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## <sup>1</sup> Eco-CaMnO<sub>x</sub>: A Greener Generation of Eco-catalysts for Eco-friendly <sup>2</sup> Oxidation Processes

3 Camille Bihanic, Sébastien Diliberto, Franck Pelissier, Eddy Petit, Clotilde Boulanger, 4 and Claude Grison\*



18 manganese oxides:  $Ca_2Mn_3O_8$  and  $CaMnO_3$ . The high efficiency of Eco-CaMnO<sub>x</sub> catalysts was demonstrated via the epoxidation of 19 various biosourced terpenes and lipids, using the mixture  $H_2O_2/NaHCO_3$  as a green co-oxidant. This study demonstrated not only 20 the high potential of Eco-CaMnO<sub>x</sub> catalysts as alternatives to oxidative reagents prohibited by REACH regulation but also the 21 efficient synthesis of biosourced epoxides, which can be used as monomers for the preparation of biodegradable polymers. Finally, 22 the original composition of Eco-CaMnO<sub>x</sub> catalysts led to distinctive catalytic behaviors compared to previously studied Eco-Mn and 23 Pyr-Mn, allowing the preparation of sensitive epoxides such as linalool epoxide.

24 KEYWORDS: rehabilitation of mining sites: phytoextraction, biosourced Mn catalyst, Ca–Mn cluster, sustainable oxidation, eco-catalysis

#### 25 INTRODUCTION

<sup>26</sup> Along with the increase of the world's population, which keeps <sup>27</sup> demanding a higher standard of living, the claim for mineral <sup>28</sup> resources is also rising. While several concerns have been <sup>29</sup> raised over the elemental sustainability, the depletion of "trace <sup>30</sup> metallic elements" (or "TEs") is intensifying.<sup>1</sup> Growing <sup>31</sup> exploitation of mineral resources is one of the main causes <sup>32</sup> for the serious dissemination of TEs throughout the environ-<sup>33</sup> ment. TEs are among the most harmful pollutants. As they are <sup>34</sup> not biodegradable, their wide dispersion into different <sup>35</sup> ecosystems has raised concerns over their potential risks on <sup>36</sup> human health and the environment.<sup>2</sup>

<sup>37</sup> New Caledonia provides a demonstrative case of this <sup>38</sup> situation. The New Caledonian lagoon is the largest in the <sup>39</sup> world, being classified as one of the UNESCO World Heritage <sup>40</sup> Sites. New Caledonia is one of the highest biodiversity <sup>41</sup> "hotspots" in the world.<sup>3</sup> This high biodiversity results from <sup>42</sup> the unusual composition of its soil, which is rich in heavy <sup>43</sup> metals, particularly in nickel. However, nickel in soils also <sup>44</sup> implies intensive mining activities.<sup>4</sup> Nickel mines are opencast. <sup>45</sup> Excavations to access deep nickel lodes require the removal of <sup>46</sup> topsoil, upper soil horizons, and vegetation. The removal of the plant cover leads to the destruction of biodiversity, which <sup>47</sup> promotes soil erosion.<sup>5,6</sup> The leaching of bare soils drags the <sup>48</sup> sediments away into the streams near mining sites and then <sup>49</sup> into the lagoon, threatening the New Caledonian coral reef.<sup>7,8</sup> <sub>50</sub> This erosion also leads to dramatic events in the neighbor- <sub>51</sub> hood, such as landslides. <sub>52</sub>

The rehabilitation of mining sites is becoming a major 53 priority. Over the last decade, our laboratory has led a large- 54 scale program of ecological restoration of mining sites by the 55 reintroduction of a vegetal cover, based on the rich endemic 56 biodiversity of New Caledonia. Depending on the location of 57 the mining site, pioneer species adapted to local constraints 58 were selected. Among these species, many have the capacity to 59 concentrate heavy metals from the soils into their aerial 60 parts.<sup>9–11</sup> Manganese accumulators are the most widespread 61 and the most adapted to the restoration of mining sites. In 62

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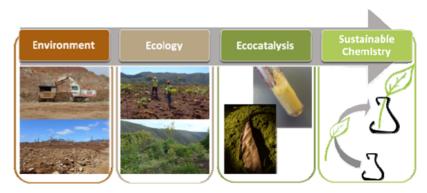


Figure 1. From the ecological restoration of New Caledonian mining sites to ecocatalysis.



Figure 2. Steps for preparation of the previously studied Eco-Mn catalysts and of the new Eco-CaMnO<sub>x</sub> from Mn-accumulating plant species.

63 particular, species of the genus Grevillea (Proteaceae) are 64 considered as the leading species for restoration, representing 65 about 58% of the species reintroduced by our group (Figure 66 1).<sup>12,13</sup>

f1

f1

f2

As such ecological programs could represent an economic 67 68 cost for mining operators, our group has combined restoration 69 with economic outlets. Taking advantage of the adaptive 70 capacity of these particular plants to accumulate heavy metals, 71 it is possible to directly turn metal-rich leaves into green and 72 efficient catalysts used in organic chemistry. This original 73 valorization of biomass has opened a new perspective in 74 sustainable chemistry: "eco-catalysis" (Figure 1).<sup>14,15</sup> The 75 catalysts coming from biomass, named eco-catalysts (Eco-76 M), associate the phytoextracted metal with many physio-77 logical elements essential for plant metabolism. These 78 polymetallic systems create original chemical species and 79 generate synergetic catalytic effects between their components. 80 A wide range of eco-catalysts has been prepared and used in 81 many revisited mechanisms of chemistry, such as green <sup>82</sup> oxidation,<sup>16–19</sup> green reduction,<sup>20,21</sup> Lewis acid catalysis,<sup>2</sup> <sup>83</sup> and cross-coupling reactions.<sup>15,29–31</sup>

<sup>84</sup> Concerning manganese, two generations of Eco-Mn catalysts <sup>85</sup> were prepared from Mn-accumulating plant species belonging <sup>86</sup> to the genus of Grevillea (Figure 2). In each case, the first step <sup>87</sup> was the preparation of an intermediate Eco-Mn<sub>1</sub>. It was based <sup>88</sup> on a controlled thermal treatment of Mn-rich biomass, <sup>89</sup> followed by a chemical activation by HCl.<sup>16</sup> From Eco-Mn<sub>1</sub>, <sup>90</sup> two oxidative eco-catalysts were formed by a sequential <sup>91</sup> addition of either NaOH/O<sub>2</sub>/HCl (Eco-Mn<sub>2</sub>)<sup>16</sup> or H<sub>2</sub>O<sub>2</sub>/ <sup>92</sup> NaOH (Eco-MnO<sub>2</sub>).<sup>17</sup>

<sup>93</sup> Eco-Mn revealed an original polymetallic composition <sup>94</sup> resulting in marked Brønsted and Lewis acidities and displayed <sup>95</sup> superior catalytic performances than conventional Mn <sup>96</sup> catalysts. For example, Eco-Mn<sub>1</sub> was successfully employed <sup>97</sup> in the aminoreduction of ketones<sup>20</sup> and constitutes the first <sup>98</sup> example of reduction promoted by a Mn-based catalyst. Eco-<sup>99</sup> Mn<sub>2</sub> and Eco-MnO<sub>x</sub> led to a practical and elegant solution to the long-standing challenge of oxidative cleavage of 1,2-diols 100 into aldehyde or ketones.<sup>17,18</sup> Supported Eco-Mn<sub>1</sub> provided 101 also a huge potential as green catalysts for valuable 102 epoxidation.<sup>18</sup> Finally, Eco-Mn<sub>1</sub> acted as "Janus catalysts" by 103 promoting tandem sequences of multicomponent type 104 oxidations (synthesis of substituted pyridines) and cyclizations 105 (synthesis of *p*-cymene).<sup>16</sup> Comparison of their properties to 106 that of commercial salts highlighted the superior catalytic 107 activities of Eco-Mn. 108

Recently we reported an extensive structural study of Eco- 109  $Mn_1$ , characterized by inductive coupled plasma-mass spec- 110 troscopy, X-ray powder diffraction spectroscopy (XRPD), and 111 X-ray absorption spectroscopy (XANES and EXAFS), 112 completed with density functional theory calculations.<sup>32</sup> In a 113 systematic analysis, we also analyzed the thermal residues, from 114 New Caledonian Mn-accumulating plant species of Grevillea 115 generated before the chemical activation, by XPRD (Figure 2). 116 We detected a polymetallic oxide (a mixed manganese– 117 calcium oxide, Ca<sub>2</sub>Mn<sub>3</sub>O<sub>8</sub>) instead of polymetallic chlorides as 118 for Eco-Mn<sub>1</sub> and Eco-Mn<sub>2</sub>.

