



HAL
open science

Fluid-particle suspension by gas release from a granular bed

Tess Homan, Valérie Vidal, Clément Picard, Sylvain Joubaud

► **To cite this version:**

Tess Homan, Valérie Vidal, Clément Picard, Sylvain Joubaud. Fluid-particle suspension by gas release from a granular bed. *Physical Review Fluids*, In press, 10.1103/PhysRevFluids.00.004300 . hal-02948990v1

HAL Id: hal-02948990

<https://hal.science/hal-02948990v1>

Submitted on 25 Sep 2020 (v1), last revised 29 Nov 2020 (v2)

HAL is a multi-disciplinary open access archive for the deposit and dissemination of scientific research documents, whether they are published or not. The documents may come from teaching and research institutions in France or abroad, or from public or private research centers.

L'archive ouverte pluridisciplinaire **HAL**, est destinée au dépôt et à la diffusion de documents scientifiques de niveau recherche, publiés ou non, émanant des établissements d'enseignement et de recherche français ou étrangers, des laboratoires publics ou privés.

Fluid-particle suspension by gas release from a granular bed

Tess Homan,^{1,2} Valérie Vidal,¹ Clément Picard,¹ and Sylvain Joubaud^{1,3}

¹*Univ Lyon, ENS de Lyon, Univ Claude Bernard,
CNRS, Laboratoire de Physique, F-69342 Lyon, France*

²*Mechanical Engineering, Eindhoven University of Technology, Eindhoven, The Netherlands*

³*Institut Universitaire de France (IUF)*

(Dated: August 19, 2020)

We have studied experimentally particle suspension when injecting a gas at the bottom of an immersed granular layer confined in a Hele-Shaw cell. This work focuses on the dynamics of particles slightly denser than the surrounding fluid. The gas, injected at constant flow-rate, rises through the granular bed then forms bubbles which entrain particles in the above liquid layer. The particles settle down on the edges of the cell, avalanche on the crater formed at the granular bed free surface, and are further entrained by the continuous bubbling at the center. We report the existence of a stationary state, resulting from the competition between particle entrainment and sedimentation. The average solid fraction in the suspension is derived from a simple measurement of the granular bed apparent area. A phenomenological model based on the balance between particle lift by bubbles at the center of the cell and their settling on its sides demonstrates that most of the particles entrained by bubbles come from a global recirculation of the suspension.

I. INTRODUCTION

Recently, there has been a growing research interest for multiphase flows, as their understanding is one of the grand natural and industrial challenges in fluid dynamics [1]. Among the multitude of geophysical flows, gas release in a particle-laden fluid is a widespread phenomenon which may have drastic consequences on the environment [2]. On the one hand, the understanding of methane production and transport in sedimentary basins and its subsequent release is crucial in terms of climate change and global warming [3–5]. On the other hand, exsolved volatiles rising through crystal-rich magmas strongly influence volcanic eruption dynamics [6–8]. Quantifying the mechanisms leading to such resuspension and the generated turbidity current is also essential for the effects of human activities of the production of crude oil from the Canadian oil sands [9] and deep-sea mining [10]. In the industry, catalytic gas-fluidized bed reactors have been widely investigated for the optimization of chemical processes [11–13]. In most of these applications, the interplay between the gas and the particles is one of the key parameters of the global dynamics of such multiphase flow. Therefore, understanding and quantifying the ability of gas to entrain and maintain particles in suspension is a question of paramount importance.

To tackle this question, we consider particle entrainment immersed granular beds. The resuspension of particles forming this solid-like settled state and the induced erosion, chimney or crater formation have been investigated using different mechanisms such as shearing flow [14, 15], impact of liquid jets [16–19], thermal convection or plume emission [20–24], underground cavity collapse [25], fluidization [26], etc. The present paper focuses on gas release from a granular bed, a scenario highlighted in the above applications. In the past years, two classes of model systems have been developed to exhibit the physical mechanisms at stake in such three-phase flows, where the coupling between the grains, gas and liquid may have a strong impact on the global dynamics. On the one hand, to remove or neglect the effect of gravity, experiments have been performed in horizontal setups and/or using isodense particles [27–35]. On the other hand, buoyancy-driven systems have mostly focus on gas patterns in a dense granular bed, with particles much heavier than the surrounding fluid [36–43]. Depending on the gas injection flow rate or pressure and the local solid fraction, the gas may either percolate through the grains or fracture the bed. At the grain free surface, the successive ejection of gas bubbles entrains particles in the liquid. The competition between the particle lift and sedimentation leads at long time to a crater formation [39].

In the present paper, we study experimentally the global characteristics of the suspension formed by particles slightly heavier than the surrounding fluid which are entrained by continuous gas injection. In particular, we focus on the balance between entrainment by the bubble rise and sedimentation. The goal is to identify and quantify the controlling parameters of the extension and average solid fraction of the suspension. We demonstrate that this latter can be estimated at each time from the size of the granular bed which remains at the cell bottom. We then quantify the existence and properties of a steady state when varying the cell geometry and particles properties. We finally propose a simple model based on the balance between entrainment and sedimentation which unravels the particle entrainment mechanism in the stationary state.

The manuscript is organized as follows. After a description of the experimental set-up (section II), the analysis of the experimental results and the influence of the various parameters is presented in section III. In a second stage, the

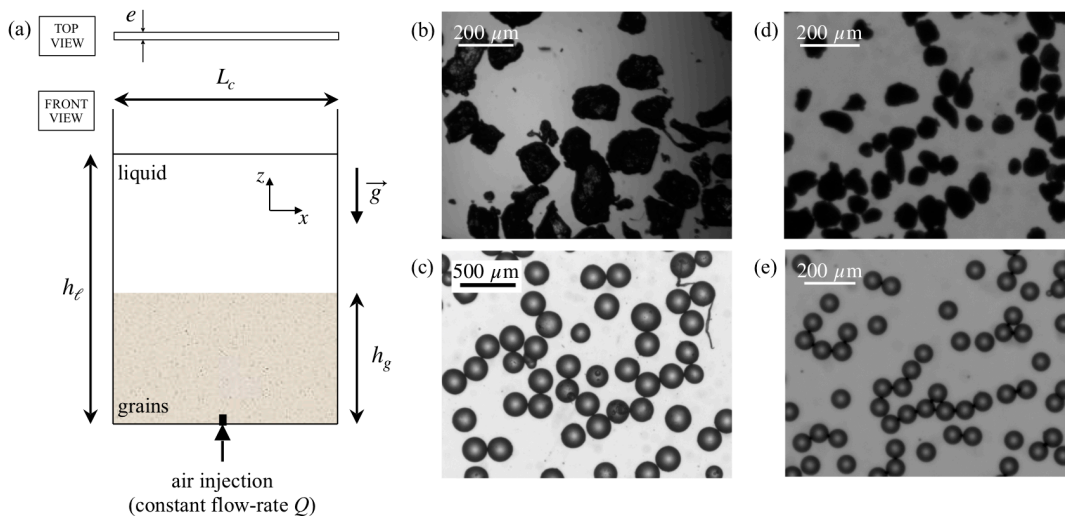


FIG. 1. (a) Schematic view of the experimental setup. Air is injected at constant flow rate Q at the bottom of an immersed granular layer in a Hele-Shaw cell (see text). The subsequent suspension and the remaining granular bed are observed using shadowgraphy. The different notations of the geometrical parameters are indicated. On the right, images of different batches of grains (see Table I): (b) non spherical polydisperse polystyrene beads (PS 130P); (c) spherical monodisperse polystyrene beads (PS 250M); (d) non spherical polydisperse PVC beads (PVC 110P); (e) spherical monodisperse PS beads (PS 80M).

different ingredients of a simple model are presented in section IV and its predictions compared to the experimental results in section V. Finally, we conclude and draw some perspectives in section VI.

