



HAL
open science

Pickering emulsions of fluorinated TiO₂: a new route for intensification of photocatalytic degradation of nitrobenzene

Nidhal Fessi, Mohamed Faouzi Nsib, Yves Chevalier, C. Guillard, Frederic Dappozze, Ammar Houas, Leonardo Palmisano, Francesco Parrino

► To cite this version:

Nidhal Fessi, Mohamed Faouzi Nsib, Yves Chevalier, C. Guillard, Frederic Dappozze, et al.. Pickering emulsions of fluorinated TiO₂: a new route for intensification of photocatalytic degradation of nitrobenzene. *Langmuir*, 2020, 36 (45), pp.13545-13554. 10.1021/acs.langmuir.0c02285 . hal-03023907

HAL Id: hal-03023907

<https://hal.science/hal-03023907>

Submitted on 30 Nov 2020

HAL is a multi-disciplinary open access archive for the deposit and dissemination of scientific research documents, whether they are published or not. The documents may come from teaching and research institutions in France or abroad, or from public or private research centers.

L'archive ouverte pluridisciplinaire **HAL**, est destinée au dépôt et à la diffusion de documents scientifiques de niveau recherche, publiés ou non, émanant des établissements d'enseignement et de recherche français ou étrangers, des laboratoires publics ou privés.

Pickering emulsions of fluorinated TiO₂: a new route for intensification of photocatalytic degradation of nitrobenzene

Nidhal Fessi,^{†,‡} Mohamed Faouzi Nsib,^{†,§} Yves Chevalier,^{*,‡} Chantal Guillard,^{||} Frédéric Dappozze,^{||} Ammar Houas,[†] Leonardo Palmisano,[⊥] and Francesco Parrino^{*,#}

[†] Laboratoire de Recherche Catalyse et Matériaux pour l'Environnement et les Procédés LRCMEP (UR11ES85), Faculté des Sciences de Gabès, University of Gabès, Campus Universitaire, Cité Erriadh, 6072 Gabès, Tunisia.

[‡] University of Lyon, Laboratoire d'Automatique et de Génie des Procédés (LAGEPP), UMR 5007 CNRS, University Claude Bernard Lyon 1, 43 bd 11 Novembre, 69622 Villeurbanne, France.

[§] Higher School of Sciences and Technology, University of Sousse, rue Tahar Ben Achour, 4003 Sousse, Tunisia.

^{||} University of Lyon, Institut de Recherches sur la Catalyse et l'Environnement de Lyon (IRCELYON), UMR 5256 CNRS, Université Claude Bernard Lyon 1, 2 av Albert Einstein, 69626 Villeurbanne, France.

[⊥] Dipartimento di Ingegneria, University of Palermo, viale delle Scienze Ed. 6, 90128 Palermo, Italy.

[#] Department of Industrial Engineering, University of Trento, via Sommarive 9, 38123 Trento, Italy.

Corresponding authors: Francesco Parrino / Yves Chevalier
e-mail: francesco.parrino@unitn.it / yves.chevalier@univ-lyon1.fr

Abstract

Fluorination of the TiO₂ surface has been often reported as a tool to increase the photocatalytic efficiency, due to the beneficial effects in terms of production of oxidizing radicals. Moreover, it is shown that the unique amphiphilic properties of the fluorinated TiO₂ (TiO₂-F) surface allow to use this material as stabilizer for the formulation of Pickering emulsions of poorly soluble pollutants such as nitrobenzene (NB) in water. The emulsions have been characterized in terms of size of the droplets, type of emulsion, possibility of phase inversion, contact angle measurements and optical microscopy. The emulsified system presents micrometer-sized droplets of pollutant surrounded by the TiO₂-F photocatalyst. Consequently, the system can be considered as composed by microreactors for the degradation of the pollutant, which maximize the contact area between the photocatalyst and the substrate. The enhanced photocatalytic activity of TiO₂-F was confirmed in the present paper, as the apparent rate constants of NB photodegradation were 16×10^{-3} and $12 \times 10^{-3} \text{ min}^{-1}$ for fluorinated and bare TiO₂, respectively. At NB concentrations largely exceeding its solubility, the rate constant was $0.04 \times 10^{-3} \text{ min}^{-1}$ in the presence of both TiO₂ and TiO₂-F. However, unlike TiO₂, TiO₂-F stabilized NB/water emulsions and, under these conditions, the efficiency of NB photocatalytic degradation in the emulsified system was ca. 18 times higher than in the non-emulsified one. This result is relevant also in terms of practical applications because it opens the route to one-pot treatments of biphasic polluted streams without the need of preliminary physical separation treatments.

Keywords: Fluorinated TiO₂, Pickering emulsions, Photocatalysis, Nitrobenzene.

Introduction

Nitrobenzene (NB) is a toxic and bio-persistent aromatic compound.¹ It affects the central nervous and cardiovascular systems, is suspected to be carcinogenic², and poses serious concerns for its effects in the environment³⁻⁶. However, NB is implemented in many industrial processes for the production of perfumes, resins, dyes, explosives and pesticides⁷⁻⁹. Therefore, it is often present not only in industrial wastewater streams, but also in surface and ground water¹⁰ because its high chemical stability and its low water solubility lead to its accumulation in the environment. Conventional purification and decontamination relies on physical treatments such as separation techniques^{11,12}. These methods are generally expensive, poorly efficient, and afford only removal of the pollutants without chemical degradation.

Photocatalysis is a promising advanced oxidation process that has been often proposed for water remediation applications, as it allows oxidizing almost all harmful organic species. Upon absorption of light of suitable energy, reactive oxygen species (ROS) possessing high oxidizing ability are generated. The transfer of the photocatalytic process from the laboratory to real applications is a current concern that deserves a great deal of research efforts. The photodegradation of poorly water soluble substrates faces some problems whose solution still requires basic research. In these cases, polluted water cannot be directly used as in most photocatalytic applications¹³ because of the low concentration of the dissolved substrate and its low affinity with the generally hydrophilic surface of the photocatalyst. These factors negatively affect the quantum efficiency of the process and consequently its economic feasibility. The use of different solvents has been proposed to overcome these problems in cases where photocatalysis was used for organic synthesis purposes¹⁴. For instance, the degradation of polycyclic aromatic hydrocarbons (PAH's) has been recently carried out in the green solvent dimethyl carbonate in the presence of a minimum amount of water necessary to induce the formation of oxidizing radical species. Such shift of solvent is better restricted to the synthesis of compounds with high added value. Using solvents other than water for environmental remediation faces hard problems of costs and management, especially in view of large scale applications.

A different approach consists in the formation of emulsions of the hydrophobic pollutant dispersed in water in which the photocatalyst can also act as a stabilizer of the emulsion. In this way, the preliminary physical separation of the pollutant can be by-passed and the degradation reaction can take place inside microreactor-like droplets of the substrate surrounded (and stabilized) by the photocatalyst itself. This configuration is beneficial in terms of photocatalytic

activity as it creates larger contact area between the catalyst and the pollutant, optimizes the availability of the active sites, and offers all of the advantages of working in micrometer-sized reactors¹⁵.

The organic pollutant plays the role of the “oil” in the emulsion. The emulsion can be obtained by applying external energy either in the form of mechanical stirring or sonication. When the emulsion is stabilized by solid nanoparticles located at the oil-water interface, a “Pickering emulsion”¹⁶ is obtained.

Pickering emulsions can be of the oil-in-water (o/w), water-in-oil (w/o), or even multiple types^{17–19}. They possess the basic properties of classical emulsions stabilized by soluble surfactants (emulsifiers)²⁰. However, the stabilization produced by solid particles confers specific properties. The high resistance to coalescence is the main benefit^{21–23}. Furthermore, Pickering emulsions are stable in a wide range of experimental conditions; in particular, they are not very affected by temperature variations, changes of the composition of the oil phase, and the pH of the aqueous phase²⁴. This makes them useful in pharmaceutical^{25,26}, cosmetic²⁷ and food industry^{28,29}. In 2010, the pioneering work by Crossley et al.³⁰ paved the way for catalytic reactions in Pickering emulsions^{31–38}. However, only few examples of photocatalytic reactions carried out in Pickering emulsions have been reported^{39–41}. As far as we know, fluorinated TiO₂ has never been proposed for that purpose, while it is instead widely studied as a photocatalyst because of its higher photoactivity than pure TiO₂. Its high photoactivity has been mainly attributed to (i) the presence of a defective surface which increases the lifetime of the photogenerated charges⁴², (ii) the greater production of highly oxidizing hydroxyl radicals due to the better availability of photogenerated holes⁴³, and (iii) the possible production of singlet oxygen⁴⁴.

