

# CO2 valorization by a new microbiological process

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# ▶ To cite this version:

A. Ruiz-Valencia, D. Benmeziane, N. Pen, E. Petit, V. Bonniol, et al.. CO2 valorization by a new microbiological process. Catalysis Today, 2020, 346, pp.106-111. 10.1016/j.cattod.2019.03.053 . hal-02930313

# HAL Id: hal-02930313 https://hal.science/hal-02930313v1

Submitted on 7 Nov 2020

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1	CO <sub>2</sub> valorization by a new microbiological process		
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12	Abstract. Carbon dioxide constitutes one of the largest carbon feedstocks for fuel production. This work		
13	demonstrates that an environmental bacterial consortium grown on methane is able to directly and selectively		
14	reduce $CO_2$ into formate. The conversion was carried out at 30°C and atmospheric pressure, without any the		
15	addition of organic molecules (such as cofactor), photons or $H_2$ to the reaction medium. When exposed to a		
16	CO <sub>2</sub> :air (1:1 $\nu/\nu$ ) mixture, the consortium was able to produce 280 ± 10 mg·g dry cell <sup>-1</sup> of formate in 15 days. A		
17	control experiment performed solely with air coupled to NMR analysis suggested that at least 17 % of the		
18	formate was produced from direct $\text{CO}_2$ reduction. The formate produced could be used as a precursor for		
19	methanol production from methane by methanotrophic bacteria or it could be acidified to feed Direct Formic		
20	Acid Fuel Cells.		
21			
22	Key words. Carbon dioxide, reduction, formate, bio-catalytic process, microbial process.		
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24			

### 25 **1. Introduction**

- Carbon dioxide (CO<sub>2</sub>) accounts for more than 75% of global greenhouse gas (GHG) emissions, with annual anthropogenic emissions of about 25 to 35 Gt [1]. These emissions, which today represent around 65% of GHG
- 28 emissions in CO<sub>2</sub> equivalents [1], derive mainly from heavy and energy producing industries (cement plants,
- aluminum and steel production sites, coal and oil-fired power plants), as well as transport [1, 2]. Use of CO<sub>2</sub> as
- 30 a raw material at the industrial level is currently being studied as a possible solution to reduce levels of this gas
- 31 in the atmosphere. However, today, industrially,  $CO_2$  is mainly used as a fluid rather than a reactant and it
- 32 originates mainly from natural sources or fermentation plants, its industrial use representing less than 1% (i.e.
- 33 100 Mt/yr) of annual emissions [2]. Indeed, industrial use of the gas as a chemical reactant is currently very
- 34 limited and based on the affinity of some nucleophilic molecules for CO<sub>2</sub> to form urea, carbamates and cyclic
- 35 organic carbonates [3].

36 In this context, over the last fifty years direct conversion of anthropogenic  $CO_2$  into alternative fuels (such as

- 37 methane,  $C_1$ - $C_5$  alcohols or formic acid) has become a major research topic because it could help solve two
- 38 major future challenges, namely climate change and fossil fuel shortages. Nevertheless, activation of  $CO_2$
- 39 molecules is very difficult because dissociation of the C=O bond requires a large amount of energy (i.e. 795
- 40 kJ.mol<sup>-1</sup>). Activation of CO<sub>2</sub> therefore requires efficient and selective catalysts but also, quite often, relatively
- 41 high temperatures and pressures.
- 42 Both homogeneous and heterogeneous catalysts have been reported to catalyze hydrogenation reactions [2, 4,
- 43 5], artificial photosynthesis [6-10] and electrochemical reduction [3, 11, 12], giving rise to fuels and molecule
   44 platforms from CO<sub>2</sub>. However, despite recent progress, these chemical conversion routes still exhibit low
- 45 durability and/or selectivity [6, 13-15].
- 46 The biological processes for  $CO_2$  activation are interesting because they are usually selective and require mild conditions. These biological processes are considered sustainable as they are low-energy-consuming and 47 48 reagent use and/or by-product release that could have a negative environmental impact is generally limited. 49 Currently, only processes implementing photosynthetic microorganisms such as microalgae or cyanobacteria 50 have been developed at the industrial scale. The main products recovered from CO<sub>2</sub> valorization by these 51 processes are lipids which can be then converted into biodiesel [16, 17]. Open raceway technology has allowed 52 the scaling-up of microalgae processes but their development is still limited due to (i) nutrients and mass transfer 53 limitations, (ii) the need for good sunlight capture with special bioreactors requiring very large areas and low 54 depths, (iii) the need to maintain a basic pH (8-10), and (iv) the need to harvest the microorganisms in order to 55 extract the compounds of interest. All these constraints limit productivity and generate relatively high costs 56 [18]. At the laboratory scale, cyanobacteria have been genetically modified to produce alcohols directly from 57 CO<sub>2</sub> [18-21]. Very recently, the carbon assimilation pathway of the cyanobacterium Synechococcus elongatus 58 PCC 7942 has been directed towards the production of 2,3-butanediol from  $CO_2$  and glucose in the dark [22]. 59 Such an advance overcomes the limitations related to the need for sunlight, but the need to add glucose still 60 makes the bioprocess unattractive from an economic point of view. In addition, the biological stability of the
- 61 modified cyanobacteria has yet to be improved for industrialization purposes [18-22].

