain a greater amount of undesirable heteroatoms that will have to be removed. Removals of 99.99% of sulfur from typical crude oil and the corresponding processes have been termed as deep-HDS. The main issue of deep-HDS is the elimination of refractory sulfur compounds such as 4,6-dimethyldibenzothiophene (4,6-DMDBT). In order to achieve this issue without expensive costs in process modifications, the development of more efficient deep-HDS catalysts is required.

Typically, a HDS catalyst contains a metal from the group VIB (chromium, molybdenum or tungsten) promoted with a metal from the group VII (cobalt or nickel) and supported, classically, on alumina <sup>5-7</sup>. These conventional catalysts are generally obtained by impregnation of  $\gamma\text{-Al}_2\text{O}_3$  with aqueous solutions of  $(\text{NH}_4)_6\text{Mo}_7\text{O}_{24} \cdot 4\text{H}_2\text{O}$  and  $\text{Co}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$  or  $\text{Ni}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$  followed by drying, calcination and activation under  $\text{H}_2/\text{H}_2\text{S}$  <sup>8</sup> in order to obtain  $\text{MoS}_2$  layers well dispersed on the  $\gamma\text{-Al}_2\text{O}_3$  support and edges-decorated with Co or Ni <sup>9</sup>. However, current HDS catalysts revealed to be insufficient and strong optimizations have been investigated over the past decades, such as improvement of the support and/or of the active phase<sup>10</sup>.

On the other hand, some unsupported materials have been described with higher activity and/or selectivity than traditional

supported catalysts, leading to a growing interest in unsupported HDS nano-catalysts <sup>11-20</sup>. This category of catalysts can easily be obtained by thermal decomposition <sup>21,22</sup>, metal amines metallates <sup>16</sup>, hydrothermal <sup>23</sup>, citrate <sup>24</sup>, freeze-drying <sup>25</sup> and impregnation <sup>26</sup> for the most classical methods. However, their main weakness compared to supported catalysts is their low specific surface area ( $S_{\text{BET}}$ ), down to 10 to  $80 \text{ m}^2 \cdot \text{g}^{-1}$  for most of the unsupported catalysts <sup>16,21,26-29</sup>. However recent works have reported maximum values for  $S_{\text{BET}}$  around 200 to  $300 \text{ m}^2 \cdot \text{g}^{-1}$  <sup>30,31</sup>, similar than those presented by alumina supported catalysts ( $200$  to  $300 \text{ m}^2 \cdot \text{g}^{-1}$ ) <sup>32</sup>.

Increasing  $S_{\text{BET}}$  appears to be a very interesting challenge in the development of this new generation of catalysts but most of the time, high  $S_{\text{BET}}$  unsupported catalysts synthesis generate toxic compounds and therefore are difficult to implement as industrial scale<sup>31</sup>. In order to do so, supercritical fluids technologies are known to be efficient to prepare highly dispersed nanostructures<sup>33</sup> and nanopowders with high  $S_{\text{BET}}$ <sup>34,35</sup> without generation of toxic compounds. In this work we propose the use of green solvents (water/alcohols), inexpensive (ten times cheaper than the ones use in conventional methods for high  $S_{\text{BET}}$  materials<sup>31</sup>) and friendly precursors. Moreover, our approach allows the synthesis of crystalline materials with controlled and adjustable composition<sup>36-39</sup> but also with a tuneable specific surface area<sup>34</sup> by playing with the carbon length of the alcohol used. These materials are produced in a fast, sustainable and continuous process which is a major asset for upscaling<sup>40</sup>. All these advantages are obviously linked to the good activities of our materials in deep-HDS. Our catalyst precursors have shown a similar activity in removing the most refractory compound (4,6-DMDBT) to those of a reference catalyst but to a lower reaction temperature of  $40^\circ\text{C}$ . As far as we know, the use of this

method to synthesize Ni(Co)MoO<sub>4</sub> has not been so far reported in the literature.

## Experimental

### Materials and methods

Bis(acetylacetonato)dioxomolybdenum(VI) (MoO<sub>2</sub>(CH<sub>3</sub>COCHCOCH<sub>3</sub>)<sub>2</sub>, Alfa Aesar, 99%), nickel(II) acetate tetrahydrate (Ni(CH<sub>3</sub>COO)<sub>2</sub>·4H<sub>2</sub>O, Alfa Aesar, 99%) and cobalt(II) acetate tetrahydrate (Co(CH<sub>3</sub>COO)<sub>2</sub>·4H<sub>2</sub>O, Alfa Aesar, 98%) were used without further purification.