Otherwise, the wettability by oils and water and the dynamics of water molecules on the fluorinated TiO₂ surface have been poorly studied. It has been proposed, for example, that fluorination gives rise to an increase in the Lewis acidic strength of Ti⁴⁺ surface sites, which retain adsorbed water molecules⁴⁵, thereby increasing the hydrophilic character of the surface. Similar conclusions have also been reached by other authors⁴⁶. UV irradiation increases the polarity of the surface⁴⁷. However, Mino et al.⁴⁸ recently revealed the complexity of the topic by showing evidence of different behaviors of the various exposed crystalline facets and the different contributions of bulk and surface doping. Interestingly, this study disclosed that the presence of terminal fluoride groups on the {001} facet of TiO₂ decreased of ca. two times the hydrophilicity of the material. Therefore, the physical chemistry of fluorinated TiO₂ in

Pickering emulsions is not trivial from a scientific point of view due to the complex interactions of its surface with water and oils⁴⁹.

We recently reported on the changes induced by surface fluorination on the morphological, structural, surface, and electronic features of TiO₂⁵⁰. While surface fluorination does not affect the bulk structural properties and the morphology of TiO₂ nanoparticles, it induces significant changes in terms of surface and electronic properties. In particular, the surface charge turns more negative upon fluorination, and supplementary intra-band-gap energy states located up to 1.3 eV above the valence band are generated by the local interaction of chemisorbed fluorine atoms with the semiconducting structure of TiO₂. The correlation between the opto-electronic features and the photocatalytic activity has been discussed⁵⁰. The unique surface properties of fluorinated TiO₂ deserve further investigations and can be exploited for specific applications. For instance, their influence on the selectivity of the industrially relevant photocatalytic synthesis of high added-value compounds has recently been demonstrated⁵¹.

This paper reports the influence of surface fluorination of a nanostructured sol-gel derived TiO₂ material on the stability of nitrobenzene/water emulsions and on the consequent efficiency of the photocatalytic degradation of nitrobenzene under UV irradiation. Notably, the possibility to treat in one pot biphasic polluted streams, without the need of costly physical separation processes upstream, is of practical relevance.

Experimental

Preparation of the photocatalysts

TiO₂ nanoparticles were synthesized by using a facile sol-gel technique. 19 mL of titanium tetraisopropoxide (Ti[OCH(CH₃)₂]₄, 97 %, Alfa Aesar) were added to 4 mL of methanol (MeOH, 99.9 %, Aldrich) and the obtained solution sonicated in an ultrasonic bath (Elma, T460/H, 35 kHz and 170 W). The hydrolysis process was then performed by adding dropwise 74 mL of deionized water under reflux and magnetic stirring. The obtained white gel was filtered and washed several times using ethanol and deionized water. The resulting powder was dried at 100 °C for 18 h in order to evaporate water and the volatile organic compounds. Finally, the powder, labelled simply as TiO₂, was calcined in a muffle furnace at 400 °C for 4 h. Fluorination of TiO₂ was carried out by dispersing 1 g of the synthesized TiO₂ nanoparticles into 50 mL of 4 % sodium fluoride (NaF, p.a. Aldrich) aqueous solution at pH 3.2 (obtained by addition of HNO₃) and stirring the suspension at room temperature for 48 h. The nanoparticles

were separated by centrifugation, washed several times with HNO₃ aqueous solutions at pH 3.2, and finally dried at 80 °C for 2 h. The resulting powder was labelled as TiO₂-F.

The amount of fluorine in samples was determined by means of ion chromatography after digestion dissolution of the TiO₂ material by fusion with potassium hydrogen sulfate and extraction of the melt with dilute sulfuric acid⁵². Collected samples were then analyzed for F⁻ anions using ion chromatography (930 Compact IC Flex, Metrohm, Switzerland) equipped with a chemical suppressor and conductivity detection. Elution solvent was 8 mmol·L⁻¹ sodium carbonate (Fisher Scientific, Illkirch, France) in ultrapure water. Metrosep A Supp 5 250/4.0 column with an adequate pre-column at a temperature of 35 °C was used. Calibration curve was linear in the range from 0.06 to 2000 μmol·kg⁻¹ ($R^2 = 0.999$).

Preparation of Pickering emulsions and characterization

Nitrobenzene NB (C₆H₅NO₂, 95% Aldrich, solubility in water 0.19 wt% at 20 °C) constituted the oil phase of the Pickering emulsions. In the beginning, aqueous dispersions of 1 wt% TiO₂ or TiO₂-F were obtained by means of an UltraTurrax T25 rotor-stator device equipped with a S25N18G shaft (IKA, Germany) rotating at 22000 rpm for 5 min in order to de-aggregate the particles. Thereafter, NB (up to 20 vol%) was added to the aqueous dispersion and stirred during 5 min with an UltraTurrax T25 under the same conditions. The size distribution of the TiO₂ nanoparticles was determined by dynamic light scattering using a Zetasizer NanoZS instrument (Malvern, UK).

Emulsions droplets were observed by optical microscopy using a Leica DMLM (Germany) microscope equipped with a video camera. The concentrated emulsions were diluted and spread between glass plate and cover slip for microscopic observation in transmission mode and image analysis. The size distribution was determined using the analysis image software AnalySISTM. Droplets size measurements of o/w emulsions were carried out at small-angle light scattering using a Mastersizer 3000 instrument (Malvern, UK). The refractive indexes of the optical model used for data processing were 1.332 for water and 1.552 for NB.

The electrical conductivity of emulsions was measured with a Radiometer CDM 210 conductivity meter at 25°C.

Contact angles of NB/photocatalyst/water were measured by the sessile drop method on the flat photocatalyst surface using Drop Shape Analysis System DSA10Mk2 (Krüss, Germany). A pellet of the photocatalyst was pressed under 7 kPa pressure. A drop of NB (volume 5–6 μL)

was deposited on the surface of the pellet immersed in water with a syringe needle and the drop picture was recorded with a CCD camera.

Photocatalytic experiments

The photocatalytic experiments were carried out in a cylindrical Pyrex batch photoreactor (diameter: 10 cm) equipped with a mechanical stirrer rotating at 500 rpm. 160 mL of emulsion containing 0.1 vol% of NB and 1 wt% of catalyst were illuminated by a PLL lamp UVA ($8 \text{ mW}\cdot\text{cm}^{-2}$) placed horizontally below the photoreactor. The lateral walls were covered with aluminum foil. Cooling water circulated in a thimble surrounding the reactor in order to maintain the temperature at ambient value. Samples were withdrawn at fixed time intervals, mixed with 50 vol% of a solution acetonitrile/water (50/50) in order to break the emulsion trapped by solid particles, and filtered (Millipore PTFE $0.45 \mu\text{m}$) before analysis.

Notably, the amount of catalyst chosen for the photodegradation tests was selected from a compromise between issues related to photocatalysis and to the stability of the emulsion. The amount of photocatalyst allowed to neglect the backscattering which would be relevant only for small values of the optical thickness⁵³. Nevertheless, as the system was not optimized with respect to the radiant field distribution, no information on the intrinsic reaction kinetics could be retrieved. Therefore, the apparent kinetic constants reported throughout the text are intended to provide only a numerical comparison between degradation kinetics obtained under the same experimental conditions.

The time evolution of the photocatalytic degradation of NB emulsion was followed by using a HPLC system model 1290 Infinity. This apparatus was equipped with a binary pump (Agilent Technologies, G4220B), an autosampler (Agilent Technologies, 1290 Sampler), a Photodiode Array (PDA) Detector (Agilent Technologies, 1260) and a C18 NUCLEOSIL 100-5 column (Machery Nagel: $4.6\times 250 \text{ mm}$). The injected sample volume was $20 \mu\text{L}$. The eluent circulating at a flow rate of $1 \text{ mL}\cdot\text{min}^{-1}$ consisted of ultrapure water (40 %) and acetonitrile (60 %). The resulting data were collected by using Agilent Mass Hunter software.

Results and discussion

Emulsification experiments

The formulation process of Pickering emulsions requires a precise control of the intervening parameters in order to effectively tailor type, stability and droplets size. Preliminary

experiments aimed to show the feasibility of the formulation of nitrobenzene/water (NB/W) emulsions with pristine TiO_2 and $\text{TiO}_2\text{-F}$ as the stabilizers.

Figure 1 (A and B) presents NB/W emulsions obtained in the presence of pristine TiO_2 and $\text{TiO}_2\text{-F}$, respectively. In both cases, the phase containing NB sedimented, leaving a supernatant aqueous phase due to the higher density of NB ($1.2 \text{ g}\cdot\text{mL}^{-1}$) with respect to water.