II. EXPERIMENTAL SETUP

The experimental setup, sketched in figure 1(a), consists of a vertical Hele-Shaw cell of height 30 cm, width L_c ($L_c = 13.6, 24$ or 35.6 cm) and gap e ($e = 2$ or 3 mm). The cell is filled with ethanol (absolute, Merck Millipore, density $\rho_\ell = 789$ kg/m³, viscosity $\mu = 1.2 \times 10^{-3}$ Pa.s) and beads of either polystyrene (PS, density $\rho_g = 1059$ kg/m³) or polyvinyl chloride (PVC, density $\rho_g = 1379$ kg/m³), with different size and shape (typical diameter d , monodisperse (M) or polydisperse (P), see Table I). Images of the different batches are displayed on figure 1b-e. Note that the use of ethanol prevents the formation of particles aggregates. Air is injected at constant flow-rate Q at the bottom of the cell through a central gas-inlet (inner diameter 1 mm). The flow-rate is varied between $Q = 0.013$ and 1.5 L/min by means of a mass-flow controller (Bronkhorst, Mass Stream D-5111 for $0.01 \leq Q \leq 0.05$ L/min and D-6311 for $0.05 \leq Q \leq 2$ L/min). A reproducible initial condition is obtained by mixing the particles and the liquid with a strong air flow-rate (2 L/min) for 3 minutes. The air flow is then turned off and the particles left to sediment gently, leading to a homogeneous loose-packing initial bed. As expected, the obtained solid fraction, φ_b^0 for the monodisperse spherical particles corresponds to a random loose packing situation [44] (Table I). Note that φ_b^0 is much smaller for polydisperse non-spherical angular particles, for which the bed is in a very loose state [45] (Table I). The initial bed height, h_g , is varied up to 10 cm and the liquid height is adjusted to a given value $h_\ell > h_g$ (see Fig. 1(a)). The ratio h_ℓ/h_g lies in the range 1.2–4.

The setup is illuminated from behind by a strong homogeneous backlight (Dalle LED, Euroshopled). Shadowgraph imaging of the container, the granular bed and the suspension is performed using a camera (PixeLINK, PL-B741U) capturing images at 1 Hz. A contour detection, based on intensity thresholding, makes it possible to infer the granular bed area A , and thus its volume Ae , for each image, and get its temporal evolution during each experiment. We denote A_0 the initial bed area and $h_g = A_0/L_c$ the initial bed height. Finally, bubble contour detection is performed in the suspension in the stationary regime, to quantify the typical bubble size (see section V A).

particles	provider	shape	distribution	$\Delta\rho$ [kg/m ³]	d [μm]	φ_b^0 [%]	$U_s = \frac{\Delta\rho g d^2}{18\mu}$ [mm/s]	$\text{Ar} = \rho_\ell U_s d / \mu$
PVC 110P	Goodfellow [®]	non spherical	polydisperse	590	110 ± 50	41.9 ± 0.5	3.2	0.23
PS 130P	Goodfellow [®]	non spherical	polydisperse	270	130 ± 80	42.0 ± 0.5	2.1	0.18
PS 250M	Dynoseeds [®]	spherical	monodisperse	270	230 ± 10	56.2 ± 0.5	6.5	0.98
PS 80M	Dynoseeds [®]	spherical	monodisperse	270	80 ± 5	57.8 ± 0.5	0.8	0.04

TABLE I. Characteristics of the polystyrene (PS) or polyvinyl chloride (PVC) beads used in the experiments. $\Delta\rho = \rho_g - \rho_\ell$ is the density difference between the particles and the fluid, d the typical particle diameter and φ_b^0 the initial bed solid fraction (see text). $U_s = \Delta\rho g d^2 / (18\mu)$ is the Stokes (settling) velocity of a single particle of typical diameter d in a fluid of viscosity μ (see section IV). $\text{Ar} = \rho_\ell U_s d / \mu$ is the Archimedes number, which corresponds to the particle Reynolds number based on the Stokes velocity U_s .

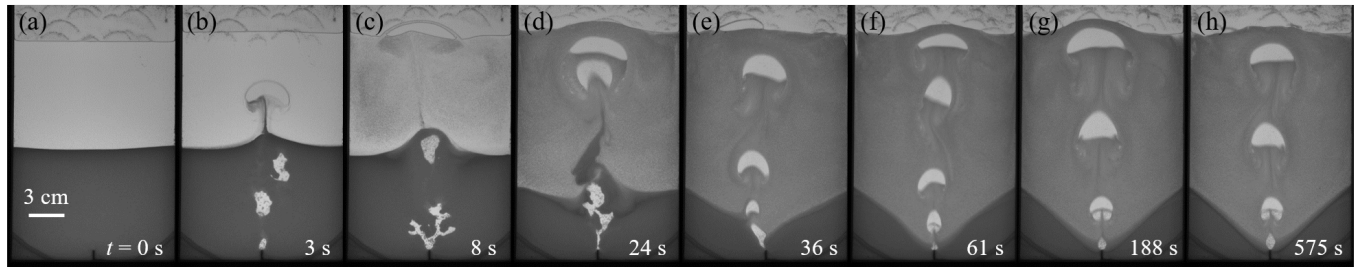


FIG. 2. Temporal evolution of the bed and suspension [PS 130P, $Q = 200$ mL/min, $h_g = 10 \pm 0.2$ cm, $h_\ell = 20 \pm 0.2$ cm, $L_c = 13.6$ cm, $e = 2$ mm]. (a) Initial loose-packing bed. (b)-(c) After turning on the gas injection, air rises through the granular bed and forms bubbles which entrain particles in their wake in the above liquid layer. (d)-(e) A crater grows and the suspension becomes denser. (f-h) The system reaches a stationary state in which the volume of the granular bed and the average solid fraction of the suspension remains constant.

III. EXPERIMENTAL RESULTS

A. Phenomenology

Figure 2 displays a typical experiment, where a time lapse shows the evolution of the granular bed and the suspended particles. At $t = 0$ s, air is injected at constant flow rate Q at the bottom of the immersed granular bed. The gas initially invades the granular bed, then air bubbles escape and rise through the above liquid layer, entraining particles in their wake [Figs. 2(b)-(c)]. This process leads to the formation of a crater which size increases in time [Figs. 2(c)-(f)]. When the particles deposit on the inner part of the crater, they avalanche back to the center and are further entrained by the continuous gas injection. The system finally reaches a stationary state (Fig. 2(f-h)) characterized by a *suspension*, resulting from the balance between particles lifted by gas bubbles and sedimentation; and a *granular bed*, corresponding to the particles which are not entrained by the gas flow. Note that a small transition region exists between the granular bed and the suspension, corresponding to the avalanching particles, slightly less dense than the granular bed. Its size is at most a few percent of the granular bed's and is included in the bed area, A , by our thresholding method.

To investigate carefully the existence and the characteristics of this stationary state, experiments have been run for a wide range of experimental parameters. Typical snapshots are shown in figure 3 for different flow rates Q and cell width L_c . At constant L_c , when increasing Q , we observe that the area occupied by the granular bed decreases and the suspension becomes darker, confirming that its volume fraction increases. In addition, the typical width occupied by the suspension, denoted as L_s , increases until it reaches the lateral boundaries of the cell, L_c . In most of our experiments, $L_s \simeq L_c$. In this work, except when explicitly mentioned, we will focus on this configuration only. While we retrieve the typical crater shape with two dunes reported by [39] for small Q and large L_c (top-left snapshot in figure 3), the flank of the crater is limited by the cell boundary for large Q and/or small L_c .

The crater and suspension characteristics in the stationary state does not depend on the finite width of the cell only, but also on the number and type of particles and the volume of liquid available above the granular bed. The influence of these parameters is presented in the supplementary materials (see A), showing typical snapshots of the stationary state when changing the granular bed height h_g , the total height of the liquid h_ℓ and the batch of particles. It can be seen that both h_ℓ and h_g have an effect on the intensity, and therefore, the volume fraction of the suspension.

