

## Opportunities and Challenges for Organic Electrodes in Electrochemical Energy Storage

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# CHEMICAL REVIEWS

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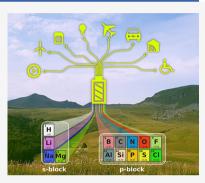
Review

### <sup>1</sup> Opportunities and Challenges for Organic Electrodes in <sup>2</sup> Electrochemical Energy Storage

3 Philippe Poizot,\* Joël Gaubicher, Stéven Renault, Lionel Dubois, Yanliang Liang, and Yan Yao

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4 **ABSTRACT:** As the world moves toward electromobility and a concomitant decarbon-5 ization of its electrical supply, modern society is also entering a so-called fourth industrial 6 revolution marked by a boom of electronic devices and digital technologies. Consequently, 7 battery demand has exploded along with the need for ores and metals to fabricate them. 8 Starting from such a critical analysis and integrating robust structural data, this review aims 9 at pointing out there is room to promote organic-based electrochemical energy storage. 10 Combined with recycling solutions, redox-active organic species could decrease the pressure 11 on inorganic compounds and offer valid options in terms of environmental footprint and 12 possible disruptive chemistries to meet the energy storage needs of both today and tomorrow. 13 We review state-of-the-art developments in organic batteries, current challenges, and prospects, 14 and we discuss the fundamental principles that govern the reversible chemistry of organic 15 structures. We provide a comprehensive overview of all reported cell configurations that involve



16 electroactive organic compounds working either in the solid state or in solution for aqueous or nonaqueous electrolytes. These 17 configurations include alkali (Li/Na/K) and multivalent (Mg, Zn)-based electrolytes for conventional "sealed" batteries and redox-flow 18 systems. We also highlight the most promising systems based on such various chemistries relying on appropriate metrics such as 19 operation voltage, specific capacity, specific energy, or cycle life to assess the performances of electrodes.

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#### **1. INTRODUCTION**

# 1.1. Current Status in Electrochemical Energy Storage in 122 Short

123 The need to build innovative electrochemical energy storage 124 (EES) technologies and conversion solutions is now recog-125 nized to be particularly critical not only by specialists in the 126 field but also by ordinary consumers eager to use different nomadic electronic devices which make their life easier, safer, 127 and more enjoyable. Representative devices of EES are 128 rechargeable (or secondary) batteries and (super)capacitors. 129 Chemists, electrochemists, and materials science researchers 130 helped by theoreticians (see for example the Materials Genome 131 Project launched by G. Ceder<sup>1</sup>) have already thoroughly 132 screened the periodic table of the elements in the quest to find 133 the best electrode associations essentially focused on increased 134 gravimetric and volumetric energy densities while improving 135 the safety, power, lifetime, and cost. Thus, decades of intensive 136 and innovative research have enabled us to develop and to 137 place on the market different kinds of primary and secondary 138 batteries able to power an increasingly diverse kind of appli- 139 cations from microchips to the emerging large-scale application 140 markets.<sup>2</sup> Without describing them one by one, it must be 141 underlined that the pioneered lead-acid (PbA) battery devised 142 by G. Planté in 1859 is still in growing demand because it is 143 unrivalled for microhybrid and internal combustion vehicles 144 or large-scale power storage units (load-leveling applications, 145 uninterrupted power supply (UPS) for entire cities) at this 146 time; this technology is also robust, safe, and affordable 147 associated with efficient recycling and disposal management 148 programs notably to prevent lead emission.<sup>3</sup> Regarding Li-ion 149 batteries (LIBs)—the current flagship technology to get high 150 energy densities-thanks to substantial improvements and 151 notably the discovery of new insertion positive electrode materials 152 (e.g., LiFePO<sub>4</sub>, LFP; Li(Ni<sub>1/2-x</sub>Mn<sub>1/2-x</sub>Co<sub>2x</sub>)O<sub>2</sub>, NMC; Li-rich 153 layered oxides  $Li(Li_{x}M_{1-x})O_{2})$ , they have become essential to 154 power the vast world of electronic equipment, robots, ongoing 155 electric transportation technologies, and some stationary 156 applications too. Consequently, nickel/metal hydride (Ni/ 157 MH) rechargeable batteries, which have fully replaced nickel/ 158 cadmium (Ni/Cd) cells, are struggling to compete with LIBs 159 in the light of recent achieved progress including at the price 160 level. For the moment, Ni-MH batteries still power more than 161 10 million hybrid electric vehicles, and companies like BASF- 162 Ovonic maintain their R&D activities.<sup>4</sup> Redox flow batteries 163 (RFBs) represent another promising choice for stationary 164 energy storage because this particular cell configuration 165 operating basically with redox-active solutions is more durable 166 and scalable than conventional "sealed" battery systems 167 working with solid state electrode materials. The major plants 168 ever built to date are essentially based on the vanadium/ 169 vanadium redox flow battery technology (VRFB)<sup>5</sup> first 170 patented and developed by Skyllas-Kazacos in Australia in 171 the mid 80s.<sup>6–8</sup> This rapid survey shows that all commercially 172 available electrochemical storage solutions deal with redox- 173 active inorganic systems, which poses now more than ever 174 certain problems in terms of metal resource constraints, pro- 175 duction cost, and environmental footprint in view of the ever 176 growing demand. 177

#### 1.2. Rise of Organics for Electrochemical Energy Storage

For several reasons, which will be thoroughly explained later, it 178 is now recognized that searching for organic matter-based 179 electrodes could bring new chemical opportunities to further 180 improve existing EES technologies while opening new play- 181 grounds to create innovative cell configurations. Thus, over the 182 last ten years, tremendous progress has been made to promote 183 electroactive organic systems attracting much interest from 184 the broad electrochemical storage community. This occurs to 185 such an extent that today we are witnessing a considerable 186 increase in the literature on the subject, ranging from 187 188 nonaqueous/aqueous RFBs to nonaqueous/aqueous "sealed" 189 batteries including both organic polymers and crystallized 190 organic compounds as will be developed in this article. In only 191 ten years, more than 45 review papers have been published for 192 which the scope was initially broad but in view of the booming 193 of primary research papers due to the versatility of the organic 194 synthesis and molecular engineering. The most recent reviews 195 are now focused on thematic research areas although it should 196 be recognized that some of them overlap. In the following list 197 sorted by year, the reader can find the series of review papers 198 on organic-based EES published since 2012 including notably 199 several remarkable contributions of both Chen's group at Nankai 200 University and Schubert's group at Friedrich Schiller University: 201 2012,<sup>9,10</sup> 2013,<sup>11,12</sup> 2015,<sup>13–15</sup> 2016,<sup>16–27</sup> 2017,<sup>28–35</sup> 2018,<sup>36–46</sup> 202 2019.<sup>47–58</sup>

Basically, before 2011 the literature on the topic was clearly 203 204 limited. The reference review article dealing with organic 205 electrodes in this period was published by Novák et al. in 206 1997<sup>59</sup> on the basis of the existing literature focused at that 207 time only on conducting polymers following the discovery 208 of polyacetylene (PAc) by Shirakawa in 1974<sup>60</sup> and its 209 subsequent chemical "p- or n-doping" (see section 4.3) to give 210 a series of semiconductors and ultimately "organic metals" 211 thanks to overlap of adjacent  $\pi$ -orbitals.<sup>61-64</sup> A few years later, 212 the possible use of PAc as electrode material to store electricity 213 was readily demonstrated by MacDiarmid taking advantage of 214 both p- or n-doping.<sup>65,66</sup> Channels were opened to develop 215 other conjugated polymers such as polyaniline (PAni), polypyrrole 216 (PPy), or polythiophene (PT), which were particularly 217 explored in the 80s as positive electrode materials in "dual-218 ion cell configurations" (see section 4.3) using metals or alloys 219 as the negative electrode (e.g., lithium (Li), sodium (Na), or 220 the stoichiometric lithium-aluminum alloy (LiAl)), which led 221 to the first practical polymer batteries with the commercializa-222 tion of two types of metal-organic dual-ion cells by Varta 223 Corp. (with PPy) and Bridgestone Corp. (with PAni).<sup>67-</sup> 224 Note that for the discovery and the development of conductive 225 polymers, Alan G. MacDiarmid, Alan J. Heeger, and Hideki 226 Shirakawa were awarded the 2000 Nobel Prize in Chemistry. However, shorter cycle life ( $\sim$ 500 cycles), higher self-discharge 227 228 values, and limited volumetric energy densities compared to the 229 newcomer LIB commercialized by Sony Corp. in 1991 were 230 some of the reasons for the abandonment at the end of the 20th 231 century of efforts to make organic batteries from conjugated 232 polymers. Note that in the 1990s organosulfur polymers were 233 also investigated in Li batteries but as "n-type" electrode 234 materials for which reversible Li<sup>+</sup> uptake/release reactions take 235 place. Indeed, among the myriad of possible molecular organic 236 arrangements, sulfur atoms can also be linked onto a carbon 237 backbone (-C-S-S-C-) allowing the use of the redox-238 active disulfide bond; the charge transfer reaction involves 2 239 electrons together with the cleavage of the S-S bond. Pioneering 240 research was performed by Visco and co-workers<sup>70-72</sup> with a 241 survey of diverse groups of organodisulfide as positive electrode 242 materials essentially main-chain type organosulfur polymers. 243 For example, 2,5-dimercapto-1,3,4-thiadiazole (DMcT) with a 244 theoretical specific capacity as high as 362 mAh  $g^{-1}$  is one 245 of the best well-known organosulfur compounds. However, 246 such electrode materials are generally impeded by sluggish 247 kinetics along with a large polarization as well as solubility 248 issues stemming from the repeated scission/reconstruction of 249 disulfide bonds. Better results were obtained with side-chain 250 type organodisulfide polymer such as poly(2,2'-dithiodianiline)

(PDTDA) and other related derivatives, but long-lasting cyclings <sup>251</sup> were never attempted.<sup>73</sup> Note that in the quest to develop <sup>252</sup> lithium–sulfur (Li–S) batteries while limiting the polysulfide <sup>253</sup> shuttle, high sulfur content organic materials have been recently <sup>254</sup> investigated such as a new cross-linked disulfide material <sup>255</sup> C<sub>6</sub>(SLi)<sub>6</sub> developed by Wudl's group but the restored specific <sup>256</sup> capacity is still limited with 1/4 of the theoretical value.<sup>74</sup> <sup>257</sup>

A new class of polymers (nonconjugated) able to store 258 electric energy and consisting of a stable organic polymeric 259 chain bearing stabilized nitroxyl radicals such as 2,2,6,6- 260 tetramethylpiperidinyl-N-oxy (TEMPO) radicals emerged in 261 the early 2000s thanks to joint efforts of NEC Corp. and 262 Nishide's group in Japan.<sup>75-77</sup> These studies have led to the 263 development of the so-called organic radical batteries (ORBs) 264 which are characterized by excellent rate performance, a 265 flexible design, but moderate energy density values due to the 266 adding of high amounts of conductive carbon in electrodes. 267 The achievement of robust 0.3 mm-thick ORB prototypes 268 compatible with functional smart card and wearable devices 269 was, however, announced by NEC Corp. as early as 2012.<sup>78</sup> 270 This innovative chemistry coupled with the emergence of 271 promising high-capacity organic compounds characterized by 272 multiple electroactive carbonyl (C=O) functional groups<sup>79-83</sup>  $_{273}$ (a redox-active moiety encountered in the chemistry of life and 274 numerous natural substances) enabled the publication of a 275 broader review in 2011 focused this time on the perspectives of 276 organic batteries in addressing some eco-development issues 277 through the possibility of integrating the concept of "renew- 278 ability" in electrode material design and the prospect of 279 realizing greener and sustainable batteries.<sup>84</sup> The use of 280 organics emerges also in RFBs with a first organic/inorganic 281 flow battery reported in 2009 by Xu et al.<sup>85</sup> based on the Cd- 282 chloranil system operating in sulfuric acid aqueous medium. 283 Two years later, an all-organic redox flow battery (ORFB) 284 working in nonaqueous medium (NaClO<sub>4</sub>/acetonitrile) was 285 reported by Li et al.<sup>86</sup> employing 2,2,6,6-tetramethyl- 286 1-piperidinyloxy as the posolyte and N-methylphthalimide as 287 the negolyte, respectively. Many other examples were then 288 reported in the literature as developed later (section 9). The 289 interest taken over time by organics in the field of electro- 290 chemical storage can simply be assessed thanks to common 291 data analysis tools like Scopus with suitable query string 292 (Figure S1). The histogram shows that the number of 293 publications (including articles, conference papers, reviews, 294 book chapters, conference reviews) focused on organic-based 295 electrochemical storage devices and published by year from 296 1972 onward follows a clear increase over the past 10 years. 297 One can also observe two successive bumps ranging from 1980 298 to 2000 due to the investigations of conducting polymers then 299 organodisulfide positive electrode materials followed by a 300 larger increase thanks to the impetus given by ORBs.

Although beyond the scope herein, it seems instructive to 302 briefly recall in this Introduction that the addition of elec- 303 troactive molecules has also been shown to benefit carbon- 304 based electrostatic double-layer capacitors (EDLCs) as well as 305 the merging field of Li-ion capacitors.<sup>87–102</sup> As early as 1983, 306 Saga Sanyo was the first company to integrate highly conducting 307 organic material (tetracyanoquinodimethane, TCNQ) in 308 electrolytic capacitors.<sup>69</sup> Electroactive molecules are used to 309 significantly improve storage performance by adding a reversible 310 faradaic contribution (pseudocapacitance) to the double-layer 311 capacitance at the carbon electrode surface; these devices, 312 referred to as supercapacitors or ultracapacitors, can work both 313 pubs.acs.org/CR

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314 in aqueous and nonaqueous electrolyte media. Different 315 chemistries such as the functionalization of the carbon surface 316 by self-assembly or grafting of the redox-active organic 317 molecule can be used.<sup>87–97</sup> Although covalent anchoring of 318 the carbon substrate via the diazonium chemistry<sup>94</sup> appears as 319 the main approach, some authors have also reported the direct 320 incorporation of the redox-active organic molecules into the 321 electrolyte formulation referred to as "redox electrolyte" to 322 improve the specific capacitance of carbon-based electro-323 chemical capacitors.<sup>93,95,96</sup> A relevant example of "organic" 324 electrochemical pseudocapacitor consisting of activated carbon 325 powder electrodes modified with naphthalimide and 2,2,6,6-326 tetramethylpiperidine-N-oxyl (TEMPO) was reported by 327 Lebègue et al.<sup>97</sup> It shows an increase in specific capacitance 328 up to 51%, an extended operating voltage of 2.9 V in propylene 329 carbonate, compared to 1.9 V for the unmodified system, and a 330 power 2.5 times higher. Alternatively, redox-active polymer 331 electrodes can be employed including, for instance, PPy, PAni, 332 and PT derivatives which offer advantages for making light-333 weight and flexible (micro)supercapacitors while being com-<sup>334</sup> patible with aqueous electrolytes.<sup>98–100</sup> Note that electroactive 335 organic molecules have also recently been introduced as key 336 materials to improve the sought-after "prelithiation" step of 337 Li-ion capacitors as well as the sustainability while reducing the 338 cost and complexity.<sup>101,102</sup>

It should be underlined that the boundary between faradaic 339 340 organic-adding for supercapacitors and capacitive carbon-adding 341 for organic batteries is sometimes not so clear. For instance, 342 Wang's group<sup>103</sup> have reported a home-made hierarchical 343 porous carbon nanotubes (HPCNTs) decorated with anthra-344 quinone (AQ) molecules exhibiting ultrahigh specific capacitance 345 of 710 F  $g^{-1}$  (measured at 1 A  $g^{-1}$ ) when tested in 1 M H<sub>2</sub>SO<sub>4</sub> 346 aqueous solution with the optimized mass ratio 7:5 indicating a 347 larger specific organic loading. Otherwise, recent years have 348 seen the emergence of so-called carbon-supported organic 349 electrode materials for LIBs/SIBs, that actually mirrors a 350 strategy to counteract common physical limitations of most 351 low-weight (neutral) organic molecules: their high solubility in 352 organic electrolytes and poor electrical conductivity. By mixing 353 these small organic molecules with large amounts of carbon 354 (generally by impregnation), a better stability can be expected 355 on cycling especially at high rate thanks to the establishment of 356  $\pi - \pi$  stacking bonds with the surface of carbon particles (typical 357 carbon loading: >55 wt %); this phenomenon being reinforced 358 with extended aromatic cores. Note that biomolecules such as <sup>359</sup> flavine<sup>104</sup> or dopamine<sup>105</sup> were reported. Chen and co-workers 360 have reviewed this peculiar topic in 2015<sup>13</sup> by questioning 361 some relevant points for practical applications such as the 362 uniformity/reproducibility at large scale production of carbon-363 supported organic electrodes or the poor as-obtained energy 364 density values (especially in volumetric metrics).

#### 1.3. Goal, Scope, and Organization of This Review

365 Following these introductory elements, it is obvious that a 366 consequent and growing amount of literature is now easily 367 available on organic batteries after years of silence. However, it 368 must be noted that because a certain disciplinary boundary 369 naturally exists between inorganic and organic compounds and 370 because the redox chemistry of organics is sometimes subtle 371 (involving often reactive delocalized charges), reading research 372 articles dealing with organic batteries (whatever the considered 373 technology) could be somewhat challenging for nonspecialist 374 readers. Therefore, the authors have thought it would be timely to bridge the gap by providing a kind of "tutorial"-oriented 375 review for a broader audience to take smoothly in hands the 376 most relevant points and achievements dealing with this 377 peculiar field without being redundant with the multiple review 378 articles already published today. Based on the latest selected 379 and reliable input data from both general and specialized 380 scientific literature (typically reported after 2015), this contribution aims also at providing the readers with a better critical 382 view of the current evolution trends in our technology-oriented 383 modern societies and the consecutive global demand for elec-384 trical energy sources, materials, and batteries before reviewing 385 the main achievements obtained with organic-based electrode 386 materials. 387

In practice, the layout of the article is structured in such a 388 way as the reader will be able to select the parts that interest 389 him most. From a chemical point of view, the following 390 approach will be stepwise addressed in this review: 391

- basic working principles and fundamental properties of key 392 redox-active organic moieties and comparison with the 393 formalism commonly used for inorganic materials together 394 with corresponding cell configurations (section 4), 395
- a selection (with description) of original/promising organic- 396 based batteries to date working either in the solid state 397 ("sealed" batteries) or in solubilized state (ORFBs) for 398 designing better realistic organic batteries in the future 399 (sections 5–9). Note that the reader can find specific 400 reviews on polymer-based organic batteries including radical 401 polymers in refs 10 and 18. 402

But as a preliminary step of this overview, it is thought 403 particularly relevant for some readers to provide a snapshot of 404 the global context that justifies there is room for reversible elec- 405 troactive organic systems in the future electrochemical storage 406 landscape in view of the particular conjunction of several critical 407 factors facing mankind at the turn of the 21st century. Such a 408 tricky exercise, which is seldom considered in other review 409 articles, will constitute the background of sections 2 and 3 of this 410 paper.

#### 2. FOURTH INDUSTRIAL REVOLUTION: BATTERIES AT THE CROSSROADS

#### 2.1. Background

Since the appearance on the market of LIBs 30 years ago 413 the world has drastically changed. We have now entered the 414 so-called Fourth Industrial Revolution!<sup>106</sup> In short, the First 415 Industrial Revolution used water and steam power to mech- 416 anize production, the Second used electric power to create 417 mass production, and the Third, emerging in the 60s with the 418 birth of computers, used electronics and information tech- 419 nologies to automate production. Starting at the end of the 420 20th century, the Fourth Industrial Revolution is built on the 421 Third and is characterized by (i) a fusion of technologies that 422 is blurring the lines between the physical, digital, and biological 423 spheres, (ii) an exponential rather than a linear pace, and (iii) 424 probably no control over either technology or the disruption 425 that will come. Basically, the driving forces of this revolution 426 are nestled in the digital and information technologies with 427 more active roles for the artificial intelligence (AI) that enables 428 innovations in "physical assets" such as autonomous vehicles, 429 Internet of things (IoT), robotics, electric unmanned aerial 430 vehicles (UAVs) or drones, 3-D printing, ... as well as "digital" 431 innovations (e.g., blockchain<sup>107</sup>). It is worth noting that a 432 rapid analysis of these innovative steps relies on a common 433 434 denominator which is the finer and finer control of the 435 electron.

If we ignore herein that such innovations are also raising major ethical and spiritual questions,<sup>106</sup> the corollary of all this technology-oriented and more recently "connected" society is the ever-growing demand for energy especially for electrical power sources and related storage devices ranging from mWh to MWh: an era sometimes named "the Power Revolution". Unambiguously, it is well established that access to electricity improves life in a tangible way.<sup>108</sup> However, as previously the pointed out in a former Perspective article a few years ago,<sup>84</sup> two related crucial threats cannot be ignored:

1. "Global warming" with its numerous and dangerous 446 induced impacts (e.g., extreme and destructive climate 447 events, rise in sea level with its aftermath, relocating 448 industrial and farming areas, biodiversity alteration, new 449 distribution of populations with conflicts over water and 450 food, and so on). This major threat which seems to 451 correlate to anthropogenic greenhouse gas (GHG) emis-452 sions represents not only ecological but also socio-453 ecological and economic issues. At the COP21/CMP11 454 (Conference of the Parties) meeting in Paris in 2015, 455 195 countries signed a legally binding agreement to keep 456 global warming "well below 2°C above pre-industrial 457 levels, and to pursue efforts to limit the temperature 458 increase even further to 1.5°C" within this century. 459 460 In practice, this means an 81% reduction of GHG intensity by 2050, which is equivalent to 4.4% annual improve-461 ment.<sup>109</sup> In 2018 almost all countries in the world have 462 committed themselves to reduce their GHG emissions in 463 their pledges to the Paris Agreement. Note that global 464 warming is likely to reach 1.5 °C between 2030 and 2052 465 if it continues to increase at the current rate as reported by 466 the Intergovernmental Panel on Climate Change (IPCC) 467 special report on January 2019.<sup>110</sup> 468

469 2. The constant increase in the world population which
470 results in more and more energy consumers and there471 fore more GHG emissions as nicely shown in Figure 1.

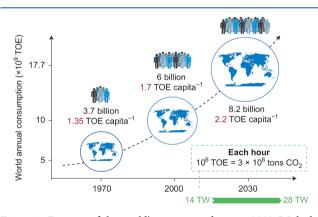


Figure 1. Forecast of the world's energy needs up to 2050. With the changing lifestyles of an increasing number of inhabitants, our energy rate demand will double from 14 TW (2010) to 28 TW (2050). TOE = ton of oil equivalent. Reproduced with permission from ref 112. Copyright 2015 Nature Publishing Group.

472 Predictions estimate around 9–10 billion the human
473 load by the year 2050 (2.5 billion in Africa against
474 1.3 billion today) 66% of which will reside in urban
475 areas in developing economies.<sup>111</sup> For comparison, the

population was 700 million at the beginning of the first 476 Industrial Revolution. 477

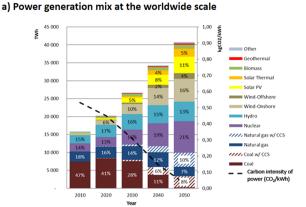
Although not yet fully accepted all over the world, such a 478 mankind development still falls short in terms of sustainability 479 and calls for a rapid and radical change in our current energy 480 engineering together with a responsible behavior in our 481 consuming fashion (pro-environmental behavior, "Nudge"  $_{482}$  theory, ...  $^{113,114}$ ). It is interesting for example to read the  $_{483}$ study of Dong et al.<sup>115</sup> on the nexus among carbon dioxide 484 emissions, economic and population growth, and renewable 485 energy across regions. Their data allow us to underline that 486 economic growth is highly emission intensive, and economic 487 growth often means rising energy consumption and increasing 488 CO<sub>2</sub> emissions with a proportional effect of the population 489 size. Hence our entering this Fourth Industrial Revolution can 490 be perceived as a threat but also as an opportunity to rethink 491 the development of mankind as a whole. Positive initiatives are 492 now under way, and some policy makers and important energy 493 stakeholders are making things happen probably also pushed 494 by the ostensibly large number of recent extreme weather 495 events<sup>116</sup> such as Category 5 Katerina hurricane in 2005. 496 Basically, new political goals and innovative/disruptive 497 economy models (like the "green growth" models, the circular 498 economy governed by 3Rs, namely Reduce, Reuse, and Recycle) 499 must also be formulated, notably in reference with  $CO_2$  emission 500 limits, in the quest for a long-term sustainability conjugating 501 Ecology/Economy/Society. [The reader who would be inter- 502 ested in this exciting field could find relevant and very informative 503 economic analyses in the specialized literature.<sup>109,117-119</sup>] 504

For a more technological point of view, generation of 505 decarbonized electricity and low-carbon transportation solutions 506 are the two main levers (in association with better energy 507 efficiency and conservation and the carbon capture utilization and 508 storage<sup>120</sup>) put traditionally forward to move toward a deep 509 decarbonization of the energy system.<sup>121</sup> To better forecast the 510 future in this regard, we recap below the main observed trends 511 with supporting figures highlighting that rechargeable batteries 512 are expected at the crossroads of several paths in the global 513 demand pattern for electrical functionalities of today and 514 tomorrow, some applications being to mitigate GHG emissions 515 while others are probably less virtuous. 516

# 2.2. Decarbonizing the Power Supply and Its Related Storage Challenges

Regarding the future of electric grids, thanks to the efforts 518 of worldwide researchers, engineers, and policy makers, 519 remarkable progress has been made to connect renewable 520 energy sources (RESs) for electricity generation.<sup>122</sup> For 521 instance, the European Directive 2009/28/EC<sup>123</sup> aims at 522 promoting the use of RESs in the European Union (EU) with 523 a targeted value of 20% by 2020 with specific values regarding 524 each member state. The most exploited RESs are hydroelectric, 525 photovoltaic (PV), and wind. Other emerging renewable 526 technologies include wave and tidal energy conversion and 527 biomass energy conversion. Therefore, some predictions seem 528 to indicate that GHG emissions in the power sector could be 529 drastically reduced thus becoming a major contributor to 530 decarbonization (Figure 2). Although the total electricity 531 production is expected to more than double between 2010 and 532 2050 giving rise to the incredible value of more than 40 000 533 TWh of generated energy per year (notably to power the elec- 534 tromobility, see below), total emissions for the power sector 535 could be divided by more than four according the Deep 536

517



#### b) Power CO<sub>2</sub> emissions at the worldwide scale

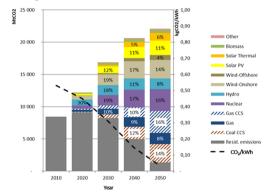
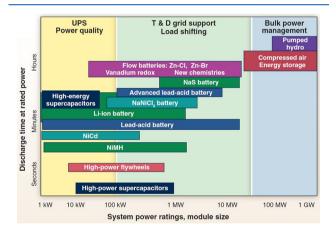


Figure 2. (a, b) Decarbonization Wedges in the power sector extracted from the ANCRE's report<sup>124</sup> (with permission) elaborated in the DDPP and by considering the most ambitious scenario in each country; "worldwide scale" refers to only the 16 most emitting countries. These histograms show the emission trajectories for the electricity sector in the absence of any technological evolution and (in gray) the evolutions of the emissions within the framework of decarbonization scenarios; the difference between the two corresponds to reductions that allow different technologies (e.g., solar in yellow and orange, hydro in blue); CCS meaning carbon capture and sequestration. Further descriptions of the "Decarbonization Wedges" methodology can be found in ref 126.

<sup>537</sup> Decarbonization Pathway Project (DDPP)<sup>124,125</sup> by considering <sup>538</sup> the most ambitious scenario in the 16 largest GHG-emitting <sup>539</sup> countries representing 75% of current GHG emissions. According <sup>540</sup> to these scenarios, the electricity mix could be completely <sup>541</sup> modified with almost 90% of power generation from non-CO<sub>2</sub> <sup>542</sup> emitting technologies, among which 54% is from renewable <sup>543</sup> sources (together with 21% from nuclear power plants); coal is <sup>544</sup> today responsible for 42% of CO<sub>2</sub> emissions worldwide. The <sup>545</sup> electricity sector could be widely decarbonized by 2050 with a <sup>546</sup> reduction from the current 530 gCO<sub>2</sub> kWh<sup>-1</sup> to about <sup>547</sup> 33 gCO<sub>2</sub> kWh<sup>-1</sup> [the complete description of the "Decarbon-<sup>548</sup> ization Wedges" methodology as well as additional subscenar-<sup>549</sup> ios have been recently published by Mathy et al.<sup>126</sup>].

However, huge infrastructure investments will obviously be ss1 needed to satisfy such perspectives in electricity generation. Ss2 For instance, some of these newly developed technologies (e.g., PV, wind power) cannot serve as stable energy sources ss4 alone because of their natural sensitivity to weather, landform, Ss5 or other environmental conditions (i.e., variability and high ss6 ramping characteristics) requiring sophisticated planning and ss7 operation scheduling to ensure the necessary and subtle balance between electricity production and consumption. New 558 technologies are currently being developed to upgrade existing 559 electricity grid infrastructures that will enable so-called "smart 560 grids", which are characterized by improved grid reliability and 561 utilization, the synergies between the power electronics, control, 562 and communication fields as well as the change from radial 563 networks to mesh networks with the possibility to reconfigure 564 and self-heal.<sup>127,128</sup> Thus, the role of IoT will be eminent with a 565 significant reduction of costs associated with sensors, bandwidth, 566 processing, and memory/storage.<sup>129</sup> 567

Consequently, energy storage is increasingly seen as a 568 valuable asset for electricity grids and one of the important 569 tools of mitigation not only as a technical solution for network 570 management, ensuring real-time load leveling, but it is also a 571 means of better utilizing RESs by avoiding load shedding in 572 times of overproduction. For the moment, the worldwide 573 stationary electrical storage remains by far dominated by 574 pumped storage hydropower (98% of the installed power) but 575 the use of rechargeable batteries is emerging fast as underlined 576 in 2011 by Dunn et al.<sup>130</sup> in a visionary paper; the wide use of 577 batteries is now clearly included in the roadmap storage 578 technologies.<sup>131,132</sup> Already widely used for load-leveling 579 applications and UPS for entire cities (especially the PbA 580 technology), the reduction of costs in the electrochemical 581 storage technologies is attracting considerable interest for 582 short-term storage (for a period of seconds to a few days) 583 using "sealed" batteries and redox-flow batteries (RFBs) as 584 shown in Figure 3. Thus, LIBs in various chemistries are even 585



**Figure 3.** Comparison of discharge time and power rating for various electrical energy storage technologies highlighting the broad contribution of batteries with various chemistries; the latter being only based on inorganic electroactive materials, essentially metals. Reproduced with permission from ref 130. Copyright 2011 Science Publishing Group.

more seriously envisaged<sup>132</sup> because the cost of battery storage 586 has declined fast in a few years with a drop of 73% between 587 2010 to 2016 to reach \$273 kWh<sup>-1</sup> as market value while a 588 value of \$73 kWh<sup>-1</sup> is forecast in 2030.<sup>133</sup> Competing with gas- 589 fired peaking plants is made possible. For example, more than 590 18 000 LIB packs (400-MW peak hour battery) would replace 591 a gas-fired power in California.<sup>134</sup> Interestingly, the analysis of 592 3 years of real usage of LIBs (1 MW/250 kWh using 384 593 modules connected in series) installed and in operation in 594 Hawaii has been recently reported by Dubarry et al.<sup>135</sup>

For such stationary applications, the capital invested and 596 operational costs (maintenance, energy lost during cycling, 597

<sup>598</sup> aging) are very important factors to consider for the entire life <sup>599</sup> of the system. The reader could find compared cost factors in <sup>600</sup> the literature including PbA, RFBs, LIBs, and so on.<sup>5,130,136</sup> <sup>601</sup> The cost of storage can be calculated through the so-called <sup>602</sup> levelized cost of stored energy (LCOE) defined as the total <sup>603</sup> lifetime cost of the investment divided by the cumulated <sup>604</sup> generated energy by this investment. The LCOE values at <sup>605</sup> 25 years for an installed storage power of 1 MW are estimated <sup>606</sup> at 0.338 and €1.978/kWh for RFBs and LIBs, respectively <sup>607</sup> (against 3.072 for the PbA technology).<sup>137</sup>

# 2.3. Decarbonizing the Transportation Sector Through the 608 Electrification Scheme

609 Beyond the electric grid, the pressure on batteries is also 610 particularly intensive due to the deployment of decarbonized 611 transportation systems through the massive use of electric 612 motors (the so-called "electromobility" or "e-mobility") 613 although the use of biofuels, oil-based fuels, and liquefied 614 natural gas (LNG) has recently gained more attention.<sup>121,138</sup> 615 [LNG consists mostly of CH<sub>4</sub> and has the potential to reduce 616 SO<sub>2</sub>-emissions over 90%, NOx-emissions with 80%, and CO<sub>2</sub>-617 emissions 20%, which seems a competitive alternative in this 618 sector provided there is less than 2% leakage.] Indeed, the 619 transport sector's dependence on fossil fuels is another big part 620 of the necessary transition toward a climate-neutral and 621 sustainable society. Transport is a major source of total GHG 622 emissions (22%), with road transport being the biggest 623 contributor and responsible for about 72% of CO<sub>2</sub> emissions 624 worldwide according to IPCC analyses.<sup>139</sup> Note that over 625 1.2 billion vehicles were in service in 2015 according to the 626 International Organization of Motor Vehicle Manufacturers 627 (OICA).<sup>140</sup> Moreover commercial air transportation still 628 represents about 11% of global fuel consumption across all 629 sectors, 2% of global CO<sub>2</sub> emissions, and 13% of emissions in 630 the transport sector alone.<sup>141</sup> Beyond the dangerous GHG 631 emissions when using Internal combustion engines (ICEs), the 632 electric motor intrinsically possesses several advantages that 633 have always been known such as better energy efficiencies 634 (>90% because not subject to the Carnot cycle limitations of 635 heat engines). They are also quieter, easy to miniaturize, and 636 more importantly simpler in their design making the direct 637 motor and wheel coupling possible. Conversely, a conventional 638 ICE powered car typically has 10 000 moving parts (essentially 639 within the drive train) against only 150 in battery electric 640 vehicles (BEVs) today and only one of which is in the drive 641 train as underlined by Parker.<sup>142</sup> The gains in maintenance as 642 well as in energy efficiency are obvious.