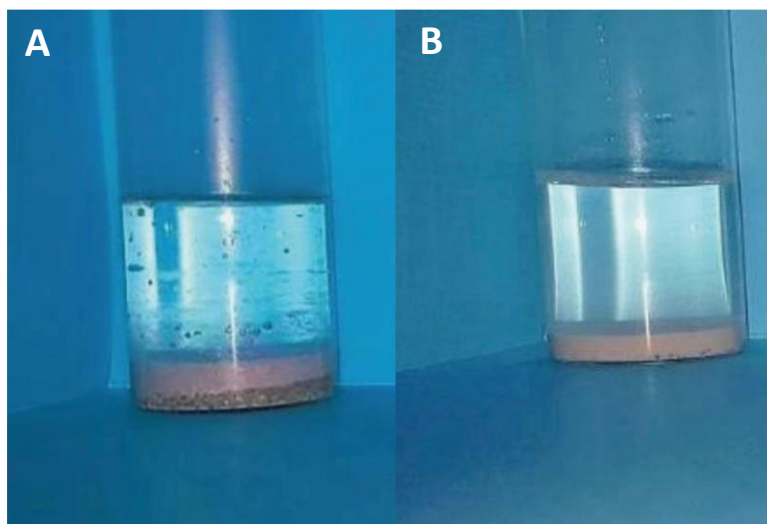


Figure 1. NB (20 vol%)/water Pickering emulsions stabilized by 1 wt% of pristine TiO_2 (A) and $\text{TiO}_2\text{-F}$ (B). Both pictures taken after 24 h storage at rest show a clear aqueous supernatant because all materials denser than water underwent sedimentation. Part A shows a sediment of solid particles of TiO_2 that are not adsorbed at the NB/water interface topped by a layer of mixed pure NB and coarse emulsion. Part B shows a sediment of Pickering emulsion and no free $\text{TiO}_2\text{-F}$ particles.

When pristine TiO_2 was used as the emulsifier (Figure 1A) fast sedimentation of TiO_2 particles took place and a release of NB was observed. Therefore, pristine TiO_2 nanoparticles were unable to stabilize the NB/W emulsions. In fact, the hydrophobic NB molecules show low tendency to adsorb onto the hydroxylated and highly hydrophilic TiO_2 surface. Conversely, $\text{TiO}_2\text{-F}$ could stabilize NB/W emulsions quite efficiently under the same conditions (Figure 1B). The droplets size was ca. $128 \mu\text{m}$ and no release of pure NB was observed during at least 2 months (Figure 2). The NB droplets undergo sedimentation quite fast because of the density of NB higher than water and quite large droplet size. The mean diameter of the NB droplets, however, did not change during storage, demonstrating that coalescence did not occur.

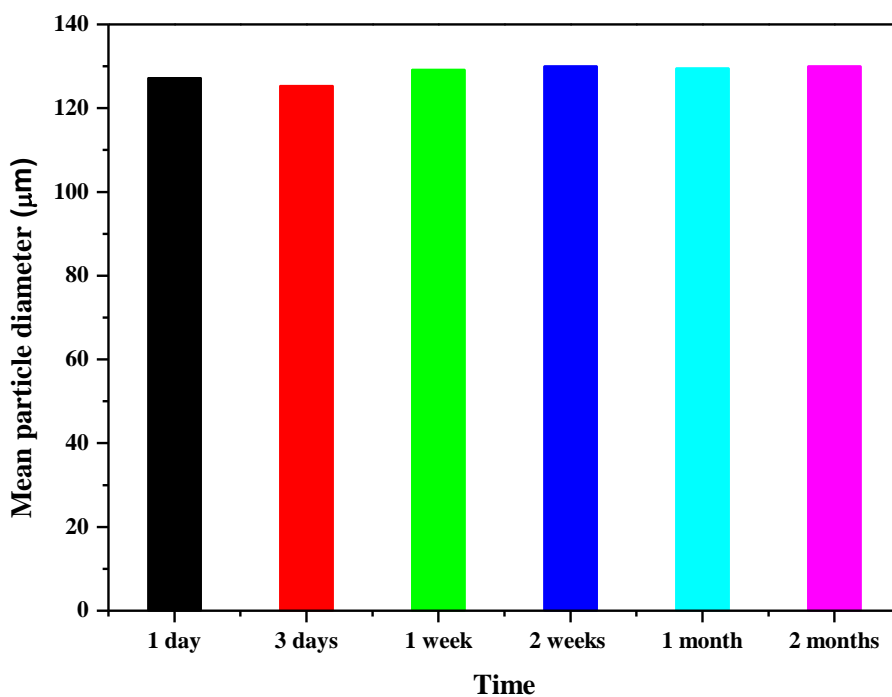


Figure 2. Mean droplets size of NB (20 vol%) in Pickering emulsions stabilized by 1 wt% of TiO₂-F nanoparticles as a function of time. T = 25°C. Each measurement was repeated 3 times and the standard deviation was lower than ± 4%.

These results were confirmed by the optical microscopy images shown in Figure 3 where it is evident that NB droplets of ca. 130 µm size are nicely dispersed in a continuous water phase.

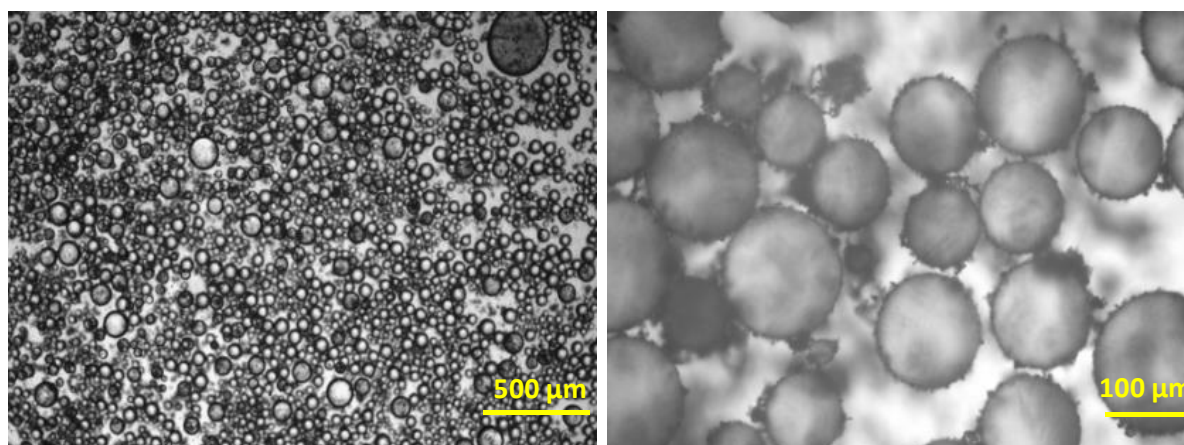
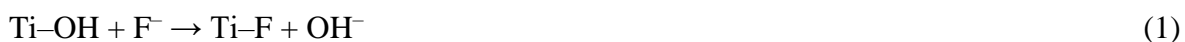


Figure 3. Optical microscopy images of NB (20 vol%) in water emulsions stabilized by TiO₂-F (1 wt%).

The different behavior of the TiO₂-F sample with respect to the pristine TiO₂ material can be explained by its surface properties. The fluorinated material was prepared by a simple ligand exchange of surface hydroxyl groups with F⁻ ions^{54,55}, as expressed by Equation 1.



Equation 1 does not express a simple adsorption equilibrium of F⁻ ions because fluoride modification is stable upon washing during the preparation procedure and the reverse process, a nucleophilic substitution by hydroxide ions, requires high NaOH concentrations (ca. 1 M) and does not reach completion⁵⁶.

The surface density of F⁻ ions on the surface of TiO₂ has been determined by means of ion chromatography. By considering that the specific surface area of the TiO₂ sample is 103 m²·g⁻¹ and its average hydroxylation degree ranges between 4.8 and 6.1 Ti-OH·nm⁻²⁵⁷, a maximum fluorine grafting was achieved at pH = 3.2. The fluorine surface density was 3 fluorinated surface sites per nm², corresponding to 50–60 % of the total surface sites⁵⁰. Therefore, the surface of the fluorinated TiO₂ presents two functionalities almost equally distributed, which endow it with amphiphilic features.

Contact angle measurements

The stabilization of Pickering emulsions requires that partial wetting condition of the solid particles by water and NB are fulfilled. The wettability of the photocatalyst was assessed by means of contact angle measurements. The classical technique of contact angle measurement consists in the optical observation of a small drop of oil deposited onto the solid surface immersed in water (or of a drop of water deposited on the surface immersed in oil) and in the determination of the contact angle in water on the picture. Furthermore, this technique affords information on the type and stability of Pickering emulsions^{58,59}. In particular, contact angles close to 90° provide the most efficient stabilization of Pickering emulsions. Contact angles lower than 90° are indicative of hydrophilic particles that can better stabilize oil in water emulsions, while particles with contact angles higher than 90° better stabilize water in oil emulsions.

It was not possible to calculate the contact angle of NB over pristine TiO₂ because the drop of NB floated and rolled at the surface of the solid. This indicated total wetting by water and the absence of any interaction between TiO₂ and NB. This result explains why it was not possible to stabilize Pickering emulsions containing NB by using pristine TiO₂ as the emulsifier. On the contrary, the measurement was possible on TiO₂-F sample as shown in Figure 4.

