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7 1 Formulation of Metal-Organic Framework Inks for
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11 2 the 3D Printing of Robust Microporous Solids
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15 3 Towards High-Pressure Gas Storage and Separation
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51 15 Keywords: 3D Printing ; Metal-Organic Frameworks ; Inks Formulation ; Methane Storage ;
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53 16 Ethane/Ethylene Separation
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6 2 **ABSTRACT.**
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10 3 Shaping of metal-organic frameworks (MOFs) has become increasingly studied over the past few
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12 4 years because it represents a major bottleneck toward their further applications at larger scale.
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14 5 MOF-based macroscale solids should present similar performances to their powder counterparts
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16 6 along with adequate mechanical resistance. 3D printing is one of the promising technologies as it
17
18 7 allows the fast prototyping of materials at the macroscale; however, the large amounts of added
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20 8 binders have a detrimental effect on the porous properties of the solids. Herein, a 3D printer was
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22 9 modified to prepare a variety of MOF-based solids with controlled morphology from shear-
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24 10 thinning inks containing 2-hydroxyethyl cellulose. Four benchmark MOFs were tested for this
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26 11 purpose: HKUST-1, CPL-1, ZIF-8 and UiO-66-NH₂. All solids are mechanically stable up to 0.6
27
28 12 MPa of uniaxial compression and highly porous with BET specific surface areas lowered by 0 to
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30 13 -25%. Furthermore, these solids were applied to high pressure hydrocarbon sorption (CH₄, C₂H₄
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32 14 and C₂H₆) and presented consequent methane gravimetric uptake (UiO-66-NH₂, ZIF-8, and
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34 15 HKUST-1) and highly preferential adsorption of ethylene of ethane (CPL-1).
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1 2 3 1 4 2 INTRODUCTION

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6 3 Metal-organic frameworks (MOFs) constitute a fast-growing class of microporous
7 4 materials, assembled from metallic nodes – either ions or clusters – and multitopic organic linkers.
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9 5 By changing the length, nature, and shape of linkers or the geometry of metallic nodes, one can
10
11 6 design the final pore size, shape and pore surface functionality.^{1,2} This exceptional structural
12
13 7 diversity strongly contributes to rank MOFs among the best materials reported so far in the
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15 8 literature for catalysis and gas processing.³ Especially, in the context of the development of new
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17 9 technologies for mobility, MOFs show some of the highest gravimetric capacities reported for
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19 10 methane and hydrogen storage.^{4,5} As membranes, MOFs are also highly attractive for separation
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21 11 in gas and liquid phases.⁶ Thus, a consequent effort has been deployed during the past few years
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23 12 for rationalizing and scaling-up the synthesis of promising MOF structures using various
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25 13 techniques such as continuous flow synthesis,⁷ spray-drying,⁸ mechanochemistry,⁹ or
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27 14 electrochemistry.¹⁰ This dynamic led to the first commercial applications of MOFs in 2016.¹¹

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35 15 While MOFs are produced as loose powders and tested as such at the laboratory scale,
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37 16 applications generally require handleable solids with a specific shape and sufficient mechanical
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39 17 robustness to withstand overtime damaging stresses such as attrition and hydrostatic pressure.¹²
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41 18 Therefore, various technologies are being evaluated for the shaping of MOFs. For example,
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43 19 binderless pelletization proved to be a good compromise between mechanical stability and final
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45 20 volumetric uptake in the cases of the zirconium-based UiO family and the Cu₃(btc)₂ (btc = 1,3,5-
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47 21 benzenetricarboxylate) also known as HKUST-1.¹³ High gravimetric uptake was reported for
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49 22 MOF-based grains prepared with an alumina binder,¹⁴ and with MOF beads prepared in the
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51 23 presence of gelling agents.¹⁵ Multiporous monoliths could be obtained by gelation, freeze-casting,
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53 24 or phase separation (spinodal decomposition) starting from a MOF dispersion,¹⁶⁻¹⁸ while well-

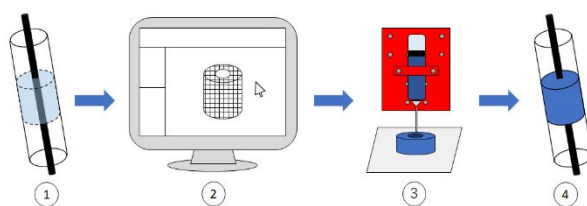
1 controlled thin layers were obtained by chemical vapour deposition.¹⁹ Thus, most application
2 requirements can be covered owing to the current state-of-the-art of MOF shaping; however each
3 technique is limited to a narrow set of obtainable solids. Every application having different
4 specifications, and by anticipating that new applications will require unconventional shaping
5 methods, it is of tremendous interest to develop highly versatile techniques to produce robust
6 macroscale MOF solids.

7 Up to now, additive manufacturing, also called 3D printing, was mostly investigated to
8 produce highly dense ceramics and metal oxides with custom morphologies.²⁰ Lately, a few
9 examples of porous solids were reported, including MOFs. MOF/thermoplastic composites were
10 prepared for direct use as replacements of the commercial polymer filaments in usual 3D
11 printers.^{21,22} When HKUST-1 crystals were mixed with an acrylate monomer and a photoinitiator,
12 porous and flexible macrostructures were obtained by a spatially-controlled polymerization step
13 (DLP).²³ These methods are straightforward to implement on existing 3D printing setups, but the
14 resulting porous properties are heavily affected by the polymers' presence in significant quantity.

15 Instead of using filaments, another approach employs modified 3D printers to extrude inks
16 formulated in the presence of an organic binder. This robocasting approach was evaluated by H.
17 Thakkar *et al.* to prepare MOF-74(Ni)- and UTSA-16(Co)-based materials with a woodpile
18 structure,²⁴ which was also replicated by S. Sultan *et al.* starting from ZIF-8 and MIL-100(Fe),²⁵
19 and A. J. Young *et al.* starting from UiO-66.²⁶ In these cases, a fine control of the inks shear-
20 thinning properties is mandatory to obtain macroscale solids replicating the 3D models. These
21 materials presented an accessible porosity related to their MOF loading – between 30 and 85 wt%
22 - and were successfully applied for the capture of guest molecules in gas- and liquid-phases. While

1 these studies undeniably proved the advantages of combining inks and 3D printing, limited data
2 were given on the inks' rheology and the mechanical robustness of as-prepared solids.

3 This study focuses on the preparation of MOF-based solids by robocasting with controlled
4 macroscale morphology and superior textural properties. The general principle is illustrated on
5 Figure 1. In an effort to rationalize this approach, emphasis is given on measuring the viscosity of
6 inks formulated with four different MOF structures: $[\text{Cu}_2(\text{pzdc})_2(\text{pyz})]$ (CPL-1; pzdc = pyrazine-
7 2,3-dicarboxylate, pyz = pyrazine), $[\text{Cu}_3(\text{btc})_2]$ (HKUST-1; btc = 1,3,5-benzenetricarboxylate),
8 $[\text{Zn}(\text{MeIm})_2]$ (ZIF-8, MeIm = 2-methylimidazol-1-ide) and $[\text{Zr}_6\text{O}_4(\text{OH})_4(\text{bdc-NH}_2)_6]$ (UiO-66-
9 NH_2 , bdc- NH_2 = 2-amino-1,4-benzenedicarboxylate). In a second step, the effect of the
10 robocasting process on the structural and porous properties of copper-paddlewheel-based HKUST-
11 1, which is reputed unstable, are investigated. Moreover, the mechanical robustness of as-prepared
12 solids is evaluated and compared to binderless pellets. Finally, these macroscale structures are
13 evaluated for high-pressure methane storage (HKUST-1, ZIF-8, UiO-66- NH_2) and ethane/ethylene
14 separation (CPL-1), for which their powder counterparts present excellent performances.