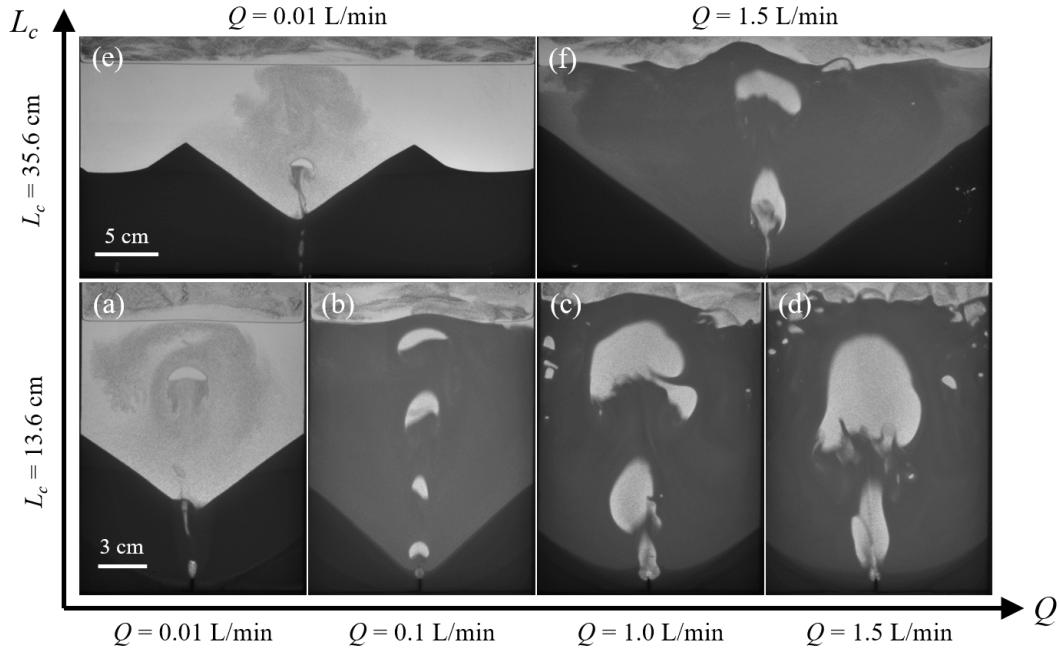


FIG. 3. Snapshots of the experiment in the stationary regime for different values of the flow rate Q and different cell width L_c [PVC 110P, $h_g = 9 \pm 0.5$ cm, $h_\ell = 18 \pm 0.5$ cm]. The thickness of the cell is $e = 2$ mm for the lower panel [$L_c = 13.6$ cm] and $e = 3$ mm for the upper panel [$L_c = 35.6$ cm].

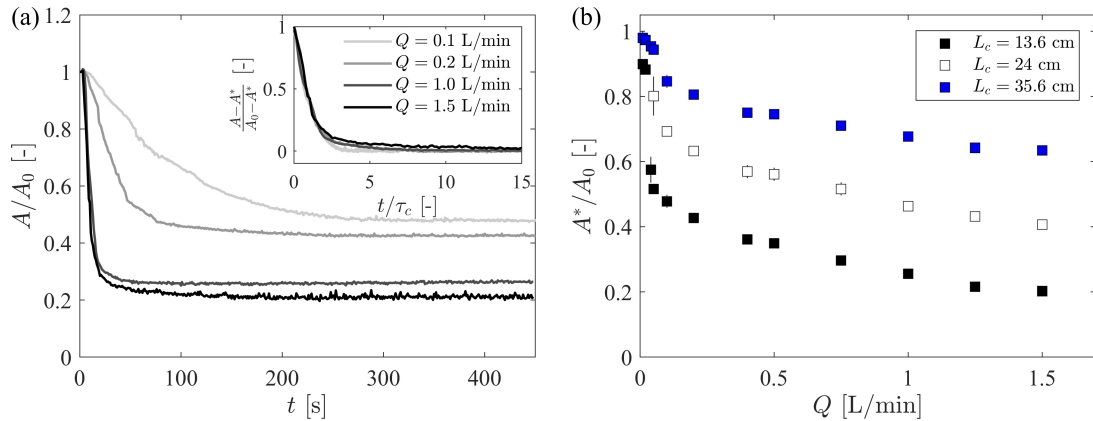


FIG. 4. (a) Temporal evolution of the bed normalized area, A/A_0 for different air flow-rate Q (decreasing for light gray to dark gray). Experimental parameters are those given in the caption of figure 3 [PVC 110P, $h_g = 9 \pm 0.5$ cm, $h_\ell = 18 \pm 0.5$ cm, $L_c = 13.6$ cm, $e = 2$ mm]. Inset: Normalized plot, $(A - A^*) / (A - A_0)$, as a function of t/τ_c . (b) Bed normalized area in the stationary state, A^*/A_0 , as a function of the injected air flow-rate Q for different cell width. [$e = 2$ mm for $L_c = 13.6$ cm and 24 cm and $e = 3$ mm for $L_c = 35.6$ cm]

However, no clear trend can be highlighted. Finally, as expected, the small particles (PS80 M) are more easily put into suspension than larger particles (PS 250M) (Figure 10).

B. Temporal evolution and quantitative measurement of the granular bed size

Figure 4(a) displays the temporal evolution of the normalized bed volume (or area), A/A_0 , defined as its surface A times the cell gap e , relative to the initial bed volume, $A_0 e$. For different air injection flow rates Q (increasing from 0.1 L/min to 1.5 L/min), the system always reaches a stationary regime in which the volume of the granular bed remains constant. The final area of the bed is denoted A^* . As expected, the characteristic time τ_c to reach the

steady state for A/A_0 decreases when increasing Q . Such behavior was previously reported for the fluidization of heavy particles bed ($d \sim 3$ mm, $\rho_g = 2230$ kg/m³) in two-phase systems [46]. The normalized plot $(A - A^*)/(A - A_0)$ as a function of t/τ_c is displayed as an inset of Figure 4(a) and shows that all the curves collapse on the same master curve, indicating that the dependence of τ_c with Q is related to the dependence of A^* with Q . In the present paper, we focus only on the characteristics of the granular bed and the suspension in the stationary regime. In the following, the quantities in the stationary state are denoted with $*$.

To quantify the phenomenological observations, the final volume of the granular bed is displayed in figure 4(b) as a function of the flow rate for different values of the cell width L_c . For each cell width, A^*/A_0 decreases with Q . It drops abruptly at small flow rates $Q < 250$ mL/min, while for $Q > 250$ mL/min, the size of the granular bed decreases gently. In addition, the decrease of A^*/A_0 as a function of Q is more abrupt for small cell width. Thus, more particles remain in the granular bed when increasing the flow-rate for large L_c compared to small L_c . This result can be easily explained, since for large L_c , most particles are further to the injected point and a larger flow rate is necessary to reach them. In addition, when the particles are resuspended into the fluid, they have a larger volume they can occupy for a large cell that for a small cell. The solid fraction of the induced suspension is therefore also smaller for large L_c .

C. Mean solid fraction of the suspension

As underlined in the introduction, an important quantity is the number of particles in the particle-laden liquid above the granular bed. In the previous section, we qualitatively comment on the solid fraction of the suspension. Here, we present a quantitative method to compute the mean solid fraction φ_s^* of the suspension from the measurement of the final bed size A^*/A_0 using mass conservation. The total number of particles in the suspension, denoted N_s^* , occupies a volume $V_s^* = A_s^*e$, where A_s^* is the area occupied by the suspension. The mean solid fraction of the suspension can therefore be written as $\varphi_s^* = N_s^*V_g/V_s^*$, where $V_g \simeq (4/3)\pi(d/2)^3$ is the typical grain volume. The final bed size, A^*/A_0 , and φ_s^* are not independent variable, since they are directly linked by the particles mass conservation. Indeed, the number of grains N_g is fixed in the experiment and can be computed using the bed area in the initial state (figure 5a). In the stationary state (figure 5b), it can be decomposed into two populations: N_{bed}^* particles that are still in the granular bed, while N_s^* particles have been lifted in suspension, such that

$$N_g = N_{\text{bed}}^* + N_s^*. \quad (1)$$

Using the definition of the solid fraction, one can get

$$\varphi_b^0 A_0 = \varphi_b^* A^* + \varphi_s^* A_s^*. \quad (2)$$

where φ_b^* is the solid fraction of the granular bed in the stationary state. At the beginning of the experiment, we observe a quick compaction by a few percent of the granular bed. This observation can be related to the compaction reported classically for dry or granular beds under mechanical vibration, which are here triggered by the upward flow [47]. After this quick compaction, the bed packing remains constant. To get an estimate of the volume occupied by the suspension, a typical sketch of the stationary state regime is proposed in figure 5c). The liquid height in the stationary state h_ℓ^* is larger than in the initial condition due to the presence of the bubbles. Moreover, in most of the experimental configurations presented in the present paper, the suspension has reached the side boundaries of the cell. In the following, we consider only data for which $L_s \simeq L_c$. The volume occupied by the suspension is therefore equal to $h_\ell^* L_c e - A^* e - V_{\text{Bubbles}}$, where the final volume of the granular bed $A^* e$ and the volume of the bubbles V_{Bubbles} have been subtracted to the total volume $h_\ell^* L_c e$ occupied by the system. Since the liquid is incompressible, $h_\ell^* L_c e - V_{\text{Bubbles}}$ is simply equal to $h_\ell L_c e$. After some algebra, one gets the solid fraction in the suspension, in the stationary regime, as a function of A^*/A_0 :

$$\varphi_s^* = \frac{\varphi_b^0 - (A^*/A_0)\varphi_b^*}{(h_\ell/h_g) - (A^*/A_0)}. \quad (3)$$