- 62 Among the biological catalysts, Formate Dehydrogenase (FDH) enzymes are known to be reversible and several 63 works have focused on the selective reduction reaction of CO<sub>2</sub> into formate by extracted, purified and improved 64 FDH [23, 24]. Recently, the enzyme nitrogenase, a well-known N<sub>2</sub>-reducing enzyme, has also been reported to 65 be able to catalyze the conversion of  $CO_2$  into formate and methane [25, 26]. However, the scaling-up of this 66 bio-conversion process is difficult because it requires the addition of costly cofactors to provide the essential 67 electrons and protons for  $CO_2$  bio-reduction [27, 28]. Electrochemically assisted reactors (also known as bio-68 electrolyzers), inoculated with electro-active litho-autotrophic bacteria, constitute another biological means of CO<sub>2</sub> conversion [16, 29-34]. Two different configurations are possible with these systems: (1) CO<sub>2</sub> reduction 69 70 may be catalyzed by the biotic cathode and the required electrons are supplied by the polarized cathode while 71 the protons derive from water oxidation at the anode or (2), in the case of use of hydrogenotrophic bacteria, the 72 cathode electrons and the protons arising from the anode can be used *in situ* to generate dihydrogen  $(H_2)$  that 73 will then be assimilated by the bacteria. Recently, a methylotrophic bacterium, Methylobacterium extorquens 74 AM1, was reported to have produced formate from  $CO_2$  with the first bio-electrolyzer configuration, but no 75 cathodic current driven by the presence of  $CO_2$  was evidenced and the  $CO_2$  reduction reaction was not 76 demonstrated [31]. When hydrogenotrophic bacteria were used with the second configuration, different 77 products such as methane [31], acetate [32], PolyHydroxyButyrate (PHB), biomass and C3-C5 alcohols [33] 78 were obtained from  $CO_2$  and  $H_2$ . However, the fact that hydrogen ( $H_2$ ) is an expensive energy vector and its 79 solubility in water is low constitute major drawbacks for the scaling-up of this process that produces molecules 80 with a lower energy potential than H<sub>2</sub>.
- The hydrogenotrophic bacterium *Ralstonia eutropha* H16 has been genetically modified to use formate as a source of carbon and protons instead of  $CO_2$  and  $H_2$  to produce isobutanol and 1-methyl-butanol [34]. Bioelectrolyzer tests were carried out with the bacterium to try and generate formate *in situ* at the cathode by reduction of  $CO_2$  [34], but electrochemical reduction of  $CO_2$  still remains difficult.
- 85 Finally, methanotrophic bacteria (Methylosinus trichosporium IMV 3011 and Methylosinus sporium) have been 86 reported to selectively convert  $CO_2$  into methanol with their enzymes (including FDH first that can reduce  $CO_2$ 87 into formate) and their intracellular PHB stock being used as a source of electrons and protons [35-37]. Contrary 88 to the other biocatalysts, with these bacteria, there is no need to add costly chemicals such as cofactors or  $H_2$  to 89 the reaction medium, or to provide the reaction system with light, or to genetically modify the metabolic 90 pathway of the bacteria to recover products directly from CO<sub>2</sub>. Moreover, methanotrophic bacteria use methane 91 (CH<sub>4</sub>) as a carbon and energy source to grow, meaning the global carbon balance of the CO<sub>2</sub> valorization 92 bioprocess is positive as our city and agricultural wastes are a renewable source of methane. Methanotrophic 93 bacteria are thus interesting biocatalysts for CO<sub>2</sub> reduction. However, the methanol production obtained was 94 very low  $(3.6 \,\mu\text{mol}_{\text{methanol}} \cdot g_{\text{dry cell}}^{-1})$ .
- 95