Historically, the invention of ICE occurred in the middle of 643 644 the 19th century just like that of the electric motor but at a 645 time when oil and its derivatives were becoming cheap and 646 widely available whereas high energy batteries did not exist yet. 647 Gaston Planté had just invented the first rechargeable battery 648 with its PbA technology (then improved by Camille Faure in 649 1881), which enabled however the first automobile speed 650 record in 1899 (100 km h<sup>-1</sup> but only on 2 km range) thanks to 651 the first BEV named "La jamais contente" powered by 750 kg of 652 Fulmen PbA batteries. In the early 1900s, 38% of the US 653 automobile market was captured by electric vehicles. Even after 654 this feat, ICEs would increasingly supplant the electric car for 655 the next century especially thanks to Ford's innovations with 656 the consequences that we are now witnessing. Now vehicle 657 emission regulations have been forcing the automotive industry 658 worldwide to reduce its carbon footprint especially in the EU,

China, and India while governments around the world (like the 659 Electric Vehicles Initiative (EVI))<sup>143</sup> are providing incentives 660 to the citizens for buying electrified vehicles (EVs). The 661 French government is to take the initiative to propose an 662 ambitious Euro 7 emission standard at European level and set 663 the goal of ending the sale of cars emitting greenhouse gases 664 in 2040! The Swedish automaker Volvo has announced 665 that from 2019 all its new models would be either hybrid or 666 100% electric. Note that EVs include battery electric vehicles 667 (BEVs), plug-in hybrid electric vehicles (PHEVs), and fuel-cell 668 electric vehicles (FCEVs). As a reminder, the key difference 669 between BEVs and PHEVs is that FCEVs use a primary 670 electrochemical cell (*i.e.*, fuel cell) to power the electric motor; 671 the recharging step of FCEVs needing hydrogen as a fuel 672 instead of electricity. 673

Based on the current roadmap reported by the International 674 Energy Agency (IEA) in the BLUE Map scenario<sup>144</sup> (Figure 4a), 675 rechargeable batteries are likely to remain the better choice to 676 power light duty vehicles (LDV) in the next 2 decades whereas 677 FCEVs are considered as the future vision for the global 678 automotive industry beyond 2040–2050 because this technol- 679 ogy and related hydrogen supply infrastructures are still not at 680 the desirable level,<sup>121,145</sup> with the production of low-carbon H<sub>2</sub> 681 being required too. For the present time progress made in 682 recent years to improve battery performance and reduce 683 costs<sup>133</sup> has already enabled the use of LIBs in numerous 684 e-mobility applications such as two-wheelers, buses, taxis, 685 shared cars, ride-hailing services, and the upcoming self-driving 686 (or driverless) cars. 687

Thus, sales of new electric cars worldwide surpassed 1 million 688 units in 2017 (for 3 million EVs in circulation), a record volume 689 which represents a growth in new electric car sales of 54% 690 compared with 2016 (more than half of global sales of electric 691 cars were in the People's Republic of China) whereas the 692 EV30@30 scenario makes as projection 228 million EVs 693 (excluding two- and three-wheelers) on the road by 2030 as 694 shown in Figure 4b;<sup>143</sup> the EV30@30 campaign redefining the 695 EVI ambition originally set at 20 million EVs on the road by 696 2020. More recently, Hache et al.<sup>146</sup> have reported a bottom- 697 up analysis using the Times Integrated Assessment Model 698 (TIAM-IFPEN version) to forecast the diffusion of electrified 699 road transportation modes by integrating two climate scenarios 700 (4 and 2 °C) and two shapes of mobility (high/low mobility). 701 The electric vehicles fleet could reach up to 1/3 of global fleet 702 by 2050 in the 4 °C scenarios, while it could be up to 3/4 in 703 the 2 °C scenarios both with high mobility, mostly located in 704 Asian countries (China, India, and other developing countries 705 in Asia) due to the large presence of 2- and 3-wheelers (Figure S2). 706 Consequently, electric transportation is integrated into the smart 707 grid/smart cities master plans<sup>147</sup> first because the electricity needs 708 will boom but also as a means of flexibility since integrating BEVs/ 709 PHEVs into the electric utility grid facilitates both vehicle-to-grid 710 (V2G) and grid-to-vehicle applications owing to the bidirectional 711 nature of the power flows between the BEVs/PHEVs and the grid. 712

Last but not least, developing electric/hybrid aircraft is in 713 progress too because electric propulsion has the potential to 714 revolutionize aviation opening real opportunities for cleaner, 715 quieter travel to completely new types of transportation 716 models. In November 2017 Airbus announced the launching of 717 E-Fan X with its partners Siemens and Rolls-Royce which is an 718 ambitious technology demonstrator project: a hybrid civil 719 aircraft, another emerging sector calling for high-performance 720 batteries. Other equivalent projects exist such as the ZUNUM 721

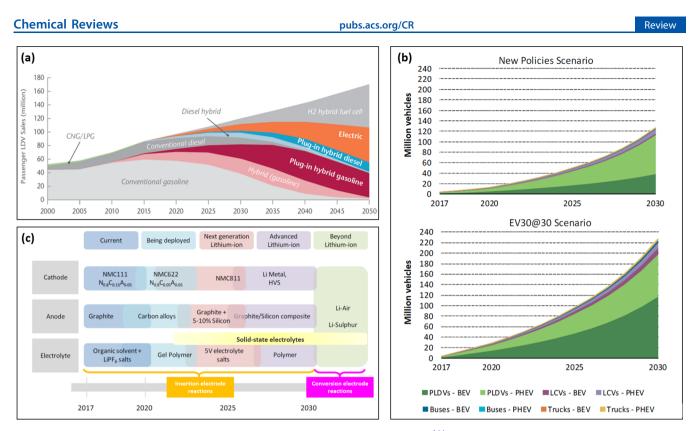


Figure 4. (a) Annual light-duty vehicle (LDV) sales according to the BLUE Map scenario,<sup>144</sup> 2000–2050 reported by IEA; combined EV/PHEV sales should share at least 50% of LDV sales worldwide by 2050. (b) Global EV stock for 2017–2030 excluding two- and three-wheelers by considering both New Policies Scenario and the EV30@30 Scenario reported by IEA<sup>143</sup> (PLDVs = passenger light duty vehicles; LCVs = light commercial vehicles; BEVs = battery electric vehicles; PHEV = plug-in hybrid electric vehicles). (c) Battery technology roadmap adapted from IEA<sup>143</sup> (HVS = high voltage spinel). Adapted with permission, copyrights of IEA.

722 Aero airliner project supported by Boeing. Interesting inno-723 vations can therefore be expected in the next decade even if 724 there is a long way to go for large-scale practical applications.

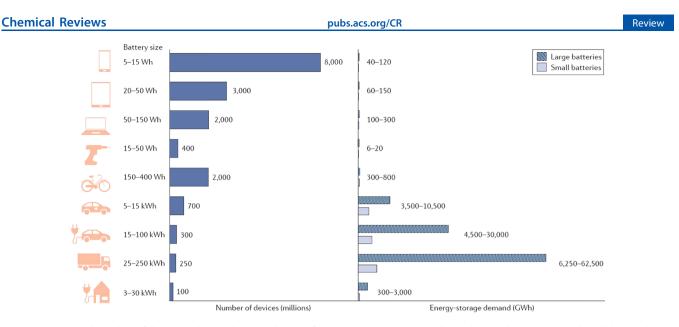
#### 2.4. Digitalization and Growing Consumption of Electronic 725 Devices

The boom in electronic devices and digital technologies has 727 been going on for almost 30 years, and batteries are generally 728 needed to power them. The worldwide development of mobile 729 phones is probably the most vivid example. As underlined by 730 Galetovic et al.<sup>148</sup> in a very interesting world mobile phone 731 industry study, the number of mobile phones sold rose 62-fold 732 between 1994 and 2013 whereas in June 2015 there were 733 around 7.5 billion subscriber connections, one for every person 734 on the planet. But all this has an energy cost but also an 735 environmental one. As an example, the entire mobile phone 736 system in a small country like Italy consumes approximately 737 2200 GWh per year (0.7% of the national electricity consump-738 tion) while producing potential e-waste from end-of-life 739 devices totaling over 11 thousand tons for the period from 740 2007 to 2012.

Today, consumer electronics (CE) mainly encompasses the whole range of home electronic equipment, from audio systems, home automation, home computing, and low-power electronics real to multimedia systems. In addition, IoT has nowadays gained an incredible attraction<sup>149,150</sup> imparting networked connectivreal incredible attraction in the physical world with numerous ration in logistics, manufacturing, retailing, environreal monitoring, healthcare monitoring, industrial monitorreal ing, traffic monitoring, ... (as well as important monitoring in rate shows the smart grid and EVs to relate to the previous paragraph). In 2015, IBM predicted that 1 trillion devices would be connected 751 to the Internet and the IoT. In 2017, a Cisco-revised forecast 752 called for 50 billion devices to be connected by 2020 and, most 753 recently, the GSMA Association predicted 25 billion IoT devices 754 by 2025! Interesting data are reported by "The Shift Project" in 755 several reports.<sup>151</sup> For example, the energy consumption of 756 Information and Communication Technologies (ICT) is 757 increasing by 9% every year while the share of ICT in GHG 758 emissions has increased by half since 2013, rising from 2.5% to 759 3.7% in a few years. 760

Remarkable progress has also been made in many aspects of 761 robotics for which 10 grand challenges have recently been 762 pointed out in a Perspective article published in Science 763 Robotics<sup>152</sup> including one related to power and energy sources 764 to make the deployment of mobile robotics possible. In par- 765 ticular, "service robots" which smartly mix IoT and AI to assist 766 human beings—typically by performing a job that is dirty, dull, 767 distant, dangerous or repetitive, including household chores- 768 are on the verge of equipping our homes and some public 769 places. Impressive statistics and forecast have been announced 770 by The International Federation of Robotics in the Executive 771 Summary World Robotics 2018 Service Robots reports.<sup>153</sup> For 772 instance, it was estimated in 2017 that nearly 6.1 million robots 773 for domestic tasks, including vacuum cleaning, lawn-mowing, 774 window cleaning and other types, were sold which corresponds 775 to a 31% increase compared to 2016. The market for elderly 776 and handicap assistance is also expected to increase substan- 777 tially within the next 20 years. 778

In the same vein of recent developments, benefiting of 779 electric propulsion R&D, the market of drones (UAVs) is also 780 expected to rise at unprecedented rates due to growing interest 781



**Figure 5.** Estimated number of devices and related energy demand for 2016–2050. Note that all possible needs are not considered like the electric grid. Reproduced with permission from ref 154. Copyright 2019 Nature Publishing Group.

782 in monitoring applications by the military, researchers, farmers, 783 hobbyists, and investors in e-business since drones offer 784 superior abilities over their ground alternatives. It should be 785 pointed out that using drones for commercial deliveries was 786 something improbable ten years ago. Interestingly, Vaalma 787 et al.<sup>154</sup> have very recently established a scenario-based supply 788 and demand analysis concerning LIBs for 2016-2050 con-789 sidering some selected applications including portable elec-790 tronic devices and tools as well as several electrified road trans-791 portation modes and small stationary energy-storage devices 792 (Figure 5). Clearly, if portable electronics dominates in terms 793 of number of devices, they account for much less in terms of 794 the total energy-storage demand if electric vehicles and 795 residential energy-storage devices reach the high production 796 numbers estimated in their scenarios.<sup>154</sup> However, several key 797 applications such as the powering of domestic robots, drones, 798 or IoT are not included in the scenario.

#### 2.5. Summary

799 To sum up this overview, we are unambiguously facing a 800 tremendous need for EES for a double reason, first as a key 801 ingredient of the future energy engineering to fight global 802 warming and, second, as a central hub for the emergence of 803 disruptive technologies consecutive to the continuous moderni-804 zation and development of mankind. The scale-up of industrial 805 facilities for the production of rechargeable batteries, especially 806 LIBs due to their high energy density values, is consequently 807 an opened and sensitive question. The production is currently 808 dominated by East-Asian competitors; with Panasonic (Japan) 809 and LG Chem (South Korea), these leading manufacturers on 810 the automotive market are closely followed by Samsung SDI 811 (South Korea), CATL (China), and SK Innovation (South 812 Korea). With its Gigafactory built in Nevada, Tesla (with 813 Panasonic as a partner) is now on the road too on US soil 814 whereas in the EU, things are moving forward to reduce its 815 dependence on the Asia and US suppliers. Sweden's Northvolt 816 has raised in June 2019 \$1 billion in equity capital to complete 817 funding for its future Gigafactory while France and Germany 818 launched an Airbus-style €6 billion foray into the battery-819 building business. Considering a typical battery capacity range 820 of 20-75 kWh, these factory capacities translate into a yearly

production volume ranging between 6 000 to 400 000 packs.<sup>143</sup> 821 To better visualize the world LIB manufacturing capacity and 822 related international trade flows, Figures S3-4 report the 823 thorough mapping analysis performed by Mayyas et al.<sup>155</sup> 824 based on reliable collected data in 2016; the total LIB manu- 825 facturing capacity for this year was 189 762 MWh including 826 114 484 MWh for automobile LIBs. Finally, Bloomberg NEF 827 announced in November 2018 a need for 1800 GWh by 2030 828 of LIBs including annual passenger EVs and E-buses, consumer 829 electronics, and stationary storage; roughly eight out of every 830 10 batteries sold annually will find their way into a passenger 831 electric vehicle;<sup>156</sup> however, details regarding the modeling and 832 technical assumptions are not available. Anyway, the bottom 833 line is battery production will have to be strongly scaled up in 834 any scenario because a significant difference between supply 835 and demand could occur. 836

But departing from these capability considerations, it is 837 particularly important to avoid any pitfalls in this frenetic 838 endeavor and make sure that proposed technical solutions are 839 themselves sufficiently eco-friendly and sustainable. In other 840 words, such large-scale perspectives force us to consider the 841 environmental impact of rechargeable batteries (notably LIBs) 842 as well as dependencies on raw materials. This critical point 843 will be specifically discussed in the next section on the base of a 844 selection of relevant data again ranging from chemical element 845 abundance to potential environmental concerns related to their 846 production and disposal. 847

#### 3. MATERIAL SUPPLY FOR ELECTROCHEMICAL STORAGE: RESOURCE CONSTRAINTS ISSUES, 848 ENVIRONMENTAL BURDEN, AND OPPORTUNITIES 849 PROVIDED BY ORGANIC ELECTRODE MATERIALS 850

Even if some currents of thought advocate a negative or zero 851 growth as a solution, it is believed that technology and its 852 progressive developments should constitute the most important 853 pillars of energy saving and GHG reducing. Nevertheless, it 854 seems also established that with all decarbonization innovations 855 notably in the broad field of energy, new environmental and 856 resource issues are introduced with the growing need for ores 857 and refined metals;<sup>126,157</sup> which partly offset the gains of 858 859 innovative solutions; a phenomenon known in the economic 860 field as the "Jevons' paradox" or the Rebond effect.<sup>158,159</sup> In a 861 very interesting paper published in 2011, Graedel wrote:<sup>160</sup> 862 Assessors of technology no longer tend to ask, "What is being used?" 863 but rather, "What is not being used?" The answer to the last 864 question is, increasingly, "Almost nothing." In the last 20 years 865 (1994–2014), world mining production of indium, rare earth 866 elements (REEs), lithium, and cobalt increased from 149 to 867 819 tons, 64.5 to 133 ktons, 6.0 to 36.0 ktons, and 18.5 to 868 112.0 ktons, respectively, together with e-waste which is at the 869 world scale unfortunately poorly collected and recycled.<sup>161</sup> 870 Hence the large quantities of waste electrical and electronic 871 equipment (WEEE) generated have raised a serious alarm on 872 their potential adverse health and environmental consequences 873 when incorrectly disposed of.

In 2012, Vesborg and Jaramillo<sup>162</sup> very nicely studied the 875 tricky question about the scalability in the supply of chemical 876 elements (and the related cost in energy) to promote tech-877 nologies for energy harvesting, conversion or storage at the 878 required TW-level for a sustainable future. Numerous relevant 879 data are provided in this article such as correlations between 880 crustal abundance and production of dozens of chemical elements 881 while underlining the significant energy costs associated with 882 providing the current flow of raw materials for energy tech-883 nologies. Today's turbine blade alloys and coatings for wind 884 energy converter make use of as many as a dozen metals while 885 Electrical and Electronic Equipment (EEEs) incorporate some 886 60 metals most of which are classified as "critical metals" 887 (CMs).<sup>160,163,164</sup> In short, CM refers roughly to imbalances 888 between metal supply and demand (real or anticipated) at 889 national, regional, or very local level, which induces variable 890 appreciations, several definitions, and assessment method-891 ologies. An extension to "critical raw materials" (CRMs) and 892 the "criticality" term have appeared in the literature too. <sup>146,164</sup> 893 For instance, through the Raw Materials Initiative (RMI) <sup>893</sup> Hor instance, unough the functional functional field in 2008,<sup>146,165</sup> the European Commission<sup>166</sup> has 895 defined CRM when it faces high supply risks (e.g., geological, 896 geopolitical, or production risk) or high environmental risks 897 and is of high economic importance; 14 CRMs were identified 898 in 2011, 20 in 2014, and 27 in 2017 as shown in Figure S5. 899 Interestingly, Li is not considered as CM for the European 900 Commission while the US has included it in its own list as 901 reported by the Department Of the Interior in 2018.<sup>167</sup>

Respective to the scope of this article, the relevant question 903 is therefore to establish if the current available and future 904 battery technologies depend on high material resource constraints 905 and at what cost in terms of environmental burden. A few 906 elements of an answer will be provided below.

#### 3.1. Resource Constraints Forecast in Conventional 907 Material Supply

908 Based on the present state-of-the-art and whatever the con-909 sidered technologies, electrode reactions involve redox-active 910 inorganic compounds especially metal-based electroactive com-911 ponents, which is an historic heritage of the pioneered redox 912 chemistry (the voltaic pile followed by the PbA secondary cell) 913 as well as the material engineering that resulted (Figure 3). For 914 instance, if we consider the battery technology roadmap for 915 electrified vehicles (Figure 4c) it is expected that at least until 916 2030 matured and advanced insertion inorganic positive 917 electrode materials will be essentially based on the 3d-metal 918 redox chemistry. However, it is also widely acknowledged that 919 traditional Li-ion batteries are starting to approach their limits especially for long-range EVs. Beyond 2030 other battery 920 chemistries are envisaged namely post-LIB systems. First, it is 921 commonly forecast that conversion-based cathode reactions 922 could be used (with  $O_2$  and S) in Li-metal battery configuration 923(Figure 4c), which supposes however the achievement of 924 consequent improvements.<sup>168</sup> Recent R&D trends also indicate 925 an expected switch from liquid (organic) electrolytes to ceramic 926 electrolytes (or solid state electrolytes, SEEs) notably following 927 the recent discovery of lithium superionic conductors at room 928 temperature by Kanno and co-workers ( $\sigma_{Li}^+ = 25 \text{ mS cm}^{-1}$  for 929 Li<sub>9.54</sub>Si<sub>1.74</sub>P<sub>1.44</sub>S<sub>11.7</sub>Cl<sub>0.3</sub>).<sup>169,170</sup> All-solid-state batteries operating 930 at moderate temperatures offer an attractive option for non- 931 flammable batteries while achieving both high power and high 932 energy densities because it is also a relevant option to reopen 933 the safe use of pure alkali metals especially Li as anode material 934 when paired with high-potential insertion materials (5 V spinel 935 materials, Figure 4c) or with conversion  $S/O_2$ -based cathodes.<sup>171</sup> 936 Nevertheless, this ceramic electrolyte option could require again 937 the consumption of more inorganic materials such as metal-based 938 sulfides, oxides, or phosphates.<sup>169,172</sup> It is worth noting that the 939 emerging field of Na and Na-ion batteries which are also 940 considered in the post-LIB field logically follows the same 941 trajectory in terms of materials choice and design as a sister 942 material chemistry of Li-based batteries.<sup>173,174</sup> In addition, it 943 should be remembered that major built RFBs also draw their 944 chemical power from 3d-metals as well as already underlined 945 above.

While the number of publications and other reports has 947 greatly increased in recent years on the potential bottlenecks in 948 material supplies due to the ramping up of LIBs, <sup>146,155,154,175–177</sup> 040 the resource issue questionings in the field of energy storage 950 are not new especially for EV fleets since interesting estimates 951 were already reported by Andersson and Råde<sup>178</sup> as early as 952 2001 by taking into account almost all cell chemistries at that 953 time: Li-metal polymer (LMP), LIBs, sodium nickel chloride 954 (NaNiCl or ZEBRA batteries), Ni-metal hydrides (Ni-MH), 955 and PbA. Generally speaking, batteries that contain two or 956 more scarce metals may suffer from being limited by the 957 availability of any of them. With the pressure on LIBs and 958 future Li-based technologies, the main current concern is 959 about the potential risks surrounding the supply (and related 960 price volatility) of lithium and 3d-metals with battery-grade 961 quality (Co and Ni, essentially), which also raises the tricky 962 question of the mining interdependencies of elements;<sup>155</sup> note 963 that natural graphite is commonly reported as CRM. Indeed, 964 the supply of cobalt is complicated by the fact that this element 965 is not typically the primary product of mining operations; 966 it is a coproduct of nickel (50%) mining.<sup>179</sup> Figure S6 shows a 967 mapping and quantified data regarding the world mining 968 industry production for materials used in LIBs.<sup>155</sup> Taking 2016 969 as the year of reference, the battery industry's demand for 970 lithium and cobalt is 46% and 50% of the world production, 971 respectively.<sup>154</sup> It should also be underlined that 54% of the 972 mining production of Co comes from the Democratic Republic 973 of Congo, a country characterized by socio-political instability, 974 a persistent economic stagnation, and no environmental policies; 975 the country could lose 40% of its forests by 2050 notably due to 976 mining activities.<sup>180</sup>

To ensure continuous flows of raw materials, new agreements 978 are set up between critical material suppliers and different 979 customers; for example, Apple Inc. seems interested in buying 980 long-term supplies of cobalt directly from miners.<sup>181</sup> As previ- 981 ously stated by Andersson and Råde,<sup>178</sup> closed loop recycling 982

1068

983 solutions and a high level of collection of spent batteries 984 are required to ensure that the stock of available metals for 985 batteries is not drained. The case of PbA batteries constitutes a 986 textbook example with a collection of spent batteries above 987 99.9% thanks to environmental rules due to the lead toxicity 988 together with existing efficient recycling processes of this 989 simpler battery chemistry based essentially on Pb(Bi). In 2016, 990 almost all end-of-life LIB were batteries from consumer elec-991 tronics and 95% of spent LIB were unfortunately landfilled.<sup>182</sup> 992 Unlike recycling of PbA batteries, recycling of LIBs seems for 993 the moment not economically profitable albeit recycling LIBs 994 could save up to 51.3% of the natural resource required to 995 produce virgin materials (concept of Urban Mines).<sup>182</sup> Today, 996 most recyclers focus on recovering expensive materials mainly 997 from positive electrode powders, but lithium is rarely recovered 998 (less than 1% of lithium is recycled). Stronger political incen-999 tives seem required to promote recycling. In the EU, the 2006/ 1000 66/EC European directive<sup>183</sup> imposes a minimum recycling 1001 efficiency of Li-batteries at 50% by average weight into materials 1002 for their original purpose or for other purposes and second, 1003 encourages technological developments that improve the envi-1004 ronmental performance of batteries throughout their entire life. 1005 The reader can get precise and recent data regarding recycling 1006 end-of-life batteries, processing, and collections reported in refs 1007 146, 155, 182, and 184-187. Another hot point is that 1008 predictions underlined that all the material demand just for EV 1009 batteries will have to be supplied by resource extraction at least 1010 up to 2030 whatever the collection and recycling of spent 1011 battery electrode materials due to the eight-to-ten-year lifetime 1012 of EV batteries.<sup>143</sup> Note that reuse of EV batteries can offset 1013 the production burden of new batteries by extending battery 1014 service life.

#### 3.2. Sustainability and Environmental Aspects

1015 Beyond battery resource considerations which are getting all 1016 the attention today, let us also remember that mining opera-1017 tions are destructive for the environment and energy-greedy 1018 and fall short of both the sustainability and CO<sub>2</sub> footprint 1019 criteria.<sup>84,112</sup> Moreover, the scarcity of most of these elements 1020 in the earth crust (Figure 6) could make their excavation more 1021 and more energy intensive and costly depending on the nature 1022 of the deposit because it must be kept in mind that elemental 1023 availability cannot be judged by crustal abundance alone (see 1024 ref 162 for more details). Moreover, after the extraction of 1025 ores, several refining steps are necessary to obtain the final 1026 reagents which will be engaged thereafter in high temperature 1027 synthesis reactions ( $T \approx 600$  °C) to produce the desired 1028 electrode material.

1029 At this stage, relevant data to evaluate potential environment 1030 concerns as well as the related energy cost for the production 1031 of batteries can be found in life cycle assessment (LCA) 1032 studies. Although LCA can be considered as a standardized 1033 methodology, it depends on the inventory database used and 1034 system boundaries. Consequently, LCA results in the literature 1035 differ significantly due to these uncertainties. Peters et al.<sup>192</sup> 1036 have reported in 2017 an interesting review of LCA studies on 1037 LIBs. After a thorough review of 113 available publications 1038 on the topic, a total of 36 LCA studies were identified as very 1039 reliable because they provide detailed results for LIB produc-1040 tion and sufficient information to recalculate the reported 1041 results. The conclusion is, on average, a cumulative energy 1042 demand (denoted "embodied energy") of 328 kWh is needed across all chemistries to produce 1 kWh of stored electro- 1043 chemical energy producing GHG emissions of 110 gCO<sub>2</sub>eq. 1044

Beyond LIBs, other similar values concerning PbA, Ni-MH, 1045 or VRFBs can be found in the literature too.<sup>193,194</sup> Note that 1046 the majority of existing studies are focused on GHG emissions 1047 or energy demand; however, other Eco indicators such as 1048 human toxicity (HTP) might be even more important.<sup>192,195</sup> 1049 More importantly, such LCA studies are restricted at the manufacturing outlet ("cradle-to-gate analyses" and not "cradle-to-1051 grave analyses"), so they do not take into account both 1052 collection and recycling steps. Yet the results obtained show 1053 that battery manufacturing is energy-intensive because of the 1054 involvement of quite high flows of exergy mainly due to the 1055 chemical nature of the commonly used materials (inorganic 1056 compounds).<sup>112,162</sup>

As a result, one common recommendation of current LCA 1058 analyses is the deployment of batteries with higher round-trip 1059 efficiency to extend the cycle life in operation but also the 1060 need for low-carbon innovations in future technologies while 1061 favoring the use of naturally abundant chemical elements of 1062 low toxicity. Within this background, one current trend in the 1063 post-LIB field is to reinvestigate Na-ion batteries as candidates 1064 for medium and large-scale stationary energy storage in light 1065 of possible concerns in terms of cost and abundancy of 1066 lithium.<sup>174,196,197</sup>

# 3.3. Positioning Redox-Active Organic Species in the Battery Landscape

Within this background, which is particularly tense in many 1069 ways, the idea of taking advantage of organic chemistry for the 1070 electrochemical storage of energy can make sense. As stated in 1071 the Introduction, the idea to use organic electrode materials 1072 (OEMs) for rechargeable batteries is not new and goes back 1073 to the discovery of reversible redox-activity of conducting 1074 polymers in the late 70s following the discovery of PAc by 1075 Shirakawa<sup>61-64</sup> and its subsequent electrochemical activity 1076 (doping) both in oxidation and in reduction.<sup>65,66</sup> These findings 1077 led to the development of various conducting polymers as well 1078 as a first attempt to emerge in the marketplace before the boom 1079 of high-energy LIBs. 59,69 Today the motivations are different and 1080 authors agree that organics can be notably seen as a pathway to 1081 stabilize the pressure on the CRM for energy storage while 1082 seeking to improve the environmental footprint as well as finding 1083 innovative storage solutions.<sup>42,84</sup> Of course, OEMs have 1084 limitations especially when talking about volumetric energy 1085 density that can be achieved due to their intrinsic low 1086 volumetric mass densities (<2 g cm<sup>-3</sup>). Excluding ORFBs, this 1087 issue can be exacerbated by the need for large carbon addition 1088 when preparing composite electrodes. Moreover, their greater 1089 propensity to solubilize in liquids compared to inorganic com- 1090 pounds is an issue for solid electrodes but an asset for ORFBs. 1091 The development of organic batteries is clearly in its early 1092 stages compared to 150 years of intensive research and inno- 1093 vations dedicated to conventional inorganic-based electrochemical 1094 storage devices explaining why some room is expected to be given 1095 to redox-active organic species in the battery landscape. To be 1096 convinced, Figure 7 reports an interesting assessment for the 1097 electrochemical storage of OEMs classified by families.<sup>31</sup> In fact, 1098 organics exhibit several interesting assets as recapped below. 1099

First, organics make potential access to low cost and greener 1100 chemistry possible because they are mainly composed of C, H, 1101 O, N, and S, which are naturally abundant elements as well as 1102 the main constituents of biomass (Figure 6).<sup>191</sup> This situation 1103

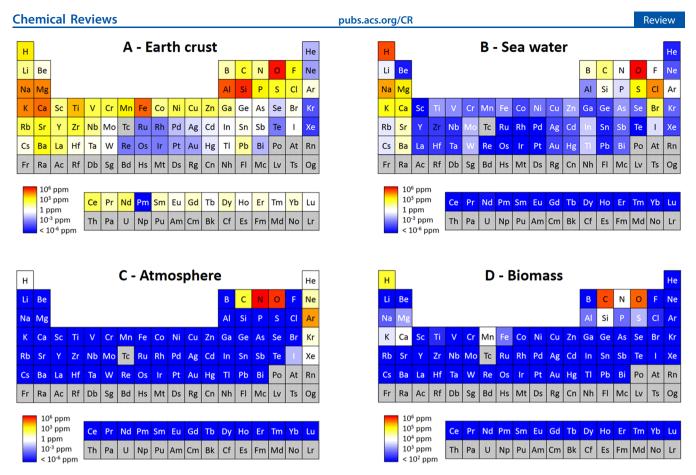


Figure 6. Periodic tables showing the abundance of elements in the Earth's crust (A), in the seawater (B), in the atmosphere (C), and in biomass (D); elements in gray indicate natural and/or radioactive elements. Courtesy of L. Simonin, CEA-Liten, adapted from ref 188 taking into account data from refs 189–191. This analysis highlights that among the naturally occurring elements only a few of them are abundant in each of these four compartments, which demonstrates the importance of developing recycling solutions too.

1104 offers opportunities to prepare electrodes (and other components 1105 in a cell like binders)<sup>198</sup> from renewable resources benefiting from 1106 ongoing progress in the vast field of biorefineries too. 199-201 1107 Hydrolysis lignin features were even assessed in primary Li-cell<sup>202</sup> 1108 or more interestingly in combination with PPy in an inter-1109 penetrating lignosulfonate/PPy thin-film composite electrode 1110 tested in 0.1 M aqueous HClO<sub>4</sub> as electrolyte, with the 1111 catechol moiety in lignin being used for reversible electron and 1112 proton storage/uptake.<sup>203</sup> Several naturally occurring poly-1113 phenols (e.g., ellagic acid,<sup>204</sup> purpurin,<sup>205</sup> lawsone<sup>206</sup>) were 1114 electrochemically assessed in Li/Na half cells; however, the 1115 proof of concept of making a "renewable" all-organic Li-ion 1116 battery was first demonstrated with oxocarbon derivatives as 1117 active electrode materials ten years ago.<sup>82-84</sup> Esquivel and co-workers<sup>207</sup> have also demonstrated opportunities for portable 1118 and disposable single-use applications to power small devices 1120 with the concept of PowerPAD (Power: Portable And Disposable), 1121 a fully organic and completely biodegradable battery designed 1122 to operate for relatively short periods of time (from minutes to 1123 1-2 h). The promising field of ORFBs (see section 9) has also 1124 demonstrated interest in the use of redox-active naturally 1125 occurring polyphenols/quinones for abundancy and cost 1126 reasons.<sup>20,34</sup> At this stage, it must be underlined that common 1127 routes to synthesize OEMs in this emerging field deal with 1128 petrochemicals. However, even if large scale production were 1129 used for high-performance OEMs in the future, petrochemicals 1130 are higher-value products than petroleum products for 1131 combustion (only a small fraction ( $\approx 4\%$ ) of oil worldwide is

used to make chemicals<sup>42</sup>). In terms of cost, it is difficult to 1132 make predictions for petrochemical reagents notably if in the 1133 future the demand for petroleum products used for combustion 1134 decreases; the access to new markets and applications can 1135 change the game. However, it is generally accepted that 1136 fluorinated derivatives are among the most expensive compounds. 1137

Second, simplified recycling managements of organic spent 1138 batteries (Figure S7) can be expected notably with solid 1139 electrodes since organic structures are typical fuels that can be 1140 consumed by combustion at medium temperatures producing 1141 heat (energy recovery). Interestingly, if spent organic batteries 1142 were inadvertently not collected (spread out in the wild), the 1143 loss of scarce and costly metallic chemical is notably reduced 1144 compared to the current battery technologies. Moreover, the 1145 use of biodegradable materials can be envisaged too. 1146

Last but not least, organic chemistry offers high structural 1147 designability providing great opportunities to find novel and 1148 innovative electrode materials with specific properties includ-1149 ing the elaboration of multimodal systems such as electro-1150 chemical/chemical or electrochemical/photochemical rechar-1151 geability.<sup>208–210</sup> More importantly, physicochemical properties 1152 can be rationally tuned using well-established principles of 1153 organic chemistry and molecular engineering giving access to 1154 redox-active species able to work: 1155

 from dissolved to solid state (including polymers) in 1156 aqueous or nonaqueous electrolytes making them 1157 versatile in terms of electrochemical storage devices 1158 including access to flexible devices; 1159 pubs.acs.org/CR

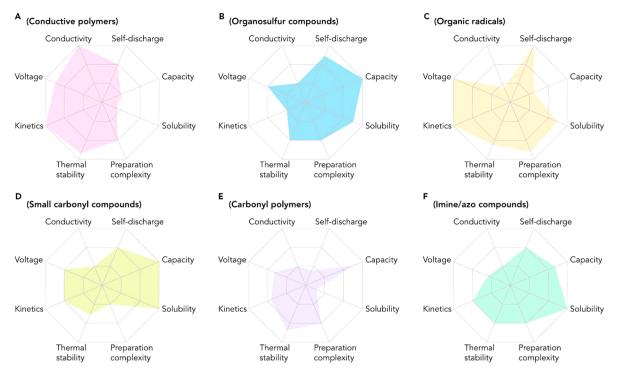


Figure 7. Overview of fundamental properties of different types of organic electrode materials. Reproduced with permission from ref 38. Copyright 2018 Elsevier Ltd.

- through two electrochemical storage mechanisms (n- or p-type electrode reaction with cation or anion charge compensation) making various electrode configurations possible (see the next section);
- at adjusted redox potential because the electron density 1164 at the molecular level can be easily tuned by mesomerism 1165 in conjugated systems and more importantly by inductive 1166 effects using either electron-withdrawing (-I) groups or 1167 electron-donating (+I) groups. For example, computa-1168 tional modeling concerning the one-electron reduction 1169 potential of various substituted quinones shows a possible 1170 potential tuning ( $\Delta E^{\circ}$ ) of about 1.5 V;<sup>211</sup> 1171
- with potentially reversible multielectron reactions which
   could counterbalance a slightly too important molecular
   weight;
- with multivalent cation and bulky ions (e.g., Mg<sup>2+</sup>, K<sup>+</sup>, PF<sub>6</sub><sup>-</sup>) because organics (polymers and crystallized host structures) can better accommodate structural changes thanks to weak-bond networking;
- potentially without any metal following the concept of "molecular organic-ion battery".<sup>212-214</sup>

<sup>1181</sup> Whether organic chemistry offers high structural desig-<sup>1182</sup> nability through this multiplicity of chemical combinations at <sup>1183</sup> the molecular level, it could be somewhat challenging to grasp <sup>1184</sup> the electrochemical working principle of the reported OEMs in <sup>1185</sup> the literature for researchers more familiar with inorganic <sup>1186</sup> electrode materials. In the next section we will try to make under-<sup>1187</sup> standable all the redox functioning of organic molecular assemblies <sup>1188</sup> with the basics of electrochemical cells as a starting point.