This estimate can be compared to a more direct measurement of the number of particles in the suspension. At the end of the experiment, the air flow is turned off and all the particles in suspension sediment in loose packing granular bed with the same solid fraction of the initial state, φ_b^0 . Since φ_b^0 and φ_b^* are slightly different, two regions in this final granular state can be distinguished (figure 5d): the granular bed of size A^* and the bed formed by the particles previously in suspension of size A_s^{sed} . The solid fraction in the latter bed is equal to

$$\varphi_b^0 = \frac{N_s^* V_g}{A_s^{\text{sed}} e} \quad (4)$$

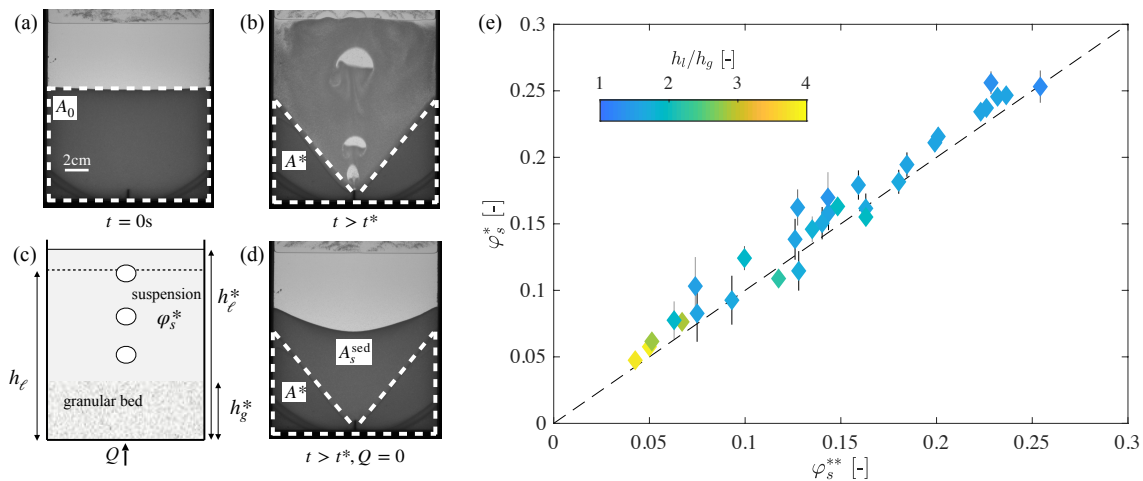


FIG. 5. Snapshots of the experiments just after turning on the flow rate (a) and in the stationary regime (b). [PS 130P; $Q = 100$ mL/min; $L_c = 13.6$ cm; $e = 2$ mm; $h_g = 9.3 \pm 0.5$ cm; $h_\ell = 14.4 \pm 0.5$ cm] (c) Schematic view of the mass conservation model used to compute the solid fraction, of the suspension. (d) Snapshots of the experiments after turning off the flow rate. (e) solid fraction of the suspension φ_s^* , computed using the mass conservation model (eq. 3), as a function of φ_s^{**} , computed using the number of particles that have sedimented after turning off the flow rate for different ratio h_ℓ/h_g . The error bars corresponds to the estimation of the compaction of the granular bed ($\phi_b^* = (1.05 \pm 0.05)\phi_b^0$). The dashed line corresponds to the first bisector.

Using Eq. 4 and the expression of the volume occupied by the suspension as a function of A^* , one can get a second estimate of the solid fraction of the suspension, denoted φ_s^{**} , as

$$\varphi_s^{**} = \frac{N_s^* V_g}{V_s^*} = \varphi_b^0 \frac{A_s^{\text{sed}}}{h_\ell L_c - A^*}. \quad (5)$$

Figure 5(d) displays the solid fraction measured in the stationary state, φ_s^* as a function of the one computed at the end of the experiment, φ_s^{**} for different values of the height ratio, h_ℓ/h_g . As expected, all the data points collapse on the first bisector within experimental error bars, showing that the two estimations are in very good agreement, which validates the computation of the suspension solid fraction using the bed final size. For all experiments, we can thus determine the average solid fraction in the suspension, φ_s , at all time. In the following sections, we focus on the stationary state, where this solid fraction is denoted φ_s^* .

IV. PHENOMENOLOGICAL MODEL

In this section, we propose a phenomenological model to explain the dependence of the spatial average solid fraction in the suspension, φ_s , on the experimental parameters. In the stationary state, the suspension results from the balance between grains advected by the bubbles rising in the above liquid layer, and particles settling on the sides. The following subsections propose an expression of the number of particles sedimenting on the sides of the cell (sec. IV A) or entrained by the bubbles at the centre (sec. IV B), with a final expression of the suspension average solid fraction in the stationary state, φ_s^* , resulting from the competition between both mechanisms (sec. IV C).

A. Particle settling

Let us note dN^+ the particles in a volume dV^+ of the suspension settling on the granular bed during the time interval dt (Figure 6a, dark gray zones on the suspension sides).

$$dN^+ = \varphi_s \frac{dV^+}{V_g} = \varphi_s \frac{(L_s - L_b)eU_p dt}{V_g} \quad (6)$$

where V_g is the volume of a single grain, φ_s the solid fraction of the suspension and U_p the particle settling velocity. As a reminder, L_s represents the typical width occupied by the suspension, which reaches the lateral boundaries of

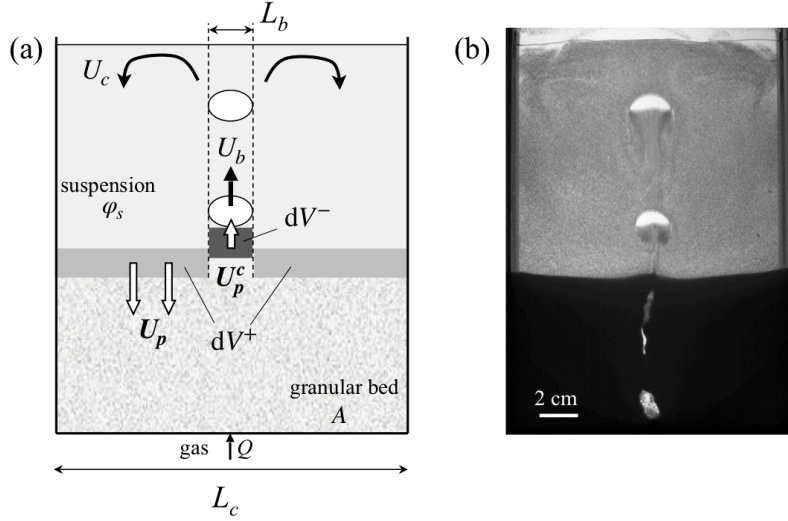


FIG. 6. (a) Sketch of the fluid-particle suspension by gas injection (phenomenological model, see section IV). Gas is injected at constant flow-rate Q at the bottom center of the cell and crosses the granular bed. Bubbles rising in the above liquid layer (velocity U_b) entrain particles upwards in the central column (width L_b) and form a suspension of width L_s which is of the order of L_c in all the data discussed in section IV. Particles on both sides settle due to both sedimentation and fluid recirculation (see text). (b) Picture of bubbles rising out of the granular bed entraining particles in its wake [PVC 110P, $h_g = 9$ cm, $h_\ell = 18$ cm, $Q = 0.05$ L/min; $L_c = 13.6$ cm, $e = 2$ mm].