While rare examples have described the use of mixed  $Mn-_{120}$  Ca oxide nanoparticles as oxidants,<sup>33,34</sup> no description was 121 found for the use of Ca<sub>2</sub>Mn<sub>3</sub>O<sub>8</sub> in organic synthesis. However, 122 mixed Mn–Ca oxides display biomimetic oxidative properties 123 of the natural cofactor CaMn<sub>4</sub>O<sub>5</sub> of Photosystem II. Indeed, 124 CaMn<sub>4</sub>O<sub>5</sub> performs the oxidation of water during the 125 photosynthesis process,<sup>35</sup> and the complex Ca<sub>2</sub>Mn<sub>3</sub>O<sub>8</sub> presents 126 similar oxidative activities in the electrochemical oxidation of 127 water.<sup>36–38</sup>

The above facts prompted us to further structurally 129 characterize these new potential oxidative eco-catalysts, 130 which we named Eco-CaMnO<sub>x</sub>. We investigated the mineral 131 composition of Eco-CaMnO<sub>x</sub> by microwave plasma-atomic 132 emission spectrometer (MP-AES) and their crystalline 133 composition by XRPD. The morphology of Eco-CaMnO<sub>x</sub> 134 was analyzed by high-resolution transmission electron 135 microscopy (HRTEM), and the structural distribution of 136

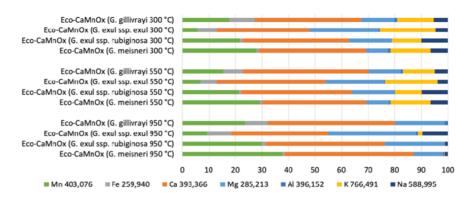


Figure 3. Histogram representing the relative weight percentages of elements in  $Eco-CaMnO_x$  catalysts, prepared from different plant species of Grevillea and thermal treatments, determined by MP-AES analyses.

<sup>137</sup> mineral species was mapped by scanning transmission electron
 <sup>138</sup> microscopy-energy-dispersive X-ray spectroscopy (STEM <sup>139</sup> EDX).

The oxidative potential of Eco-CaMnO<sub>x</sub> catalysts was then 141 investigated in the epoxidation of terpenes with new challenges 142 that would meet the principles of green chemistry: (1) 143 developing a "waste-free" process to prepare catalysts, by 144 suppressing the acidic and basic activation steps; (2) 145 generating catalysts with high catalytic oxidative performances; 146 and (3) providing an eco-friendlier synthesis of biosourced 147 epoxides.

#### 148 **EXPERIMENTAL SECTION**

Chemicals. All materials and reagents were purchased from Sigma-150 Aldrich and were used without further purification.

**Preparation of Eco-CaMnO<sub>x</sub> Catalysts.** Eco-CaMnO<sub>x</sub> were 152 prepared from harvested leaves of New Caledonian manganese-153 accumulating plants: *Grevillea exul ssp. exul, Grevillea exul ssp.* 154 *rubiginosa, Grevillea gillivrayi,* and *Grevillea meisneri*. Plant leaves were 155 coming from the litter of the plants. Harvests are made respecting 156 legal authorizations. Harvested biomass was air-dried at room 157 temperature (rt) and grinded. The obtained powder was thermally 158 treated in an oven under air flow at 300, 550, or 950 °C for 6 h.

**Preparation of Synthetic Catalysts.** Synthetic ashes were to obtained by mixing all together well-chosen commercial metallic tal salts, so that the relative percentage of metallic elements in the sarting mixture was exactly the same as in the leaves of *Grevillea exul* ssp. *rubiginosa*. The salt mixture was then thermally treated at 550 °C tak following the same procedure as used for Eco-CaMnO<sub>x</sub>. The chosen tals salts were the following: manganese malate trihydrate (MnC<sub>4</sub>H<sub>4</sub>O<sub>5</sub>. tal 3H<sub>2</sub>O), calcium oxalate (CaC<sub>2</sub>O<sub>4</sub>·2H<sub>2</sub>O), iron phosphate (FePO<sub>4</sub>· tal 2H<sub>2</sub>O), magnesium phosphate (Mg<sub>3</sub>(PO<sub>4</sub>)<sub>2</sub>·xH<sub>2</sub>O), sodium chloride tals (NaCl), potassium chloride (KCl), and aluminum oxalate (Al<sub>2</sub>C<sub>6</sub>O<sub>12</sub>· tals 2H<sub>2</sub>O).

 $_{170}$  Ca<sub>2</sub>Mn<sub>3</sub>O<sub>8</sub> was synthesized by grinding CaCO<sub>3</sub> (4 mmol, 400 mg)  $_{171}$  and MnCO<sub>3</sub> (6 mmol, 690 mg) in a mortar until the obtained powder  $_{172}$  was homogeneous. The powder was then thermally treated in an oven  $_{173}$  under air flow at 800  $^\circ C$  for 18 h.

**Epoxidation of Alkenes.** In a typical procedure, the alkene (1.6 175 mmol, 1 equiv), the catalyst (8  $\mu$ mol, 0.005 equiv Mn), and NaHCO<sub>3</sub> 176 (8 mmol, 5 equiv) were stirred in a mixture of acetone (20 mL) and 177 water (20 mL) at room temperature for 10 min. H<sub>2</sub>O<sub>2</sub> (30% w/w in 178 H<sub>2</sub>O, 8 mmol, 5 equiv) was added dropwise during 2 h in the mixture 179 while stirring. After 2 h, the catalyst was filtered off and the reaction 180 mixture was extracted with ethyl acetate. The organic phases were 181 gathered and dried with Na<sub>2</sub>SO<sub>4</sub>. The solvent was then removed by 182 evaporation.

#### RESULTS AND DISCUSSION

Preparation and Characterization of Eco-CaMnO<sub>x</sub> <sup>184</sup> Catalysts. Preparation of Eco-CaMnO<sub>x</sub> Catalysts. Eco- <sup>185</sup> CaMnO<sub>x</sub> catalysts were prepared from Mn-rich biomass. <sup>186</sup> Four species of the Grevillea genus are mainly used to <sup>187</sup> rehabilitate mining sites across both provinces in New <sup>188</sup> Caledonia: G. gillivrayi, G. meisneri, G. exul ssp. exul, and G. <sup>189</sup> exul ssp. rubiginosa. Plant leaves were harvested by hand from <sup>190</sup> the plant litter, on the mining sites, which are currently <sup>191</sup> rehabilitated by our group. <sup>192</sup>

183

In this study, two parameters were studied to investigate 193 their influence on Eco-CaMnO<sub>x</sub> catalytic properties: the plant 194 species, from which the catalysts were prepared, and the 195 temperature of the thermal treatment. The dried leaves, from 196 each of the four species of the Grevillea genus, were thermally 197 treated in an oven, under air flow, at 300, 550, or 950 °C for 6 198 h, to destroy the organic matter. Indeed, these temperatures 199 were chosen according to the literature, as different manganese 200 oxides could be formed depending on the corresponding 201 heating temperature: MnO<sub>2</sub>, Mn<sub>2</sub>O<sub>3</sub>, or Mn<sub>3</sub>O<sub>4</sub>.<sup>39,40</sup> Eco- 202 CaMnO<sub>x</sub> catalysts were then characterized by MP-AES, XRPD, 203 HRTEM, and STEM-EDX mapping. 204

MP-AES Analysis of Eco-CaMnO<sub>x</sub> Catalysts. Metallic 205 composition of intact Mn-accumulating plant leaves and of 206 Eco-CaMnO<sub>x</sub> catalysts, resulting from different plant species 207 and thermal treatments, was studied by MP-AES analyses. 208 Analyses were performed in triplicate for each sample to 209 determine the standard deviation of the measurement (Table 210 S1). 211

The results showed that Mn was the major transition metal 212 in all eco-catalysts (1 to 16.1 wt %), except for Eco-CaMnO<sub>x</sub>  $^{213}$ (G. exul ssp. exul 300 °C) (Figure 3). As Ca, Mg, Na, K, and 214 f3 Fe are essential mineral components of plants, they were found 215 in Eco-CaMnO<sub>x</sub> catalysts, Ca being the major mineral element 216for every eco-catalyst. Interestingly, the composition of Eco- 217 CaMnO<sub>x</sub> catalysts derived from different plants of the same 218 species was quite similar, as shown by low RSD (Table S1). 219 This reproducibility of composition within species could be 220 explained by the harvest timing.<sup>13</sup> Indeed, leaves were 221 harvested when they became a vegetal litter: they have the 222 highest Mn concentration for each species. As a result of the 223 accumulating specificity of each plant species, the chemical 224 composition appeared different between Eco-CaMnO<sub>x</sub> cata- 225 lysts. 226