#### 4. FUNDAMENTALS OF ORGANIC ELECTRODE COMPOUNDS FOR ELECTROCHEMICAL STORAGE

#### 4.1. Basics of Electrochemical Cells

1190 As reported in all undergraduate chemistry books, primary and 1191 secondary (rechargeable) cells (or batteries) produce discharge DC current for an output voltage of a few volts by direct con- 1192 version of chemical energy by virtue of two opposite oxidation- 1193 reduction processes occurring at two separated electrodes 1194 (current collectors) maintained in ionic contact through an 1195 electrolytic medium (Figure 8).<sup>84</sup> In such a situation, the two 1196 half redox reactions taking place at electrodes are called 1197 "electrochemical reactions". During discharge (spontaneous 1198 cell reaction or galvanic cell reaction), the electrochemical 1199 reduction reaction occurs at the positive electrode whereas the 1200 electrochemical oxidation reaction occurs at the negative 1201 electrode. For rechargeable cells, the terminology should be 1202 obviously reversed during charge (electrolysis cell reaction). 1203 Therefore, to avoid confusions, the terms "positive" electrode 1204 or "negative" electrode are preferred whatever the considered 1205 cell reaction (i.e., charging or discharging), with the positive 1206 electrode always displaying the highest potential value. Note 1207 that a cell is the basic electrochemical unit. A battery is com- 1208 posed, strictly speaking, of two or more such cells connected in 1209 g series or parallel. However, the term battery has evolved, 1210 especially in the language of the end user; therefore, the term 1211 "battery" will be used herein without this distinction for the 1212 sake of simplicity. 1213

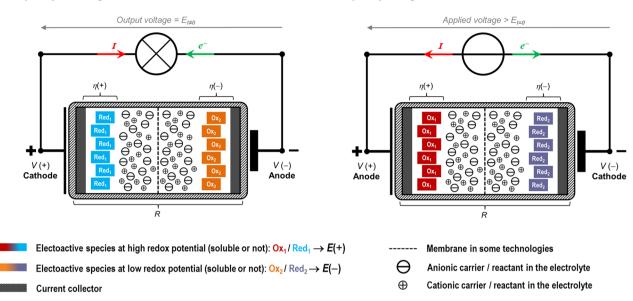
The use of two antagonist redox couples is then required 1214 with (e.g.,  $Ox_1/Red_1$  and  $Ox_2/Red_2$  characterized by standard 1215 potentials  $E^{\circ}(Ox_1/Red_1) > E^{\circ}(Ox_2/Red_2))$  to reach high 1216 electromotive force (*emf* =  $E_{I=0}$ , in V) at the cell level under 1217 zero current since *emf* depends on the difference  $E^{\circ}(Ox_1/Red_1)$  1218  $- E^{\circ}(Ox_2/Red_2) > 0$  or more generally on the difference E(+) 1219 - E(-) > 0. In short, it depends on the thermodynamics of the 1220 chosen electrode chemistries because  $E_{I=0}$  is related to the 1221 Gibbs free energy change of the galvanic cell reaction,  $\Delta_r G$ , as 1222 g follows:  $\Delta_r G = -n \cdot E_{I=0} \cdot F$  (*n* being the number of electrons 1223 involved in the cell reaction and *F* is the Faraday constant, 1224 equal to 96,485 C mol<sup>-1</sup>). Under discharge current (*I*, in mA), 1225 for example, the operating voltage,  $E_{I\neq0}$ , is lower than the  $E_{I=0}$  1226

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b) Fully charged state

Review

#### a) Fully discharged state



**Figure 8.** General architecture of an electrochemical cell for energy storage whatever the considered technology is. Note that additional electrolyte can be stored externally and then pumped through the cell in the particular case of a flow battery (see Section 9). (a) Cell under discharge (namely galvanic cell) at 100% depth-of-discharge (DOD). (b) Cell under charge (namely electrolysis cell) at 100% state-of-charge (SOC); the electromotive force value (*emf* =  $E_{I=0}$ ) is, in principle, at the maximum value. The measured capacity, Q (in mAh), is experimentally obtained by integrating the operating time with current:  $Q = \int_0^t I(t) \cdot dt = I \cdot \Delta t$  which gives rise to  $Q = I \cdot \Delta t$  whereas the energy,  $\varepsilon$  (in mWh), is obtained by multiplying Q with the voltage  $E_{I \neq 0}$ .

1227 value because of (*i*) kinetic limitations at the electrodes 1228 (overpotentials or polarization losses,  $\eta$ ) and (*ii*) ohmic drop 1229 ("*R*·*I*" term) due to the overall ohmic resistance (*R*, in  $\Omega$ ) of 1230 electrodes and electrolytes as shown below:

$$E_{I\neq 0} = [E(+) - E(-)] - [\eta(+) + \eta(-)] - [R \cdot I]$$

1231 Obviously, high  $E_{I=0}$  values with minimum losses in 1232 operation are sought after together with high capacity values, 1233  $Q_i$  in C (or Ah a unit more generally used in the field of 1234 electrochemical generators). By virtue of Faraday's law, the 1235 theoretical expected Q value of a cell is proportional to *n* and 1236 the amounts of the redox (electroactive) chemical species. 1237 Normalizations of Q are often reported to make performance 1238 comparison easier giving rise for example to specific capacity 1239 ( $Q_m$ ) per gram of electroactive compound and volumetric 1240 capacity ( $Q_v$ ) per cm<sup>3</sup> of electroactive compound (*M* being the 1241 molar mass and  $\rho$  the specific density of the electroactive 1242 species, respectively):

$$Q_m$$
 (C g<sup>-1</sup>) =  $n \cdot F/M$  or  $Q_m$  (mAh g<sup>-1</sup>) =  $n \cdot 26805/M$   
 $Q_v$  (C cm<sup>-3</sup>) =  $n \cdot F \cdot \rho/M$  or  $Q_v$  (mAh cm<sup>-3</sup>) =  $n \cdot 26805 \cdot \rho/M$ 

1243 Multiplying Q with  $E_{I\neq0}$  at any time during the discharge makes 1244 the calculation of the as-obtained energy,  $\varepsilon$  (in mWh). Of course, 1245 high reversibility of the cell reaction (good cyclability), high 1246 Coulombic efficiency, and low self-discharge are notably required 1247 for long-lasting cycling of rechargeable batteries. More details can 1248 be found in specialized books (see for example, ref 2).

#### 4.2. Bridging the Gap between Inorganic and Organic 1249 Redox Chemistry

1250 As previously recapped, oxidation—reduction reactions make elec-1251 tricity production possible when properly used in a two-electrode 1252 cell design. Hence, redox-active chemical systems (especially reversible ones) constitute the workhorse of the electrochemist 1253 in the design of electrochemical generators. Beyond exploiting 1254 the potential values of redox couples (thermodynamics) to 1255 decide if the interest for a given system is related to positive or 1256 negative electrode application, the electrochemist follows with 1257 a great deal of interest variations of oxidation states ( $OS_3$ ; or 1258 oxidation number, ON) of chemical elements constituting 1259 the considered redox couples because it allows us to readily 1260 understand and rationalize the formal involved redox center as 1261 well as subsequently determine the number of electrons involved 1262 in the half-reaction. Latimer appears to be the first to introduce 1263 this concept within the context of redox half-reactions.<sup>215</sup>

According to the IUPAC definition,<sup>216</sup> the *OS* of an atom is 1265 the charge of that atom after an ionic approximation of its 1266 heteroatomic bonds. The bonds between atoms of the same 1267 element are not replaced by ionic bonds; they are divided 1268 equally. In other words, to determine the *OS* of a given atom, it 1269 is therefore considered that all heteroatomic bonds in which it 1270 participates are 100% ionic and the electrons of each of these 1271 bonds are assigned to the most electronegative atom (Allen's scale). 1272 Moreover, IUPAC recommends two closely related general algo-1273 rithms for *OS* calculation in molecules, ions, and extended solids:<sup>216</sup> 1274

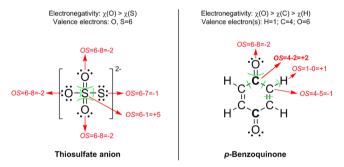
- Algorithm of assigning bonds. This algorithm works on 1275 structural Lewis formulas of molecules and ions which 1276 show all valence electrons. 1277
- Algorithm of summing bond orders. This algorithm 1278 works on structural Lewis formulas and bond graphs for 1279 an extended solid, especially iono-covalent structures. 1280

However, as thoroughly explained above, because the used 1281 redox chemistry in battery applications is related to the OS 1282 change of the 3d-metallic redox centers (e.g., Ti, V, Mn, Fe, 1283 Co, Ni) or elemental/diatomic substances (e.g., Li, Na, Mg, C, 1284  $O_2$ , Si, P, S, Sn),<sup>11</sup> a set of more general rules for determining 1285 OS is more readily used (e.g., *"the sum of OS for all atoms in the* 1286

1287 species is zero to ensure electroneutrality", "Fluorine: -1", 1288 "Oxygen: -2 unless combined with fluorine", and so on) as 1289 nicely recalled by Walsh et al.<sup>217</sup> Although not recommended 1290 by IUPAC, this simplest method is quite sufficient to assign OS 1291 of most (inorganic) ions and extended solids. Complications 1292 occur when two identical atoms have different OS in the same 1293 compound like observed with several inorganic compounds 1294 based on chemical elements prone to catenation (*e.g.*, C, N, S, 1295 Si, I). This is precisely the situation encountered with organic 1296 compounds, which justifies the use of the algorithm of assigning 1297 bonds recommended by IUPAC based on Lewis formulas of 1298 molecules and ions to determine OS or organics. In practice, after 1299 assignment of electrons of each bond to the most electronegative 1300 element, the OS of element "*i*" is calculated as follows:

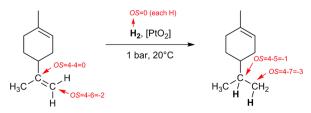
### OS(i) = valence electrons of the element "*i*" - $\sum$ assigned electrons

1301 Two selected examples are shown below including the case of 1302 the inorganic thiosulfate anion  $(S_2O_3^{2-})$  considering that the 1303 sulfur–sulfur bond is practically a single bond together with 1304 *p*-benzoquinone as representative redox-active organic molecule. 1305 Note that only half of *OS* are reported due to the molecule 1306 symmetry whereas the green lines indicate the electrons 1307 assigned per atom. To briefly comment on the redox activity of 1308 *p*-benzoquinone, each carbon atom bearing the oxygen (in 1309 bold) exhibits an *OS* value of +2 that is decreased at +1 after 1310 the two-electron reduction to produce *p*-hydroquinone.



#### 4.3. Reversible Organic Redox Chemistry and Cell 1311 Configurations

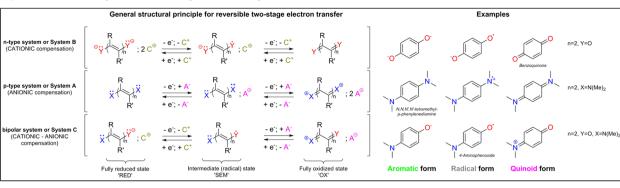
1312 Oxidation-reduction processes in organic chemistry, which 1313 commonly involve both *s* and *p* orbitals, can be classified in 1314 two different groups. In the first group, the electronic process 1315 is accompanied by atom transfer reaction (e.g., gain of oxygen 1316 for oxidation or hydrogen for reduction) including possible 1317 fragmentation or condensation subsequent reactions.<sup>218</sup> However, 1318 such organic redox reactions are basically used for organic 1319 synthesis purpose as shown below in the case of the hydro-1320 genation reaction of the most accessible double bond of 1321 limonene (reduction process of the C=C double bond with 1322 decreasing of the *OS* of the two carbon atoms whereas the two 1323 incorporated H atoms exhibiting an *OS* of +1).



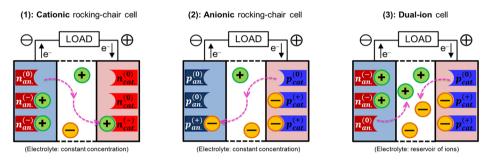
More interestingly for us are the redox processes for which 1324 no formation or rupture of electron-pair single bonds occurs 1325 after simple charge transfer reaction. In this latter case, 1326 stepwise transfer of single electrons must in principle be taken 1327 into account<sup>219</sup> giving potentially access to reversible organic 1328 redox couples like conventional third-kind electrode reactions 1329 (e.g.,  $Ce^{4+} + e^- \Rightarrow Ce^{3+}$ ). However, caution should be 1330 exercised because one-electron oxidation or reduction of a 1331 neutral or ionic organic scaffold produces generally reactive ion 1332 radicals or radicals with possible subsequent reaction such as 1333 radical coupling. Consequently, some chemical tricks have to 1334 be used to ensure the production of stable (persistent) radical 1335 structures after charge transfer. <sup>220,221</sup> Thus, simple  $\pi$ -extension 1336 and substituents of resonance electron donating or with- 1337 drawing groups (mesomerism) make delocalization of spin and 1338 charge density possible which deeply reduces the reactivity of 1339 the odd electron (e.g., galvinoxyl or tris(pentachlorophenyl)- 1340 methyl radicals). Aromatization after electron transfer and 1341 appropriate steric protection play also important role to protect 1342 a reactive radical center. Robust functional groups bearing an 1343 unpaired electron also exist such as nitroxide radicals (>N-O<sup>•</sup>). 1344 In this family, 2,2,6,6-tetramethylpiperidinyl-N-oxy (TEMPO) 1345 constitutes the most representative example. Beyond the reali- 1346 zation of magnetic organic materials,<sup>221</sup> the nitroxide redox 1347 chemistry is at the origin of the rise of ORBs,<sup>10,75-77</sup> a field 1348 particularly studied by Nishide, Oyaizu, and co-workers as 1349 previously underlined in the Introduction. Finally, the general 1350 structure principles that lead to multistage organic redox 1351 systems (expected reversible from a redox point of view) are 1352 owed to Deuchert and Hünig<sup>219</sup> reported in a comprehensive 1353 article published in 1978. 1354

Figure 9a recalls the three general key organic structures and 1355 their related charge transfer steps deriving from Hünig's 1356 classification together with representative examples of chemical 1357 compounds. Basically, two electrochemical storage mecha- 1358 nisms are accessible with organics characterized either by anion 1359 charge compensation (p-type system or System A) or by cation 1360 charge compensation (n-type system or System B); System C 1361 being a mixed assembly also named "bipolar" system. At other- 1362 wise constant conditions it is worth noting that redox-active 1363 p-type moiety exhibits as a rule higher formal potential values 1364 compared to n-type systems.<sup>219</sup> Figure 9b shows the corre- 1365 sponding cell configurations. For instance, developing Li-ion 1366 organic batteries requires two n-type compounds (Figure 9b-1). 1367 The p-type redox reactivity is rarely encountered with inorganic 1368 electrode materials. Except carbonaceous materials which 1369 intercalate ions at relatively high potential (use as positive 1370 electrode),  $^{222-225}$  only a few conversion-type electrode 1371 materials have been reported to date (for F-ion batteries) 1372 exhibiting however poor electrochemical performances.<sup>226</sup> On 1373 the other hand, p-type organic compounds enable, in principle, 1374 the development of anionic rocking-chair cells<sup>227,228</sup> and 1375 potentially full "molecular" organic-ion batteries if the shuttling 1376 anion is metal free (Figure 9b-2). Nevertheless, the cell 1377 assembly most often encountered in the literature remains the 1378 dual-ion battery (Figure 9b-3) as recently review by Zhou 1379 et al.<sup>229</sup> The use at the electrode level of advanced mixed 1380 p/n-type organic scaffolds that exchange simultaneously 1381 cations and anions can also be envisaged as recently shown 1382 in aqueous batteries with naphthalene diimide repeating units 1383 coupled to bipyridinium.<sup>230–232</sup> The molecular engineering 1384 can even allow cation shuttling in the electrolyte while using 1385 p-type electrodes as reported by Nishide, Oyaizu, and co-workers 1386

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**Figure 9.** (a) Key reversible redox-active organic systems at the molecular level and their related charge transfer steps (adapted from refs 219 and 234) together with representative examples exhibiting the redox rocking from aromatic to quinoid form. X/Y could be N, O, S, P,  $\pi$ -systems but also carboxylate, anhydride, or amide functional groups; R, R' being potentiality integrated within the same cyclic structure. Note that that p- and n-type structures correspond to system A and B, respectively, according to Hünig's classification.<sup>219</sup> (b) Corresponding cell configurations obtained by playing with both n- and p-type systems shown during the discharge process. Again, additional electrolyte can be stored externally and then pumped through the cell in the particular case of a flow battery (see Section 9). Adapted with permission from ref 36. Copyright 2018 Elsevier Ltd.

1387 with copolymer compositions of TEMPO–sulfonate anionic 1388 group.<sup>233</sup>

a) Electrochemical storage mechanisms using redox-active organic centers

Finally, before reporting our selection (with description) of the 1390 best organic-based batteries to date, a summary of the organic 1391 families of interest for electrochemical storage is shown in Table 1 1392 demonstrating the richness in terms of formal redox center as well 1393 as the relevance of conjugated structures in general.

#### 5. PERFORMANCES OF NONAQUEOUS 1394 LITHIUM–ORGANIC BATTERIES

1395 This section constitutes the first in a series of five (from section 1396 5 to 9) in which a personal selection of organic-based recharge-1397 able cells will be described and commented on. Nonaqueous 1398 Li-organic batteries have by far the longest history among all 1399 branches of battery OEMs applications. The results from these 1400 pieces of research have also directly fueled or inspired the 1401 design of OEMs for other emerging organic batteries. Several 1402 comprehensive review articles have covered virtually every 1403 category of OEMs used in Li–organic batteries;<sup>9,39,43,47</sup> hence, 1404 another comprehensive write-up on the topic is not intended 1405 herein. Instead, we will focus on the best performance ever 1406 achieved by OEMs in these batteries as well as the design 1407 rationale behind these successes. In particular, three key 1408 performance parameters will be reviewed: operating potential, 1409 specific capacity, and cycling stability. The properties and cell 1410 performance of these materials are summarized for compre-1411 hensive comparison (Table 2).

#### 5.1. Positioning the Operation Voltage

1412 A large variety of redox active functional groups have been 1413 explored for designing OEMs for Li-based batteries, and the voltages of cells based on these OEMs vary by a wide extent as 1414 a result. Depending on their operating potentials, OEMs may 1415 be used either as positive electrode (>2.2 V vs Li<sup>+</sup>/Li) or 1416 negative electrode (<1.5 V vs Li<sup>+</sup>/Li) active materials. Again, 1417 OEMs intrinsically showing the highest potentials, e.g. >3.5 V 1418 vs Li<sup>+</sup>/Li, are p-type compounds which, upon charge, lose 1419 electrons and accept anions from the electrolytes (Figure 9). 1420 As previously mentioned, conductive polymers, which had 1421 been intensively studied as positive electrode materials to 1422 enable Li batteries (dual-ion cell configuration, Figure 9b-3), 1423 fall into this category too. Prime examples include the PAc<sup>292</sup> 1424 (Table 2, entry 1), PAni, PPy, PT, and poly(p-phenylene) 1425 families.<sup>59</sup> Their operating potentials vary according to the 1426 type of polymer backbones and can approach 4 V vs Li<sup>+</sup>/Li due 1427 to the p-type redox activity. The charge storage mechanism 1428 of conductive polymers is based on multiple  $\pi$ -conjugated 1429 repeating units stabilizing one positive charge via charge 1430 delocalization. Unfortunately, as more charges are stored, fewer 1431 repeating units are available to stabilize the charges, and the 1432 polymers become less stable. 1433

More recent designs of high-potential p-type OEMs relied 1434 on dedicated redox centers for positive charge stabilization. 1435 These redox centers usually involve either carbon, oxygen, or 1436 nitrogen centers stabilized by aromatic structures and electron-1437 donating functional groups. The polycyclic aromatic hydro-1438 carbon coronene mimics mini graphene sheets and reversibly 1439 gives out 0.68 electrons per molecule upon charging (Table 2, 1440 entry 2).<sup>235</sup> It delivers one of the highest average discharge 1441 potentials of 4.0 V vs Li<sup>+</sup>/Li among OEMs. 2,3,6,7,10,11- 1442 Hexamethoxytriphenylene (HMTP) undergoes a full one- 1443 electron redox reaction despite the smaller polycyclic aromatic 1444

Reversible redox-active moiety	Classification	General redox mechanism	Example of electrode reaction
Conjugated carbonyl	n-type	$\overset{;;;;}{\bigvee} \xrightarrow{e^{e^{i}}} \overset{;;;;}{\bigvee} \xrightarrow{e^{e^{i}}} \overset{;;;;;}{\bigvee}$	$\left( \bigvee_{n=0}^{\infty} S_{n}^{*} \right)_{n} : 2 C^{*} \xrightarrow{2 e^{*}_{1} \cdot 2 C^{*}}_{+2 e^{*}_{1} \cdot 2 C^{*}} \left( \bigvee_{n=0}^{\infty} S_{n}^{*} \right)_{n} PBQS$
Organodisulfide	n-type	2 ; :: :: :: :: :: :: :: :: :: :: :: :: ::	$\begin{array}{c} S \\ S $
Conjugated azo group	n-type	$ \begin{array}{c c} & & & & \\ \hline & & & \\ & & & & \\ & & & & \\ & & & \\ & & & & \\ & & & & \\ & & & & \\ & & & & \\ & & & & \\ & & & & \\ & & & & \\ & & & & \\ & & & $	$LiO_2C - \underbrace{N}_{N} - \underbrace{CO_2Li}_{; 2 C^*} (2 C^* + \frac{2 e^*; -2 C^*}{42 e^*; +2 C^*} + LiO_2C - \underbrace{N}_{N} - \underbrace{CO_2Li}_{N} ADALS$
Conjugated nitrile	n-type	← C = N : +e' ← C = N :	$ \begin{array}{c} \overset{N}{\underset{()}{()}{\underset{()}{\atop()}{\underset{()}{\underset{()}{\atop()}{\underset{()}{\underset{()}{\atop()}{\underset{()}{\underset{()}{\atop()}{\underset{()}{\underset{()}{\underset{()}{\underset{()}{\underset{()}{\underset{()}{\underset{()}{\underset{()}{\underset{()}{\underset{()}{\atop()}{\underset{()}{\underset{()}{\underset{()}{\underset{()}{\underset{()}{\underset{()}{\atop()}{\underset{()}{\underset{()}{\underset{()}{\atop()}{\underset{()}{\atop()}{\underset{()}{\atop()}{\underset{()}{\atop()}{\underset{()}{\atop()}{\underset{()}{\atop()}{\underset{()}{\atop()}{\underset{()}{\atop()}{\underset{()}{\atop()}{\atop()}{\underset{()}{\atop()}{\atop()}{\underset{()}{\atop()}{\atop()}{\underset{()}{\atop()}{\underset{()}{\atop()}{\underset{()}{\atop()}{\atop()}{\atop()}{\underset{()}{\atop()}{\atop()}{\underset{()}{\atop()}{\atop()}{\atop()}{\atop()}{\atop()}{\underset{()}{\atop()}{\atop()}{\underset{()}{\atop()}{\atop()}{\atop()}{\atop()}{\atop()}{\underset{()}{\atop()}{\atop()}{\atop()}{\atop()}{\atop()}{\atop()}{\atop()}{$
Conjugated amine	p-type		$Ppy \left( \begin{array}{c} H \\ N \\ H \end{array} \right) \left( \begin{array}{c} H \\ H \end{array} \right) \left( \begin{array}{c} 2 e^{i} + 2 A^{i} \\ \bullet^{i} + 2 e^{i} + 2 A^{i} \end{array} \right) \left( \begin{array}{c} H \\ H \\ H \end{array} \right) \left( \begin{array}{c} H \\ H \\ H \end{array} \right) \left( \begin{array}{c} H \\ H \\ H \end{array} \right) \left( \begin{array}{c} H \\ H \\ H \end{array} \right) \left( \begin{array}{c} H \\ H \\ H \\ H \end{array} \right) \left( \begin{array}{c} H \\ H \\ H \\ H \end{array} \right) \left( \begin{array}{c} H \\ H \\ H \\ H \\ H \end{array} \right) \left( \begin{array}{c} H \\ $
Conjugated etheroxide	p-type	$\bigvee_{i=1}^{0} \bigvee_{i=1}^{-e^{i}} \bigvee_{i=1}^{+e^{i}} \bigvee_{i=1}^{$	
Conjugated thioether	p-type	$\bigvee \stackrel{\tilde{s}}{\longrightarrow} \bigvee \stackrel{\tilde{-e^{-}}}{\longleftrightarrow} \bigvee \stackrel{\tilde{s}}{\longleftarrow} \bigvee$	$PT  \left( \begin{array}{c} S \\ S $
Nitroxide radical	n/p-type (bipolar)	$\overset{A}{\overset{N}{\overset{N}{\overset{-e}{\overset{e}{\overset{A}{\overset{H}{\overset{H}{\overset{+e}{\overset{e}{\overset{A}{\overset{N}{\overset{A}{\overset{H}}{\overset{H}{\overset{H}{\overset{H}{\overset{H}}{\overset{H}{\overset{H}{\overset{H}{\overset{H}}{\overset{H}{\overset{H}{\overset{H}}{\overset{H}{\overset{H}}{\overset{H}{\overset{H}{\overset{H}{\overset{H}{\overset{H}}}}}}}}}$	$\begin{array}{c} \left( \begin{array}{c} \begin{array}{c} \\ \\ \\ \end{array}\right)^n \\ \\ \end{array}\right)^n \\ \left( \begin{array}{c} \\ \\ \end{array}\right)^n \\ \end{array}\right)^n \\ \left( \begin{array}{c} \\ \\ \end{array}\right)^n \\ \end{array}\right)^n \\ \left( \begin{array}{c} \\ \\ \end{array}\right)^n \\ \left( \begin{array}{c} \\ \\ \end{array}\right)^n \\ \end{array}\right)^n \\ \left( \begin{array}{c} \\ \\ \\ \end{array}\right)^n \\ \left( \begin{array}{c} \\ \end{array})^n \\ \left( \begin{array}{$

#### Table 1. A Few Electrochemical Storage Mechanisms in Redox-Active Organics Together with Examples<sup>4</sup>

<sup>a</sup>PBQS: poly(benzoquinonyl sulfide); PDTTA: poly(5,8-dihydro-1*H*,4*H*-2,3,6,7-tetrathia-anthracene; ADALS: azobenzene-4,4'-dicarboxylic acid lithium salt; TCNQ: tetracyanoquinodimethane; PPy: polypyrrole; DBMMB: 2,5-di-*tert*-butyl-1-methoxy-4-[2'-methoxyethoxy]benzene; PT: polythiophene; PTMA: poly(2,2,6,6-tetramethylpiperidinyloxy-4-yl methacrylate). Note the redox-active nitroxide radical is bipolar, in practice, good kinetics are only attempted with the p-type activity.

1445 hydrocarbon core than that found in coronene (Table 2, 1446 entry 3).<sup>236</sup> The auxiliary electron-donating methoxy groups 1447 seem to have contributed to the higher p-doping level albeit 1448 with a lower discharge potential of 3.5 V vs Li<sup>+</sup>/Li. 1449 Tetrathiafulvalene (TTF) is a  $\pi$ -conjugated molecule famous 1450 for its distinctive electronic properties in the highly stabilized 1451 oxidized form. OEMs incorporating the TTF structure, such as 1452 2,2'-bis[5-(1,3-dithiol-2-ylidene)-1,3,4,6-tetrathiapentanyli-1453 dene] (TTPY, Table 2, entry 4) and pentakis-fused TTF 1454 (Table 2, entry 5), show almost full utilization of two electrons 1455 power of the sulfur atoms.<sup>237</sup> Pentakis-fused TTF shows a 1457 higher voltage than that of TTPY (3.56 against 3.4 V vs Li<sup>+</sup>/Li) 1458 due to the higher number of electrons involved in the reaction 1459 (Figure 10A).<sup>238</sup>

Beyond conjugated hydrocarbon and thioether families, the 1460 1461 one-electron oxidation reaction of nitroxide radical<sup>10,75–77</sup> has 1462 spawned a large body of literature on radical polymer electrodes 1463 (Table 1). The poster-child building block of radical polymers 1464 is 2,2,6,6-tetramethyl-1-piperidinyloxy (TEMPO), where the 1465 nitroxide radical is sterically stabilized by the neighboring 1466 methyl groups. Polymers incorporating the TEMPO block, 1467 most notably poly(2,2,6,6-tetramethyl-1-piperidinyloxy-4-yl 1468 methacrylate) (PTMA) (Table 2, entry 6), deliver discharge 1469 potential of ~3.55 V vs Li<sup>+</sup>/Li (Figure 10B).<sup>75,239</sup> The 1470 potential can be tuned by using different nitroxide-containing 1471 cores. For example, poly(2,2,5,5-tetramethyl-3-oxiranyl-3-pyrro-1472 lin-1-oxyl ethylene oxide) (PTEO, Table 2, entry 7), which 1473 contains the 2,2,5,5-tetramethyl-1-pyrrolidineoxy (PROXYL) 1474 core, shows a higher potential of 3.7 V vs Li<sup>+</sup>/Li.<sup>240</sup> Recently, 1475 a nonradical oxygen center was reported in the form of dibenzo-1476 1,4-dioxin (DD) (Figure 10C, Table 2, entry 8).<sup>241</sup> A remark-1477 ably high discharge potential of 4.1 V vs Li<sup>+</sup>/Li was observed,

though only one out of the two oxygen atoms in the molecule 1478 contributed to charge storage. Nitrogen centers in aromatic 1479 amines may be easier to incorporate into a molecule from the 1480 organic synthesis point of view. Triphenylamine (TPA) is 1481 among the most studied building blocks in organic electronics. 1482 TPA-based OEMs, such as triphenylamine-based polymers 1483 (PTPA, Table 2, entry 9) show competitive discharge 1484 potentials of ~3.6 V vs Li<sup>+</sup>/Li.<sup>242</sup> Many other aromatic amines 1485 have been studied as OEMs as well including small mole- 1486 cules<sup>243,244</sup> and organic salt forms such as dilithium 2,5- 1487 (dianilino)terephthalate (Li<sub>2</sub>DAnT), which are quite less soluble 1488 than non-salt molecules as further explained below (Table 2, 1489 entry 10).<sup>245</sup>

Compared with p-type OEMs, the n-type counterparts have 1491 attracted greater research interest because of giving access 1492 to the reversible storage of Li<sup>+</sup> and potentially to cationic 1493 "rocking-chair"-type batteries when n-type electrode materials 1494 are properly designed (Figure 9). p-Benzoquinone (p-BQ) is 1495 one of the most studied n-type building blocks for OEMs 1496 (Table 1). The basic p-BQ molecule shows two discharge 1497 plateaus at 2.9 and 2.5 V vs Li<sup>+</sup>/Li with equal capacities, 1498 averaging to a discharge potential of 2.7 V vs Li<sup>+</sup>/Li (Figure 10D, 1499 Table 2, entry 12).<sup>246</sup> OEMs resembling the *p*-BQ structure show 1500 similar potentials as p-BQ. BBQ, a dimer of p-BQ, and 1,4,5,8-1501 phenanthrenediquinone (PADQ), a three-ring molecule incorpo- 1502 rating two p-BQ units show discharge potentials at 2.9 and 2.77 V 1503 vs Li<sup>+</sup>/Li, respectively (Table 2, entry 18, 19).<sup>247,248</sup> The slightly 1504 higher potential than that of p-BQ may be related to the limited 1505 specific capacity (i.e., relatively small depth of discharge) rather 1506 than performance improvement by design, however. Polymers 1507 that incorporate the p-BQ structure without much modifica- 1508 tion to the building block preserve the discharge potential. 1509 PBQS and poly(2,5-dihydro-p-benzoquinonyl sulfide) (PDBS) 1510

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#### Table 2. Performances of Selected Nonaqueous Li-Organic Batteries

#	Cell configuration (ionic carriers)	Positive electrode (or "cathode") active material	Negative electrode (or "anode")	Electrolyte	Output voltage (V)	Cycling stability: retention, cycles, rate or current density	Specific capacity (mAh g <sup>-1</sup> ) and Specific energy (Wh kg <sup>-1</sup> ) <sup>a</sup> per mass of active material, Final coulombic efficiency, Loading (mg cm <sup>-2</sup> )	Ref.
1	ClO4 <sup>-</sup>	, Polyacetylene	Li	1 M LiClO4 in PC	4.0	N/A	200, 471	[ <sup>292</sup> ]
2	PF6 <sup></sup>	Coronene	Li	1 M LiPF <sub>6</sub> in EC/DEC	4.0	92%, 960, 20 mA g <sup>-1</sup>	40, 140	[235]
3	PF <sub>6</sub> −	H <sub>3</sub> CO H <sub>3</sub> CO H <sub>3</sub> CO OCH <sub>3</sub> HMTP	Li	1 M LiPF6 in EC/DEC	3.5	92%, 80, 1 C	67, 190	[ <sup>236</sup> ]
4	$\mathrm{BF_4}^-$	$\begin{bmatrix} s \\ s $	Li	1 M LiBF4 in EC/DEC	3.3	84%, 100, 0.2 C	168, 349	[ <sup>237</sup> ]
5	PF6 <sup>−</sup>	$\overset{H_{V}GS}{\overset{h}{\underset{H_{V}GS}}} \overset{S}{\underset{H_{V}GS}} \overset{S}{H_$	Li	l M LiPF₀ in EC/DEC	3.56	72%, 30, 0.2 C	196, 414	[238]
6	PF6 <sup>-</sup>	tyt,	Li	1 M LiPF6 in EC/DEC	3.55	95%, 200, 2 C	103, 269	[239]
	$\mathrm{Li}^+,\mathrm{PF6}^-$	PTMA	Li	1 M LiPF6 in EC /DMC/DEC (w/w/w 1:1:1)	3.0	55%, 20 000, 100 mA g <sup>-1</sup>	100, 269	[279]
7	$\mathrm{PF_6}^-$	to	Li	1 M LiPF6 in EC/DEC	3.7	80%, 1 000, 10 C	85, 242	[ <sup>240</sup> ]
8	ClO <sub>4</sub> -		Li	5 M LiClO4 in EC/DMC	4.1	N/A	80, 256	[ <sup>241</sup> ]
9	$\mathrm{PF}_{6}^{-}$		Li	1 M LiPF <sub>6</sub> in EC/DMC (v/v 1:1)	3.6	95%, 500, 2 000 mA g <sup>-1</sup>	98, 263	[ <sup>242</sup> ]
10	ClO4-	Ph-HN CO <sub>2</sub> Li Li2DAnT	Li	1 M LiClO4 in PC	3.2	87%, 100, 3.7 mA g <sup>-1</sup> (carbon free)	180, 376	[ <sup>245</sup> ]
11	PF6 <sup>-</sup>	s s p VMPT	Li	1 M LiPF6 in EC:DMC (1: 1 v/v)	3.5	93%, 10000, 10 C	50, 149	[ <sup>280</sup> ]
12	Li*	P-BQ	Li	1 M LiTFSI in DOL/DME	2.7	32%, 20, 50 mA g <sup>-1</sup>	429, 1004	[ <sup>246</sup> ]
13	Li <sup>+</sup>	H <sub>3</sub> CO DMBQ	Li	1 M LiClO4 in γ- butyl lactone	2.7	82%, 10, 20 mA g <sup>-1</sup>	320, 798	[270]

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#### Table 2. continued

#	Cell configuration (ionic carriers)	Positive electrode (or "cathode") active material	Negative electrode (or "anode")	Electrolyte	Output voltage (V)	Cycling stability: retention, cycles, rate or current density	Specific capacity (mAh g <sup>-1</sup> ) and Specific energy (Wh kg <sup>-1</sup> ) <sup>o</sup> per mass of active material, Final coulombic efficiency, Loading (mg cm <sup>-2</sup> )	Ref.
14	Li <sup>+</sup>	F <sub>3</sub> C CF <sub>3</sub> CF <sub>3</sub> -BQ	Li	1 M LiPF6 in EC/DEC (v/v 3:7)	3.0	37%, 20, 0.1 mA	162, 466	[ <sup>250</sup> ]
15	Li <sup>+</sup>	C <sub>4</sub> F <sub>9</sub> C <sub>4</sub> F <sub>9</sub> Rf4-BQ	Li	1 M LiPF6 in EC/DEC (v/v 3:7)	3.0	50%, 20, 0.1 mA	115, 335	[ <sup>250</sup> ]
16	Li <sup>+</sup>	C <sub>6</sub> F <sub>13</sub> Cl Cl Cl Cl Cl Cl Cl Cl Cl Cl Cl Cl Cl	Li	1 M LiPF6 in EC/DEC (v/v 3:7)	3.1	55%, 20, 0.1 mA	177, 525	[ <sup>250</sup> ]
17	Li*	$ \begin{bmatrix} 0 & \downarrow & 0 \\ 0 & \downarrow & \downarrow & 0 \\ 0 & 0 & \downarrow & \downarrow \\ 0 & 0 & \downarrow & 1 \end{bmatrix}^{2^{+}}_{Mg} \overset{2^{+}}{\overset{2^{+}}} \\ Mg(\text{Li}_2) \cdot p \cdot \text{DHT} $	Li	1 M LiPF <sub>6</sub> in EC/DMC (w/w 1:1)	3.4	92%, 80, 23 mA g <sup>-1</sup>	100, 340	[252]
18	Li*	BBQ	Li	2.75 M LiTFSI in G4	2.8	67%, 20, 40 mA g <sup>-1</sup>	358, 917	[ <sup>247</sup> ]
19	Li*	PADQ	Li	1 M LiPF6 in DMC/EMC/EC (v/v/v 1:1:1)	2.77	N/A	370, 935	[ <sup>248</sup> ]
20	Li*		Li	PMA/PEG-based gel polymer electrolyte with LiClO4/DMSO loading	2.6	90%, 100, 0.2 C	422, 989	[272]
21	Li*	PSQ	Li	PMA/PEG- LiClO4-SiO2 composite	2.6	89%, 50, 0.2 C	409, 964	[273]
22	Li*	+↓↓↓s+, PBQS	Li	1 M LiTFSI in DOL/DME (v/v 1:1)	2.7	86%, 1 000, 5000 mA g <sup>-1</sup>	275, 691	[ <sup>246</sup> ]
23	Li <sup>+</sup>	OH H	Li	1 M LiPF6/EC/DMC (v/v 1/1)	2.0	53%, 100, 15 mA g <sup>-1</sup>	250, 470	[ <sup>274</sup> ]
24	Li*	HO PDBS	Li	1 M LiTFSI in DOL/DME (v/v 1:1)	2.5	50%, 20, 50 mA g <sup>-1</sup>	200, 475	[ <sup>249</sup> ]
25	Li*	OLi Lio Lio LioPDBS	Li	1 M LiTFSI in DOL/DME (v/v 1:1)	2.0	87%, 1 500, 500 mA g <sup>-1</sup>	247, 464	[ <sup>249</sup> ]