the cell in all the data that will be discussed in this model, so that $L_s \approx L_c$. The particle sedimentation velocity U_p can be expressed using the relative velocity between a particle and the surrounding suspension which is often written as [48–50]

$$U_p - U = U_s(1 - \varphi_s)^5. \quad (7)$$

$$(8)$$

Since the Archimedes number Ar , which corresponds to the particle Reynolds number based on the Stokes velocity $U_s = \Delta\rho g d^2 / (18\mu)$, is smaller than 1 (see Table I), the Stokes velocity U_s is the pertinent settling velocity and the exponent 5 corresponds to the correction due to collective effects [51, 52]. The velocity U corresponds to the velocity of the suspension, which is the volume average velocity, and takes into account the velocity of the particles U_p and the velocity of the fluid U_c due to the recirculation generated by the rising bubbles:

$$U = \varphi_s U_p + (1 - \varphi_s) U_c. \quad (9)$$

Using mass conservation, the average fluid velocity given by the recirculating flow is $U_c = U_b L_b / (L_s - L_b)$. The particle velocity on the cell sides can therefore be written $U_p = U_c + U_s(1 - \varphi_s)^4$ and leads to an expression for the number of particles settling on the granular bed during dt :

$$dN^+ = \varphi_s \frac{(L_s - L_b)e}{V_g} \left[U_s(1 - \varphi_s)^4 + \frac{U_b L_b}{L_s - L_b} \right] dt. \quad (10)$$

B. Entrainment

Let us note dN^- the particles entrained during the same time interval dt (Figure 6a, black zone in the central column). The particles entrained can come either from the granular bed, or from the recirculating suspension. We thus write:

$$dN^- = (\chi_s \varphi_s + \chi_b \varphi_b) \frac{L_b e U_p^c dt}{V_g} \quad (11)$$

where χ_s and χ_b are coefficients representing the fraction of particles entrained from the suspension, χ_s , or the granular bed, χ_b , and U_p^c is the particle velocity in the bubble's wake. This latter can be written, as previously for the particles on the cell sides, as the velocity composition between the fluid, equal to the bubble rising velocity U_b in the central column, and the term due to particle sedimentation:

$$U_p^c - U^c = U_s(1 - \varphi_s)^5 \quad (12)$$

in which U^c is the velocity of the suspension in the central region and is given by an average between the velocity of the particle U_p^c and the fluid velocity, equal to the bubble velocity U_b :

$$U^c = \varphi_s U_p^c + (1 - \varphi_s) U_b. \quad (13)$$

The combination of the two previous equations leads to

$$U_p^c = U_b - U_s(1 - \varphi_s)^4. \quad (14)$$

The number of particles entrained during a time interval dt is therefore

$$dN^- = (\chi_s \varphi_s + \chi_b \varphi_b) \frac{L_b e}{V_g} [U_b - U_s(1 - \varphi_s)^4] dt. \quad (15)$$

C. Stationary state

In the stationary state, $dN^+ = dN^-$. We introduce the dimensionless variables $\ell = L_b/L_s$ and $u = U_b/U_s$. Note that the parameter u represents the inverse of a Rouse number defined as the velocity ratio between the entraining, rising fluid and the sedimentation of a single particle. After some algebra, one gets the following relation for φ_s^* , the solid fraction in the suspension in the stationary regime:

$$\varphi_s^* = (\chi_s \varphi_s^* + \chi_b \varphi_b^*) \frac{u - (1 - \varphi_s^*)^4}{u + \frac{1-\ell}{\ell}(1 - \varphi_s^*)^4}. \quad (16)$$

V. PARTICLE SUSPENSIONS

In this section, we compare the average solid fraction of the suspension inferred from experimental measurements of A^*/A_0 , in the stationary regime (equation 3), with the model prediction of its variation upon u , ℓ and φ_b^* (equation 16). In section V A, we propose an estimation of the bubble typical size and velocity. χ_s and χ_b are *a priori* unknown and will be discussed in section V B.

A. Typical bubble size & velocity

In confined geometry, previous studies have shown that the thickness of the lubrication film between the bubble and the wall is given by $e_f/e \sim \text{Ca}^{2/3}/(1 + \text{Ca}^{2/3})$, where $\text{Ca} = \mu U_b/\sigma$ is the capillary number [53, 54] and $\sigma \simeq 22$ mN/m the air/ethanol surface tension at room temperature. In our experiments, a rough estimate of the bubble velocity is $U_b \sim 10$ cm/s, leading to $e_f/e \ll 1$. We can therefore estimate the bubble volume as their apparent surface S , computed from the images, multiplied by the cell gap e . The typical bubble size can then be estimated as its equivalent diameter, $L_b = \sqrt{4S/\pi}$.

Figures 7a,b display histograms of bubble population for PVC particles, at two different flow rates, in the stationary regime. The picture in inset of each figure shows an example of bubble contour detection (in blue). For $Q > 0.3$ L/min, a population of small bubbles appear jointly with the larger bubbles. The maxima of each distribution is picked and reported in figure 7. The small bubble equivalent diameter, L_b^s , remains roughly constant and of the order of 4.5 mm as a function of the gas flow-rate Q . They are generated by bubble fragmentation and almost always on the sides of the central vertical line above the injection nozzle. Consequently, they do not play any significant role in particle entrainment in the central zone, and will be further ignored. The larger bubble size increases as the square root of the flow-rate, here $L_b = 0.38 + 2.9\sqrt{Q}$ for the PVC 110P. This dependence on \sqrt{Q} does not seem to vary significantly when changing the particles, and is not directly governed by gravity either, as pointed out by previous experiments with PVC particles in tilted cells [55].

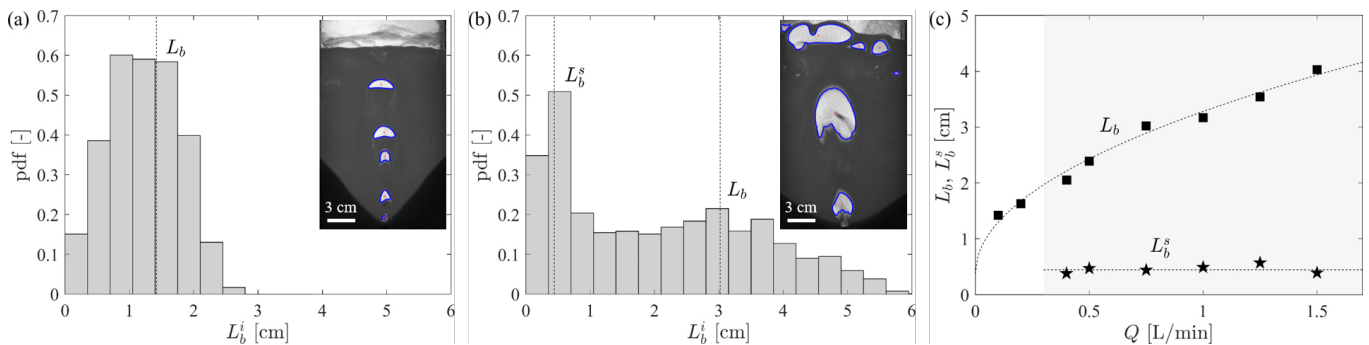


FIG. 7. (a,b) Probability density function of the bubble equivalent diameter (L_b^i indicates the equivalent diameter for bubble i) in the stationary regime. The inset displays a snapshot of the corresponding image sequence with bubble contour (blue line) and center of mass (red cross) determination. (a) At low flow rate [$Q = 0.1$ L/min], the bubble population displays a single characteristic size L_b . (b) At high flow rate [$Q = 0.75$ L/min], small bubbles resulting from bubble fragmentation appear, with a typical size L_b^s . (c) Equivalent bubble diameter as a function of the flow rate Q . For $Q > 0.3$ L/min, we observe two bubble populations (corresponding to the two peaks in (b)). Small bubbles are roughly constant in size (horizontal dashed line) while large bubbles follow $L_b = 0.38 + 2.9\sqrt{Q}$ (increasing dashed line). [PVC 110P; $L_c = 13.6$ cm; $e = 2$ mm; $h_g = 9.3 \pm 0.5$ cm; $h_\ell = 18 \pm 0.5$ cm]

