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Effect of exhaust gas recirculation composition on soot in ECN spray A conditions

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Abstract. Due to its strong impact on health, particulate matter is increasingly regulated by government emission standards for vehicles. As one of the sources of particulate matter is the soot produced by internal combustion engines, it remains a challenge to improve advanced combustion modes to reduce it. There is still, however, some lack of understanding about the formation and oxidation processes of soot, especially in “realistic” conditions, such as for example at high temperature and pressure conditions with or without the presence of exhaust gases. The objective of this study is to investigate soot formation in the case of *n*-Dodecane spray flames at conventional Diesel engine conditions generated in the New One Shot Engine by using diffused back-illumination extinction with different CO₂ and water vapour contents. It was found that CO₂ addition reduces the soot mass fraction if its volumetric concentration in ambient mixtures is at least 4.5% while 1% of water is sufficient to significantly reduce the soot mass fraction. The impact of the ambient mixture obtained in ECN spray A pre-burn vessels was also investigated to assess the accuracy against soot measurements available in the literature.

1 Introduction

Human exposure to soot is responsible for cancer, cardiovascular diseases and respiratory diseases [1]. Soot is an amorphous carbon substance, generally produced during combustion processes. In the case of conventional Diesel combustion, the formation of soot is due to the reduced amount of air available to burn the fuel completely at high temperature and pressure conditions during fuel spray combustion, especially during the diffusion phase [2]. Soot formation is also affected by the presence of other ambient gases such as CO₂ or H₂O [3, 4]. These gases induce (i) a reduction in interparticle interaction caused by dilution (ii) a change in temperature and heat capacity of the flame caused by thermal effects, and (iii) chemical reactions that either oxidize soot or react with gaseous precursors. As, in modern internal combustion engines, one way to strongly reduce NO_x is the recirculation of exhaust gas, the presence of CO₂ or H₂O in the combustion chamber is now usual and can impact soot formation. Several numerical and experimental studies about their effects on ethylene (both premixed and diffusion flames) [5–8] concluded that they have an effect on soot reduction, due especially to chemical effects.

Measuring the volume fraction of soot requires the use of optical diagnostics with optimised signal processing.

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In the context of the Engine Combustion Network [9], it is mainly measured by means of two optical techniques: light based extinction techniques usually called Diffused Back-Illumination (DBI) and Laser-Induced Incandescence (LII) [10, 11]. The first method is based on the attenuation of light through the soot cloud due to elastic scattering and to absorption by the soot particles. However, in the case of Spray A conditions, *i.e.* 900 K and 60 bar as ambient thermodynamic initial conditions, the beam steering is so strong that it becomes difficult to distinguish absorption- or scattering-induced attenuation [12]. Therefore, Ghandhi and Heim [13] worked on the quality of the collimated light needed for DBI and its transmission within the region of interest. In their study, the collimated light of an automotive headlamp was passed through a pinhole and was collected by a Fresnel lens before being transferred to an engineered diffuser to direct it towards the region. A high intensity pulsating LED with 100 W peak optical power to be used as source for the soot measurement in high pressure-high temperature spray flames was developed recently [12, 14]. This modified technique is considered as the ECN reference. The data obtained in the Constant volume Preburn Vessel (CPV) were compared with simulation results obtained from different soot models coupled with a large-eddy simulation for *n*-Dodecane combustion [10, 15–17] or a *k*- ϵ turbulence model [18, 19]. The simulations were validated with 15% of oxygen and various combustion products. To complete the available database

and to improve modelling concepts, a parametric study on the effects of EGR composition on soot formation for ECN spray A is needed.

In the present study, the New One Shot Engine (NOSE) was used as experimental set-up since the initial conditions required for ECN-spray A are attainable and the ambient mixture composition can be adjusted as desired [20]. The experiments were conducted for Spray A conditions, *i.e.* 900 K and 22.8 kg/m³ with an oxygen concentration of 15% but with a variation of Nitrogen (N₂) content with the addition of CO₂ (0–7% vol) and H₂O (0–5% vol). Moreover, to evaluate the robustness of previous results obtained in other vessels (such as constant pressure flow or constant pre-burn), the impact of ambient compositions similar to those in a CPV as in [9], *i.e.* 6.22% CO₂ and 3.62% H₂O, on soot production was also explored.

The next Section 2 discusses the experimental setup and conditions, and is followed by Sections 3–5.

2 Experimental setup and conditions

2.1 Experimental facility

The main specifications of NOSE, a one-shot rapid compression machine, and the Spray A – ECN conditions, *i.e.* 900 K, 22.8 kg/m³, are summarized in Table 1 and fully described in [21]. The *n*-Dodecane fuel was injected through a BOSCH CR2.16 single hole injector at the injection pressure of 150 MPa in the optical chamber filled with a mixture of ambient gases at a constant O₂ percentage of 15% vol (Tab. 2).

2.2 Ambient gas composition matrix

Table 2 shows the different compositions of ambient gases selected with a constant oxygen concentration (15% vol) and the adjustment of N₂, alone, according to the addition of CO₂ and H₂O. Moreover, to perform tests at a constant ambient gas density inside the chamber the back pressure (P_{back}) and the temperature at the injection timing were adjusted. The theoretical adiabatic temperature of the air/fuel mixture for the global equivalence ratio (0.0313) as a function of the ambient gas composition is also indicated.