15
16 **Figure 1.** Typical process workflow based on the methodology developed herein: 1/ identification
17 of the need, 2/ computer-assisted modelling of the fitting solids, 3/ MOF-based ink deposition
18 using a 3D printer, 4/ evaluation of the performance of the solid.

19 EXPERIMENTAL SECTION

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5 2 *N,N*-Dimethylformamide (DMF, 99.5 %), ethanol (EtOH, 99.5 %), methanol (MeOH, 99.8 %),
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7 3 Basolite Z1200 (ZIF-8), zirconium tetrachloride (ZrCl_4 , ≥ 97 %), hydrochloric acid (HCl, 35 %),
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9 4 2-aminoterephthalic acid ($\text{H}_2\text{BDC-NH}_2$, > 97 %), copper acetate hydrate ($\text{Cu(OAc)}_2 \cdot 2.5 \text{H}_2\text{O}$, 99
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11 5 %), copper nitrate hemi(pentahydrate) ($\text{Cu(NO}_3)_2 \cdot 2.5\text{H}_2\text{O}$, > 98 %), pyrazine-2,3-dicarboxylic
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13 6 acid (H_2pzdc , > 98 %), pyrazine (pyz, > 98 %), trimesic acid (H_3BTC , 95 %), 2-hydroxyethyl
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15 7 cellulose (HEC, $M_w = 250000$ g/mol), polyvinyl alcohol (PVA, $M_w = 1500$ g/mol). All reagents
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17 8 and reactants were purchased from Wako Pure Chemical Industries or Sigma-Aldrich and were
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19 9 used without further purification.
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24 10 **Synthesis of CPL-1 MOF.** The synthesis is based on previous works from M. Bonneau *et al.*²⁷ A
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26 11 solution of $\text{Cu(NO}_3)_2 \cdot 2.5 \text{H}_2\text{O}$ (4.30 mmol) and pyz (8.60 mmol) in 30 mL of H_2O was stirred at
27
28 12 room temperature for 10 minutes. A solution of H_2pzdc (4.30 mmol) with NaOH (8.52 mmol) in
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30 13 a 30 mL mixture 7:3 of $\text{H}_2\text{O}/\text{EtOH}$ was added dropwise to the stirring mixture. A blue precipitate
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32 14 is noted. After one hour, the crude product is collected by centrifugation and was washed two times
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34 15 with H_2O and three times with EtOH. The blue powder is dried under vacuum at room temperature
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36 16 overnight. Final yield = 95 %.
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41 17 **Synthesis of UiO-66-NH₂ MOF.** The synthesis is based on previous works from M.J. Katz *et*
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43 18 *al.*²⁸ In a 110 mL glass vial, 2.08 mmol of ZrCl_4 were dissolved in a mixture of 20 mL of DMF
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45 19 and 4 mL of HCl under sonication for 20 minutes to obtain a clear solution. Then 2.92 mmol of
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47 20 $\text{H}_2\text{BDC-NH}_2$ and 40 mL of DMF were added and the mixture was sonicated for an additional 20
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49 21 min. The vial was left in static conditions in an oven at 80°C. The product was recovered by
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51 22 centrifugation, washed three times with DMF, four times with EtOH, and then dried overnight in
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53 23 a vacuum oven at 100°C. Final yield = 52 %.
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3 **1 Synthesis of HKUST-1 MOF nanocrystals.** The synthesis is based on previous works from J.
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5 **2** Huo *et al.*²⁹ In a 1 L Erlenmeyer, 6.62 mmol of Cu(OAc)₂·2.5 H₂O were dissolved in 150 mL of
6
7 **3** deionized H₂O. Meanwhile, 15.0 mmol of H₃BTC were dispersed in 150 mL of H₂O under
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9 **4** sonication for 20 min. The H₃BTC suspension was quickly added to the Cu(OAc)₂ solution and
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11 **5** the mixture was stirred at 1200 rpm for 1 h at 23°C. Additionally, 24 h in those conditions led to
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13 **6** the formation of larger crystals. The product was recovered by centrifugation, washed twice with
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15 **7** MeOH, soaked overnight in MeOH, and washed again twice with MeOH. Finally, the powder was
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17 **8** dried overnight in a vacuum oven at 100°C. Final yield = 29 % (nanocrystals).
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22 **9 Preparation of shear-thinning inks.** A stock solution of HEC in H₂O was prepared by first
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24 **10** dissolving an adequate quantity of powder at 80°C under stirring and then leaving the obtained
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26 **11** clear solution in the fridge overnight before storage at room temperature. A defined quantity of
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28 **12** this stock solution was mixed at 1000 rpm for 10 h with MOF powder deagglomerated beforehand
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30 **13** and PVA, here acting as a plasticizer during the subsequent printing step. For example, appropriate
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32 **14** shear-thinning properties were obtained with the following weight composition: 0.25 CPL-1 MOF:
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34 **15** 0.01 PVA: 0.02 HEC: 0.65 H₂O. Reproducibility of the protocol was verified by preparing three
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36 **16** times this ink' composition and measuring the relating apparent viscosity at different shear rates
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38 **17** (Figure S1). An average standard deviation of 16% can be observed. Therefore, the following
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40 **18** apparent viscosities will be plotted as confidence intervals.
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46 **19** In the case of HKUST-1, a mixture 50 vol% H₂O/50 vol% EtOH is used instead of pure H₂O to
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48 **20** limit hydrolysis.
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52 **21 Solids design and description of the robocasting process.** The Part Design workbench of the
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54 **22** computer-assisted design software FreeCAD was used to model the different solids to be printed,
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1 then exported under a stereolithography (STL) file format. This file was loaded in Cura, a slicer
2 software, and relevant parameters for the 3D printing step were defined at this step. These
3 parameters include the printing speed, the temperature of the heating bed, and the thickness of the
4 layer deposited. The resulting set of data was saved under a g-code (GCODE) file, enabling to
5 pilot the 3D printer in a layer-by-layer fashion.