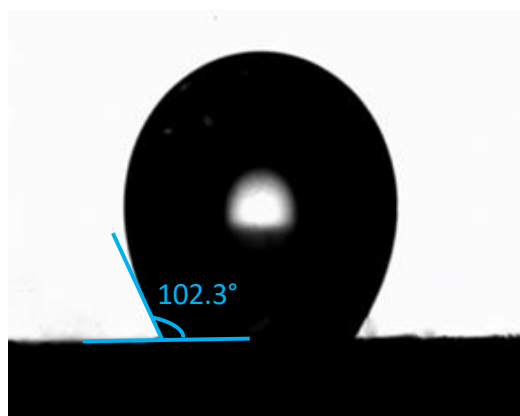


Figure 4. Drop of NB on the TiO₂-F surface immersed in water. T = 25°C.

A drop of NB on TiO₂-F immersed in water presents a contact angle of $102.3 \pm 0.6^\circ$. This indicates partial wettability and lower hydrophilicity of the TiO₂-F surface with respect to the pristine TiO₂. Such contact angle close to 90° allows the stabilization of either O/W or W/O Pickering emulsions by TiO₂-F particles, depending on the relative amounts of oil and water⁶⁰. Hence, NB/water emulsions should be obtained when the NB content is smaller than that of water.

Characterization of the emulsion

Two crucial features of the emulsion have been investigated: the size of the droplets and the type of emulsion as a function of the amount of the solid nanoparticles (TiO₂-F) and of the volume fraction of the oil phase (Φ_{NB}).

The type of emulsion has been identified by varying the volume fraction of NB (Figure 5A). Conductivity measurements performed on emulsions with different volume fractions of the oil phase gave evidence of a phase inversion phenomenon from O/W type (NB droplets in water, high conductivity) to W/O type (water droplets in NB, low conductivity) when Φ_{NB} exceeded ca. 50 vol%. Notably, the possibility to switch between two emulsion types is a significant advantage of the present system with respect to analogous systems stabilized by surfactants, therefore, it is possible to stabilize with the same type of particles both direct and inverse emulsions.

The droplet size is a relevant parameter characterizing the ability of adsorbed particles to stabilize the emulsion. The stability of Pickering emulsions is governed by the reduction of the free energy of the system caused by the transfer of the photocatalyst from the aqueous dispersion to the NB/W interface. This transfer produces a variation in the size of the droplets

and the consequent increase of the interfacial area. Therefore, the droplets size mainly depends on the amount of stabilizer ($\text{TiO}_2\text{-F}$). Figure 5B shows the changes of the mean diameter of the droplets at different contents of $\text{TiO}_2\text{-F}$ while keeping constant the amount of NB (20 vol%). At low concentration of $\text{TiO}_2\text{-F}$ (less than 0.5 wt%) emulsions were not stable and coalesced immediately after the emulsification procedure. Conversely, the stability of Pickering emulsions increased for $\text{TiO}_2\text{-F}$ loadings higher than 0.5 wt%. By increasing the content of $\text{TiO}_2\text{-F}$ nanoparticles, the droplets size decreased until it reached a “plateau”, where further increasing the $\text{TiO}_2\text{-F}$ content did not result in size reduction. Indeed, $\text{TiO}_2\text{-F}$ concentrations above 4 wt% produced almost a constant NB droplets size (mean value $57.5 \mu\text{m}$). This can be explained by a lack of efficiency of the emulsification process because the UltraTurrax disperser was unable to reduce the NB droplets size down to the sizes that would have been expected by extrapolation of the curve in the first regime. As a consequence, $\text{TiO}_2\text{-F}$ nanoparticles were in excess once the plateau region was reached.

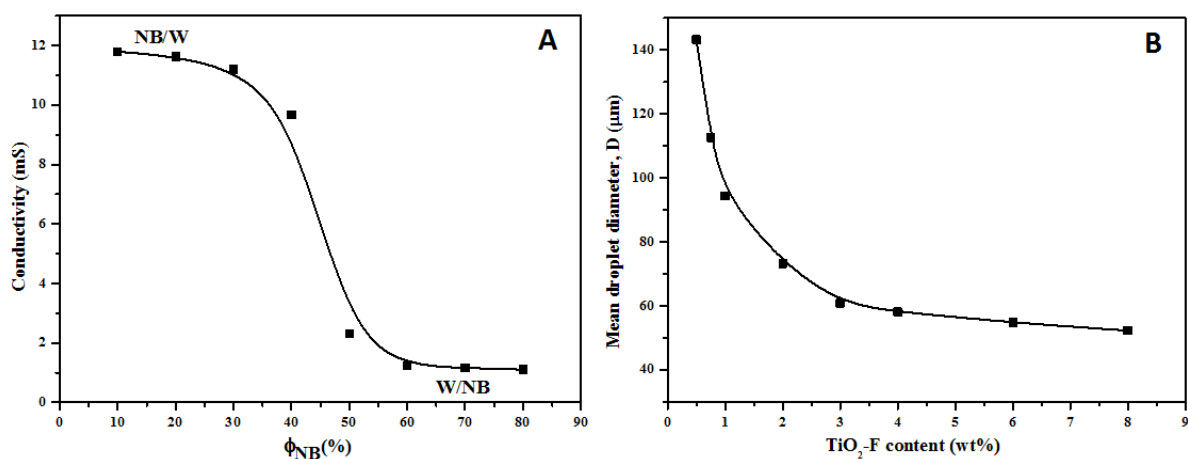


Figure 5. (A) Phase inversion of emulsions of NB in water stabilized by $\text{TiO}_2\text{-F}$ (1 wt%) nanoparticles. (B) Mean NB droplet diameter of NB (20 vol%)/water emulsions as a function of $\text{TiO}_2\text{-F}$ content. $T = 25^\circ\text{C}$.

In the plateau region, the Pickering emulsion is comprised of micrometer sized NB droplets surrounded by $\text{TiO}_2\text{-F}$ which dually acts as stabilizer and, once irradiated, as photocatalyst. Therefore, the stabilized droplets can be seen as microreactors in which the photocatalytic reaction rate can be maximized due to the reduced mass transfer limitations and to the enhanced contact area between the substrate and the photocatalyst.

Photocatalytic activity

The photocatalytic experiments were performed using NB/water/TiO₂-F Pickering emulsions containing 0.1 vol% of NB (1200 ppm). Figure 6 shows the mean size distribution of the NB droplets along with an optical microscopy image (inset) of the emulsion.

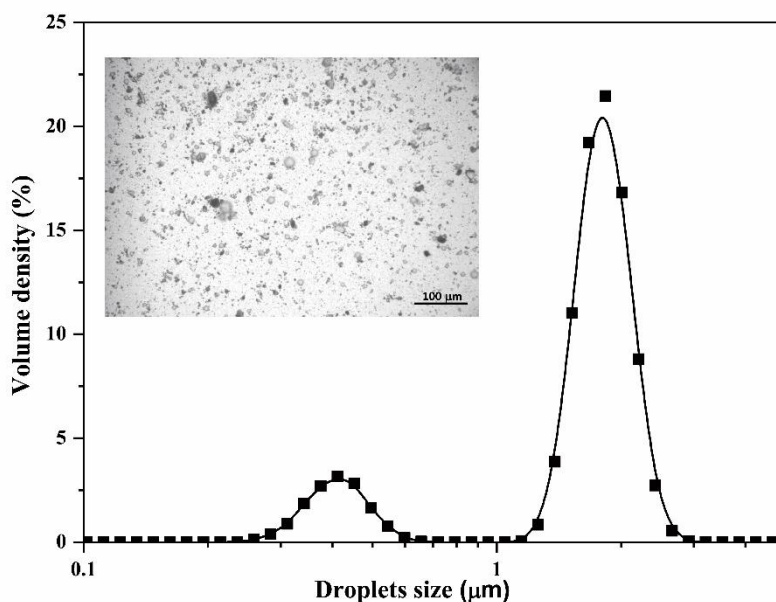


Figure 6. Mean size distribution of the NB droplets. Inset: optical microscopy image of the emulsion ([NB] 0.1 vol%, TiO₂-F amount: 1 wt%). T = 25°C.

A stable Pickering emulsion with small NB droplets nicely dispersed in water is evident. Most of the droplets have diameter ranging between 1.5 and 3 μm while a smaller fraction presents diameters ranging between 0.3 and 0.6 μm. This smaller fraction corresponds to the amount of TiO₂-F in excess that was not adsorbed on the surface of the NB droplets.

The presence of fluorine dually acts in improving the photocatalytic system. In fact, it enhances the photocatalytic activity with respect to pristine TiO₂, and stabilizes the emulsion favoring formation of micrometer-sized droplets.

The superior photocatalytic activity of the fluorinated TiO₂ has been tested by choosing an initial NB concentration which could dissolve in water, i.e. 50 ppm, and performing its photodegradation in the presence of TiO₂ and TiO₂-F. Results are reported in Figure 7.