Within a species the heating temperature at 550 and 950  $^{\circ}$ C 227 did not have much influence on the chemical composition. But 228 at 300  $^{\circ}$ C the elements were less concentrated. This might be 229

|  | CaCO <sub>3</sub> | CaSO <sub>4</sub> | KCl | $Ca_2Mn_3O_8$ | CaMnO <sub>3</sub> | $Mn_2O_3$ | K <sub>2</sub> SO <sub>4</sub> | $K_3Na(SO_4)_2$ |
|--|-------------------|-------------------|-----|---------------|--------------------|-----------|--------------------------------|-----------------|
| Eco-CaMnO <sub>x</sub> (G. gillivrayi 300 °C) <sup>a</sup>     | х                 |                   |     |               |                    |           |                                |                 |
| Eco-CaMnO <sub>x</sub> (G. gillivrayi 550 °C)                  | х                 |                   | х   | x             |                    |           |                                | х               |
| Eco-CaMnO <sub>x</sub> (G. gillivrayi 950 °C)                  |                   | х                 |     |               | х                  | х         |                                |                 |
| Eco-CaMnO <sub>x</sub> (G. exul ssp. exul 550 °C) <sup>a</sup> | х                 |                   | x   |               |                    |           | х                              |                 |
| Eco-CaMnO <sub>x</sub> (G. exul ssp. rubiginosa 550 °C)        | х                 |                   | x   | x             |                    |           |                                | х               |
| Eco-CaMnO <sub>x</sub> (G. meisneri 550 °C)                    | х                 |                   | x   | x             |                    |           |                                | х               |
| synthetic ash control (550 °C)                                 |                   |                   | х   |               |                    | х         |                                |                 |
| <sup><i>a</i></sup> Mn was not present in a crystalline form.  |                   |                   |     |               |                    |           |                                |                 |

Table 1. Crystalline Species Identified in Eco-CaMnO<sub>x</sub> Catalysts and in Synthetic Ash Control

 $^{230}$  due to a partial degradation of the organic matter at 300  $^\circ \rm C$   $^{231}$  and a total degradation above 550  $^\circ \rm C.$ 

<sup>232</sup> For further characterizations and experimentations, *G.* <sup>233</sup> *gillivrayi* was chosen as the model species because the Eco-<sup>234</sup> CaMnO<sub>x</sub> catalysts from *G. gillivrayi* present an average <sup>235</sup> composition of minerals among the other species.

236 XRPD Analysis of Eco-CaMnO<sub>x</sub> Catalysts. XRPD was 237 performed to deliver insights on the crystalline species present 238 in Eco-CaMnO<sub>x</sub> catalysts and to compare with a reconstituted 239 control of synthetic ashes. The synthetic ash control was 240 obtained by mixing commercial metallic salts chosen so that 241 the relative percentage of metallic elements in the starting 242 mixture was exactly the same as in the leaves of *G. exul* ssp. 243 *rubiginosa*, and was followed by a thermal treatment at 550 °C. 244 The identified crystalline phases are summarized in Table 1. 245 Mn was not present in a crystalline form in the eco-catalysts

246 prepared at 300 °C.

Interestingly, for the other temperatures, Mn was present as mixed calcium-manganese oxides.  $Ca_2Mn_3O_8$  was identified in example all Eco-CaMnO<sub>x</sub> prepared at 550 °C, except for *G. exul* ssp. so *exul* in which crystalline species of manganese was not observed. The absence of crystalline manganese species in *G.* so *exul* ssp. *exul* could be linked to a low ratio of Mn/Ca (Table S1) preventing the crystallization process. CaMnO<sub>3</sub> was so *exul* in all Eco-CaMnO<sub>x</sub> prepared at 950 °C. CaMnO<sub>3</sub> so could result from the degradation of  $Ca_2Mn_3O_8$  at high temperature, which was consistent with the calcination temperatures used by Han et al. to prepare these two se complexes.<sup>41</sup>

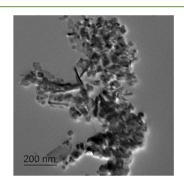
No crystalline mixed manganese–calcium oxide was observed in the synthetic ash control. It suggested that a crystallization mechanism is specific to plant-derived ecocatalysts and that it cannot be reproduced in a simple mixture of ashes. This difference in crystallization pathways illustrates the vegetal footprint of Eco-CaMnO<sub>xy</sub> which is in accordance with what we reported for Eco-Mn<sub>1</sub>.<sup>32</sup>

<sup>266</sup> The structure of  $Ca_2Mn_3O_8$  has been reported as infinite <sup>267</sup> sheets of  $Mn_3O_8^{4-}$  held together by calcium ions. Mn ions are <sup>268</sup> octahedrally coordinated by oxygen atoms and occupy three-<sup>269</sup> fourths of the octahedral layer sites. The other one-fourth is <sup>270</sup> vacant.<sup>37,42</sup> The negative charge is further compensated by the <sup>271</sup> presence of Ca ions in trigonal prismatic sites located above <sup>272</sup> and below layer vacancies.<sup>38</sup>

273 CaMnO<sub>3</sub> has a perovskite structure based on corner-shared 274 MnO<sub>6</sub>-octahedra. Mn ions, present in the oxidation state IV, 275 are located at the center of the octahedron, while each Ca ion 276 occupies the interoctahedral sites.<sup>38,41</sup>

The layered structure of  $Ca_2Mn_3O_8$  shares similarities with the cofactor  $CaMn_4O_5$ , the oxygen-evolving complex present in Photosystem II, which performs the photo-oxidation of water during photosynthesis. The incorporation of calcium into manganese oxides greatly improves water oxidation capaci- <sup>281</sup> ties. <sup>43,44</sup> Research on a series of manganese–calcium oxides <sup>282</sup> showed that  $Ca_2Mn_3O_8$  and  $CaMnO_3$  were efficient catalysts <sup>283</sup> for the oxygen evolution reaction and oxygen reduction <sup>284</sup> reaction. Indeed, manganese ions in  $Ca_2Mn_3O_8$  and  $CaMnO_3$  <sup>285</sup> are in the oxidation state IV and they may present interesting <sup>286</sup> oxidative properties similar to  $MnO_2$ .

HRTEM Analysis of Eco-CaMnO<sub>x</sub> Catalysts (G. gillivrayi, 288 550 °C). HRTEM images of Eco-CaMnO<sub>x</sub> (G. gillivrayi, 550 289 °C) revealed different particles with various shapes (Figure 4). 290 f4

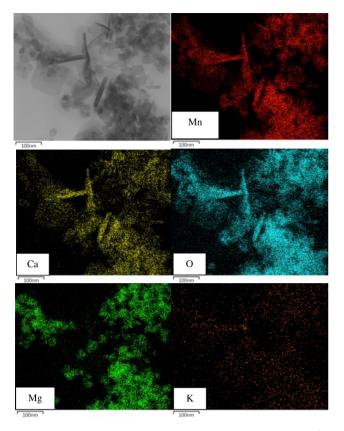


**Figure 4.** HRTEM image of Eco-CaMnO<sub>x</sub> catalysts (*G. gillivrayi* 550 °C).

Small round particles of about 10–50 nm in diameter, lamellar 291 particles of about 10 nm width over 100 nm length, as well as 292 thin layer-shape particles seemed blended together into a 293 matrix. 294

STEM-EDX Mapping of Eco-CaMnO<sub>x</sub> (G. gillivrayi, 550 °C). 295 The STEM-EDX analysis was used to establish the chemical 296 composition mapping of Eco-CaMnO<sub>x</sub> catalysts (G. gillivrayi, 297 550 °C) (Figure 5). Manganese, calcium, magnesium, and 298 fS potassium were expectedly present, as shown by MP-AES 299 analyses. The polymetallic structure of Eco-CaMnO<sub>x</sub> catalysts 300 was supported by the aggregation of manganese, oxygen, and 301 all of the other elements in the round particles, the layer-shape 302 particles, and the matrix. However, it should be noticed that 303 the lamellar particles were exclusively composed of manganese, 304 oxygen, and calcium. The association of these only three 305 elements in a single well-defined shape of particles confirmed 306 the presence of the Ca<sub>2</sub>Mn<sub>3</sub>O<sub>8</sub> complex, and that this complex 307 is organized in lamellar sheets. 308

Extensive structural analyses of the different Eco-CaMnO<sub>x</sub> 309 catalysts showed the presence of two unusual and valuable 310 mixed calcium-manganese complexes:  $Ca_2Mn_3O_8$  and 311 CaMnO<sub>3</sub>. The oxidative potential of the Eco-CaMnO<sub>x</sub> 312 catalysts was studied in the epoxidation of alkenes and 313 especially terpenes, as biosourced substrates. 314



**Figure 5.** STEM-EDX mapping of Eco-CaMnO<sub>x</sub> catalysts (*G. gillivrayi*, 550 °C).

Use of Eco-CaMnO<sub>x</sub> Catalysts in Synthesis. The 315 316 standard methods used in fine chemical industries can access 317 epoxidation of substitute alkenes by the use of stoichiometric 318 amounts of organic peroxides or percarboxylic acids, such as 319 meta-chloroperoxybenzoic acid.<sup>45</sup> Other methods include the use of dimethyldioxirane (also known as Murray's reagent), 320 formed in situ from the reaction between acetone and oxone, 321 or electrophilic halide source in the presence of a base.<sup>47</sup> 322 Owing to safety concerns and/or the issue of large production 323 of wastes by these processes, there is a strong need to develop 324 325 new safer and eco-friendlier methods.