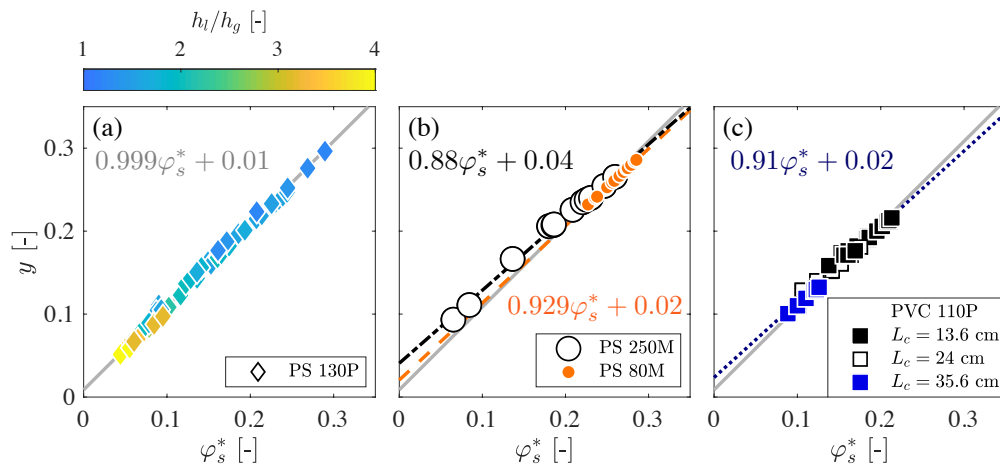


FIG. 8. Parameter y as a function of φ_s^* (see text). Following the prediction of the phenomenological model, $y = \chi_s\varphi_s^* + \chi_b\varphi_b^*$ where χ_s and χ_b depend on the nature of the particles only. (a) PS 130P for different h_ℓ/h_g (cf. colorscale) [$L_c = 13.6$ cm, $e = 2$ mm]. The solid gray line indicates the linear fit (reported on b,c for comparison), whose equation is indicated in gray on the figure. (b) PS 250M and PS 80M [$h_g = 9$ cm, $h_\ell = 18$ cm, $L_c = 13.6$ cm, $e = 2$ mm]. Dashed black (resp. orange) line: linear fit for the PS 250M (resp. PS 80M) particles. The fit equations are indicated in black (resp. orange) on the figure. (c) PVC 110P [$h_g = 9$ cm, $h_\ell = 16$ cm]. All data collapse independently of the cell width L_c (blue dotted line: linear fit, whose equation is indicated in blue). [$e = 2$ mm for $L_c = 13.6$ cm and 24 cm and $e = 3$ mm for $L_c = 35.6$ cm]

The bubble velocity U_b cannot be measured directly in our experiments. Indeed, we capture the stationary state of the suspension over long times, and the acquisition frame rate (1 Hz) is too low to determine the bubble rising speed. From rough observations, we can estimate the bubble velocity between a few and a few tens of centimeters per second. It is of the same order of magnitude as the typical rise time of bubbles in a Hele-Shaw cell filled with water only. Previous works investigated experimentally the velocity of bubbles rising in Hele-Shaw cells and found that, for Reynolds number smaller than 10^3 , as in our experiments, the bubble velocity can be written as $U_b \sim 0.5\sqrt{gL_b}$ [54, 56]. This expression can be interpreted as a simple balance between the buoyancy force and the drag force exerted on the free edges of the bubble, the contribution of the viscous shear stress of the liquid films being negligible [54, 56, 57].

B. Entrainment mechanism

In figure 8, we plot $y = \varphi_s^* / \left[\frac{u - (1 - \varphi_s^*)^4}{u + \frac{1-\ell}{\ell}(1 - \varphi_s^*)^4} \right]$ as a function of φ_s^* . Our experiments have a range of the two parameters ℓ and u of $0.019 < \ell < 0.31$ and $24 < u < 427$ respectively. As predicted by the phenomenological model, for a given type of particles, all data collapse on a linear trend, $\chi_s \varphi_s^* + \chi_b \varphi_b^*$. This result is independent of the height ratio h_ℓ/h_g (Figure 8a) or of the cell width (Figure 8c), as long as $L_s \simeq L_c$ (see section IV). The different coefficients of the linear trend depend on the different batches of grains as indicated by the fit equations provided for all data sets in Figure 8. The model therefore predicts well, at first order, the behavior of the suspension. Interestingly, for all particles, we find $\chi_s \gg \chi_b$, with χ_s of the order of 90–99 % and χ_b of the order of 2–7%. This means that, in the stationary regime, the majority of the particles forming the suspension come from the global recirculation, and not from particles which have settled in the bed and are later extracted and entrained by the bubbles. PS 250M (black dotted line in figure 8b) and PS 130P (gray thick line in figures 8a,b) clearly follow a different linear trend. Several features can explain this difference: the particle different size (see Table I), shape (angular vs. spherical, see figure 1b,c) or polydispersity (monodisperse PS 250M vs. polydisperse PS 130P, see Table I). Figure 8b compares two different sizes of the same monodisperse, polystyrene particles, PS 250M and PS 80M. Although a difference in the linear trend seem to appear, with PS 80M being closer to PS 130P particles trend (gray solid line, figure 8b), it is difficult at this point to conclude univocally. Indeed, the PS 80M particles are easily entrained and sediment very slowly (see Stokes velocity, Table I) and it was impossible, in our experimental conditions, to form suspensions with $\varphi_s^* < 20\%$. Similarly, although the linear trends characterizing the PS 130P and PVC 110P particles appear slightly different (figure 8c), they cannot be distinguished unambiguously due to the difficulty to span a large range of φ_s^* for PVS 110P. Therefore, within the experimental error bars, we cannot conclude with the present work on the dependence of the parameters (χ_s, χ_b) on the particle sedimentation velocity or polydispersity.

VI. CONCLUSION

In this paper, we have explored experimentally the resuspension of particles of an initial loose packing immersed granular bed. We have observed that continuous air injection at the bottom of the granular bed leads to a final steady state for different sets of controlling parameters. This final steady state is made of a crater-shaped final granular bed and a more or less homogeneous suspension formed by the particles entrained in the above liquid layer by the gas bubbles emerging from the granular bed. The final global characteristics of the suspension is quantified by its spatial-averaged solid fraction, which is computed using the final granular bed volume based on mass conservation. We have finally proposed a phenomenological model for the steady state, reflecting the balance between the entrainment of particles by the air bubbles and their settling on the sides of the experimental cell. This model captures with a good agreement the main features of this resuspension mechanism using empirical laws for the gas bubbles size and velocity. Moreover, we have shown that the suspension is almost “self-sustained”, meaning that almost all the particles entrained by the air bubbles come from a global recirculation mechanism and therefore do not go back into the granular bed. Only a few percent of particles settle and are further extracted from the granular bed.

Even if the phenomenological model gives interesting insights on the behavior of suspension generated by gas release, it cannot be predictive. Indeed, it strongly depends on the behavior of the gas bubbles which depends in particular on the suspension itself. As underlined in [58], bubbles are still a challenge for scientists to understand and/or control their behavior in many complex situations. The effect of the suspension on the dynamics of bubbles is beyond the scope of this paper. It would also be interesting to study not only the global behavior of the suspension but also the local evolution of the solid fraction since the inhomogeneities may be very large. These perspectives shall be the topic of future studies.

ACKNOWLEDGEMENTS

We thank D. Bénâtre for insightful discussions. This work was supported by the LABEX iMUST (ANR-10-LABX-0064) of Université de Lyon, within the program "Investissements d'Avenir" (ANR-11-IDEX-0007) operated by the French National Research Agency (ANR).

[1] T. Dauxois *et al*, Confronting Grand Challenges in Environmental Fluid Dynamics., submitted (2019).