6 A modified Anet A8 3D printer, shown on Figure S2, was used for this work. According
7 to its technical specifications, its spatial resolution along x/y axes is ± 0.2 mm. The main
8 modifications include the addition of a borosilicate glass on the top of the heating bed for chemical
9 passivity and improved adhesion during ink deposition, and the replacement of the filament
10 feeding system by a customizable carriage printed with polylactic acid (PLA) to hold syringe
11 barrels filled with inks. The model was created by TNS and is licensed under the Creative
12 Commons – Attribution – Non-Commercial- Share Alike license on Thingiverse. The length of
13 the 0.8 mm diameter syringe needle was reduced to 20 mm to obtain a flat extremity and a constant
14 shear stress zone. Manual z-calibration was done between each experiment. To obtain a constant
15 flowrate during the printing, a peristaltic pump was pushing water upstream of the syringe, with a
16 rubber cap insuring no contact with the loaded ink and a homogeneous repartition of the pressure
17 applied. Accurate 3D replications were obtained with the following set of data: 20 mm/s (printing
18 speed); 60 °C (heating plate temperature); 0.5 mm (layers thickness); 0.8 mm (needle diameter);
19 7 μ l/s (pump flow rate). As a simple accuracy test, a model made of lines and circles was printed
20 (Figure S3). When taking into account the spatial resolution of the printer, an average deviation of
21 4% is observed between the model and the 3D printed solid. After partial drying on the heating
22 plate, the solids were recovered and dried overnight in a vacuum oven at 90°C before
23 characterization.

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3 **1 Characterization and gas sorption.** Viscosity of the inks at 23 °C was evaluated using a
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5 2 Brookfield DV2T viscosimeter in a cone-plate configuration, with a cone radius of 2.4 cm and a
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7 3 cone angle of 0.8 °. Shear rates from 0.2 to 100 s⁻¹ were applied in an increasing fashion, in a range
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9 4 comprised between 10% and 100% of the maximum torque. Wide-angle powder X-ray diffraction
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11 5 (PXRD) patterns were recorded on a Rigaku Ultima III diffractometer equipped with a Cu K_{α1}
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13 6 monochromatic radiation source (45 kV, 200 mA). Diffraction patterns in the 5-50 ° region were
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15 7 recorded with a 0.02 ° step size (step time = 0.3 s). Before measurement, the powder was deposited
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17 8 on a glass substrate and automatic alignment was made. Thermogravimetry-differential thermal
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19 9 analysis (TG-DTA) was performed on Rigaku Thermo plus EVO II between 23 and 800 °C, at a
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21 10 heating rate of 5 °C.min⁻¹ under nitrogen flow. Microstructures of the as-prepared MOF crystals
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23 11 and the fractured surfaces of robocasted solids were observed under a Hitachi SU5000 scanning
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25 12 electron microscope (SEM). Samples were directly deposited on a conductive carbon tape and
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27 13 coated with 10 nm of osmium. Fourier-Transform Infrared (FT-IR) spectra were recorded in
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29 14 attenuated total reflectance (ATR) using a Jasco FT/IR-6100 spectrometer equipped with a
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31 15 TriGlycine Sulfate detector.
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39 16 Mechanical properties of 3D-printed solids were compared to their binderless pelletized
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41 17 counterparts, prepared using a AS ONE manual tableting instrument. The die, with an inner
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43 18 diameter of 10 mm, was filled with an appropriate amount of MOF powder to obtain a final height
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45 19 of 5 mm +/- 0.5 mm after maintaining a pressure of 200 bars for 2 minutes. The unidirectional
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47 20 compression tests were carried out using a material tester (Autograph AG-X plus, Shimadzu Corp.,
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49 21 Japan). The pressure applied on the force sensor was recorded as a function of the displacement of
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51 22 the punch at a constant speed of 5.0 mm.min⁻¹. One representative solid of each composition and
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53 23 from each shaping technique was tested.
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3 1 Prior to sorption isotherm measurements, all samples were degassed at 120 °C under
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5 2 secondary vacuum during 14 h. Nitrogen (N₂) and carbon dioxide (CO₂) adsorption isotherms were
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7 3 recorded on a BEL Japan BELSORP-mini volumetric-adsorption instrument at 77 K and 195 K,
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9 4 respectively. Specific surface areas (SSA) were determined using the BET method on a linear
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11 5 portion of the nitrogen adsorption isotherm below $P/P^0 = 0.3$, with $R > 0.999$ and $C > 0$. The
12
13 6 micropore ($V_{\text{micro.}}$) and total pore ($V_{\text{tot.}}$) volumes were estimated from the adsorbed volume of N₂
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15 7 at $P/P^0 = 0.30$ and 0.99, respectively. High pressure methane (CH₄), ethane (C₂H₆) and ethylene
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17 8 (C₂H₄) sorption isotherms were recorded on a BEL Japan BELSORP-max volumetric-adsorption
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19 9 instrument at 298 K up to 55 bars (CH₄) and 19 bars (C₂H₄, C₂H₆). Expected deviation on
20
21 10 physisorption measurements is around ± 1 %.

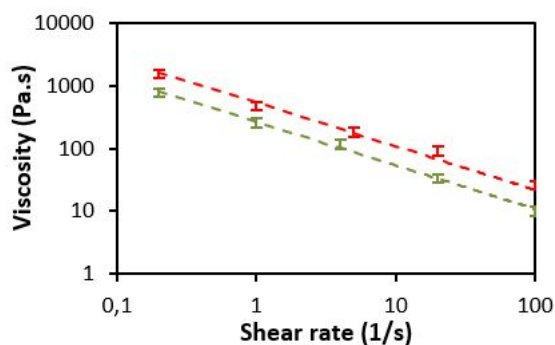
27 11 **RESULTS AND DISCUSSION**

30 12 **Optimization of MOF inks' composition**

33 13 At first, the composition of inks containing MOF crystals was optimized to obtain the best
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35 14 compromise between high loading of MOF crystals and good processability. For robocasting, inks
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37 15 should demonstrate controlled shear-thinning properties, with proper flowability when an external
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39 16 force is applied, while holding their shape in stationary state. Thus, it is expected that the inks
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41 17 should be as viscous as possible, within a range allowing a continuous flow rate by the peristaltic
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43 18 pump. This flow rate also has to be in adequation with the printing speed of the 3D printer and the
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45 19 thickness of the deposited layer. Because many parameters have a notable influence on the printing
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47 20 quality, all parameters relating to the 3D-printing operation were set constant and only the inks
48
49 21 composition was modified accordingly. After a preliminary screening, a combination of 2-
50
51 22 hydroxyethyl cellulose (HEC) and polyvinyl alcohol (PVA) was selected as binders over Pluronic

1 F-127 and polyvinylpyrrolidone K25 owing to the higher viscosity obtained using small (< 10
2 wt%) quantities. This is mandatory to maximize the porosity of the final object and hence its
3 performances. HEC is derived from cellulose and is widely used as a gelling agent in cosmetics
4 and household products. Note that the use of methylcellulose, another product derived from
5 cellulose, was reported for the preparation of zeolite-based monoliths by 3D-printing.³⁰

6 Figure 2 presents the apparent viscosity of inks formulated with different concentrations of
7 CPL-1, while maintaining constant MOF/HEC and HEC/PVA ratio. All points can be fitted by a
8 power law with a negative exponent, which is characteristic of a shear-thinning behaviour.³¹
9 Higher concentrations lead to higher apparent viscosities, with more than a two-fold increase of
10 the viscosity when the concentration is increased by a factor 1.5. When used for robocasting, solids
11 replicating the models were successfully obtained with the ink formulated with 35 wt% of CPL-1
12 (Figure 3a). On the other hand, poorly defined solids were obtained with the more concentrated
13 ink (51 wt%), as evidenced on Figure 3b.



