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Tailoring the Oxygen Reduction Activity of Pt Nanoparticles through Surface Defects: A Simple Top-Down Approach

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ABSTRACT

Results from Pt model catalyst surfaces have demonstrated that surface defects, in particular surface concavities, can improve the oxygen reduction reaction (ORR) kinetics. It is, however, a challenging task to synthesize nanostructured catalysts with such defective surfaces. Hence, we present a one-step and up-scalable top-down approach to produce Pt/C catalyst (with ~3 nm Pt nanoparticle diameter). Using high-resolution transmission electron microscopy and tomography, electrochemical techniques, high energy X-ray measurements and positron annihilation spectroscopy, we provide evidence of a high density of surface defects (including surface concavities). The ORR activity of the developed catalyst exceeds that of commercial Pt/C catalyst, at least 2.7-times in terms of specific (~1.62 mA/cm²_{Pt} at 0.9 V *vs* the reversible hydrogen electrode) and at least 1.7-times in terms of mass activity (\sim 712 mA/mg_{Pt}), which can be correlated to the enhanced amount of surface defects. Besides, the technique used here reduces the

complexity of the synthesis (and therefore production costs) compared to state-of-the-art bottom-up techniques.

Introduction

With the increased awareness of preventing the climate change, efforts are made to decouple our society's energy demands from the so-called carbon cycle. One promising approach is to reduce emissions caused by automotive combustion engines, for instance by replacing this technology with electric motors that are powered by either batteries and/or hydrogen fuel cells.^{1,2} Even though the market launch of hydrogen fuel cell driven cars is on the rise, further cost reductions are required to make the technology commercially more competitive. Today, anode and cathode catalyst layer of proton exchange membrane fuel cells (PEMFCs) typically consist of Pt-based nanostructures supported on high surface area carbon (Pt/C).³ While the hydrogen oxidation reaction taking place at the anode side of the cell is a rapid process, the oxygen reduction reaction (ORR) at the cathode side exhibits sluggish kinetics. In order to improve the activity of such catalysts, two approaches are typically pursued. One way is to alloy Pt nanoparticles

with less precious transition metal elements (*e.g.,* Co, Ni, Cu) or lanthanides (*e.g.,*

Pr),^{4,5,6,7} which alters the electronic properties of the catalyst surface by a combination of so-called "strain" and "ligand" effects. This weakens the strong surface-intermediate interactions and allows to optimize electron transfer.^{8,9} In particular, both Pt₃Ni bulk and nanoscale alloy structures notably exceeded the activity of pure Pt.^{10,11,12} However, due to the dissolution of the solute metal during PEMFC operation (commonly known as "dealloying"), the membrane electrode assembly can get poisoned, resulting in poor long term performance.¹³ Another promising approach is to directly alter the catalytic properties of Pt nanoparticles by the modification of their surface structure. Exemplary, tailoring the size of the nanoparticles and the design of unusual catalyst shapes with enhanced surface area (e.g., hollow nanoparticles, aerogels) can be mentioned.^{14,15,16} Importantly, in such cases the increased activity towards the ORR can, amongst others, also be attributed to the generation of highly active defect-like surface sites. In particular, Calle-Vallejo *et al.* demonstrated that surface concavities on Pt significantly improve ORR kinetics.^{17,18} This is due to the optimized geometric structure at the concave sites, as quantified by the so-called generalized coordination number (\overline{CN}) approach. Particularly

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high \overline{CN} values have been predicted for $e.g.,$ hollow or coalescing nanoparticles at their

boundary, confirming aforementioned experimental findings. Furthermore, the activity of concave-shaped nanocubes was experimentally demonstrated by Yu *et al.*, ¹⁹ but the degree of negative curvature was not very pronounced and the size of the concave nanocubes was larger than 20 nm, which results in low mass activity. Furthermore, development of a simple production method for such concave nanoparticles often is a non-trivial endeavor. Current research mainly focuses on the synthesis of such catalysts using conventional bottom-up techniques, which typically suffer from complex and timeconsuming multiple-step procedures.²⁰ Hence, the development of a facile synthetic method for Pt nanostructures, which contain these active sites, is a crucial step towards the commercial realization of PEMFC-driven cars on a large scale. Here, we take advantage of a novel top-down synthetic route, in order to prepare Pt/C catalysts with a high degree of surface defects. This top-down approach, which was initially discovered decades prior to the beginnings of nanotechnology and introduced as atomization of metal cathodes,²¹ uses high alternating anodic and cathodic biases applied to metal wires immersed in an alkaline electrolyte, in order to produce nanoparticles at the electrode

surface and subsequently release them into the electrolyte. Fundamental experiments on

the nanoparticle synthesis by this approach were provided by Koper's, Li's and Bandarenka's groups in recent years and extended to different types of noble and nonnoble metals as well as alloys and oxide materials.^{22,23,24,25,26} With the help of highresolution transmission electron microscopy (HR-TEM), high-resolution scanning transmission electron microscopy with a high-angle annular detector (HR-STEM-HAADF), STEM-HAADF tomography visualization, Rietvield refinement of wide-angle Xray scattering (WAXS), electrochemical techniques and positron annihilation spectroscopy (PAS), we provide evidence that the top-down synthesis leads to the formation of Pt nanoparticles with rough, disordered surfaces. In particular, this includes surface concavities. Furthermore, utilizing the rotating disk electrode (RDE) technique and single-cell PEMFC measurements, we show that Pt/C produced by this top-down approach (denoted as Pt/C_{TD} in the following) is indeed highly active towards the ORR.