96 In this work, an environmental bacterial consortium rich in methanotrophic bacteria was shown to directly and 97 selectively catalyze the reduction of CO<sub>2</sub> into formate, a chemical which could be considered as a future 98 energetic vector since its acidic form, i.e. formic acid, can be used as fuel in Direct Formic Acid Fuel Cells 99 (DFAFCs) or as an H<sub>2</sub>-storage molecule. Formate could also be employed as an electron donor for oxidation of 100 CH<sub>4</sub> into methanol by methanotrophic bacteria [38, 39]. Significant amounts of formate were able to be 101 produced (1.06 mmol <sub>formate</sub>·g <sub>dry cell</sub><sup>-1</sup>) without the addition of costly chemicals to the reaction medium or *in situ* 102 generating compounds for CO<sub>2</sub> reduction. In addition, the native consortium was grown on methane, a 103 renewable source of carbon. This new CO<sub>2</sub> valorization route appears very promising and a patent application 104 was therefore submitted [40], justifying the composition of the bacterial consortium remaining confidential 105 until publication of said patent.

106

### 107 **2. Materials and methods**

- 108
- 109

#### 2.1. Bacteria and culture conditions

110 A bacterial consortium [40] containing methanotrophic bacteria, the composition of which remains confidential, 111 was grown in a modified nitrate mineral salts (NMS) medium enriched with copper and iron. The bacteria were 112 grown in sealed vials incubated at 30°C on a rotary shaker (Unimax 1010, Heidolph) operated at 160 rpm. The 113 headspace of the vials was filled with a mixture of CH<sub>4</sub> and air (1:1  $\nu/\nu$ ) that was used as the source of carbon 114 and energy; the gas volume was 3-fold that of the liquid. The NMS medium was composed of 1.06 g/L KH<sub>2</sub>PO<sub>4</sub>, 115 4.34 g/L Na<sub>2</sub>HPO<sub>4</sub>·12H<sub>2</sub>O, 1.7 g/L NaNO<sub>3</sub>, 0.34 g/L K<sub>2</sub>SO<sub>4</sub> and 0.074 g/L MgSO<sub>4</sub>·7H<sub>2</sub>O; the pH of NMS 116 medium was adjusted to  $7.0 \pm 0.1$  with NaOH, 0.1 M or HCl, 0.1 M and the medium was then autoclaved. 117 Mineral, copper and iron solutions were prepared independently and sterilized by filtration on a 0.2-µm acetate 118 cellulose membrane (Sartorius) before being added to the NMS medium. The final concentrations of the mineral 119 solutions were 0.57 mg/L ZnSO4<sup>·7</sup>H<sub>2</sub>O, 0.446 mg/L MnSO4·H<sub>2</sub>O, 0.124 mg/L H<sub>3</sub>BO<sub>3</sub>, 0.096 mg/L Na<sub>2</sub>MoO<sub>4</sub>·2H<sub>2</sub>O, 0.096 mg/L KI, 7.00 mg/L CaCl<sub>2</sub>·2H<sub>2</sub>O, that of the copper solution 0.798 mg/L CuSO<sub>4</sub>, and 120 121 that of the iron solution 11.20 mg/L FeSO<sub>4</sub>.7H<sub>2</sub>O.

122 123

# 2.2. Preparation of the bacterial suspension

At the beginning of the stationary phase, the cultured cells were harvested by centrifugation at 4000 g for 20 min at 4°C and then washed once with phosphate buffer 20 mM at pH 7.0. A reaction medium containing 20 mM of phosphate buffer at pH 7.0 and 5 mM of MgCl<sub>2</sub> was used to re-suspend the cells to reach a final optical density at 600 nm (OD<sub>600</sub>) of about 10. Part of the resulting suspension was stored at -20°C with glycerol (20 % w/w) for further biochemical analysis.