2.3 Optical techniques

Two optical measurements were simultaneously used. First, the OH* chemiluminescence imaging technique was set up to obtain the Lift-Off Length (LOL) of the flame by using an intensified CMOS camera (Photron – APX-I2) with a UV lens 60 mm f/3.5 and a BP filter centered at 310 nm with FWHM at 10 nm. The frame rate was kept at 2 kHz. During the steady phase of combustion (1800–3000 μ s after SOE), three images were analysed following the post-processing recommended by [22].

Second, the measurement of soot was done by DBI, based on the transmission of an initial light with I_0 as intensity. When this light passes through the sooting flame, a certain amount of the light is absorbed and scattered by

Table 1. Main specifications of new one shot engine for spray A conditions.

Specifications	Value
Volume of the chamber	~0.24l
Injector tip protrusion	6 mm
Wall temperature	373 K
Fuel	<i>n</i> -Dodecane
Injection pressure	150 MPa
Orifice diameter	89.7 μ m, $K_s = 1.5$, $Cd = 0.96$
Ambient temperature	900 K
Ambient density	22.8 kg/m ³
Injection duration	~3.2 ms

the soot and the remainder is transmitted to the receiver, with an intensity of I . Using Beer-Lambert's law, the amount of soot can be deduced with the product of the path length, L and the extinction coefficient, K [23]:

$$\frac{I}{I_0} = e^{-KL}. \quad (1)$$

Figure 1 shows the schematic of the DBI setup around NOSE. The light source was generated by a green LED (CBT-120-GC11-JM200) at $\lambda = 532$ nm. The illuminating rays of the LED were transferred to a Fresnel lens with an effective diameter of 63.5 mm and a focal length of 99 mm through a pinhole to generate parallel light beam. Then these rays were transferred to an engineering diffuser to generate a homogeneous distribution of the light in the region of interest. The images of the transmitted light were captured by a Phantom V16 CMOS camera at the frame rate of 45 kHz. An AF Micro-Nikon 50 mm f/1.8 D lens with two filters, a BP filter centered at 532 nm with 10 nm FWHM and a neutral density filter of 75% were used.

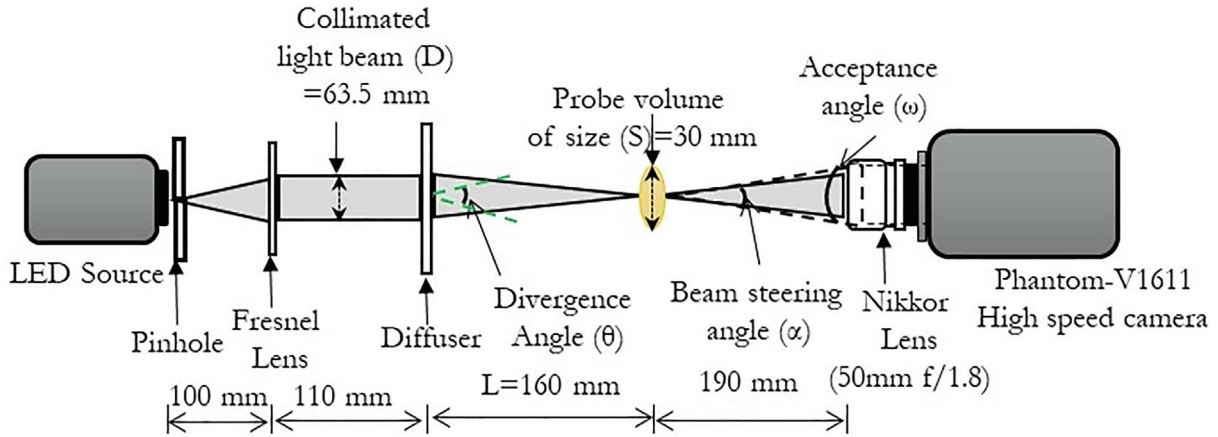
The first challenge when applying the DBI technique is to reduce beam steering by choosing the optimal distance between the different optical elements as presented in Figure 1. As indicated in equation (2), the divergence angle of the diffuser, θ must be larger than the sum of the maximum anticipated beam steering angle, α with the acceptance angle of the collecting optics, ω , as underlined in [23]. If the divergence angle of the diffuser is not large enough, then there is a possibility that some area of the extinction beam might be moved out of the imaged area. However, the diffuser used in our setup has a 15° divergence angle θ and the acceptance angle ω of our optics is 8.36°, this system therefore ensures a beam steering angle, α of 6.64° which is large enough to fulfil the first requirement [9]:

$$\theta \geq \alpha + \omega. \quad (2)$$

The second criterion is the size of the collimated beam. The beam diameter, D should be higher than the sum of the probe volume, S and the tangential of the addition of the beam steering angle and the acceptance angle across the length L , between the probe volume and the CMOS

Table 2. Test conditions.

Nomenclature	Ambient gas composition (% volume)				P_{back} at injection timing (MPa)	T at real injection timing [K] ± 4 K	Adiabatic Flame Temperature ($T_{\text{adiabatic}}$) K
	O ₂	N ₂	CO ₂	H ₂ O			
0% CO ₂ /0% H ₂ O	15.00	85.00	x	x	6.0	901	957
2% CO ₂	15.00	83.00	2.00	x	5.9	901	957
4.5% CO ₂	15.00	80.50	4.50	x	5.8	898	954
7% CO ₂	15.00	78.00	7.00	x	5.7	890	946
1% H ₂ O	15.00	84.00	x	1.00	6.0	901	957
2% H ₂ O	15.00	83.00	x	2.00	6.0	901	957
3% H ₂ O	15.00	82.00	x	3.00	6.0	900	956
4% H ₂ O	15.00	81.00	x	4.00	6.0	898	953
5% H ₂ O	15.00	80.00	x	5.00	6.0	895	950
6.22% CO ₂ + 3.63% H ₂ O	15.00	75.15	6.22	3.63	5.7	889	945

**Fig. 1.** Detailed optical arrangement at DBI setup.

sensor. If this criterion is not fulfilled, there will be beam steering along the edges of the probe volume,

$$D \geq S + \tan(\alpha + \omega) \cdot L. \quad (3)$$

This is obtained for the present optical setup for a beam steering angle, $\alpha = 2.86^\circ$ [12].