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#### Table 2. continued

#	Cell configuration (ionic carriers)	Positive electrode (or "cathode") active material	Negative electrode (or "anode")	Electrolyte	Output voltage (V)	Cycling stability: retention, cycles, rate or current density	Specific capacity (mAh g <sup>-1</sup> ) and Specific energy (Wh kg <sup>-1</sup> ) <sup>a</sup> per mass of active material, Final coulombic efficiency, Loading (mg cm <sup>-2</sup> )	Ref.
26	Li*		Li	1 M LiTFSI in DME:DOL (v/v 1:2)	2.5	91%, 100, 0.2 C	223, 527	[287]
27	Li <sup>+</sup>	Cli Clawsone-Li	Li	1 M LiTFSI in DME:DOL (v/v 1:2)	2.4	98%, 1 000, 0.5 C	280, 627	[ <sup>271</sup> ]
28	Li*	N V V V V V V V V V V V V V V V V V V V	Li	1 M LiPF6 in EC/DMC (w/w 1:1)	2.71	80%, 20, 0.1 C	207, 532	[258]
29	Li <sup>+</sup>		Li	1 M LiTFSI in DOL + DME (v/v 2:1)	2.1	98%, 100, 0.2 C	263, 517	[275]
30	Li*	S O OLI	Li	1 M LiTFSI in DOL/DME ( v:v 2:1)	2.5	60%, 1 200, 2 C	330, 760	[ <sup>276</sup> ]
31	Li*	HN HN HN HN DAAQ-TFP	Li	1 M LiTFSI in TEGDME	2.4	98%, 1 800, 500 mA g <sup>-1</sup>	107, 250	[283]
32	Li <sup>+</sup>		Li	1 M LiClO4 in DOL/DME (v/v 1:1)	2.5	96%, 250, 0.1 C	200, 475	[288]
33	Li <sup>+</sup>		Li	1 M Li[Tf₂N] in [EMIm][Tf₂N] and 1 M LiClO₄ EC/DEC	2.8	78%, 100, 0.2 C	260, 682	[254]
34	Li <sup>+</sup>	NC CN F F NC F F-TCNQ	Li	1 M LiPF6 in EC/DEC	3.1	N/A	183, 542	[255]
35	Li*	NC_CN F_F F_F NC_CN F2-TCNQ	Li	1 M LiPF6 in EC/DEC	3.15	N/A	110, 342	[255]
36	Li*	N 1,8-PhenQ	Li	1 M LiPF6 EC/EMC (v/v 1:3)	2.94	NA	230, 638	[256]

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#### Table 2. continued

#	Cell configuration (ionic carriers)	Positive electrode (or "cathode") active material	Negative electrode (or "anode")	Electrolyte	Output voltage (V)	Cycling stability: retention, cycles, rate or current density	Specific capacity (mAh g <sup>-1</sup> ) and Specific energy (Wh kg <sup>-1</sup> ) <sup>a</sup> per mass of active material, Final coulombic efficiency, Loading (mg cm <sup>-2</sup> )	Ref.
37	Li <sup>+</sup>	4,5-PhenQ	Li	1 M LiPF6 in EC/DMC (w/w 1:1)	2.74	N/A	231, 597	[257]
38	Li*	Lio Liooc LieocDHT	Li	1 M LiPF6 in EC/DMC (v/v 1:1)	2.85	95%, 30, 0.2–5 C	105, 299	[ <sup>234</sup> ]
39	Li*	PTO PTO	Li	1 M LiPF₀ in EC–DMC	2.59	27%, 50, N/A	360, 853	[257]
40	Li <sup>+</sup>	HN HN Polydopamine	Li	1 M LiPF6 in EC:DMC (v/v 3:7)	2.5	106%, 10 000, 0.1 A g <sup>-1</sup>	108, 263	[105]
41	$\mathrm{Li}^{*}$	LiOOCCOOLi Li terephthalate	Li	1 M LiPF <sub>6</sub> in EC/DMC (w/w 1:1)	0.8	78%, 50, 0.1 C	300, N/A	[ <sup>261</sup> ]
42	$\mathrm{Li}^*$		Li	1 M LiPF6 in EC/DMC (v/v 1:1)	0.7	60%, 25, 1 C	250, N/A	[ <sup>264</sup> ]
43	$\mathrm{Li}^{*}$	Lio 4.4- tolane-dicarboxylate	Li	1 M LiPF6 in EC/DMC (v/v 1:1)	0.65	90%, 50, 0.025 C	130, N/A	[ <sup>265</sup> ]
44	Li <sup>+</sup>	$\begin{array}{c} \overset{*_{h} S \cdot S}{\longrightarrow} & \overset{*}{\rightarrow} *$	Li	0.38 M LiTFSI, 0.31 M LiNO3 in DOL/DME	2.1	82%, 100, 167 mA g <sup>-1</sup> , 0,1 C	1000, 1668	[ <sup>266</sup> ]
45	Li <sup>+</sup>	$ \begin{array}{c} & & \\ & & \\ & & \\ & & \\ & & \\ & & \\ & & \\ & & \\ & $	Li	l M LiPF₀ in EC/DEC	1.8	73%, 1 000, 0.4 C	1200, 1648	[ <sup>268</sup> ]
46	Li*		Li	1 M LiPF6 in EC/DEC	2.1	N/A	580, 1059	[82]
47	Li <sup>+</sup>		Li	0.3 M LiTFSI- [PY13][TFSI] at 70°C	1.7	82%, 100, 50 mA g <sup>-1</sup>	902, 1243	[ <sup>269</sup> ]
48	Li*	$ \begin{array}{c}                                     $	Li	1.0 M LiTFSI in DOL/DME	2.0	70%, 10 000, 20 C	395, 717	[277]
49	Li*	$\begin{array}{c} CN \\ NC + N \\ N + N + CN \\ NC + N \\ NC \\ CN \\ 6CN \end{array}$	Li	1 M LiClO4 in EC/DEC (v/v 1:1)	2.4	83%, 30, 0.2 C	300, 668	[ <sup>278</sup> ]

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#### Table 2. continued

#	Cell configuration (ionic carriers)	Positive electrode (or "cathode") active material	Negative electrode (or "anode")	Electrolyte	Output voltage (V)	Cycling stability: retention, cycles, rate or current density	Specific capacity (mAh g <sup>-1</sup> ) and Specific energy (Wh kg <sup>-1</sup> ) <sup>6</sup> per mass of active material, Final coulombic efficiency, Loading (mg cm <sup>-2</sup> )	Ref.
50	Li*	$C_{0}H_{11}$ $C_{0}H_{1}$ $C_{0}H_{1}$ $C_{0}H_{1}$ $C_{0}H_{1}$ $C_{0}H_{1}$ $C_{0}H_{1}$ $C_{0}H_{1}$ $P(NDI2OD-T2)$	Li	l M LiClO4 in DOL/DME (v/v 1:1)	2.4	96%, 3 000, 10 C	54, 128	[ <sup>281</sup> ]
51	$\mathrm{Li}^{+}$	+N PPDIE	Li	4 M LiFSI-DME	2.0	82%, 10 000, 10 C	180, 344	[ <sup>282</sup> ]
52	$\mathrm{Li}^+$	PDI-Tc	Li	1 M LiPF₀ in EC/DME (v/v 1:1)	2.4	80%, 500, 2 C	76, 179	[ <sup>284</sup> ]
53	Li <sup>+</sup>		Li	1 M LiTFSI and 0.2 M LiNO3 in DOL/DME (v/v 1:1)	2.5	60%, 300, 10 C	146, 352	[ <sup>285</sup> ]
54	$\mathrm{Li}^{*}$	ноос-	Li	1 M LiPF₅ in EC:DEC (v/v 1:1)	2.4	88%, 200, 5 C	90, 211	[ <sup>286</sup> ]
55	$\mathrm{Li}^+$	PBALS	Li	7 M LiTFSI in DME:DOL (v/v 1:1)	1.4	85%, 500, 10 C	95, N/A	[ <sup>289</sup> ]

<sup>a</sup>Specific energy considers the weight of both the cathode and anode materials. For p-type OEMs, LiBF<sub>4</sub> is considered as the Li salt due to its relatively light weight.

1511 show some of the highest discharge potentials for n-type 1512 polymer OEMs (Figure 10D, Table 2, entry 22, 23).<sup>246,249</sup> 1513 Since the discharge potentials of *p*-BQ-containing OEMs are

1514 noticeably lower than those of p-type OEMs as well as 1515 common intercalation compounds (>3.5 V vs Li<sup>+</sup>/Li), efforts 1516 have been made to obtain higher potentials. Installation of 1517 perfluoroalkyl groups and chlorine atoms at the carbon ring 1518 of p-BQ gives rise to CF<sub>3</sub>-BQ (Table 2, entry 14), Rf4-BQ 1519 (Table 2, entry 15), and Rf6-Cl-BO (Table 2, entry 16), which 1520 show increased potentials of 3.0-3.1 V vs Li<sup>+</sup>/Li.<sup>250</sup> The 1521 introduction of these auxiliary groups, however, inevitably 1522 decreases the specific capacity and could be counterproductive 1523 when high specific energy is the goal. Dilithium (2,5-dilithium-1524 oxy)-terephthalate (Li<sub>2</sub>(Li<sub>2</sub>)-p-DHT or Li<sub>4</sub>-p-DHT) may be 1525 seen as a carboxylate-substituted p-BQ (crystallized "host" 1526 electrode material) synthesized at its discharged (lithiated) 1527 state;<sup>208,251</sup> with its polyanionic structure making this material 1528 highly insoluble.<sup>84</sup> Since its life as an OEM starts from charging, 1529 like commercial positive electrode materials in LIBs do, it is one 1530 of the few n-type OEMs that can be paired with a Li-free anode, 1531 a great benefit for industrial cell production. However, this very 1532 interesting organic was hampered by a relatively low operating 1533 potential (2.55 V vs Li<sup>+</sup>/Li). Replacing the Li<sup>+</sup> in the carboxylate 1534 groups with high-electronegativity cations such as Mg<sup>2+</sup> and 1535 Ca<sup>2+</sup> amazingly increases the redox potential several hundreds 1536 of millivolts (Figure 10E).<sup>252</sup> Thus the resulting magnesium

(2,5-dilithium-oxy)-terephthalate (Mg(Li<sub>2</sub>)-*p*-DHT) shows the 1537 highest working potential (3.45 V vs Li<sup>+</sup>/Li) among n-type 1538 OEMs approaching the well-known LiFePO<sub>4</sub> electrode ma- 1539 terial (Table 2, entry 17). Note that an attempt to switch from 1540 the carboxylate functional groups present in Li<sub>4</sub>-*p*-DHT to the 1541 sulfonate substituent giving rise to the tetralithium salt of 2,5- 1542 dihydroxy-1,4-benzenedisulfonate (Li<sub>4</sub>-*p*-DHBDS)<sup>253</sup> enables 1543 also a voltage gain (+650 mV) but with inferior electrochemical 1544 performance upon cycling. 1545

A closely related structure to *p*-BQ is tetracyanoquinodi- 1546 methane (TCNQ), where the oxygen atoms in *p*-BQ are 1547 replaced by the even more electron-withdrawing dicyano- 1548 methylene groups (Table 2, entry 33). TCNQ itself is known 1549 as an electron acceptor for preparation of charge transfer salts, 1550 such as TTF-TCNQ. In a Li-battery, TCNQ discharges at 1551 2.9 V vs Li<sup>+</sup>/Li, a noticeable improvement over *p*-BQ.<sup>254</sup> Further 1552 increase in potential was achieved by installing electron- 1553 withdrawing groups to the carbon ring. As the number of 1554 fluorine atoms installed to TCNQ increased from two (F-TCNQ) 1555 to four (F2-TCNQ), the average discharge potential increased 1556 from 3.1 to 3.15 V vs Li<sup>+</sup>/Li (Figure 10F, Table 2, entry 34, 35).<sup>255</sup> 1557

The *ortho*-regioisomer of *p*-BQ gives rise to higher discharge 1558 potentials in general. The simplest molecule, *ortho*-benzoqui- 1559 none (*o*-BQ), has not been directly studied probably due 1560 to chemical stability issues, but *o*-BQ as a building block for 1561 OEMs is well documented. The pyridine rings-fused 1,8-diaza- 1562

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в С 4.5 5 Pentakis-fused TTF Voltage (V vs. Li/Li<sup>+</sup>) DD 4.0 3 /oltage (V vs. Li/Li+) 1.0 mA/cm 1e<sup>.</sup> 2 0.1 mA/cm Voltage [V] 8 3.5 3 3.0 charaind 2 2.5 4 200 150 100 50 20 10 **DD-TCNQ** 05 3 2.0 PTMA 3e 2 150 250 n 0 50 100 200 0.0 0.5 1.0 15 20 25 30 80 100 140 160 0 20 40 60 120 Capacity (mAh/g) e- transferred in formula unit C h/g] E 4.5 F Discharge Charge 1 TCNQ 4.0 Discharge Charge 4.0 2 Me-TCNQ Potential (V) vs. Li<sup>+</sup>/Li Voltage / V vs Li⁺/Li 3. 3 F-TCNO 3.5 vs. Li/Li<sup>+</sup>/ V 4 F2-TCNQ 3.0 3.0 21 2.5 2. BQ:KB:PTFE=3:6:1 2.0 Ma(Lia)-p-DHT PBQS:KB:PTFE=6:3:1 Li<sub>2</sub>(Li<sub>2</sub>)-p-DHT 1.5 \_ 2 100 150 200 250 300 350 450 0 400 -1 200 Specific Capacity / mAh g d*Q*/d*E* (a.u.) Capacity/A h kg **G** 3.5 Potential (V) vs. Li<sup>\*</sup>/Li<sup>0</sup> **H** - Phenanthragulnone 3.5 DISCHARGE CHARGE - 1,8-PhenQ Voltage / V vs. Li/Li\* 3.25 234 mA 4.5-PhenQ Ш 0 2.75 2.5 Li -o-DHT 2.25 -Li<sub>4</sub>-p-DHT 0. 2.0-Li terephthalate 250 100 200 -15 15 0 50 150 -10 -5 0 5 10 20 Capacity / mAh g<sup>-1</sup> dQ/dE (a.u.) x in Lis . . C+H2O2

Figure 10. Voltage profiles of selected high-potential positive OEMs and low-potential negative OEMs measured vs Li including (A) pentakis-fused TTF (reproduced with permission from ref 238. Copyright 2014 The Royal Society of Chemistry), (B) PTMA (reproduced with permission from ref 75. Copyright 2002 Elsevier Ltd.), (C) DD (reproduced with permission from ref 241. Copyright 2019 Elsevier Ltd.), (D) BQ and PBQS (reproduced with permission from ref 246. Copyright 2015 John Wiley & Sons, Inc.), (E) Li<sub>2</sub>(Li<sub>2</sub>)-p-DHT and Mg(Li<sub>2</sub>)-p-DHT (reproduced from ref 252), (F) TCNQ, F-TCNQ, and F2-TCNQ (reproduced with permission from ref 255. Copyright 2013 John Wiley & Sons, Inc.), (G) 1,8-PhenQ and 4,5-PhenQ (reproduced with permission from ref 257. Copyright 2013 The Royal Society of Chemistry, (H) Li4-0-DHT (reproduced with permission from ref 234. Copyright 2014 American Chemical Society), and (I) Li terephthalate (reproduced with permission from ref 261. Copyright 2009 Nature Publishing group).

1563 9,10-phenanthrenequinone (1,8-PhenQ, Table 2, entry 36) 1564 and 4,5-diaza-9,10-phenanthrenequinone (4,5-PhenQ, Table 2, entry 37) discharge at 2.94 and 2.74 V vs Li<sup>+</sup>/Li (Figure 10G), 1565 respectively, both higher than the 2.71 V for their p-BQ-1566 containing isomer pyrido[3,4-g]isoquinoline-5,10-dione (PID).<sup>256–258</sup> Interestingly, the position of nitrogen atoms in 1567 1568 1569 the fusing pyridine rings has a considerable impact on discharge potential: the pyridine nitrogen and the carbonyl oxygen being 1570 adjacent (as in the case of 1,8-PhenQ) promote favorable 1571 coordination of Li<sup>+</sup>, which leads to extra gain in potential. This 1572 explains the noticeably higher potential of 1,8-PhenQ than that 1573 of 4,5-PhenQ (+200 mV as gain). As previously attempted with 1574 p-DHT redox-active ligand, attaching carboxylate functional 1575 1576 groups to the carbon ring of the reduced form of o-BQ gives rise 1577 to another highly insoluble and lithiated electrode material 1578 namely (2,3-dilithium-oxy)-terephthalate (Li<sub>4</sub>-o-DHT, Table 2, 1579 entry 38), which can be prepared from biomass too.<sup>234</sup> Alike 1580 Li<sub>4</sub>-p-DHT, this regioisomer is able to release/uptake Li ions 1581 over dozens of cycles but at higher operating potential (2.85 V 1582 vs Li<sup>+</sup>/Li) due to specific electronic effects<sup>211</sup> occurring in 1583 orthoquinones (Figure 10H). Since only one out of the two 1584 lithoxy groups in the carbon ring appears redox active, it may 1585 be reasonable to assume that upon possible full utilization, an 1586 even higher average potential could be achieved.

N-type OEMs with sufficiently low operating potential 1587 can be used as negative electrode materials as well. Many 1588 conductive polymers can be n-doped at <1 V vs Li<sup>+</sup>/Li, but the 1589 doped states usually lack stability, and the doping level is 1590 typically half of that for the p-doping of the same polymer.<sup>259</sup> 1591 Two other mechanisms are currently being actively researched: 1592 lithiation of  $\pi$ -conjugated carboxylate and "superlithiation" 1593 (see section 7.3) of  $\pi$ -conjugated systems.<sup>260</sup> A pioneering 1594 report on carboxylate negative electrodes concerned dilithium 1595 terephthalate<sup>261</sup> which discharged at 0.8 V vs Li<sup>+</sup>/Li (Figure 10I, 1596 Table 2, entry 41). [Note: For a negative electrode material 1597 tested in a Li cell, the charging potential is more relevant, 1598 however, discharging potential is used here for consistency.] 1599 Since this work, the family of  $\pi$ -conjugated carboxylates has 1600 been widely extended, and it has been shown that the working 1601 potential can be slightly adjusted by playing with the electronic 1602 effects on the organic skeleton notably by Lakraychi et al.<sup>262,263</sup> 1603 Replacing the phenyl group in dilithium terephthalate with 1604 biphenyl gives the dilithium 4,4'-biphenyl dicarboxylate 1605 (Li<sub>2</sub>BPDC, Table 2, entry 42) with a discharge potential of  $_{1606}$  0.7 V vs Li<sup>+</sup>/Li.<sup>264</sup> The lower potential compared with Li  $_{1607}$ terephthalate was ascribed to the  $\pi$ -conjugation enhancement 1608 destabilizing the LUMO orbitals of the molecule. Further 1609 expansion of the  $\pi$ -conjugated system to diphenylacetylene 1610

Review

A

(mA h g<sup>-1</sup>) 800

D

Voltage (V)

G

Voltage (V vs Li/Li<sup>+</sup>)

4.0

2.5

2.0

1.5

1,200

1 000

600 Capacity

400

200

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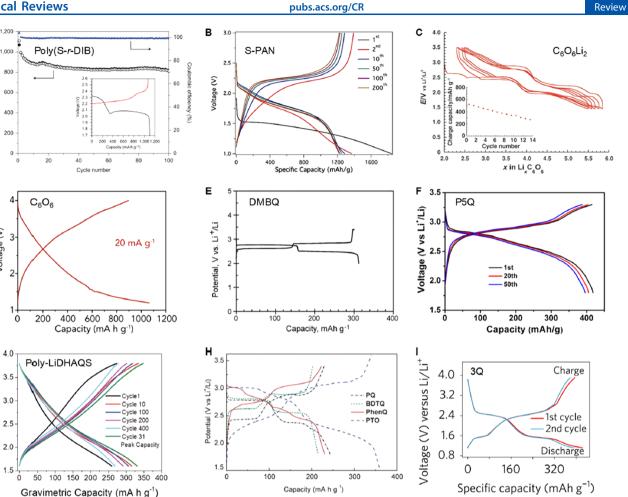


Figure 11. Voltage profiles of selected high-capacity OEMs measured vs Li including (A) poly(S-r-DIB) (reproduced with permission from ref 266. Copyright 2013 Nature Publishing group), (B) S-PAN (reproduced with permission from ref 268. Copyright 2015 American Chemical Society), (C)  $Li_2C_6O_6$  (reproduced with permission from ref 82. Copyright 2008 John Wiley & Sons, Inc.), (D)  $C_6O_6$  (reproduced with permission from ref 269. Copyright 2019 John Wiley & Sons, Inc.), (E) DMBQ (reproduced with permission from ref 270. Copyright 2010 Elsevier Ltd.), (F) PSQ (reproduced with permission from ref 273. Copyright 2014 American Chemical Society), (G) poly-LiDHAQS (reproduced with permission from ref 276. Copyright 2017 John Wiley & Sons, Inc.), (H) PTO (reproduced from ref 257. Copyright 2013 The Royal Society of Chemistry), and (I) 3Q (reproduced with permission from ref 277. Copyright 2013 Nature Publishing group).

1611 results in dilithium 4,4'-tolane-dicarboxylate, which discharges 1612 at an even lower potential of 0.65 V vs Li<sup>+</sup>/Li (Table 2, entry 1613 43).<sup>265</sup> OEMs that undergo the peculiar "superlithiation" 1614 process (see section 7.3) exhibit sloping discharge profiles that 1615 start from >1.5 V and eventually approach 0 V vs Li<sup>+</sup>/Li and 1616 then charge at  $\geq 1$  V vs Li<sup>+</sup>/Li on average. Due to the unique-1617 ness of the reaction, these OEMs are to be separately covered 1618 in section 7.

#### 5.2. Organic Electrode Materials with High Specific 1619 Capacity

1620 To gain high specific capacity, both formula weight and 1621 number of transferrable electrons are key considerations. 1622 Among the major classes of organic electrodes, organosulfur 1623 compounds offer the largest capacities. In particular, organo-1624 sulfur polymers bearing polysulfide bonds not only exhibit high 1625 capacities but also stable cycling. Poly(sulfur-random-1,3-1626 diisopropenylbenzene) (poly(S-r-DIB)) is one such example, 1627 which was copolymerized between molten S<sub>8</sub> and 1,3-diisopro-1628 penylbenzene (DIB) through inverse vulcanization.<sup>266</sup> The 1629 DIB feed ratios can be varied between 10-50 wt % during the 1630 synthesis. Galvanostatic voltage profiles of poly(S-r-DIB) with 1631 10 wt % DIB show distinct discharge plateaus at 2.3 and 2.1 V

vs Li<sup>+</sup>/Li (Figure 11A, Table 2, entry 44). The initial discharge 1632 capacity is 1100 mAh g<sup>-1</sup>. Sulfur-polyacrylonitrile (S-PAN) is 1633 another organosulfur polymer attracting significant attention 1634 due to the ease of synthesis and high performance.<sup>267</sup> S-PAN 1635 was formed by mixing and heating sulfur and polyacrylonitrile 1636 (PAN). It is interesting to note that S-PAN exhibits good 1637 capacity retention in a carbonate-based electrolyte, a behavior 1638 in sharp contrast with sulfur, which works well only in ethereal 1639 electrolytes.<sup>268</sup> S-PAN shows a single plateau at 2.1 V with a 1640 high specific capacity of 1200 mAh  $g^{-1}$  (Figure 11B, Table 2, 1641 entry 45). 1642

Carbonyl group undergoes reversible one-electron reduction 1643 to form a radical anion. When multiple carbonyls are con- 1644 jugatedly connected as in quinones, the uncoupled electrons 1645 generated during reduction could combine intramolecularly to 1646 form multivalent anions. The theoretical capacity of carbonyl- 1647 based electrodes is typically lower than that of organosulfur 1648 polymers. Dilithium rhodizonate (Li<sub>2</sub>C<sub>6</sub>O<sub>6</sub>) undergoes rever- 1649 sible four-electron reaction per  $C_6O_6$  ring (Table 2, entry 46). 1650 The observed initial discharge capacity of 580 mAh  $g^{-1}$  set the 1651 record capacity among carbonyl-based OEMs since its 1652 discovery in 2008 (Figure 11C).<sup>82</sup> The fact that  $Li_6C_6O_6$  can 1653 be prepared from a renewable natural precursor opens up new 1654

1655 pathways toward sustainable batteries for future clean energy 1656 economy. Recently, cyclohexanehexone ( $C_6O_6$ ) was claimed to 1657 be successively synthesized and surpass  $\text{Li}_2C_6O_6$  in terms of 1658 specific capacity (Table 2, entry 47).<sup>269</sup>  $C_6O_6$ , a cyclic ketone 1659 composed of carbonyls without redundant mass, exhibits a 1660 higher capacity of 902 mAh g<sup>-1</sup> (i.e., six-electron reaction per 1661 formula) (Figure 11D). Note that such an ultrahigh capacity 1662 was observed in an ionic liquid-based electrolyte measured at 1663 70 °C. The compound exhibits sloping and polarized cycling 1664 curves, in contrast to the multiple plateaus observed for 1665  $\text{Li}_2C_6O_6$ .<sup>82</sup>

After the C<sub>6</sub>O<sub>6</sub> motif, p-BQ offers the highest theoretical 1666 1667 specific capacity among common n-type OEM building blocks. 1668 p-BQ itself can deliver a specific capacity of 429 mAh g<sup>-1</sup> 1669 during the initial discharge, but the capacity retention was only 1670 32% after 20 cycles due to its high solubility in organic 1671 solvents.<sup>246</sup> Due to the ready dissolution of *p*-BQ into non-1672 aqueous electrolyte solutions, many OEMs containing the 1673 p-BQ unit have been developed to reduce dissolution while 1674 maintaining high capacity. They may be categorized into three 1675 types according to their molecular sizes. The first type includes 1676 molecules with one single p-BQ core modified with electron 1677 donating or withdrawing groups. Installation of methoxy 1678 functional groups on p-BQ results as DMBQ, which improves 1679 the stability compared to p-BQ albeit the discharge capacity is <sup>1680</sup> reduced to 320 mAh g<sup>-1</sup> (Figure 11E, Table 2, entry 13).<sup>270</sup> <sup>1681</sup> Lawsone-Li is another example showing modification of 1682 naphthoquinone (NQ) with lithoxy results in lawsone-Li salt. 1683 Lawsone (2-hydroxy-1,4-naphthoquinone) is a nature-derived 1684 red-orange dye. Lithium cells based on lawsone-Li as positive 1685 electrode material displayed a capacity of 280 mAh g<sup>-1</sup> and a 1686 cycle life of 1000 cycles (Table 2, entry 27).<sup>271</sup>

1687 The second type includes molecules with multiple *p*-BQ 1688 units. 2,2'-Bis-*p*-benzoquinone (BBQ), calix[4]quinone (C4Q), 1689 and pillar[5]quinone (P5Q) contain two, four, and five *p*-BQ 1690 units, respectively (Table 2, entries 18, 20, and 21). It seems 1691 that dissolution of oligomers could still be observed in liquid 1692 electrolytes; therefore, polymer electrolytes containing poly-1693 (methacrylate) (PMA) and poly(ethylene glycol) (PEG) 1694 were used to increase capacity retention. Compared to BBQ 1695 (358 mAh g<sup>-1</sup>), P5Q and C4Q show higher specific capacity of 1696 409 and 422 mAh g<sup>-1</sup> (Figure 11F).<sup>247,272,273</sup>

1697 The third type includes polymers with (modified) *p*-BQ. 1698 units. PBQS, PDBS, and Li<sub>2</sub>PDBS present three examples of 1699 *p*-BQ-based polymers when using sulfur as the linker (Table 2, 1700 entry 22–25).<sup>246,249,274</sup> Among the three polymers, PBQS 1701 shows the highest specific capacity of 275 mAh g<sup>-1</sup> for 1000 1702 cycles. Due to the addition of lithoxy and hydroxy groups on 1703 PBQS, Li<sub>2</sub>PDHBQS and PDBS exhibit slightly lower specific 1704 capacity of ~250 mAh g<sup>-1</sup>. Anthraquinone (AQ) can be 1705 considered as *p*-BQ with extended conjugation, which also has 1706 the solubility issue. Polymerization approach has been equally 1707 successful for AQ. P14AQ and poly-LiDHAQS are two 1708 polymers based on AQ. The specific capacities are 263 and 1709 330 mAh g<sup>-1</sup>, respectively (Figure 11G, Table 2, entries 29 1710 and 30).<sup>275,276</sup>

1711 A closely related structure to *p*-BQ is pyrene-4,5,9,10-1712 tetraone (PTO) where two *o*-BQ units are connected with 1713 extended  $\pi$ -conjugated structure (Table 2, entry 39). PTO 1714 undergoes a four-electron reduction with a specific capacity of 1715 360 mAh g<sup>-1</sup> in EC/DMC and an average discharge voltage 1716 of 2.59 V vs Li<sup>+</sup>/Li (Figure 11H).<sup>257</sup> TCNQ can also be 1717 formed by replacing the oxygen atoms in *p*-BQ with more electron-withdrawing dicyanomethylene groups (Table 2, 1718 entry 33). The discharge capacity of TCNQ is lowered to 1719 260 mAh  $g^{-1}$  albeit voltage is increased to 3.2 V.<sup>254</sup> 1720

π-Conjugated heteroaromatic molecules represent another 1721 class of OEMs with high specific capacity. Fused quinoxaline 1722 building blocks afford multiple redox-active sites centered on 1723 N atoms. Hexaazatrinaphthylene (3Q) enables six-electron 1724 reduction with a specific capacity of 395 mAh g<sup>-1</sup> (Figure 11I, 1725 Table 2, entry 48).<sup>277</sup> When hybridized with graphene, 3Q 1726 shows 70% capacity retention after 10 000 cycles. Hexaaza- 1727 triphenylenehexacarbonitrile (6CN, Table 2, entry 49) shows 1728 higher redox voltage at 2.4 V vs Li<sup>+</sup>/Li by replacing the 1729 benzene groups in 3Q with electron-withdrawing cyanide 1730 groups.<sup>278</sup> When the discharge potential cutoff is set at 1.5 V vs 1731 Li<sup>+</sup>/Li, 6CN shows a specific capacity of 300 mAh g<sup>-1</sup>. 1732

#### 5.3. Organic Electrode Materials with Long Cycle Life

Researchers have almost always attributed the capacity 1733 decay of OEMs to either chemical degradation or dissolution. 1734 In typical nonaqueous Li electrolytes, chemical degradation of 1735 OEMs is rarely observed; hence, material dissolution from the 1736 solid electrode into the electrolyte is the main degradation 1737 mechanism. For the most part, increasing the cycling stability 1738 of OEMs in nonaqueous Li batteries equals minimizing the 1739 solubility of OEMs in electrolytes. As long as material disso- 1740 lution is effectively suppressed, apparently most OEMs can 1741 deliver stable cycling performance. Even small-molecule OEMs 1742 that readily decay due to dissolution can be made stable when 1743 a sufficiently large amount of high-surface-area carbon adsor- 1744 bent is included in the positive composite electrode as previ- 1745 ously underlined in section 1.2.<sup>13</sup> Due to practical consid- 1746 erations, cycling performances enabled by intricate adsorbents 1747 are not a priority for this review.

The most stable OEMs for nonaqueous Li batteries have 1749 been polymers. Polymer OEMs containing varying types of redox 1750 centers, from p-type to n-type, from nitroxides (e.g., PTMA)<sup>279</sup> to 1751 aromatic amines (e.g., poly(3-vinyl-N-methylphenothiazine) or 1752 PVMPT<sup>280</sup> to quinones (e.g., polydopamine)<sup>105</sup> to imides (e.g., 1753) poly{[N,N'-bis(2-octyldodecyl)-1,4,5,8-naphthalenedicarboxi- 1754 mide-2,6-diyl]-alt-5,5'-(2,2'-bithiophene)} or P(NDI2OD-T2), 1755 Table 2, entry 50 and poly(ethylene-pyromellitic diimide) or 1756 PPDIE, Table 2, entry 51),<sup>281,282</sup> have all been reported to 1757 cycle for thousands to tens of thousands of cycles. It may be 1758 reasonable to extrapolate that, with proper polymerization, 1759 OEMs of all types can be made stable, even though synthetic 1760 difficulty may vary from type to type. With judicious selection 1761 of polymerization strategies, two- and three-dimensional 1762 polymer OEMs have been synthesized based on aromatic 1763 amines (e.g., polytriphenylamine or PTPA),<sup>242</sup> quinones (e.g., 1764 2,6-diaminoanthraquinone-1,3,5-triformylphluroglucinol or 1765 DAAQ-TFP),<sup>283</sup> and imides (e.g., perylene diimide- 1766 triptycene or PDI-Tc, Table 2, entry 52).<sup>284</sup> These additional 1767 architectures are proposed to further improve cycling stability. 1768

The advantage of polymer OEMs in cyclability does not 1769 preclude molecular OEMs from being important. Molecular 1770 materials can still be preferred for their well-defined structures, 1771 high specific capacity, flexibility in processing, and so on. 1772 Therefore, approaches to improve the cyclability of small 1773 molecules are still being developed. Considering the success of 1774 polymer OEMs, a widely practiced strategy is to increase the 1775 molecular weight of molecules or simply oligomerization. Both 1776 3Q and coronene are big planar molecules which benefit from 1777 relatively strong van de Waals interaction and effective  $\pi$ – $\pi$  1778

1844

1779 stacking.<sup>235,277</sup> Even when the active cores are not as big, it is 1780 still convenient to connect multiple building blocks together 1781 to artificially increase the molecular weight. Some examples 1782 include a triangle molecule (–)-NDI- $\Delta^{285}$  (Table 2, entry 53) 1783 which incorporates three naphthalenediimide (NDI) units plus 1784 linkers, benzoic-PDI<sup>286</sup> (Table 2, entry 54) which attaches 1785 more aryls to the already large molecule perylenediimide (PDI), and 2,3,5,6-tetraphthalimido-1,4-benzoquinone 1786  $(TPB)^{287}$  which incorporates two seemingly unrelated redox 1787 1788 centers (tetraphthalimide and *p*-BQ) into one molecule. These 1789 molecules exhibit cycling stabilities that clearly set them apart 1790 from simple molecules without sacrificing most advantages of 1791 molecular OEMs. The large size of these molecules is blurring 1792 the boundary between molecules and polymers. In fact, some "polymer" OEMs such as poly(benzo[1,2-b:4,5-b']-1793 1794 dithiophene-4,8-dione-2,6-diyl) (PBDTD)<sup>288</sup> contain few 1795 repeating units (e.g.,  $\leq 5$ ) per polymer chain. They may as 1796 well be considered as molecular OEMs.