Experimental Section

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Synthesis: In a typical synthesis of Pt/C_{TD}, 20 mg of Vulcan XC72R active carbon (Cabot,

USA) were dispersed in 25 ml of a 1 M KOH (85%, Grüssing, Germany) solution. To improve the wettability of the carbon support, \sim 100 µl of ethanol (puriss, $>$ 99.8%, Sigma Aldrich, Germany) were added to the suspension, followed by sonication for 15 min. Subsequently, two Pt wires (99,999%, Goodfellow, Germany) with a diameter of ~0.2 mm were connected as electrodes and immersed in the suspension under vigorous stirring. To produce Pt nanoparticles, a sinusoidal potential of ±10 V *vs* Pt pseudo-reference (frequency: 200 Hz) was applied, leading to the erosion of the Pt wires. After generation of the demanded Pt weight fraction, the suspension was stirred for 12h at room temperature, followed by filtering, washing with ultrapure water (Evoqua, Germany) and drying in the oven at 60°C. As a reference catalyst, TEC10V20E Pt/C (19.6 wt.%) from Tanaka Kikinzoku Kogyo ($P t/C_{TKK}$) was used without further modification.

Pt on carbon weight loading: The weight fraction of Pt_{TD} nanoparticles on carbon was determined using TGA. The measurements were carried out with a METTLER TOLEDO TG-MS coupling instrument with an air flow of 50 ml/min and heating speed of 50 K/min

> to 1100°C. Prior to ramping the temperature, the sample was dried at ~135°C, followed by determination of its initial weight. Before cooling down, the sample was kept at 1100°C for 50 minutes until no further weight loss could be observed. The mass was compared after cooling down to 135°C.

> **Electron microscopy:** For TEM imaging of the Pt/C_{TD} electrocatalyst, a Philips CM100 EM, operated at 100 kV, was used. The samples were prepared by sonicating the catalyst powder in isopropanol, followed by drop-casting the dispersion on formvar-supported carbon-coated Cu400 TEM grids (Science Services, Germany). HR-(S)TEM imaging of the unsupported Pt_{TD} nanoparticles was conducted on a TITAN Themis 60-300 (ThermoFisher Scientific, USA) operated at 300 kV and equipped with a Schottky FEG type emission gun, a spherical aberration corrector for the objective lens and HAADF detector (Fischione, USA). The TEM sample of the unsupported Pt_{TD} nanoparticles was prepared from Pt nanoparticles dispersed in ultrapure water by sonication for 15 minutes, which were immediately dripped on a copper TEM grid with quantifoil holey carbon membrane covered by graphene oxide. The HR-TEM and HR-STEM images were

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acquired using the software Velox v.2.6 (ThermoFisher Scientific, USA) and Fourier

filtering was performed using masks on selected spots in fast Fourier transformation (FFT) patterns in the software Digital Micrograph GSM 2 (Gatan Inc., USA). The tomography of the unsupported Pt_{TD} nanoparticles was conducted on a TITAN 80-300 (FEI company, USA) operated at 300 kV in STEM mode using the HAADF detector, which allows imaging with high contrast between Pt nanoparticles and the carbon membrane of the TEM grid. The same sample as for TEM analysis (described above) was used, but round Au tracking nanoparticles with ~6.5 nm in size, dissolved in high-purity water, were dripped on the grid additionally to allow later alignment of the images in the whole tilting range. The used tilting range was +/-72° and the STEM-HAADF images were taken in 2° steps. A 2020 high field-of-view single-tilt tomography holder (Fishione, USA) was used for the tomography tilt series acquisition. The tomography data were obtained using the corresponding STEM tomography data acquisition software v.4.1 (ThermoFisher Scientific, USA) with automatic and dynamic focusing. The post processing of the tomography data consisted of three parts: alignment, reconstruction and visualization. The alignment was performed using the open-source software IMOD v.4 (University of

Colorado, USA) with plugin eTomo, where a fiducial model was created by manual tracking of Au beads surrounding the structure of interest with a residual error of the alignment of 1.2 pixel. The reconstruction was performed using the software Inspect3D v.3.1 (FEI company, USA) from the previously aligned dataset and a 3D volume of the desired size was created. The final colorful visualization of reconstructed volume was performed using the software AMIRA (ThermoFisher Scientific, USA). **Electrochemical measurements:** Electrocatalytic activity measurements were performed

using a standard electrochemical cell, filled with 0.1 M HClO₄ (Suprapur®, Merck, Germany) as electrolyte. The cell was frequently cleaned with a 3:1 ratio of sulfuric acid and hydrogen peroxide, followed by boiling the cell with ultrapure water. Electrochemical measurements were conducted using a BioLogic VSP-300 (BioLogic, France) potentiostat. As a substrate for Pt/C_{TD} , a glassy carbon electrode with a diameter of 5 mm and an area of 0.196 cm² (Pine instruments, USA) in combination with a Pine MSR electrode rotator (Pine instruments, USA) was used. For electrochemical studies, freshly prepared catalyst inks were used. A typical catalyst ink ratio consisted of ~10 mg finely

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grinded catalyst powder, 3.6 ml of ultrapure water, 1.466 ml of isopropanol (puriss., >99.8%, Sigma Aldrich, Germany) and 0.03 ml of Nafion dispersion (5 wt.% in lower aliphatic alcohols and water, Sigma Aldrich, Germany). To obtain a homogeneous dispersion, the inks were sonicated for 20 minutes prior to their first use. Prior to usage, the electrode was polished with alumina paste (1.0, 0.3, and 0.05 µm) and rinsed with ultrapure water. A commercial mercury/ mercurous sulfate electrode (Schott, Germany) served as reference electrode. A Pt wire (99.9%, Goodfellow, Germany) served as counter electrode. It has to be noted that CO-stripping voltammetry was recorded in a slightly modified setup. As a reference electrode, a commercial Hydroflex® hydrogen electrode (Gaskatel, Germany) was utilized. Experiments were operated with an Autolab PGSTAT302N potentiostat (Metrohm, France).