129

### 130 **2.3.** CO<sub>2</sub>-reduction tests in batch mode

The batch reactors were 60 mL-glass vials sealed with aluminium caps. The bacterial suspension was distributed into the batch reactors, with 6 mL being added per reactor. To assess the ability of the consortium to reduce CO<sub>2</sub>, several experiments were conducted with different headspace atmospheres (Table 1) that were first sterilized by filtration on 0.2-μm PTFE filters (Sartorius). For experiments A, B and C, a large set of vials was filled with the same bacterial suspension and incubated at 30°C under constant rotation (160 rpm). Each experiment was monitored for 20 days and at each sampling point, a vial was taken for analytical measurements. Different measurements were performed: optical density at 600 nm (OD<sub>600</sub>), pH, salts analysis by ionic

- 138 chromatography (IC) and quantification of the volatile organic compounds (VOC) contained in the liquid
- 139 samples by headspace GC-MS.
- 140 Each experiment was conducted in triplicate. CO<sub>2</sub>-reduction tests were also carried out with <sup>13</sup>CO<sub>2</sub> to confirm
- 141 the origin of the products arising from CO<sub>2</sub> reduction by carbon NMR analyses.
- 142
- 143 Table 1. Experimental conditions for the CO<sub>2</sub> reduction tests
- 144

Experiment	Presence of bacteria	Headspace atmosphere
А	Yes	CO <sub>2</sub> :Air (1:1 <i>v/v</i> )
В	Yes	Only Air (100 %)
С	Yes	Only N <sub>2</sub> (100%)
D	No	CO <sub>2</sub> :Air (1:1 <i>v/v</i> )

145

146 Air was taken from the atmosphere while  $CO_2$  (99.995 %) and  $N_2$  (99. 995 %) were obtained from Air Liquide 147 and <sup>13</sup>CO<sub>2</sub> (99.9 %) was obtained from Sigma Aldrich.

148

# 149 **2.4.** Sample processing

At various reaction times, the bacterial suspensions in the reaction vials (i.e. 6 mL) were recovered and divided into different fractions. A first fraction was used to measure pH and  $OD_{600}$ . A second fraction was centrifuged at 10 000 g at 4°C for 10 min; the supernatant was then recovered to be immediately analyzed (by GC-MS or ionic chromatography). In case of NMR characterization, a portion of the freshly sampled suspension (0.5 mL) was transferred into NMR tubes for direct analysis.

155

# 156 **2.5. Analytical methods**

Optical density (OD<sub>600</sub>) was measured at 600 nm with a UV-2400 spectrophotometer (Shimadzu, Japan) and
 pH was measured with a C831 pH-meter (Consort, Belgium).

Volatile organic compounds, including methanol, ethanol, formaldehyde and acetaldehyde, were quantified by gas chromatography (Clarus 580, Perkin Elmer), coupled to mass spectrometry (Clarus SQ-8-MS, Perkin Elmer). A headspace system (Turbomatrix 16S, Perkin Elmer) was used for sample injection. Prior to analysis, acetonitrile was used as an internal standard at a final concentration of  $39.3 \pm 0.2$  mg·L<sup>-1</sup>. The method included a 15-min sample heating step to 75°C followed by injection into the GC system. Separation was carried out using a capillary column (Rt-Q-Bond Plot, Restek) under isothermal conditions (150°C for 25 min). Calibration curves were obtained independently for each VOC.

166 Salt quantification of supernatants was carried out by ionic chromatography (IC). Sample portions of 25  $\mu$ L

- 167 were injected into a Dionex ICS-1000 system (Thermo Scientific<sup>TM</sup>) with an IonPAc AS19 (0.4 x 250 mm)
- capillary column and elution was carried out under the following conditions: 10 mM KOH (0 to 10 min), then
- 169 10-45 mM KOH (10 to 30 min).