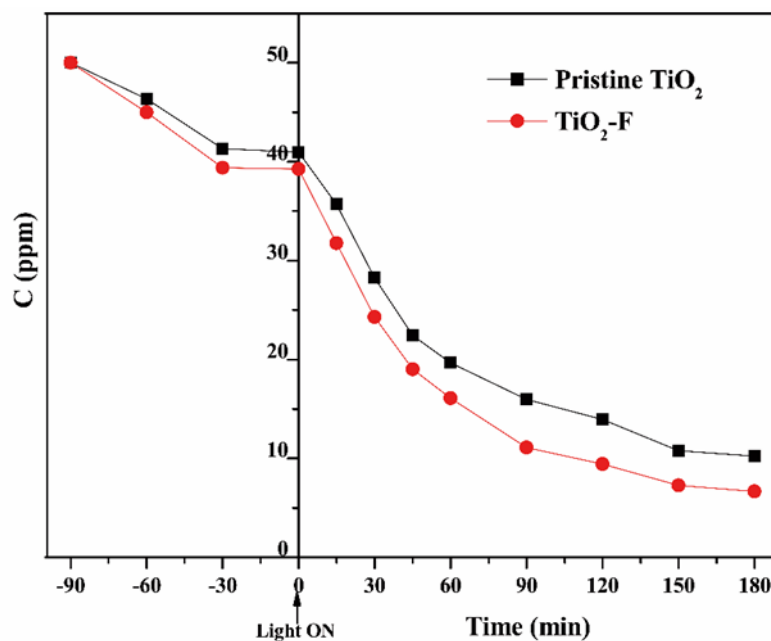


Figure 7. Photodegradation of NB aqueous solutions over pristine TiO₂ and TiO₂-F under UV irradiation. Initial concentration of NB was 50 ppm. The sample was in the dark at negative times before the UV light was switched on. T = 25°C.

The NB photodegradation is faster in the presence of the fluorinated sample. In particular, the apparent observed kinetic constants, determined by differentiating the experimental data at the initial time, by using a five points formula for equally spaced points^{61,62}, were 16×10^{-3} and $12 \times 10^{-3} \text{ min}^{-1}$, for the fluorinated and the bare sample, respectively. This evidence, often reported in literature, has been generally related to the higher availability of photogenerated holes which eventually results in higher production of hydroxyl radicals⁴³. Other authors attributed the enhanced activity to the presence of singlet oxygen generated through a prevailing energy transfer mechanism⁴⁴. Moreover, the intra band gap energy states within 1.3 eV above the valence band, whose existence has been theoretically predicted^{63,64} and only recently experimentally demonstrated⁵⁰, could also be beneficial, acting as traps enhancing the life time of the photogenerated holes.

However, by taking into account the above reported surface features, the affinity of the photocatalyst surface with the organic substrate may also play a significant role. In fact, TiO₂ surface fluorination decreases its hydrophilicity favoring then adsorption of NB and then its direct oxidation through the photogenerated holes.

In order to provide evidence of the contribution of the emulsification process on the photocatalytic activity, the photodegradation of NB has been carried out in emulsified and non-

emulsified NB/water mixtures in the presence of TiO₂-F. The results of the runs are illustrated in Figure 8 in terms of normalized concentration (NB concentration at time t / initial NB concentration × 100). For the sake of comparison, an experiment in the absence of the photocatalyst is also reported.

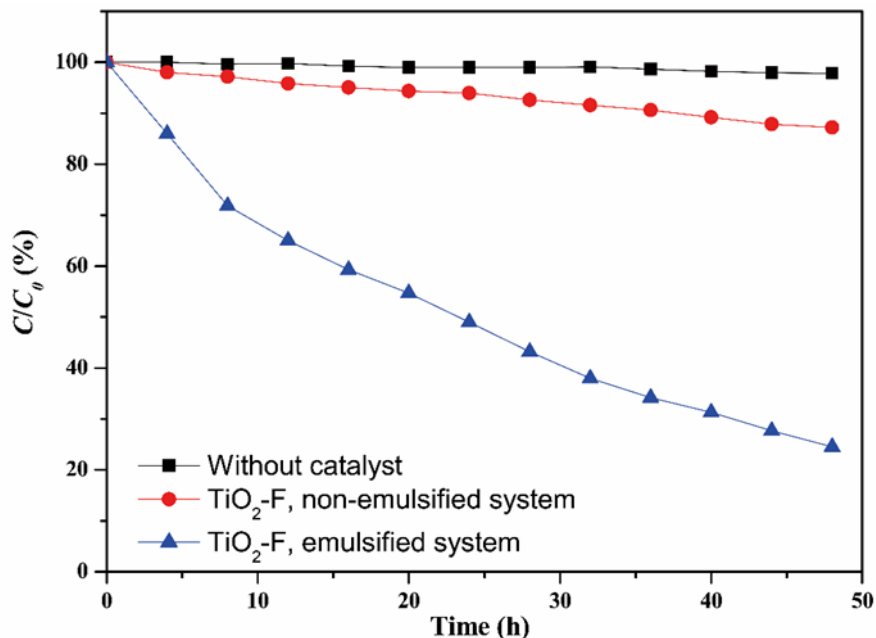


Figure 8. Normalized NB concentration (C/C_0) during irradiation time in the absence of photocatalyst (black squares), in the presence of TiO₂-F but without emulsification (red circles), and in the presence of TiO₂-F after emulsification (blue triangles). Photocatalyst amount: 1 wt %; initial NB concentration: 0.1 vol% (1200 ppm). T = 25°C.

NB concentration always decreased in the presence of TiO₂-F photocatalyst under UV irradiation. However, only 13 % of the initial NB concentration was photodegraded after 48 h in the case of the non-emulsified NB/W system. The photocatalytic degradation was significantly higher in the emulsified systems reaching 75 % after the same reaction time. The apparent rate constants, determined as above, were 0.7×10^{-3} and $0.04 \times 10^{-3} \text{ min}^{-1}$ for the emulsified and non-emulsified TiO₂-F system, respectively. In other words, the emulsified system showed an initial NB degradation rate ca. 18 times greater than that retrieved for the non-emulsified system.

By comparing the results reported in Figures 7 and 8 it is evident that the stabilizing effect of TiO₂-F plays a predominant role in determining the global efficiency with respect to the intrinsic higher efficiency of the fluorinated sample. In fact, the amphiphilic properties of the

fluorinated surface give rise to adsorption equilibrium of the two phases, thus increasing the dispersive capacity of the TiO₂-F nanoparticles and thermodynamically favoring formation of micrometer sized NB droplets. The resulting high contact surface area between the photocatalyst and the substrate improves the photocatalytic activity. Indeed, by considering the photoreactor volume $V = 160$ mL, the volume fraction of NB $\Phi_{NB} = 0.1$ vol% and the NB droplet size $D = 2$ μm , the total NB-water interfacial area in the emulsified system is 0.48 m² as calculated by Equation 2.

$$A = \frac{6V\Phi_{NB}}{D} = 0.48 \text{ m}^2 \quad (2)$$

Contrarily, in the non-emulsified system the photocatalyst nanoparticles are mainly located at the planar interface between the two liquid phases (ca. 8×10^{-3} m²).

Notably, by considering that only half of the surface hydroxyl groups are substituted by fluorine, adsorption of water still takes place contributing to the photocatalytic reaction in various ways. Photogenerated holes induce water oxidation and produce hydroxyl radicals which can in turn oxidize NB. Moreover, water may compete for adsorption with oxygenated degradation products, thus avoiding poisoning the photocatalyst. It is worth mentioning that, even if the apparent rate constant of TiO₂-F in emulsion (0.7×10^{-3} min⁻¹) is much smaller than that in solution (16×10^{-3} min⁻¹), in the first case it was possible to treat 1200 ppm NB, while only 50 ppm could be treated in solution. At this high NB concentration, the “classical” non-emulsified TiO₂-F system is virtually not active (0.04×10^{-3} min⁻¹). Therefore, the size distribution of the droplets is a critical parameter both for the photocatalytic activity and for the stability of the emulsion. The remarkable efficiency enhancement observed in the emulsified system allows to treat in one pot high amounts of insoluble pollutants without implementing physical separation methods which, in any case, require costly chemical degradation downstream.

The oxidation by products of the photocatalytic oxidation of NB dissolved in TiO₂ aqueous suspensions have been already reported in the relevant literature as mainly deriving from NB hydroxylation induced by hydroxyl radicals photocatalytically generated^{3,6,65}. Accordingly, in the present investigation, 4-nitrophenol (4-NP) and 3-nitrophenol (3-NP) were the main intermediates after 180 min irradiation time for the NB degradation tests shown in Figure 7. Figure 9 reports the correspondent chromatograms and the UV-vis spectra of the intermediates for the run carried out in the presence of TiO₂-F.