Membrane electrode assembly measurements:

Single-cell PEMFC measurements were conducted in a home-made cell setup. Fuel cell performance was evaluated on a Greenlight Innovation G60 test station (Greenlight Innovation

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Corp., Canada), coupled with a Gamry reference 3000 potentiostat (Gamry Instruments, USA). 5 cm² catalyst layers were prepared using the decal transfer method, *i.e.,* by rod coating on a PTFE decal, followed by drying at room temperature. As anode catalyst, commercial Pt/C_{TKK} (TEC10V20E) with an anode loading of 0.08 mg_{Pt}/cm² was used. As cathode catalyst, Pt/C_{TD} with a cathode loading of 0.1 mg_{Pt}/cm² was utilized. Synthesis of Pt/C_{TD} electrocatalyst was conducted as described in the previous sections, however, the batch size was increased from \sim 20 mg to \sim 100 mg of Pt/C_{TD} . For ink preparation, the catalyst was dispersed in a mixture of 1-propanol and water $(\sim 10 \text{ wt\%})$ and an ionomer (Nafion, 5%_{wt} in lower aliphatic alcohols and water, Sigma Aldrich, Germany) to carbon (I/C) ratio of 0.65 was adjusted. The ink was mixed on a roller mill for 18 h at room temperature, using $ZrO₂$ beads. Anode, 15 μ m membrane and cathode were hot-pressed for 3 min at 155°C and 4 kN. A Freudenberg H14C7 (Freudenberg & Co. KG, Germany) served as the gas diffusion layer. To record CO-stripping voltammograms, the cell was purged with 10% CO in N₂ for \sim 10 min at a constant potential of 0.1 V, followed by purging with pure N₂ to remove excess of CO. The voltammograms were recorded at a scan rate of 100 mV/s. Differential flow H_2/O_2 (2000 nccm/5000 nccm) polarization curves were recorded at 80°C, 170 kPa_{abs} and 100% relative humidity. The ohmic resistance was determined via electrochemical impedance spectroscopy. The H_2 crossover was determined in H_2/N_2 atmosphere.

Positron annihilation spectroscopy: For the present study, coincident Doppler broadening spectroscopy (CDBS) was performed at the CDB spectrometer using the mono-energetic positron beam at NEPOMUC located at the research neutron source Heinz Maier-Leibnitz (FRM II).²⁷ The positron implantation energy was varied between 0.10 and 30 keV.28,29 In

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order to examine the near surface region, small energy steps of 0.10 and 0.20 keV were chosen up to an implantation energy of 8 keV. The energy of the emitted annihilation radiation was recorded by high-purity Ge detectors with a typical energy resolution of 1.30 keV at 511 keV. For the calculation of the *S*-parameter the central energy interval was set to (511± 0.85) keV. The CDB spectra were recorded at a positron implantation energy of 0.4 keV where the contribution of the Si substrate can be neglected according to the calculated Makhov profile. Preparation of the samples was performed by dispersing 10 mg of Pt/C_{TD} and commercial Pt/C_{TKK} catalyst powder in 1 ml of ethanol via sonication. The as-prepared inks were drop-casted onto a silicon wafer, followed by drying of the sample at 60°C for 1 h.

WAXS measurements and Rietveld refinement: WAXS patterns of Pt/C_{TD} and the commercial Pt/ C_{TKK} were measured at the ID31 beamline of the European synchrotron radiation facility (ESRF, Grenoble, France). High energy X-ray radiations of 70 keV were focused on the catalyst powder contained either in a Kapton® tape (powder film removed from a rotating disk electrode) or Kapton® capillary for Pt/C_{TD} and commercial Pt/C_{TKK},

respectively. The scattered signal was collected using a Dectris Pilatus CdTe 2M detector within 5 s exposure time. The 2D signal was azimuthally integrated and reduced to a 1D curve using the pyFAI software package after the energy, detector distance and tilt were calibrated using a standard $CeO₂$ powder. The lattice parameter, crystallite size and microstrain values for the electrocatalysts were estimated by Rietveld refinement of the WAXS patterns using an *Fm3m* structure of metallic Pt and the Fullprof software.³¹ Due to an external pollution by Ni, an additional Ni phase was added to refine Pt/C_{TD} . The instrument resolution function was determined from the $CeO₂$ standard WAXS pattern, the peak shape and the background were described using the Thompson-Cox-Hastings (TCH) function and by a polynomial function, respectively. A possibility for uniaxial anisotropic description of nanoparticle size along the [111] direction axis was also implemented.

Results and Discussion

During the top-down synthesis process (see Figure1A), Pt wires are exposed to strongly polarizing, alternating voltages. Thereby, nanoparticles can be rapidly eroded from the

wire surface and subsequently be released into the electrolyte. Due to the rough conditions of our synthetic route, we assume to produce a wide variety of nanoparticle shapes, including surface concavities, combined with the introduction of local strain. In order to investigate the surface-defective character of Pt/C_{TD} , five different approaches were exploited:

- 1. HR-(S)TEM was used to visualize certain defective surface sites of unsupported Pt_{TD} nanoparticles.
- 2. STEM-HAADF tomography visualization was performed to obtain 3D information about the disordered surface regions of unsupported Pt_{TD} nanoparticles.
- 3. PAS was employed to compare the defect concentration of Pt/C_{TD} to commercial Pt/C_{TKK} (detailed information about the reference catalyst is given in the experimental section).
- 4. Rietveld refinement of WAXS measurements was performed to investigate and quantitatively compare the defect-induced degree of microstrain of Pt/C_{TD} to commercial Pt/C_{TKK} .

5. Electroanalytical methods were used to monitor and compare structural defects

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Figure 1. (A) Schematic description of the synthetic procedure towards Pt/C_{TD} electrocatalyst. Application of an alternating sinusoidal potential (±10V, 200 Hz) to Pt wires immersed in a suspension of Vulcan carbon in 1 M KOH and ethanol under vigorous stirring leads to the formation of carbon supported Pt nanoparticles. (B,E) HR-STEM images of unsupported Pt_{TD} single nanoparticles with corresponding (C,F) Fourier filtered images and (D,G) FFT patterns (Z.A. = zonal axis). Certain concavities are highlighted by red arrows. Twin boundaries and twin grains A, B, B´ are marked in (F). (H,I) HR-TEM images of unsupported Pt_{TD} nanoparticles. Concave regions are highlighted by red arrows. (J) 3D visualization of two unsupported, single Pt_{TD} nanoparticles, as well as a fraction of unsupported nanoparticle agglomerate, using STEM-HAADF tomography. Several concave regions are visible on both the individual as well as on the agglomerated nanoparticles.