### Synthesis procedures

The starting Ni(Co)- and Mo-containing solutions were prepared as follows: Mo salt was dissolved in a water/alcohol mixture of molar ratio 1:1 and Ni(Co) precursor was previously dissolved in distilled water before adding the same quantity of alcohol in order to prevent the precipitation due to alcohol aversion of the acetate. The alcohols used in this study were methanol, ethanol and isopropanol. Molybdenum concentration was fixed at [Mo]=7.2·10<sup>-3</sup> mol·L<sup>-1</sup> and Ni concentration was adjusted to vary the metal molar ratios (36 – 50 – 57 – 60 – 66 at%). For cobalt, the concentration used was equal to the one of Mo. Those solutions of precursors were then injected in a continuous reactor, where they reached supercritical conditions, typically for a residence time of 55s<sup>37,38</sup>. A chemical reaction takes place leading to the nucleation and growth of the NiMo or CoMo nanoparticles. These last ones followed their way to a filter deepened in an ice bath to quench their growth. The obtained powder was washed with distilled water, recovered by vacuum filtration and dried at room temperature before a thermal treatment at 400°C for 3 hours.

### Characterization techniques

Metal ratios were determined by Inductively Coupled Plasma/Optical Emission Spectrometry (ICP-OES) using a Varian 720-ES equipment. Carbon pollutions were detected using CHNS-O analysis, accomplished by combustion analysis according to the Pregl-Dumas procedure. The equipment used was a Flash EH 1112 from Thermo Fisher.

X-Ray powder diffraction (XRD) patterns were obtained from a Philips PW1820 and a PANalytical X'Pert X-Ray diffractometers in Bragg-Brentano geometry equipped with Cu K $\alpha$ 1 source and an X'Celerator detector. Diffraction patterns were collected with a 2 $\theta$  step of 0.02° and a 0.0358°·s<sup>-1</sup> scan speed routine mode; for more advanced investigations a 0.008° step and a 0.0053°·s<sup>-1</sup> scan speed were used on a PANalytical X'Pert pro MOO equipped with primary Ge (111) monochromator Cu K $\alpha$ 1 source. The cell fitting, and thus the cell volume, were obtained by profile fitting of the pattern with the FULLPROF program. The fits were performed using a pseudo-Voigt peak-shape function. In the final runs, the usual profile parameters (scale factors, background coefficients, zero point,

half-widths, pseudo-Voigt and asymmetry parameters for the peak shape) were refined.

The morphology of the powders was observed using a scanning electron microscope (JEOL 6700F) operating at an accelerating voltage of 30 kV. The size of the nanoparticles was evaluated using a high-resolution transmission electron microscope (JEOL JEM-2200FS) enable to switch to a scanning mode to make chemical X-Ray mapping of nanoparticles.

Physisorption measurements were performed using an Autosorb-1 instrument from Quantachrome. The BET specific areas were determined by N<sub>2</sub> adsorption at 77K assuming a cross-sectional area of 0.162 nm<sup>2</sup> for the nitrogen molecule. Prior to adsorption measurements, the samples were outgassed in a vacuum at room temperature for 2 hours.

### Catalytic tests

The model feedstock used was composed of 60 wt% of paraffins, 30 wt% of olefins and 10 wt% of aromatic hydrocarbons, in order to deal with a possible “matrix effect”. The detailed composition can be found in Table S3 enclosed in S.I. The total sulfur content was 500 wppm with 100 wppm as 4,6-DMDBT, the most refractory compound. No nitrogen compounds were added to the feedstock in order to avoid the competition with HDN.

The activity tests were conducted in a fixed bed tubular reactor. The reactor was charged with 160  $\mu$ L of catalyst (pelletized at a diameter comprised between 0.250  $\mu$ m and 0.425  $\mu$ m) and diluted in SiC (diluent/catalyst volume ratio of 12). The activation of the catalyst was done *in situ* using a mixture of H<sub>2</sub>S/H<sub>2</sub> with 10 vol% H<sub>2</sub>S at atmospheric pressure and a temperature of 400°C for 3 h. The reaction conditions were the following: total pressure of 3.5 MPa, temperature of reaction between 320 and 400°C, Liquid Hourly Space Velocity (LHSV) of 39 h<sup>-1</sup> and a ratio H<sub>2</sub>/feed of 5. For each test, liquid samples were accumulated, weighted and analyzed at intervals of about 40 min. For all catalysts, a constant composition of the reactor outlet stream was observed after reaction periods of 3 to 4 h. Results reported in this work correspond to the steady-state period of operation. The composition of feed and products was analyzed by gas chromatography in a Varian 3800 equipped with a 30 m column (VF 5ms CP8944) with an inner diameter of 0.25 mm and a bonded stationary phase made of a 0.25  $\mu$ m thick film of (5 % phenyl, 95 % dimethyl) polysiloxane, and two detectors, a Flame Ionization Detector and a sulfur specific Pulsed Flame Photometric Detector.

## Results and discussion

### NiMo based catalyst precursors for deep HDS

NiMoO<sub>4</sub> may exist in several polymorphs at atmospheric pressure: the low temperature stable  $\alpha$ -phase<sup>41</sup>, the high temperature stable  $\beta$ -phase<sup>42</sup> and the hydrate NiMoO<sub>4</sub>·nH<sub>2</sub>O (n=0,75, 1) phase<sup>43-46</sup>. According to the literature, the pure  $\beta$ -

phase is generated by heating the  $\alpha$ -NiMoO<sub>4</sub> at temperatures above 690 °C and is stable only if kept over 180 °C<sup>28,47</sup>.