Another issue is the effect of the “negative image lag”, due to the incomplete reset of the CMOS sensor during the pixel readout. The residual signal with this negative image lag affects the next image and therefore the estimate of KL. However, this effect can be removed by analysing a third image without LED. In our case a comparison of LED off frame with and without LED pulsing showed that the residual negative signal is negligible. The high speed camera acquired the images with and without LED light, a frame rate of 45 kHz with an exposure time of 3 μ s while the LED frequency was kept at 22 500 pulse/sec, as shown in Figure 2. This choice is a good compromise between a good temporal resolution, a high stability of the light-source intensity and very low negative image lag.

2.4 Image processing

Figure 3 describes the different steps followed to post-process the DBI image as recommended in [23] by the ECN. The first image corresponds to when the LED is ON, and consists of the LED signal and the natural luminosity of the soot cloud, $I_{\text{LED+NL}}$. Complete LED-light extinction is never measured. The second image is obtained for the LED off frame and consists purely of the natural luminosity signal, I_{NL} . Images of the background due to the dark noise were previously recorded and due to the CMOS technology, it was considered as to be zero. The third image represents the light intensity without flame and soot, I_0 in the probe volume S . Soot extinction, KL, for one DBI image, j , is obtained thanks to equation (1),

$$\text{KL} = -\ln\left(\frac{I_{\text{LED}}}{I_0}\right), \quad (4)$$

where $I_{\text{LED}} = I_{\text{LED+NL},j} - I_{\text{NL},j-1}$.

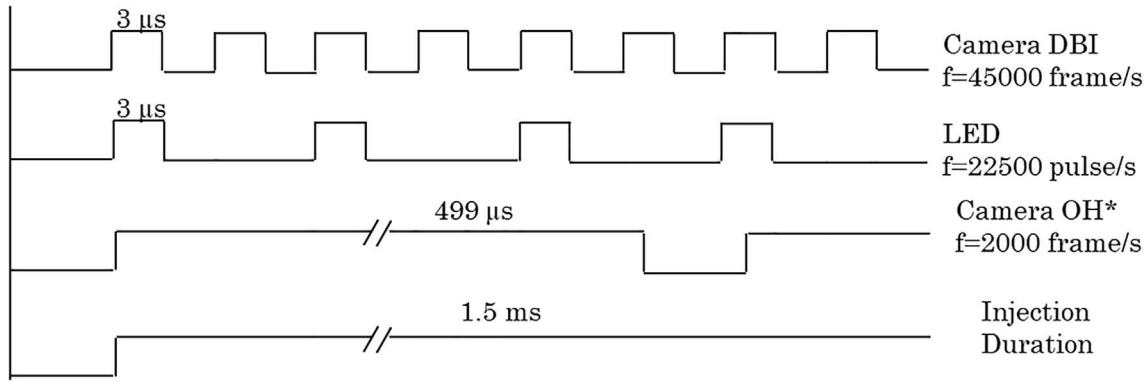


Fig. 2. Signal arrangement for the setup.

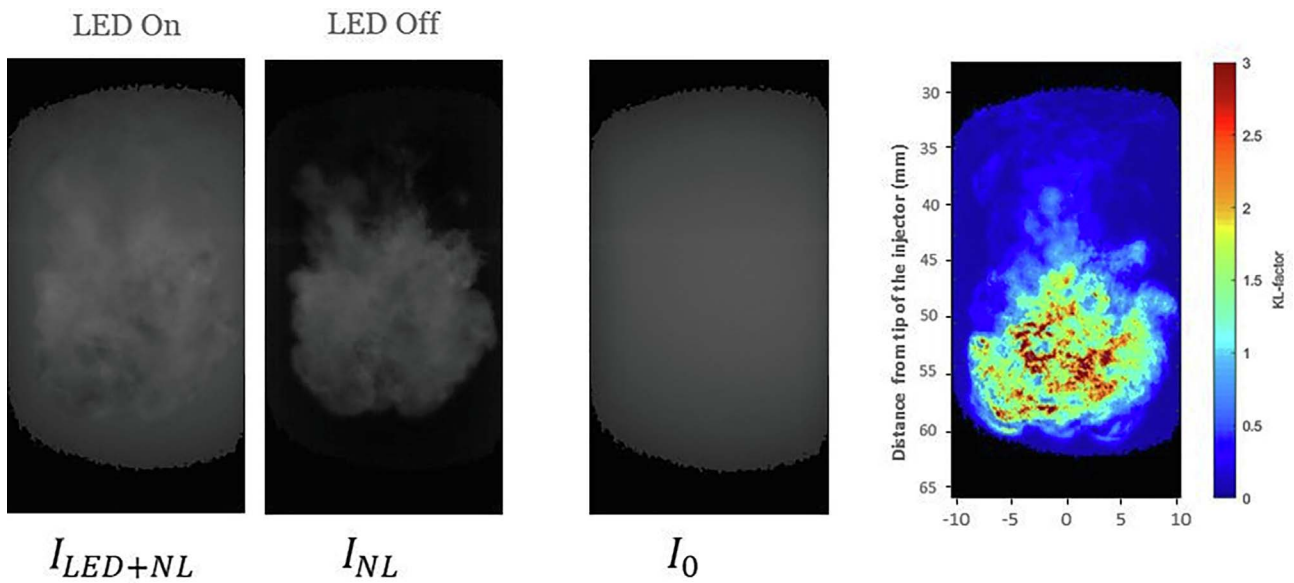


Fig. 3. Steps for the post processing of the KL factor.