- [2] J. Olsen and P. Skjetne, Current Understanding of Subsea Gas Release: A Review., *The Canadian Journal of Chemical Engineering* **94**, 209 (2016).
- [3] A. Judd, M. Hovland, L. Dimitrov, S. Garcia-Gil, and V. Jukes, The geological methane budget at Continental Margins and its influence on climate change., *Geofluids* **2**, 109 (2002).
- [4] H. Svensen, S. Planke, A. Malthes-Sorensen, B. Jamtveit, R. Myklebust, T. Eidem, and S. Rey, Release of methane from a volcanic basin as a mechanism for initial Eocene global warming., *Nature* **429**, 542 (2004).
- [5] L. Naudts, J. Greinert, Y. Artemov, S. Beaubien, C. Borowski, and M. D. Batist, Anomalous sea-floor backscatter patterns in methane venting areas, Dnepr paleo-delta, {NW} Black Sea., *Marine Geology* **251(3-4)**, 253 (2008).
- [6] J. Sable, B. Houghton, P. D. Carlo, and M. Coltelli, Changing conditions of magma ascent and fragmentation during the Etna 122 BC basaltic Plinian eruption: evidence from clast microtextures., *Journal of Volcanology and Geothermal Research* **158(3-4)**, 333 (2006).
- [7] J. Oppenheimer, A. Rust, K. Cashman, and B. Sandnes, Gas migration regimes and outgassing in particle-rich suspensions, *Frontiers in Physics* **3**, 60 (2015).
- [8] K. Cashman, R. Sparks, and J. Blundy, Vertically extensive and unstable magmatic systems: A unified view of igneous processes., *Science* **355** (2017).
- [9] G. Lawrence, E. Tedford, and R. Pieters, Suspended solids in an end pit lake: potential mixing mechanisms., *Canadian Journal of Civil Engineering* **43**, 211 (2016).
- [10] T. Peacock and M. Alford, Is deep-sea mining worth it?, *Scientific American* **318(5)**, 72 (2018).
- [11] M. Dudukovic, F. Larachi, and P. Mills, Multiphase catalytic reactors : A perspective on current knowledge and future trends., *Catalysis Reviews Science and Engineering* **44(1)**, 123 (2002).
- [12] N. Rados, *Slurry bubble column hydrodynamics.*, Ph.D. thesis, Sever Institute of Washington Technology (2003).
- [13] K. Pangarkar, T. Schildhauer, J. van Ommen, J. Nijenhuis, F. Kapteijn, and J. Moulijn, Structured packings for multiphase catalytic reactors., *Industrial and Engineering Chemistry Research* **47(10)**, 3720 (2008).
- [14] P. Aussilous, J. Chauchat, M. Pailha, M. Medale, and E. Guazzelli, Investigation of the mobile granular layer in bedload transport by laminar shearing flows., *Journal of Fluid Mechanics* **736**, 954 (2013).
- [15] M. Houssais, C. Ortiz, D. Durian, and D. Jerolmack, Rheology of sediment transported by a laminar flow., *Physical Review E* **94**, 062609 (2016).
- [16] S. Badr, G. Gauthier, and P. Gondret, Erosion threshold of a liquid immersed granular bed by an impinging plane liquid jet., *Physics of Fluids* **26(2)**, 023302 (2014).
- [17] B. R. Sutherland and S. Dalziel, Bedload transport by a vertical jet impinging upon sediments., *Physics of Fluids* **26(3)**, 035103 (2014).
- [18] S. Badr, G. Gauthier, and P. Gondret, Crater jet morphology., *Physics of Fluids* **28(3)**, 033305 (2016).
- [19] J. Vessaire and G. Varas and S. Joubaud and R. Volk and M. Bourgoïn and V. Vidal, Stability of a Liquid Jet Impinging on Confined Saturated Sand., *Physical Review Letters* **124**, 224502 (2020).
- [20] D. Martin and R. Nokes, Crystal settling in a vigorously convecting magma chamber., *Nature* **332**, 534–536 (1988).
- [21] V. S. Solomatov, P. Olson, and D. J. Stevenson, Entrainment from a bed of particles by thermal convection., *Earth and Planetary Science Letters* **120**, 387 (1993).
- [22] G. Lavorel and M. L. Bars, Sedimentation of particles in a vigorously convecting fluid., *Physical Review E* **80(4)**, 046324 (2009).
- [23] C. Morize, E. Herbert, and A. Sauret, Resuspension threshold of a granular bed by localized heating., *Physical Review E* **96**, 032903 (2017).
- [24] E. Herbert, C. Morize, A. Louis-Napoléon, C. Goupil, P. Jop, and Y. D'Angelo, Buoyancy-driven destabilization of an immersed granular bed., *Journal of Fluid Mechanics* **834**, 778809 (2018).
- [25] F. Loranca-Ramos, J. Carrillo-Estrada, and F. Pacheco-Vazquez, Craters and Granular Jets Generated by Underground Cavity Collapse., *Physical Review Letters* **115**, 028001 (2015).
- [26] M. Houssais, C. Maldarelli, and J. Morris, Soil granular dynamics on-a-chip: fluidization inception under scrutiny., *Lab Chip* **19(7)**, 1226 (2019).
- [27] O. Johnsen, R. Toussaint, K. J. Måløy, and E. G. Flekkøy, Pattern formation during air injection into granular materials confiner in a circular Hele-Shaw cell., *Physical Review E* **74**, 011301 (2006).
- [28] C. Chevalier, A. Lindner, and E. Clément, Destabilization of a Saffman-Taylor Fingerlike Pattern in a Granular Suspension., *Physical Review Letters* **99(17)**, 174501 (2007).
- [29] O. Johnsen, C. Chevalier, A. Lindner, R. Toussaint, E. Clément, K. J. Måløy, E. G. Flekkøy, and J. Schmittbuhl, De-compaction and fluidization of a saturated and confined granular medium by injection of a viscous liquid or gas., *Physical Review E* **78**, 051302 (2008).
- [30] X. Cheng, L. Xu, A. Patterson, H. Jaeger, and S. Nagel, Towards the zero-surface-tension limit in granular fingering instability., *Nature Physics* **4**, 234 (2008).
- [31] C. Chevalier, A. Lindner, and M. Leroux, Morphodynamics during air injection into a confined granular suspension., *Journal of Non-Newtonian Fluid Mechanics* **158**, 63 (2009).
- [32] B. Sandnes, E. G. Flekkøy, H. A. Knudsen, K. J. Måløy, and H. See, Patterns and flow in frictional fluid dynamics., *Nature Communications* **2** (2011).
- [33] R. Holtzman, M. Szulczewski, and R. Juanes, Capillary fracturing in granular media., *Physical Review Letters* **108**, 264504 (2012).
- [34] N. Hooshyar, J. van Ommen, P. Hamersma, S. Sundaresan, and R. Mudde, Dynamics of Single Rising Bubbles in Neutrally Buoyant Liquid-Solid Suspensions., *Physical Review Letters* **110**, 244501 (2013).