In Figure 1B–I, unsupported Pt single nanoparticles are characterized with use of HR-TEM and HR-STEM imaging. The images reveal a non-spherical structure of the

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nanoparticles produced. Indeed, several concave-shaped surface regions can be found,

 $\overline{2}$

> as exemplary highlighted by red arrows. In detail, several complex shapes of the nanoparticles were found, as it is demonstrated by two nanoparticles imaged by HR-STEM-HAADF technique in Figure 1B and E, where smaller concavities in the order of few crystal lattice planes and a sharp, deep concavity were revealed. These defects are highlighted in Figure 1C and F, respectively, where a Fourier filtering was used to reduce noise in original HR-STEM images to improve visibility of the atomic structure details. FFT patterns of both nanoparticles (Figure 1D and G), which were obtained from the original HR-STEM images, show spots corresponding to platinum {111} and {002} lattice planes with spacing of 0.227 nm and 0.196 nm, respectively,³² and crystal orientation of the nanoparticles to zone axis [110] of the face-centered cubic (FCC) lattice. The nanoparticle in Figure 1B was found to be a pure single crystal, while in the case of the nanoparticle in Figure 1E a twinned structure was revealed by FFT. The FFT in Figure 1G shows two [110] FCC zone axis patterns (marked by lattice indexes "A" and "B" and by dotted and dashed lines), which are rotated with respect to each other around the common {111} twin plane. Hand to hand to this finding, twinning of the nanoparticle by two corresponding

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planes of the {111} type was identified, which divides the crystal into three twin grains A,

B and B´, as it is marked in Figure 1F. In addition, the complex shape of the nanoparticles can be seen from a variation in contrast within both crystals imaged by the HR-STEM-HAADF technique in Figure 1B and E. The resulting contrast at the used imaging conditions is predominantly dependent on atomic number *Z* and thickness of the sample.³³ As the studied nanoparticles are pure Pt crystals, the contrast variations must originate from variations of the sample thickness. Therefore, it is also possible to demonstrate the topological complexity of both nanoparticles. Figure 1H and I show HR-TEM images of two Pt nanoparticles with "strawberry"-like shape, including up to three concave surface regions, which can be considered particularly interesting for electrocatalytic applications. To judge the complexity of the nanoparticle shapes in broader view, a state-of-the-art STEM-HAADF tomography technique, utilized for the visualization of complex 3D samples with high lateral resolution, was performed on unsupported Pt_{TD} nanoparticles. The final 3D visualization of top-down synthesized single nanoparticles confirms the presence of surface concavities, as it is exemplarily illustrated in Figure 1J (left). Moreover, it is visible that surface concave regions appear on both,

smaller particles, as well as on larger particles. Even though the unsupported nanoparticles tend to agglomerate, the used tomography technique revealed the irregular shape of many individual nanoparticles on surface of a bigger nanoparticle cluster, as it is illustrated in Figure 1J (right side). Compared to the typically spherically shaped commercial Pt nanoparticles such as the reference catalyst,^{34,35,36} the complex shapes of P_{tr} nanoparticles prefigure an activity increase. However, a representative quantification of the particularly active sites is not possible due to the individual character of each single nanoparticle.

B

 $\overline{4}$

 3

 $\overline{\mathbf{2}}$

1

 $0₀$

 1.0

 0.5

 $\mathbf{0.0}$

 -0.5

 -1.0

 -1.5

 0.0

 Pt/C_{TKK}

Ratio to Carbon-reference

D

J (mA/cm²_{geo})

3 4 5 6 7
Energy (keV)

.
Pt surface

oxide formatic

 1.0

50 µA

 0.6

 1.2

 Pt/C_{TD}

 0.7

 0.8

 E vs RHE (V)

 $\overline{25}$

 30

 $\overline{20}$

 p_L (10⁻³ m₀c)

60

 $\overline{10}$

Pt surface oxid

 0.8

duction

 0.6

 E vs RHE (V)

∆Energy (keV)

Pt/C_{TKK}

80

Bulk Pt

Pt/C_{TKK}

 Pt/C_{TD}

Vulcan XC72R

 $\overline{15}$

,
Pt surface

oxide formatio

Ar-sat. 0.1 M HCIO,

50 mV/s, 23.5 $\mu g_{\rm Pt} / \rm cm^2$

 1.0

 1.2

100

40

 $\overline{5}$

H⁺ desorption

H⁺ adsorption

 0.2

 0.9

 0.4

20

shows a magnified energy range of 0-10 keV. (B) Ratio curves normalized to the curve of the carbon reference obtained by CDBS. Pt/C_{TD} shows a much lower Pt signature (7.5%) compared to its commercial counterpart (18.2%). Hence, the positron annihilation probability with Pt core electrons is significantly decreased in Pt/C_{TD} , which is ascribed to a higher defect concentration. (C,D) Typical CVs of Pt/C_{TD} and commercial Pt/C_{TKK}, respectively. Electrolyte: Ar-saturated 0.1 M HClO₄. Scan rate: 50 mV/s. Red arrows indicate typical H_{UPD} peak positions of Pt/C_{TKK}. Pt/C_{TD} shows an additional peak shoulder (orange arrow), which indicates the presence of surface structural defects (see main text). (E) CO-stripping peaks of PUC_{TD} (black curve) and commercial Pt/ C_{TKK} (green curve). The peak shift indicates the presence of surface structural defects. It has to be noted that the CO-stripping voltammograms were recorded separately, using a slightly modified setup (see experimental section). COcoverage was achieved by bubbling 0.1 M HClO₄ with pure CO for \sim 6 minutes while applying a constant potential of 0.1 V *vs* RHE. Saturation of the electrolyte with Ar for

~30 min, followed by a subsequent performance of a full CV cycle further leads to the oxidation of the CO monolayer. Scan rate: 20 mV/s.