Other strategies for stabilizing molecular OEMs include salt 1797 1798 formation and grafting as previously mentioned.<sup>84</sup> Salt 1799 formation has long been an established strategy to stabilize 1800 molecular OEMs: ionic groups introduced to OEMs increase 1801 their intermolecular interactions and decrease the similarity 1802 in polarity with nonaqueous electrolytes, thus decreasing <sup>32</sup> Some recent excellent examples include Mg(Li<sub>2</sub>)-<sup>1803</sup> solubility.<sup>82</sup> Some recent excellent examples include Mg(Li<sub>2</sub>)-<sup>1804</sup> *p*-DHT,<sup>252</sup> lawsone-Li,<sup>271</sup> and 4-(phenylazo) benzoic acid 1805 lithium salt (PBALS, Table 2, entry 55)<sup>289</sup>; all show barely any 1806 capacity decay after hundreds of cycles. Grafting is also a 1807 known, if still exotic, method for enabling small-molecule 1808 OEMs. The key to successful grafting is rational functionaliza-1809 tion of high-capacity OEM building blocks for covalent linking 1810 to high-surface-area substrates. Grafted naphthoquinone (n-type) 1811 and pyrene (p-type) derivatives can show no obvious capacity 1812 decay over a long cycling period.<sup>290–29</sup>

1813 We would like to note that although the cycle numbers for 1814 the examples discussed above vary from hundreds to tens of 1815 thousands, these numbers, in a lot of cases, seem to be limited 1816 by how fast the researchers felt comfortable to cycle their 1817 cells instead of the actual stability of the OEMs. Figure 12

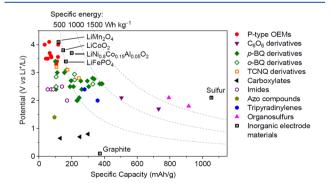


Figure 12. Comparison of the discharge potentials and specific capacities of state-of-the-art OEMs and inorganic electrode materials for Li batteries. Specific capacity calculation considers the weight of the lithiated form of positive electrode materials and delithiated form of negative electrode materials (e.g., azo compounds, carboxylates, and graphite). The highest observed reversible capacities are used instead of theoretical values.

1818 summarizes the discharge potentials and active material-level 1819 specific capacities of Li-organic batteries discussed in this 1820 section and compares them with those of state-of-the-art inorganic electrode materials. Note that the specific capacities of 1821 batteries with p-type OEMs are impacted by the weight of the Li 1822 salt in the electrolyte (dual-ion cell configuration, Figure 9b-3). 1823

For comparison convenience, the calculation of all batteries 1824 with p-type OEMs considers LiBF<sub>4</sub> as the Li salt. Although 1825 p-type OEMs have comparable discharge potentials and 1826 specific capacities as those of inorganic electrode materials, 1827 batteries based on them fall short in specific energy where the 1828 weight of the electrolyte is included. Therefore, p-type OEMs 1829 are not yet contenders as high-energy battery cathode materials 1830 but may find applications in, for example, fast charging devices 1831 and wearables. Many quinone-based OEMs have surpassed 1832 inorganic electrode materials in terms of specific energy at the 1833 active material level (i.e., only the weight of active materials is 1834 included in calculation). In practice, however, most high- 1835 energy OEMs still require too much conductive agents in their 1836 electrode composites for decent performance, which decreases 1837 specific energies at the cell level. Another challenge for OEMs 1838 is to simultaneously achieve high specific energy and high 1839 cycling stability. Future development of OEMs for nonaqueous 1840 Li batteries demands deeper understandings of their electron 1841 and ion conduction mechanics as well as performance degra- 1842 dation mechanisms and strategies to address them. 1843

# 6. PERFORMANCES OF NONAQUEOUS SODIUM-ORGANIC BATTERIES

For decades, nonaqueous organic sodium-ion batteries have 1845 been overshadowed by other electrochemical energy systems 1846 (such as inorganic lithium-ion batteries, inorganic sodium-ion 1847 batteries, and later organic lithium-ion batteries) and have only 1848 been sporadically investigated.<sup>293</sup> However, in 2012, three 1849 different groups published their works on disodium tereph- 1850 thalate within a time frame of four months, marking then the 1851 beginning of the recent boom in this field.<sup>294–296</sup> Since then, 1852 disodium terephthalate has been regularly investigated as a 1853 model compound for composite electrode formulation.<sup>297-301</sup> 1854 In parallel, many other new materials were reported in the 1855 literature as already exhaustively covered in recent reviews. 16,40,41,302 1856 Considering that strategies known to affect the potential with 1857 inductive effects (electron-withdrawing/donating groups) or 1858 appropriate aromatic ring design will have similar effects in 1859 organic LIBs and SIBs, the only distinctions to keep in mind 1860 are the differences in electrochemical potential for the refer- 1861 ence metal (-3.04 V vs SHE for the Li<sup>+</sup>/Li redox couple 1862 against -2.71 V vs SHE for the Na<sup>+</sup>/Na redox couple) and 1863 atomic differences. For instance, a sodium carboxylate is expected 1864 to insert a sodium ion at an average potential slightly lower than 1865 the potential of lithium ion insertion for the corresponding 1866 lithium carboxylate with the same aromatic system -0.33 V (e.g., 1867 0.9 V vs Li<sup>+</sup>/Li average redox potential for dilithium terephthalate 1868 and 0.4 V vs Na<sup>+</sup>/Na for disodium terephthalate: 0.5 V difference 1869 instead of 0.33 V). Similarly, the strategies for improving the 1870 specific capacity or reducing the dissolution phenomenon of 1871 active species within the electrolyte system such as polymer- 1872 ization work usually as well for organic SIBs as they do for 1873 organic LIBs and hence will not be repeated in this section. 1874 As a reminder, the use of sodium instead of lithium is also 1875 motivated by higher abundance and lower cost of the resource, 1876 with Na being widely distributed in the earth's crust and 1877 oceans (Figure 6) and nontoxic.

As previously stated, only the materials delivering the best 1879 performances in specific capacity, operating potential, and 1880

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#	Positive electrode (or "cathode") active material	Negative electrode (or "anode") active material	Electrolyte	Output voltage (V)	Cycling stability: retention, cycles, rate or current density	Specific capacity (mAh g <sup>-1</sup> ) and Specific energy (Wh kg <sup>-1</sup> ) per mass of positive active material if not specified otherwise, Final coulombic efficiency, Loading (mg cm <sup>-2</sup> )	Ref.
		Organic electro	de materials with hig	h/low voltag	je		
1		Na	Saturated NaPF6 in DOL/DME (v/v 1:1)	3.6	82%, 200, 5 C (500 mA g <sup>-1</sup> )	95, 342, 99, n.d.	[ <sup>307</sup> ]
2			Saturated NaPF6 in DOL/DME (v/v 1:1)	~1.8	85%, 500, 8 C	180-155,° 324,° 99, n.d.	[ <sup>307</sup> ]
3		Na	0.5 M NaPF6 in EC/PC (v/v 1:1)	3.38	68%, 1 000, 1 C	94-64, 318, n.d., 1.0-2.0	[308]
4	$\begin{pmatrix} NC \\ NC \\ NC \\ CN \end{pmatrix} (Cu^\star)$	Na	1 M NaClO4 in EC/PC (v/v 1:1)	~3.6	78%, 1 200, 1 C (300 mA g <sup>-1</sup> )	98, 353,~100, n.d.	[309]
5	$\binom{\circ}{\circ} \stackrel{\circ}{\longrightarrow} \stackrel{\circ}{\longrightarrow} \stackrel{\circ}{\longrightarrow} \stackrel{\circ}{\longrightarrow} \stackrel{\circ}{\longrightarrow} \stackrel{\circ}{\longrightarrow} \binom{\circ}{\circ} (c_{\circ}^{**})$	Na	1 M NaClO4 in PC	~0.5	79%, <sup>b</sup> 1 000, (100 mA g <sup>-1</sup> )	209, 105, ~100, n.d.	[ <sup>317</sup> ]
		Ν	a-ion organic batter	ies			
6	$Na_{0.75}Mn_{0.70}Ni_{0.23}O_2$	NaO ONa	1 M NaPF6 in EC/EMC (v/v 3:7)	~3.6	93%, <sup>b</sup> 50, C/13 (20 mA g <sup>-1</sup> )	111,° 400,° 99, 1.3-2.5	[ <sup>296</sup> ]
7	$Na_3V_2O_2(PO_4)_2F$	NaO	1 M NaClO4 in PC	3.3	50%, 20, C/10 (13 mA g <sup>-1</sup> )	270-135, <sup>a</sup> 891, <sup>a</sup> 73, 2	[ <sup>324</sup> ]
8	NaiFe(CN)6		1 M NaClO4 in EC/DEC (v/v 1:1)	1.2	73%, 100, 1 C (140 mA g <sup>-1</sup> )	158-102, <sup>d</sup> 190, <sup>d</sup> 95, n.d.	[ <sup>325</sup> ]
9	Na3V(PO4)3		1 M NaClO4 in EC/DEC (v/v 1:1)	1.2	70%, 100, 1 C (140 mA g <sup>-1</sup> )	150, <sup>d</sup> 180, <sup>d</sup> 95, n.d.	[ <sup>325</sup> ]
10		Na-predoped hard carbon	1 M NaClO₄ in PC	~2.2	85%, <sup>b</sup> 40, C/10 (18 mA g <sup>-1</sup> )	178-152,° 356,° n.d., 3.1	[ <sup>326</sup> ]
11	ONa O ONa O ONa	Na P@C NaO Disodium terephthalate	0.6 NaPF6 in DEGDME	1.5 1.3 1.25	91%, 50, 500 mA g <sup>-1</sup> 83%, 50, 500 mA g <sup>-1</sup> 85%, 30, 50 mA g <sup>-1</sup>	390, 585, ~100, 3-20 264, <sup>a</sup> 281, <sup>a</sup> ~100, 3-20 137, <sup>a</sup> 141, <sup>a</sup> ~100, 3-20	[ <sup>327</sup> ] [ <sup>327</sup> ] [ <sup>327</sup> ]

#### Table 3. Performances of Selected Nonaqueous Na-Organic Batteries

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#### Table 3. continued

#	Positive electrode (or "cathode") active material	Negative electrode (or "anode") active material	Electrolyte	Output voltage (V)	Cycling stability: retention, cycles, rate or current density	Specific capacity (mAh g <sup>-1</sup> ) and Specific energy (Wh kg <sup>-1</sup> ) per mass of positive active material if not specified otherwise, Final coulombic efficiency, Loading (mg cm <sup>-2</sup> )	Ref.
12		NaO ONa	1 M NaPF6 in PC	~1.6	70%, 20, 50 mA g <sup>-1</sup>	73-51, <sup>d</sup> 117, <sup>d</sup> n.d., 1.4	[ <sup>328</sup> ]
13	NaO NaO NaO ONa	NaO NaO NaO	1 M NaClO4 in EC/DMC (v/v 1:1)	~2.0	76%, 100, C/10 (19 mA g <sup>-1</sup> )	204-155,° 65,° 99, 1.0-1.8	[ <sup>329</sup> ]
		Organic electro	ode materials with h	igh specific	capacity		
14		Na	1 M NaPF <sub>6</sub> in EC/PC (v/v 1:1)	1.0	100%, <sup>b</sup> 1024, 50 mA g <sup>-1</sup>	500, 500 ,~100, 1.0	[ <sup>330</sup> ]
15	$ \begin{array}{c} ( ) \\ ( ) $	Na	1 M NaClO4 in EC/DMC (v/v 1:1)	~1	95%, 500, 100 mA g <sup>-1</sup> 97%, 2600, 1 A g <sup>-1</sup>	320, 320, ~100, 0.7 218-258, 250, ~100, 0.7	[ <sup>331</sup> ]
16	, , , , , , , , , , , , , , , , , , ,	Na	1 M NaClO4 in EC/DMC (v/v 1:1)	~0.9	82%, 100, 100 mA g <sup>-1</sup> 99%, 10 000, 5 A g <sup>-1</sup>	420, 378, ~100, n.d. 198, 178, ~100, n.d.	[ <sup>332</sup> ]
17	NaS SNa	Na	1 M NaClO4 in EC/DMC/FEC	1.3	66%, 250, 500 mA g <sup>-1</sup>	567, 737, ~100, 1.0	[ <sup>333</sup> ]
	г – – – –	Organic elect	rode materials with	high stabili	ty		
18		Na	1 M NaClO4 in EC/PC/FEC	2.1	90%, 1 000, 10 C	90-80, 189, ~100, 0.7	[ <sup>338</sup> ]
19		Na	1 M NaPF6 in EC/DMC (v/v 1:1) 1 M NaPF6 in EC/DMC (v/v 1:1)	~2.2	87.5%, 5 000, 0.8 C (200 mA g <sup>-1</sup> ) 100%, 1000, 1 A g <sup>-1</sup>	111, 285, ~100, n.d. 100, 220, ~100, 0.8	[ <sup>339</sup> ] [ <sup>340</sup> ]
20		Na	1 M NaPF6 in EC/DMC (v/v 1:1)	~2.1	97%, 1 000, 1 A g <sup>-1</sup>	95, 200, ~100, 0.8	[ <sup>340</sup> ]
21		Na	1 M NaPF <sub>6</sub> in EC/DMC (v/v 1:1)	~2.1	93%, 1 000, 1 A g <sup>-1</sup>	82, 172, ~100, 0.8	[ <sup>340</sup> ]

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#### Table 3. continued

#	Positive electrode (or "cathode") active material	Negative electrode (or "anode") active material	Electrolyte	Output voltage (V)	Cycling stability: retention, cycles, rate or current density	Specific capacity (mAh g <sup>-1</sup> ) and Specific energy (Wh kg <sup>-1</sup> ) per mass of positive active material if not specified otherwise, Final coulombic efficiency, Loading (mg cm <sup>-2</sup> )	Ref.
22		Na	0.1 M NaPF6 in DME/DOL (v/v 1:1)	1.6	84%, 1 000, 0.5 C	157-132, 251,~100, 2.0	[ <sup>341</sup> ]
23	NaO <sub>3</sub> S	Na	1 M NaPF6 in DME	1.8	90%, 1 000, 1 A g <sup>-1</sup>	104-94, 187, ~100, 1.8-2	[ <sup>342</sup> ]
24		Na	1 M NaPF6 in DME	1.6	88%, 10 000, 514 C (50 A g <sup>-1</sup> )	110, 176, ~100, 1.0	[ <sup>334</sup> ]
25		Na	1 M NaPF <sub>6</sub> in DEGDME	1.25	81%, 1 000, 10 C 85%, 2 000, 20 C	140-113, 175, ~100, 1.5 115-98, 144, ~100, 1.5	[ <sup>335</sup> ]
26		Na	1 M NaBF₄ in TEG/DME	~0.5	75%, 1 500, 10 C	100, 50, ~100, 2.0-2.5	[ <sup>336</sup> ]
27		Na	1 M NaClO4 in PC	~2.6	80%, 7 000, 1 A g <sup>-1</sup>	~90, 234, ~100, ~1.5	[ <sup>337</sup> ]
28		Na	1 M NaClO <sub>4</sub> in EC/DEC (v/v 1:1)	~1.25	~100%, <sup>e</sup> 1 000, 5 A g <sup>-1</sup>	107, 134, ~100, n.d.	[ <sup>343</sup> ]
29		Na	1 M NaClO <sub>4</sub> in EC/DEC (v/v 1:1)	~1	83%, <sup>b</sup> 1 000, 5 A g <sup>-1</sup>	89, 89,~100, n.d.	[ <sup>343</sup> ]
30		Na	1 M NaPF6 in DME	1.65	86%, <sup>f</sup> 1 000, 0.56 C (100 mA g <sup>-1</sup> ) 95%, <sup>f</sup> 1 400, 5.6 C (1 A g <sup>-1</sup> )	177-145, 292, ~100, n.d. 128-121, 211, ~100, n.d.	[ <sup>344</sup> ]

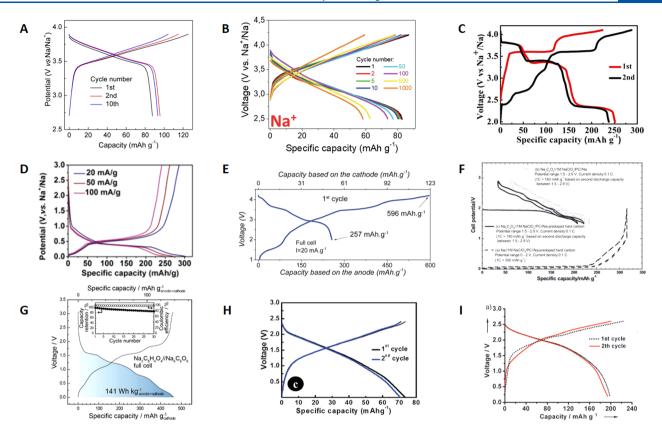
<sup>a</sup>Based on cathode material weight. <sup>b</sup>The first cycle is not taken into account. <sup>c</sup>Based on anode material weight. <sup>d</sup>Based on cathode and anode.

1881 cycling stability will be presented in the subsequent section 1882 (Table 3).

#### 6.1. High/Low Voltage Organic Electrode Materials and 1883 Hybrid/All-Organic High Output Voltage Na-Ion Batteries

1884 The design of high and low voltage OEMs for SIBs has clearly 1885 taken inspiration from the lithium equivalents. "p-type" 1886 materials (*i.e.*, anion insertion materials) are hence the most 1887 common compounds able to react at potential >3.0 V vs Na<sup>+</sup>/ 1888 Na, while materials reacting at low potential <1.5 V vs Na<sup>+</sup>/Na 1889 belong to "n-type" (*i.e.*, cation insertion materials). Conductive 1890 polymers are an example of a type of material which could belong to any or both of these categories. Early research on  $_{1891}$  conductive polymers for SIBs has been carried out by Yang's  $_{1892}$  group, who used polyaniline derivatives (p-type),  $^{303}$  doped  $_{1893}$  PPy $^{304,305}$  (p-type), or PT $^{306}$  (n-type) in some of the first  $_{1894}$  articles in this field. Soon after, they reported the activity of  $_{1895}$  polytriphenylamine (PTPAn, Table 3, entry 1) as p-type  $_{1896}$  material with PF $_6^-$  ingress.<sup>307</sup> Each triphenylamine unit can  $_{1897}$  lose one electron and intercalate one anion upon oxidation at  $_{1898}$  an average redox potential of 3.6 V vs Na<sup>+</sup>/Na forming then  $_{1899}$  quinoneimine units (Figure 13A). PTPAn displays stable  $_{1900}$  reversible capacity even at high C-rate with 88 mAh g<sup>-1</sup> at a 1901

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**Figure 13.** Voltage profiles of selected OEMs measured vs Na and all-organic Na-ion full cells including (A) PTPAn (reproduced from ref 307), (B) PDPPD (reproduced with permission from ref 308. Copyright 2019 The Royal Society of Chemistry), (C) CuTCNQ (reproduced with permission from ref 309. Copyright 2017 John Wiley & Sons, Inc.), (D) Co-bpdc (reproduced with permission from ref 317. Copyright 2018 The Royal Society of Chemistry), (E) Na<sub>0.75</sub>Mn<sub>0.70</sub>Ni<sub>0.23</sub>O<sub>2</sub>//Na<sub>2</sub>C<sub>8</sub>H<sub>4</sub>O<sub>4</sub> (from ref 296. Copyright 2012 Royal Society of Chemistry), (F) Na<sub>2</sub>C<sub>6</sub>O<sub>6</sub>//Na<sub>2</sub>C<sub>6</sub>O<sub>6</sub>//Na<sub>2</sub>C<sub>6</sub>O<sub>6</sub>//Na<sub>2</sub>C<sub>6</sub>O<sub>6</sub>//Na<sub>2</sub>C<sub>6</sub>O<sub>6</sub>//Na<sub>2</sub>C<sub>6</sub>O<sub>6</sub>//Na<sub>2</sub>C<sub>6</sub>O<sub>6</sub>//Na<sub>2</sub>C<sub>6</sub>O<sub>6</sub>//Na<sub>2</sub>C<sub>6</sub>O<sub>6</sub>//Na<sub>2</sub>C<sub>6</sub>O<sub>6</sub>//Na<sub>2</sub>C<sub>6</sub>O<sub>6</sub>//Na<sub>2</sub>C<sub>6</sub>O<sub>6</sub>//Na<sub>2</sub>C<sub>6</sub>O<sub>6</sub>//Na<sub>2</sub>C<sub>6</sub>O<sub>6</sub>//Na<sub>2</sub>C<sub>6</sub>O<sub>6</sub>//Na<sub>2</sub>C<sub>6</sub>O<sub>6</sub>//Na<sub>2</sub>C<sub>6</sub>O<sub>6</sub>//Na<sub>2</sub>C<sub>6</sub>O<sub>6</sub>//Na<sub>2</sub>C<sub>6</sub>O<sub>6</sub>//Na<sub>2</sub>C<sub>6</sub>O<sub>6</sub>//Na<sub>2</sub>C<sub>6</sub>O<sub>6</sub>//Na<sub>4</sub>C<sub>6</sub>O<sub>6</sub>//Na<sub>4</sub>C<sub>6</sub>O<sub>6</sub>//Na<sub>4</sub>C<sub>6</sub>H<sub>2</sub>O<sub>6</sub>/(Reproduced with permission from ref 328. Copyright 2015 The Royal Society of Chemistry), and (I) Na<sub>4</sub>C<sub>8</sub>H<sub>2</sub>O<sub>6</sub>//Na<sub>4</sub>C<sub>8</sub>H<sub>2</sub>O<sub>6</sub> (reproduced with permission from ref 329. Copyright 2014 John Wiley & Sons, Inc.).

1902 current of 20 C and 97% capacity retention over 200 cycles 1903 when cycled at a current of 5 C. This material has also been 1904 cycled in dual-ion cell configuration paired with poly-(anthraquinoyl sulfide) (PAQS, Table 3, entry 2), an n-type 1905 1906 material. This cell has an average voltage of 1.8 V and exhibits 1907 surprisingly high rate capability with 118 mAh  $g^{-1}$  reversible capacity (anode limitation design) at 32 C rate. At a rate of 1908 1909 8 C, the cell displays 85% capacity retention over 500 cycles. 1910 Poly(N,N'-diphenyl-*p*-phenylenediamine) (PDPPD, Table 3, 1911 entry 3) can be seen as another p-type derivative of polyaniline 1912 and can be used in lithium, sodium, or potassium batteries.<sup>308</sup> 1913 At an average redox potential of 3.38 V vs Na<sup>+</sup>/Na, its initial 1914 capacity is 94 mAh  $g^{-1}$  and sustains 76% of this value after 1915 500 cycles at a 1 C rate (Figure 13B). But the most striking 1916 performance of this polymer is certainly its ability to deliver 1917 capacity at current as high as 1000 C. At a current rate of 1, 10, 1918 50, or 100 C, the capacity losses are reasonable after 1000 1919 cycles.<sup>308</sup>

1920 Metal organic compounds can also be used as positive 1921 electrode materials for SIBs. One such example is CuTCNQ 1922 (Table 3, entry 4).<sup>309,310</sup> In its original redox state, CuTCNQ 1923 is a salt formed of cuprous ions (Cu<sup>+</sup>) and TNCQ<sup>-</sup> anion. Three 1924 redox stages could be obtained from this material at ca. 2.5, 3.4, 1925 and 3.9 V vs Na<sup>+</sup>/Na, corresponding to TNCQ<sup>2-</sup>/TNCQ<sup>-</sup>, 1926 TNCQ<sup>-</sup>/TNCQ<sup>0</sup>, and Cu<sup>+</sup>/Cu, respectively (Figure 13C). 1927 When nanostructured as flower-like nanorods anchored on 1-D carbon nanofibers (CNFs), CuTNCQ/CNFs composite 1928 displays reversible capacity of 137 mAh  $g^{-1}$  with 85% capacity 1929 retention after 300 cycles at a rate of 300 mA  $g^{-1}$  using the 1930 3 redox couples. If restricted to a cutoff voltage of 2.5–4.1 V vs 1931 Na<sup>+</sup>/Na which corresponds to TNCQ<sup>-</sup>/TNCQ<sup>0</sup> and Cu<sup>+</sup>/Cu<sup>0</sup> 1932 redox couples, the cell exhibits a capacity retention of 78% 1933 after 1200 cycles for an average redox potential of 3.6 V vs 1934 Na<sup>+</sup>/Na. But in this case, the high redox potential is shifted 1935 up due to the contribution of a metal center, unlike p-type 1936 OEMs.

For low potential OEMs for SIBs, carboxylates (e.g., 1938 disodium terephthalate, disodium naphthalene dicarboxy- 1939 late, <sup>311</sup> disodium pyridine-2,5-dicarboxylate, <sup>312</sup> disodium 4,4'- 1940 biphenyldicarboxylate, <sup>313</sup> and so on) or Schiff bases<sup>314–316</sup> 1941 have already been covered in recent reviews. <sup>16,40,41,302</sup> The 1942 only recent example that will be covered here is the case of a 1943 metal organic framework (MOF) made of cobalt and 4,4'- 1944 biphenyldicarboxylate ligands (Co-bpdc, Table 3, entry 5). <sup>317</sup> 1945 According to the authors, the cobalt ions do not undergo 1946 reduction during the electrochemical process, leaving the redox 1947 activity to the sole organic moiety. The reversible sodium 1948 insertion/deinsertion occurs at an average potential of 0.5 V vs 1949 Na<sup>+</sup>/Na and exhibits stable capacity of ca. 300 mAh g<sup>-1</sup> with 90% 1950 capacity retention for 50 cycles at 20 mA g<sup>-1</sup> or 264 mAh g<sup>-1</sup> 1951 and 79% capacity retention for 1000 cycles at 100 mA g<sup>-1</sup> 1952 (Figure 13D).

2020

The interest for low potential OEMs for SIBs started to rise 1954 1955 when poor long-term stability or safety issues were reported 1956 with classical inorganic materials or soft/hard carbons, while 1957 positive inorganic electrodes gave promising results.<sup>1'</sup> 1958 The larger ion diffusion pathways in OEMs are believed to be 1959 appropriate for the large sodium ions (as compared to lithium 1960 ions) while more constrained ion diffusion pathways in inor-1961 ganic materials might be too restricted for sodium intercalation 1962 at low potentials.<sup>323</sup> Ideally, a good compromise could be 1963 found with hybrid organic/inorganic sodium-ion batteries 1964 using inorganic materials as the positive electrode and OEMs 1965 as the negative electrode. One early example is the full sodium-1966 ion cell made of disodium terephthalate as negative elec-1967 trode and Na<sub>0.75</sub>Mn<sub>0.70</sub>Ni<sub>0.23</sub>O<sub>2</sub> as positive electrode (Table 3, 1968 entry 6).<sup>296</sup> With 3.6 V as output voltage, this cell delivers 1969 257 mAh g<sup>-1</sup> initial capacity (anode limitation design) with 1970 limited capacity loss after 50 cycles (93% capacity retention, 1971 (Figure 13E). Interestingly, its stability is better for this full cell 1972 rather than the two half-cells using both electrodes and 1973 metallic sodium as counter electrode. However, this better 1974 stability for a hybrid organic/inorganic sodium-ion full cell is 1975 not systematic. In the case of a  $Na_3V_2O_2(PO_4)_2F/rGO//$ 1976 disodium naphthalene-2,6-dicarboxylate cell with an average 1977 redox potential of 3.3 V vs Na<sup>+</sup>/Na, a severe capacity decay is 1978 noticeable after merely 20 cycles (Table 3, entry 7), while the 1979 half-cells display a better capacity retention.<sup>324</sup> Other examples 1980 with acceptable stability include  $Na_4Fe(CN)_6//poly$  1,4,5,8-1981 naphthalenetetracarboxylic dianhydride (PNTCD) and Na<sub>2</sub>V- $(PO_4)_3//PNTCD.^{325}$  However, like most diimide compounds, 1982 1983 the average redox potential of PNTCD is 2.1 V vs Na<sup>+</sup>/Na, 1984 which considerably restricts the average output voltage of the 1985 full cells to 1.2 V (Table 3, entry 8, 9).

1986 Examples of a hybrid organic/inorganic sodium-ion full cell 1987 using an OEM as the positive electrode are scarcer. One of the 1988 few cases is disodium rhodizonate which was cycled vs Na-1989 predoped hard carbon with improved cyclability as compared to 1990 cycling vs metallic sodium (Table 3, entry 10 and Figure 13F).<sup>326</sup> 1991 Comparably to its lithium counterpart, disodium rhodizonate 1992 is able to reversibly intercalate four sodium ions (Table 3, 1993 entry 11).<sup>327</sup> When nanosized, it delivers up to 484 mAh g<sup>-1</sup> 1994 with several electrochemical features corresponding to the 1995 different sodium ion insertions. Disodium rhodizonate can also 1996 be cycled in a hybrid organic/inorganic full cell vs phosphorus 1997 encapsulated in a carbon scaffold (P@C) or in an all-organic 1998 configuration vs disodium terephthalate (Figure 13G).

All-organic Na-ion batteries is an attractive concept without 2000 sensitive metals (price, rarity, geopolitics) such as cobalt, nickel, 2001 or lithium. But merely some examples have been reported in the 2002 literature. In addition to previously mentioned cases (Table 3, 2003 entries 2 and 11), a cell using N,N'-diamino-3,4,9,10-2004 perylenetetracarboxylic polyimide (PI) as the positive elec-2005 trode and disodium terephthalate as the negative electrode has 2006 been described (Table 3, entry 12, Figure 13H).<sup>328</sup> The 2007 limited output voltage of 1.6 V is here also connected to the 2008 choice of a polyimide whose average redox potential is 2.2 V vs 2009 Na<sup>+</sup>/Na.

<sup>2010</sup> There is still to date only one example of an all-organic <sup>2011</sup> rocking chair sodium-ion battery published by Chen's group <sup>2012</sup> (Table 3, entry 13 and Figure 13I).<sup>329</sup> The tetrasodium salt of <sup>2013</sup> 2,5-dihydroxyterephthalic acid (Na<sub>4</sub>DHTPA or Na<sub>4</sub>-*p*-DHT) is <sup>2014</sup> used in the same time as both positive and negative electrodes <sup>2015</sup> in a symmetrical cell as previously demonstrated in the case of <sup>2016</sup> the lithium chemistry.<sup>251</sup> With 2 V as output voltage, this cell is hampered by the irreversible capacity of the negative electrode  $_{2017}$  and displays reversible capacity of 198 mAh  $g^{-1}$  with 76%  $_{2018}$  capacity retention after 100 cycles at a rate of C/10.  $_{2019}$ 

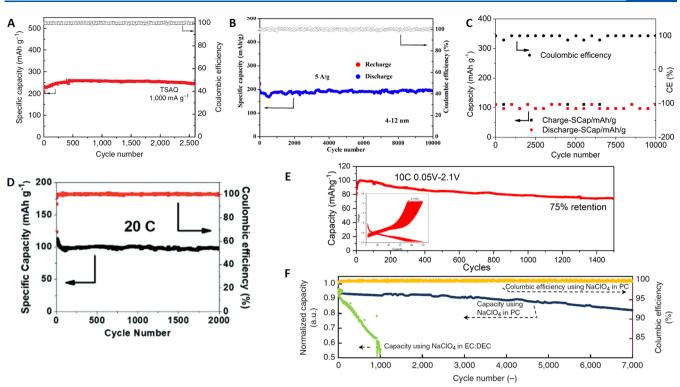
# 6.2. Organic Electrode Materials with High Specific Capacity

All materials selected in this section are able to deliver more 2021 than 300 mAh  $g^{-1}$  over tens of cycles without conductive 2022 additive contribution. Interestingly, besides the previously 2023 mentioned disodium rhodizonate, many other high-capacity 2024 materials for SIBs involve the intercalation of sodium ions onto 2025 unsaturated carbons, as a sodium equivalent of the mechanism 2026 coined as "superlithiation" (see section 7.3), which will be 2027 thoroughly covered in the section 7.3.<sup>21,260</sup> Consequently, their 2028 electrochemical features display similarities such as the 2029 requirement for large polarization values, sloping curves, and 2030 poor round trip efficiency. A first example is polydopamine 2031 (PDA, Table 3, entry 14) employed as both electrode and 2032 redox-active binder material, obtained as a mixture of ortho- 2033 catechol and ortho-quinone.<sup>330</sup> After a first cycle with low 2034 Coulombic efficiency which could be explained by the solid 2035 electrolyte interface (SEI) formation and proton/sodium exchange 2036 in the catechol moieties, it shows an impressive stable capacity of 2037 500 mAh  $g^{-1}$  with no obvious capacity loss over 1024 cycles. 2038

The group of Zhouguang Lu has investigated several 2039 derivatives of tri- $\beta$ -ketoenamine linked compounds, either as a 2040 single molecule or as covalent organic frameworks (COF).<sup>331,332</sup> 2041 If cycled at low potential vs Na<sup>+</sup>/Na, after the expected 2042 reduction of carbonyls from the anthraquinone moieties, the 2043 enolization of carbonyls of the tri- $\beta$ -ketoenamine generates a 2044 triradical. The storage of three additional sodium ions is 2045 allowed by the reduction of the carbon backbone. Surprisingly, 2046 neither the triradical intermediate nor the organosodium 2047 species display major stability issues. In the case of TSAQ 2048 (Table 3, entry 15), the electrodes show a highly reversible 2049 capacity of 320 mAh  $g^{-1}$  with capacity retention higher than 2050 95% after 50 cycles at a current density of 100 mA  $g^{-1.331}$  2051 When cycled at a current 10 times higher, a capacity above 2052 220 mAh  $g^{-1}$  is sustained for 2600 cycles (Figure 14A). For 2053 DAAQ-COF (Table 3, entry 16), which can be seen as a 2054 COF derivative of TSAQ, the specific capacities are highly 2055 dependent on the particle size, even if this parameter does not 2056 seem to hamper the stability. The best performances are 2057 obtained with 4-12 nm particles that can sustain specific 2058 capacity above 400 mAh  $g^{-1}$  for 100 cycles. More impressively, 2059 when cycled at a current as high as 5 A  $g^{-1}$ , ca. 200 mAh  $g^{-1}$ 2060 are maintained for 10 000 cycles (Figure 14B). 2061

As an alternative to carboxylates such as disodium tere- 2062 phthalate, their sulfur derivatives thiocarboxylates have been 2063 investigated, where either one or two of the oxygen atoms of 2064 the carboxylate function are replaced by sulfur atom in this 2065 series of analogues.<sup>333</sup> The best performances are obtained 2066 with the compound Table 3, entry 17 with capacity as high as 2067 567 mAh  $g^{-1}$  at a current density of 50 mAh  $g^{-1}$  and limited 2068 capacity loss after 250 cycles. Considering this compound has a 2069 larger molecular weight as compared to disodium tereph- 2070 thalate, its theoretical capacity per exchanged electron is lower 2071 (97.7 mAh  $g^{-1}$  against 127.5 mAh  $g^{-1}$ ). However, while 2072 disodium terephthalate is limited to two electrons exchanged, 2073 compound 17 can accommodate up to 6 electrons with 2074 partial reversible reduction of its benzene ring through the 2075 "supersodiation" process (similar to "superlithiation", see 2076 section 7.3). 2077

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**Figure 14.** Capacity retention of selected OEMs measured vs Na including (A) TSAQ (reproduced from ref 331), (B) DAAQ-COF (reproduced with permission from ref 332. Copyright 2019 American Chemical Society), (C) PPTS (reproduced with permission from ref 334. Copyright 2018 Elsevier Ltd.), (D) ADASS (reproduced with permission from ref 335. Copyright 2018 John Wiley & Sons, Inc.), (E) Na<sub>3</sub>C<sub>9</sub>H<sub>3</sub>O<sub>6</sub> (reproduced with permission from ref 336. Copyright 2018 John Wiley & Sons, Inc.), and (F) BPOE (reproduced from ref 337).