Hydrogen peroxide is considered as an ideal alternative 326 327 oxidant on both environmental and economic grounds.<sup>48</sup> Not only is it relatively cheap, easily available, and stable at the 328 usual concentration (typically <60 wt %), but it is also a clean 329 oxidizing reagent, as it only forms water as a byproduct. 330 However, it requires an activation to catalyze the oxygen-331 transfer process. Many catalytic systems using H2O2 as the 332 oxidant for epoxidation of alkenes were based on transition-333 metal catalysts.<sup>49-51</sup> However, the use of economically and 334 environmentally unsustainable metals, such as rhenium, 335 vanadium,<sup>56,57</sup> molybdenum,<sup>58-60</sup> or tungsten,<sup>61-64</sup> prompted 336 337 the research toward inexpensive, abundant, and innocuous transition metals. In particular, iron or manganese revealed to 338 339 be one of the more promising elements thanks to their 340 relatively low toxicity and their abundance in Earth's crust.<sup>65,66</sup> 341 Porphyrin-Mn have been extensively investigated as a mimic 342 of cytochrome P450,<sup>67–70</sup> but suffer from difficulties in 343 synthesis and purification. As they offer synthetical advantages 344 over porphyrin systems, considerable attention was given to 345 Salen-Mn,<sup>71,72</sup> in particular to the Jacobsen asymmetric

epoxidation reaction.<sup>73–75</sup> However, the homogeneous nature 346 of such metalloporphyrin and Schiff base complexes leads not 347 only to deactivation due to oxidative degradation of the 348 ligand<sup>76</sup> but also to environmental costs concerning their 349 nonrecyclability. To rectify both problems, heterogenization of 350 these Mn-based catalysts was demonstrated, by grafting on a 351 solid support or immobilization into porous solids, such as 352 silica, polymers, nanoparticles, and zeolites.<sup>77–80</sup> For example, 353 heterogeneous Ti silicates are nowadays used at an industrial 354 scale with  $H_2O_2$  for conducting epoxidation reactions with very 355 high catalytic and environmental performances.<sup>81</sup>

In our previous works, we showed that montmorillonite- 357 supported Eco-Mn<sub>1</sub> catalyzed the epoxidation of styrene. Eco- 358 Mn<sub>1</sub> contained only 0.31 mol % of manganese, a much lower 359 content of manganese than that reported in previously 360 described Mn-derived heterogeneous catalysts.  $^{82,83}$  Compar- 361 ison of Eco-Mn<sub>1</sub> properties to those of heterogeneous catalysts 362 made by incorporation of commercial MnCl<sub>2</sub>·4H<sub>2</sub>O and FeCl<sub>3</sub>· 363 6H<sub>2</sub>O highlighted the superior catalytic activity of polymetallic 364 species present in Eco-Mn<sub>1</sub>. These promising results prompted 365 us to investigate the utilization of Eco-CaMnO<sub>x</sub> as an 366 epoxidizing agent and to study the possible cooperative 367 catalytic effect between Ca and Mn.

Optimization of the Conditions for the Epoxidation of  $\alpha$ - 369 pinene. The epoxidation of  $\alpha$ -pinene was chosen as a probe 370 reaction to optimize the reaction conditions.  $\alpha$ -pinene is a 371 monoterpene mostly found in pine trees, an abundant natural 372 resource. The pinene oxide represents an inexpensive 373 biosourced starting material for the synthesis of flavors, 374 fragrances, and agrochemical and therapeutic substances.<sup>84–86</sup> 375 However,  $\alpha$ -pinene oxide is a sensitive and reactive substrate, 376 which rearranges easily in acid conditions.<sup>87,88</sup> The rearrange- 377 ment of  $\alpha$ -pinene oxide leads to the formation of a wide range 378 of products, which depends largely on the acid-base 379 properties of the catalytic system. Over 200 compounds were 380 reported when the isomerization-reaction temperature was 381 above 100 °C.<sup>87</sup> It is well described that Lewis acid sites favor 382 the formation of campholenic aldehyde, pinocarveol, and iso- 383 pinocamphone, whereas Brønsted acid sites result in the 384 formation of *trans*-carveol, *trans*-sobrerol, and *p*-cymene.<sup>89-91</sup> 385 For instance, one of the most desired products resulting from 386 the  $\alpha$ -pinene oxide is campholenic aldehyde because it is an 387 intermediate for the manufacture of sandalwood fragrances. 388 The epoxidation of  $\alpha$ -pinene into  $\alpha$ -pinene oxide remains a 389 challenge because of its isomerization into many different 390 byproducts. 391

In a typical procedure,  $\alpha$ -pinene, Eco-CaMnO<sub>x</sub> (*G. gillivrayi* 392 550 °C), and NaHCO<sub>3</sub> were stirred in a mixture of 393 acetone:water (1:1) at room temperature for 10 min. H<sub>2</sub>O<sub>2</sub> 394 (30% w/w in H<sub>2</sub>O) was added dropwise during 2 h in the 395 mixture while stirring. After 2 h, the catalyst was filtered off and 396 the reaction mixture was extracted with ethyl acetate. The 397 organic layers were gathered and dried with Na<sub>2</sub>SO<sub>4</sub>. The 398 solvent was then removed by evaporation and the reaction 399 products analyzed by gas chromatography–mass spectrometry 400 (GC–MS)/flame ionization detector (FID). 401

Effect of  $H_2O_2$  Amount. The effect of the quantity of  $H_2O_2$  402 added into the reaction mixture was studied, as an excessive 403 amount of  $H_2O_2$  could lead to a decrease in epoxide selectivity 404 by overoxidation.<sup>92</sup> The conversion, yield, and selectivity 405 followed the same trend (Table 2). Increasing the quantity of 406 t2  $H_2O_2$  increased the conversion, yield, and selectivity before 407 reaching a threshold. Almost total conversion of  $\alpha$ -pinene **1a** 408

Table 2. Effect of the Amount of  $H_2O_2$  and of the Adding Time on the Epoxidation of  $\alpha$ -pinene<sup>*a*</sup>

|       |   | Eco-CaMnOx (G. gillivra<br>NaHCC<br>H <sub>2</sub> O <sub>2</sub> (<br>H <sub>2</sub> O /<br>rt | Mn)      |                           |                                   |  |
|-------|---|---|----------|---------------------------|-----------------------------------|--|
| entry | $\begin{array}{c} H_2O_2\\ (equiv) \end{array}$ | addition time<br>(min)  | $(\%)^b$ | yield<br>(%) <sup>b</sup> | selectivity<br>(%) <sup>b,c</sup> |  |
| 1     | 0   | 120   | 0        | 0                         | 0                                 |  |
| 2     | 1   | 120   | 62       | 21                        | 34                                |  |
| 3     | 3   | 120   | 80       | 44                        | 55                                |  |
| 4     | 4   | 120   | 77       | 47                        | 61                                |  |
| 5     | 5   | 120   | 98       | 64                        | 65                                |  |
| 6     | 10  | 120   | 99       | 62                        | 63                                |  |
| 7     | 10  | 60  | 98       | 65                        | 66                                |  |
| 8     | 10  | 30  | 63       | 41                        | 65                                |  |

<sup>*a*</sup>Reaction conditions:  $\alpha$ -pinene (1.6 mmol, 1 equiv), catalyst (8  $\mu$ mol, 0.005 equiv Mn), NaHCO<sub>3</sub> (8 mmol, 5 equiv), H<sub>2</sub>O<sub>2</sub> (30 wt %), and H<sub>2</sub>O (20 mL): acetone (20 mL), rt, 2 h. <sup>*b*</sup>Conversion, yield, and selectivity were established by FID using biphenyl as internal standard. <sup>*c*</sup>Selectivity was calculated as the ratio of yield over conversion.