- 170 For NMR analysis, 450  $\mu$ L of the sample (complete suspension) was poured into a 5 mm NMR tube with 50
- 171 µL of D<sub>2</sub>O. The analyses were performed using a NMR BRUKER Avance III 500MHz spectrometer -
- 172 CryoProbe Helium system for four hours. Different standards prepared in the reaction medium were analyzed
- 173 independently by NMR to obtain the carbon spectra of these molecules.
- 174

## 175 **3. Results and Discussion**

As detailed in Table 1, different experimental conditions were used to check the ability of the consortium to reduce  $CO_2$  into formate. The conditions of experiment A correspond to the reaction conditions for formate production, i.e. bacterial consortium in presence of a  $CO_2$ :air mixture (1:1  $\nu/\nu$ ). Experiments B, C and D, performed without adding  $CO_2$  (B, C) or without bacteria (D), were blanks or control tests. Experiments B and C aimed to assess whether there was any possible microbial by-product release when the bacteria were placed in presence of air (B) or N<sub>2</sub> (C). Experiment D was performed without bacteria and in presence of  $CO_2$  to check

- $182 \qquad that \ spontaneous \ CO_2 \ reduction \ could \ not \ occur.$
- 183

184 Figure 1 presents the results obtained in the batch reactors where formate appeared in the reaction medium, i.e.

185 experiments A and B (Table 1); for each experiment, three independent runs were performed in parallel and

186 each point represents the mean values obtained.



187

**Figure 1.** Reaction profiles of formate production, pH and OD600/(OD600)i obtained for experiments A and

189 B. A: bacterial consortium with an equimolar CO2:air mixture and B: bacterial consortium with only air;

190 (OD600)i means initial OD600; (OD600)i =  $7.6 \pm 0.6$ 

191 corresponding to 2.45 g dry cell.L-1.

192

193 Regarding OD<sub>600</sub>, a nearly 25 % decrease in bacterial concentration was observed during the first few days 194 which then remained constant (from day 5), with no differences being observed between headspace atmospheres 195 A and B (Fig. 1). As the initial OD<sub>600</sub> was high ( $7.6 \pm 0.6$ ), the biomass concentration still remained significant 196 during the experiments despite the decrease. The observations regarding OD<sub>600</sub> were similar for experiment C 197 (data not shown). The fact that methanotrophic bacteria have been reported to be very resistant and able to form 198 spores in stressing conditions [41] could also explain the preservation of  $OD_{600}$  over 20 days despite the fact 199 that the bacteria were exposed to unusual conditions (i.e. absence of their substrate CH<sub>4</sub> and high CO<sub>2</sub> content). 200 In the reactors where CO<sub>2</sub> was added (experiment A), pH decreased from 7.0 to  $6.4 \pm 0.2$  within 5 days and then remained at that value which corresponds to the first acid dissociation constant (pKa) of CO<sub>2</sub> in water. A 201 202 similar change in pH was observed in the reactors of experiment D as they also contained high levels of CO<sub>2</sub> 203 (data not shown). In the vials containing only air (experiment B), pH decreased slightly to  $6.8 \pm 0.1$  due to the 204 presence of traces of CO<sub>2</sub> (i.e. 400 ppmv). When the headspace contained N<sub>2</sub> (experiment C), pH remained 205 constant at its initial value, i.e.  $7.0 \pm 0.1$  (data not shown).

206

The control tests carried out with the consortium and  $N_2$  (experiment C) showed no evidence of microbial byproduct release or formation by GC-MS or ionic chromatography throughout the duration of the experiment. No products were detected either in the control tests performed without bacteria but with an equimolar mixture of CO<sub>2</sub> and air (experiment D), which confirmed that spontaneous CO<sub>2</sub> reduction did not occur.

211

In experiments A and B (consortium exposed to an equimolar mixture of  $CO_2$  and air or to air), no VOC were detected by GC-MS. Nevertheless, ionic chromatography analyses demonstrated the appearance of formate after 8 days in both of the experiments (Fig. 1). The consortium was able to produce up to 750 mg·L<sup>-1</sup> of formate in the CO<sub>2</sub>:air mixture (1:1) at day 15 of the reaction, corresponding to a formate production of  $280 \pm 10 \text{ mg} \cdot \text{g}_{dry}$ .  $cell^{-1}$  (taking into account the bacterial mass initially introduced into the reactors).

217

When the consortium was exposed to air (experiment B), which contains a small fraction of CO<sub>2</sub> (400 ppmv), formate production was lower than that of experiment A (Fig. 1). In fact, 330 mg·L<sup>-1</sup> of formate were produced corresponding to a production of  $145 \pm 15 \text{ mg} \cdot \text{g}_{dry \text{ cell}}^{-1}$ . These results show that formate production is CO<sub>2</sub>- and bacteria-dependant and suggest that formate could be formed from CO<sub>2</sub> present in the atmosphere.