The image presented in the right-most panel of Figure 3 corresponds to the processed image: a 2D distribution of soot extinction, KL.

The soot mass can be estimated by equation (5), with ρ_{soot} , the soot density, considered as 1.8 g/cm^3 as in [24], k_e , the non-dimensional extinction coefficient, set at 7.46 as in [25] and dx, dy the pixel sizes, here $11.2 \mu\text{m}/\text{pix}$,

$$m_{\text{soot}} = \frac{\lambda_{\text{LED}} \rho_{\text{soot}}}{k_e} dx \int_{-R}^R \text{KL} dy. \quad (5)$$

3 Results

This section is divided into three parts. The first part focuses on the comparison between the results obtained in the reference condition, *i.e.* 15% O_2 , 85% N_2 and the ECN pre-burn condition, namely with CO_2 and H_2O residue from the pre-combustion (15% O_2 , 75.15% N_2 , 6.22% CO_2 , and 3.63% H_2O). The second and the third parts will

cover the effects of CO_2 and water vapour addition on the flame soot, respectively.

3.1 Effect of pre-burn products

Figure 4 presents an example of the soot extinction images obtained at 15% O_2 , 75.15% N_2 , 6.33% CO_2 , and 3.62% H_2O , representing ECN pre-burn conditions in comparison with those obtained without any exhaust gases *i.e.* the reference condition of 15% O_2 and 85% N_2 , the reference condition, from 1.022 ms to 1.689 ms after the start of injection. For the two cases, the soot area increases with the combustion development. Soot formation starts in the periphery of the jet, due to the higher temperature and comparatively leaner mixture in the surrounding as compared to the central part of the jet [26]. During the flame development, soot volume fraction increases at the core of the jet (images from 1.378 ms to 1.689 ms) and stabilizes at the periphery. According to Cenker *et al.* [26] the air entrainment increases, soot first starts to oxidize in oxygen-rich high-temperature

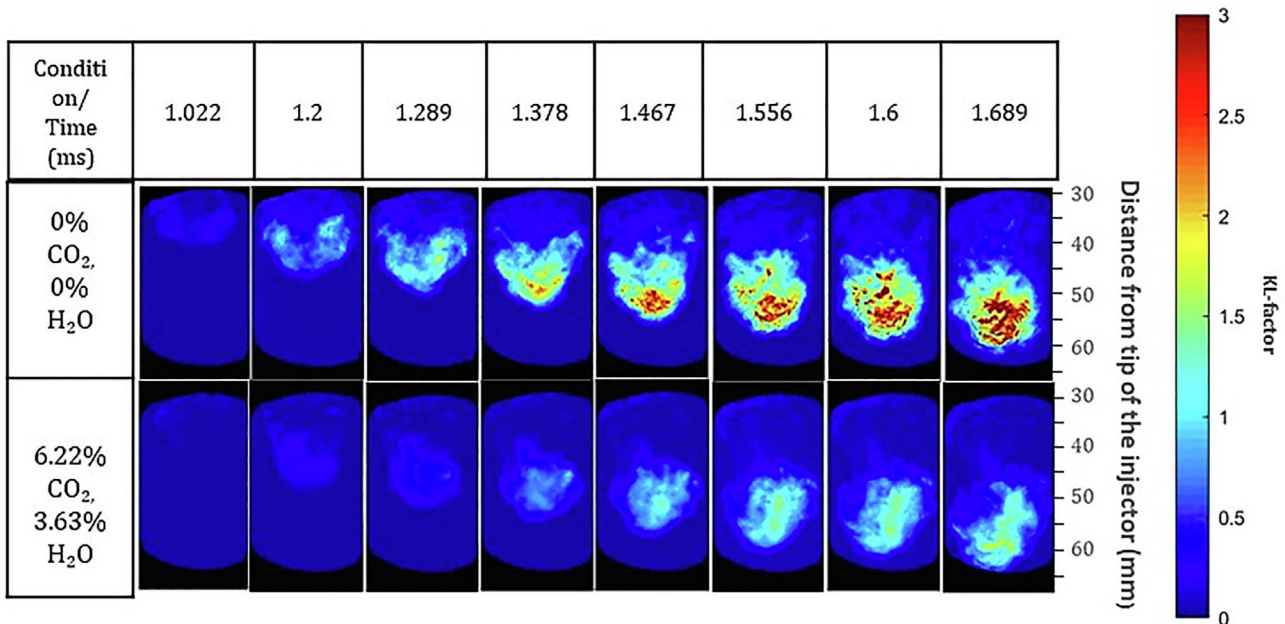


Fig. 4. Example of soot extinction images – comparison with ECN preburn gases composition and no exhaust gases in ambient gases (reference case).

zones such as the boundaries of the jet. The highest level of soot extinction is observed at the head of the front at 1.689 ms. After this event, the head of the soot cloud is outside the observation area but traces of the soot are observed till ~ 4 ms for the tail of the flame.