Both phases ( $\alpha$  and  $\beta$ ) are monoclinic with space group C2/m<sup>48</sup>. The structural building units of  $\alpha$ -NiMoO<sub>4</sub> (isotypic with  $\alpha$ -CoMoO<sub>4</sub><sup>41</sup>) are NiO<sub>6</sub> and MoO<sub>6</sub> distorted octahedra, which share edges and form chains parallel to the “c” direction. Each chain is surrounded by four other chains and linked to them by corner sharing of oxygen atoms. Between the filled chains there are chains of unfilled octahedra. It also presents alternative layers of NiMo<sub>6</sub> and MoO<sub>6</sub> parallel to the “b” direction. The structure of  $\beta$ -NiMoO<sub>4</sub> is isotypic with  $\alpha$ -MnMoO<sub>4</sub> (ICSD #78328). By analogy, it consists of molybdate distorted tetrahedra, which share corners with four different nickelate octahedra. The general description is similar to the  $\alpha$ -phase with chains joined by corner sharing of oxygen atoms and with chains of unfilled octahedral between them. The difference between the two phases is a contraction in the “c” axis and an expansion in the “a” and “b” axes of the cell in the  $\beta$ -form compared to the  $\alpha$ -form. The formal oxidation state of Ni is +II, whereas the one of Mo is +VI as in MoO<sub>3</sub><sup>44</sup>.

Recent studies give a description of the hydrated phase NiMoO<sub>4</sub>.nH<sub>2</sub>O with n = 1 or 0.75<sup>46</sup>. Measurements of differential thermal analysis (DTA) suggest that in these systems the metal cations have a coordination similar to that observed in  $\beta$ -NiMoO<sub>4</sub>. The NiMoO<sub>4</sub>.0.75H<sub>2</sub>O structure has been described as a triclinic system (space group *P*-1) with tetrameric z-shaped unit of Ni octahedra, two NiO<sub>6</sub> and two NiO<sub>5</sub>(OH<sub>2</sub>), that share edges. These units are interconnected by MoO<sub>4</sub> tetrahedra to form a network structure with open channels<sup>46</sup>. NiMoO<sub>4</sub>.H<sub>2</sub>O might present a similar structure with lattice and coordination water. The HDS activity of these systems increased in the following order:  $\alpha < \beta < \text{hydrate}$ <sup>27,28</sup>.

The TGA-MS of the powders obtained directly after synthesis in supercritical water/alcohol system displays three main mass losses for a total mass loss of 8 wt% (see Figure S1 enclosed in S.I.). A first loss of 2.8 wt% between room temperature and 243 °C can be attributed to adsorbed water as shown in the mass spectrometry results (line of mass 18). The second mass loss of 4.20 wt% occurring from 243 °C to 468 °C can be attributed this time to the departure of structural water and some carbon according to the line shape of masses 18 and 44 (CHNS-O analyses give a mean of 0.4 wt% carbon in the powders) as for the third mass loss of 0.5 wt% between 468 °C and 538 °C. The last mass loss which occurred between 538 °C and 800 °C seems to be exclusively due to the carbon departure. Those water losses are in good agreement with results obtained by Rodriguez *et al.*<sup>43</sup> and Eda *et al.*<sup>46</sup> on their study of NiMoO<sub>4</sub>.nH<sub>2</sub>O (n = 0.75 or 1). Upon heating NiMoO<sub>4</sub>.nH<sub>2</sub>O to high temperatures in TGA-MS experiments, they also observed that water desorbs in three peaks. The first at 100-200 °C is associated with water molecules reversibly bounded to the hydrate. The second from 200 to 400 °C corresponds to desorption of water molecules that form part of the hydrate crystal structure, and they also assessed that at the onset of this peak, the formation of  $\beta$ -NiMoO<sub>4</sub> starts. They pointed out an additional small desorption peak between 490 °C and 520 °C,

also attributed to water. Eda considers that the ideal hydrate is NiMoO<sub>4</sub>.0.75H<sub>2</sub>O, and based on the mass loss obtained with our TGA, we may approximate the same value for our material.