Nevertheless, the amount of formate obtained (i.e.  $330 \text{ mg} \cdot \text{L}^{-1} \text{ x } 6. 10^{-3} \text{ mL} = 1.98 \text{ mg}$ ) in experiment B (only air) was much higher than the expected theoretical quantity taking into account the CO<sub>2</sub> content of air (54 mL of air with 400 ppmv of CO<sub>2</sub> that can be transformed to a maximal formate mass of 0.04 mg). A possible explanation for the appearance of formate in excess in the reaction medium could be mixed acid fermentation. This bacterial phenomenon occurs under oxygen limitation and could give rise to products such as acetate and formate by cleavage of intracellular pyruvate by pyruvate formate lyase [42]. In this work, anoxic conditions

- could have occurred due to a rapid depletion of the oxygen initially present in the reactors since oxygen is the usual final electron acceptor for the consortium; the bacterial consortium is indeed first grown under aerobic conditions before being exposed to  $CO_2$  (section 2.1).
- 231
- 232 In order to confirm the actual ability of the consortium to reduce CO<sub>2</sub> into formate, a new set of experiments
- 233 was carried out using a mixture of <sup>13</sup>CO<sub>2</sub>:air (1:1). The reaction was then monitored by <sup>13</sup>C NMR. Nuclear
- 234 magnetic resonance spectroscopy (NMR) is only sensitive to <sup>13</sup>C since it has a spin number of <sup>1</sup>/<sub>2</sub>. <sup>13</sup>CO<sub>2</sub>-
- 235 labelling was consequently used to monitor any potential <sup>13</sup>C-containing product. In addition, the technique can
- be used to detect products irrespective of their localization (i.e. inside or outside the cells) as the NMR magnetic
- field can penetrate bacterial cells. The NMR spectrum obtained after 8 days of reaction is shown in Figure 2.



238

Figure 2. NMR spectrum at (a) t = 0 days, where CO<sub>2</sub> and HCO<sub>3</sub><sup>-</sup> are presents; (b) t = 8 days showing a new compound with a chemical shift corresponding to formate, which is enlarged (c).

241

Resonance peaks for  ${}^{13}CO_2$  ( $\delta = 124.6$  ppm) and its corresponding ionized form  $H^{13}CO_3$  ( $\delta = 160.2$  ppm) were 242 243 visible at the beginning. After 8 days of reaction, a new peak appeared ( $\delta = 170.9$  ppm), corresponding to the standard fingerprint of <sup>13</sup>C-labelled sodium formate. Since no other labelled compound was detected in the 244 reaction medium, the labelled formate is thus likely to result from direct <sup>13</sup>CO<sub>2</sub> reduction. This result 245 demonstrates that the consortium is thus able to reduce  $CO_2$  into formate. However, in this experiment, it was 246 not possible to recover semi-quantitative information about the labelled formate concentration produced since 247 the <sup>13</sup>CO<sub>2</sub> and H<sup>13</sup>CO<sub>3</sub><sup>-</sup> signals were saturated. The only available information was that the formate 248 249 concentration on day 8 was higher than the low NMR threshold for detection of labelled formate (i.e. 6 mg·L<sup>-</sup> <sup>1</sup>). If it is considered that bacteria exposed to CO<sub>2</sub>:air (Fig. 1, run A) were able to produce  $35 \pm 2 \text{ mg} \cdot \text{L}^{-1}$  of 250 formate on day 9, it can be assumed that at least 17 % (= 6 / 35 x 100 %) of the formate produced resulted from 251 252 CO<sub>2</sub> reduction.

253

254 Reduction of  $CO_2$  by the consortium may be explained by several possible enzymatic cycles inside the bacteria. 255 Among the bacteria of the consortium, methanotrophic bacteria are supposed to be of  $CO_2$  reduction catalysts. These bacteria use CH<sub>4</sub> as an energy and carbon source. As described in Figure 3.A, the first step involves 256 257 methane oxidation to methanol by methanol monooxygenase (MMO); methanol is then successively converted 258 into formaldehyde and then formate by methanol dehydrogenase (MDH) and formaldehyde dehydrogenase 259 (FADH), respectively. Finally, formate dehydrogenase (FDH) catalyzes the oxidation of formate to  $CO_2$ . The 260 methane consumed is fixed in the carbon cycle for protein and biomass production, and the CO<sub>2</sub> produced from 261 CH<sub>4</sub> oxidation is reported to be also mainly fixed in the carbon cycle through carboxylase enzymes incorporating CO<sub>2</sub> into organic molecules already present inside the cells [43]. In addition, formate can also 262 263 enter the carbon cycle for the production of bacterial material, and PolyHydroxyButyrate (PHB) in particular. 264 PolyHydroxyButyrate is an energy storage polymer accumulated during the culture phase under oxygen and 265 nitrogen limitation [44, 45].