In this example, two trends can be observed: the soot onset time is shifted when pre-burn gases are taken into account in the ambient gases, and the extinction level is decreased by at least half. Ten repetitive tests were conducted to determine an average image. The maximum soot extinction value is 3 for the ECN pre-burn condition, against 4.5 for the reference condition. In Figure 5, the average KL factor, normalized by the maximum value obtained for the reference case is plotted as a function of the time After the Start of Injection (ASOI). The temporal evolution of KL values follows the same pattern as that presented by Musculus and Pickett [27] or [11, 23]. KL values reach the maximum when the head of the jet passes through the field of view. Once the head of the jet has passed through this position, the tail of the flame appears in the observation window till ~ 4 ms. In this part, the KL factor decreases by 40% in the two cases.

Figure 6a presents the estimate of soot mass 50 mm from the injector tip for ECN and reference conditions. The soot mass is reduced by 50% with the presence of 6.22% CO₂ and 3.63% H₂O in the ambient gases. Figure 6b presents the comparison between the total soot mass for both conditions with the results obtained in [7], named “SNL CVP vessel”. The soot mass fraction for the ECN condition with pre-burn constituents in the ambient gases is around half of 51 μg , obtained in reference conditions. The value of, 25 μg is in good agreement with the results obtained in the actual pre-burn vessel [9]. Thanks to this comparison, it is highlighted that this reduction can be mainly attributed to the presence of inert gases, here

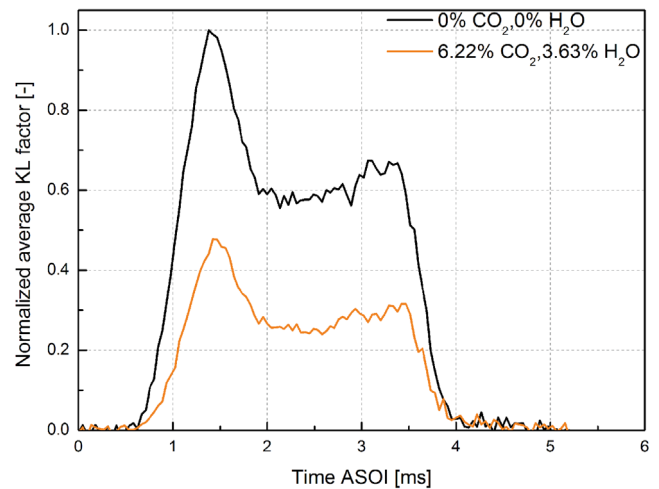


Fig. 5. Normalized average KL factor for ECN condition with pre-burn ambient gases composition and for reference condition, 15% O₂ and 85% N₂.

a mixture of CO₂ and H₂O, certainly due to the chemical reaction supported with dilution and thermal effects as discussed below.

3.2 Effects of CO₂ addition on soot

The average KL factor, obtained for 10 individual tests, and normalized by the maximum value obtained for the reference condition is presented in Figure 7a for the four amounts of CO₂. It can be clearly seen that the soot onset time is shifted. This shows that 2% CO₂ does not affect the soot extinction levels but that a significant decrease is obtained when at least 4.5% is added. In Figure 7b, the

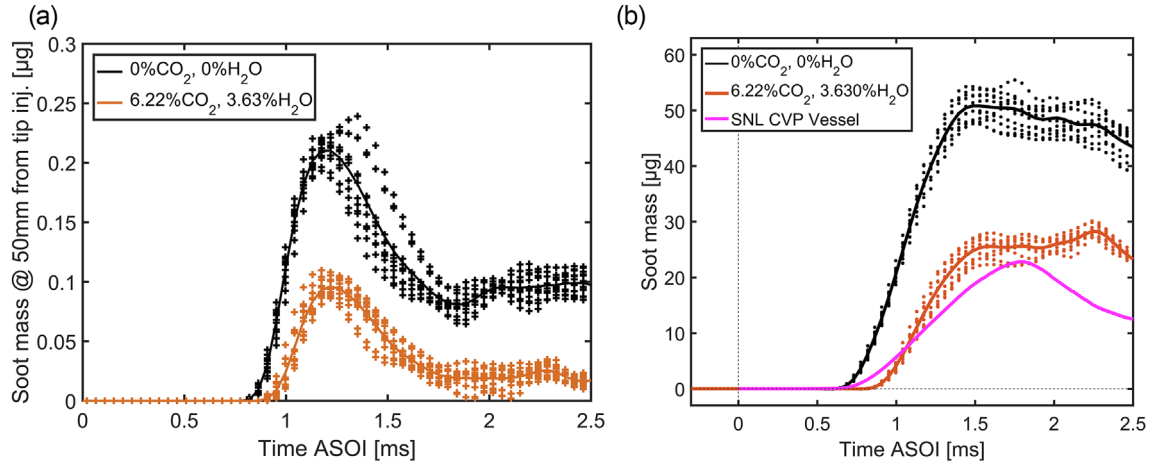


Fig. 6. (a) Soot mass 50 mm from the injector tip, (b) soot mass comparison with results in pre-burn vessel [9].

