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Measurements and modeling of high-pressure O₂ and CO₂ solubility in brine (H₂O+NaCl) between 303 and 373 K and pressures up to 36 MPa

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Abstract

Knowledge of the solubility of oxygen in natural water, which is generally saline, is important for several scientific and engineering fields. Applications such as geological storage of gas (containing O₂, e.g. flue gas) or energy (Compressed Air Energy Storage) operate at high pressure. However, to date, there is no high-pressure O₂ solubility data in brine, which has led researchers to develop models to predict this important property. To overcome the lack of data, solubility of O₂ in brine has been measured using two different techniques, at molalities between 0.5 and 4 mol/kg_w (NaCl), temperatures between 303 and 373 K and pressures up to 36 MPa. In order to validate the experimental methods, measurements of the solubility of CO₂ in a highly concentrated brine (6 mol/kg_w of NaCl) at temperatures between 303 and 373 K and pressures up to 39.5 MPa, were performed also in this work. These measurements allowed the evaluation of existing models such as the well-known Geng and Duan model, and the model recently developed by Zheng and Mao (ZM). The e-PR-CPA, Soreide-Whitson, and geochemical models used in our previous work were also used to process the new data. These last three models have been parameterized on measured and reported literature O₂ solubility data, and new optimized parameters of the ZM model have been proposed. These models reproduce the effect of temperature, pressure and NaCl concentration on solubility with an average absolute deviation less than 5% from the measured data.

1. Introduction

Knowledge of the solubility of oxygen in natural water, which is generally saline, is important for several scientific and engineering fields such as hydrometallurgy¹, bioprocess engineering², oceanography and geochemistry³, etc. Underground gas and energy storage is one of the geochemical applications that require the knowledge of the phase equilibrium of the O₂ + water + salt mixture, since oxygen is generally always present in gas streams, whether as impurity as in the case of flue gases storage in the context of Carbon Capture and Storage (CCS), or in large quantities as in the case of Compressed Air Energy Storage (CAES). Due to its very high reactivity in the aqueous phase, oxygen can participate in geochemical reactions such as the oxidation of pyrite possibly present in the geological formation or can be used by micro-organisms leading to the contamination of the stored products⁴.

The oxycombustion process uses oxygen as an oxidant instead of air for energy production while avoiding NO_x emissions and facilitating the recovery of CO₂ from the flue gases since they are mostly enriched by the latter. This technology needs large quantities of oxygen and requires the centralization of oxygen production and storage. In the framework of the ANR FLUIDSTORY project, an innovative concept (Electrolysis-Methanation-Oxycombustion (EMO) unit)⁵ for energy storage concerns the supply of oxycombustion with oxygen from water electrolysis using renewable electricity, and with methane produced by methanation using hydrogen from electrolysis as well and CO₂ recovered from oxycombustion flue gases. To manage the time laps between the production and use of these energy carriers (H₂, O₂, CH₄, and CO₂), the underground storage in salt caverns is suggested since it is considered to be the most suitable technique for large gas storage. The risks related to the reactivity of oxygen, which are discussed earlier, must be considered in the case of storage of oxygen (pure or mixed) in salt caverns. Accurate determination of oxygen solubility in the aqueous phase (residual brine in the caverns) under the thermodynamic conditions of storage (temperature, pressure, and salinity) is therefore necessary.

Several experimental studies exist for the solubility of O₂ in pure and saline water. Existing data for these systems have been well reviewed by Battino⁶, and recently by Geng and Duan⁷ and Zheng and Mao⁸. These reviews have shown that there is a lack of high pressure solubility data especially for O₂ solubility in saline water which has only been studied at atmospheric pressure and low temperature (≤ 318 K). This lack of data has prompted researchers to develop models (Geng and Duan⁷, Li et al.⁹, Valderrama et al.¹⁰, Zheng and

Mao ⁸⁾ to estimate solubilities outside the range of available experimental data. Due to their unavailability to date, no data of O₂ solubility in salt water at high pressure were included in the adjustment of these models, hence the need for high pressure solubility measurements of O₂ in brine, and more specifically in NaCl brine since sodium and chloride are the main species present in natural saline water.

In this work, the solubility of O₂ in H₂O+NaCl with two different techniques was measured under geological storage conditions (temperature $303 \leq T \text{ (K)} \leq 373$, pressure up to 36 MPa and NaCl molality $0.5 \leq m_{\text{NaCl}} \text{ (mol/kg}_w) \leq 4$). CO₂ solubility measurements at very high molality (6 mol/kg_w of NaCl) were also performed to complete our previous work ¹¹ and also to validate the measurement technique. The modeling of literature data and the measured solubilities of this study, was performed using several models (e-PR-CPA, Soreide and Whitson, and geochemical models) developed and presented in our recent work ¹¹. In order to improve the accuracy of the model proposed by Zheng and Mao, the model parameters were readjusted on experimental data including the new measured data.

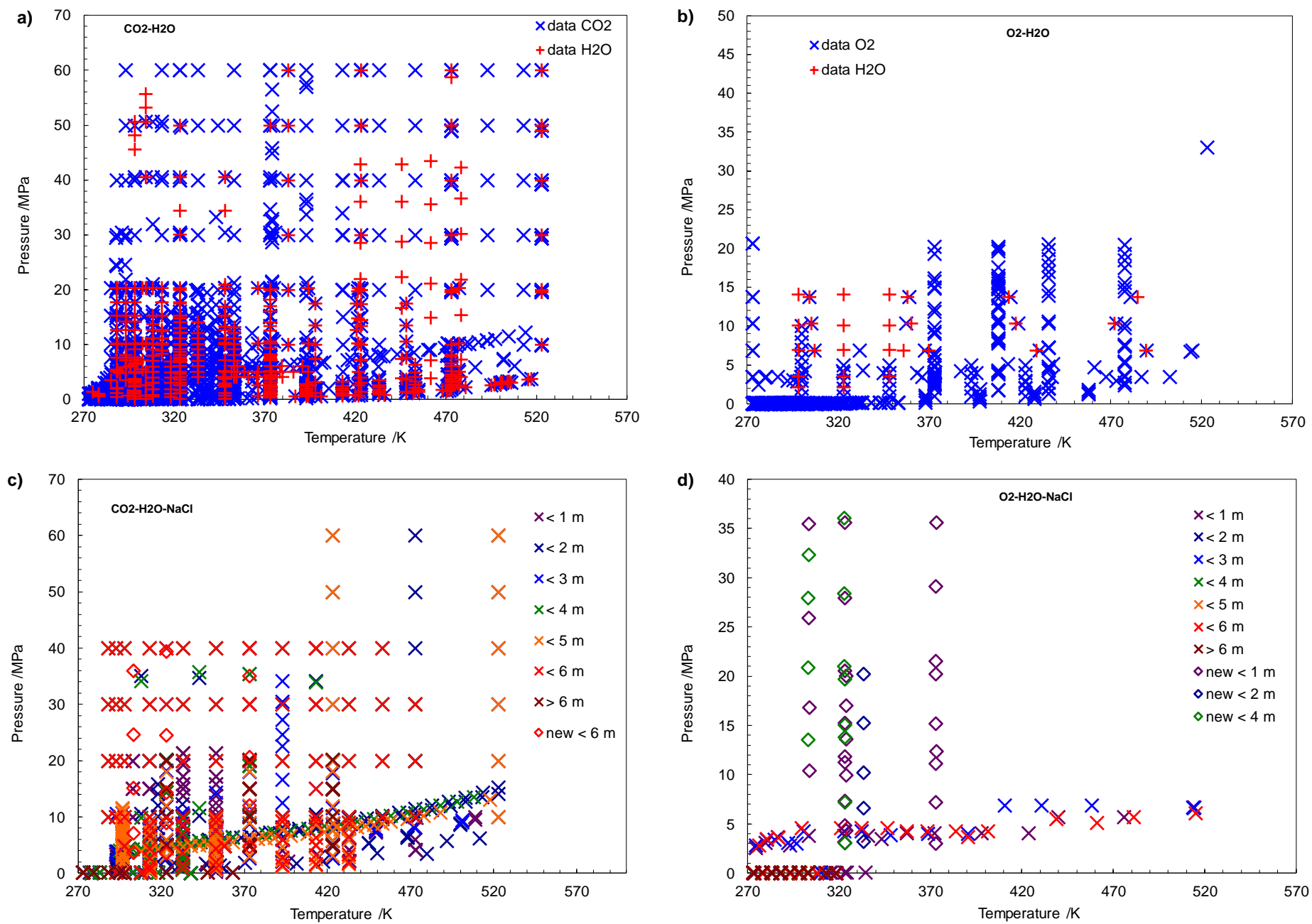


Figure 1 : Distribution of literature (x) and new measured (◊) solubility data. (a): CO₂+H₂O system (solubility and water content); (b): O₂+H₂O system (solubility and water content); (c): CO₂ solubility in NaCl brine; (d): O₂ solubility in NaCl brine (m=mol/kg_w).