#### 6.3. Organic Electrode Materials with Long Cycle Life

2078 In general, poorer stabilities are observed for SIBs as compared 2079 to LIBs due to SEI layer compounds dissolution in the 2080 electrolyte system, to the very unstable metallic sodium for the 2081 half-cell configurations (dendrites formation), or to Na<sub>x</sub>C 2082 formed from sodium intercalation into the conductive additive 2083 at low potential. Achieving 1000 cycles or more for SIBs 2084 without severe capacity loss is hence a challenge. However, 2085 some OEMs are able to sustain high capacities for such long 2086 cycling. Some examples were previously commented (Table 3, 2087 entries 3, 4, 5, 14, 15, and 16).

As already seen, the average redox potential of polyimides 2089 is usually in the 2.1–2.2 V vs Na<sup>+</sup>/Na potential range. 2090 Consequently, they suffer less long-term instability due to 2091 extreme potential windows. Polyethylenediamine 1,4,5,8-2092 naphthalenetetracarboxylic dianhydride (PEDA-NTCDA, 2093 Table 3, entry 18),<sup>338</sup> polyethylenediamine 3,4,9,10-perylene-2094 tetracarboxylic dianhydride (PEDA–PTCDA, Table 3, entry 2095 19),<sup>339,340</sup> polypropylenediamine 3,4,9,10-perylenetetracarbox-2096 ylic dianhydride (PPDA–PTCDA, Table 3, entry 20),<sup>340</sup> and 2097 polyhexylenediamine 3,4,9,10-perylenetetracarboxylic dianhy-2098 dride (PHDA–PTCDA, Table 3, entry 21),<sup>340</sup> have all been 2099 cycled for at least 1000 cycles with negligible capacity loss. 2100 Especially, PEDA–PTCDA retained 87.5% of its initial 2101 capacity after 5000 cycles (Figure 14C).<sup>339</sup>

2102 Anthraquinones reversibly insert sodium at average redox 2103 potential slightly lower as compared to polyimides (*i.e.*, 1.6– 2104 1.8 V vs Na<sup>+</sup>/Na), limiting also the risk of side reactions. 2105 Anthraquinones as polymers (PAQS, Table 3, entry 22)<sup>341</sup> or 2106 as salts (disodium 9,10-anthraquinone-2,6-disulfonate, 2107 Na<sub>2</sub>AQ26DS, Table 3, entry 23)<sup>342</sup> have been success-2108 fully cycled for 1000 cycles. An anthraquinone derivative, poly(pentacenetetrone sulfide) (PPTS, Table 3, entry 24)  $_{2109}$  exhibits a remarkable stability at a very high rate of 50 A g<sup>-1</sup>  $_{2110}$  corresponding to a full charge in 7 s. After 10 000 cycles, it still  $_{2111}$  maintains 97 mAh g<sup>-1</sup> (Figure 14C).  $_{2112}$ 

Azobenzene-4,4'-dicarboxylic acid sodium salt (ADASS, 2113 Table 3, entry 25) is a material that can reversibly insert two 2114 sodium ions on its azo (-N=N-) function at an average 2115 redox potential of 1.25 V vs Na<sup>+</sup>/Na.<sup>335</sup> It can be cycled at 2116 a high current of 10 or 20 C for 1000 and 2000 cycles, 2117 respectively, with moderate capacity losses (Figure 14D). The 2118 average redox potential of sodium carboxylates is rather low 2119 (usually in the 0.3–0.8 V range vs Na<sup>+</sup>/Na) which makes side 2120 reaction likely to occur during long time cycling. Still, the 2121 group of Palani Balaya succeeded to cycle trisodium-1,3,5- 2122 benzene tricarboxylate (Table 3, entry 26) for 1500 cycles at a 2123 rate of 10 C with 75% capacity retention with a lower cutoff 2124 potential of 50 mV (Figure 14E).<sup>336</sup>

Several covalent organic frameworks (COFs) have shown 2126 excellent cyclability. An early example from the literature is a 2127 p-type material (Table 3, entry 27) that reversibly inserts anion 2128 (ClO<sub>4</sub><sup>-</sup>) at an average potential of 2.6 V vs Na<sup>+</sup>/Na and 2129 sustains 80% of its capacity after 7000 cycles at a rate of 2130 1 A g<sup>-1</sup> (Figure 14F).<sup>337</sup> Other triazine-based COFs have been 2131 used as n-type materials with the integration of carbonyl- 2132 containing moieties (Table 3, entry 28, 29).<sup>343</sup> After a stabi- 2133 lization period corresponding to 30 cycles, they sustain most 2134 of their capacities over 1000 cycles at a high rate of 5 A g<sup>-1</sup>. 2135 In addition to the previously mentioned tri- $\beta$ -ketoenamine 2136 derivatives, which have already shown excellent stability (Table 3, 2137 entry 15, 16), the pentacenetetrone derivative 30 is able to maintain 95% of its capacity after 1400 cycles at a rate of 1 A g<sup>-1</sup>.<sup>344</sup> 2139

#	Positive electrode (or "cathode") active material	Negative electrode (or "anode") active material	Electrolyte	Output voltage (V)	Cycling stability: retention, cycles, rate or current density	Specific capacity (mAh g <sup>-1</sup> ) and Specific energy (Wh kg <sup>-1</sup> ) per mass of positive active material if not specified otherwise, Final coulombic efficiency, Loading (mg cm <sup>-2</sup> )	Ref.		
1	ко	K	1 M KPF6 in DME	0.6	95%, <sup>a</sup> 500, 1 A g <sup>-1</sup>	194, 116, ~100, 1.2-1.6	[ <sup>346</sup> ]		
2		К	1 M KPF₀ in DME	1.7	74%, 3 000, 24 C (5 A g <sup>-1</sup> )	258, 439, 99, 1.0-2.0	[ <sup>347</sup> ]		
3		КО	1 M KPF6 in DME	~1.1	66%, 100, 100 mA g <sup>-1</sup>	254, <sup>b</sup> 122, <sup>b</sup> 99, 1.0-2.0	[ <sup>347</sup> ]		
4	ко	ко ск	1.25 M KPF6 in DME	~1.25	n.d., 10, 25 mA g <sup>-1</sup>	~28, <sup>b</sup> 35 <sup>b</sup> n.d., 1.5-2.0	[ <sup>348</sup> ]		
5		К	1 M KPF6 in PC/FEC (v/v 98:2)	4.05	86%, 100, 50 mA g <sup>-1</sup> 55%, 500, 2 A g <sup>-1</sup>	125, 487, 88, 2.0 85, 351, 88, 2.0	[ <sup>349</sup> ]		
6		К	0.5 M KPF6 in EC/DEC (v/v 1:1)	3.52	63%, 1 000, 10 C	62-39, 218, n.d., 1.0-2.0	[ <sup>308</sup> ]		
7	{-{~-}-#-{~-#}-	К	PMMA / 0.8 M KPF6 in EC/DEC/FEC (v/v/v 45:45:10)	3.15	98%, 100, 50 mA g <sup>-1</sup>	125, 394,n.d., 3.0	[ <sup>350</sup> ]		
<sup><i>a</i></sup> The	<sup><i>a</i></sup> The first cycle is not taken into account. <sup><i>b</i></sup> Based on cathode material weight.								

#### Table 4. Performances of Selected Nonaqueous K-Organic Batteries

To sum up, the development of organic SIBs has gained 2140 2141 remarkably increased attention since 2012 and is considered as 2142 an interesting alternative to organic LIBs making the devel-2143 opment of cationic rocking-chair batteries made of abundant 2144 elements possible. Although great achievements have been 2145 made, many challenges still remain to tackle problems such as 2146 capacity fading or low energy density. Polymerization, metal/ 2147 covalent organic frameworks, or insoluble salts are successful 2148 strategies to suppress the former, and very long cycling batte-2149 ries have been reported without structural instability. As compared 2150 to their inorganic counterparts, promising results have been 2151 obtained for negative electrodes as an alternative to metallic 2152 sodium, graphite, or even hard/soft carbons. Improving the 2153 energy density is more complex and requires advanced elec-2154 trode design in order to suppress as much conductive additive 2155 as possible. Nevertheless, the combination of renewable 2156 organic materials together with the high abundance of sodium 2157 raw materials provides an appealing concept, which is enough 2158 for encouraging continuous progress, and research in this field 2159 should certainly be esteemed.

#### 7. PERFORMANCES OF OTHER NONAQUEOUS **ORGANIC BATTERIES** 2160

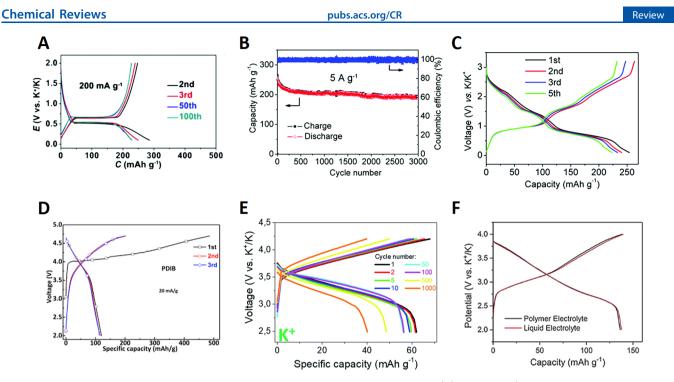
#### 7.1. Performances of Nonaqueous Potassium-Organic 2161 Batteries

2162 Surprisingly, despite the natural abundance of potassium, its 2163 relative low-cost, and the low electrochemical potential of 2164  $K^+/K$  (-2.94 V vs SHE), K-ion batteries (KIBs) have not been 2165 thoroughly investigated until recently,<sup>345</sup> with the motivation

being related to its abundancy like Na compared to Li. One 2166 scientific reason is the large 1.38 Å ionic radius of K<sup>+</sup> (0.76 Å 2167 for  $Li^+$ , 1.02 Å for  $Na^+$ ), which makes a challenge the design of 2168 inorganic materials able to reversibly insert such large ions into 2169 a rigid and constrained framework. Considering their larger 2170 interlayer spacing and flexible framework, OEMs for KIBs have 2171 then attracted the attention of researchers in parallel with the 2172 early development of their inorganic counterparts and not 2173 years or decades later unlike LIBs or SIBs. The research 2174 on OEMs for KIBs has clearly taken advantage of the years 2175 of development of OEMs for LIBs and SIBs and organic 2176 templates, which have been proven successful in these devices, 2177 have been adapted for KIBs, swapping from lithium or sodium 2178 salt to potassium salts when necessary. 2179

One such example is the dipotassium terephthalate (Table 4, 2180 entry 1) which intercalates/deintercalates potassium ion at 2181 an average potential of 0.6 V vs K+/K with a well-defined 2182 plateau after the first cycle.<sup>346</sup> It exhibits reversible capacity up to 2183 249 mAh g<sup>-1</sup>, and good capacity retention of 95% over 500 cycles 2184 is obtained when cycled at a rate of 1000 mA  $g^{-1}$  (Figure 15A). 2185 Quinone derivatives have already displayed their robustness 2186 in other EES devices. Poly(pentacenetetrone sulfide) (PPTS, 2187 Table 4, entry 2) can be cycled for 3000 cycles at a rate of 2188 5 A  $g^{-1}$  with limited capacity decay (Figure 15B).<sup>347</sup> Interestingly, 2189 at such a high rate, the Coulombic efficiency is much higher as 2190 compared to cycling at a rate of 0.1 A/g (~99% against ~90%), 2191 which is due to the highly reactive metallic potassium counter 2192 electrode and dendrite formation according to the authors. 2193

These two materials have been cycled in an all-organic full cell 2194 (thereby without metallic potassium) which delivers 254 mAh  $g^{-1}$  2195



**Figure 15.** Voltage profiles or capacity retention of selected OEMs measured vs K including (A)  $K_2C_8H_4O_4$  (reproduced with permission from ref 346. Copyright 2017 The Royal Society of Chemistry), (B) PPTS (reproduced with permission from ref 347. Copyright 2019 The Royal Society of Chemistry), (C) PPTS//K<sub>2</sub>C<sub>8</sub>H<sub>4</sub>O<sub>4</sub> (reproduced with permission from ref 347. Copyright 2019 The Royal Society of Chemistry), (D) PVK (reproduced with permission from ref 349. Copyright 2019 Elsevier Ltd.), (E) PDPPD (reproduced with permission from ref 308. Copyright 2019 The Royal Society of Chemistry), and (F) PAni (reproduced with permission from ref 350. Copyright 2018 John Wiley and Sons).

2196 initial capacity and 66% capacity retention after 100 cycles with 2197 an average Coulombic efficiency of 99% (Table 4, entry 3, 2198 Figure 15 C). Another example of an all-organic full cell has 2199 been realized by Chen's group using dipotassium rhodizonate as 2200 the positive electrode of tetrapotassium salt of tetrahydroxyquinone 2201 as the negative electrode (Table 4, entry 4).<sup>348</sup> Unfortunately, 2202 this cell displays very limited stability.

2203 Materials with an average redox potential above 3.0 V vs 2204 K<sup>+</sup>/K all belong to the p-type class and hence insert anions instead 2205 of potassium ions (dual-ion cell configuration, Figure 9b-3). 2206 The highest redox voltage for an organic KIB to date has been 2207 obtained using poly(*N*-vinylcabazole) (PVK) which can insert 2208 PF<sub>6</sub><sup>-</sup> at an average redox potential of 4.05 V vs K<sup>+</sup>/K but with 2209 poor Coulombic efficiency (Figure 15D).<sup>349</sup> Other remarkable 2210 performances have been obtained with PDPPD (3.52 V vs 2211 K<sup>+</sup>/K, Figure 15E)<sup>308</sup> and polyaniline (PAni, 3.15 V vs K<sup>+</sup>/K, 2212 Figure 15F).<sup>350</sup>

In short, the research on KIBs is still in its infancy after starting 2214 to bloom in 2015 for inorganic electrode materials and 2016 for 2215 OEMs. One major challenge is the replacement of metallic potas-2216 sium with a more stable negative electrode. But this has not pre-2217 vented the development of long-term cycling batteries with more 2218 than 1000 cycles (Table 4, entries 2 and 6; see also refs 351–356).

# 7.2. Nonaqueous Multivalent Metal–Organic Batteries 2219 (Mg, Al, Zn)

2220 Among the investigated post-LIB systems, rechargeable batte-2221 ries based on multivalent metal-ion shuttling (including Mg<sup>2+</sup>, 2222 Ca<sup>2+</sup>, Al<sup>3+</sup>, Zn<sup>2+</sup>) are expected to offer significant improvement 2223 in volumetric energy density simply by using the corresponding 2224 metal as the negative electrode material (e.g.,  $\approx$ 3833 mAh cm<sup>-3</sup> 2225 theoretical volumetric energy density for Mg compared to 2226 ~2046 mAh cm<sup>-3</sup> for Li metal). In addition, the abundancy of 2227 such elements is not critical (2.5% of the earth's crust for Mg against 0.0017% for Li).<sup>357,358</sup> The current status is that few 2228 regular host inorganic electrode compounds, based on which 2229 Li-ion batteries are established, are able to deliver reasonable 2230 electrode performance for storing multivalent metal-ions. For 2231 Mg batteries, the flagship multivalent-metal batteries, Chevrel 2232 phase  $Mo_6X_8$  (X = S, Se), continue to be the only reliable 2233 positive electrode materials despite the limited specific energy 2234 of the  $Mo_6X_8$ -Mg systems (up to 140 Wh kg<sup>-1</sup>).<sup>359,360</sup> Recent 2235 discoveries of spinel Ti<sub>2</sub>S<sub>4</sub> and sulfur as Mg positive electrode 2236 materials in conjunction with the continuous development of 2237 non-nucleophilic chloride-free electrolytes greatly expanded 2238 the technology, but sluggish kinetics remain and stability issues 2239 are real.<sup>361,362</sup> This is where OEMs start to look interesting: 2240 some OEMs have been reported to show adequate kinetics 2241 even at room temperature and deliver higher specific energies 2242 than those achieved by inorganic intercalation compounds at 2243 elevated temperatures. Due to these early successes, OEMs are 2244 now regarded by some as a wild card to enable multivalent- 2245 metal batteries.<sup>48,358,363</sup> The properties and cell performance of 2246 these materials are summarized for comprehensive comparison 2247 (Table 5). 2248

The promises aside, it is necessary to emphasize that 2249 multivalent chemistries are more complicated than monovalent 2250 ones, and the ion storage mechanism has not received enough 2251 scrutinization for many OEMs. For example,  $Mg^{2+}$  is noto- 2252 riously difficult to be dissociated from electrolyte solution 2253 species such as Cl<sup>-</sup> and ethereal solvent molecules.<sup>364,365</sup> 2254 While most studies on Mg–organic batteries employed 2255 Cl<sup>-</sup>-containing electrolytes, a very recent study showed that 2256 probably all n-type OEMs store MgCl<sup>+</sup> instead of the presumed 2257 Mg<sup>2+</sup> in these electrolytes.<sup>366</sup> This unintended storage mechanism 2258 would effectively make most Mg–organic batteries hybrid 2259 batteries, that is, the charge carrier ions at the positive and 2260 negative electrodes are different, and the electrolyte solution 2261

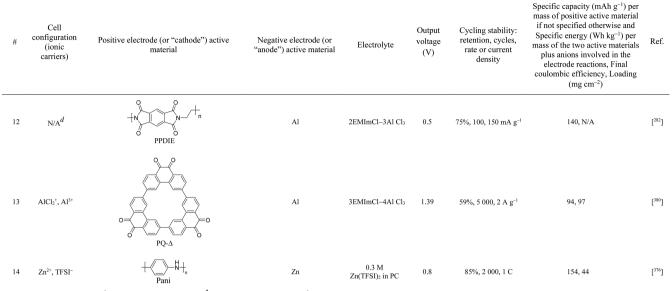
### Table 5. Performances of Selected Nonaqueous Multivalent Metal–Organic<sup>e</sup>

#	Cell configuration (ionic carriers)	Positive electrode (or "cathode") active material	Negative electrode (or "anode") active material	Electrolyte	Output voltage (V)	Cycling stability: retention, cycles, rate or current density	Specific capacity (mAh g <sup>-1</sup> ) per mass of positive active material if not specified otherwise and Specific energy (Wh kg <sup>-1</sup> ) per mass of the two active materials plus anions involved in the electrode reactions, Final coulombic efficiency, Loading (mg cm <sup>-2</sup> )	Ref.
1	N/A <sup>a</sup>	$\underbrace{+ \swarrow }_{Pani} \overset{H}{\rightarrow}_{n}$	(Pt)	0.025 M MgSO4 in EMIES	2.09	53%, 60, 667 mAh g <sup>-1</sup>	116, N/A	[ <sup>367</sup> ]
2	Mg²⁺, ClO₄⁻	PTPA	AC	1 M Mg(ClO <sub>4</sub> ) <sub>2</sub> in AN	3.2	N/A	N/A	[ <sup>368</sup> ]
3	Mg <sup>2+</sup> , TFSI⁻		Mg	0.3 M Mg(TFSI) <sub>2</sub> in G1/G2	~2.3	N/A	38, 62	[ <sup>369</sup> ]
4	N/A <sup>b</sup>	carbyne polysulfide	Mg	0.25 M Mg(AlCl2EtBu)2 in THF	1.25	71%, 23, 5.4 mA g <sup>-1</sup>	328, N/A	[ <sup>373</sup> ]
5	N/A <sup>b</sup>	HO + S - s - s - s - h PHBQS	Mg	0.16 M 3MgCl <sub>2</sub> 2Mg(TFSI) <sub>2</sub> in G4/DOL	1.8	c	158, N/A	[371]
6	N/A <sup>b</sup>		Mg	0.5 M Mg(ClO <sub>4</sub> ) <sub>2</sub> in GBL 0.5 M Mg(TFSI) <sub>2</sub> -2	0.95	85%, 5, 260 mA g <sup>−1</sup> 38%, 30, 0.2C	260, N/A 226, N/A	[ <sup>374</sup> ] [ <sup>370</sup> ]
7	Mg <sup>2+</sup>	o + Pl4AQ	Mg	MgCl <sub>2</sub> in DME 0.2 M Mg(TFSI) <sub>2</sub> in G2	1.36	72%, 100, 130 mA g <sup>-1</sup>	180, 227	[ <sup>366</sup> ]
8	Mg <sup>2+</sup>	$C_{\theta}H_{17} \rightarrow C_{\theta}H_{17} \rightarrow C_{\theta}H_{17} \rightarrow C_{\theta}H_{17} \rightarrow C_{\theta}H_{17} \rightarrow C_{10}H_{17} \rightarrow C_{10}H_{$	Mg	0.2 M Mg(TFSI) <sub>2</sub> in G2	1.45	87%, 2 500, 300 mA g <sup>-</sup>	54, 76	[ <sup>366</sup> ]
9	N/A <sup>b</sup>	+N PPDIE	Mg	PhMgCl-AlCl3 in THF	1.2	89%, 200, 150 mA g <sup>-1</sup>	140, N/A	[282]
10	AlCl4 <sup>-</sup> , Al <sup>3+</sup>	H_SJ+ <sub>n</sub> polythiophene	Al	2EMImCl-3Al Cl <sub>3</sub>	1.35	80%, 100, 16 mA g <sup>-1</sup>	88, 76	[ <sup>375</sup> ]
11	AlCl4 <sup>-</sup> , Al <sup>3+</sup>	$ \begin{array}{c} NO_2 \\ I $	AI	EMImCI–1.3Al Cl <sub>3</sub>	1.75	76%, 1 000, 200 mA g <sup>-</sup>	70, 85	[ <sup>377</sup> ]

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#### Table 5. continued



<sup>*a*</sup>Could be either  $SO_4^{2^-}$  or  $CH_3CH_2SO_3^{-}$ . <sup>*b*</sup>Could be either  $Mg^{2^+}$  or  $MgCl^+$ . <sup>*c*</sup>Only showed the initial "activation" cycles where capacity was increasing. <sup>*d*</sup>Could be either  $Al^{3^+}$  or  $AlCl_2^{+}$ . <sup>*c*</sup>Abbreviations: EMIES = 1-ethyl-3-methylimidazolium ethyl sulfate; AN = acetonitrile; G1 = monoglyme; G2 = diglyme; G4 = tetraglyme; TFSI = bis(trifluoromethane)sulfonimide; DOL = dioxolane; THF = tetrahydrofuran; GBL =  $\gamma$ -lactone; EMIm = 1-ethyl-3-methylimidazolium; PC = propylene carbonate; DME = dimethoxyethane.

2262 must contain enough of the necessary ions to maintain charge 2263 balance. Cell specific capacity will be heavily limited by the weight of the electrolyte solution as a result. Since unambig-2264 2265 uous determination of the stored species in most previously 2266 reported Mg-organic batteries has been overlooked, it would be difficult to estimate the actual specific capacity of those 2267 2268 systems. In fact, such negligence is not specific to Mg-organic 2269 batteries studies but Mg-ion storing positive electrode material 2270 research in general. In the future, this situation can be reverted 2271 by dedicated characterizations and rational selection of electro-2272 lyte solutions. This section mainly concerns the apparent spe-2273 cific capacity of OEMs and only discusses storage mechanism 2274 where sufficient experimental evidence of stored species is 2275 available.

Similar to nonaqueous Li-organic batteries, the highest 2276 2277 discharge potentials for Mg-organic batteries have been 2278 reported for p-type OEMs. Conductive polymer polyaniline 2279 (PAni), nitrogen-centered PTPA, and oxygen radical-centered 2280 PTMA all discharge at >2 V vs  $Mg^{2+}/Mg$ , with PTPA showing 2281 the highest discharge potential at 3.2 V vs  $Mg^{2+}/Mg$ .<sup>3</sup> 2282 Note that none of these materials were tested in electrolyte 2283 solutions where reversible Mg plating/stripping is possible. 2284 Among n-type OEMs, p-BQ-based molecule DMBQ and 2285 polymer poly(hydrobenzoquinonyl-benzoquinonyl sulfide) 2286 (PHBQS) show the highest discharge potentials of 1.63 and 2287 1.8 V vs Mg<sup>2+</sup>/Mg, respectively (Figure 16B, C).<sup>370,371</sup> Other 2288 carbonyl compounds based on anthraquinone and imides 2289 discharge at lower potentials, as they also do in Li batteries.<sup>372</sup> 2290 As far as specific capacity is concerned, the organosulfur compound 2291 carbyne polysulfide shows the highest 328 mAh  $g^{-1}$  (Figure 16A), 2292 with carbonyl compounds DMBQ (up to 260 mAh  $g^{-1}$ ) and 2293 P14AQ (180 mAh  $g^{-1}$ ) following (Figure 16C, D).<sup>366,373,374</sup> The 2294 change of charge carrier ion from Li<sup>+</sup> to Mg<sup>2+</sup> does not seem to 2295 alter the cycling stability generally observed for Li<sup>+</sup>-storing polymer 2296 OEMs. P(NDI2OD-T2) and PPDIE lose 13% and 11% of their 2297 initial capacities after 2500 and 200 deep cycles, respectively, which stability is rarely seen from inorganic positive electrode materials

(Figure 16E).<sup>282,366</sup> While these are quite some attractive numbers, 2299 there is no OEM that simultaneously shows high discharge 2300 potential, specific capacity, and cycling stability. There are also few 2301 OEMs that have been confirmed to store  $Mg^{2+}$  instead of complex 2302 ions. Therefore, there is a lot of opportunity lying ahead for 2303 developing better OEMs for Mg-organic batteries. 2304

OEMs for other nonaqueous multivalent metal-ions storage 2305 are quite rare. Most OEMs reported for multivalent-metal- 2306 organic batteries have been p-type materials where storage of 2307 anions rather than cations takes place (dual-ion cell configu- 2308 ration). Conductive polymers PT and PAni have been studied 2309 in Al and Zn batteries, respectively, showing decent to great 2310 cycling stability.<sup>375,376</sup> Poly(nitropyrene-co-pyrene) shows the 2311 highest discharge potential for an Al-organic battery at 1.75 V 2312 with great 75% capacity retention after 1000 cycles.<sup>377</sup> Note 2313 that for Al batteries, only graphite, also a p-type material in this 2314 case, shows viable performances despite limited specific 2315 capacity.<sup>378,379</sup> OEMs are thus welcomed additions to the 2316 technology. More interestingly, very recent studies show that 2317 efficient storage of Al in n-type OEMs is also possible. 2318 Phenanthraquinone triangle PQ- $\Delta$  uniquely stores AlCl<sub>2</sub><sup>+</sup> 2319 instead of AlCl<sub>4</sub><sup>-</sup> which basically every other decent cathode 2320 stores, hence opening up a brand new design space for Al 2321 positive electrode materials (Figure 16F).<sup>380</sup> PPDIE also seems 2322 to store cationic Al species considering it being an n-type 2323 material at the corresponding potential (0.5 V vs Al<sup>3+</sup>/Al), 2324 though more characterization would be needed to reveal the 2325 nature of the stored ions.<sup>282</sup> 2326

Overall, OEMs indeed look promising as unique enablers for 2327 the otherwise quite problematic multivalent-metal batteries, 2328 even though detailed studies regarding the ion storage mech- 2329 anism and performance improvement have only just begun. 2330

# 7.3. Comments on The Peculiar Multiple Cation Insertion Phenomenon in Organics 2331

The electrochemical process coined as "superlithiation" 2332 corresponds to a two-electron reduction of a carbon–carbon 2333

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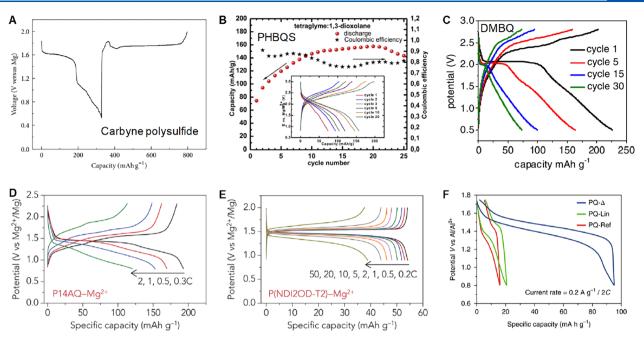


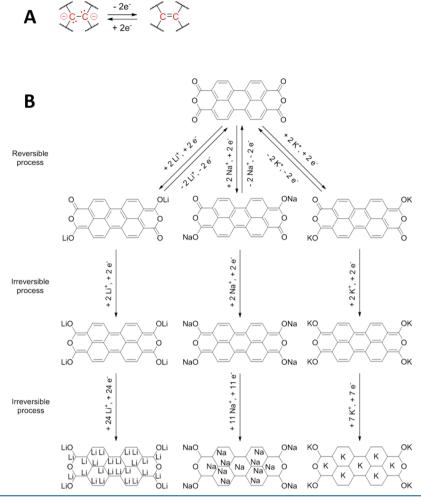
Figure 16. Voltage profiles of selected OEMs studied measured vs Mg (A–E) and Al (F). (A) Carbyne polysulfide (reproduced from ref 373), (B) PHBQS (reproduced with permission from ref 371. Copyright 2016 Elsevier Ltd.), (C) DMBQ (reproduced with permission from ref 370. Copyright 2016 The Electrochemical Society), (D) P14AQ (reproduced with permission from ref 366. Copyright 2018 Elsevier Ltd.), (E) P(NDI2OD-T2) P14AQ (reproduced with permission from ref 366. Copyright 2018 Elsevier Ltd.), and (F) PQ- $\Delta$  (reproduced with permission from ref 380. Copyright 2016 Nature Publishing Group).

2334 double bond with a concomitant uptake of two lithium ions for 2335 charge compensation (Scheme 1A). Consequently, a material 2336 with solely sp<sup>2</sup> hybridized carbons could in theory reach a 1/12337 Li/C ratio when fully reduced, allowing us to reach extremely high specific capacities. It was first established in 2012 in an article from Taolei Sun where 1,4,5,8-naphthalenetetracarboxylic dianhydride (NTCDA), a material with 4 carbonyls and 14 sp<sup>2</sup> 2340 hybridized carbons, could insert 18 lithium ions.<sup>381</sup> This work 2341 was accompanied by an NMR study which displayed partic-2342 ularly shielded <sup>1</sup>H peaks for the "superlithiated" NTCDA, 2343 matching their proposed mechanism. 2344

2345 Remarkably, some template molecules seem to be subjected 2346 to diverse multiple alkali metal ions insertions; the process is 2347 hence not limited to lithium ion uptake. For instance, 3,4,9,10-2348 perylene-tetracarboxylicacid-dianhydride (PTCDA) is able 2349 to uptake up to 28 lithium ions,<sup>381</sup> 15 sodium ions<sup>382</sup> or 11 2350 potassium ions (Scheme 1B).<sup>383</sup> It is interesting to note that 2351 the larger the radius of the concerned cation, the fewer could 2352 be inserted onto PTCDA, possibly due to steric hindrance. 2353 However, in the case of PTCDA, the mere reduction of the 2354 first two carbonyls is a reversible process, while the reduction 2355 of the last two and the "superlithiation/sodation/potation" is 2356 not. Nonetheless, over the course of the last years, many 2357 materials have been described reacting according to reversible 2358 "superlithiation" and are able to deliver specific capacities 2359 sometimes exceeding 1000 mAh g<sup>-1</sup> for hundreds of cycles.

The typical electrochemical feature of the "superlithiation" 2361 process is a sloping curve without obvious plateau requiring a 2362 large potential window to achieve high Coulombic efficiency 2363 (typically 0.05-3 V) and exhibiting a large hysteresis 2364 (polarization) sometimes exceeding 1 V (Figure 17A). Despite 2365 the attractive specific capacities obtained with these materials 2366 and the intriguing science (but still poorly understood) behind 2367 it, these electrochemical features make them of no practical 2368 use. Nevertheless, while initially believed to be connected with fused aromatic rings or to be kinetically limited, numerous 2369 examples have been described with a single<sup>260</sup> or no aromatic 2370 <sup>4</sup> and with excellent capacity at a high current rate, and 2371 ring<sup>38</sup> there is still hope for further developments of this redox 2372 process. By nature, "superlithiated" materials are typically inves- 2373 tigated as negative electrode (starting with a cation uptake). 2374 The only case of a "superlithiated" positive electrode (starting 2375 with a cation release) is lithium carbide  $Li_2C_2$ , where up to one 2376 lithium ion can be released from the structure.<sup>385,386</sup> As previ- 2377 ously mentioned, this review does not try to be exhaustive, and 2378 just a few examples will be presented here. The total amount 2379 of articles on materials which could be related to a "super- 2380 lithiation" process has exceeded 100. For the sake of 2381 clarification, OEMs containing a transition metal such as 2382 metal-organic frameworks, coordination polymers, or organo- 2383 metallic compounds have been excluded, considering that their 2384 specific capacity has a contribution from the transition metal in 2385 addition to the "superlithiation" corresponding to the organic 2386 moiety. 2387

Polyanthraquinone-triazine (PAT) is a COF using repeating 2388 units similar to COFs previously mentioned. However, unlike 2389 the other triazine-based and anthraquinone-based COFs, PAT 2390 undergoes a 17-electron reduction per repeating unit, corre- 2391 sponding to the reduction of 2 carbonyls (2 electrons), the 2392 triazine unit (3 electrons) and the 2 benzene rings of the 2393 anthraquinone moiety (12 electrons), leading to a maximum 2394 reversible capacity of 770 mAh g<sup>-1</sup> (Table 6, entry 1, and 2395 Figure 17B).<sup>387</sup> Interestingly, the capacity decreases in the first 2396 30 cycles before slowly increasing with time over 400 cycles, 2397 which has been assigned to a slow activation process. This 2398 behavior has been observed for several "superlithiated" 2399 materials, such as F-PDI-3-TC (Table 6, entry 2).<sup>388</sup> Its initial 2400 capacity is merely 95.7 mAh g<sup>-1</sup> but reaches 783 mAh g<sup>-1</sup> after 2401 1000 cycles (Figure 17C). Other examples include poly- 2402 (benzobisimidazobenzophenanthroline) (BBL) and poly(1,6- 2403) Scheme 1. (A) Electrochemical Storage Mechanism of the "Superlithiation"; (B) Multiple Cation Insertion for PTCDA



2404 dihydropyrazino[2,3g]quinoxaline-2,3,8-triyl-7-(2*H*)-ylidene-2405 7,8-dimethylidene) (PQL) that can reach up to 1 285 mAh  $g^{-1}$  and 2406 1 550 mAh  $g^{-1}$  of reversible capacity, respectively (Figure 17D, 2407 E).<sup>389,390</sup> For these last two materials, the capacity and kinetics 2408 are improved when cycled at 50 °C instead of room temperature. 2409 BBL and PQL display discharge capacities of 496 mAh  $g^{-1}$  and 2410 ca. 500 mAh  $g^{-1}$  at the 1000th cycle at a rate of 3 and 2.5 C, 2411 respectively.

2412 Briefly, "superlithiation" is a peculiar but fascinating elec-2413 trochemical process giving access to extremely high reversible 2414 capacities. However, very little is understood about it such as 2415 why some specific structures are subjected to "superlithiation" 2416 and others structurally closely related are not. But the main 2417 limitation is clearly the poor round trip energy efficiency of 2418 devices using "superlithiated" materials which, if not solved, 2419 will restrain this process to a scientific curiosity with no prac-2420 tical applications for the moment.