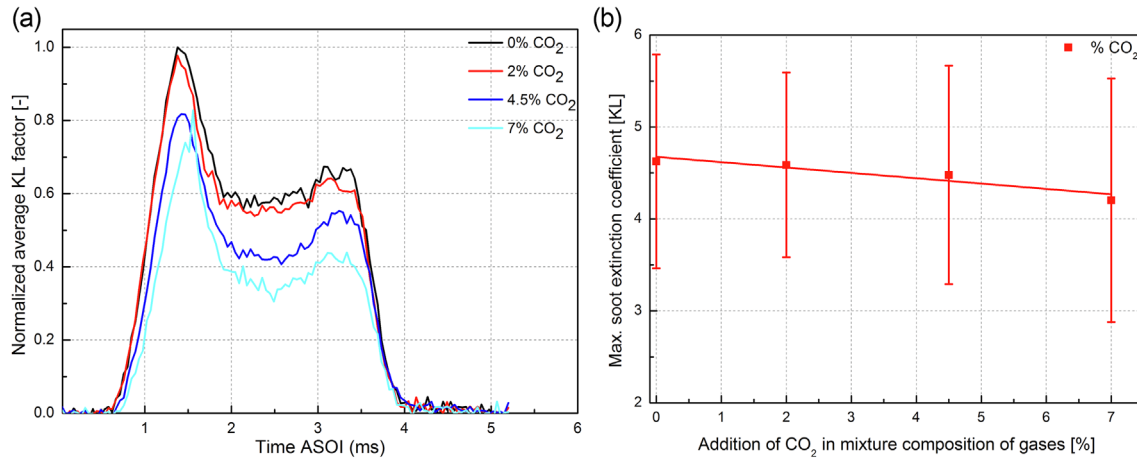


Fig. 7. (a) Normalized average KL factor *versus* time, (b) maximum of KL factor *versus* CO₂ content.

linear decrease of the maximum KL value is presented as a function of CO₂ content. For example, with 4.5% of CO₂ the maximum KL factor is decreased by 5.4%. These trends are also highlighted by the plot of the total soot mass estimate on the field of view (Fig. 8a). The highest quantity of total soot mass is observed for 0 and 2% CO₂ addition with a maximum at ~51 µg and ~48 µg respectively, while 4.5 and 7% addition of CO₂ decrease this maximum to ~43 µg and ~35 µg. Thus, a simple linear relationship can be suggested as expressed in equation (6) and seen in Figure 8b with a *R*-square of 0.97:

$$\frac{m_{\text{soot, CO}_2\%}}{m_{\text{soot, 0\%}}} = 1 - 0.045 \cdot \text{CO}_2\% \quad (6)$$

3.3 Effect of H₂O addition

The same trends can be observed with a variation in H₂O content from 1% to 5%: a shift of soot onset time and a reduction in the extinction level. However, as soon as 1% H₂O is introduced, a significant effect is observed on the

average KL factor, with ~15% of reduction, as can be seen in Figure 9a. This trend is highlighted by the evolution of the maximum KL factor *versus* the percentage of H₂O, plotted in Figure 9b. A 20% reduction in this maximum is obtained when 5% H₂O is added.

Figure 10 presents the total soot mass (a) and the maximum soot mass reached between 1 ms and 2 ms after the start of injection (b) as a function of water vapour content in the ambient mixture. The impact on the soot mass is pronounced, as, the maximum value of total soot mass is reduced to 38% with 5% H₂O compared to the reference case. The following linear relationship (*R*-square = 0.95) can be suggested

$$\frac{m_{\text{soot, H}_2\text{O}\%}}{m_{\text{soot, 0\%}}} = 1 - 0.066 \cdot \text{H}_2\text{O}\% \quad (7)$$

4 Discussion

It was clearly observed that H₂O has a stronger effect on soot reduction than CO₂. For example, 2% of CO₂ or

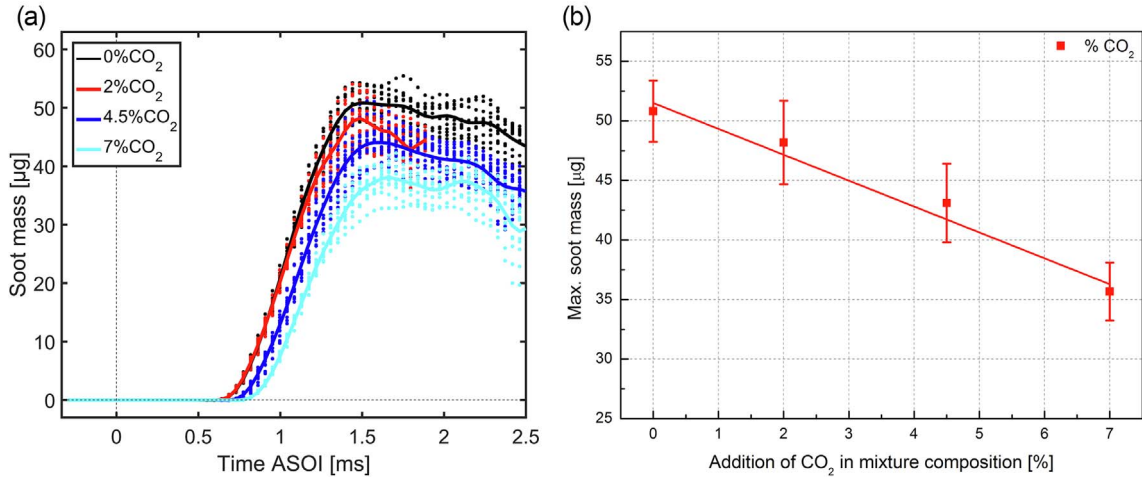


Fig. 8. Comparison of soot mass for different CO₂ content in ambient mixture (a) total soot mass, (b) maximum of soot mass between 1 ms and 2 ms ASOI.