2. Experimental

2.1. Literature and measured solubility data of CO₂ and O₂ in water and brine

In the literature, several reviews of CO₂¹²⁻¹⁴ and O₂⁶⁻⁸ solubility data in water and brine are available. To list the literature data and those measured in this work, the distribution of these data sets are presented in Figure 1 as a function of temperature, pressure and NaCl molality. As shown in this figure, data on the solubility of CO₂ in H₂O+NaCl (Figure 1.a and 1.c) and the solubility of O₂ in H₂O (Figure 1.b) are widely available. However, the measurements made in this work fill the lack of solubility data in brine at high pressure especially for O₂ (Figure 1.d).

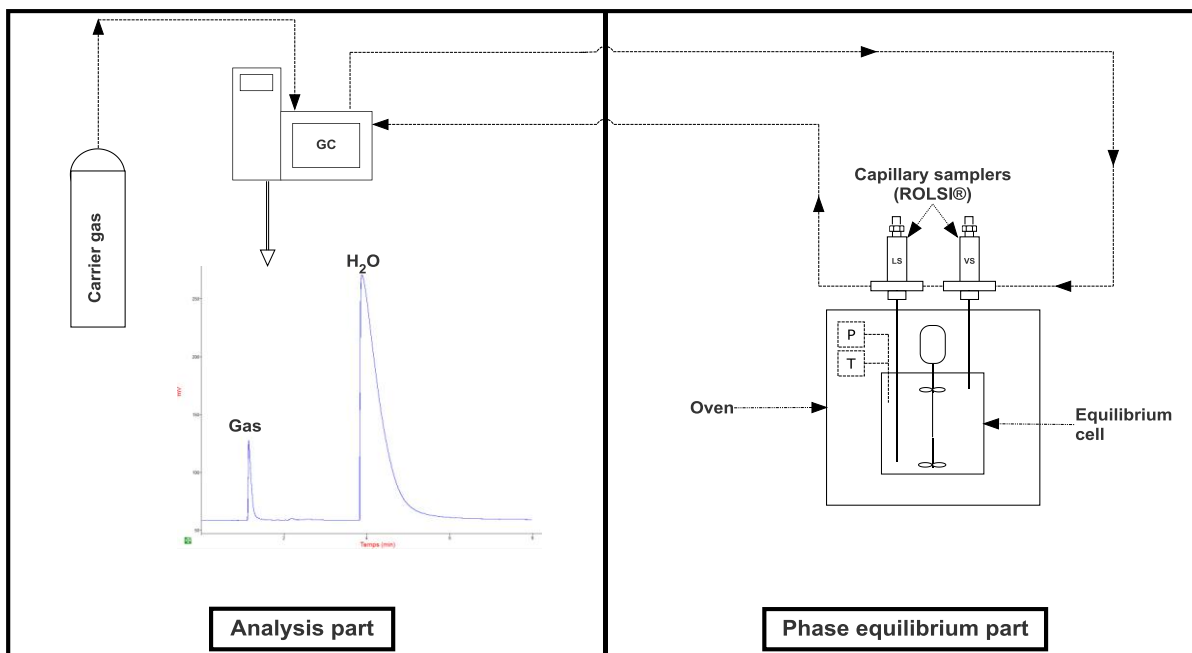


Figure 2 : Simplified schematic representation of the "static-analytic" apparatus for phase equilibria measurement.

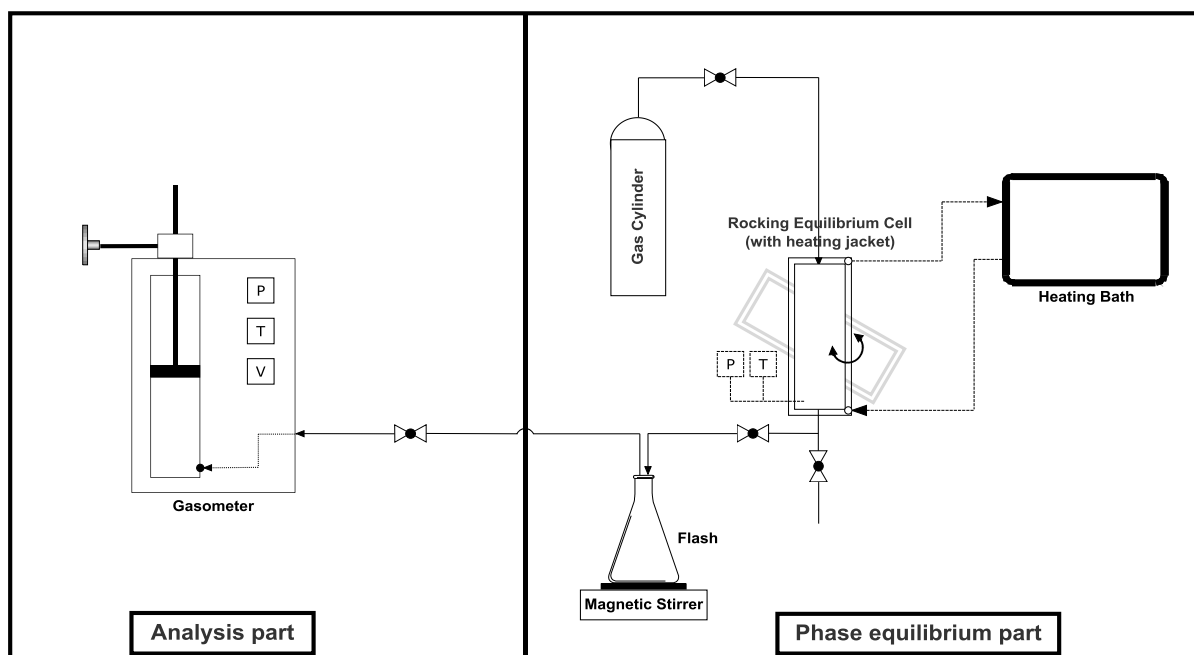


Figure 3 : Simplified schematic representation of the "Rocking cell" apparatus for solubility measurement.

2.2. Materials

In Table 1, the suppliers of the chemicals (CO_2 , O_2 and NaCl) and the given purities are listed. Carbon dioxide (CO_2 , CAS Number: 124-38-9) and oxygen (O_2 , CAS Number: 7782-44-7) were purchased from BOC with a certified volume purity greater than 99.995%. Sodium Chloride (NaCl , CAS Number: 7647-14-5) was purchased from Fisher Chemical with a

certified purity of 99.6%. Water (H₂O, CAS Number: 7732-18-5) was deionized and degassed before the preparation of the brine (H₂O + NaCl).

Table 1 : Chemical samples used for experimental work (CAS Registry Number, mole fraction purity and suppliers of chemicals).

Chemicals	CAS Reg. No.	Purity	Analysis method	Supplier
CO ₂	124-38-9	99.995 mol%	GC ^a	BOC
O ₂	7782-44-7	99.995 mol%	GC ^a	BOC / Air Liquide
NaCl	7647-14-5	99.6%	None	Fisher Chemical
H ₂ O (ultrapure)	7732-18-5	18.2 MΩ·cm		Millipore™ (direct-Q5)

a: Gas Chromatography

2.3. Apparatus and method

2.3.1. Static-analytic setup

The first setup used in this work is based on the static-analytic method and is described in detail in our recent work ¹¹. However, in Figure 2, a simplified description of this technique is illustrated. It consists of an equilibrium cell positioned in an oven for temperature control, and equipped with pressure transducers, temperature probes and two ROLSI[®] (Rapid On-Line Sampler-Injector, French patent number 0304073) capillary samplers for each phase (liquid and vapor). After setting the temperature and charging the cell with the salt solution and the gas up to the desired pressure, the thermodynamic equilibrium is reached in some dozens of minutes after continuous agitation, assuming that the equilibrium is verified by the stabilization of the temperature and pressure in the cell. Several samples are then taken by the liquid ROLSI[®] and sent through a transfer line to GC (Gas Chromatography) to determine the mole fraction of gas and water.

2.3.2. Rocking cell setup (volumetric technique)

The rocking cell setup illustrated in Figure 3 is based on a volumetric technique. It is the same as that presented by Chapoy et al. ¹⁵ and recently used by Ahmadi and Chapoy ¹⁴. It consists of a rocking equilibrium cell with a volume of 350 cm³ mounted on an adjustable rotary axis of the pneumatic rocking system and surrounded by a heating jacket connected to a thermostat bath to maintain a constant temperature. The cell is equipped with a Quartzdyne pressure

transducer and a platinum resistance thermometer placed in the heating jacket of the cell. Since the temperature probe is not placed inside the cell, the real temperature in the cell is determined by calibration with respect to the jacket temperature.