### 8. SOLID ORGANIC ELECTRODES FOR AQUEOUS 2421 BATTERIES

#### 8.1. Introductory Statement

2422 Although there are fewer examples in the literature concerning 2423 the use of OEMs in aqueous electrolyte, this application is of 2424 interest for developing low cost and environmentally friendly 2425 electrochemical storage solutions. Aqueous rechargeable 2426 batteries featuring low-cost and nonflammable water-based

electrolytes are intrinsically safe and do not rely heavily on 2427 battery management systems, thereby providing robustness 2428 and cost advantages over competing lithium-ion batteries that 2429 use volatile and toxic organic electrolytes. However, the state- 2430 of-the-art aqueous rechargeable batteries show short cycle 2431 life and fall short of meeting large-scale applications where 2432 frequent replacement of batteries is undesirable. This is typical 2433 of PbA batteries (200 cycles for deep cycling) where the lead 2434 electrode undergoes irreversible passivation of PbSO<sub>4</sub>. Similarly, 2435 the capacity retention of nickel-based alkaline batteries is altered 2436 by the volume variations of the electrodes on cycling. On the 2437 contrary, neutral aqueous ion rocking-chair batteries such as 2438 introduced by J. Dahn in 1994<sup>391</sup> appear more attractive in 2439 terms of cycle life due to smoother ion intercalation mech- 2440 anisms, but again, the commonly investigated chemistry was 2441 based on inorganic electrode materials; albeit, Alt et al.<sup>392</sup> 2442 reported as soon as 1972 an organic based aqueous cell using 2443 the tetrachloro-1,4-benzoquinone (TCQB) in 4 M sulfuric 2444 acid. Such a cell exhibited a redox potential of 0.67 V vs 2445 saturated calomel electrode (SCE) associated with the pro- 2446 tonation of the quinone structure. 2447

One of the intentions of the authors is to provide in this 2448 section a critical view on the latest advances and challenges 2449 in the exploration of organic based aqueous cell chemistries, 2450 including a quantified comparison of their properties against 2451 those of inorganic materials including the tricky question of 2452 the volumetric energy density. As part of this review, we feel 2453

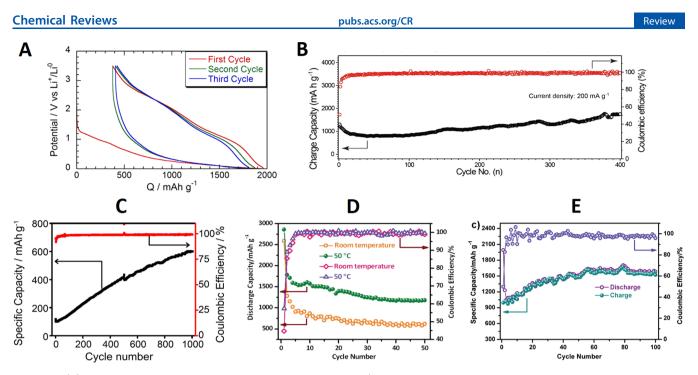


Figure 17. (A) Typical voltage profile of a "superlithiated" material:  $Li_2BDP$  (reproduced with permission from ref 260. Copyright 2016 American Chemical Society). (B–E) Capacity retention of selected OEMs: (B) PAT (reproduced with permission from from ref 387. Copyright 2018 American Chemical Society), (C) F-PDI-3-TC (reproduced with permission from ref 388. Copyright 2019 American Chemical Society), (D) BBL (reproduced with permission from ref 389. Copyright 2015 John Wiley and Sons), and (E) PQL (reproduced with permission from ref 390. Copyright 2015 John Wiley and Sons).

#	Positive electrode (or "cathode") active material	Negative electrode (or "anode")	Electrolyte	Output voltage (V)	Cycling stability: retention, cycles, rate or current density	Specific capacity (mAh g <sup>-1</sup> ) and Specific energy (Wh kg <sup>-1</sup> ) per mass of positive active material, Final coulombic efficiency, Loading (mg cm <sup>-2</sup> )	Ref.
1		Li	1 M LiPF₀ in EC/DMC	~0.9	n.d., <sup><i>a</i></sup> 400, 200 mAh g <sup>-1</sup>	1 770, 1 593, ~99, 1.1	[ <sup>387</sup> ]
2		Li	1 M LiPF6 in EC/DEC	~0.9	n.d., <sup><i>a</i></sup> 1 000, 200 mAh g <sup>-1</sup>	783, 705, ~99, n.d.	[ <sup>388</sup> ]
3		Li	1 M LiPF6 in EC/DEC	~0.9	48%, 50, 100 mAh g <sup>-1</sup>	1 285, 1 156, ~99, n.d.	[ <sup>389</sup> ]
4		Li	1 M LiPF <sub>6</sub> in EC/DEC	~0.9	n.d., <sup><i>a</i></sup> 100, 100 mAh g <sup>-1</sup>	1 550, 1 395, ~99, n.d.	[ <sup>390</sup> ]

Table 6. Performances of Selected OEMs Exhibiting the "Superlithiation" Phenomenon

<sup>*a*</sup>Due to an activation process, the capacity increases with time.

2454 it is therefore interesting to evaluate the effective chances of 2455 organics to realize user/market-acceptable aqueous batteries. 2456 In addition, we believe that such a comparison would not be 2457 complete if another bottleneck of this technology that is the 2458 price of active materials is not compared. To address these 2459 points, the latest literature data associated with the most 2460 advanced and industry relevant inorganic material for molar 2461 range aqueous battery (as opposed to water-in-salt type ones 2462 that will be briefly discussed, *vide infra*) which is the carbon 2463 coated Na(Li)Ti<sub>2</sub>(PO<sub>4</sub>)<sub>3</sub> (referred to as C@NTP or C@LTP) 2464 is considered below.

#### **Volumetric Capacity Aspect**

2465

On paper, this is not one of the most important factors for  $_{2466}$  stationary energy storage although in practice, low energy  $_{2467}$  density could also mean more layers in the stack (for a given  $_{2468}$  electrode thickness) and therefore a higher price due to a  $_{2469}$  larger amount of passive elements. The volumetric capacity of  $_{2470}$  the C@Na(Li)Ti<sub>2</sub>(PO<sub>4</sub>)<sub>3</sub> (2.6 g/cm<sup>3</sup>) can reach up to 231<sup>393</sup> –  $_{2471}$  300<sup>394</sup> mAh cm<sup>-3</sup> (93–118 mAh g<sup>-1</sup>, respectively) taking into  $_{2472}$  account the carbon coating (2.0 g·cm<sup>-3</sup>). Interestingly, such  $_{2473}$  volumetric capacities are actually lower than that obtained for a 2474

2475 quinone derivative also used on the negative side, the poly 2476 pyrene-4,5,9,10-tetraone (PPTO): 1.68 g cm<sup>-3</sup>, 338 mAh cm<sup>-3</sup>, 2477 201 mAh g<sup>-1</sup> cycled in Na<sup>+</sup>-based aqueous electrolyte.<sup>395</sup> 2478 Although the PPTO electrode contained 30 wt.% of carbon 2479 additive its electrode volumetric capacity (144 mAh cm<sup>-3</sup>) 2480 remains in the vicinity of that derived for the titanium 2481 phosphate ones: 121 mAh cm<sup>-3</sup>, ref 393 and 152 mAh cm<sup>-3</sup>, 2482 ref 394. It is also important to point out that the previous 2483 results were obtained from relatively thin electrodes with areal 2484 capacity in the vicinity or below 1 mAh cm<sup>-2</sup>.

For thicker ones (close to 2 mAh cm<sup>-2</sup>), Y. M. Chiang's 2485 2486 group<sup>396</sup> obtained 310 mAh cm<sup>-3</sup> by volume of C@NTP at 2487 0.6 C, which turns into 161 mAh cm<sup>-3</sup> by volume of composite 2488 electrode. Industrially relevant aqueous batteries were dem-2489 onstrated by Whitacre with impressive electrode loadings (between 20 and 450 mg·cm<sup>-2</sup>) using NTP derived from very 2491 cheap synthesis protocols.<sup>397</sup> These good results pair, however, 2492 with a lower volumetric capacity of the C@NTP material 2493 (182 mAh cm<sup>-3</sup> in approximately 20 mAh cm<sup>-2</sup> pouch cells 2494 and 159 mAh cm<sup>-3</sup> in approximately 1 mAh cm<sup>-2</sup> coin cells<sup>397</sup>) 2495 which falls down to 83 and 77 mAh cm<sup>-3</sup> in terms of electrode 2496 volume for pouch and coin cells, respectively, using the 2497 corresponding electrode chemistry. In comparison, the highest <sup>2498</sup> areal capacity demonstrated with organic materials lies in the <sup>2499</sup> vicinity of 4.5 mAh cm<sup>-2,232,398</sup> Indeed, Perticarari et al.<sup>232</sup> 2500 achieved nearly 100 mAh cm<sup>-3</sup> of material and 66 mAh cm<sup>-3</sup> 2501 of electrode using a diblock oligomer and 25 wt.% of carbon 2502 additive for 4.5 mAh cm<sup>-2</sup> while Nishide's group obtained 2503 3 mAh cm<sup>-2</sup> using on a carbon nanotube hybridized poly 2504 (2,2,6,6-tetramethylpiperidin-4-yl) acrylamide (PTAm) polymer.<sup>35</sup> To sum up, this short literature analysis of both inorganic 2505 2506 and organic active materials for aqueous batteries near neutral 2507 pH highlights that some of the proposed organic electroactive 2508 materials have already surpassed inorganic ones in term of 2509 volumetric capacity in the case of thin electrodes and are not 2510 too far behind in the case of thick ones.

## 2511 Cost Aspect

2512 According to Whitacre,<sup>397</sup> NTP can be produced with pre-2513 cursor materials cost of \$4 per kg upon two synthesis steps, ball 2514 milling and calcination. Taking 5/kg/step, which is an average 2515 in the pigment industry, an estimate of the NTP price should 2516 be roughly 14\$/kg. In comparison, competitive organic 2517 materials (in terms of volumetric capacity) in neutral molar 2518 aqueous media such as PNDI and PPTO are approximately 2519 \$4–6/kg and \$10–15/kg, respectively, highlighting similar or 2520 even lower prices can indeed be achieved for organics.

Lastly, it is noted that water-in-salt (WiSE)<sup>399</sup> or hydrate-2521 2522 melt<sup>400</sup> electrolytes have emerged as interesting opportunities 2523 to significantly improve the energy density and the Coulombic 2524 efficiency and mitigate corrosion issues (materials, current 2525 collectors, ...) of these new classes of "water containing" 2526 batteries. A comprehensive and critical review of the scientific 2527 understanding as well as the electrochemical and physical 2528 properties of these new electrolytes has been recently 2529 published by Yamada et al.<sup>401</sup> It is noted that the ability of 2530 WiSE electrolytes to extend the electrochemical window can 2531 be significantly improved by using an immiscible electrolyte 2532 additive, the 1,1,2,2-tetrafluoroethyl-2',2',2'-trifluoroethyl 2533 ether (HFE). The latter electrochemically decomposes at the 2534 surface of the materials and by virtue of its hydrophobicity 2535 expels water molecules from the inner-Helmholtz interface of 2536 the electrode thereby mitigating hydrogen formation at the

expense of a more efficient SEI.<sup>402</sup> Because, some articles 2537 commented in this review refer to these types of electrolytes, 2538 we feel that a few general comments should be recalled 2539 regarding this type of battery chemistry. First, such highly 2540 concentrated electrolytes have a volumetric density in the range 2541 of 1.6-1.9 g cm<sup>-3</sup>, which partially offsets the gain in energy 2542 density. For instance the mass of a 700 cm<sup>2</sup> stack cell such as 2543 presented in ref 232 (taking 5 mAh cm<sup>-2</sup> electrodes of 580  $\mu$ m- 2544 thick and 40% porosity) increases by 14% considering a WiSE 2545 electrolyte of 1.7 g cm<sup>-3</sup> compared to a "salt in water" 1 M one. 2546 Second, the viscosity of these electrolytes is approximately ten 2547 times higher than molar range ones which considerably 2548 increases the wetting time of the electrodes and especially 2549 thick ones.<sup>401</sup> Last but not least, the price of these electrolytes 2550 is obviously the most challenging issue to be overcome before 2551 commercialization can be considered. Indeed, recent results 2552 point to the fact that expensive imide based anions (as 2553 opposed for instance to acetate ones) would have a significant 2554 role in the widening of the electrochemical window on the 2555 negative electrode side.<sup>403</sup> 2556

Based on the previous comments, this section aims at providing 2557 the reader with a selection of relevant organic materials, that is to 2558 say those that allow performances approaching or higher than 2559 lead acid battery ones but with much extended cyclability. 2560 Accordingly, the lower limits were set to roughly 30 Wh kg<sup>-1</sup> 2561 per mass of the two materials and a capacity retention >80% 2562 after 500 cycles at 1 C rate or equivalent. The intention of the 2563 authors is to give a critical view of the selected papers and also 2564 to highlight advantages and drawbacks vs those associated 2565 with inorganic materials. Key performances are reported in 2566 (Table 7) along with materials structures, aqueous electrolyte 2567 formulations, cycling conditions and electrode loading. Note 2568 that this critical review is focused on neutral pH batteries 2569 because they inherently offer reduced production costs and 2570 mitigated corrosion issues. Results are subcategorized into 2571 hybrid cells, where only one of the electrodes contains an 2572 organic electroactive material and all organic cells. 2573

### 8.2. Hybrid Organic-Inorganic Batteries

8.2.1. Aqueous Lithium-Ion Batteries (ALIBs). Some of 2574 the most attractive organic materials for aqueous battery to date 2575 are among the polyimide derivatives. These materials indeed 2576 combine both a high capacity (typically 130–160 mAh  $g^{-1}$ , 2577  $208-256 \text{ mAh cm}^{-3}$ ) and a low price ( $\$4-6/kg^{395}$ ). To our 2578 knowledge such a dual advantage has not been reached by any 2579 inorganic materials used in the aqueous battery field. The 2580 electrochemical reduction/oxidation of a polyimide core is 2581 highly reversible in water at neutral pH. The redox centers 2582 have been identified as involving the aromatic-carbonyl system 2583 of the imide functional moiety following two redox steps. The 2584 first one corresponds to the formation of a radical-anion upon 2585 enolization of a carbonyl group by one electron, followed by a 2586 second electron reduction into the dianion quinoid form.<sup>404</sup> 2587 Further reduction cannot be reached in molar range elec- 2588 trolyte at neutral pH before water hydrolysis is triggered. The 2589 delocalization of excess electron density in the reduced states 2590 has been studied by FTIR and UV-vis spectroscopy.<sup>405</sup> Dong 2591 et al.<sup>406</sup> introduce a mixed liquid/solid cationic rocking chair 2592 aqueous battery using a  $I_3^{-}/I^{-}$  based posolyte and a polyimide 2593 derivative negative electrode (poly(1,4,5,8-naphthalenetetra- 2594 carboxylic)dianhydride-derived polyimide, PNTCDA) separated 2595 by a Nafion membrane allowing the Li<sup>+</sup> (or Na<sup>+</sup>) diffusion. This 2596 system delivers roughly 35 000 deep cycles at a high current of 2597 pubs.acs.org/CR

Review

#	Cell configuration (ionic carriers)	Positive electrode (or "cathode") active material	Negative electrode (or "anode") active material	Electrolyte	Output voltage (V)	Cycling stability: retention, cycles, rate or current density	Specific capacity (mAh g <sup>-1</sup> ), Specific energy (Wh kg <sup>-1</sup> )	Ref.
			Hybrid organic/inorga	nic aqueous	systems			
1	Li <sup>+</sup> (or Na <sup>+</sup> )	Is"/I"	$\left\{ \begin{array}{c} 0 \\ N \\ 0 \end{array} \right\} $ $\left\{ \begin{array}{c} 0 \\ N \end{array} \right\} $ $\left\{ \begin{array}{c} 0 \\ $	LiNO3 1 M (pH 7)	~0.7-0.8	80%, 35 000, 10 A g <sup>-1</sup> ,	~110, <sup><i>a</i></sup> ~88, <sup><i>a</i></sup> ~100, 1	[ <sup>406</sup> ]
2	Li*- ion	LiMn <sub>2</sub> O <sub>4</sub>		Li <sub>2</sub> SO <sub>4</sub> 2.5 M (pH 7)	1.13	80%, 3 000 (3 500 h), 280 mA g <sup>-1</sup>	81, <sup>b</sup> 92, <sup>b</sup> 92%, -, 2	[ <sup>395</sup> ]
3	K+	$K_{s}Fe_{s}Mn_{1-y}[Fe(CN)_{6}]_{w}\cdot zH_{2}O$	$\left( \begin{array}{c} 0 \\ 0 \\ 0 \end{array} \right) \left( \begin{array}{c} 0 \end{array} \right) \left( \begin{array}{c} 0 \\ 0 \end{array} \right) \left( \begin{array}{c} 0 \end{array} \right) \left$	KCF3SO3, 22 M	1.27	73%, 2 000, 4 C	$63, {}^{b}80, {}^{b}\sim 100, 5-6$ all these values are at 0.5 C	[ <sup>411</sup> ]
4	Zn <sup>2+</sup>	ŶÇŶŢ	Zn	Zn(CF <sub>3</sub> SO <sub>3</sub> ) <sub>2</sub> 3 M	1	87%, 1 000, 500 mA g <sup>-1</sup>	197, <sup><i>c</i></sup> 80, <sup><i>d</i></sup> ~100, 2.5-10	[ <sup>412</sup> ]
5	Mg <sup>2+</sup>	Na14Ni13Fe(CN)6·5H2O	$\left\{ \begin{array}{c} 0 \\ 0 \\ 0 \\ 0 \end{array} \right\} $ $\left\{ \begin{array}{c} 0 \\ 0 \\ 0 \\ 0 \\ 0 \end{array} \right\} $ $\left[ \begin{array}{c} 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 $	MgSO4 1 M	1.3	57, 5 000, 2 A g <sup>-1</sup>	35, <sup>b</sup> 45, <sup>b</sup> ~100, 2-3, all these values are at 0.5 A g <sup>-1</sup>	[ <sup>413</sup> ]
5	$\mathrm{Mg}^{2+}$	$\mathrm{Li}_{3}\mathrm{V}_{2}(\mathrm{PO}_{4})_{3}@\mathrm{C}$		Mg(TFSI)2 4 m	1.9	87%, 1 000, 2 C	52, <sup>b</sup> 62.4, <sup>b</sup> ~100, 2-3, all these values are at 1C (0.1 A g <sup>-1</sup> )	[ <sup>414</sup> ]
,	Ca <sup>2+</sup>	$K_{0.02}Cu[Fe(Cu)_6]_{0.66}\cdot 3.7H_2O$	$\left\{ \begin{array}{c} 0 \\ N \\ 0 \end{array} \right\} $ $\left\{ \begin{array}{c} 0 \\ N \end{array} \right\} $ $\left\{ \left\{ \begin{array}{c} 0 \\ N \end{array} \right\} \right\} $ $\left\{ \left\{ \begin{array}{c} 0 \\ N \end{array} \right\} $ $\left\{ \left\{ \begin{array}{c} 0 \\ N \end{array} \right\} \right\} $ $\left\{ \left\{ \begin{array}{c} 0 \\ N \end{array} \right\} \right\} $ $\left\{ \left\{ \begin{array}{c} 0 \\ N \end{array} \right\} $ $\left\{ \left\{ \begin{array}{c} 0 \\ N \end{array} \right\} \right\} $ $\left\{ \left\{ \begin{array}{c} 0 \\ N \end{array} \right\} \right\} $ $\left\{ \left\{ \begin{array}{c} 0 \\ N \end{array} \right\} $ $\left\{ \left\{ \begin{array}{c} 0 \\ N \end{array} \right\} \right\} $ $\left\{ \left\{ \left$	Ca(NO <sub>3</sub> ) <sub>2</sub> 2.5 M (pH 5.1)	1.2	88, 1 000, 10 C	$45, {}^{b}54, {}^{b}\sim 100, 5$ , all these values are at 1 C	[ <sup>415</sup> ]
3	NH4 <sup>+</sup> - ion	(NH4)1.47Ni[Fe(CN)6]0.88	HN H	(NH4)2SO4 1 M (pH 6)	1	67%, 1 000, 0.120 mA g <sup>-1</sup>	35, <sup>b</sup> 43, <sup>b</sup> 97.6%, 2-5	[ <sup>416</sup> ]
			All-organic aqu	ieous system	15			
•	Cl <sup>.</sup> - ion			NaCl 0.1 M (pH 7)	1.3	80%, 2 000, 10.5 A g <sup>-1</sup>	165, <sup><i>a</i></sup> 214, <sup><i>a</i></sup> - (100 nm to 1 μm thin films)	[ <sup>418</sup> ]
0	BF4 <sup>°</sup> - ion		$ \begin{array}{c} & & \\ & & $	NaBF4 0.1 M (pH 7)	1.2	75-80%, >2 000, 60 C (67 μA·cm <sup>-2</sup> )	104, <sup>C</sup> 108, <sup>C</sup> 95 (100 nm thin films)	[ <sup>419</sup> ]
1	Dual-ion (TFSI <sup>-</sup> /Li <sup>+</sup> )		$\left\{ \begin{array}{c} 0 \\ 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \end{array} \right\} = \left\{ \begin{array}{c} 0 \\ 0 \end{array} \right\} = \left\{ \left\{ \begin{array}{c} 0 \\ 0$	LiTFSI 21 m (pH 7)	1	85%, 700, 0.5 A g <sup>-1</sup>	105, <sup>c</sup> 53, <sup>c</sup> ~100, 1	[ <sup>420</sup> ]

# Table 7. Performances of Selected Aqueous Organic Batteries

### **Chemical Reviews**

Table 7. continued

Cycling Cell Output stability: configuration Specific capacity (mAh g-1) Positive electrode (or Negative electrode (or "anode") active voltage retention, Ref Electrolyte (ionic Specific energy (Wh kg-1) "cathode") active material material cycles, rate or (V)carriers) current density Mixed dual 70%, 1680 and anionic NaClO<sub>4</sub>  $33^b$ ,  $36^b$ , >99.6, all these values [<sup>231</sup>] 12 1.1 (1100 h), 0.075 rocking-chair 2.5 M (pH 7) to 0.6 A gare at 0.075 A g<sup>-1</sup>, 10 (ClO4<sup>-</sup>/Na<sup>+</sup>) Mixed dual and anionio NaClO<sub>4</sub> 97%, 500 h 35,<sup>b</sup>28,<sup>b</sup>~100, 85 (4.5 mAh cm<sup>-2</sup>) 13 0.8 [232] rocking-chair 0.075 A g M (pH 7 (ClO4-/Na+)

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<sup>*a*</sup>Based on anode material weight. <sup>*b*</sup>Based on cathode and anode materials weight. <sup>*c*</sup>Based on cathode material weight. <sup>*d*</sup>Based on the whole cell weight.

2598 10 A  $g^{-1}$  (55 C nominal, that leads to a nominal ratio (number 2599 of cycles/C-rate) = 636) before reaching 80% of the initial 2600 capacity ( $Q_0 = 105 \text{ mAh g}^{-1}$ ) (Table 7, entry 1). More recently, another negative electrode organic material 2601 2602 was shown to stand out of the crowd, the quinone derivative 2603 PPTO.<sup>395</sup> The latter exhibits storage properties rivaling those 2604 of any inorganic materials from mildly acidic to strongly basic 2605 media. In neutral 2.5 M Li<sub>2</sub>SO<sub>4</sub> aqueous electrolyte, this  $_{2606}$  material enables 92 Wh  $kg^{-1}{}_{materials}$  (208 Wh  $L^{-1})$  when paired  $_{2607}$  with LiMn<sub>2</sub>O<sub>4</sub> at an average voltage of 1.13 V (Table 7, entry 2). 2608 This performance is in the same range as the competing system  $_{2609}$  LiTi<sub>2</sub>(PO<sub>4</sub>)<sub>3</sub>-LiMn<sub>2</sub>O<sub>4</sub> (90 Wh kg<sup>-1</sup><sub>materials</sub> (243 Wh L<sup>-1</sup>, 1.5 V) 2610 thanks to the extremely high capacity of the PPTO electrode 2611 material (229 mAh g<sup>-1</sup>, 366 mAh cm<sup>-3</sup> at 1 C rate). In addition, 2612 this PPTO-based cell shows quite a promising capacity retention 2613 of more than 3500 h (3000 cycles) (Figure 18). Among all 2614 aqueous systems that have been reviewed herein, PPTO/ 2615 LiMn<sub>2</sub>O<sub>4</sub> is by far the most promising one in the authors' 2616 opinion. In addition, as a quinone derivative, the fully reduced  $_{2617}$  form of PPTO (PPTO-Li<sub>4</sub>) can support reversible oxidation by 2618 dissolved oxygen without impacting its charge-discharge 2619 properties.<sup>395</sup> This is an important advantage over  $LiTi_2(PO_4)_3$ 2620 for instance, which was shown to undergo rapid capacity fading 2621 in nondeaerated electrolyte. Indeed, PPTO based cell can 2622 therefore support the "oxygen cycle" (Figure 18), which is a 2623 built-in safety mechanism for aqueous battery at high charge 2624 states. Importantly, in such events the local pH at the negative 2625 electrode can be fairly alkaline (pH 13). However, thanks to 2626 the combination of the chemical inertness of the quinone core, 2627 as well as the poor solubility, and robust amide linkage of the 2628 PPTO derivative, a capacity retention of 83% was demonstrated 2629 after 1200 h cycling in these pH conditions.<sup>395</sup> Accordingly, this 2630 oxygen consumption capability of quinones enables in principle, 2631 to increase the state of charge of the positive electrode material (such as  $LiMn_2O_4$  for instance) without significantly altering the 2632 2633 mass balancing of the cell therefore paving the way toward the 2634 use of materials working at even higher potentials.

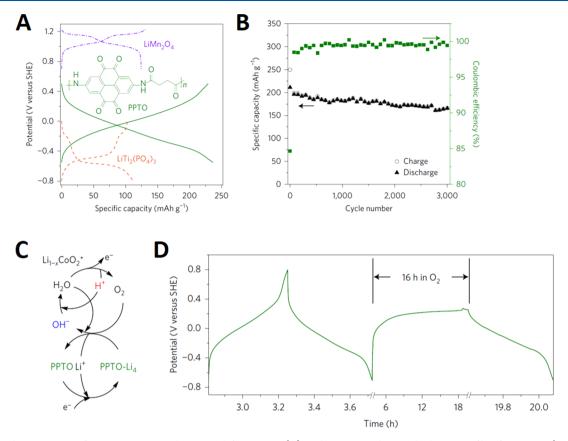
**8.2.2. Aqueous Sodium-Ion Batteries (ASIBs).** As for 2636 Li-ion batteries, Na-based aqueous batteries must be 2637 investigated to counteract possible upcoming issues associated 2638 with geo-localized Li resources. One of the first instances of 2639 hybrid ASIBs bearing an organic electroactive material uses a

polyimide derivative PNDI at the negative electrode and a 2640 NaVPO<sub>4</sub>F based positive electrode in a 5 M NaNO<sub>3</sub> aqueous 2641 electrolyte.<sup>404</sup> This system shows, however, a very poor capacity 2642 retention (-25% in 20 cycles) that was mainly ascribed to 2643 NaVPO<sub>4</sub>F (-30% loss of capacity in 20 cycles) compared to 2644 -17% for PNDIE.<sup>404</sup> Yao's group<sup>395</sup> slightly improved these 2645 cyclability results to nearly 80% of capacity retention after 2646 80 cycles (150 h) by substituting  $Na_3V_2(PO_4)_3$  for  $NaVPO_4F_{2647}$ and PPTO (208 mAh  $g^{-1}$ ) for PNDIE (160 mAh  $g^{-1}$ ). To 2648 date, ASIB hybrid aqueous batteries are therefore not compet- 2649 itive with corresponding ALIB as reported above especially in 2650 terms of capacity retention. For this reason, ASIB related research 2651 has mainly focused on the use of inorganic compounds<sup>173</sup> such as 2652 NaFePO<sub>4</sub><sup>407</sup> as well as fully inorganic systems based on 2653 Prussian (white)blue,<sup>408</sup> carbon coated phosphates (NTP<sup>397</sup> and 2654  $Na_3MnTi(PO_4)_3^{,409}$  and manganese oxides  $Na_{0.44}MnO_2^{,396}$  and  $_{2655}Na_{0.44}[Mn_{1-x}Ti_x]O_2^{,410}$  We note however, that all these materials  $_{2656}$ enable capacity values in the range of 40 to 60 mAh  $g^{-1}$  and 2657 energy density values in the range of 30-40 Wh kg<sup>-1</sup> per mass of 2658 materials in molar range electrolyte which is the average value 2659 generally observed for most organic based aqueous cells. 2660

Review

8.2.3. Aqueous Potassium-Ion Batteries (AKIBs). Full 2661 organic-inorganic hybrid AKIBs have not been reported until 2662 very recently owing to the scarcity of suitable electroactive 2663 materials and electrolytes. Hu's group<sup>411</sup> demonstrated an 2664 AKIB cell based on an Fe-substituted Mn-rich Prussian blue 2665  $K_rFe_rMn_1 = \sqrt{Fe(CN)_6} = \frac{1}{2} \cdot \frac{1}{2$ electrode and the 3,4,9,10-perylenetetracarboxylic diimide 2667 derivative as the negative one in a 22 M KCF<sub>3</sub>SO<sub>3</sub> water-in- 2668 salt electrolyte (Table 7, entry 3). The low water activity of the 2669 latter allowed not only to mitigate dissolution of both electrode 2670 materials but also to charge the positive electrode up to 1.2 V 2671 vs Ag/AgCl electrode, which allowed KFeMnHCF to 2672 reversibly reach 135 mAh  $g^{-1}$  at 0.5 C above 0 V vs SCE. In 2673 addition, thanks to the mitigation of phase transitions by Fe 2674 substitution, KFeMnHCF achieves 70% capacity retention at 2675 100 C over 10 000 cycles. This pioneering AKIB system shows 2676 a high energy density of 80 Wh kg<sup>-1</sup> by mass of the two 2677 electrodes at a power density of 41 W kg<sup>-1</sup> (0.5 C) and 73%  $_{2678}$ capacity retention over 2000 cycles at 4 C (Figure 19A-C) 2679 which makes it one of the most attractive systems to date. 2680 Interestingly, authors have evaluated their system in pouch cell 2681

Review



**Figure 18.** Characteristics of PPTO as an anode material for ALIBs. (A) Galvanostatic charge–discharge profiles for PPTO (280 mA  $g^{-1}$ ), LiTi<sub>2</sub>(PO<sub>4</sub>)<sub>3</sub> (120 mA  $g^{-1}$ ), and LiMn<sub>2</sub>O<sub>4</sub> (140 mA  $g^{-1}$ ) in 2.5 M Li<sub>2</sub>SO<sub>4</sub> (pH 7). (B) Capacity retention of a LiMn<sub>2</sub>O<sub>4</sub>–PPTO cell during galvanostatic cycling at 1 C in 2.5 M Li<sub>2</sub>SO<sub>4</sub> (pH 7). (C) Schematic explaining the oxygen cycle in ALIBs: H<sub>2</sub>O is oxidized at the catalytic sites (\*) on the cathode (for example, LiCoO<sub>2</sub>) to generate O<sub>2</sub> and HC; the latter is then reduced by the charged anode (for example, PPTO-Li<sub>4</sub>) to afford OH<sup>-</sup>. (D) Oxygen consumption by charged PPTO: a PPTO electrode is first electrochemically discharged (oxidized) and charged (reduced) under Ar for one cycle, then left to rest under O<sub>2</sub>, and finally put under Ar and charged again. Reproduced from ref 395. Copyright 2017 Nature Publishing Group.

2682 configuration and at several temperatures to better grasp the 2683 prospect of large-scale applications: an 11 mAh pouch cell was 2684 shown to exert superior performance at low rates (i.e., 0.5 C/0.1 C) 2685 and low/high temperatures (i.e., -20 °C/-10 and 25 °C/60 °C) 2686 and was able to operate from -20 to  $60 \degree C$  (Figure 19 D,E). 8.2.4. Aqueous Multivalent Metal-Ion Batteries (Mg, 2687 **Ca**, **Zn**).  $Zn^{2+}$ . Chen's group demonstrated that high energy 2688 2689 values could be obtained at the cell level (pouch cell) by 2690 pairing quinones (calix[4]quinone, referred to as C4Q) to a <sup>2691</sup> zinc negative electrode in a 3 M  $(ZnCF_3SO_3)_2$  aqueous <sup>2692</sup> electrolyte (Table 7, entry 4).<sup>412</sup> This system develops 1 V as output voltage and up to  $337 \text{ mAh g}^{-1}$  by mass of materials at 2693  $_{2694}$  low current density (5 mA g<sup>-1</sup>). The pouch cell achieved 220 <sup>2695</sup> Wh kg<sup>-1</sup> at 500 mA g<sup>-1</sup> considering the electroactive mass <sup>2696</sup> fraction of the materials (which are 89% for the C4Q and 49%  $_{2697}$  for Zn) and 80 Wh g<sup>-1</sup> by mass of the whole cell with an 2698 energy efficiency close to 80%. However, due to the dissolution 2699 of the C4Q, a Nafion membrane was required to stabilize the 2700 capacity retention at 87% after 1000 cycles (-0.015%/cycle). 2701 It is instructive to note that although the development of mild 2702 electrolyte based Zn batteries is still in its infancy, this kind of 2703 system clearly brings energy densities in the same order as 2704 those associated with the use of "water-in-salt" electrolytes. 2705 This point should therefore motivate more research in the near 2706 future to enhance the depth of discharge and cyclability and 2707 prevent the use of membranes.

 $Mq^{2+}$ . Xia et al.<sup>413</sup> recently developed a 33 Wh kg<sup>-1</sup> (1 V as 2708 output voltage) per mass of active materials considering 2709  $Na_{1,4}Ni_{1,3}Fe(CN)_{6,5}H_2O$  paired with poly[N,N'-(ethane-1,2-2710) diyl)-1,4,5,8-naphthalene tetracarboximide (PNDIE) using 1 M 2711 MgSO<sub>4</sub> aqueous electrolyte (Table 7, entry 4). This assembly 2712 allowed to achieve 1000 cycles at 2 C rate while keeping 2713 approximately 88% of the initial capacity. Interestingly, Wang 2714 et al.<sup>414</sup> obtained nearly two times more energy density 2715 (62.4 Wh kg<sup>-1</sup> per mass of materials) using  $Li_3V_2(PO_4)_{31}$  as the 2716 positive electrode and lighter diimide derivatives (polypyromel- 2717 litic dianhydride), as the negative electrode (Table 7, entry 6). 2718 Compared to the more often used naphthalene derivative, 2719 the smaller delocalization backbone of the polypyromellitic 2720 destabilizes the radical anion and dianions that form on reduc- 2721 tion and push the potential to lower values. The cell shows 2722 indeed a high voltage of 1.9 V which can be realized by using a 2723 relatively concentrated electrolyte (4 M Mg(TFSI)<sub>2</sub>).<sup>414</sup> This 2724 resulted in a promising capacity retention of nearly 87% after 2725 1000 cycles at 2 C rate. 2726

 $Ca^{2+}$ . Ca<sup>2+</sup> is another interesting abundant ion to play with 2727 in aqueous media. Yao's group<sup>415</sup> recently showed that the 2728 diffusion of Ca<sup>2+</sup> is higher than that of Mg<sup>2+</sup> both in the solid 2729 state and in the aqueous electrolyte media. These results were 2730 ascribed to smaller size of the hydrated Ca<sup>2+</sup> complex and its 2731 more facile dehydration during the charge transfer process. 2732 This group assembled a battery with a copper hexacyanoferrate 2733

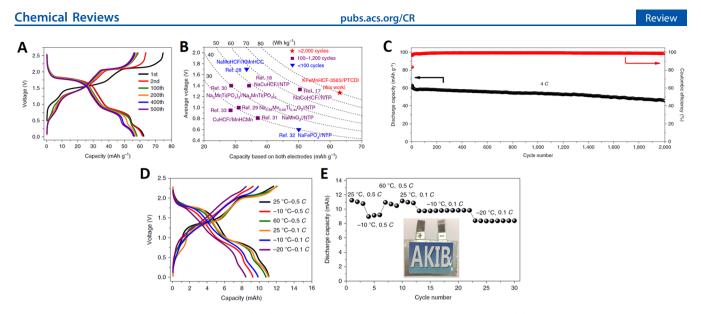


Figure 19. Performance of the K<sub>1.85</sub>Fe<sub>0.33</sub>Mn<sub>0.67</sub>[Fe(CN)<sub>6</sub>]<sub>0.98</sub>·0.77H<sub>2</sub>Ol22 M KCF<sub>3</sub>SO<sub>3</sub>|PTCDI full battery. (A) Charge–discharge curves for coin cells at 4 C from 0 to 2.6 V (1 C = 0.13 A g<sup>-1</sup>). (B) Comparison of average voltage, capacity based on total mass of both electrodes, lifespan, and energy density for the full battery with reported aqueous Na-ion full batteries. (C) Long-term cycling performance of the coin cell at 4 C. (D, E) Corresponding electrochemical performance measured in pouch cell at different rates (0.5/0.1 C) and temperatures (-20/-10/25/60 °C). Reproduced with permission from ref 411. Copyright 2019 Nature Publishing Group.