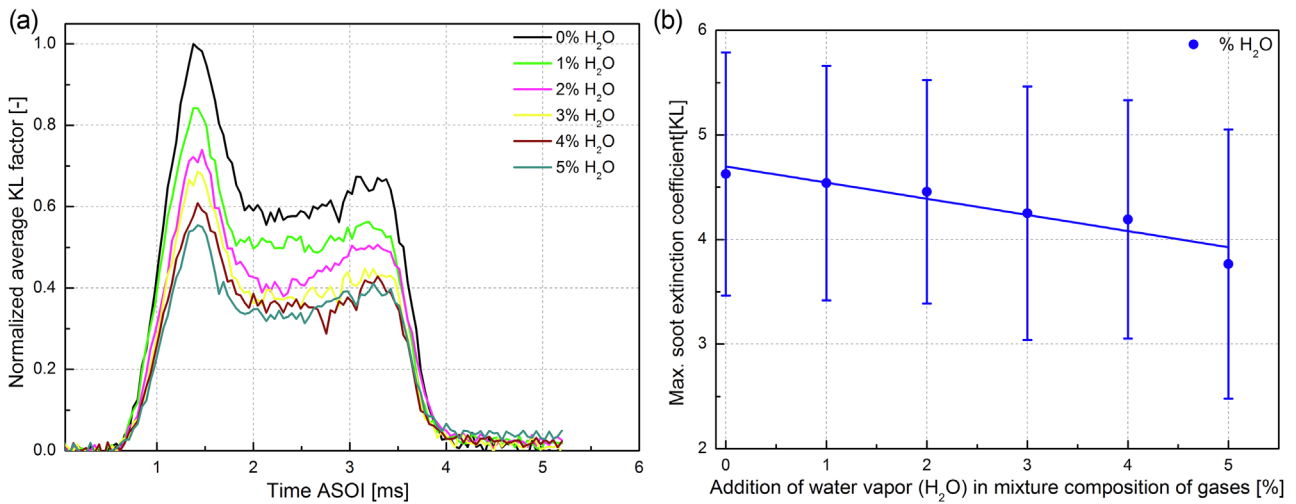


Fig. 9. (a) Normalized average KL factor as a function of H₂O content, (b) maximum soot extinction coefficient as a function of H₂O content.

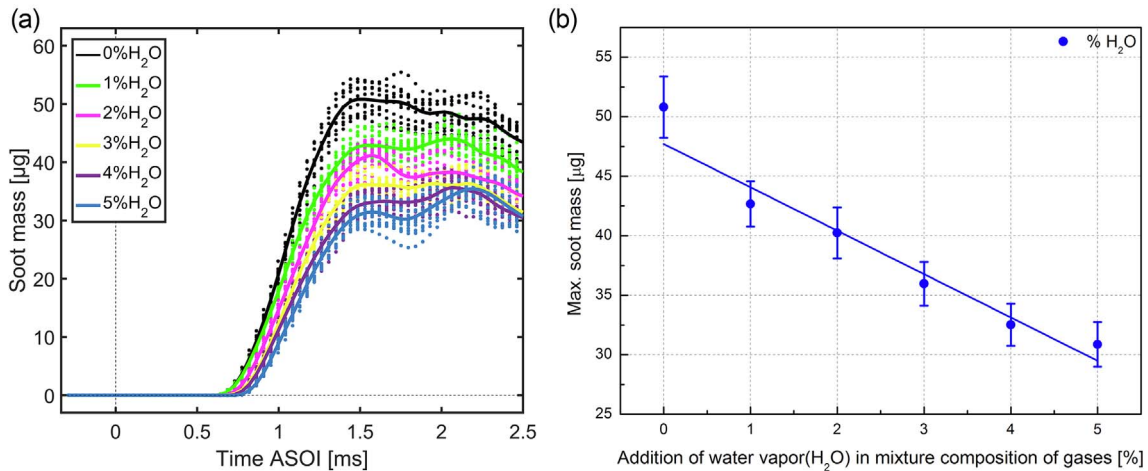


Fig. 10. Comparison of soot mass fraction as a function of H₂O content in mixture composition (a) total soot mass, (b) maximum soot mass between 1 ms and 2 ms ASOI.

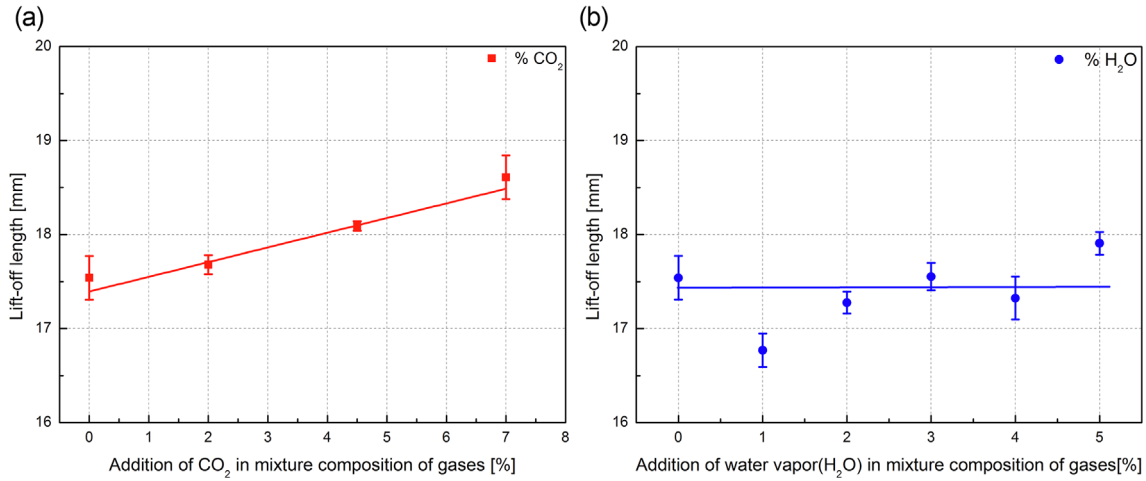


Fig. 11. Lift-off length as a function of the (a) CO₂ or (b) H₂O addition in ambient gases.