For each measured point, the following procedure was followed: setting the target temperature, introducing 300 cm³ of the saline solution and evacuating the equilibrium cell to remove the air. Then, the gas is introduced until the desired pressure is reached. The gas injection line is disconnected to allow the shaking of the system by the rocking system. Once the pressure and temperature are stabilized, the rocking is stopped and the cell is locked in a vertical position to take a sample of the aqueous phase. The gas injection line is reconnected to the cell, the flash tank is connected to the bottom of the cell to collect the sample, and the gasometer (VINCI TECHNOLOGIES) is connected to the flash tank. During sampling, the gas is injected continuously to maintain a constant pressure. The gas is separated from the liquid at the flash tank and transferred to the gasometer. The volume difference at constant pressure and temperature is then determined using the gasometer and knowing the density of the pure gas, the mass of the gas is deduced. The mass of the brine is determined gravimetrically using a balance. Finally, by knowing the quantities of gas and brine in the sample, the solubility of the gas is obtained. The calculation procedure is described in detail by Ahmadi and Chapoy¹⁴. More gas is added to increase the pressure, and the procedure is repeated to measure another equilibrium point.

3. Thermodynamic modeling

The models used in this work are fully programmed and parameterized, and are described in detail in our recent work¹¹. Their main equations are presented in Appendix A. These models are based on two thermodynamic approaches:

- Asymmetric (gamma-phi) approach:

Being simple and fast, the gamma-phi approach is the most used approach by geochemists for correlating gas solubility data in water and brine. This approach consists of using an equation of state for the gas phase and an activity coefficient model for the liquid phase. Among the best known works are those of Duan et al.^{16, 17} and Spycher et al.^{18, 19} on the solubility of CO₂ in water/brine, and those of Geng and Duan⁷ and Valderrama et al.¹⁰ on the solubility of O₂ in water/brine.

The geochemical model implemented in CHESS/HYTEC software (Corvisier, 2013 ²⁰; Corvisier et al., 2013 ²¹) was used, as well as the model proposed by Zheng and Mao ⁸ reparameterized by including the new measured data from this work.

- Symmetric (phi-phi) approach:

Unlike the asymmetric approach, the symmetric approach consists in representing all the fluid phases (liquid and vapor) of the system with a single equation of state. Using this approach, two types of equations of state (cubic and non-cubic) were used.

The first EoS is the Soreide-Whitson model ²² (revision of the PR model) which is widely used in reservoir engineering (mixture of gas, oil, water, salts, etc.), and is implemented in several modeling and simulation software (Eclipse 300 - Schlumberger, IPM - Petex, Simulis Thermodynamics – Prosim France, etc.).

The second EoS used is the e-PR-CPA (electrolyte Peng-Robinson Cubic Plus Association) model that was presented in our previous work ¹¹. With this model, all molecular and electrolyte interactions are taken into account. In the e-PR-CPA model, the PR cubic EoS has been selected to represent attractive and dispersive interactions, and the Wertheim's theory (used in SAFT and CPA type EoS) has been considered to account for the association phenomenon. Concerning electrolyte interactions, the long-range interactions (between ions) are taken into account by the MSA (Mean Spherical Approximation) theory, and the phenomenon of solvation of the ions by the solvent (water) is considered by the Born term.

4. Results and discussions

4.1. Experimental results

In this section, measurements concerning the high-pressure solubility of CO₂ and O₂ in H₂O + NaCl are presented. The standard uncertainties $u(T)$, $u(P)$ and $u(x)$ of the measurements performed by the static-analytic setup were calculated by the NIST method ²³. The calibration (the polynomial correlation) uncertainty and repeatability uncertainty are the two sources of uncertainties involved in the calculation of $u(T)$ and $u(P)$. The third source of uncertainty was associated with the injection of the pure compound by the syringe during GC calibration, $u(x)$. For the measurements carried out with the Rocking Cell apparatus, the uncertainties for temperature, pressure and composition were calculated in the same way as that of Ahmadi and Chapoy ¹⁴, since the same installation and the same calibrations were used. The standard

uncertainties for temperature $u(T)$ and pressure $u(P)$ are 0.02 K and 0.005 MPa respectively for the static-analytic setup and 0.17 K and 0.068 MPa respectively for the rocking cell setup. The standard uncertainties related to the measurement of the composition $u(x_{CO_2})$ and $u(x_{O_2})$ are listed with the results in Tables 2 and 3. The gas solubility is expressed as "salt-free" mole fractions: $x_{gas} = m_{gas}/(m_{gas} + 1000/M_{H_2O})$, m_{gas} is the gas molality (in mol/kg_w), and M_{H_2O} is the molecular weight of water (in g/mol).

4.1.1. CO₂ solubility in H₂O + NaCl

The experimental measurements of the CO₂+H₂O+NaCl system were performed by the rocking cell setup at molality of 6 mol NaCl/kg_w, temperatures between 303 and 373 K and pressures up to 39.5 MPa and are listed in Table 2. These measurements were used to validate the experimental setup by comparing some obtained results with literature data from Messabeb et al.¹³ and Zhao et al.²⁴ (Figure 4), and also to complement the existing data for this system, especially at high pressure.

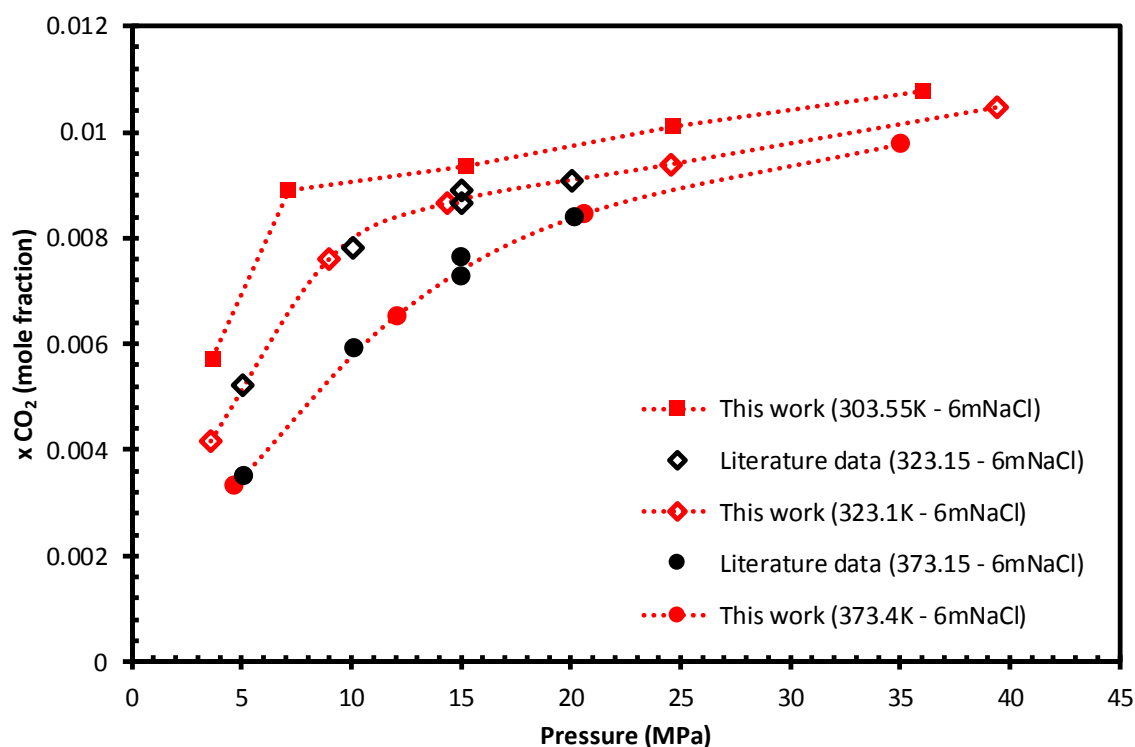


Figure 4 : CO₂+H₂O+NaCl system : Experimental CO₂ solubility in 6 mNaCl (mol/kg_w) NaCl-brine at 323 K and 373 K. The black symbols are the literature data^{13, 24}, and the red symbols with dotted lines (to guide the eye) are the measured data.

Table 2 : Measured solubility of CO₂ in the H₂O + NaCl at 6 mol/kg_w NaCl by the rocking cell setup, expressed as "salt-free" mole fractions x_{CO_2} and their standard uncertainties $u(x_{CO_2})$. $u(m_{NaCl}) = 0.002$ mol/kg_w, $u(T) = 0.17$ K and $u(P) = 0.068$ MPa.