409 and a yield of 64% in epoxide **2a** were reached with 5 equiv of 410  $H_2O_2$  (Table 2, entry 5). The addition time of  $H_2O_2$  in the 411 reaction mixture was also investigated. Although the selectivity 412 in epoxide remained similar by decreasing the addition time, 413 the conversion dropped from 98% in 1–2 h (Table 2, entries 6, 414 7) to 63% in 30 min (Table 2, entry 8). These results 415 supported the importance of a slow addition of  $H_2O_2$  in 416 oxidative reactions. Indeed, it was reported that a gradual 417 addition of  $H_2O_2$  decreased its self-decomposition.<sup>93,94</sup>

The selectivity in  $\alpha$ -pinene oxide gave some information 418 419 about Eco-CaMnO<sub>x</sub>. The oxygenated byproducts observed, 420 such as campholenic aldehyde, carveol, and iso-pinocamphone, 421 could be explained by the easy opening and rearrangement of 422 the epoxide by Lewis acid sites. This could reveal the presence 423 of many metallic species in our catalysts, like Fe, Ca, and Mg, 424 which could confer Lewis acid properties to Eco-CaMnO<sub>x</sub> 425 catalysts. As it was reported that  $\alpha$ -pinene oxide could also 426 rearrange spontaneously in acid or neutral aqueous phase <sup>427</sup> media,<sup>90</sup> the epoxide was directly engaged in the reaction with 428 and without any catalyst, to test its stability. In the presence of 429 Eco-CaMnO<sub>x</sub> catalysts a conversion of 45% was observed, 430 whereas it was fully recovered without any catalyst. This result 431 indicated that the epoxide was stable in our conditions, even in 432 the presence of water, and that its rearrangement only occurred 433 in the presence of Eco-CaMnO<sub>x</sub>. This supports the presence of 434 Lewis acid sites in Eco-CaMnO<sub>x</sub>. Allylic oxidation is often a 435 competitive process of epoxidation in the oxidation of cyclic 436 olefins.<sup>95,96</sup> As both processes could occur simultaneously, it 437 could explain the formation of verbenone, identified among the 438 different byproducts.

For the following reactions, 5 equiv of  $H_2O_2$  was employed 440 as it represented the smallest amount affording total 441 conversion and high yield in epoxide. The addition time was 442 kept at 2 h.

443 Effect of NaHCO<sub>3</sub> Amount. The effect of the quantity of 444 NaHCO<sub>3</sub> added into the reaction mixture was investigated 445 (Table 3). No conversion of α-pinene was observed in the 446 absence of sodium hydrogen carbonate (Table 3, entry 1). 447 This result supported the essential presence of sodium 448 hydrogen carbonate allowing the epoxidation. It is assumed

Table 3. Effect of the Amount of NaHCO<sub>3</sub> on the Epoxidation of  $\alpha$ -pinene<sup>*a*</sup>

| -     | -                          |   |                        |                                |
|-------|----------------------------|---|------------------------|--------------------------------|
|       | Eco-CaN                    | InOx ( <i>G. gillivrayi</i> 550 °C) (0<br>NaHCO <sub>3</sub><br>H <sub>2</sub> O <sub>2</sub> (30 wt%; 5 eq.) | .005 eq. Mn)           | $\searrow$                     |
|       |                            | H <sub>2</sub> O / Acetone<br>rt, 2 h   |                        | 2a                             |
| entry | NaHCO <sub>3</sub> (equiv) | conversion (%) <sup>b</sup>   | yield (%) <sup>b</sup> | selectivity (%) <sup>b,c</sup> |
| 1     | 0                          | 0   | 0                      | 0                              |
| 2     | 0.5                        | 36  | 2                      | 6                              |
| 3     | 1                          | 47  | 7                      | 15                             |
| 4     | 3                          | 82  | 38                     | 46                             |
| 5     | 5                          | 98  | 64                     | 65                             |

<sup>*a*</sup>Reaction conditions:  $\alpha$ -pinene (1.6 mmol, 1 equiv), catalyst (8  $\mu$ mol, 0.005 equiv Mn), NaHCO<sub>3</sub>, H<sub>2</sub>O<sub>2</sub> (30 wt %; 8 mmol, 5 equiv), and H<sub>2</sub>O (20 mL): acetone (20 mL), rt, 2 h. <sup>*b*</sup>Conversion, yield, and selectivity were established by FID using biphenyl as internal standard. <sup>*c*</sup>Selectivity was calculated as the ratio of yield over conversion.

that NaHCO<sub>3</sub> and  $H_2O_2$  could produce in situ peroxymono- 449 carbonate ions  $(HCO_4^{-})$ ,<sup>97,98</sup> which would react with the Mn- 450 eco-catalyst to form the active epoxidizing reagent. Indeed, a 451 neutral or slightly basic pH (range from 7 to 9) is optimal for 452 this bicarbonate-activated peroxide system, which corresponds 453 to the pH values of the aqueous phase that ranged from 8.2 to 454 8.8 in our system. 455

An attempt to reduce  $NaHCO_3$  quantity resulted in 456 decreasing conversion, yield, and selectivity in epoxide. 457 Therefore, 5 equiv of  $NaHCO_3$  seemed to be the lowest 458 quantity giving high conversion and yield (Table 3, entry 5). 459

Effect of Catalyst Loading. The effect of the quantity of 460 Eco-CaMnO<sub>x</sub> catalysts was then studied using  $\alpha$ -pinene as the 461 substrate (Table 4). A low quantity of manganese gave high 462 t4 conversion rates. Almost total conversion and 64% yield were 463 obtained with only 0.005 equiv in manganese (Table 4, entry 464 4). This result is remarkable compared to standard manganese-465 based catalysts, which usually require to be used in excess.<sup>99</sup> 466

As a control, the reaction was carried out in the absence of  $_{467}$  Eco-CaMnO<sub>x</sub> catalysts. The reaction could not occur in the  $_{468}$  corresponding reaction time, in 2 h (Table 4, entry 1).

The oxidative capacity of Eco-CaMnO<sub>x</sub> was also compared 470 to synthetic catalysts (Table 4, entries 7–9). The synthetic 471  $Ca_2Mn_3O_8$  catalyst was prepared following the procedure 472 described by Najafpour et al.,<sup>38</sup> and commercial manganese 473 dioxide was activated. 474

As expected, conversion of  $\alpha$ -pinene catalyzed by calcium 475 oxide was negligible (Table 4, entry 9). Calcium oxide species 476 alone cannot catalyze the epoxidation of  $\alpha$ -pinene, since 477 calcium is not electroactive. However, conversion was 478 increased by the addition of calcium to manganese oxide 479 species; yields of 15 and 32% were obtained with commercial 480 activated MnO<sub>2</sub> and synthetic Ca<sub>2</sub>Mn<sub>3</sub>O<sub>8</sub> catalysts, respectively 481 (Table 4, entries 7 and 8). A comparison of these three 482 experiments shows that calcium enhances the reactivity of 483 manganese, suggesting a synergistic effect of mixed calcium- 484 manganese oxides toward epoxidation. These findings suggest 485 that the addition of calcium does not change the oxidation 486 potential of manganese, but might change the dispersion and/ 487 or exposition of manganese, enhancing its reactivity as 488 suggested by the works of Han et al. on mixed calcium- 489 manganese oxides.<sup>41</sup> 490