The XRD patterns shown in Figure 1 are representative of the products resulting from the synthesis in supercritical water/alcohol system ((a) isopropanol, (b) ethanol). Most of the peaks can be assigned to the above mentioned hydrate nickel molybdate NiMoO<sub>4</sub>.xH<sub>2</sub>O (JCPDS N° 13-0128) (no defined value for x, structure represented in Figure 1); this is consistent with the assumption made previously. The presence of MoO<sub>3</sub>.H<sub>2</sub>O (JCPDS N° 01-0125) and MoO<sub>2</sub> (JCPDS N° 32-0671) is also detected. This is due to an excess of Mo in those specific samples. More surprisingly,  $\beta$ -NiMoO<sub>4</sub> (JCPDS N° 45-0142) is also detected despite the fact that it is not stable at room temperature. During thermal treatment (400 °C, 3 h, air atmosphere), the most remarkable features observed on XRD patterns acquired in temperature are the systematic transition of the hydrate NiMoO<sub>4</sub>.0.75H<sub>2</sub>O into  $\beta$ -NiMoO<sub>4</sub> at 400 °C while heating and the systematic transition into  $\alpha$ -NiMoO<sub>4</sub> (JCPDS N° 86-0361) at 200 °C when cooling down. The nature of these two phases has been assessed by Rietveld refinement with fairly good refinement parameters ( $\beta$ : Bragg R-factor = 4.96,  $\chi^2$  = 2.38, cR<sub>wp</sub> = 14.3;  $\alpha$ : Bragg R-factor = 7.35,  $\chi^2$  = 4.11, cR<sub>wp</sub> = 14.2, see Table S1 and Table S2 enclosed in S.I.).

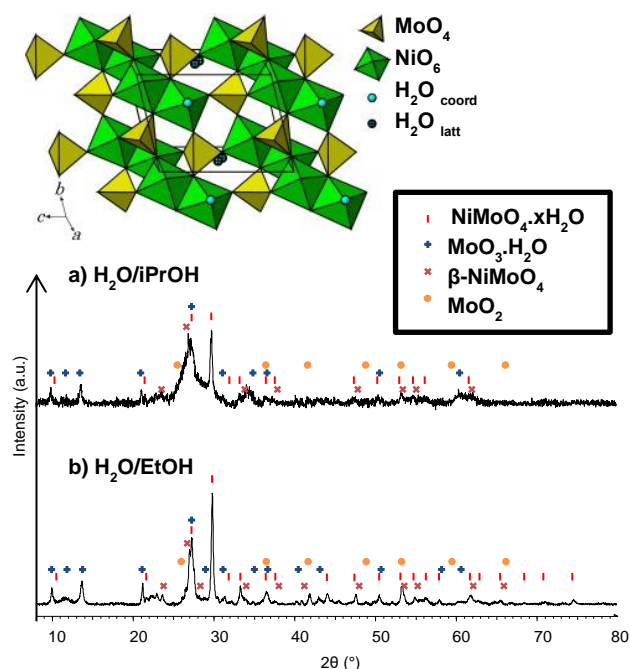


Figure 1: XRD patterns of a stoichiometric “NiMo” based powder synthesized in a) scH<sub>2</sub>O/iPrOH and b) scH<sub>2</sub>O/EtOH. Above is the structure of NiMoO<sub>4</sub>.0.75H<sub>2</sub>O (from Eda *et al.*<sup>37</sup>)

The SEM micrographs of the as-obtained powders and calcined powders (400 °C, 3 h) are shown in Figure 2.a) (synthesis carried out in ethanol). The as-obtained powders mainly consist of rod-like NiMoO<sub>4</sub>.0.75H<sub>2</sub>O particles of dispersed sizes. After calcination the rods have collapsed and somehow sintered.

The most interesting result obtained concerns the evolution of the specific surface area as a function of the alcohol nature as illustrated in Figure 2.b. The nature of the alcohol used plays a major role on the specific surface area, that increases from a value of 79  $\text{m}^2\cdot\text{g}^{-1}$  using methanol as solvent up to 179  $\text{m}^2\cdot\text{g}^{-1}$  using isopropanol as solvent. This result is fully consistent with a previous study on the formation of  $\text{CeO}_2$  nanocrystals in supercritical alcohols<sup>34</sup>.  $\text{CeO}_2$  nanopowders exhibit specific surface areas of 60, 106 and 140  $\text{m}^2\cdot\text{g}^{-1}$  when prepared in pure methanol, ethanol and isopropanol, respectively. The same trend is observed for NiMo synthesis in the  $\text{H}_2\text{O}/\text{ROH}$  systems. This means that the alcohol is playing the role of solvent with water but also of functionalization agent as demonstrated for  $\text{CeO}_2$ <sup>49</sup> with a direct impact on the catalyst precursor thermal stability<sup>34</sup>.