Equilibrium	T (K)	P (MPa)	x_{CO_2}	$u(x_{CO_2})$
Vapor-Liquid (VLE)	303.55	3.6721	0.00572	0.00010
VLE	303.55	7.1333	0.00890	0.00008
Liquid-Liquid (LLE)	303.55	15.1857	0.00936	0.00010
LLE	303.55	24.6777	0.01012	0.00010
LLE	303.55	36.0196	0.01077	0.00010
VLE	323.10	3.5818	0.00418	0.00010
VLE	323.10	8.9744	0.00760	0.00007
VLE	323.10	14.3618	0.00866	0.00009
VLE	323.10	24.5798	0.00939	0.00010
VLE	323.10	39.4477	0.01046	0.00010
VLE	373.29	4.676	0.00333	0.00010
VLE	373.39	12.0603	0.00654	0.00006
VLE	373.39	20.5905	0.00846	0.00008
VLE	373.39	35.0185	0.00978	0.00010

4.1.2. O₂ solubility in H₂O + NaCl

The solubility of O₂ in H₂O+NaCl was measured with both apparatus (technique 1: static-analytic, technique 2: rocking cell (volumetric)). The experimental results obtained at molalities between 0.5 and 4 mol/kg_w, temperatures between 303 and 373 K and pressures up to 36 MPa, are listed in Table 3. For validation purpose, some measurements were made with both techniques under the same experimental conditions (T, P, mNaCl). As shown in Figure 5, the two datasets are consistent and follow similar trends, which validates both measurement techniques (including equipment and calibration).

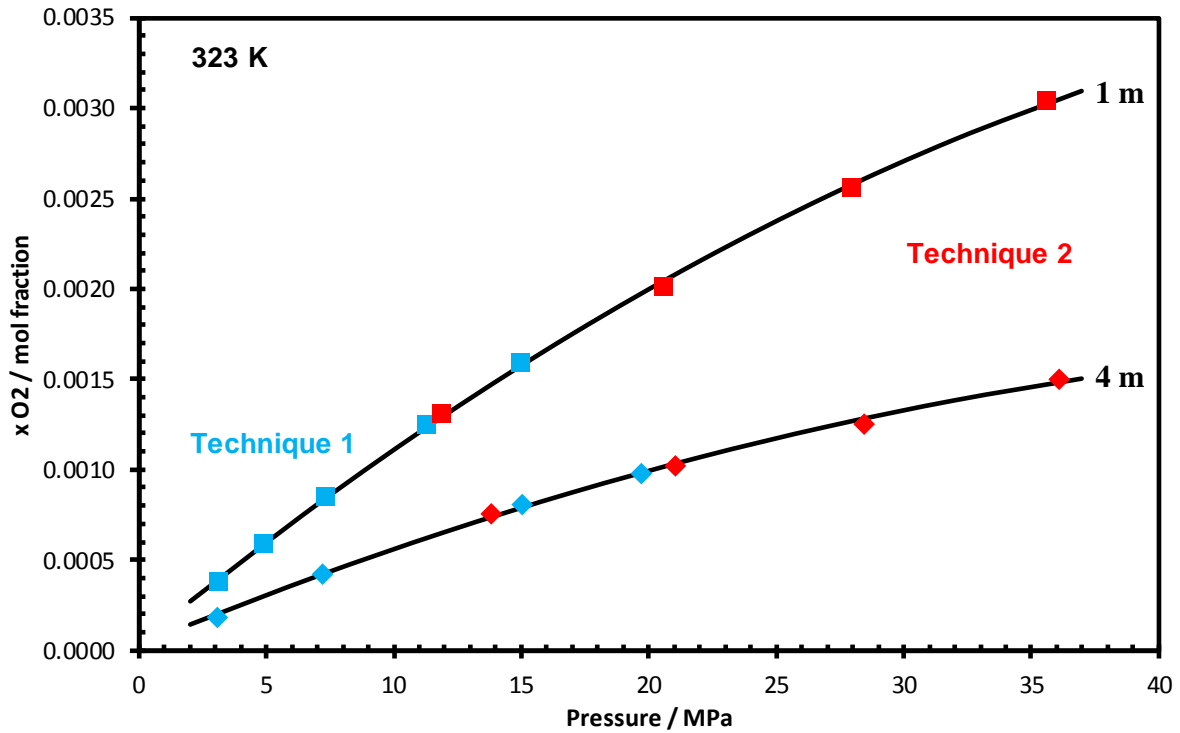


Figure 5 : O₂+H₂O+NaCl system : Validation of measured O₂ solubility data in 1m and 4m (m=mol/kg_w) NaCl-brine at 323 K. The blue and red symbols represent data measured by the Technique 1 and 2 respectively. The solid lines represent a trend line to guide the eye.

Table 3 : Measured solubility of O₂ in the H₂O + NaCl, expressed as "salt-free" mole fractions x_{O_2} and their standard uncertainties $u(x_{O_2})$. $u(m_{NaCl}) = 0.002 \text{ mol/kg}_w$, for Technique 1: $u(T) = 0.02 \text{ K}$ and $u(P) = 0.005 \text{ MPa}$; For Technique 2: $u(T) = 0.17 \text{ K}$ and $u(P) = 0.068 \text{ MPa}$.

Technique	m_{NaCl} (mol/kg _w)	T (K)	P (MPa)	x_{O_2}	$u(x_{O_2})$
Technique 1: static-analytic	0.5	324.00	4.3540	0.00064	0.000020
		323.95	9.9310	0.00140	0.000100
		323.94	13.6330	0.00180	0.000100
		323.93	17.0180	0.00210	0.000100
		323.93	20.0710	0.00240	0.000100
	1	323.16	3.1210	0.00038	0.000010
		323.17	7.3479	0.00085	0.000020
		323.14	4.8790	0.00059	0.000010
		323.14	11.2857	0.00125	0.000040
		323.17	15.2399	0.00160	0.000050
	4	323.18	3.0720	0.00018	0.000010
		323.16	7.2104	0.00042	0.000010
		323.13	15.0404	0.00080	0.000030
		323.16	19.6893	0.00098	0.000030
1*		372.92	3.0516	0.00029	0.000010

Technique 2: rocking cell (volumetric)		373.11	7.2294	0.00070	0.000010
		373.07	11.1250	0.00106	0.000020
		373.10	15.1719	0.00139	0.000020
		373.09	20.2617	0.00175	0.000040
		333.30	3.1964	0.00029	0.000010
		333.53	6.6156	0.00057	0.000010
	2	333.53	10.2178	0.00083	0.000060
		333.52	15.2950	0.00118	0.000040
		333.53	20.2640	0.00146	0.000080
		303.74	10.4249	0.00141	0.000050
	1	303.74	16.8653	0.00206	0.000053
		303.55	25.9464	0.00290	0.000055
		303.55	35.4577	0.00350	0.000058
		323.20	11.8555	0.00131	0.000050
	1	323.20	20.5567	0.00201	0.000054
		323.20	27.9341	0.00256	0.000055
		323.20	35.6287	0.00304	0.000056
		373.10	29.1304	0.00245	0.000054
	1	373.10	21.5461	0.00197	0.000054
		373.19	12.3554	0.00129	0.000053
	373.19	35.5839	0.00286	0.000055	
	303.26	13.5379	0.00078	0.000050	
4	303.26	20.8808	0.00112	0.000053	
	303.26	27.9272	0.00134	0.000053	
	303.64	32.3123	0.00153	0.000054	
	323.10	13.8274	0.00075	0.000050	
4	323.01	21.0325	0.00102	0.000053	
	323.01	28.4305	0.00125	0.000054	
	323.01	36.0630	0.00150	0.000054	

* Initial NaCl molality must have increased due to experimental error (see explanation in Section 4.2.).

4.2. Modeling results

4.2.1. CO₂ + H₂O + NaCl system

The solubility of CO₂ in the CO₂ + H₂O + NaCl system was modeled by the Soreide and Whitson models (SW, with improved binary interaction parameters, see Chabab et al. ¹¹) and the e-PR-CPA model using the phi-phi approach, as well as the geochemical model using the gamma-phi approach. For the e-PR-CPA model the solvation of CO₂ by water molecules was

considered by attributing to CO₂ a single electron acceptor association site and to H₂O four association sites (2 electron donor sites and 2 electron acceptor sites). The predictions were compared with data from the literature and those measured in this work. This was done under geological storage conditions, either in saline aquifers (low or medium salinity) or in salt caverns (saturated brine). An example of modeling results at different salinities (in terms of molality), ranging from pure water to saline water with very high salt concentration (close to saturation ~ 6 mol/kg_w NaCl), is shown in figure 6. The model predictions are in good agreement with the literature and measured solubility data. Calculations of CO₂ solubility in water and NaCl brine generated by the e-PR-CPA model over a wide range of temperature, pressure and molality are listed in Table S1 in Supporting Information.