In order to expand the study of single nanoparticles to the whole system, PAS was employed. It was chosen to examine the defective character of Pt/C_{TD} in comparison to commercial Pt/ C_{TKK} . PAS is known as a powerful, non-destructive tool to detect open volume defects, *i.e.,* vacancies or vacancy clusters in a crystal lattice. Due to the effective trapping of positrons in such crystal defects, the positron is applied as highly-mobile micro-probe with outstanding sensitivity to vacancy concentrations as low as 10-7 in metals. For the present study, a low-energy positron beam is required in order to investigate the near-surface region of the Pt/C samples. For better understanding, some elementary parts of PAS will be explained in the following text, whereas further details can be found in the literature.^{38,39} After being implanted in a solid, positrons thermalize within picoseconds and can then diffuse quasi-freely through the crystal lattice within a diffusion length typically in the order of 100 nm. They eventually annihilate with a core or valence electron either in the unperturbed crystal lattice or after being trapped at defect

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sites. The positron-electron annihilation leads predominantly to a back-to-back emission

of two 511 keV γ-quanta in the center-of-mass-system. These γ-quanta are most important for gaining information about defects, as they will be detected during the experiment. In the laboratory system, the longitudinal component of the electron momentum (p_L) causes a Doppler-shift of the annihilation quanta. The resulting broadened annihilation photo peak, *i.e.,* recorded counts as a function of γ-energy, is analyzed in DBS. For quantitative analysis of the line shape, the so-called *S*-parameter is commonly applied, which is defined as the fraction of counts in a fixed central region around the 511 keV annihilation peak. Since the central part of the annihilation peak is dominated by positrons annihilating preferably with low-momentum valence electrons, the *S*-parameter increases with an increasing number of vacancies or vacancy clusters.⁴⁰ In CDBS, both γ-quanta of an annihilation event are detected simultaneously in a collinear detector setup. Due to the effective suppression of the background, the annihilation of high momentum (core) electrons becomes experimentally accessible, *i.e.,* chemical information can be gained from the surrounding of the annihilation site. For evaluation, CDB spectra are normalized, mirrored at 511 keV and usually divided by a reference

spectrum in order to obtain so-called ratio curves in which the elemental signatures can be clearly observed.

Figure 2A shows the *S*-parameter as a function of the positron implantation energy, which is a measure of the probed sample depth.⁴¹ Towards high energies (> 25 keV), the commercial carbon reference material (Vulcan XC72R) in form of carbon nanoparticles with a particle size between 30-60 nm,⁴² as well as both the commercial Pt/C_{TKK} and Pt/C_{TD} nanoparticles supported on Vulcan carbon approach the same *S*-parameter. This is expected since at higher energy the positrons are implanted with a higher implantation depth, *i.e.,* most of the positrons annihilate in the Si substrate. At low energies (< 20 keV), the carbon reference possesses a higher *S*-parameter than both the commercial Pt/C_{TKK} and Pt/C_{TD}. This can be ascribed to the generally lower *S*-parameter of Pt compared to the carbon reference, as also observed in the normalized projection of the CDB spectra (Figure S1) and the low-energy region of the ratio curves (Figure 2B). More interesting, comparing both samples, Pt/C_{TD} shows a significantly higher *S*-parameter than commercial Pt/C_{TKK}. For the interpretation, it has to be mentioned that Pt/C_{TD} and

commercial Pt/ C_{TKK} slightly differ in Pt on carbon weight fraction (thermogravimetric

analysis [TGA] reveals ~15 wt.% for Pt/C_{TD} and ~20 wt.% for the commercial Pt/C_{TKK}), whereas the overall Pt loading on the substrate was adjusted. Therefore, due to its slightly smaller Pt content a slightly higher *S*-parameter of Pt/C_{TD} compared to commercial Pt/C_{TKK} was expected. However, the significantly higher S-parameter of Pt/C_{TD} cannot be caused by only the comparably small difference in weight fractions of the samples with similar overall Pt loading. Instead, this effect is attributed to a higher concentration of (open-volume) defects in Pt/C_{TD} than in commercial Pt/C_{TKK}. In order to additionally access the element-specific high-momentum part of the annihilation line related to core electrons, CDBS was carried out. Figure 2B shows the ratio curves of Pt/C_{TD} and commercial Pt/ C_{TKK} samples. These ratio curves are obtained by normalizing the individual CDBS raw spectra to same intensity and subsequent division by a reference spectrum, which is in this case a CDBS spectrum of a carbon reference. For comparison, a spectrum obtained for a bulk Pt reference is shown as well. For both, Pt/C_{TKK} and Pt/C_{TD} , the typical signature of Pt is visible ($pL=10-80x10^{-3}$ m₀c). Assuming a simple model that positrons annihilate either in defect-free Pt or carbon, one would expect that the

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respective Pt signal relates to the measured Pt weight fractions (see TGA result above),

i.e., the Pt signatures in Pt/C_{TD} would amount to 0.75 of that in Pt/C_{TKK}. As determined by fitting the curves (see SI), however, the Pt signature in Pt/C_{TD} (7.5%) is 0.59 less distinct than in the commercial Pt/C_{TKK} (18.2%). Hence, the positron annihilation probability with Pt core electrons is significantly decreased in Pt/C_{TD} . This effect is explained by the presence of a higher density of vacancy-like defects in Pt/C_{TD} , since positrons are likely to be trapped at vacancies, where, in turn, the annihilation probability with core electrons is reduced. This conclusion is in accordance with the lower density of structural defects in the commercial sample, as observed in the DBS measurements.

Another approach to investigate the presence of structural defects in nanostructured catalysts is the use of high energy X-rays. Indeed, recent studies have used Rietveld refinement of WAXS patterns to extract the microstrain (*i.e.,* the local strain) contribution from the experimental Bragg peak broadening.43,44,45 Microstrain broadening in diffraction data originates in the local atom displacements from their ideal position, such as caused by atomic vacancies, stacking faults or grain boundaries.⁴⁶ Here, it should be noted that

at the grain boundary of coalescing particles similarly active concave sites are formed.