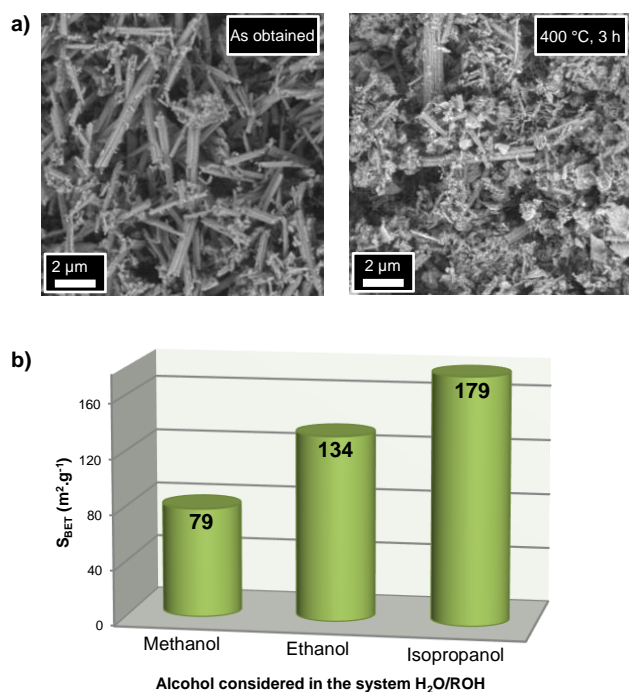
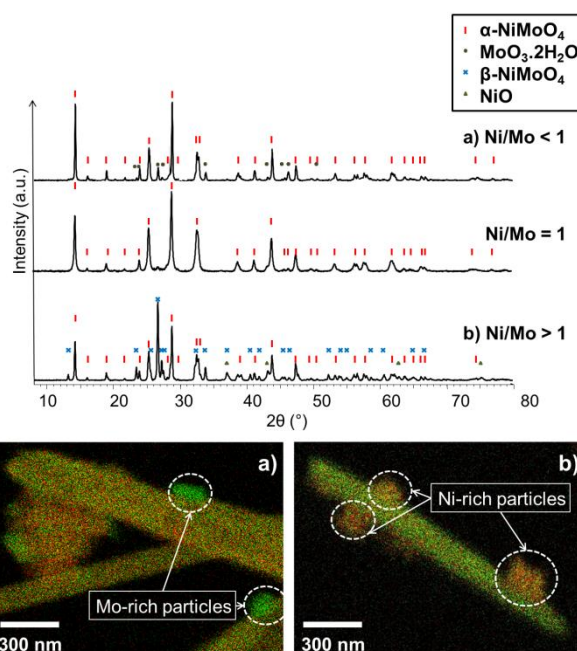


Figure 2: a) SEM micrographs of as obtained powder synthesized in  $\text{H}_2\text{O}/\text{EtOH}$  mixture on the left and the same powder treated for 3 h at 400°C on the right and b) Evolution of the catalyst precursor  $S_{\text{BET}}$  as a function of the alcohol nature used in the supercritical solvent before thermal treatment.

XRD patterns of calcined powders (3 h at 400 °C) with a different cations ratio are displayed in Figure 3. Two trends arise: for  $\text{Ni}/\text{Mo} < 1$ , we obtain the  $\alpha$ - $\text{NiMoO}_4$  phase together with  $\text{MoO}_3\cdot 2\text{H}_2\text{O}$  phase (XRD pattern of the powder with 64 at% Mo) and for  $\text{Ni}/\text{Mo} > 1$ , we obtain both  $\alpha$ - and  $\beta$ -phases of  $\text{NiMoO}_4$  together with  $\text{NiO}$ .

The STEM-EDX chemical mapping associated with these two compositions illustrates this fact showing the presence of particles containing only Mo for a) and particularly rich in Ni for b). These results are in agreement with studies carried out by Di Renzo *et al.*<sup>50,51</sup> concerning the stabilization of  $\beta$ - $\text{NiMoO}_4$  at

room temperature with an excess of nickel. According to their work, only the  $\alpha$ -phase can be considered as a stoichiometric



compound whereas the  $\beta$ -phases can form solid solutions with Ni by insertion in localized vacant sites in the network of  $\beta$ - $\text{NiMoO}_4$ , thus stabilizing its structure. This effect is not observed with Mo assumingly due to an obvious matter of steric hindrance.

Figure 3: XRD patterns and their associated SEM-EDX chemical mappings of “NiMo” based powder synthesized in supercritical  $\text{H}_2\text{O}/\text{iPrOH}$  mixture with a) an excess of Mo and b) an excess of Ni. Powders are calcined 3 h at 400°C

For most of the synthesized samples, the hydrate nickel molybdate phase was obtained with another phase depending of the stoichiometric ratio of each element.

#### CoMo catalyst precursors for deep HDS

Since our main objective concerns deep-HDS,  $\text{CoMoO}_4$  was not the privileged material since it is less efficient than  $\text{NiMoO}_4$ . However, it was interesting to study the application of our fast (55s) and continuous synthesis method on  $\text{CoMoO}_4$ .  $\text{CoMoO}_4$  can adopt two different polymorphic forms,  $\alpha$  and  $\beta$ <sup>52</sup>. The  $\beta$ - $\text{CoMoO}_4$  is the high temperature stable phase. Like in  $\text{NiMoO}_4$ , the structure of the  $\beta$  form is monoclinic (space group  $C2/m$ ) with 6 and 4 as coordination numbers, respectively for Co(II) and Mo(VI). The structure of the  $\alpha$ - $\text{CoMoO}_4$  is also monoclinic with the same space group. It is more compact and differs from  $\beta$ - $\text{CoMoO}_4$  in the coordination of Mo(VI) which is 6 in this case. The difference between the two phases again lies is a contraction in the “c” axis and an expansion in the “a” and “b” axes of the cell.