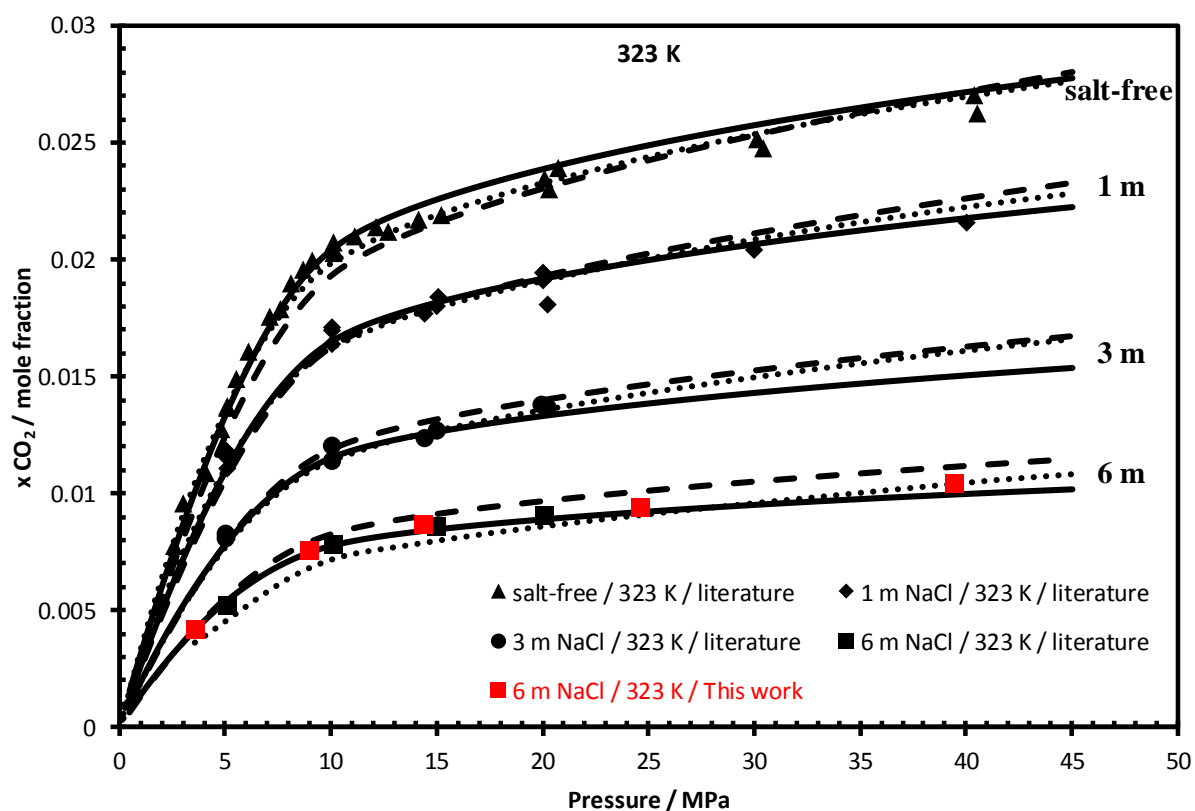


Figure 6 : CO₂+H₂O+NaCl system : Prediction of CO₂ solubility at different NaCl molality *m* (mol/kg_w) by e-PR-CPA (solid line), SW (dashed line) and geochemical (dotted line) models. The black symbols are the literature data ^{13, 14, 25-31}, and the red symbols are the measured data (Table 2).

4.2.2. O₂ + H₂O + NaCl system

In order to check more or less the consistency of the measured solubilities of O₂ in water + NaCl, we verified the linearity of the experimental data in terms of Ln(P/xO₂) as a function of P, following the Krichevsky-Kasarnovsky ³² approach. This linearity condition can be easily demonstrated from the gamma-phi approach, by considering the fugacity coefficient of the

gas (Li et al. ⁹) or by neglecting it (assuming that the vapor phase is ideal, see Descamps et al. ³³).

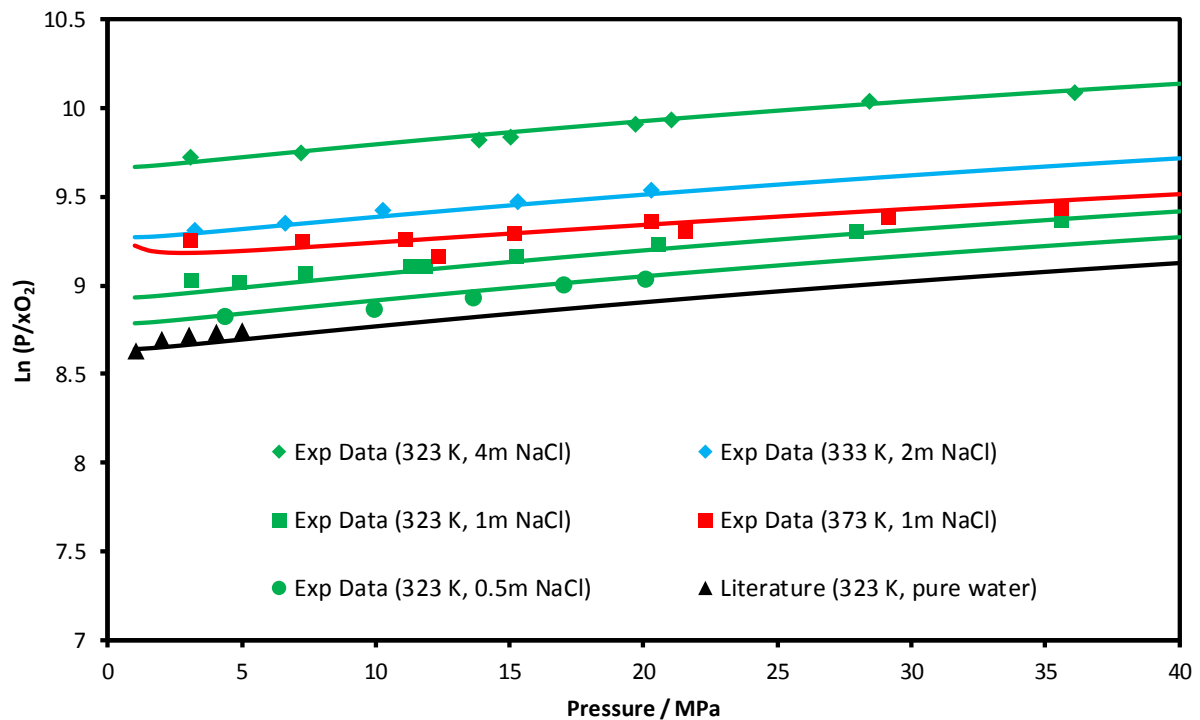


Figure 7 : Solubility of O₂ in H₂O + NaCl at different NaCl molality m (mol/kg_w). The black symbols are the literature data ³⁴, the red symbols are the measured data (Table 3), and the solid lines are the prediction by e-PR-CPA model.

In Figure 7, the linearity of the experimental data was checked and compared with the predictions of the e-PR-CPA model. All measurements appear to be consistent and linear except for the isotherm at 373 K (1 mol/kg_w NaCl). This inconsistency with respect to this isotherm can be explained by the fact that the points were not measured at the same molality, since we used two different techniques. The deviations concern only the measurements made with the technique 1 at 373 K (1 mol/kg_w), assuming that the initial molality has increased, since by mistake, after filling the cell with the prepared brine solution (at 1 mol/kg_w), we evacuated it at high temperature (373 K). This allowed the water to evaporate more and increase the molality.

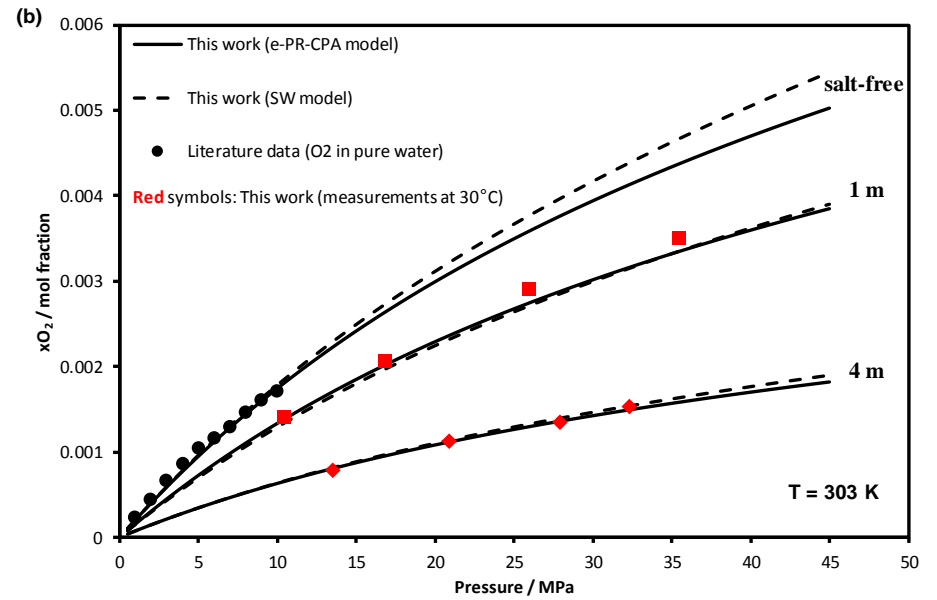
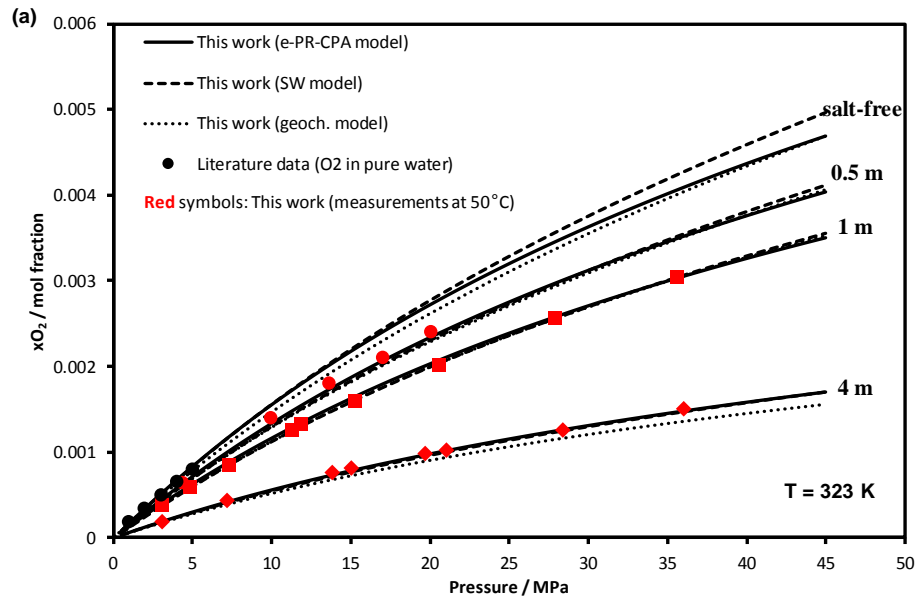