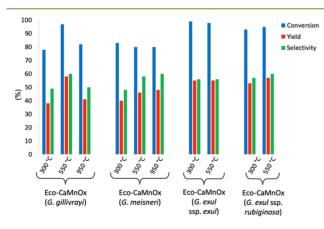
Table 4. Effect of the Catalyst Loading on the Epoxidation of  $\alpha$ -pinene<sup>a</sup>

|       |                            |          | Eco-CaMnOx (G. gill<br>NaHCO <sub>3</sub> (5<br>H <sub>2</sub> O <sub>2</sub> (30 wt%<br>H <sub>2</sub> O / Acc<br>a rt, 2 t | eq.)<br>, 5 eq.)       | 2a                             |     |                   |
|-------|----------------------------|----------|--|------------------------|--------------------------------|-----|-------------------|
| entry | catalyst                   | equiv Mn | conversion $(\%)^{b}$  | yield (%) <sup>b</sup> | selectivity (%) <sup>b,c</sup> | TON | $TOF^{g}(h^{-1})$ |
| 1     | Eco-CaMnO <sub>x</sub>     | 0        | 0  | 0                      | 0                              | 0   | 0                 |
| 2     | Eco-CaMnO <sub>x</sub>     | 0.001    | 89   | 49                     | 55                             | 490 | 245               |
| 3     | Eco-CaMnO <sub>x</sub>     | 0.0025   | 97   | 48                     | 49                             | 192 | 96                |
| 4     | Eco-CaMnO <sub>x</sub>     | 0.005    | 97   | 62                     | 64                             | 124 | 62                |
| 5     | Eco-CaMnO <sub>x</sub>     | 0.01     | 94   | 55                     | 59                             | 55  | 28                |
| 6     | Eco-CaMnO <sub>x</sub>     | 0.1      | 91   | 61                     | 67                             | 6   | 3                 |
| 7     | Ca2Mn3O8                   | 0.005    | 51   | 32                     | 63                             | 64  | 32                |
| 8     | activated MnO <sub>2</sub> | 0.005    | 55   | 15                     | 27                             | 30  | 15                |
| 9     | CaO                        | d        | 7 <sup>e</sup>   | 0                      | 0                              |     |                   |

<sup>*a*</sup>Reaction conditions: α-pinene (1.6 mmol, 1 equiv), the catalyst, NaHCO<sub>3</sub> (8 mmol, 5 equiv), H<sub>2</sub>O<sub>2</sub> (30 wt %; 8 mmol, 5 equiv), and H<sub>2</sub>O (20 mL): acetone (20 mL), rt, 2 h. <sup>*b*</sup>Conversion, yield, and selectivity were established by FID using biphenyl as the internal standard. <sup>*c*</sup>Selectivity was calculated as the ratio of yield over conversion. <sup>*d*</sup>0.02 equiv Ca was used, corresponding to the quantity of Ca engaged by 0.005 equiv Mn with Eco-CaMnO<sub>x</sub>. <sup>*e*</sup>Traces of verbenol, carveol, and campholenic aldehyde were detected by GC–MS. <sup>*f*</sup>TON = number of mol of the product formed per mol of catalyst. <sup>*g*</sup>TOF = number of mol of the product formed per mol of catalyst and per unit of time.

<sup>491</sup> Interestingly, Eco-CaMnO<sub>x</sub> catalysts gave a twice-higher <sup>492</sup> yield compared to synthetic  $Ca_2Mn_3O_8$  (Table 4, entries 4 and <sup>493</sup> 7). The enhanced reactivity of our catalyst might be due to a <sup>494</sup> different structural organization of manganese linked to its <sup>495</sup> vegetal footprint and/or due to the presence of traces of other <sup>496</sup> electroactive metal species.

Effect of the Plant Species and the Temperature of the the Thermal Treatment Used to Prepare Eco-CaMnO<sub>x</sub>. The different Eco-CaMnO<sub>x</sub> catalysts prepared from the four species soo of Grevillea were tested in the epoxidation of  $\alpha$ -pinene by so1 using the optimized reaction conditions. The influence of the so2 heating temperature during the thermal treatment of biomass so3 was also investigated (Figure 6). For each plant species, each so4 corresponding Eco-CaMnO<sub>x</sub> catalyst showed a potent catalytic so5 activity. These results guarantee that every manganeseso6 accumulating plant species used in rehabilitation could be so7 valorized afterward by this process.



**Figure 6.** Effect of the plant species and of the temperature of the thermal treatment used to prepare Eco-CaMnO<sub>x</sub> on the epoxidation of  $\alpha$ -pinene. Reaction conditions:  $\alpha$  -pinene (1.6 mmol, 1 equiv), catalyst (8 mmol, 0.005 equiv Mn), NaHCO<sub>3</sub> (8 mmol, 5 equiv), H<sub>2</sub>O<sub>2</sub> (30 wt %; 8 mmol, 5 equiv), and H<sub>2</sub>O (20 mL): acetone (20 mL), rt, 2 h. Conversion, yield, and selectivity were established by FID using biphenyl as internal standard. Selectivity was calculated as the ratio of yield over conversion.

Within a species, the temperature of the thermal treatment 508 did not seem to have much influence on the Eco-CaMnO<sub>x</sub> 509 activities. Surprisingly, no loss of activity was observed for the 510 eco-catalysts formed at 300 °C despite the residual organic 511 matter. The Eco-CaMnO<sub>x</sub> catalysts of *G. gillivrayi* and *G.* 512 *meisneri* prepared at 950 °C revealed similar activities as the 513 corresponding Eco-CaMnO<sub>x</sub> catalysts prepared at lower 514 temperatures (300 and 550 °C). The best catalyst in terms 515 of activity and energy required for its preparation remained the 516 one prepared at 550 °C.

The reaction conditions to perform the epoxidation of  $\alpha$ - 518 pinene were optimized to reach a good compromise of the 519 high efficiency of the reaction with sustainable and eco- 520 responsible use of chemical products and solvents. In these 521 conditions, almost total conversion was accessed with 65% 522 selectivity in pinene oxide. Longer reaction times were tested, 523 but it only resulted in a decrease in selectivity, the conversion 524 remaining total. This result was in accordance with the high 525 reactivity of pinene oxide and thus its conversion into isomeric 526 products.<sup>100,101</sup> 527

Our system can be advantageously compared to other 528 bicarbonate-activated peroxide systems based on Mn catalysts. 529 For instance, Lane et al. obtained 89% yield but only in the 530 presence of additives.<sup>82</sup> Qi et al. reached 40% selectivity using 531 Mn<sup>2+</sup>-exchanged zeolites.<sup>92</sup> 532

Substrate Scope for the Epoxidation of Terpenes and  $_{533}$ Lipids by Eco-CaMnO<sub>x</sub> Catalysts. The epoxidation of diverse  $_{534}$  terpenes and lipids was carried out to evaluate the scope of our  $_{535}$  process (Table 5).  $_{536 tes}$ 

High conversions and yields were obtained with a large 537 variety of terpenes, from cyclic to terminal substrates, which 538 confirmed the efficiency of the method. In some cases, a longer 539 reaction time was needed to reach higher conversions. 540

The chemoselectivity of Eco-CaMnO<sub>x</sub> catalysts was 541 illustrated through the selective epoxidation of terpenes 542 (Table 5, entries 2–8) bearing various functional groups, 543 such as alcohol, ester, or enone, that remained unmodified. 544 The epoxidation of monoterpenes like terpineol, isopulegol, 545 and citronellyl acetate (Table 4, entries 2, 3 and 5) gave total 546 conversion and selectivity. The epoxidation of (R)-(+)-limo- 547 nene, linalool, geranyl acetate,  $\alpha$ -ionone, and  $\beta$ -ionone gave 548

Table 5. Substrate Scope for the Epoxidation of Natural Substrates by Ecocatalysts (Eco-CaMnO<sub>x</sub><sup>*a*</sup>, Eco-Mn<sub>1</sub>,<sup>18</sup> and Pyr-Mn<sup>120</sup>)