Figure S2A displays the WAXS pattern measured at the ID31 beamline of the European synchrotron radiation facility (ESRF, Grenoble, France), including the calculated patterns for the Pt/C_{TD} catalyst (details about the WAXS pattern of the commercial Pt/C_{TKK} catalyst are available in Figure S2B). Results shown in Table S1 unambiguously support the conclusions obtained from DBS measurements: while commercial Pt/C_{TKK} features zero value of microstrain, a value of 0.60% is found for Pt/C_{TD} (being comparable or higher than some PtNi alloyed samples),^{[45](#page-27-0)} confirming its highly defective structure. The resulting surface distortion (SD) value was derived as 3.9 \pm 0.2 % for the synthesized Pt/C_{TD} (for further information see reference [45](#page-27-0)). It has to be noted that both techniques are not solely surface sensitive, but partially also include bulk information.

Electrochemical measurements further validate the presence of structural surface defects. Figure 2C and D shows typical cyclic voltammograms (CVs) of Pt/C_{TD} and commercial Pt/C_{TKK}. In both cases, in the potential range of ~0.05-0.40 V νs the reversible hydrogen electrode (RHE), typical hydrogen adsorption and desorption (H_{ads/des}) features

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of polycrystalline Pt are visible. In detail, commercial Pt/C_{TKK} depicts a sharp peak doublet with maxima at ~0.15 and ~0.22 V *vs* RHE (red dotted lines). According to Vidal-Iglesias *et al.*, using HClO₄ as an electrolyte, features in the range between 0.09 V and 0.22 V *vs* RHE can be addressed to the $H_{ads/des}$ on Pt(110) facets, while the impact of (111) and (100) facets cannot be clearly attributed.⁴⁷ Contrary, Pt/C_{TD} shows an additional distinct peak shoulder at ~0.27 V *vs* RHE (orange dotted line), which can be assigned to the Hads/des on defective surface structures, as proposed by Chattot *et al*. [44](#page-27-1) Herein, we assume that the broad H_{des} peak structure provides further evidence for the presence of structural defects on the Pt_{TD} nanoparticle surface.

CO-stripping voltammograms of both commercial Pt/C $_{TKK}$ and Pt/C $_{TD}$ are shown in Figure 2E. While the commercial Pt/C only shows a single peak at a potential of ~0.78 V *vs* RHE, indicating majorly isolated, well-distributed nanoparticles, Pt/C_{TD} shows a peak doublet with maxima located at ~0.67 V and ~0.69 V *vs* RHE and a singlet at a potential slightly lower than 0.78 V *vs* RHE. Based on the findings of Maillard *et al.*, appearance of the peak doublet structure at lower potentials can be traced back to the presence of structural

defects on complex isolated as well as agglomerated nanoparticles.^{[44](#page-27-1),48} Recently, Chattot *et al.* compared the ratio between charge Q derived from CO_{ads} and H_{ads/des} peaks with the level of SD of different Pt-based ORR nanocatalysts, indicating a quasi-linear relationship.⁴⁹ Taken the proposed evaluation protocols into account, Pt/C_{TD} catalyst shows a $Q_{CO}/2Q_H$ ratio of 0.85 ± 0.4, which indicates high density of surface defects and is comparable to *e.g.,* hollow PtNi/C.

Figure 3. (A) TEM image of Pt/ C_{TD} . The image reveals a homogeneous Pt nanoparticle coverage of the carbon support, however, parts of the support are less densely covered than others. The inset shows a magnification of some particles marked by a green frame (green scale bar: 20 nm). (B) Corresponding PSD of Pt/C_{TD} , revealing a number-

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averaged diameter (d_N) of ~3.2 ± 1.0 nm and a surface-averaged diameter (d_S) of ~3.4 nm. The PSD was derived from the investigation of 125 isolated Pt nanoparticles.

Previously mentioned observations can be further validated by observations derived from TEM imaging, as depicted in Figure 3A. Indeed, several small Pt nanoparticle agglomerates can be observed. Overall, the Pt nanoparticles are homogeneously distributed on Vulcan carbon, however, Pt nanoparticle density partially varies. The image shows that next to particles in the size range of 3-6 nm, several smaller particles with diameter \leq 2 nm can be observed. The corresponding particle size distribution (PSD) from the investigation of 125 isolated nanoparticles is given in Figure 3B, taking into account both edges of each individual particle and no particle agglomerates. PSD analysis was performed using the ImageJ software. Based on the broad size distribution, the numberaveraged (*dN*) and surface-averaged (*dS*) diameter of the isolated Pt nanoparticles was determined to be \sim 3.2 \pm 1.0 nm and \sim 3.4 nm, respectively. In case of the commercial Pt/C_{TKK} sample used, a number-averaged diameter of \sim 2.8 ± 0.8 nm can be found in the literature.⁵⁰ In contrast to the mean size determined from TEM, WAXS shows a global average

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size of 8.3 nm (Table S1), which indicates a bimodal size distribution consisting of smaller, isolated nanoparticles and larger particle aggregates. Similar observations have previously been reported by Chattot *et al.*, where partially aggregated A-Pt/C electrocatalyst showed a TEM derived mean particle size of 3.4 nm, while WAXS revealed a global average size of 7.4 nm.^{[45](#page-27-0)}

In order to evaluate the electrocatalytic activity of Pt/C_{TD} towards the ORR, RDE measurements of freshly prepared catalyst inks were conducted. A typical polarization curve of Pt/ C_{TD} is depicted in Figure 4A. Evaluation of the kinetic current was performed using the Koutecký -Levich equation (Equation 1)

$$
I_{kin} = |(I \cdot I_{lim})| / |(I_{lim} - I)| \ (1)
$$

with *I* being the measured current, I_{kin} being the kinetic current and I_{lim} being the O_2 diffusion-limited current of the polarization curve. The kinetic current curve extracted from the polarization curve in a range of 0.85 V – 1.0 V is shown in the inset of Figure 4A. The corresponding analysis of commercial $P\text{t/C}_{TKK}$ is depicted in Figure S3. As described earlier, due to the high concentration of surface structural defects of Pt/C_{TD} , we predict an activity increase compared to commercial Pt/C. Indeed, at 0.90 V *vs* RHE, we observe a ~3.6-times enhanced mass activity (~712 \pm 20 mA/mg_{Pt}) and a ~6.8-times enhanced