Figure 8 : $O_2+H_2O+NaCl$ system : Prediction of O_2 solubility at different NaCl molality m (mol/kg_w) by e-PR-CPA (solid line), SW (dashed line) and geochemical (dotted line) models. The black symbols are the literature data ((a) : ³⁴, (b) : ³⁵), and the red symbols are the measured data (Table 3).

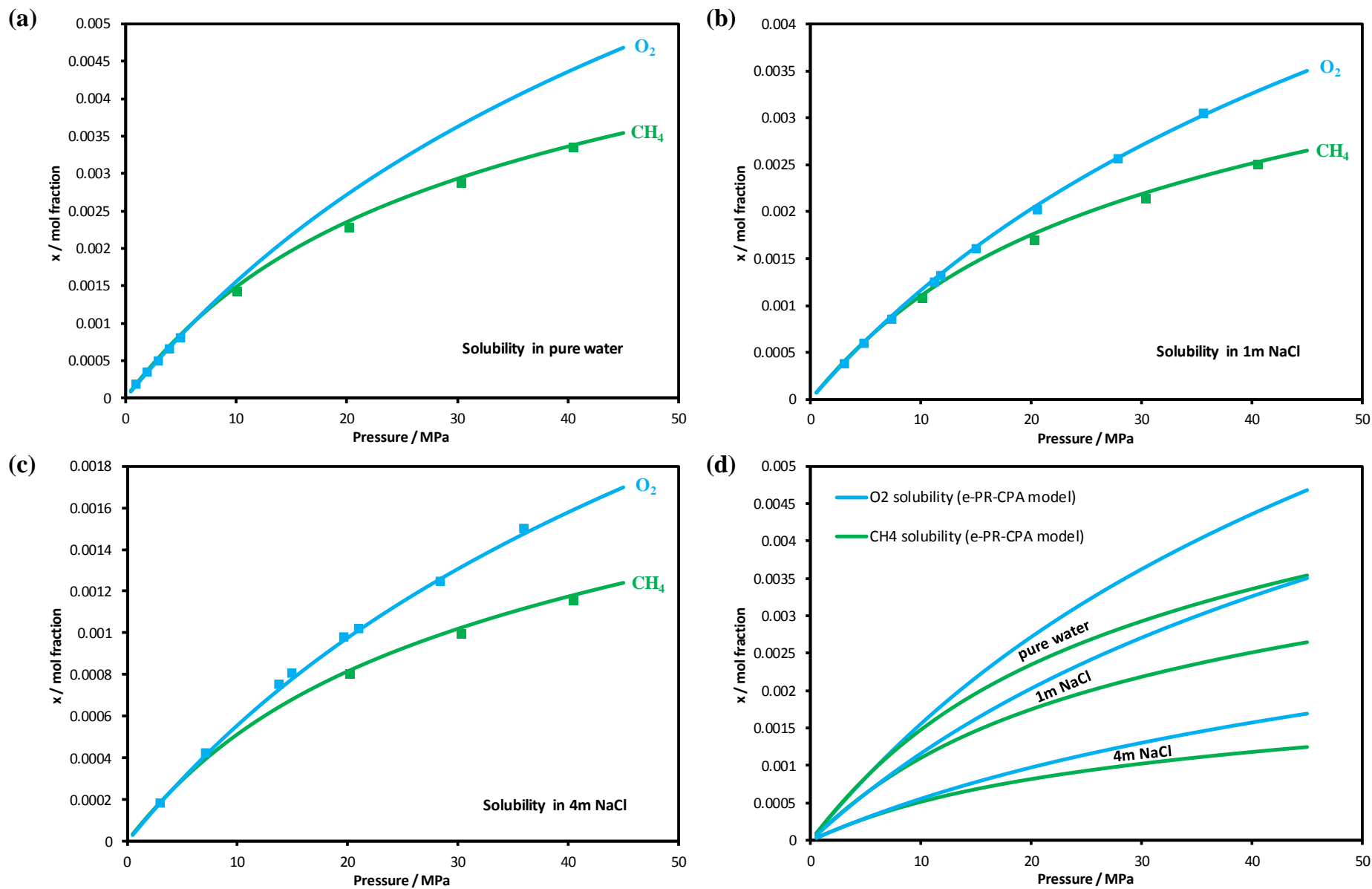


Figure 9 : Comparison of O_2 and CH_4 solubilities in pure water (a) and NaCl brine (water+NaCl; b: 1m; c: 4m; d: 0-4m; m=mol/kg_w) at 323 K. The symbols represent the experimental data (O_2 in water: ³⁴; O_2 in brine: from this work (Table 3); CH_4 in water and brine: ³⁶) and the solid lines represent the predictions by the e-PR-CPA model.

The solubility of O₂ in H₂O + NaCl was also modeled by the three models. The binary interaction parameters of the different models were fitted to the literature and measured data. For the e-PR-CPA model (See Appendix A2), the cross-association (solvation) between O₂ molecules and H₂O molecules was not considered (no Lewis Acid-Lewis Base interaction), since O₂ is not considered as an associative species. Therefore, only the binary interaction parameters $k_{O_2-H_2O}$ and k_{O_2-ion} were adjusted. As in our previous work ¹¹, we considered temperature dependence in k_{gas-H_2O} and salt molality dependence in $k_{gas-ion}$.

$$k_{O_2-H_2O} = 9.51493975 \times 10^{-11}T^2 + 3.22791135 \times 10^{-3}T - 0.726309790 \quad (1)$$

$$k_{O_2-Na^+} = -1.49034322 \times m_{NaCl} + 0.10603754 \quad (2)$$

$$k_{O_2-Cl^-} = 1.286649425 \times m_{NaCl} - 0.62173576 \quad (3)$$

The “asymmetric” binary interaction parameters (one for each phase) of the Soreide and Whitson (SW) model (See Appendix A1) depend on temperature (in K) and salt molality. In the original paper of the SW model ²², there is no expression of these parameters for O₂. We propose the following expression (the same is used for N₂ in the original paper) whose coefficients (Table 4) have been fitted to solubility and water content data:

$$(k_{O_2,H_2O}^{AQ})_{SW} = A_0(1 + \alpha_0 m_{NaCl}^{0.8}) + A_1 \frac{T}{T_{c,O_2}} (1 + \alpha_1 m_{NaCl}^{0.8}) \quad (4)$$

$$(k_{O_2,H_2O}^{NA})_{SW} = 0.58165 \quad (5)$$

Table 4 : Coefficients of the binary interaction parameter $(k_{O_2,H_2O}^{AQ})_{SW}$ of the SW model (Equation 4)

A_0	α_0	A_1	α_1	T_{c,O_2} (K)
-1.1677444	3.361921×10^{-2}	0.4666067	8.4573057×10^{-2}	154.581

The geochemical model (See Appendix A3), based on a dissymmetrical approach, solves a large set of mass balances and mass action laws to calculate the whole system speciation (i.e. aqueous, gaseous and solid quantities and activities/fugacities). Equations shall remain generic, in order that the model handles multi-components either for the gas phase and the electrolyte. For the gas phase, the PR-SW EoS is used with the classical mixing rule. For the aqueous solution and particularly for

saline solutions with high ionic strength, activity coefficients can be calculated using Specific Ion Theory (SIT) showing satisfactory results.