The XRD pattern acquired directly after reaction fits with a mixture of the two different structures of  $\text{CoMoO}_4$  (Figure 4.a). The  $\beta$ -isomorph is clearly the majority phase. Nothing surprising since it has already been proved that, unlike  $\beta$ - $\text{NiMoO}_4$ , which is unstable below 180 °C,  $\beta$ - $\text{CoMoO}_4$  can be easily stabilized at

room temperature<sup>52</sup>. As the XRD patterns also shown (Figure 4.b), the  $\alpha$ -phase almost disappears after thermal treatment at 400 °C for 3 h.

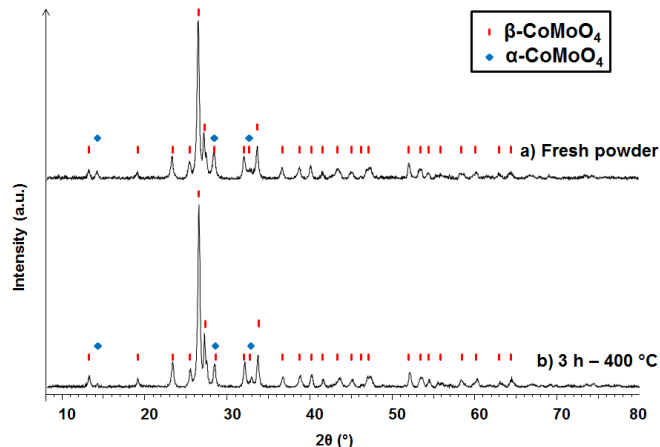


Figure 4: XRD patterns of stoichiometric "CoMo" based powders synthesized in  $\text{scH}_2\text{O}/i\text{PrOH}$  mixture with a) the obtained powder and b) after calcination for 3 h at 400 °C.

#### Catalytic tests

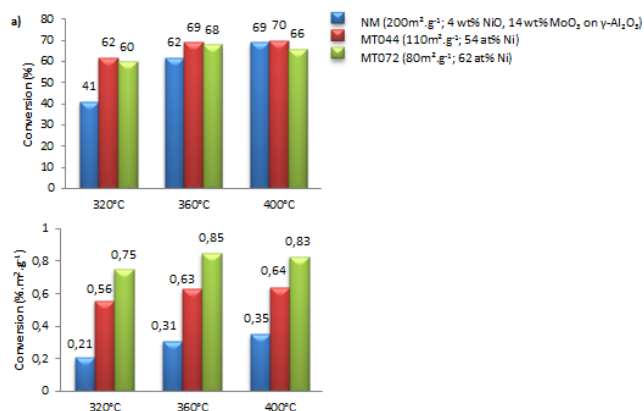
The catalytic behaviour of these materials was evaluated by comparison with a commercial supported catalyst, NM, used as reference ( $200 \text{ m}^2 \cdot \text{g}^{-1}$ , 4 wt% NiO, 14 wt%  $\text{MoO}_3/\gamma\text{-Al}_2\text{O}_3$ ).

In order to study the influence of the composition in our unsupported catalysts, three different compositions with a ratio Ni/Mo > 1 were tested and compared to the reference supported catalyst. First, the materials with a Ni atomic fraction of 54 at% (MT044) and of 62 at% (MT072) were tested at a LHSV of  $39 \text{ h}^{-1}$  and results are presented in Figure 5.a. In a second series, the materials with a Ni atomic fraction of 69 at% (MT043) and of 62 at% (MT072) were tested at a LHSV of  $150 \text{ h}^{-1}$  and results are presented in Figure 5.b. 4,6-DMDBT conversion is presented in absolute values (top) and normalized considering the total surface area (bottom) in order to focus on the effect of the composition and minimizing the contribution of the specific surface area.

The results show that our bulk materials are significantly more active than the commercial reference when we directly compare the 4,6-DMDBT conversion obtained with catalysts MT044 and MT072 at our lowest operation temperature of 320 °C (see Figure 5-a, top). The DMDBT conversion values obtained with these unsupported catalysts at 320 °C are comparable to the conversion given by the  $\text{NiMo}/\text{Al}_2\text{O}_3$  (NM) at 360 °C. Thus, for similar conversion and similar amount of catalyst, the unsupported nanostructured catalysts can operate at lower temperature than NM and therefore, for similar conversion under similar operating conditions, a lower mass of our catalyst would be required to achieve the same conversion levels of the commercial reference. The lower activity of NM at lower temperature becomes even more evident when the results are given as surface area activities, normalized according to the BET surface area of the catalysts

(see Figure 5-a, bottom). In previous publications<sup>13</sup>, the activity of unsupported HDS catalysts was only comparable to that of commercial  $\text{Al}_2\text{O}_3$  supported catalysts, and the latter was surpassed only when normalized to the catalyst surface area. Eijsbouts et al.<sup>12</sup> have shown that addition of unsupported transition metal sulfide catalysts (Nebula® belonging to the NEBULA catalyst family developed by Albemarle Catalysts and ExxonMobil) to a conventional HDS catalyst allows decreasing their ULSD operation temperature in 15 °C. It must be noted that the NEBULA Technology is being used commercially since 2001. Unsupported Ni-W-Mo catalysts were shown recently to be more active than a traditional supported reference catalyst for HDS of a straight-run gas oil<sup>53</sup>. However, comparison with our results is not straightforward, as these catalysts were diluted with an alumina binder, and catalytic tests were performed at a considerably lower space velocity (LHSV=2  $\text{h}^{-1}$ , instead of 39-150  $\text{h}^{-1}$  used in this work).