of H₂O resulted in a 5% and 20% reduction in the maximum soot value, respectively. Similar results were observed by Zhang *et al.* [6]. They found a more significant reduction of Polycyclic Aromatic Hydrocarbons (PAH) formation by H₂O when compared to CO₂ for the same blending ratio in laminar premixed C₂H₄/O₂/Ar flames. The soot onset time is also more delayed with H₂O compared to CO₂.

The reduction in soot with the addition of CO₂ or H₂O in ambient gases can be attributed to different effects. First, due to the thermal capacities of these species in comparison to N₂, the flame temperature has to be reduced [28]. It can be noted that 7% CO₂ induced only a ~1.15% reduction in the adiabatic flame temperature (so from 957 K to 946 K) and 5% H₂O induced only a ~0.73% reduction in the adiabatic flame temperature (from 957 K to 950 K). As the impact on temperature is very small, other effects have to be considered according to [4].

The presence of CO₂ or H₂O in the ambient gases can also affect the location of the flame stabilization. This is highlighted in Figure 11 where an increase in the lift-off length can be noticed in the case of CO₂ (Fig. 11a) but not in the case of H₂O (Fig. 11b) as the variation is on the same order of variability. In fact the LOL depends on the initial ambient temperature [29] and in Table 2, the addition of CO₂ induces an initial temperature reduction of 11 K while only 6 K with the addition of H₂O. Figure 12 highlights the good correlation between LOL and the scaling law LOL* [29]. The variation in initial ambient temperature could explain the evolution of the LOL with addition of CO₂.

The flame with addition of CO₂ is stabilized in a leaner area, which could contribute to a soot reduction [29, 30]. However, as the effect of H₂O is greater than of CO₂, the soot reduction has to be mainly attributed according to [3, 5, 6, 31], to the chemical reactions.

In the case of CO₂, an interaction with H radicals such as CO₂ + H ↔ OH + CO, increases the amount of hydroxyl radicals, which enhances the oxidation process of the soot precursors. In the case of H₂O, as specified in [5], both

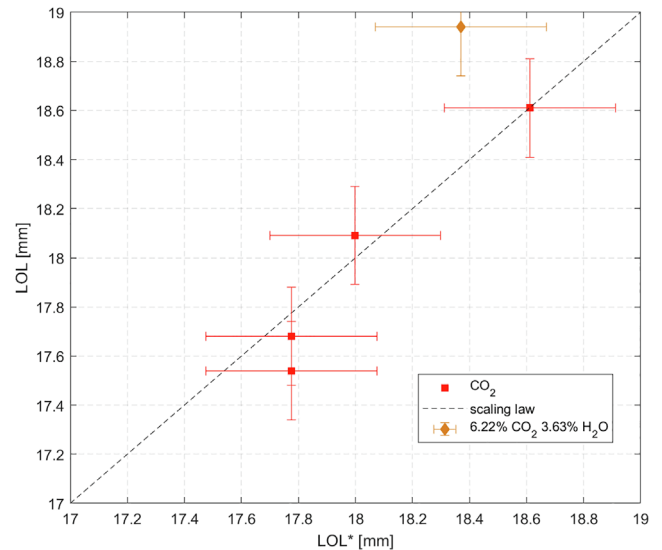


Fig. 12. LOL_i versus LOL* with addition of CO₂ LOL* = $LOL_{ref} \left(\frac{T_{amb}}{T_{ref}} \right)^{-3.74}$ with $LOL_{ref} = 17,85$ mm and $T_{ref} = 900$ K.

the reverse reactions of H₂O + H ↔ OH + H₂ and H₂O + O ↔ OH + OH mainly contribute to reducing the formation of soot. According to Teini *et al.* [3], the addition of CO₂ and H₂O influences the growth of OH radicals in different areas of the flame. While CO₂ may begin to deplete soot mass through OH radical attacks in the oxidation zone, H₂O, inhibited PAH molecule growth reactions in fuel rich, soot formation regions. It results in the higher reduction of soot with H₂O addition as compared to CO₂.

5 Conclusion

Thanks to the NOSE experimental set-up, the effects of presence of CO₂ and H₂O in ambient mixtures on soot

formation were evaluated for the first time in the case of dodecane spray combustion. It was clearly observed that H₂O has a stronger effect on soot reduction than CO₂, as previously observed in ethane flames. The soot reduction is certainly due to reactions between H radicals and CO₂ or H₂O and between O radical and H₂O. The reactions promote OH radicals which are reduced by oxidation in PAH. By combining CO₂ and H₂O in the ambient mixture as in real ECN pre-burn conditions, a reduction of 50% in comparison to the reference condition (15%O₂ + 85%N₂) is estimated and is in very good agreement by real measurements in a pre-burn vessel. This confirms that the presence of these species has to be considered in any simulations of results for ECN pre-burn vessels in order to increase the model prediction accuracy.

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