14
15 **Figure 2.** Viscosity plots of inks formulated with 35 wt% (green) and 51 wt% (red) of CPL-1.
16 MOF/HEC = 12.5 ; HEC/PVA = 2.0. Error bars = 10%.

17 A similar observation was made with inks formulated with different concentrations of ZIF-
18 8 (Figure S4). This is because of limitations induced by the use of a peristaltic pump, whose torque

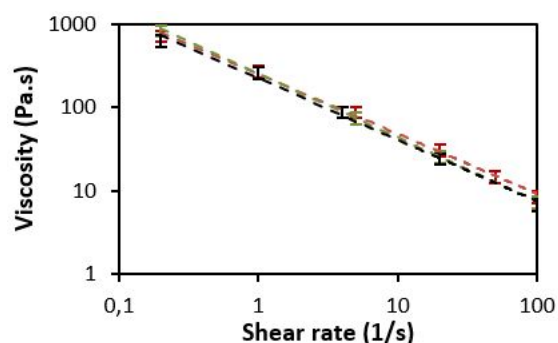
1 is not able to maintain a constant flow rate of inks with apparent viscosities above 1000 Pa.s under
2 a shear rate of 0.2 s^{-1} . Therefore, this value was set as a higher limit when formulating MOF-based
3 inks. On the other hand, when the apparent viscosity at low shear rate is ten-fold lower, consequent
4 spreading of the ink occurs after its deposition on the plate (Figure S5), resulting in a poor
5 replication of the 3D model. Therefore, a careful balance needs to be reached.



6
7 **Figure 3.** Photographs of CPL-1-based objects printed under the same conditions with inks
8 formulated with 35 wt% (a) and 51 wt% (b) of CPL-1.

9 Previous rheological studies have shown that, in the case of dense non-colloidal
10 suspensions, viscosity increases mostly with the particles fraction. In these conditions, the size of
11 particles have a minor impact on the viscosity.³² However, when a gelling agent and particles are
12 mixed, the resulting rheological properties become unpredictable by the standard models as the
13 two species can compete in forming the gel structure.³³ Therefore, to evaluate if the crystals size
14 has an impact on the inks shear-thinning properties, two HKUST-1 samples presenting different
15 crystal size distributions (50-100 nm and 500-2000 nm, Figure S6) were used for inks formulation
16 and compared to the stock solution of HEC. Interestingly, similar rheological behaviors are
17 observed on Figure 4 with smaller crystals and higher weight fraction (16 wt%) and with larger
18 crystals and lower weight fraction (11 wt%). Therefore, and in adequation with the literature,³² the
19 crystals size seems to have only a minor impact on the measured viscosity of the inks. Additionally,
20 both inks are slightly more viscous at low shear rates ($< 10 \text{ 1/s}$) than the stock solution of HEC.

1 The highest concentration of crystals for a processable ink was obtained in the presence of
2 CPL-1 (35 wt%). CPL-1 consists of 2D layers of copper(II) and pyrazine, pillared by pyrazine-
3 2,3-dicarboxylate compounds. The resulting crystals are highly anisotropic, as displayed in Figure
4 S7. In comparison, the crystals obtained with HKUST-1, ZIF-8, and UiO-66-NH₂ are isotropic
5 (Figures S6 and S7). The influence of anisotropic particles, and especially clays, on the rheological
6 properties of suspensions has been extensively studied.³⁴ In particular, under high shear rates,
7 anisotropic materials becomes oriented with the flow direction, therefore minimizing the intrinsic
8 viscosity and increasing the maximum packing density. Interestingly, this observation further
9 means that anisotropic materials might be more suited for the 3D printing of inks.

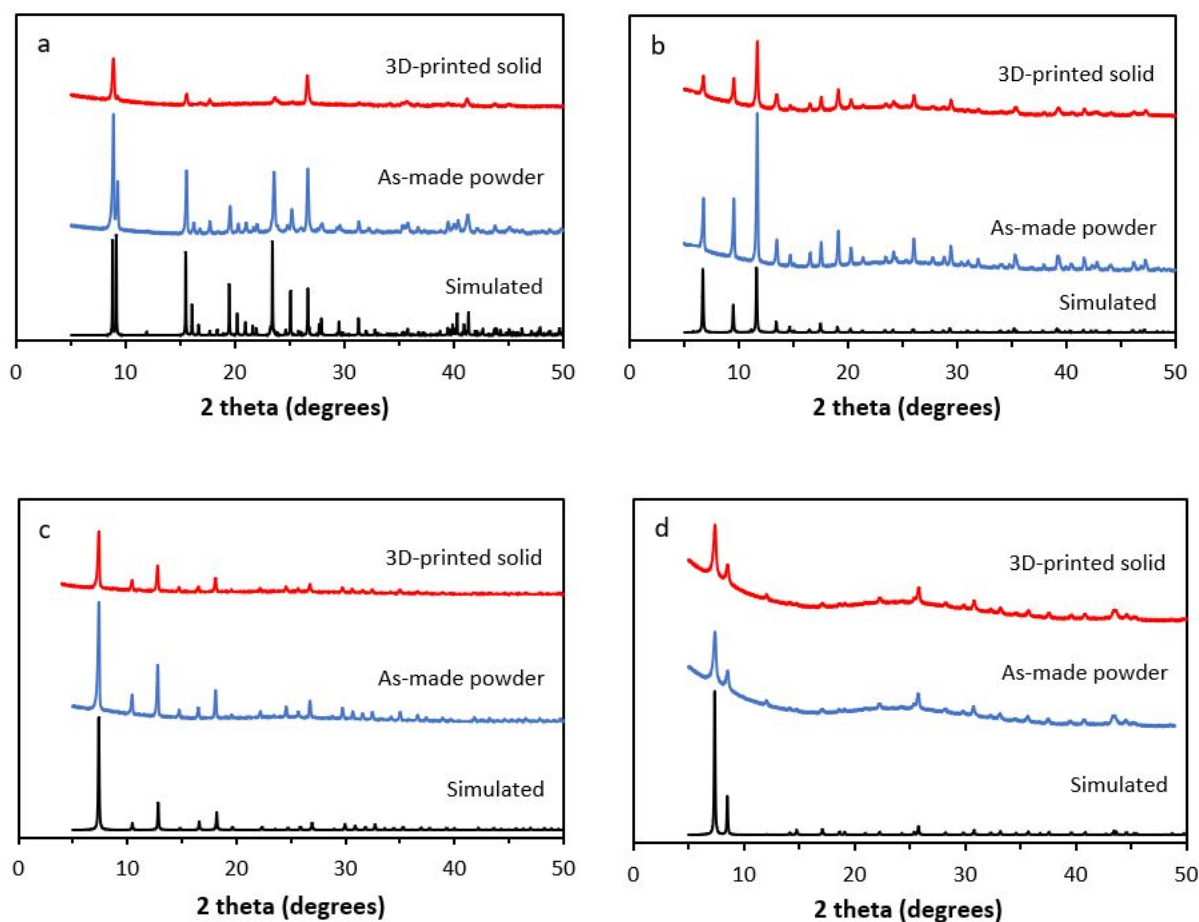


10
11 **Figure 4.** Viscosity plots of a pure HEC solution (black), and HKUST-1-based inks formulated
12 with 11 wt% of large crystals (red) and with 16 wt% of nanocrystals (green). MOF/HEC = 4.9
13 (blue) and 6.9 (green); HEC/PVA = 2.1.