Secondly, combining results of experiments done at a LHSV of  $39 \text{ h}^{-1}$  and at a LHSV of  $150 \text{ h}^{-1}$ , the trend of activity is the following: MT072 (62 at% Ni) > MT043 (69 at% Ni) and MT072 (62 at% Ni) > MT042 (54 at% Ni). This suggests that an optimum atomic percentage of Ni exists (around 60 at% Ni) for which the conversion of 4,6-DMDBT is maximum. We think that the higher the Ni content in the material, the higher the  $\beta\text{-NiMoO}_4$  proportion phase in our unsupported HDS catalyst precursor. As known, when sulfided, the  $\beta\text{-NiMoO}_4$  is the most active phase in HDS. Moreover, it is known that the active sites are located on the  $\text{MoS}_2$  layers whereas Ni has a promoting effect. An excess of Ni will cover the  $\text{MoS}_2$  surface and may reduce the accessibility of sulfur compounds to the active sites. Thus, there should be a maximum Ni content (comprised between 54 at% and 69 at% of Ni) for which the formation of the  $\beta\text{-NiMoO}_4$  phase is maximized without diminishing the number of active sites. An optimum Ni/(Mo+Ni) mole ratio of 0.5 was also found for unsupported NiMo sulfide catalysts prepared by means of hydrothermal synthesis<sup>54</sup>. The sample with this composition gave maximum DBT and 4,6-DMDBT conversion at 350 °C under batch conditions.



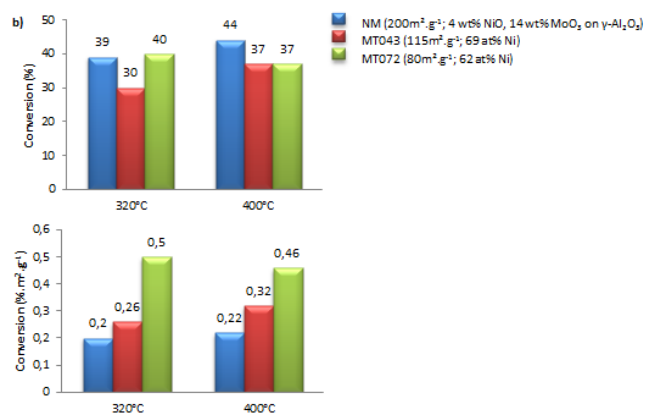


Figure 5: a) Conversion of 4,6-DMDBT in a model feedstock (see Experimental part, LHSV=39h<sup>-1</sup>), b) Conversion of 4,6-DMDBT in a model feedstock (see Experimental part, LHSV=150 h<sup>-1</sup>)

Our samples have been tested under HDS conditions for deep-HDS of a complex model feedstock in order to study their efficiency of removing organosulfur molecules. They have shown significantly higher conversion as compared to a commercial reference at low temperatures (320°C). This could be translated into reduced energetics or catalyst related costs when using the bulk precursors obtained by continuous supercritical synthesis at conversion levels comparable to those obtained with conventional supported catalysts. It has also been shown that a maximum of activity exists for a Ni content around 60 at%.

Finally, tests were carried out on an industrial Light Cycled Oil (LCO) feedstock (S content = 5200 wppm, more details are given in S.I.) in order to evaluate the behaviour of our material under more realistic deep-HDS conditions. The preliminary results obtained at a pressure of 3.5 MPa, LHSV of 150 h<sup>-1</sup> and MG/ML of 5, are presented in Figure 6. Even though experimental conditions were not fully optimized, this first set of experiments demonstrates the capability of the new materials described in this work for the desulfurization of an industrial feedstock and evidences their potential as deep-HDS bulk catalysts.

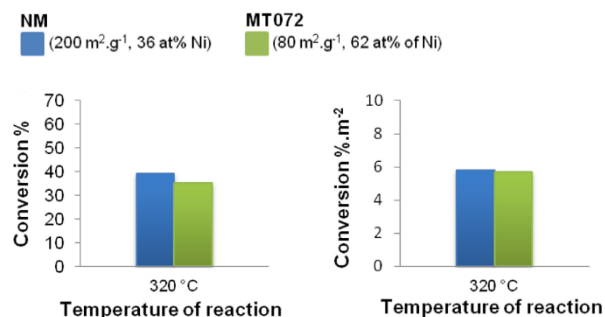


Figure 6: Total sulfur conversion by deep-HDS of an industrial feedstock (P=3.5 MPa, LHSV = 150 h<sup>-1</sup>, MG/ML = 5)