It requires a thermodynamic database and simulations presented here are run along with the Thermoddem database including Henry's constants and parameters for PR-SW EoS (Blanc et al. 2012³⁷), and parameters for molar volume of the dissolved gaseous component at infinite dilution (Shock et al. 1989³⁸; Schulte et al. 2001³⁹). Gas binary interaction parameters for PR-SW and aqueous binary interactions parameters for SIT have been fitted on experimental data.

- $k_{CO_2H_2O}$ and $k_{O_2H_2O}$ are equal to 0.193 and 0.591 respectively.
- $\varepsilon_{H^+Cl^-}$ and $\varepsilon_{Na^+Cl^-}$ are equal to -0.097 and -0.035 using HCl and NaCl solutions activity measurements (Schneider et al., 2004⁴⁰; Sakaida and Kakiuchi, 2011⁴¹; Khoshkbarchi and Vera, 1996⁴²).
- $\varepsilon_{CO_2Na^+}$ varies with temperature (from 0.085 at 298 K to 0.077 at 473 K) and $\varepsilon_{O_2Na^+}$ as well (from 0.124 at 298 K to 0.107 at 473 K) using numerous CO₂ and O₂ solubility measurements in NaCl solutions.

As shown in Figure 8, comparing with measured and literature^{34, 35} data, the models capture qualitatively (salting-out effect) and quantitatively very well the effect of NaCl on solubility over a wide range of pressure and molality. The e-PR-CPA, SW, and geochemical models respectively reproduce the O₂ solubility with an average absolute deviation of 2.8%, 2.9%, and 4.3% from the measured data. It should be noted that the geochemical model has been fitted to all literature and measured data, and most of these data are at low pressure and temperature, therefore it is more accurate at low pressure. The e-PR-CPA and SW models have been adjusted on high pressure data (≥ 1 MPa), hence they estimate the solubility at high pressure more precisely. The calculated values for solubility of O₂ in water and NaCl brine estimated using the e-PR-CPA model over a wide range of temperature, pressure and molality are listed in Table S2 (in Supporting Information). In Figure 9, the solubility of O₂ in pure water and NaCl brine was compared with that of CH₄ under the same conditions of temperature (323 K) and NaCl molality (0, 1 and 4 mol/kg of water). The e-PR-CPA model also predicts well the solubility of CH₄ in pure water and brine an average absolute deviation of 1.9% and BIAS of 0.8%. The binary interaction coefficients for CH₄-H₂O are provided in Equations 6-8. In Figure 9, it is observed that the solubility in pure water and brine of O₂ becomes more important than that of CH₄ at high pressure, which is not the case at lower pressures (<5 MPa). Moreover, the binary gas/water interaction parameters are more important for O₂ (between 0.24 and 0.48 for temperatures between 298 and 373 K) than CH₄ (between 0.11 and 0.29 for

temperatures between 298 and 373 K). This can perhaps be explained by the difference in polarizability between the molecules of O₂ (1.6 Å³) and CH₄ (2.6 Å³)⁴³: O₂ is less polarizable, so the attractive water-gas interactions are less strong for O₂ than for CH₄.

$$k_{CH_4-H_2O} = -8.270968 \times 10^{-6}T^2 + 8.012843 \times 10^{-3}T - 1.543212 \quad (6)$$

$$k_{CH_4-Na^+} = -0.93612817 \times m_{NaCl} - 2.78121097 \quad (7)$$

$$k_{CH_4-Cl^-} = 0.66659884 \times m_{NaCl} + 2.46759704 \quad (8)$$

The difference in solubility of CH₄ and O₂ can be explained by their size. The critical volume of methane (98.62 cm³/mol⁴⁴) is larger than that of oxygen (73.36 cm³/mol⁴⁴), which is related to the size of the molecule. Therefore, methane requires more energy than oxygen to form a cavity in the aqueous phase. The same remark was given by Battino and Seybold⁴⁵ to explain the mystery of the solubilities of O₂ and N₂ in water.

The interaction parameters $\lambda_{O_2-Na^+}$ and $\xi_{O_2-Na^+-Cl^-}$ of the Zheng and Mao (ZM)⁸ model have been readjusted by including the new measured data. In Table 5, the old and new parameters are listed, and the comparison of the O₂ solubility predictions using the two sets of parameters is shown in Figure 10. With the new parameters, the solubility calculation by the ZM model has been improved by reproducing the new measured data with an absolute average deviation of 4% instead of 11% (with the original parameters).

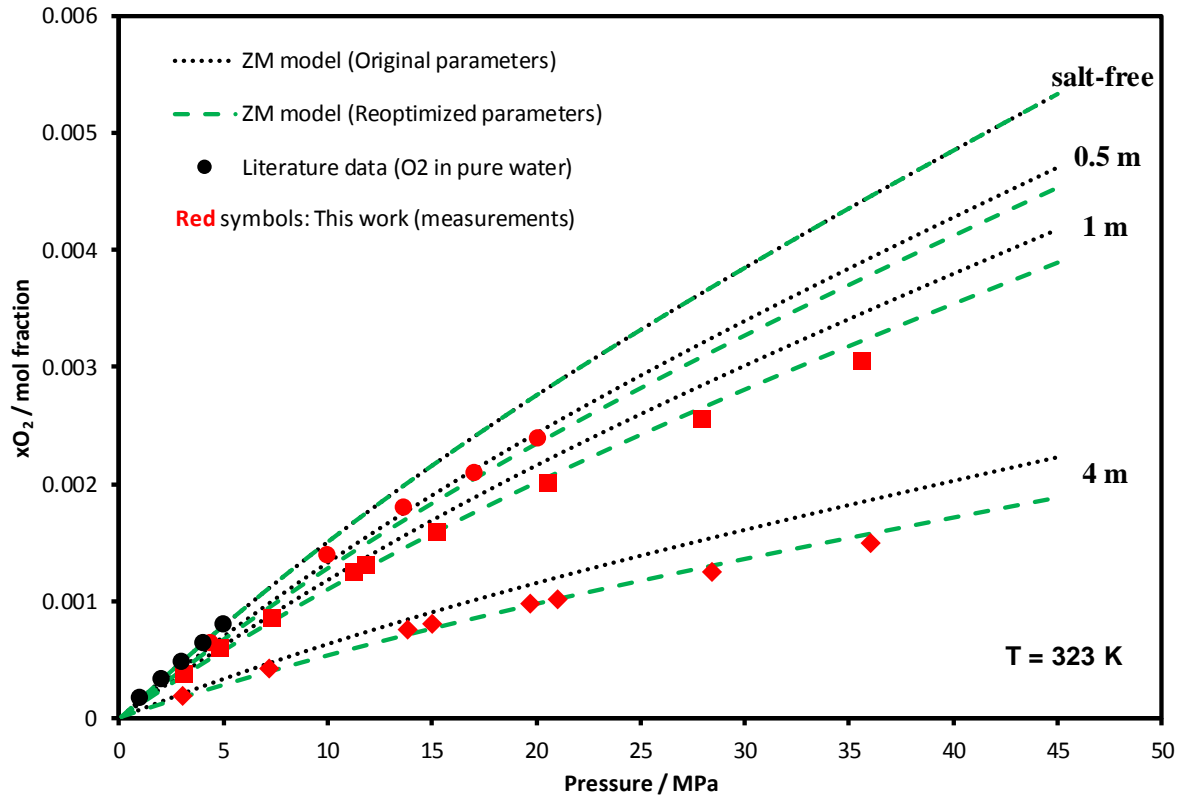


Figure 10 : O₂+H₂O+NaCl system : Calculation of O₂ solubility at different NaCl molality *m* (mol/kg_w) by the Zheng and Mao (ZM) model using original (dotted line) and reoptimized (dashed line) parameters (Table 5). The black symbols are the literature data³⁴, and the red symbols are the measured data (Table 3).

Table 5 : Zheng and Mao model interaction parameters for the O₂ solubility in NaCl brine

ZM model parameters	$\lambda_{O_2-Na^+}$	$\xi_{O_2-Na^+-Cl^-}$	AAD (%) ^a
Original ⁸	$0.4670997 - 0.10500795 \times 10^{-2}T$	$-0.90085535 \times 10^{-2}$	11.23
Reoptimized (this work)	$0.33428760 - 5.14803685 \times 10^{-4}T$	$-1.8659617215 \times 10^{-2}$	3.97

^a AAD %: average absolute deviation (from the data measured in this work), AAD % =

$$\frac{100}{N_{exp}} \sum_{i=1}^{N_{exp}} \left(\left| \frac{x_{O_2 i}^{cal} - x_{O_2 i}^{exp}}{x_{O_2 i}^{exp}} \right| \right)$$

In Figure 11, one of the isotherms measured in this work was compared with the predictions of the well-known Geng and Duan⁷ model. The predictions are somewhat acceptable (underestimation of the O₂ solubility in brine), but can be improved by readjusting the model parameters by including the new data.