14 Therefore, viscosity is proposed as a reliable descriptor to evaluate the inks processability,
15 with apparent viscosities comprised between 100 and 1000 Pa.s under a shear rate of 0.2 s⁻¹ and a
16 shear-thinning behaviour allowing their use for robocasting. These criteria should be met in future
17 studies involving MOF-based inks and similar setups.

18 **Characterization of the 3D printed solids**

1 Fresh inks formulated with the different MOF structures were prepared and their measured
2 apparent viscosity is given on Figure S8. Cylinders of 10 x 10 mm were prepared for
3 characterization and mechanical tests, along with various solids displayed on Figure S9. After
4 drying, these solids present a uniform volume shrinkage of about 6%. (Figure S10).



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7 **Figure 5.** PXRD patterns of the as-made MOF powders and the related 3D-printed solids: CPL-1
8 (a), HKUST-1 (b), ZIF-8 (c) and UiO-66-NH₂ (d).

9 Figure 5 presents PXRD patterns of the as-prepared MOF powders and the 3D-printed
10 solids. As evidenced by the diffraction data, the robocasting process only slightly affected the
11 structures of MOFs. No secondary crystalline phase can be detected, while lower diffraction

1 intensities can be attributed either to a partial loss of long-range order – especially in the case of
2 HKUST-1 – or to the presence of amorphous PVA and HEC in significant quantity. Their presence
3 is also attested by thermogravimetric analysis (TGA) under N₂ flow (Figure S11), with an
4 increased weight loss above 200 °C matching with the ink's composition. In the case of CPL-1,
5 the 3D-printed solid presents different relative intensities compared to the as-made powder
6 (Figures 5a). This is due to the preferential orientation of the anisotropic crystals along the *b*-axis
7 after formulation of the ink and deposition, as observed on Figure S12. Infrared spectroscopy with
8 attenuated total reflection mode (IR-ATR) was also conducted on all samples and revealed similar
9 surface properties between the as-prepared powders and the 3D-printed solids (Figure S13). An
10 additional low-to-medium band at 1060 cm⁻¹ can be attributed to primary alcohol functions coming
11 from the hydroxyethyl cellulose in the 3D-printed solids. Thus, the 3D-printed solids retained the
12 MOF microporous structures even in the case of the more sensitive copper-paddlewheel-based
13 structures.

14 Porous properties of as-made powders and 3D-printed solids were confronted using CO₂
15 and N₂ physisorption, and the resulting isotherms are presented on Figure 6 and Figure S14,
16 respectively. For direct comparison, the adsorbed volume was recalculated using the proportion of
17 MOF in the solids as indicated by TGA (Tab. S1). In the case of ZIF-8, comparable isotherms are
18 obtained with both gases (-1 to +3 %). This means that neither the binders' presence or the shaping
19 process affect the adsorption capacity of the ZIF-8 MOF, and by extension that the binders should
20 not modify significantly the adsorption capacity of any MOF.

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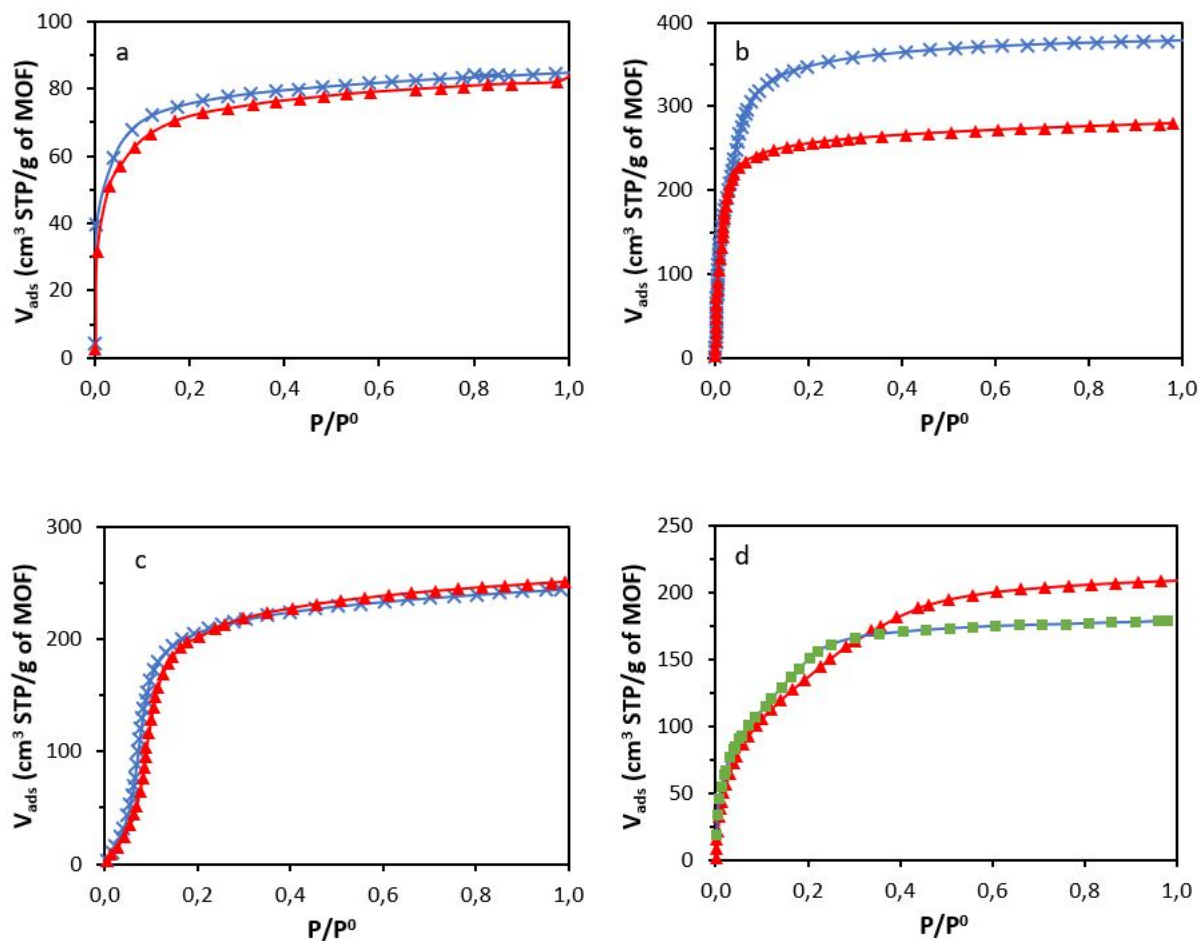


Figure 6. Carbon dioxide adsorption isotherms at 195 K of the as-made MOF powders (cross), and the related crushed pellets (square) and 3D-printed solids (triangle): CPL-1 (a), HKUST-1 (b), ZIF-8 (c) and UiO-66-NH₂ (d).