## Conclusions

This paper proposes a novel, fast and continuous method to produce high specific surface area deep HDS unsupported catalyst precursors with controlled composition using supercritical water/alcohols mixtures. Furthermore, this method provides an exceptional opportunity to produce nanostructured catalyst precursors in an environmentally friendly medium with high production rate and possible scale up at an industrial scale. This study describes the synthesis of high surface area materials Ni-Mo and Co-Mo based oxides in supercritical fluids. The most active phases in HDS (NiMoO<sub>4</sub>·0.75H<sub>2</sub>O and β-NiMoO<sub>4</sub>), according to the literature, have been obtained and stabilized at room temperature. It has been shown that the nature of the alcohol plays a major role in the evolution of surface area.

Catalytic tests have shown better conversion of 4,6-DMDBT than the commercial reference and the deep-HDS reaction can be performed at lower temperature when using these nanostructured unsupported catalysts. It has also been demonstrated that there is an optimal value for Ni concentration where the activity of the catalyst is the maximum.

## Acknowledgements

This work was supported by the CNRS and UPV. Dr M. Théodet is grateful to the French Ministry of Education, Research and Technology (MENRT) for a doctoral grant. The authors acknowledge Multifunctional Materials Institute (EMMI). Dr S. Pechev is also acknowledged for his priceless help in interpreting the XRD patterns.

Financial support by the Spanish Government-MINECO through “Severo Ochoa” (SEV 2012-0267), Consolider Ingenio 2010-Multicat, CTQ2015-70126-R, and by the European Union through ERC-AdG-2014-671093 – SynCatMatch is acknowledged.

## Notes and references

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Electronic Supplementary Information (ESI) available: See DOI: 10.1039/b000000x/

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# Continuous supercritical synthesis of unsupported and high specific surface area catalyst precursors for deep-hydrodesulfurization

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Benzene	80	3 wt%
Toluene	110	2 wt%
Thiophene	84	100 wppm (S)
Methylthiophene	113	100 wppm (S)
Tetrahydrothiophene	119	50 wppm (S)
Benzothiophene	222	50 wppm (S)
Dibenzothiophene	333	100 wppm (S)
4,6-Dimethyldibenzothiophene	340	100 wppm (S)

## Supporting information:

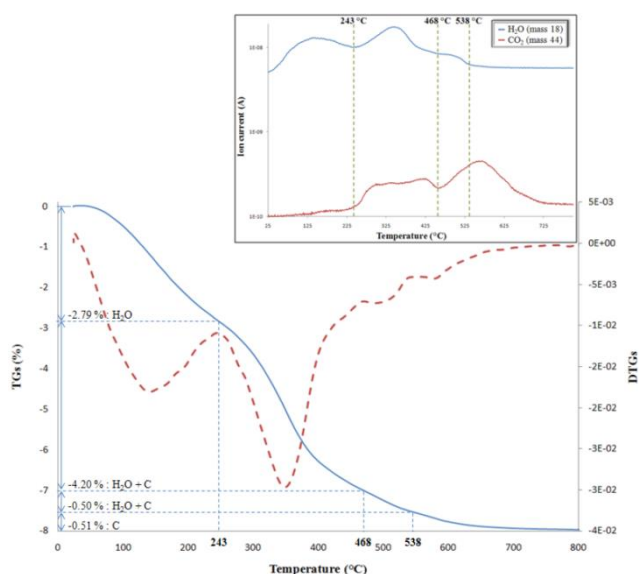


Figure S1: TGA-MS of the stoichiometric Ni-Mo based powder synthesized in supercritical H<sub>2</sub>O/EtOH mixture, from room temperature to 800°C under Ar atmosphere, ramp rate 1°C.min<sup>-1</sup>.

Table S1: Cell parameters obtained for the stoichiometric NiMo based powder synthesized in supercritical H<sub>2</sub>O/EtOH mixture annealed at 400°C.

Space group	a (Å)	b (Å)	c (Å)	β (Å)
C 2/m	10.187(5)	9.246(5)	7.020(2)	107.09(3)
JCPDS 45-0142	10,184	9,241	7,0189	107,09

Table S2: Cell parameters obtained at 200°C for the stoichiometric NiMo based powder synthesized in supercritical H<sub>2</sub>O/EtOH, when cooling down after investigation in temperature.

Space group	a (Å)	b (Å)	c (Å)	β (Å)
C 2/m	9.589(6)	8.760(6)	7.654(5)	114.16(4)
JCPDS 86-0361	9,566	8,734	7,649	114,22

Table S3: Detailed composition of the model feedstock.

Compound	Boiling point (°C)	Concentration
Heptane	99	30 wt%
Dodecane	216	30 wt%
Hexene	63	15 wt%
Octene	123	15 wt%
Naphthalene	218	5 wt%

Table S4: D86 correlation corresponding to the industrial LCO

% Off	Temperature (°C)
IBP	187
10	239
20	252
30	263
50	286
70	318
80	336
90	359
FBP	390