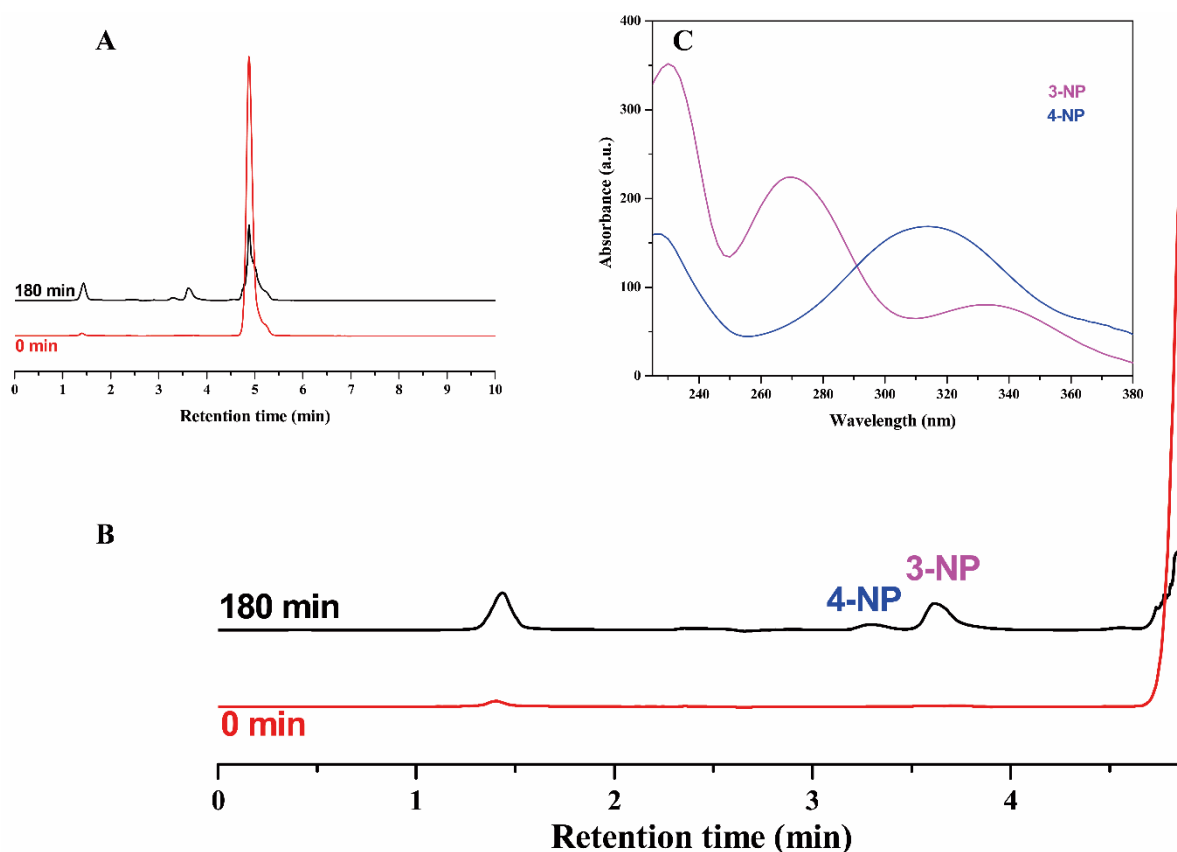


Figure 9. Panel A shows the chromatograms of samples collected at the start and after 180 min irradiation time for the NB degradation test in the presence of $\text{TiO}_2\text{-F}$, shown in Figure 7 (initial NB concentration: 50 ppm). Panel B shows a zoom of the chromatograms highlighting the two oxidation by-products identified as 4-nitrophenol (4-NP) and 3-nitrophenol (3-NP), whose UV-vis spectra are shown in Panel C. The peak at 1.4 min marks the dead volume of the column.

The intermediates were the same also in the presence of TiO_2 (data not shown) indicating, as expected, that in both cases the hydroxyl radical attack triggers NB degradation. Notably, 3-NP is the most abundant intermediate according to the activating, meta orienting nature of the nitro substituent.

Performing the reaction in NB/W emulsion (as in the runs shown in Figure 8) did not significantly affect the degradation mechanism. Figure 10 shows the intermediates identified after 48 h irradiation in the $\text{TiO}_2\text{-F}$ stabilized emulsion, along with their UV-vis spectra.

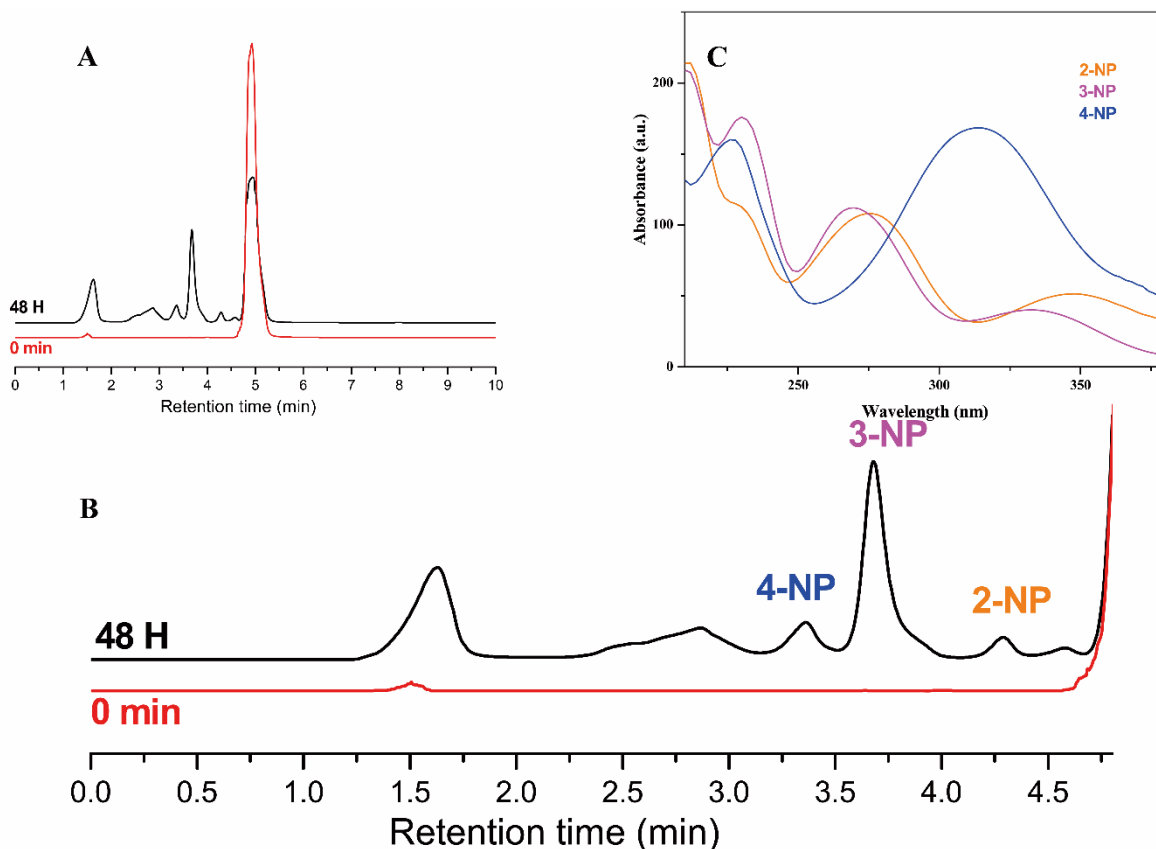


Figure 10. Panel A shows the chromatograms of samples collected at the start and after 48 h irradiation time for the NB degradation test in NB/W emulsion in the presence of $\text{TiO}_2\text{-F}$, shown in Figure 8 (initial NB concentration: 1200 ppm). Panel B shows a zoom of the chromatograms highlighting the three oxidation by-products identified as 4-nitrophenol (4-NP), 3-nitrophenol (3-NP), and 2-nitrophenol (2-NP), whose UV-vis spectra are shown in Panel C. The peak at 1.5 min marks the dead volume of the column.

Small amounts of 2-NP have been detected along with the 4-NP and 3-NP isomers, being the latter the most abundant as above mentioned. A small and broad peak is detectable between 2.25 and 3.25 minutes which could not be identified due to the low intensity and the probable overlapping of signals related to different species. However, it is plausible to ascribe this signal to di-hydroxylated compounds such as nitrocatechol or nitroresorcinol, which are more hydrophilic compounds than the nitrophenol isomers, and consequently have lower retention time. This is also in agreement with Bhatkhande et al.⁶, which also detected these intermediates in smaller amounts with respect to the monohydroxylated products.

Conclusions

The present paper reports the possibility of exploiting the unique amphiphilic properties of the fluorinated surface of TiO₂ to stabilize Pickering emulsions of organic pollutants poorly soluble in water. The obtained system is comprised of small droplets of substrate surrounded by the photocatalyst that act as microreactors for the degradation of the pollutant. This configuration allows obtaining 18 times faster photodegradation with respect to the non-emulsified system. The characterization of the physicochemical properties of the emulsion shows an inversion of the type of emulsion (from oil in water to water in oil) obtained by changing the amount of organic phase in the system. Moreover, it is highlighted the stabilizing ability of the fluorinated TiO₂ nanoparticles due to their amphiphilic surface. Therefore, the role of fluorination is dual. On one hand, fluorination affects both the electronic and the surface properties of TiO₂, and enhances the photocatalytic activity due to the higher production of hydroxyl radicals. On the other hand, the peculiar surface features allow to stabilize NB emulsions which was not possible by using bare TiO₂. The present results shine some light on the hydrophilicity of the fluorinated surface of TiO₂ and open the route for one-pot treatments of biphasic polluted streams without the need of preliminary physical separation.