266



267

Figure 3. Methanotrophic bacteria: (A) pathway for CH<sub>4</sub> assimilation and (B) suggested pathway for CO<sub>2</sub>
 reduction into formate.

A potential route for  $CO_2$  assimilation by the bacteria is described in Figure 3.B. The  $CO_2$  could indeed be reduced into formate by the direct action of FDH and in that case, the equation balance of the reaction would be:

$$CO_2 + NADH \rightarrow HCOO^- + NAD^+$$
 (Eq. 1)

275

where NADH is the reduced form of the Nicotinamide Adenine Dinucleotide (NAD) cofactor present in living cells. However, the stock of endogenous NAD is finite. For the CO<sub>2</sub> reduction reaction to occur (Eq. 1), the oxidized form of NAD (i.e. NAD<sup>+</sup>) has to also be continuously reduced into NADH (Fig. 3.B). Some intracellular enzymes such as  $\beta$ -hydroxybutyrate dehydrogenase are able to recycle NAD+ into NADH by simultaneously oxidizing an electron and proton donor source (Fig. 3.B).

281

Compared to the work of Xin (2007) [36], no methanol traces were evidenced in the samples even if the compound could have been potentially present in the reaction medium as a product of successive formate reductions catalyzed by FADH and then MDH (Fig. 3.B). One possible explanation for this phenomenon could

285 be that formate production was so high that it led to inhibition of FADH.

287 Furthermore, formate was assayed in the supernatant of the samples, meaning that the formate was external to 288 the cells. At this stage, it was assumed that the formate was produced inside the cells by the enzymatic 289 machinery required for both  $CO_2$  and NAD+ reductions and then released out of the cells. The probability that 290 these reactions were catalyzed by free enzymes resulting from cell lysis is low since the meeting probability 291 between FDH, CO<sub>2</sub>, NAD, and the enzyme regenerating NAD is low. Regarding formate excretion from the 292 cells, two phenomena could be assumed: (1) formate release could be due to a bacterial regulation process when 293 intracellular formate concentrations become too high for cell viability as formate does indeed have antimicrobial 294 properties [46] and it's intracellular accumulation could lead to cell death, and (2) population differentiation 295 could occur among the bacteria meaning that some bacteria could play the role of formate factories for the 296 survival of other bacteria consuming the formate. Formate is effectively reported in the literature as a precursor

- used by methanotrophic bacteria for cell maintenance reactions [47, 48].
- 298

299 A 5-day period seems to correspond to the adaptation phase for bacteria and their enzymes to their new carbon 300 substrate, i.e. CO<sub>2</sub> instead of CH<sub>4</sub>, before formate production occurs. A decrease in formate concentration (by 301  $27 \pm 1\%$ ) was then observed after 15 days (Fig. 1). This could be due to formate consumption. Bacterial 302 regulation or changes in bacterial population interactions or substrate limitation could be at the origin of this 303 decrease. However, the theoretical amount of CO<sub>2</sub> available in the initial CO<sub>2</sub>:air mixture of the headspace was 304 calculated according to the gas volume inside the vial (i.e. 54 mL) and the ideal gas equation. The calculated 305  $CO_2$  available (i.e. 1.09 mmol) was nearly 10 times higher than the maximum theoretical amount of  $CO_2$ 306 consumed for formate production (i.e. 0.10 mmol) assessed using Eq. (1). This means that there was no CO<sub>2</sub> 307 limitation and that the bacteria had an unlimited capacity for exogenous formate production; the result therefore indicates that the limiting factor was rather the source of electrons and protons (i.e. the internal PHB) required 308 309 for NAD recycling and thus for CO<sub>2</sub> reduction into formate (Fig. 3.B).