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specific activity (~1.62 \pm 0.32 mA/cm²_{Pt}) of Pt/C_{TD} compared to commercial Pt/C_{E-tek} (activity values taken from literature),^{51,52} and ~1.7-times mass, ~2.7-times specific activity enhancement compared to Pt/C_{TKK} . The activities of Pt/C_{TKK} are in good agreement with literature values of the same catalyst, considering the impact of the ionomer concentration.⁵³ This is a significant improvement over typically used Pt/C electrocatalysts, especially as the activity is compared to one of the most active commercial Pt/C catalysts. Moreover, the activity is even comparable to some well-known PtNi and PtCo alloyed electrocatalysts.^{54,55}

Regarding the stability of Pt/C_{TD}, preliminary accelerated durability tests of Pt/C_{TKK} and Pt/C_{TD} were conducted in RDE configuration. After 10,000 cycles between 0.6 and 1.0 V vs RHE, performed at 80 $^{\circ}$ C, Pt/C_{TD} still shows higher activity than Pt/C_{TKK} (Figure S4A). As expected, post-mortem TEM analysis of Pt/C_{TD} shows strong particle sintering at elevated temperature. Moreover, isolated particles appear to become more spherical (Figure S4B).

Figure 4. (A) Typical *IR*-corrected polarization curve of Pt/C_{TD} (anodic scan). Electrolyte: O₂-saturated 0.1 M HClO₄. Scan rate: 10 mV/s. Rotational speed: 1600 rpm. Pseudo-capacitive currents were corrected by subtraction of a background CV. The measurement is normalized to the geometrical area of the glassy carbon electrode used in the experiments (0.196 cm²) and an electrode loading of \sim 14.5 μ g_{Pt}/cm² was adjusted. The corresponding kinetic current curve in a potential range of 0.85 – 1.00 V νs RHE is displayed in the inset of the graph. (B) SSA of Pt/C_{TD} compared to the SSA

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of commercial Pt/C_{TKK}. (C) Specific activity of Pt/C_{TD} compared to commercial Pt/C_{E-tek} (activity value taken from ref. [51,](#page-33-0) benchmarked under similar conditions) and Pt/C $_{TKK}$ at 0.9 V κ RHE. (D) Mass activity of Pt/C_{TD} compared to commercial Pt/C_{E-tek} (activity value taken from ref. [51](#page-33-0), benchmarked under similar conditions) and Pt/C_{TKK} at 0.9 V *vs* RHE.

To determine the specific activity of Pt/C_{TD} , the kinetic current at 0.90 V vs RHE was normalized to the electrochemically active surface area (ECSA) of the catalyst. Integration of the H_{UPD} charge of each CV was used to determine the ECSA. For the ad- and desorption of a monolayer of H on Pt, a charge density of 210 µC/cm²_{Pt} was assumed. Determination of the mass activity was conducted by normalizing the kinetic current to the Pt mass deposited on the working electrode.

The specific surface area (SSA) of Pt/C_{TD} was determined to be \sim 46 ± 8 m²/g_{Pt}, while commercial Pt/C_{TKK} exhibits an SSA of $\sim 68 \pm 2$ m²/g_{Pt} (being comparable to literature data, considering the impact of the ionomer concentration).^{[53](#page-33-1)} In both cases, the SSA was normalized to the catalyst mass deposited on the working electrode. Comparing the

average size of both catalysts, only a slightly reduced SSA compared to Pt/C_{TKK} is expected. Hence, we assume that the actual difference in SSA is partially caused by agglomeration of the Pt nanoparticles, as can be seen in Figure 3A. The activity data and SSA values of Pt/C_{TD} and commercial Pt/C are compared in Figure 4B-D.

To further investigate the performance of Pt/C_{TD} in an actual membrane electrode assembly (MEA), preliminary measurements in a single-cell PEMFC were conducted. To meet current industrial targets to produce PEMFCs with low Pt content, MEAs with a cathode loading of \sim 0.1 mg_{Pt}/cm² were prepared and examined. The results are shown in Figure 5. Figure 5A depicts the CO-stripping voltammogram of the Pt/ C_{TD} catalyst layer. As observed in the RDE measurements, the voltammogram shows a characteristic double peak between 0.6 V and 0.9 V, associated with surface defects. Evaluation of the SSA gives a value of \sim 26.5 m²/g_{Pt}, being \sim 40% lower than the values measured in the RDE tests (assumed standard charge of a CO monolayer on Pt: 420 μ C/cm²). This observation can be due to the increased catalyst batch size, leading to stronger agglomeration of the Pt nanoparticles, or due to non-uniform ionomer wetting of the

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catalyst layer in the MEA. The ORR kinetics of Pt/C_{TD} were extracted from the H₂/O₂ polarization curves after correction of the IR-drop and the H_2 crossover. At 0.9 V, a noticeable increase of the mass activity compared to Pt/C_{TKK} (Figure 5B, C; reference data measured in the same setup under identical conditions were taken from literature⁵⁶) can be observed, validating the results obtained from RDE studies. Owed to the so-called particle size effect, the specific activity of both catalysts is poorly comparable, as the SSA of Pt/C_{TKK} is more than 2.5-times larger than the SSA of Pt/C_{TD}.^{[56,](#page-37-0)57} Hence, in order to compare the intrinsic activity of Pt/C_{TD} , we included the activity data of heat-treated Pt/C_{TKK} recorded by Schwämmlein *et al.* (HT-Pt/C_{TKK}, taken from literature^{[56](#page-37-0)}) with an SSA of \sim 7 m²/g_{Pt}. Due to the smaller SSA of HT-Pt/C_{TKK}, higher specific activity is expected. However, at 0.9 V we still observe higher specific activity of Pt/C_{TD} compared to HT-Pt/C_{TKK}, indicating higher intrinsic activity of Pt/C_{TD}. While at 0.9 V only kinetic losses are expected, at higher current densities the low roughness factor (cm²_{Pt}/cm²_{MEA}) leads to a poor O₂ mass transport, as previously reported by Harzer, Schwämmlein *et al.*^{[50](#page-31-0)[,56](#page-37-0)} Here, in particular proper wetting of the catalyst layer with ionomer has to be ensured in order to prevent losses. Thus, we assume that for up-scaled batch sizes, enhancing the SSA

of Pt/C_{TD} through an improved synthesis procedure (*e.g.*, improved mixing of the electrolyte during synthesis) and adjustment of the ionomer distribution could further improve the performance of the catalyst, especially at high current densities. Moreover, in future experimental studies, the stability of defect-rich Pt/C_{TD} in the MEA setup has to be evaluated, as this task was out of the scope of this work. However, accelerated stress tests of Schwämmlein *et al.* indicate that in the MEA, a lower SSA has beneficial effects on the stability of the catalyst, which should be considered prior to adjustment of the surface area.^{[56](#page-37-0)}