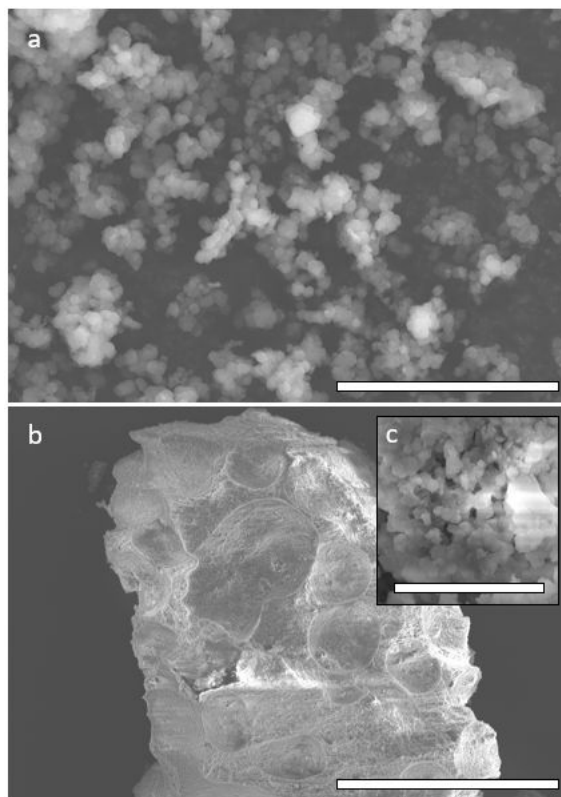
After 3D-printing UiO-66-NH₂ also presents a comparable type I N₂ adsorption isotherm (Figure S14), with a comparable specific surface area. This is expected as UiO-66-NH₂ was reported as highly stable – except in basic conditions.³⁵ More interestingly, a significant increase of about +17 % is observed on the total adsorbed CO₂ isotherm after 3D-printing, compared to a crushed pellet of the same as-made powder. Using a crushed pellet of UiO-66-NH₂ instead of the as-made powder should result in a difference of less than 5%, owing to the resistance of this

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3 1 framework towards uniaxial compression.¹³ Under a relative pressure of 0.25, both isotherms
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5 2 follow the same adsorption trend, with the adsorption branch after 3D-printing being below the
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7 3 branch of the crushed pellet. This can be interpreted as a small loss of pore accessibility due to the
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9 4 presence of binders. However, above a relative pressure of 0.25, the porosity is saturated in the
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11 5 case of the crushed pellet while the adsorbed volume continues to increase as a function of the
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13 6 relative pressure in the case of the 3D-printed solid. Owing to the small size of the crystals (< 150
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15 7 nm, Figure S7), and the increased adsorption capacity at higher relative pressure, this observation
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17 8 is most likely correlated to the formation of interstitial voids between crystals due to the presence
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19 9 of binders.
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25 10 After shaping, HKUST-1 presents a lowered BET specific surface area of about -25 %
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27 11 along with a decreased CO₂ adsorption capacity (-30 %). This is in line with the XRD
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29 12 characterization and indicates that HKUST-1 was partially degraded after the 3D-printing process.
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31 13 This MOF structure is reputed to undergo hydrolysis in the presence of water.³⁶ To avoid this
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33 14 partial degradation, water should be completely replaced by another polar solvent that can dissolve
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35 15 HEC, such as dichloroethane. Comparatively, other shaping techniques such as pelletization
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37 16 commonly lowers HKUST-1 specific surface area by -15 to -95 %, depending on the pressure
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39 17 applied.¹³
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44 18 Another result of interest comes from the CPL-1 3D-printed solid. While this solid shows
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46 19 similar CO₂ adsorption capacity at 195 K compared to its powder counterpart, a greatly reduced
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48 20 N₂ adsorption capacity is observed at 77 K (-73 % micropore volume). Regular CO₂ sorption is
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50 21 observed following the N₂ sorption of the same solid. Knowing that some flexibility was reported
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52 22 with these pillared-layer structures,³⁷ this observation could be related to a combined effect of
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1 framework flexibility and a different behaviour from HEC and PVA at 77 K, inducing a partial
2 pore blockage.



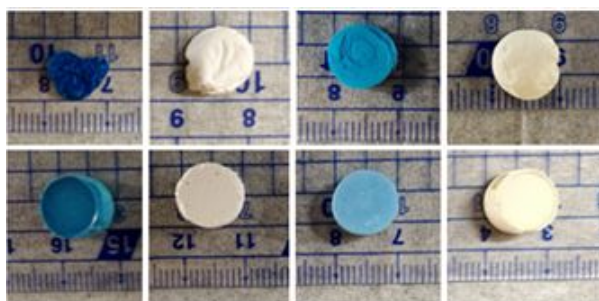
3
4 **Figure 7.** SEM micrographs of as-made ZIF-8 powders (a), and a fragment of 3D-printed ZIF-8
5 solid (b, c). Scale bars are 10 μm (a, c) and 500 μm (b).

6 SEM micrographs of ZIF-8 are presented on Figure 7. No difference can be observed in
7 terms of size and morphology between the as-prepared powder and the 3D-printed solids.
8 Interestingly, craters can be observed on 3D-printed solid fragments, resulting from the fast drying
9 of inks after printing. While water represents more than 50 vol% of the inks' composition, after
10 drying no modification of the solids dimensions is observed. Therefore, a consequent volume
11 fraction of the solids must be empty. A plausible explanation comes from the fact that, owing to
12 the shear-thinning properties of the inks, the solvent has higher mobility than the suspended

1 crystals, resulting in convective heat transfer being faster than conductive heat transfer (Peclet
2 number > 1) and hence in local radial diffusion of the crystals.³⁸ This phenomenon is similar to the
3 formation of hollow spheres by spray-drying.⁷

4 As a partial conclusion, 3D-printed solids were obtained from CPL-1, HKUST-1, ZIF-8
5 and UiO-66-NH₂ as-prepared powders with low impact on their structural and porous properties
6 (0 to -25%). In comparison, H. Thakkar *et al.* observed a decrease of the recalculated micropore
7 volume comprised between -7 % (USTA-16(Co)) and -22 % (MOF-74(Ni)) in the presence of
8 bentonite and PVA,²⁴ and S. Sultan *et al.* observed a decrease of -27 % of the micropore volume
9 of ZIF-8 in the presence of modified cellulose nanofibers and alginate.²⁵ This difference is due to
10 the use of HEC and PVA in low amounts (7-20 wt%), allowing high accessibility of the inner
11 porosity. Therefore, the inks' preparation and the robocasting methodologies described here are
12 adapted for the preparation of 3D-printed MOF-based solids with the original porous properties
13 maintained.