|       |              | $\stackrel{R_1}{>} \stackrel{R_3}{=}$ | -CaMnOx ( <i>G. gillivrayi</i> 550 °C) (0.005<br>NaHCO <sub>3</sub> (5 eq.)<br>H <sub>2</sub> O <sub>2</sub> (30 wt%; 5 eq.) | 5 eq. Mn)            | $ \begin{array}{c}     R_1 & O \\     R_2 & R_3 \\     R_4 \end{array} $    |                             |                                    |
|-------|--------------|---------------------------------------|--|----------------------|---|-----------------------------|------------------------------------|
|       |              | Ř <sub>2</sub> Ř <sub>4</sub><br>1    | H <sub>2</sub> O / Acetone<br>RT   |                      | <b>2</b>  |                             |                                    |
| Entry | Substrate 1  | Ecocatalyst<br>solvent                | Product 2  | Reaction<br>time (h) | $\begin{array}{c} \textbf{Conversion}\\ \textbf{sion}\\ (\%)^b \end{array}$ | Yield $(\%)^b$              | Selectivity<br>(%) <sup>b, c</sup> |
|       |              | Eco-<br>CaMnOx                        |  |                      |   | <b>2b</b> <sub>1</sub> : 15 | <b>2b</b> ₁: 16                    |
|       |              | H,O/Acetone                           |  | 2                    | 93  | <b>2b</b> <sub>2</sub> : 78 | <b>2b</b> <sub>2</sub> : 84        |
|       | $\downarrow$ | $\operatorname{Eco-Mn}_{1}^{18,e}$    | $\succ$ $\succ$  |                      |   |                             |                                    |
| 1     |              | H,O/ DMF                              |  | 4                    | 50  | <b>2b</b> <sub>1</sub> : 43 | <b>2b</b> <sub>1</sub> : 86        |
|       | 1b           | $n_2 o/D m$                           | $2b_1 	 2b_2$  | 4                    | 50  | <b>2b</b> <sub>2</sub> : 7  | <b>2b</b> ₂: 14                    |
|       | 10           | Pyr-Mn <sup>108,f</sup>               |  |                      |   |                             |                                    |
|       |              | H <sub>2</sub> O/Acetone              | e  | 2                    | 99  | <b>2b</b> <sub>1</sub> : 1  | <b>2b</b> <sub>1</sub> : 1         |
|       |              |                                       |  |                      |   | <b>2b</b> <sub>2</sub> : 98 | <b>2b</b> <sub>2</sub> : 99        |
| 2     | ОН           | Eco-<br>CaMnOx                        | Сон  | 2                    | > 99  | > 99                        | 100                                |
|       | 1c           | H <sub>2</sub> O/Acetone              | 2c   |                      |   |                             |                                    |
| 3     | ОН           | Eco-<br>CaMnOx                        | ОН   | 4                    | > 99  | > 99                        | 100                                |
|       | 1d           | H <sub>2</sub> O/Acetone              | 2d   |                      |   |                             |                                    |
|       |              | Eco-                                  | OH HO HO   |                      |   | <b>2e</b> <sub>1</sub> : 64 | <b>2e</b> <sub>1</sub> : 64        |
|       | ОН           | CaMnOx                                |  | 4                    | > 99  | <b>2e</b> <sub>2</sub> : 34 | <b>2e</b> <sub>2</sub> : 34        |
| 4     |              | H <sub>2</sub> O/Acetone              | $2e_1 2e_2 2e_3$   |                      |   | <b>2e</b> <sub>3</sub> : 2  | <b>2e</b> <sub>3</sub> : 2         |
|       | 1e           | Eco-Mn <sub>1</sub> <sup>18,e</sup>   | HO O   |                      |   |                             |                                    |
|       |              | H <sub>2</sub> O/ DMF                 | 2e <sub>3</sub>  | 4                    | 65  | <b>2e</b> <sub>3</sub> : 63 | <b>2e</b> <sub>3</sub> : 97        |
|       |              | Pyr-Mn <sup>108,f</sup>               | ОН   | 2                    | × 00  | <b>1</b> 0 - 20             | <b>3</b> 99                        |
|       |              | H <sub>2</sub> O/Acetone              | // / <sup>\</sup> o <sup>\</sup> \<br>2e <sub>4</sub>  | 2                    | > 99  | <b>2e₄</b> : 89             | <b>2e₄</b> : 88                    |
| 5     | L of         | Eco-<br>CaMnOx                        | Jo l   | 4                    | 99  | 99                          | 100                                |
|       | 1f           | H <sub>2</sub> O/Acetone              | 2f   |                      |   |                             |                                    |

| Entry | Substrate 1  | Ecocatalyst<br>solvent   | Product 2   | Reaction<br>time (h) | Conver-<br>sion<br>(%) <sup>b</sup> | Yield $(\%)^{\flat}$                                       | Selectivity<br>(%) <sup>b,c</sup>                          |
|-------|--------------|--|---|----------------------|-------------------------------------|--|--|
| 6     | lg           | Eco-<br>CaMnOx<br>H <sub>2</sub> O/Acetone                           | $\begin{array}{c c} & & & & \\ & & & & \\ & & & \\ & & & \\ & & & & \\ & & & & \\ & & & \\ & & & \\ & & & \\ & & & \\ & & & \\ & & & \\ & & & \\ & & &$ | 4                    | > 99                                | <b>2g</b> <sub>1</sub> : 50<br><b>2g</b> <sub>2</sub> : 50 | <b>2g</b> <sub>1</sub> : 50<br><b>2g</b> <sub>2</sub> : 50 |
| 7     | کرے لُ<br>1h | Eco-<br>CaMnOx<br>H <sub>2</sub> O/Acetone                           | $ \begin{array}{c} \overbrace{}^{\bullet} \cdot \cdot$  | 4                    | 81                                  | <b>2h</b> ₁: 71<br><b>2h₂</b> : 10                         | <b>2h</b> ₁: 88<br><b>2h</b> ₂: 12                         |
| 8     | li           | Eco-<br>CaMnOx<br>H <sub>2</sub> O/Acetone                           | $2i_1$ $2i_2$   | 2                    | > 99                                | <b>2i</b> <sub>1</sub> : 70<br><b>2i</b> <sub>2</sub> : 30 | <b>2i</b> <sub>1</sub> : 70<br><b>2i</b> <sub>2</sub> : 30 |
|       |              | Eco-<br>CaMnOx <sup><math>d</math></sup><br>H <sub>2</sub> O/Acetone |   | 4                    | 66                                  | 66   | 100  |
| 9     |              | Eco- $Mn_1^{18,f}$<br>H <sub>2</sub> O/ DMF                          |   | 4                    | 0                                   | 0  | 0  |
|       | 1j           | Pyr-Mn <sup>108,<math>f</math></sup><br>H <sub>2</sub> O/Acetone     | 2j  | 2                    | 99                                  | 82   | 80   |

<sup>*a*</sup>Reaction conditions: substrate (1.6 mmol, 1 equiv), catalyst (8  $\mu$ mol, 0.005 equiv Mn), NaHCO<sub>3</sub> (8 mmol, 5 equiv), H<sub>2</sub>O<sub>2</sub> (30 wt %; 8 mmol, 5 equiv), and H<sub>2</sub>O (20 mL): acetone (20 mL), rt. <sup>*b*</sup>Conversion, yield, and selectivity were established by FID, using biphenyl as internal standard, and then confirmed by <sup>1</sup>H NMR from the isolated product. <sup>*c*</sup>Selectivity was calculated as the ratio of yield over conversion. <sup>*d*</sup>Catalyst: 0.5 equiv Mn. <sup>*c*</sup>Terpene (0.25 mmol, 1 equiv), supported catalyst (0.0031 equiv Mn), NaHCO<sub>3</sub> (0.05 mmol, 5 equiv), H<sub>2</sub>O<sub>2</sub> (30 wt %; 0.8 mmol, 3.2 equiv), and H<sub>2</sub>O/dimethylformamide (DMF) (2 mL), 0 °C, 4 h. <sup>*f*</sup>Terpene (0.18 mmol, 1 equiv), catalyst (0.00006 equiv Mn), NaHCO<sub>3</sub> (0.88 mmol, 5 equiv), H<sub>2</sub>O<sub>2</sub> (30 wt %; 1.75 mmol, 9.7 equiv), and H<sub>2</sub>O/acetone (2.6 mL), 30 °C, 2 h.

549 mono- (Table 5, entries 7 and 8) or diepoxides (Table 5, 550 entries 1, 4, and 6) when the double bonds were electron-rich. 551 In the case of limonene, 84% of selectivity of diepoxides was 552 observed with very high conversion in 2 h (Table 4, entry 1). 553 In comparison, Eco-Mn<sub>1</sub> led to 86% of monoepoxides, with 554 only 50% of conversion.<sup>18</sup> This result highlighted the high 555 reactivity of Eco-CaMnO<sub>x</sub>, which was close to Pyr-Mn. Both 556 mono- and diepoxides are of high interest in the field of 557 biosourced polymers as they both could be used as monomers 558 for the synthesis of polycarbonates, polyethers, polyesters, or 559 poly(hydro)urethanes.<sup>102-106</sup> Thus, they could represent 560 substitutes for polymers synthesized from bisphenol A or 561 epichlorhydrin, two toxic molecules classified as CMR.

<sup>562</sup> In 4 h, the epoxidation of geranyl acetate gave a <sup>563</sup> stoichiometric mixture of mono- and diepoxides (Table 5, <sup>564</sup> entry 6). In consequence, the ester moiety did not deactivate <sup>565</sup> Eco-CaMnO<sub>x</sub> in spite of its basic Lewis properties. The same <sup>566</sup> reaction with 10 equiv of  $H_2O_2$  favored the formation of the <sup>567</sup> diepoxide, reaching 79% of selectivity. It was thus possible to <sup>568</sup> control the ratio monoepoxides/diepoxides by tuning the <sup>569</sup> amount of  $H_2O_2$ .