Figure 5. (A) CO-stripping voltammogram of the Pt/C_{TD} cathode catalyst layer, showing a characteristic double peak. Integration of the peaks and normalization to Pt mass leads to a SSA of ~26.5 m²/g_{Pt}. (B) Uncorrected and *IR*-corrected H₂/O₂ differential flow polarization curve of the Pt/C_{TD}-based MEA (0.1 mg_{Pt}/cm², 0.65 I/C ratio), recorded at a pressure of 170 kPa_{abs}, 80°C and 100% relative humidity (RH). (C) Mass and specific activity of Pt/C_{TD} at 0.9 V, compared to Pt/C_{TKK} (SSA: \sim 68 m²/g_{Pt}) and heat-treated Pt/C_{TKK} (SSA: ~7 m²/g_{Pt}). For activity evaluation, the H₂/O₂ data were corrected for the

IR-drop and the H₂ crossover current. The reference data were taken from reference [56,](#page-37-0) however, the catalyst was examined in the same setup and under identical conditions.

Conclusions

Within this work, we show an up-scalable, top-down and one-pot synthetic approach towards highly active Pt/C electrocatalysts, circumventing typical demanding multi-step synthesis procedures. In RDE studies, synthesized Pt/C_{TD} shows high activity towards the ORR with a specific and mass activity of 1.62 mA/cm²_{Pt} and 712 mA/mg_{Pt}, respectively. An ORR activity enhancement over commercial Pt/C was further confirmed in a single-cell PEMFC. Based on TEM, WAXS, CV and PAS experiments, the origin of the superior activity compared to commercial Pt/C can be correlated to the introduction of a high density of surface defects, such as surface concavities. Furthermore, considering the high complexity of classical nucleation driven bottom-up syntheses and costs of the precursor materials, the top-down approach does not only facilitate the synthesis, but should also save overall processing costs in large scale applications.

ASSOCIATED CONTENT

Supporting Information

This information is available free of charge on the ACS Publications website. Coincident Doppler broadening spectrum, WAXS measurements, Rietveld refinement data, Reference ORR polarization curve, Accelerated durability test, TEM analysis

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The manuscript was written through contributions of all authors. All authors have given

approval to the final version of the manuscript. ‡These authors contributed equally to this

work.

Notes

The authors declare no competing financial interest.

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TOC:

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REFERENCES

- (1) Thomas, C. E. Fuel Cell and Battery Electric Vehicles Compared. *Int. J. Hydrog. Energy* , *34*, 6005-6020.
- (2) Pellow, M. A.; Emmott, C. J. M.; Barnhart, C. J.; Benson, S. M. Hydrogen or Batteries for Grid Storage? A Net Energy Analysis. *Energy Environ. Sci*. **2015**, *8*, 1938-1952.
- (3) Yoshida, T.; Kojima, K. Toyota MIRAI Fuel Cell Vehicle and Progress Toward a Future Hydrogen Society. *Electrochem. Soc. Interface* **2015**, *24*, 45-49.

ACS Catalysis

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(49) Chattot, R.; Martens, I.; Scohy, M.; Herranz, J.; Drnec, J.; Maillard, F.; Dubau, L. Disclosing Pt-Bimetallic Alloy Nanoparticle Surface Lattice Distortion with Electrochemical Probes. *ACS Energy Lett.* **2019**, *5*, 162-169. (50) Harzer, G. S.; Schwämmlein, J. N.; Damjanovic, A. M.; Ghosh, S.; Gasteiger, H. A. Cathode Loading Impact on Voltage Cycling Induced PEMFC Degradation: A Voltage Loss Analysis. *J. Electrochem. Soc.* **2018**, *165*, F3118-F3131. (51) Kuttiyiel, K. A.; Sasaki, K.; Choi, Y.; Su, D.; Liu, P.; Adzic, R. R. Bimetallic IrNi Core Platinum Monolayer Shell Electrocatalysts for the Oxygen Reduction Reaction. *Energy Environ. Sci.* **2012**, *5*, 5297-5304. (52) Godínez-Salomón, F.; Rhodes, C. P.; Alcantara, K. S.; Zhu, Q.; Canton, S. E.; Calderon, H. A.; Reyes-Rodríguez, J. L.; Leyva, M. A.; Solorza-Feria, O. Tuning the Oxygen Reduction Activity and Stability of $Ni(OH)_{2}@Pt/C$ Catalysts through Controlling Pt Surface Composition, Strain, and Electronic Structure. *Electrochim. Acta* **2017**, *247*, 958- 969. (53) Orfanidi, A.; Madkikar, P.; El-Sayed, H. A.; Harzer, G. S.; Kratky, T.; Gasteiger, H. A. The Key to High Performance Low Pt Loaded Electrodes. *J. Electrochem. Soc.* **2017**, *164*, F418-F426. (54) Mezzavilla, S.; Baldizzone, C.; Swertz, A.-C.; Hodnik, N.; Pizzutilo, E.; Polymeros, G.; Keeley, G. P.; Knossalla, J.; Heggen, M.; Mayrhofer, K. J. J.; Schüth, F. Structure– Activity–Stability Relationships for Space-Confined Pt_xNi_y Nanoparticles in the Oxygen

Reduction Reaction. *ACS Catal.* **2016**, *6*, 8058-8068.

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