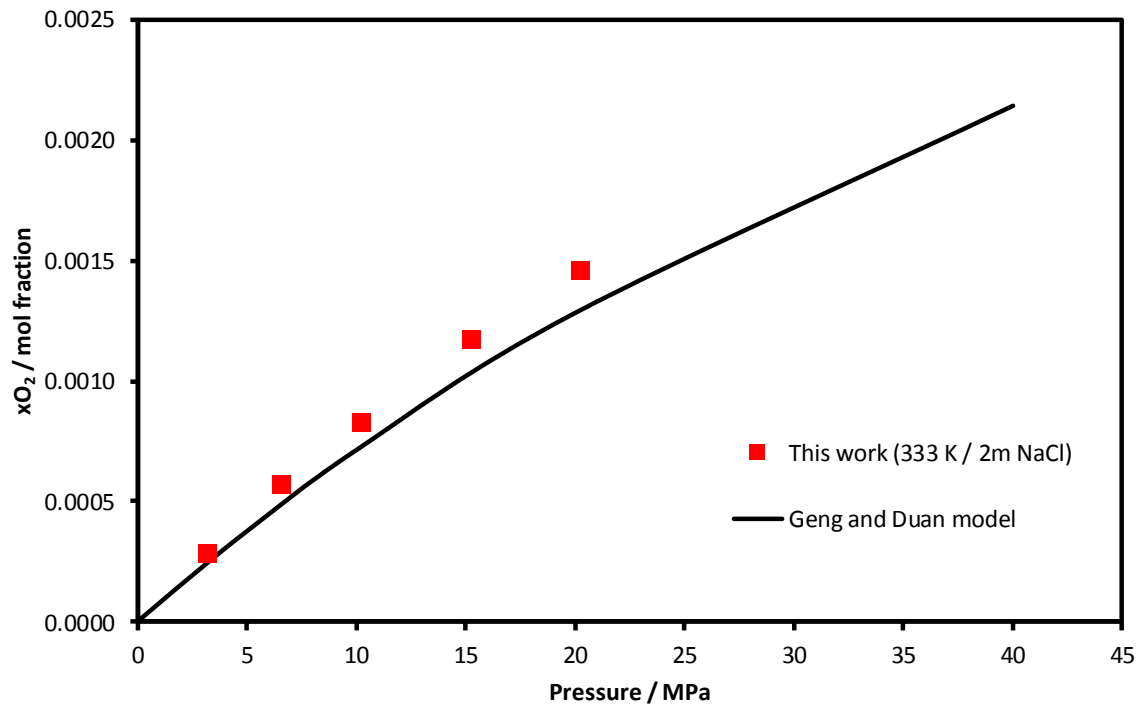


Figure 11 : Geng and Duan ^Z model predictions of O₂ solubility compared with data measured at 333 K (2 mol/kg_w).

The water content in the O₂-rich gas phase (O₂+H₂O system) was also studied. In Figure 12, the water content predictions with the e-PR-CPA, SW, and geochemical models are compared with data from the literature. All three models estimate water content very well, with a slight advantage of models with asymmetric parameters (SW and geochemical), since the gas and liquid phases are not represented by the same parameters (SW) or not by the same method (geochemical model: activity coefficient for the liquid phase and fugacity coefficient for the gas phase). However, the symmetric approach with a consistent model is preferable for reservoir simulation, since it is indispensable to perform stability analysis before each phase equilibrium calculation, especially for multi-component and multiphase systems, and this can only be achieved by consistent equations of state.

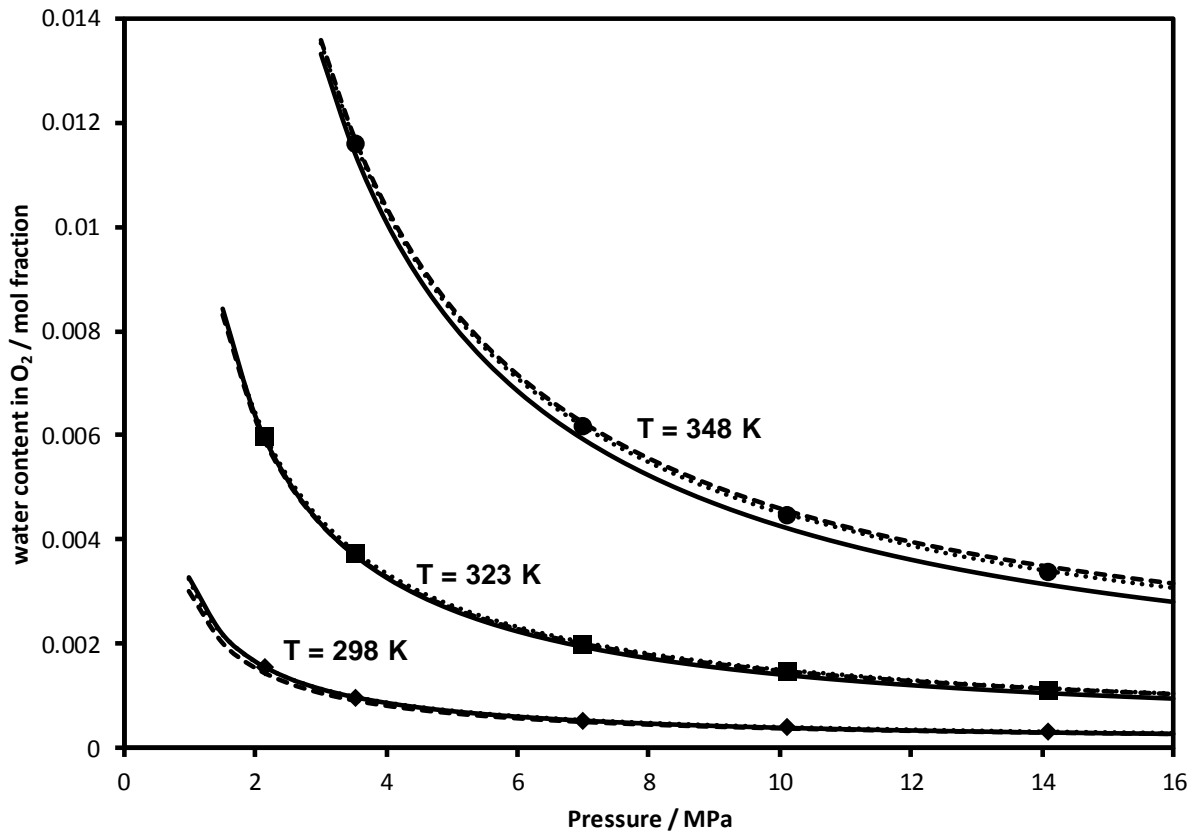


Figure 12 : Prediction of the water content in O₂ as a function of pressure at different temperatures by e-PR-CPA (solid line), SW (dashed line) and geochemical (dotted line) models. The data (symbols) are from Wylie and Fisher ⁴⁶.

Conclusions

The solubility of O₂ in NaCl brine was measured using two different techniques: the first one is based on the static-analytic method (liquid phase sampling and GC analysis) and the second one is a rocking cell setup (liquid phase sampling, gas/brine separation, gravimetric and volumetric analysis of brine and gas). For validation purpose, the measurements carried out using both techniques were compared, and consistency of results was verified. The solubility of CO₂ in NaCl brine (at high concentration) was also measured using the second technique. These measurements are intended to complement our previous work (on CO₂ solubility in brine), and also to validate the measurement technique by comparing some measurements with literature data.

The new measured solubility data were used to evaluate and improve existing or developed models. The e-PR-CPA and SW equations of state (phi-phi approach) were tested, and a geochemical model and the recently proposed model by Zheng and Mao (ZM) (gamma-phi approach) were used to process measured and literature O₂ solubility data. The measurements carried out also show the need to readjust the well-known Geng and Duan model by including these new data. The predictions of the water content in the gas phase (O₂-rich) by the three models (e-PR-CPA, SW, and geochemical) were evaluated by comparing them with literature data. All three models gave similar results. For CO₂, the solubility data were processed by the three models as well, whose parameterization was already done in our previous work.

All models capture very well the effect of temperature, pressure, and NaCl concentration on the solubility of O₂ and CO₂ with an absolute average deviation less than 5% with respect to the measured data. Each of these models can be used for solubility estimation, criteria such as accuracy, simplicity and speed of calculation can be considered in selecting the appropriate model and approach. Finally, we provided in Supporting Information tables of solubility data of O₂ and CO₂ in water and NaCl brine, generated by the e-PR-CPA model.

Supporting Information (SI)

Appendix A and tables of solubility data of O₂ and CO₂ in water and NaCl brine in a wide range of pressure and temperature.

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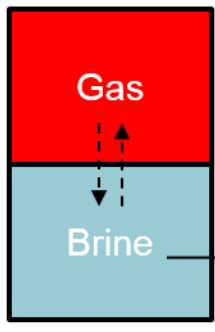
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For Table of Contents (TOC) Only

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