- [35] C. Madec, B. Collin, J. J. S. Jerome, and S. Joubaud, Puzzling bubble rise speed increase in dense granular suspensions., submitted (2020).
- [36] L. Gostiaux, H. Gayvallet, and J.-C. Géminard, Dynamics of a gas bubble rising through a thin immersed layer of granular material : an experimental study., *Granular Matter* **4**, 39 (2002).
- [37] H. Geistlinger, G. Krauss, D. Lazik, and L. Luckner, Direct gas injection into saturated glass beads: Transition from incoherent to coherent gas flow pattern., *Water Resources Research* **42**, W07403 (2006).
- [38] X.-Z. Kong, W. Kinzelbach, and F. Stauffer, Migration of air channels: An instability of air flow in mobile saturated porous media., *Chemical Engineering Science* **64**, 1528 (2009).
- [39] G. Varas, V. Vidal, and J.-C. Géminard, Dynamics of crater formations in immersed granular materials., *Physical Review E* **79**, 021301 (2009).
- [40] X.-Z. Kong, W. Kinzelbach, and F. Stauffer, Morphodynamics during air injection into water-saturated movable spherical granulates., *Chemical Engineering Science* **65**, 4652 (2010).
- [41] G. Varas, V. Vidal, and J.-C. Géminard, Venting dynamics of an immersed granular layer., *Physical Review E* **83**, 011302 (2011).
- [42] G. Varas, V. Vidal, and J.-C. Géminard, Air invasion in a granular layer immersed in a fluid : morphology and dynamics., *Granular Matter* **15**, 801 (2013).
- [43] G. Varas, G. Ramos, J.-C. Géminard, and V. Vidal, Flow and fracture in water-saturated, unconstrained granular beds., *Frontiers in Physics* **3**, 44 (2015).
- [44] B. Andreotti, Y. Forterre, and O. Pouliquen, *Granular Media: Between Fluid and Solid* (Cambridge University Press, 2013).
- [45] H. Brouwers, Particle-size distribution and packing fraction of geometric random packings., *Physical Review E* **74**, 031309 (2006).
- [46] P. Philippe and M. Badiane, Localized fluidization in a granular medium., *Physical Review E* **87**(4), 042206 (2013).
- [47] G. Gauthier and P. Gondret, Compaction of liquid immersed granular packings by small upward flows, *Physical Review Fluids* **4**, 074308 (2019).
- [48] D. Lhuillier, Migration of rigid particles in non-Brownian viscous suspensions, *Physics of Fluids* **21**, 023302 (2009).
- [49] P.R. Nott and E. Guazzelli and O. Pouliquen, The suspension balance model revisited, *Physics of Fluids* **23**, 043304 (2011).
- [50] E. Guazzelli and O. Pouliquen, Rheology of dense granular suspensions, *Journal of Fluid Mechanics* **852**, P1 (2018).
- [51] J. Richardson and W. Zaki, The sedimentation of a suspension of uniform spheres under conditions of viscous flow., *Chemical Engineering Science* **3**, 65 (1954).
- [52] E. Guazzelli and J.-F. Morris, *A physical introduction to suspension dynamics* (Cambridge Texts in Applied Mathematics, 2012).
- [53] P. Aussillous and D. Quéré, Quick deposition of a fluid on the wall of a tube., *Physics of Fluids* **12**(10), 2367 (2000).
- [54] M. Roudet, *Hydrodynamique et transfert de masse autour d'une bulle confinée entre deux plaques*, Ph.D. thesis, Institut National Polytechnique de Toulouse (2008), 131 p.
- [55] V. Vidal and C. Picard and S. Joubaud, Remontée de bulles dans une suspension dense, in *Comptes-rendus de la 21e Rencontre du Non-Linéaire*, Vol. 23, edited by Eds. E. Falcon, M. Lefranc, F. Pétrélis and C.-T. Pham, Non-Linéaire Publications (2018) pp. 79-84.
- [56] V. Roig, M. Roudet, F. Risso, and A.-M. Billet, Dynamics of a high-Reynolds-number bubble rising within a thin gap., *Journal of Fluid Mechanics* **707**, 444 (2012).
- [57] A. Filella, P. Ern, and V. Roig, Oscillatory motion and wake of a bubble rising in a thin-gap cell., *Journal of Fluid Mechanics* **778**, 60 (2015).
- [58] B. Dollet, P. Marmottant, and V. Garbin, Bubble dynamics in soft and biological matter, *Ann. Rev. of Fluid Mech.* **51**, 331 (2019).

Appendix A: Stationary state

In this section, we show typical snapshots of the final steady states displayed in a similar way than Fig 3 for additional sets of external parameters.

- Fig. 9 shows the influence of the granular bed height h_g and the liquid height h_ℓ . For each snapshots, the ratio h_ℓ/h_g is given, since it is the important reduced parameter for the computation of the packing fraction of the suspension (see Eq. (3)). These snapshots show an effect of both parameters of the final granular bed area and the final packing fraction of the suspension but do not reveal any clear trend.
- Fig. 10 shows the influence of the flow rate Q and the two different batches of monodisperse particles. As expected, the small particles (PS80 M) are more easily put into suspension than larger particles (PS 250M).

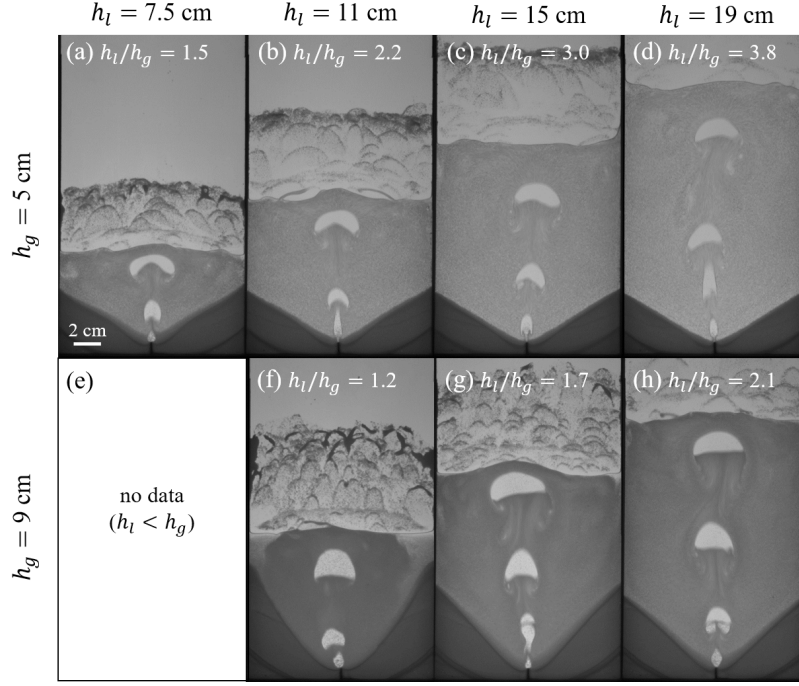


FIG. 9. Snapshots of the experiment in the stationary regime for different granular bed height h_g and liquid height h_ℓ [PS 130P; $L_c = 13.6$ cm; $e = 2$ mm; $Q = 200$ mL/min].

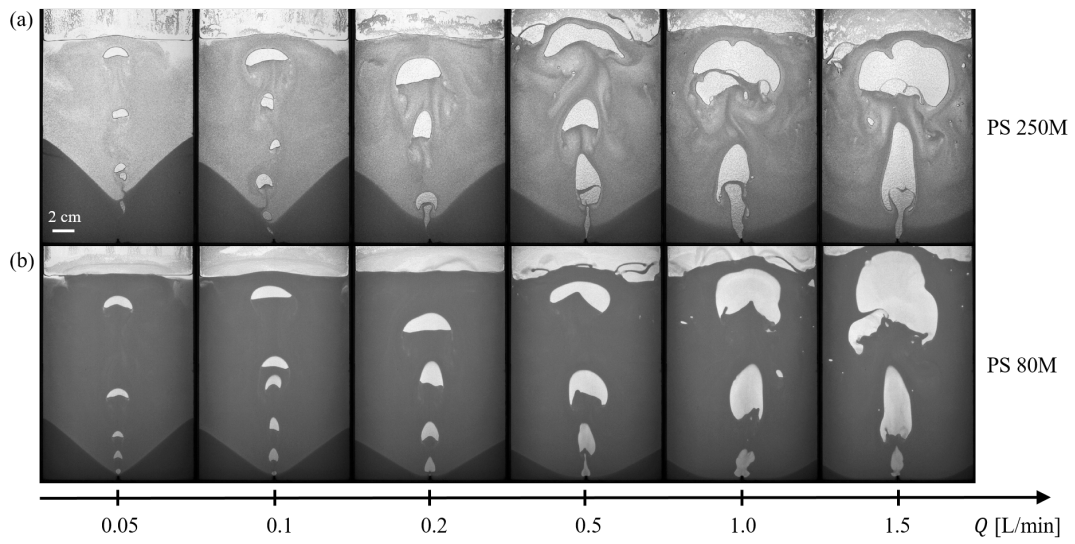


FIG. 10. Snapshots of the experiment in the stationary regime for different values of the flow rate Q and the two different batches of monodisperse particles [$L_c = 13.6$ cm; $e = 2$ mm; $h_g = 9 \pm 0.5$ cm; $h_\ell = 18 \pm 0.5$ cm].