References

- (1) Zhang, T.; Ma, J. Catalytic Ozonation of Trace Nitrobenzene in Water with Synthetic Goethite. *J. Mol. Catal. A Chem.* **2008**, 279, 82–89.
- (2) Robin C. G.; Nitrobenzene. *Encyclopedia of Toxicology (Second Edition)*, **2005**, 236–238.
- (3) Palmisano, G.; Loddo, V.; Augugliaro, V.; Palmisano, L.; Yurdakal, S. Photocatalytic Oxidation of Nitrobenzene and Phenylamine: Pathways and Kinetics, *AIChE J.* **2007**, 53, 961–968.
- (4) Majumder, P.S.; Gupta, S.K. Hybrid Reactor for Priority Pollutant Nitrobenzene Removal. *Water Res.* **2003**, 37, 4331–4336.
- (5) Jo, W.-K.; Won, Y.; Hwang, I.; Tayade, R.J. Enhanced Photocatalytic Degradation of Aqueous Nitrobenzene Using Graphitic Carbon–TiO₂ Composites, *Ind. Eng. Chem. Res.* **2014**, 53, 3455–3461.
- (6) Bhatkhande, D.S.; Pangarkara, V.G.; Beenackers, A.A.C.M. Photocatalytic Degradation of Nitrobenzene Using Titanium Dioxide and Concentrated Solar Radiation: Chemical Effects and Scale up, *Water Res.* **2003**, 37, 1223–1230.

- (7) Latifoglu, A.; Gurol, M.D.; The Effect of Humic Acids on Nitrobenzene Oxidation by Ozonation and O₃/UV Processes, *Water Res.* **2003**, *37*, 1879–1889.
- (8) Tada, H.; Ishida, T.; Takao, A.; Ito, S. Drastic Enhancement of TiO₂-Photocatalyzed Reduction of Nitrobenzene by Loading Ag Clusters, *Langmuir* **2004**, *20*, 7898–7900.
- (9) Zhao, L.; Ma, J.; Sun, Z.Z. Oxidation Products and Pathway of Ceramic Honeycomb-Catalyzed Ozonation for the Degradation of Nitrobenzene in Aqueous Solution, *Appl. Catal. B: Environ.* **2008**, *79*, 244–253.
- (10) Zhang, S.J.; Jiang, H.; Li, M.J.; Yu, H.Q.; Yin, H.; Li, Q.R. Kinetics and Mechanisms of Radiolytic Degradation of Nitrobenzene in Aqueous Solutions, *Environ. Sci. Technol.* **2007**, *41*, 1977–1982.
- (11) International Maritime Organization (IMO), 2008 revised guidelines for systems for handling oily wastes in machinery spaces of ships incorporating guidance notes for an integrated bilgewater treatment system, **2008**.
- (12) Cataldo, S.; Ianni, A.; Loddo, V.; Mirenda, E.; Palmisano, L.; Parrino, F.; Piazzese, D. Combination of advanced oxidation processes and active carbons adsorption for the treatment of simulated saline wastewater, *Sep. Purif. Technol.* **2016**, *171*, 101–111.
- (13) Parrino, F.; Camera-Roda, G.; Loddo, V.; Augugliaro, V.; Palmisano, L. Maximization of the Reaction Rate and Control of Undesired By-Products, *Applied Catalysis B: Environ.* **2015**, *178*, 37–43.
- (14) Bellardita, M.; Loddo, V.; Mele, A.; Panzeri, W.; Parrino, F.; Pibiri I.; Palmisano, L. Photocatalysis in Dimethyl Carbonate Green Solvent: Degradation and Partial Oxidation of Phenanthrene on Supported TiO₂, *RSC Adv.* **2014**, *77*, 40859–40864.
- (15) Cambié, D.; Bottecchia, C.; Straathof, N. J. W.; Hessel V.; Noël, T. Applications of Continuous-Flow Photochemistry in Organic Synthesis, Material Science, and Water Treatment, *Chem. Rev.* **2016**, *116*, 10276–10341.
- (16) Pickering, S.U. Emulsions, *J. Chem. Soc.* **1907**, *91*, 2001–2021.
- (17) Aveyard, R.; Binks, B.P.; Clint, J.H.; Emulsions Stabilized Solely by Solid Colloidal Particles, *Adv. Colloid Interface Sci.* **2003**, *100–102*, 503–546.
- (18) Binks, B.P. Particles as Surfactants—Similarities and Differences, *Curr. Opin. Colloid Interface Sci.* **2002**, *7*, 21–41.
- (19) Binks, B.P.; Horozov, T.S. Colloidal Particles at Liquid Interfaces, Cambridge University Press, **2006**.
- (20) Chevalier, Y.; Bolzinger, M.-A. Emulsions Stabilized with Solid Nanoparticles: Pickering Emulsions, *Colloids Surf. A: Physicochem. Eng. Asp.* **2013**, *439*, 23–34.

- (21) Menon, V.B.; Wasan, D.T. Coalescence of Water-in-Shale Oil Emulsions, *Sep. Sci. Technol.* **1984**, 19, 555–574.
- (22) Eley, D.D.; Hey, M.J.; Lee, M.A. Rheological Studies of Asphaltene Films Adsorbed at the Oil/Water Interface, *Colloids Surf.* **1987**, 24, 173–182.
- (23) Eley, D.D.; Hey, M.J.; Symonds, J.D. Emulsions of Water in Asphaltene-Containing Oils. 1. Droplet Size Distribution and Emulsification, *Colloids Surf.* **1988**, 32, 87–101.
- (24) Yang, F.; Shang, L.; Jian, X.; Qiang, L.; Wei, F.; Sun, D. Pickering Emulsions Stabilized Solely by Layered Double Hydroxides Particles: The Effect of Salt on Emulsion Formation and Stability, *J. Colloid Interface Sci.* **2006**, 302, 59–169.
- (25) Marku, D.; Wahlgren, M.; Rayner, M.; Sjö, M.; Timgren, A. Characterization of Starch Pickering Emulsions for Potential Applications in Topical Formulations, *Int. J. Pharm.* **2012**, 428, 1–7.
- (26) Chen, H.; Zhu, H.; Hu, J.; Zhao, Y.; Wang, Q.; Wan, J.; Yang, Y.; Xu, H.; Yang, X. Highly Compressed Assembly of Deformable Nanogels into Nanoscale Suprastructures and Their Application in Nanomedicine, *ACS Nano* **2011**, 5, 2671–2680.
- (27) Frelichowska, J.; Bolzinger, M.-A.; Pelletier, J.; Valour, J.-P.; Chevalier, Y. Topical Delivery of Lipophilic Drugs from o/w Pickering Emulsions, *Int. J. Pharm.* **2009**, 371, 56–63.
- (28) Dickinson, E. Food Emulsions and Foams: Stabilization by Particles, *Curr. Opin. Colloid Interface Sci.* **2010**, 15, 40–49.
- (29) Rayner, M.; Timgren, A.; Sjö, M.; Dejmeek, P. Quinoa Starch Granules: A Candidate for Stabilising Food-Grade Pickering Emulsions, *J. Sci. Food Agric.* **2012**, 92, 1841–1847.
- (30) Crossley, S.; Faria, J.; Shen, M.; Resasco, D.E. Solid Nanoparticles that Catalyze Biofuel Upgrade Reactions at the Water/Oil Interface, *Science* **2010**, 327, 68–72.
- (31) Leclercq, L.; Mouret, A.; Proust, A.; Schmitt, V.; Bauduin, P.; Aubry, J.-M.; Nardello-Rataj, V. Pickering Emulsion Stabilized by Catalytic Polyoxometalate Nanoparticles: A New Effective Medium for Oxidation Reactions, *Chem. Eur. J.* **2012**, 18, 14352–14358.
- (32) Holdich, R.G.; Ipek, I.Y.; Lazrigh, M.; Shama, G. Production and Evaluation of Floating Photocatalytic Composite Particles Formed Using Pickering Emulsions and Membrane Emulsification, *Ind. Eng. Chem. Res.* **2012**, 51, 12509–12516.
- (33) Yang, H.; Fu, L.; Wei, L.; Liang, J.; Binks, B.P. Compartmentalization of Incompatible Reagents within Pickering Emulsion Droplets for One-pot Cascade Reactions, *J. Am. Chem. Soc.* **2015**, 137, 1362–1371.