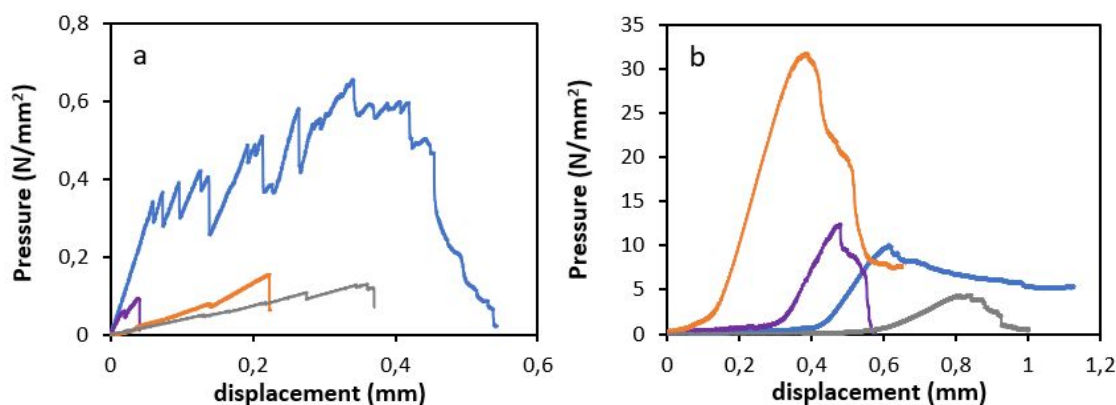
14 Evaluation of their mechanical stability



15
16 **Figure 8.** Photographs of the cylindrical 3D-printed solids (top) and their binderless pelletized
17 counterparts (bottom), whose mechanical resistance was evaluated by uniaxial compression. From
18 left to right: HKUST-1, ZIF-8, CPL-1, and UiO-66-NH₂.

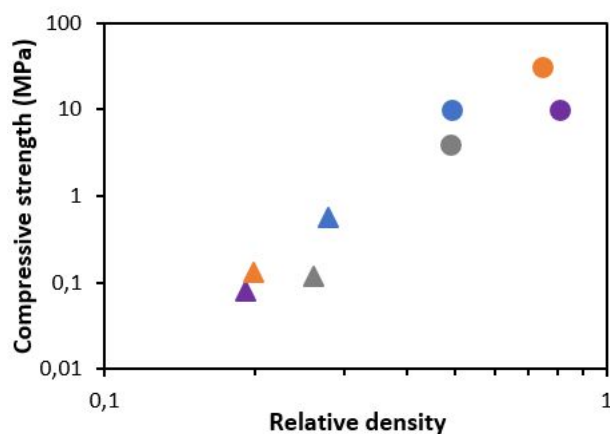
1 For long term application and cyclability, it is necessary to evaluate the mechanical
2 robustness of highly porous solids. Insufficient mechanical stability leads to their attrition,
3 generation of dust, and therefore, overtime loss of performances. In continuous flow application
4 such as gas separation, the solids also have to withstand the applied pressure drop.

5 The mechanical properties of 3D-printed solids were evaluated by uniaxial compression.
6 Cylinders of dimensions 10 x 10 mm were pressed on their flat surface at a constant displacement
7 rate and the pressure was recorded until sudden pressure drop. For comparison, binderless tablets
8 of identical dimensions were also prepared using a manual tableting instrument. All these solids
9 are presented on Figure 8. As the CPL-1-based ink contained the highest MOF crystals loading,
10 almost perfectly shaped cylindrical solids were prepared. On the other hand, lower MOF crystals
11 loadings induced partial sagging on the edges, which is expected to have an effect on the
12 mechanical test by lowering the surface in contact with the die and thus underestimating their
13 compressive strength.



14
15 **Figure 9.** Compressive pressure-displacement curves of cylindric 3D-printed solids (a) and
16 binderless tablets (b): CPL-1 (blue), HKUST-1 (purple), ZIF-8 (grey), and UiO-66-NH₂ (orange).

1 The compressive pressure-displacement curves of all tested solids are presented in Figure
2 9. One to two orders of magnitude of compressive strength difference can be observed between
3 the 3D-printed samples and the binderless tablets, defined as the maximum pressure recorded
4 before catastrophic failure. This can be explained by the considerable (> 50 vol%) voids fraction
5 inside the 3D-printed solids, favouring the fracture propagation. Nonetheless, these results are
6 remarkable as the CPL-1 solid 3D-printed from an ink incorporating 35 wt% of MOF crystals
7 presents compressive strength (0.64 MPa) in line with the solids prepared by H. Thakkar *et al.*
8 (0.56 MPa),²⁴ while incorporating less than 7 wt% of binders. This is highly desirable in order to
9 maximize the storage capacity of the materials.



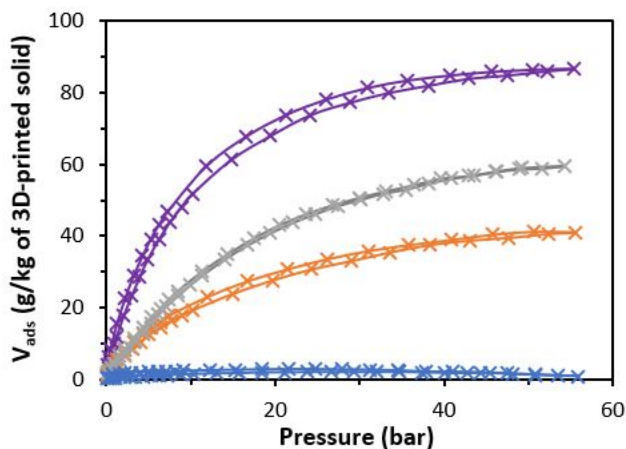
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11 **Figure 10.** Compressive strength as a function of the relative density of 3D-printed solids (triangle)
12 and binderless pellets (circles) prepared from CPL-1 (blue), HKUST-1 (purple), ZIF-8 (grey), and
13 UiO-66-NH₂ (orange) as-made powders.

14 To investigate more in details the effect of the voids fraction on the compressive strength
15 of the materials, Figure 10 presents the latter as a function of their relative density. A correlation
16 can be seen, unrelated to the shaping technique used. This correlation was also reported in the case
17 of macroporous ceramics.³⁹ Hence, the most straightforward way to further increase the

1 mechanical performances of 3D-printed solids is to increase their relative density. As previously
2 underlined, this increase can be obtained by decreasing the applied drying temperature in order to
3 slow down convective heat transfer. The resulting solids' dimensions will then shrink during
4 drying, leading to denser crystals' packing.

5 Use of 3D-printed monoliths for gas storage and separation

6 MOFs are actively screened for gas storage owing to their superior porous properties.
7 Notably, methane is seeing as an alternative to petrol for mobility applications, and MOFs show
8 some of the highest volumetric and gravimetric capacities reported so far, with HKUST-1 being
9 one of the leading materials.⁴ However, most studies evaluated methane storage capacity of MOFs
10 in powder form,^{40,41} while mobility applications require well-defined, attrition-resistant solids.
11 Therefore, high pressure methane adsorption/desorption isotherms were measured at ambient
12 temperature on the 3D-printed cylinders up to 55 bars, and displayed on Figure 11.