570 Unlike Eco-Mn and conventional catalysts, the epoxidation 571 of linalool led mainly to the monoepoxide, with 64% of 572 selectivity (Table 5, entry 4). This result is unusual as the resulting epoxide is highly reactive and acid-sensitive. It easily 573 rearranges by cyclization into hydroxyfuranes or hydroxypyr- 574 anes.<sup>107</sup> In this case, only 2% of hydroxyfuranes was observed. 575 This indicated that our catalyst was not acidic, avoiding the 576 intramolecular reaction. However, the rearrangement of the 577 epoxide into the hydroxyfurane was easily observed when 578 CDCl<sub>3</sub> was used for NMR assessments. As an example, only 579 the hydroxyfurane was obtained with a 63% yield with the 580 previous Eco-Mn,<sup>18</sup> whereas Pyr-Mn yielded hydroxypyran.<sup>108</sup> 581 Therefore, Eco-CaMnO<sub>x</sub> allowed the preparation of very 582 sensitive epoxides. The higher chemoselectivity of Eco- 583  $CaMnO_x$  is the direct consequence of its preparation by a 584 sole thermal treatment. This result is of interest, as linalool 585 epoxide is an important molecule in the communication of 586 pollinating insects.<sup>109</sup> Thirty-four percent of diepoxides were 587 also obtained. This proved the strong oxidizing properties of 588 Eco-CaMnO<sub>x</sub> as it succeeded in epoxidizing a terminal double 589bond. 590

The monoepoxide was the only one identified with  $\alpha$ - and  $\beta$ - 591 ionones. The only other byproduct formed during the reaction 592 on both ionones was the product of allylic oxidation, with 12 593 and 30% of selectivity, respectively (Table 5, entries 7, 8). 594

The other particularly noteworthy example was the 595 epoxidation of oleic acid (Table 5, entry 9). Indeed, epoxides 596

#### Table 6. Recycling Studies of Eco-CaMnO<sub>x</sub> Catalysts

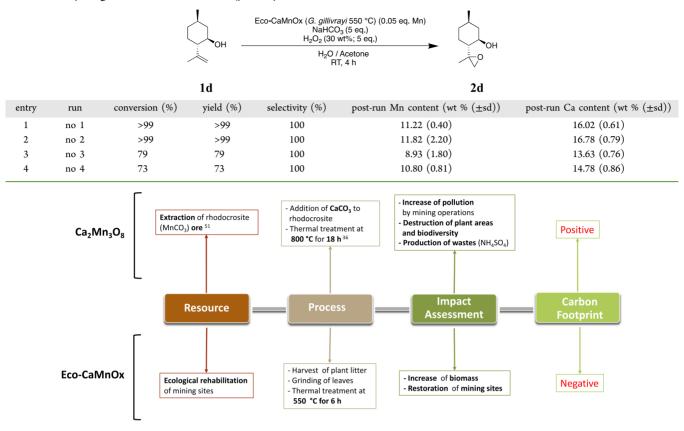


Figure 7. Qualitative environmental impact assessment of the catalyst preparation.

<sup>597</sup> of fatty acids from vegetal oils are very interesting as platform <sup>598</sup> molecules for organic chemistry, but also as biodegradable <sup>599</sup> lubricants, plasticizers, and stabilizers of polymers.<sup>110–112</sup> <sup>600</sup> Sixty-six percent of conversion with a total selectivity in <sup>601</sup> epoxide was reached in 4 h with Eco-CaMnO<sub>x</sub> (0.5 equiv Mn), <sup>602</sup> while Eco-Mn was not able to catalyze this reaction. Pyr-Mn <sup>603</sup> seemed more efficient than Eco-CaMnO<sub>x</sub> but required twice as <sup>604</sup> much H<sub>2</sub>O<sub>2</sub>.

In addition to the higher reactivity of  $\text{Eco-CaMnO}_x$ 606 compared to Eco-Mn, the experimental conditions were also 607 improved; epoxidations were conducted with acetone/H<sub>2</sub>O 608 instead of DMF. In a context of growing environmental 609 consciousness, it is motivating to be able to propose novel 610 catalysts, which combine efficiency, use of renewable resources, 611 and eco-friendly processes.

Recycling and Leaching Studies of Eco-CaMnO<sub>x</sub> Cata-612 613 lysts. Recycling of Eco-CaMnO<sub>x</sub> catalysts was investigated by conducting the epoxidation of isopulegol (Table 6). Eco-614 615 CaMnO<sub>x</sub> catalysts were recycled by separation after 616 centrifugation of the crude, washing, drying, and reuse for an 617 identical experiment. Up to four successive reactions were 618 conducted. Conversion and yield remained quantitative for the second run (Table 6, entries 1, 2), while a slight decrease was 619 observed after the third run (Table 6, entries 3, 4), suggesting a 620 small loss of activity of Eco-CaMnO<sub>x</sub> catalysts. 621

The small loss of activity was investigated by analyzing the composition and structure of Eco-CaMnO<sub>x</sub> catalysts after each caterial run. No significant change of Mn and Ca contents was cobserved by MP-AES (Table S2), and the structure characterized by XRPD remained the same. Both results indicated the high stability of  $\text{Eco-CaMnO}_x$  catalysts, even in 627 the oxidizing conditions of the reaction.

Considering that the composition and structure of Eco- 629 CaMnO<sub>x</sub> remained similar after four runs, leaching of Eco- 630 CaMnO<sub>x</sub> was unlikely to occur but was still verified. Using 631 isopulegol as substrate, a specific experiment was conducted as 632 described by Sheldon et al.<sup>113</sup> After 30 min of reaction, Eco- 633 CaMnO<sub>x</sub> was removed from the reaction mixture by filtration; 634 conversion of isopulegol was analyzed after this time at 35%. 635 The reaction mixture was stirred for another 4 h without Eco- 636 CaMnO<sub>x</sub>; conversion of isopulegol remained at 35%, 637 indicating that the reaction did not occur after removing 638 Eco-CaMnO<sub>x</sub>. As expected, the elemental composition of the 639 reaction mixture was analyzed by MP-AES and no trace of 640 metal was detected. These two results showed that the Eco- 641 CaMnO<sub>x</sub> catalyst was a heterogeneous catalyst, in which 642 leaching of Mn can be excluded in the reported conditions. 643

#### CONCLUSIONS

644

In this study, a new generation of ecocatalysts was easily 645 prepared from Mn-accumulating plant species, which are used 646 in ecological restoration. A controlled thermal treatment of 647 Mn-rich biomass led directly to green oxidative catalysts, Eco- 648 CaMnO<sub>x</sub>, thus avoiding any further chemical activation. 649 Characterization by MP-AES, XRPD, HRTEM, and STEM- 650 EDX revealed an original polymetallic system. Unusual mixed 651 manganese–calcium oxides, Ca<sub>2</sub>Mn<sub>3</sub>O<sub>8</sub> and CaMnO<sub>3</sub>, were 652 identified. All Eco-CaMnO<sub>x</sub> catalysts prepared from different 653 plant species demonstrated an excellent catalytic potential in 654 the epoxidation of terpenes and lipids, with only 0.005 equiv 655

656 Mn, in short reaction times, at room temperature, using green 657 solvents and without any ligand or activation phase. Eco-658 CaMnO<sub>x</sub> catalysts afforded much higher conversions and 659 yields than conventional activated manganese dioxide or 660 synthetic Ca<sub>2</sub>Mn<sub>3</sub>O<sub>8</sub>. Not only did these results demonstrate 661 the vegetal footprint of  $Eco-CaMnO_x$  catalysts but also they 662 proved that these catalysts could represent potential substitutes 663 to oxidative reagents inconsistent with the requirements of 664 REACH regulation. A wide range of mono- and diepoxides 665 were efficiently synthesized from terpenes, many of them 666 coming from abundant natural resources. Eco-CaMnO<sub>x</sub> opens 667 a new perspective for the valorization of Mn-rich biomass 668 through the preparation of biosourced monomers for new-669 biodegradable polymers.<sup>105,106,114</sup> This new generation of 670 ecocatalysts exhibits environmental and scientific benefits, 671 suggesting a promising life-cycle analysis (Figure 7). It can 672 drive a new approach of green chemistry with ecological, 673 economic, and social advantages.

#### 674 ASSOCIATED CONTENT

#### 675 **Supporting Information**

676 The Supporting Information is available free of charge at 677 https://pubs.acs.org/doi/10.1021/acssuschemeng.9b05444.

678 General methods for the characterization of Eco-679 CaMnO<sub>x</sub> and the analysis of the reaction products, 680 MP-AES analyses of Mn-accumulating plant leaves and 681 Eco-CaMnO<sub>x</sub>, NMR analyses, scale-up of the epox-682 idation of alkene, the study of the leaching of Eco-683 CaMnO<sub>x</sub>, recycling of Eco-CaMnO<sub>x</sub> (PDF)

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#### 707 Notes

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