- (34) Leclercq, L.; Mouret, A.; Renaudineau, S.; Schmitt, V.; Proust, A.; Nardello-Rataj, V. Self-assembled Polyoxometalates Nanoparticles as Pickering Emulsion Stabilizers, *J. Phys. Chem. B* **2015**, 119, 6326–6337.
- (35) Chen, Z.; Zhao, C.; Ju, E.; Ji, H.; Ren, J.; Binks, B.P.; Qu, X. Design of Surface-active Artificial Enzyme Particles to Stabilize Pickering emulsions for High-performance Biphasic Biocatalysis, *Adv. Mater.* **2016**, 28, 1682–1688.
- (36) Yang, B.; Leclercq, L.; Clacens, J.-M.; Nardello-Rataj, V. Acidic/amphiphilic Silica Nanoparticles: New Eco-friendly Pickering Interfacial Catalysis for Biodiesel Production, *Green Chem.* **2017**, 19, 4552–4562.
- (37) Cakmak, F.P.; Keating, C.D. Combining Catalytic Microparticles with Droplets Formed by Phase Coexistence: Adsorption and Activity of Natural Clays at the Aqueous/aqueous Interface, *Sci. Rep.* **2017**, 7, 3215.
- (38) Pera-Titus, M.; Leclercq, L.; Clacens, J.-M.; De Campo, F.; Nardello-Rataj, V. Pickering Interfacial Catalysis for Biphasic Systems: From Emulsion Design to Green Reactions, *Angew. Chem. Int. Ed.* **2015**, 54, 2006–2021.
- (39) Fessi, N.; Nsib, M.F.; Chevalier, Y.; Guillard, C.; Dapozze, F.; Houas, A.; Palmisano, L.; Parrino, F. Photocatalytic Degradation Enhancement in Pickering Emulsions Stabilized by Solid Particles of Bare TiO₂, *Langmuir* **2019**, 35, 2129–2136.
- (40) Nawaz, M.; Miran, W.; Jang, J.; Lee, S. Stabilization of Pickering Emulsion with Surface-modified Titanium Dioxide for Enhanced Photocatalytic Degradation of Direct Red 80, *Catalysis Today* **2017**, 282, 38–47.
- (41) Nsib, M. F.; Moussa, N.; Houas A.; Chevalier Y. TiO₂ Modified by Salicylic Acid as a Photocatalyst for the Degradation of Monochlorobenzene via Pickering Emulsion way, *J. Photochem. Photobiol. A: Chem.* **2013**, 251, 10–17.
- (42) Dozzi, M.V.; D'Andrea, C.; Ohtani, B.; Valentini, G.; Selli, E. Fluorine-Doped TiO₂ Materials: Photocatalytic Activity vs Time-Resolved Photoluminescence, *J. Phys. Chem. C* **2013**, 117, 25586–25595.
- (43) Mrowetz M.; Selli, E. Enhanced Photocatalytic Formation of Hydroxyl Radicals on Fluorinated TiO₂, *Phys. Chem. Chem. Phys.* **2005**, 7, 1100–1102.
- (44) Jańczyk, A.; Krakowska, E.; Stochel, G.; Macyk, W. Singlet Oxygen Photogeneration at Surface Modified Titanium Dioxide, *J. Am. Chem. Soc.* **2006**, 128, 15574–15575.
- (45) Minella, M.; Faga, M.G.; Maurino, V.; Minero, C.; Pelizzetti, E.; Coluccia S.; Martra, G. Effect of Fluorination on the Surface Properties of Titania P25 Powder: An FTIR Study, *Langmuir* **2010**, 26, 2521–2527.

- (46) Barsukov, D.V.; Saprykin, A.V.; Subbotina, I.R.; Usachev, N.Y. Beneficial Effect of TiO₂ Surface Fluorination on the Complete Photooxidation of Ethanol Vapor, *Mendeleev Commun.* **2017**, *27*, 248–250.
- (47) Tang, J.; Quan H.; Ye, J. Photocatalytic Properties and Photoinduced Hydrophilicity of Surface-Fluorinated TiO₂, *Chem. Mater.* **2007**, *19*, 116–122.
- (48) Mino, L.; Pellegrino, F.; Rades, S.; Radnik, J.; Hodoroaba, V.D.; Spoto, G.; Maurino, V.; Martra, G. Beyond Shape Engineering of TiO₂ Nanoparticles: Post-Synthesis Treatment Dependence of Surface Hydration, Hydroxylation, Lewis Acidity and Photocatalytic Activity of TiO₂ Anatase Nanoparticles with Dominant {001} or {101} Facets, *ACS Appl. Nano Mater.* **2018**, *1*, 5355–5365.
- (49) Parrino, F.; Conte, P.; De Pasquale, C.; Laudicina, V.A.; Loddo, V.; Palmisano, L. Influence of Adsorbed Water on the Activation Energy of Model Photocatalytic Reactions, *J. Phys. Chem. C* **2017**, *121*, 2258–2267.
- (50) Fessi, N.; Nsib, M.F.; Cardenas, L.; Guillard, C.; Dappozze, F.; Houas, A.; Parrino, F.; Palmisano, L.; Ledoux, G.; Amans, D.; Chevalier, Y. Surface and Electronic Features of Fluorinated TiO₂ and Their Influence on the Photocatalytic Degradation of 1-Methylnaphthalene, *J. Phys. Chem. C* **2020**, *124*, 11456–11468.
- (51) Khelifi, H.; Parisi, F.; Elsellami, L.; Camera-Roda, G.; Palmisano, L.; Ceccato, R.; Parrino, F. Photocatalytic Partial Oxidation of Tyrosol: Improving the Selectivity Towards Hydroxytyrosol by Surface Fluorination of TiO₂, *Top. Catal.* **2020**, DOI: 10.1007/s11244-020-01287-y.
- (52) Norris, J.D., Determination of Titanium in Titanium Dioxide Pigments, Paints and Other Materials by Chromium(II) Chloride Reduction and Automatic Potentiometric Titration, *Analyst* **1984**, *109*, 1475–1482.
- (53) Camera-Roda, G.; Augugliaro, V.; Cardillo, A.; Loddo, V.; Palmisano, L.; Parrino, F.; Santarelli, F. A Reaction Engineering Approach to Kinetic Analysis of Photocatalytic Reactions in Slurry Systems, *Catal. Today* **2016**, *259*, 87–96.
- (54) Chen, Y.; Chen F.; Zhang, J. Effect of Surface Fluorination on the Photocatalytic and Photo-induced Hydrophilic Properties of Porous TiO₂ Films, *Appl. Surface Sci.* **2009**, *255*, 6290–6296.
- (55) Park J.S.; Choi, W. Enhanced Remote Photocatalytic Oxidation on Surface-Fluorinated TiO₂, *Langmuir* **2004**, *20*, 11523–11527.

- (56) Wang, Q.; Chen, C.; Zhao, D.; Ma, W.; Zhao, J. Change of Adsorption Modes of Dyes on Fluorinated TiO₂ and Its Effect on Photocatalytic Degradation of Dyes under Visible Irradiation. *Langmuir* **2008**, *24*, 7338–7345.
- (57) Mueller, R.; Kammler, H.K.; Wegner, K.; Pratsinis, S.E. OH Surface Density of SiO₂ and TiO₂ by Thermogravimetric Analysis, *Langmuir* **2003**, *19*, 160–165.
- (58) Aveyard, R.; Binks, B.P.; Clint, J.H. Emulsions Stabilized Solely by Colloidal Particles, *Adv. Colloid Interface Sci.* **2003**, *100-102*, 503–546.
- (59) Binks, B.P. Particles as Surfactants –Similarities and Differences, *Curr. Opin. Colloid Interface Sci.* **2002**, *7*, 21–41.
- (60) Binks, B.P.; Lumsdon, S.O. Influence of Particle Wettability on the Type and Stability of Surfactant-Free Emulsions, *Langmuir* **2000**, *16*, 8622–8631.
- (61) Lubansky, A.S.; Yeow, Y.L.; Leong, Y.-K.; Wickramasinghe, S.R.; Han, B. A General Method of Computing the Derivate of Experimental Data, *AIChE J.* **2006**, *52*, 323–332.
- (62) Yeow, Y.L.; Wickramasinghe, S.R.; Han, B.; Leong, Y.-K. A New Method of Processing the Time-Concentration Data of Reaction Kinetics, *Chem. Eng. Sci.* **2003**, *58*, 3601–3610.
- (63) Kus, M.; Altantzis, T.; Vercauteren, S.; Caretti, I.; Leenaerts, O.; Batenburg, K.J.; Mertens, M.; Meynen, V.; Partoens, B.; Van Doorslaer, S.; Bals, S.; Cool, P. Mechanistic Insight into the Photocatalytic Working of Fluorinated Anatase {001} Nanosheets, *J. Phys. Chem. C* **2017**, *121*, 26275–26286.
- (64) Gao, H.; Zhang, D.; Yang, M.; Dong, S. Photocatalytic Behavior of Fluorinated Rutile TiO₂ (110) Surface: Understanding from the Band Model, *Sol. RRL* **2017**, *1*, 1700183.
- (65) Boddu, V.; Kim, S.; Adkins, J.; Weimer, E.; Paul, T.; Damavarapu, R. Sensitive Determination of Nitrophenol Isomers by Reverse-Phase High-Performance Liquid Chromatography in Conjunction with Liquid-Liquid Extraction, *Int. J. Environ. Anal. Chem.* **2017**, *97*, 1053–1064.

Graphical Abstract