The initial PHB dry mass content of the bacterial suspension was found to be about  $15 \pm 5\%$  (data not shown). A theoretical calculation, considering that PHB was composed of 1 000 mononer units, showed that a PHB mass content of approximately 10% would indeed make it possible to reach the maximum concentration of formate produced (i.e. 750 mg·L<sup>-1</sup>). However, the exact number of units making up intracellular PHB is unknown and PHB could also be used in other pathways such as mixed acid fermentation. This hypothesis therefore needs further investigation. Much more experimental work is also required to clarify the explanations provided above and to specify the metabolic ways of this interesting CO<sub>2</sub> activation bioprocess.

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# 318 **4.** Conclusions

A bacterial consortium containing methanotrophs was able to reduce  $CO_2$  into formate with a positive carbon balance as bacterial biocatalysts were grown on methane, which is also a greenhouse gas. This bioprocess thus constitutes a new promising way to valorize  $CO_2$ . The role of each bacterium composing the consortium will be further investigated to both fully understand the mechanism and optimize formate production from  $CO_2$ . In

- 323 addition, formate production was shown to be enhanced by another phenomenon that is likely to be mixed acid 324 fermentation. At this stage, it is assumed that 17% of the total formate produced resulted from CO<sub>2</sub> reduction; 325 however, this content needs to be precisely quantified. The impact of operating conditions should also be studied in the future to control the contribution of  $CO_2$  reduction on mixed acid fermentation. Finally, another way to 326 327 optimize the process will focus on continuous formate recovery from the reaction medium and bipolar 328 electrodialysis will also be tested. 329 330 5. Acknowledgments 331 A. Ruiz-Valencia acknowledges the Conacyt from Mexico for his PhD scholarship. Mrs Virginie Latil is 332 thanked for reading and correcting the manuscript. SATT is thanked for partial financial support. 333 6. References 334 335 336 [1] GIEC, Climate Change 2014: Synthesis Report. Contribution of Working Groups I, II and III to the Fifth 337 Assessment Report of the Intergovernmental Panel on Climate Change, [Sous la direction de l'équipe de 338 rédaction principale, R.K. Pachauri et L.A. Meye] ed., Geneve, Suisse, 2014, p. 161. 339 [2] S. Moret, P.J. Dyson, G. Laurenczy, Nature communications 5 (2014) 4017. 340 [3] X. Zhang, Z. Wu, X. Zhang, L. Li, Y. Li, H. Xu, X. Li, X. Yu, Z. Zhang, Y. Liang, Nature communications 341 8 (2017) 14675. 342 [4] W.-H. Wang, Y. Himeda, J.T. Muckerman, G.F. Manbeck, E. Fujita, Chemical reviews 115 (2015) 12936-343 12973. 344 [5] M. Albrecht, U. Rodemerck, M. Schneider, M. Bröring, D. Baabe, E.V. Kondratenko, Applied Catalysis B: 345 Environmental 204 (2017) 119-126. 346 [6] F.A. Rahman, M.M.A. Aziz, R. Saidur, W.A.W.A. Bakar, M. Hainin, R. Putrajaya, N.A. Hassan, Renewable 347 and Sustainable Energy Reviews 71 (2017) 112-126. 348 [7] O. Ola, M.M. Maroto-Valer, Journal of Photochemistry and Photobiology C: Photochemistry Reviews 24 349 (2015) 16-42. [8] A.V. Puga, Topics in Catalysis 59 (2016) 1268-1278. 350 351 [9] F. Galli, M. Compagnoni, D. Vitali, C. Pirola, C.L. Bianchi, A. Villa, L. Prati, I. Rossetti, Applied Catalysis 352 B: Environmental 200 (2017) 386-391. 353 [10] E. Haviv, L.J. Shimon, R. Neumann, Chemistry-A European Journal 23 (2017) 92-95. 354 [11] J. Qiao, Y. Liu, F. Hong, J. Zhang, Chemical Society Reviews 43 (2014) 631-675. 355 [12] K. Malik, S. Singh, S. Basu, A. Verma, Wiley Interdisciplinary Reviews: Energy and Environment 6 (2017) 356 e244. 357 [13] A. Dibenedetto, A. Angelini, P. Stufano, Journal of Chemical Technology and Biotechnology 89 (2014) 334-353.
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