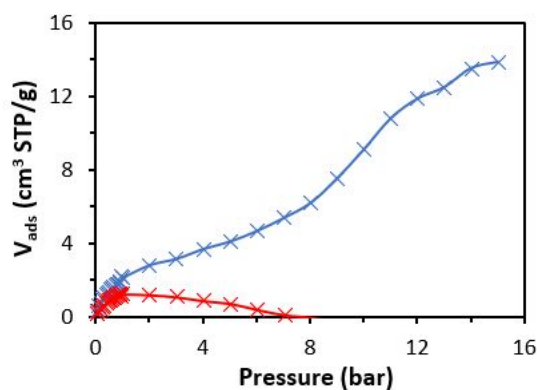
13
14 **Figure 11.** High-pressure methane physisorption isotherms at 298 K of 3D-printed monoliths:
15 CPL-1 (blue), HKUST-1 (purple), ZIF-8 (grey) and UiO-66-NH₂ (orange).

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3 1 In the literature a simple correlation between the gravimetric uptake of methane and the
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5 2 BET specific surface area of MOFs was proposed, with a plateau reached above 2400 m²/g.⁴⁰
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8 3 According to this correlation, our HKUST-1 3D-printed solids with a BET specific surface area of
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10 4 about 1200 m²/g should present a total gravimetric uptake of about 105 g of methane per kilogram
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12 5 of MOF at 298 K and 35 bar. This value is in accordance with the 81 g of methane adsorbed per
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14 6 kilogram of 3D-printed HKUST-1-based solid at 298 K and 35 bar. After taking into account the
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16 7 19.5 wt% of HEC and PVA content, the total gravimetric uptake reaches 101 g of methane
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18 8 adsorbed per kilogram of HKUST-1. Similar conclusion is drawn with the ZIF-8 3D-printed solids,
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20 9 presenting a gravimetric capacity of 59 g of methane per kilogram of ZIF-8 at 298 K and 30 bar
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22 10 (against a reported 68 g/kg of commercial ZIF-8 powder at 298 K and 30 bar).⁴²
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27 11 UiO-66-NH₂ presents the highest gravimetric methane uptake of all isoreticular UiO-66
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29 12 frameworks (76 g/kg of MOF at 298 K and 20 bar), owing to its small and polar amino groups.⁴³
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31 13 Herein, the UiO-66-NH₂-based 3D-printed solids display lower methane uptake (30 g/kg of MOF
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33 14 at 298 K and 20 bar), which could be due to its significantly lower BET specific surface area (871
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35 15 m²/g instead of 1123 m²/g). It seems that the presence of HEC and PVA does not affect
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37 16 significantly the adsorption performances of the MOFs for methane storage, as also observed for
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39 17 N₂ and CO₂ adsorption. After testing the solids were recovered with no visible failure and are
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41 18 therefore stable up to 55 bars. Thus, 3D printing could allow to design solids specific for mobility
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43 19 applications, easily stackable and with the controlled formation of macro-holes for heat dissipation
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45 20 and constant methane delivery. Further effort should focus on obtaining highly porous 3D-printed
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47 21 solids, with BET specific surface areas above 2000 m²/g.
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53 22 While CPL-1 shows neglectable methane adsorption capacity compared to other MOFs
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55 23 (Figure 11), this framework presents one of the highest reported separation capacities for C₂
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1 hydrocarbon mixtures owing to its small one-dimensional channels (4 Å x 6 Å) and flexible
2 behaviour, with the complete exclusion of ethane over ethylene at room temperature and mild
3 pressure.⁴⁴ By comparison with the ethane gas molecule, the relatively smaller size of ethylene
4 (less than 0.2 Å difference) and the interaction of ethylene double-bond with the open metal site
5 allow the adsorption of ethylene at mild pressure.^{45,46} Only a few materials are presenting this
6 behavior which is highly interesting for gas purification,⁴⁷ generally relying on highly energy-
7 costly cryogenic distillation.



8
9 **Figure 12.** High-pressure ethylene (blue) and ethane (red) physisorption isotherms at 298 K of
10 3D-printed CPL-1 monoliths.

11 Ethane and ethylene isotherms were measured on 3D-printed CPL-1-based solids (Figure
12 12). Interestingly, no adsorption of ethane is observed above 8 bar, while adsorption of ethylene
13 increases with increasing pressure up to 16 bar following a type IV isotherm.⁴⁶ Furthermore, the
14 3D printed solids did not show any visible defect after three adsorption/desorption cycles.

15 Thus, the robocasting technique is appropriate to shape MOF-based solids for high pressure
16 gas storage and separation, as long as the gravimetric capacity is the critical parameter. Little to
17 no effect of the presence of HEC and PVA is observed, beyond their contribution to the total solids

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3 1 weight. However, more investigation is required in order to densify the final solids and to increase
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5 2 their volumetric capacity as discussed above, which is highly desirable for industrial applications.
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1 CONCLUSION

2 A modified 3D printer was used for the controlled deposition of inks, formulated from four
3 different MOF powders and in the presence of low proportions of a binder (2-hydroxyethyl
4 cellulose) and a plasticizer (polyvinyl alcohol). Owing to the determination of optimal shear-
5 thinning properties, a series of MOF-based solids with controlled macroscale morphology were
6 fabricated. All characterization techniques indicate that the 3D printing process impacted only
7 slightly the MOFs' textural and structural properties. Indeed, the solids displayed a permanent
8 microporosity that is comparable to the initial powders. Interestingly, SEM analysis highlighted
9 that the 3D-printed solids present a high degree of voids, due to the fast drying step employed.
10 Nonetheless, the solids present high compressive strength, only one to two orders of magnitude
11 lower than dense binderless pellets. When used for high-pressure methane storage (HKUST-1,
12 ZIF-8, and UiO-66-NH₂), or for ethane/ethylene separation (CPL-1), the 3D-printed solids
13 displayed performances which are in line with the literature. This preliminary work needs more
14 investigation, especially for densifying the 3D-printed solids and improving their mechanical
15 robustness, but also for studying their stability in typical process conditions over cycling.
16 Especially, the 3D printer should be further modified to allow the processing of highly viscous
17 inks with shear-thinning properties, about one order of magnitude higher than the inks presented
18 herein. However, the authors believe that this study paves the way to the preparation of highly
19 porous MOF-based solids with designs completely adaptable to the applications: microreactors,
20 adsorbent beds, or separation membranes with specific morphologies to name a few.

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3 **1 ASSOCIATED CONTENT**
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6 **2 Supporting Information.** The Supporting Information is available free of charge on the ACS

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9 **3** Publications website at DOI: .

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11 **4** Additional characterization include photographs, FT-IR spectra, SEM micrographs, viscosity
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13 **5** curves, H₂O and N₂ isotherms. The following files are available free of charge.
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34 **12 Author Contributions**
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36 **13** J.D and S.F. conceived and designed the project. J.D. prepared the HKUST-1 and UiO-66-NH₂
37
38 **14** powders, the 3D-printed solids, and the pellets, and did all characterizations. M.B. prepared the
39
40 **15** CPL-1 powders and did all high-pressure gas sorption experiments. J.D., U.R. and K.K. did all
41
42 **16** mechanical tests. J.D. M.B. and S.F. analyzed the data and wrote the manuscript. All authors
43
44 **17** discussed the results and commented on the manuscript.
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49 **18 ACKNOWLEDGMENT**
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