2734 compound of composition  $K_{0.02}Cu[Fe(Cu)_6]_{0.66} \cdot 3.7H_2O$ 2735 (CuHCF) coupled to the PNDIE polyimide derivative in a 2736 2.5 M  $Ca(NO_3)_2$  aqueous electrolyte (Table 7, entry 7). 2737 CuHCF was found to proceed to insertion/deinsertion of 0.3 2738 Ca<sup>2+</sup> ion at a 0.2 C through a single-phase solid solution 2739 reaction rate at a potential of 0.72 V vs Ag/AgCl electrode. 2740 This mechanism which is paired with the  $Fe^{3+}/Fe^{2+}$  electroactivity  $_{\rm 2741}$  leads to a specific capacity of 58 mAh  $g^{-1}$  (theoretical capacity 2742  $Q_{\rm th} = 65 \text{ mAh g}^{-1}$ ) that retains 88% of its initial capacity after 2743 2000 cycles at 5 C. On the other hand, PNDIE fully reacts with 2744 Ca<sup>2+</sup> at -0.45 V vs Ag/AgCl electrode with a reversible capacity 2745 of 160 mAh g<sup>-1</sup> (theoretical capacity  $Q_{th} = 183$  mAh g<sup>-1</sup>). 2746 At 1 C rate, the full cell delivered 54 Wh kg<sup>-1</sup> of active materials 2747 for an output voltage of 1.2 V. In addition, the battery still 2748 provides 88% capacity retention after 1000 cycles at 10 C.

8.2.5. Aqueous Ammonium-Ion Battery. Little is 2749 2750 reported with ammonium as shuttling ion. However, it must 2751 be mentioned that Ji and co-workers<sup>416</sup> reported such an 2752 aqueous battery using Ni-based Prussian white at the positive 2753 electrode paired with 3,4,9,10-perylenetetracarboxylic diimide 2754 using 1 M (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> as electrolyte (pH 6) (Table 7, entry 8). 2755 This cell enables up to 43 Wh kg<sup>-1</sup> per mass of active materials 2756 with 1 V of voltage at 1.5 C and achieves a capacity retention  $_{2757}$  of 67% upon 1000 cycles at 3 C rates (120 mA g<sup>-1</sup>) with an 2758 average Coulombic efficiency of 97.6%.

## 8.3. All-Organic Aqueous Batteries

2759 Due to the lack of high potential n-type organic materials,<sup>417</sup> 2760 cation-rocking chair cells have not been reported yet. Today, 2761 all-organic aqueous cell electrochemistry is indeed either related 2762 to counteranions or both countercation and anions (one at 2763 each electrode referred to as "dual mode" and the two at one 2764 electrode referred to as "intermixed mode"). First reports were 2765 released by Nishide, Oyaizu, and co-workers.<sup>418</sup> They used a 2766 redox polymer resulting from the attachment of a (2,2,6,6-2767 tetramethylpiperidin-1-yl)oxy known as "TEMPO" side groups 2768 to a polyalkane chain backbone, with poly (2,2,6,6-2769 tetramethylpiperidin-4-yl) acrylamide (referred to as PTAm) 2770 as the positive electrode material. This material was paired to

two different polyviologen derivatives, either the highly cross- 2771 linked polyviologen hydrogel (poly tripyridiniomesitylene)<sup>418</sup> 2772 which enabled ~1.3 V as output voltage (Table 7, entry 9) or 2773 the poly(N-4,4'-bipyridinium-N-decamethylene dibromide) 2774 (Table 7, entry 10) leading to a cell average voltage of 1.2 V.<sup>419</sup> 2775 Although both cells demonstrated more than 2000 cycles in 0.1 M 2776 Na-based aqueous electrolytes, electrodes were thin film deposits 2777 in the sub- to micron-thick range. Recently however, this group<sup>398</sup> 2778 has made decisive advances by demonstrating a thick composite 2779 electrode made of PTAm with a loading of 3 mAh  $cm^{-2}$ . The 2780 latter was obtained by hybridizing PTAm with a 3-D self- 2781 assembled mesh of single-walled carbon nanotubes (SWNT). 2782 This thick electrode could still reach nearly 80 mAh g<sup>-1</sup> of 2783 material at 10 C rate. Although SWNT represents only 1% of 2784 the total electrode mass, it is noteworthy that authors demon- 2785 strated the importance of the contacts with the current 2786 collectors by showing such a high kinetics also stems from the 2787 optimization of the current collector/electrode contacts.<sup>398</sup> 2788

Dong et al.<sup>420</sup> cycled a p-type conjugated tertiary poly 2789 triphenylamine obtained by oxidative polymerization of the 2790 triphenylamine (PTPAn). The latter shows a sloppy discharge 2791 profile resulting from the superimposition of two pairs of broad 2792 peaks centered at 0.2 and 0.8 V vs SCE associated with the 2793 para and meta conformational isomers. Overall the discharge of 2794 this compound enables approximately 105 mAh  $g^{-1}_{\ PTPAn}$  at 2795  $0.5 \text{ A g}^{-1}$  (4.6 C-rate). However, the strong oxidative power of 2796 the N<sup>+</sup> species triggers the hydrolysis of water molecules that 2797 could be mitigated by the use of a "water-in-salt" electrolyte 2798 of 21 m LiTFSI. PTPAn was then coupled to 1,4,5,8- 2799 naphthalenetetracarboxylic dianhydride-derived polyimide 2800 (PNTCDA) as the negative electroactive material (Table 7, 2801 entry 11). During charge TFSI<sup>-</sup> and Li<sup>+</sup> react with the oxidized 2802 PTPAn and reduced PNTCDA, respectively (dual mode), 2803 enabling a maximum of 53 Wh kg<sup>-1</sup> per mass of electroactive 2804 materials and a capacity retention of 85% after 700 cycles at 2805 0.5 A  $g^{-1}$  (4.6 C-rate).<sup>420</sup> 2806 Some of us reported a possible new avenue to design 2807

aqueous batteries materials based on diblock-oligomers bearing 2808

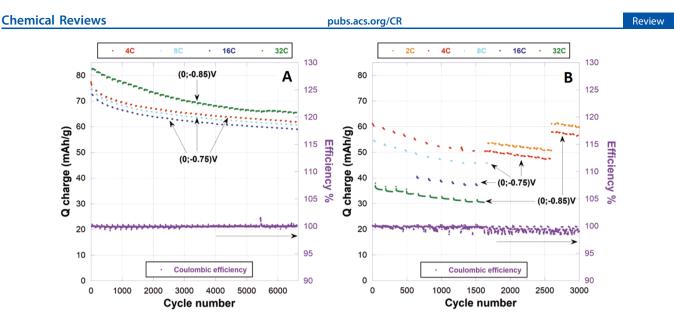


Figure 20. Capacity retention on charge (oxidation of the material) and corresponding Coulombic efficiency curves for diblock-oligomers bearing p-type viologen and n-type naphthalene diimide moieties composite electrodes in (A) 2.5 M NaClO<sub>4</sub> aqueous electrolyte and (B) ocean water. Reproduced with permission from ref 231. Copyright 2019 John Wiley and Sons.

2809 p-type viologen and n-type naphthalene diimide moieties. These 2810 types of structures enable simultaneous release and uptake of <sup>2811</sup> anions (ClO<sub>4</sub><sup>-</sup>, Cl<sup>-</sup>) and cations (Na<sup>+</sup>, Mg<sup>2+</sup>) respectively by a 2812 single electrode (intermixed mode) with the promise of mitigated volume variations on cycling.<sup>230</sup> The best performances were 2813 obtained using an oligomer that can reach up to 105 mAh g<sup>-1</sup> per 2814 mass of material and 80 mAh  $g^{-1}$  per mass of electrode.<sup>231</sup> The extremely fast kinetics of longer diblock oligomer also allowed to 2815 2816 2817 reach an unmatched specific capacity of 60 mAh  $g^{-1}_{electrode}$ (0.7 mAh cm<sup>-2</sup>) without any conducting additive while the 2819 optimum amount of carbon black additive was found to be 2820 10 wt % at C-rate and below. Its capacity retention is remark-2821 able for several thousand cycles (6500 cycles,  $\approx$ 40 days) in 2822 2.5 M NaClO<sub>4</sub> aqueous electrolyte as well as plain ocean water ( $\approx$ 3000 cycles,  $\approx$ 75 days) (Figure 20).<sup>231</sup> A 40 Wh kg<sup>-1</sup><sub>materials</sub> 2823 2824 full cell demonstration was shown with more than 1600 cycles 2825 using the commercial 4-hydroxy TEMPO benzoate as the 2826 positive material and 0.7 mAh cm<sup>-2</sup> as electrode loading (Table 7, entry 12). It is noted that a concentrated (but cheap) 2828 electrolyte (8 M NaClO<sub>4</sub>) was required to prevent dissolution of the TEMPO derivative.<sup>231,232</sup> The same system was also evalu-2829  $_{2830}$  ated using millimeter thick electrodes of 8 mAh cm<sup>-2</sup> (nominal) leading to a stable areal capacity of nearly 4.5 mAh cm<sup>-2</sup> for 2831 500 cycles at 1C rate. To further demonstrate the practicability of 2832 the system, the same electrodes were evaluated in pouch cells. 2833 2834 The output voltages were 0.78 V (C-rate) and 1.1 V (C/8-rate) 2835 leading to 22 Wh kg<sup>-1</sup> (C-rate) and 36 Wh kg<sup>-1</sup> (C/8-rate) 2836 per mass of materials with a 97% capacity retention over 500 h 2837 cycling at both C and C/8 rates (Table 7, entry 13).<sup>232</sup>

### 8.4. Summary and Outlooks

2838 Neutral aqueous batteries based on organic electroactive mate-2839 rials have been reviewed and discussed. New results point to 2840 the fact that some competitive organic materials have now 2841 surpassed inorganic ones even in terms of volumetric capacity 2842 while relatively large amounts of electrode carbon additive 2843 have been proved unnecessary for some derivatives. In addi-2844 tion, we feel that this review highlights a decisive advantage of 2845 organic materials since most of them offer a highly versatile 2846 ionic compensation chemistry characterized by possible reactions with many different cations (monovalent and 2847 divalent), anions, and even both simultaneously. This aspect, 2848 that is encountered for the Prussian blue family for cations, 2849 opens up a large panel of possibilities regarding the cell chem-2850 istry, with the additional advantage to be coupled to much 2851 larger storage capacity and, in some instance, with the possibility 2852 of supporting the oxygen cycle. 2853

Although it still remains far from that achieved with some 2854 inorganics,<sup>397</sup> the technology readiness level (TRL) of organic 2855 based aqueous batteries has increased in the latest papers by 2856 the use of either highly loaded electrodes and/or pouch cell 2857 configurations. However, studies devoted to the impact of elec- 2858 trode formulation are scarce. As an example, the polytetra- 2859 fluoroethylene (PTFE) binder that is predominantly used so 2860 far because of its readiness is presumably not the most 2861 appropriate for the wettability of composite electrodes, for the 2862 volume variations on cycling, as well as from an industrial 2863 production point of view. 2864

Among the different cell chemistries that have been reviewed 2865 herein, three main topics attract research work: all organic 2866 systems, hybrid ones bearing an inorganic electroactive material, 2867 and water-in-salt electrolytes. Because of the prohibitive price 2868 incurred by the water-in-salt type electrolytes and although 2869 related energy densities can today approach that encountered 2870 for Li-ion batteries, we believe this strategy will remain 2871 confined to fundamental studies unless cheap salts are found to 2872 replace the capability of imide based ones to form stable SEI. 2873 On the other hand, both all organic and hybrid organic batte- 2874 ries using molar electrolytes now can show promising capacity 2875 retention at the cell level. However, this aspect still remains to 2876 be confirmed in large format batteries, at different temper- 2877 atures and by including self-discharge tests. Regarding energy 2878 density and except for a few examples of hybrid cells, most 2879 results are in the range of 40-60 Wh kg<sup>-1</sup> per mass of mate- 2880 rials. However, as opposed to purely inorganic based aqueous 2881 batteries, the combination of attractive energy density, 80-2882 90 Wh kg<sup>-1</sup> per mass of materials, with promising cyclability 2883 (>3000 h) can be reached thanks to the large capacity of 2884 organics. In addition, owing to its large voltage and low price, 2885

#### a) Typical components in RFBs:

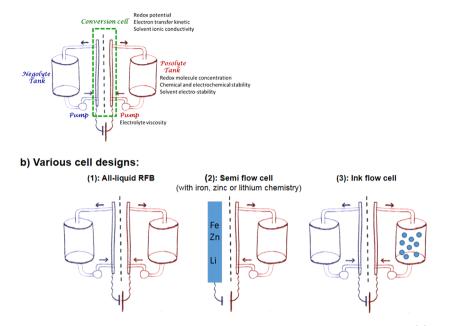


Figure 21. (a) Redox-flow battery schematic with main relevant parameters referred to redox-active compounds. (b) Possible cell configurations.

2886 the Zn system based on mild electrolyte is certainly an option 2887 to be considered more deeply in the future.

Lastly, to close this section it appears interesting to recall the ever decreasing price of Li batteries (and the increasing rRL of their novel high energy chemistries) turns them into a serious option for (off)in-grid application.<sup>421</sup> In this context, end the authors believe that the effective chances of organics to realize user/market-acceptable aqueous batteries (at least for end complementary applications) stem from their low toxicity, their abundancy, as well as their recyclability which could turn end turn to be efficient and profitable.

### 9. ORGANICS IN REDOX-FLOW BATTERIES

#### 9.1. Specificities of Redox-Flow Batteries

2897 Although we have already described the different cell 2898 assemblies using organics, some complementary details are 2899 required to better grasp the specificities of redox-flow cell for 2900 electrochemical storage (Figures 8,9). Basically, such a cell can 2901 be seen as a fuel cell where the fuel and oxidizer would be 2902 replaced by fluids with redox components in solution. As the 2903 associated electrochemical reactions are reversible, the device 2904 can be easily recharged. RFBs are energy storage devices with 2905 the advantage of dissociating power density (electrode surface 2906 area, number of cells in the conversion cell) and energy (tank 2907 volume). As currently energy densities remain low, these 2908 devices are more dedicated to stationary energy storage. The 2909 duration of storage (hour, day, week) depends mainly on the 2910 type of chemistry used.

2911 Many recent reviews related to ORFBs have been conducted 2912 in the literature.<sup>15,20,23,24,31,34,35,44,45,422</sup> These reviews focus on 2913 describing the implemented redox molecules and the different 2914 strategies used to integrate them into a redox-flow device. This 2915 section will only focus on systems that are most advanced in 2916 terms of performance and that have been tested in systems as 2917 close to the application as possible and at least in a flow cell. 2918 In terms of concentration, there are many publications where 2919 tests are carried out in a very diluted medium, so we have decided to retain only studies on the most concentrated 2920 electrolytes. In solvent-based media, generally speaking, the 2921 performance is much weaker than in the case of aqueous 2922 electrolytes, so the selection we made was less drastic. 2923

A RFB consists of three main components: an electro- 2924 chemical conversion cell where electrochemical reactions take 2925 place, tanks to store redox-active fluids, and finally pumps to 2926 allow the circulation through the cell of the two electrolytes 2927 (posolyte/negolyte) containing the redox-actives species 2928 (Figure 21a). Behind this apparent simplicity lies a device 2929 that remains very difficult to optimize. Among the main 2930 parameters or components associated with the chemistry used, 2931 we can mention: 2932

- the nature of the solvent that composes the electrolyte, 2933 on which depends the accessible potential window, as 2934 well as the power density (ionic conduction) of the 2935 conversion cell; 2936
- the redox compounds solubility; it is important that the 2937 different redox states of each couple have the highest 2938 possible solubility. The number of electrons exchanged 2939 during the redox reaction must modulate this solubility; 2940 the important parameter is the quantity of electrons 2941 exchanged by the solution (mole electrons per liter); 2942
- the electron transfer kinetics with the electrode surface; 2943 electron transfers must be fast and perfectly reversible to 2944 avoid losses due to overvoltage problems. In general, for 2945 a redox-flow conversion cell, faradic efficiencies are very 2946 good; main losses come from overvoltage problems at 2947 the electrodes (different potentials between charge and 2948 discharge); 2949
- the chemistry itself which must obviously be stable 2950 enough without bringing corrosion problems that would 2951 shorten the battery life. RFBs must have a very long 2952 lifetime (>20 years) in order to make its components 2953 more cost-effective than in a regular "sealed" battery 2954 (membrane, pumps cost, etc, ...) since stationary storage 2955 applications are targeted as previously underlined;<sup>130,136</sup> 2956

the membrane, which allows the two compartments to
 be chemically and electrically separated, while allowing
 the diffusion of ions that ensure the system electro neutrality without crossover.

9.1.1. Short Overview on Inorganic-Based Redox-2961 2962 Flow Batteries. As already mentioned in the Introduction, 2963 the most advanced and commercialized flow systems are based 2964 on inorganic materials with acidic aqueous electrolyte: vanadium, 2965 zinc-bromine, hydrogen-bromine, and so on. 5,423-425 Each 2966 system has its own limitations: cost in the case of vanadium, 2967 formation of dendrites for zinc, need to use platinum in the 2968 case of  $H_{21}$  toxicity (Br<sub>2</sub>). Energy efficiencies are between 65 to 2969 80% in the case of vanadium RFB for current densities of up to 2970 100 mA cm<sup>-2</sup> and an operating voltage of 1.25 to 1.4 V. Energy 2971 densities of 55 Wh L<sup>-1</sup> have been achieved. These values 2972 should be strongly tempered because at high vanadium con-2973 centrations (2 M), electrolytes become very sensitive to tem-2974 perature, they precipitate easily or become very viscous 2975 preventing their circulation, so the concentrations commonly 2976 used are rather in the order of 1.6 M. The shutdown system 2977 self-discharge would be in the order of 0.1% per week.

From a practical point of view, many problems of matter 2978 2979 transfer (solvent, ...) related to electro-osmosis through ion 2980 exchange membranes appear during operations. As a result, the 2981 volume of electrolytes in each tank changes according to the 2982 number of cycles and it is necessary to "redistribute" them by 2983 transferring a volume of electrolyte from one compartment 2984 to another, this approximately every 200 cycles. With this 2985 periodic rebalancing, life times of more than 2000 cycles and 2986 10 years can be achieved. This is independent of corrosion 2987 problems that require regular replacement of parts, involving 2988 high maintenance costs. In the case of chemistries other than 2989 vanadium, electrolyte "rebalancing" is not possible as each 2990 compartment has a different chemistry and the management of 2991 these solvent transfers becomes problematic. Despite these 2992 important limitations, at the moment no "alternative" chemistry 2993 can compete with inorganic flow batteries in terms of application. 9.1.2. Possible Cell Configurations for Redox-Flow 2994 2995 Batteries. Different types of ORFB have been described in the 2996 literature, with the most common being those where both 2997 electrolytes are liquid (Figure 21b). In the case where the only 2998 purpose is to evaluate a specific molecule, it is possible to use a 2999 symmetrical cell (same compounds in each compartment); 3000 however, this implies to have access to the two redox states of 3001 the molecule. There are also intermediate devices between a 3002 flow battery and a solid battery known as semisolid flow 3003 battery as proposed by Chiang's group.<sup>426</sup> This latter approach, 3004 which generally has the disadvantage of using highly viscous 3005 dispersions that require oversized pumps, will not be discussed 3006 in this review.

**9.1.3. Redox-Active Organic Species and Solvents. 9.1.3. Redox-Active Organic Species and Solvents. 9.1.3. Redox-active organic moieties identified in the ORFB literature 9.1.3. Redox-active organic moieties identified in the ORFB literature 9.1.4. Solution 9.1.5. Redox-active organic moieties identified in Table 1** including **9.1.1. The same as those found in solid batteries and also deduced 9.1.1. Table 1** including **9.1.1. The same as those found in reported in Table 1** including **9.1.1. They are however "functionalized" in order to increase solu-9.1.1. They are however "functionalized" in order to increase solu-9.1.1. They are however "functionalized" in order to increase solu-9.1.1. They are however "functionalized" in order to increase solu-9.1.1. They are however "functionalized" in order to increase solu-9.1.1. They are however "functionalized" in order to increase solu-9.1.1. They are however "functionalized" in order to increase solu-9.1.1. They are however "functionalized" in order to increase solu-9.1.1. They are however "functionalized" in order to increase solu-9.1.1. They are however "functionalized" in order to increase solution of a dual ion cell (Figure 9). It should be 9.1.1. They are however to a dual ion cell (Figure 9). It should be 9.1.1. They are however to a dual ion cell (Figure 9). It should be 9.1.1. They are however to a dual ion cell (Figure 9). It should be 9.1.1. They are however to a dual ion cell (Figure 9). It should be 9.1. They are how to be active material, the dual-ion cell 9.1.1. Solution cell or a dual ion cell (Figure 9). It should be 9.1.1. Solution cell to the mass of active material, the dual-ion cell 9.1.1. Solution cell any problems (significant loss of**  conductivity of the electrolyte). The main redox-active moieties 3020 are nitroxide, viologen, perylene diimide, ferrocene, quinone, 3021 thio, amino, phenol, ... (Figure S8). In a general way, there is a 3022 strong lack of redox-active structures able to work at very low 3023 potential (as in the case of carboxylates in organic "sealed" 3024 batteries working with solid state compounds) in order to obtain 3025 higher voltage systems. The main problem to address with redox 3026 molecule is stability. Since redox-active compounds are 3027 solubilized in the electrolyte, they are more subject to decom-3028 position than solid electrodes. Thus, upon cycling, molecules 3029 can react together with solvent or electrolyte giving rise to 3030 poor performances. This especially at high concentrations 3031 (>0.5 M) which enhance decomposition kinetics. 3032

The main role of the solvent is to dissolve the redox 3033 molecule in order to make it transportable between the tanks 3034 and the conversion cell. It must also ensure the ionic con- 3035 ductivity necessary to achieve electroneutrality at all points 3036 of the solution and avoid polarization phenomena in the 3037 conversion cell. For this purpose, the best solvent is water; its 3038 high polarity combined with its ability to dissociate elec- 3039 trolytes results from the fact that aqueous solutions have very 3040 high ionic conductivities. Moreover, in terms of cost, water is 3041 the cheapest solvent and presents the fewest safety problems 3042 (nonflammable, nontoxic). However, aqueous electrolytes 3043 display low electrochemical stability window (1.23 V from 3044 thermodynamics up to 1.5 V for kinetics reason). Organic 3045 solvents have the advantage of having larger electrochemical 3046 stability windows (>4.5 V in the case of acetonitrile or carbon- 3047 ates), but electrolyte dissociation is less efficient, resulting in an 3048 ionic conductivity of about 100 times less than in aqueous 3049 solvent. 3050

Organic solvents are chemically unreactive, so they prevent 3051 degradation phenomena in solution and increase the lifetime 3052 of redox molecules. This also makes possible the stabilization 3053 of certain highly reactive redox molecules (e.g., radicals) and 3054 makes them relevant for redox-flow applications. The main 3055 solvents used are acetonitrile, carbonates, ethers, esters, and, 3056 more anecdotally, DMSO. Generally speaking, the solubility of 3057 organic molecules is not so different between aqueous and 3058 organic electrolytes, for two reasons: in organic media high 3059 concentrations of salts are used to increase the conductivity of 3060 solutions, with the consequence that the solubility of molecules 3061 decreases. An adapted functionalization renders the redox 3062 molecules highly soluble in water. The maximum concen- 3063 trations achievable in a complete electrolyte (salt + solvent) 3064 are in the order of 2-3 M. As the conversion cells have not yet 3065 been really optimized for organic solvents, at the moment the 3066 solvent strongly conditions the type of batteries: high power 3067 density  $(0.1-0.3 \text{ W cm}^{-2})$  in aqueous solution (low voltage, 3068 high conductivity) and high energy density (>100 Wh  $L^{-1}$ ) in 3069 organic solvent (high voltage, low conductivity). It is of course 3070 possible to mix several solvents, even if this makes electrolyte 3071 development more complex.<sup>427</sup> This approach remains difficult 3072 to master because it is difficult to combine the advantages of 3073 solvents without also combining the disadvantages. 3074

One way to get around this is to use hydrotropes. A hydro- 3075 trope is a concentrated aqueous solution (several molars) of a 3076 small organic molecule such as urea, *para*-toluene sulfonic acid, 3077 nicotinic acid, and so on. Organic molecules are generally 3078 much more soluble in a hydrotrope than in water and the elec- 3079 trochemical properties are preserved or improved. The use of 3080 urea, for example, increases the solubility of benzoquinone by a 3081 factor of 7.<sup>428</sup> Other strategies have been used to make redox 3082

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3083 organic molecules "liquid". The use of ionic liquid was tested 3084 by following different paths: as a solvent, with an organic or 3085 aqueous cosolvent, and finally by making redox ionic liquids. 3086 The use of eutectics based on highly concentrated salts in a 3087 solvent has produced interesting results because they produce 3088 highly conductive solutions capable of dissolving highly polar <sup>3089</sup> redox organic molecules.<sup>429</sup> Finally, some redox molecules 3090 developed to be highly soluble have been found to be liquid 3091 due to their low solid-state cohesion. However, the addition 3092 of salt is necessary to make the liquid ionically conductive, 3093 resulting in a significant increase in viscosity. While these 3094 alternative strategies have proved to be relevant, they have not 3095 yet made possible the development of large-scale devices 3096 capable of competing with inorganic flow cells in terms of power density, energy density, or stability (cycling and calendar aging). 3097 3098 The use of ionized salt is necessary to enhance the solvent 3099 ionic conductivity and maintain electroneutrality during the 3100 electrochemical process. In aqueous media, acid (H<sub>2</sub>SO<sub>4</sub>) or 3101 base (KOH) could be used if the redox molecule does not 3102 react with them. Salts like sodium or lithium associated with 3103 nitrate, and chloride or sulfate could be used in neutral pH. 3104 In organic medium, salts need to be highly soluble and dis-3105 sociated, so lithium or tetra-alkylammonium cation associated 3106 with noncoordinating anion such as PF<sub>6</sub><sup>-</sup>, BF<sub>4</sub><sup>-</sup>, or TFSI<sup>-</sup> is 3107 mainly used, even if these salts are much more expensive than 3108 the ones used in aqueous solvents. Independently of the 3109 solvent, the choice of the supporting salt is very important on 3110 the electrochemical behavior of the redox molecule.

One of the main problems remaining for RFB concerns the 3111 3112 fact that the electrolyte in a highly concentrated solution tends 3113 to be very viscous (both in inorganic or organic RFB). In organic 3114 RFB, the problem is more important in the way that organic 3115 molecules possess a higher molecular weight compared to 3116 inorganic ones  $(M(V) = 50.9 \text{ g mol}^{-1})$ . This means, for example, 3117 that an organic redox molecule with a molecular weight of 200 g 3118 mol<sup>-1</sup>, typically nonfunctionalized anthraquinonoid derivative, 3119 at a concentration of 1 M corresponds to 200 g of molecule in 3120 1 L of solution. In some cases, the solution became as viscous 3121 as honey, precluding their use in flowing cells, apart from using 3122 a lot of energy to power the pump. A high viscosity also lowers 3123 the molecule diffusion in solution, with a direct effect on the 3124 apparent electron transfer kinetic and ionic conductivity. As a 3125 result, highly concentrated electrolytes suffer from higher cell 3126 overvoltage either in charge or in discharge.

9.1.4. Favoring Highly Soluble Redox-Active Species. 3127 3128 In order to make redox organic molecules highly soluble in 3129 the desired medium, it is necessary to functionalize them with 3130 appropriately selected groups. In aqueous media, ionic func-3131 tions or functions with a large number of heteroelements (e.g., 3132 O or N) will be favored to increase the interactions between 3133 the redox compound and water molecules. The main ionic 3134 functions used are sulfonates,<sup>430</sup> phosphates,<sup>431</sup> carboxy-3135 lates,<sup>432</sup> ammonium,<sup>433</sup> or hydroxo.<sup>434</sup> These ionic functions 3136 have also the advantage of increasing the ionic conductivity of 3137 the solution, allowing in some cases to eliminate the use of 3138 supporting salts. Neutral substituents such as PEGs are also 3139 used regularly. However, it is necessary to remain attentive to 3140 the positions chosen to graft these solubilizing groups, because 3141 the functionalization of redox molecules can completely 3142 change the electrochemical response and make it irreversible. 3143 The solubility of nonfunctionalized organic molecules is gen-3144 erally better in organic media. However, in most cases, func-3145 tionalization is necessary to achieve the solubility necessary to

develop an efficient flow battery. In organic media, neutral 3146 substituents are preferred, such as alkyl chains or PEGs. Alkyl 3147 chains are not necessarily the most efficient because of their 3148 low polarity, which is not optimal in polar solvents and which 3149 hinders the solubilization and dissociation of salts. PEG chains 3150 have the advantage of being more polar and their effect on 3151 solubility is more important. By choosing certain chain lengths, 3152 it is even possible to obtain liquid redox compounds. Finally, 3153 these PEG chains are capable of strongly complexing the alkaline 3154 cations contained in the supporting salt, thus improving its 3155 dissociation and increasing the conductivity of the solution. 3156

For the redox-flow system, the membrane is an important 3157 element; it allows the two compartments to be physically 3158 separated to avoid the mixing of species but must permit the 3159 passage of ions to ensure the electroneutrality of each of the 3160 compartments. In most cases, an ion exchange membrane is 3161 used, cationic in the case of a cationic rocking chair battery, 3162 anionic in the case of an anionic rocking chair battery, and one 3163 or the other in the case of a dual ion configuration. In aqueous 3164 environments, the most efficient membranes are mainly made 3165 of perfluoro sulfonated polymer. These membranes are very 3166 stable and have a high ionic conductivity. They have the dis- 3167 advantage of not being as stable in organic media or they tend 3168 to swell and become porous. Alternative organic membranes 3169 have been developed, but unfortunately for the moment they 3170 are not as stable as the perfluoro one. To counter this, ceramic 3171 membranes have been used, particularly in the case of mixed 3172 devices using a lithium electrode. As the cost of such membranes 3173 is important, different strategies have been deployed to try to 3174 replace them with simpler separators. Size based separators 3175 (dialysis membranes) combined with redox molecules in the 3176 form of poly/oligomer to block diffusion from one compart- 3177 ment to the other. 3178

#### 9.2. Aqueous Organic Redox-Flow Batteries

9.2.1. Generality. In aqueous media, the most studied 3179 organic molecules are undoubtedly quinones and both methyl- 3180 viologen and TEMPO derivatives. Such electrolytes have the 3181 advantage of being highly dissociating for the supporting salts, 3182 forming solutions of high ionic conductivity allowing high 3183 power densities cycling. The highest conductivities are obtained 3184 in acidic environments since proton is the cation with the 3185 highest mobility (the Grotthuss mechanism). Similarly, the 3186 hydroxide ion is the most mobile anion, so many studies in 3187 aqueous media are also carried out in basic media. However, 3188 these two electrolytes have the disadvantage of being very 3189 reactive toward organic molecules: protons are responsible 3190 for degradation by acid catalysis (polymerization etc..), and 3191 hydroxide ions are good nucleophiles (hydroxylation). For 3192 example, it should be remembered that cleaning glassware in 3193 organic chemistry is often carried out in potash baths.

In the case of quinones, these reactions are particularly 3195 troublesome (e.g., Michael reaction) and very effective in both 3196 acidic and basic media, so that after a few cycles, the initial 3197 molecule is completely transformed and in general the 3198 associated loss of capacity is significant.<sup>435</sup> Similarly, quinones 3199 tend to dimerize, decreasing the capacity that can be addressed.<sup>436</sup> 3200 As far as methyl viologen derivatives are concerned, they are 3201 stable only in a neutral or acidic medium; in a basic medium an 3202 elimination reaction takes place resulting in the loss of redox 3203 properties. These compounds also tend to dimerize, resulting 3204 in one electron reactions instead of two.<sup>437</sup> Similarly, in highly 3205 acidic environments, TEMPOs undergo degradation reactions.<sup>438</sup> 3206

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<sup>3207</sup> In all cases, it is necessary to develop sometimes complex <sup>3208</sup> strategies to avoid these adverse reactions for the battery <sup>3209</sup> operation and stability. In terms of solubility, by functionaliza-<sup>3210</sup> tion it is possible to achieve solubility values in about 2 M. <sup>3211</sup> In the case of quinones, the electrochemical and solubility <sup>3212</sup> properties are very strongly dependent on the number and <sup>3213</sup> substitution positions.<sup>430</sup> Thus 9,10-anthraquinone-2,7-disul-<sup>3214</sup> fonic acid (AQDS) retains a high electrochemical reversibility <sup>3215</sup> while being highly soluble, which is not the case for other <sup>3216</sup> disulfonates.<sup>439</sup> Generally speaking, aqueous ORFBs have <sup>3217</sup> many advantages: nontoxic, low solvent and salt costs, highly <sup>3218</sup> conductive solution. However, they pose two important and <sup>3219</sup> very difficult problems: the small window of potential <sup>3220</sup> associated with this solvent and its reactivity with organic <sup>3221</sup> molecules.

**9.2.2 9.2.2. Main Examples of Aqueous ORFB.** Many works have been carried out over the last 5 years in the field of aqueous ORFBs, we have chosen a few didactic examples to s225 show the diversity of approaches and the performances that s226 can be obtained with this technology to date.

Aziz's group (Harvard University) has conducted numerous 3227 3228 studies on the use of quinone for ORFBs, or combined 3229 organic/inorganic batteries (quinone -Br2, quinone ferrocya-3230 nide).<sup>434,440</sup> Their studies focus mainly on the use of sulfonated (AQDS acid medium) or hydroxylated (DHAQ basic medium) 3232 quinones that can achieve electron concentrations >1 M (Figure 22a). The output cell voltage obtained with the full 3233 3234 system 0.5 M DHAQ/0.4 M ferrocyanide is about 1.2 V. 3235 The battery was tested for 100 cycles at a current density of 100 mA cm<sup>-2</sup> and showed an energy efficiency greater than 3236 3237 80% and a capacity retention of 90%. The maximum power 3238 density is 400 mW·cm<sup>-2</sup>. No significant degradation of the 3239 electrolyte seems to occur. With ADQS in sulfuric acid 3240 medium (1 M) as negative electrolyte, associated with 3.5 M 3241 hydrobromic acid and dibromine (0.5 or 2 M) the cell voltage 3242 is 0.8 V. Different types of carbon felt and membranes have 3243 been tested to optimize battery performances. With a 212 3244 Nafion membrane and 2 M Br<sub>2</sub>, 3 M HBr, the battery reaches a 3245 power peak at 1 W cm<sup>-2</sup> which is extremely high for a flow 3246 battery. It should be noted, however, that this was possible 3247 thanks to extremely high electrolyte flows (400 mL min<sup>-1</sup>) for 3248 an electrode surface area of 2 cm<sup>2</sup>, which is very demanding on 3249 the consumption of the pumps.

Schubert's group (University of Jena) has developed an 3250 3251 approach combining methyl viologen derivatives (low potential) 3252 and nitroxide (high potential).<sup>441,442</sup> These organic compounds 3253 are reversible in electrochemistry and have very high electron 3254 transfer kinetics. The voltages of the cells reached are 1.4 V 3255 (Figure 22b). The TEMPTMA derivative has a solubility of 3256 2.3 M in a solution of NaCl 1.5 M which corresponds to a 3257 theoretical capacity of 61 Ah. The flow battery combining MV 3258 and TEMPTMA (2 M each) addresses the maximum capacity  $_{3259}$  of the electrolyte up to a current density of about 100 mA cm<sup>-2</sup>. 3260 The energy efficiency is greater than 70%. At 80 mA  $cm^{-2}$  the 3261 battery is stable over 100 cycles without significant degradation 3262 of performance. To avoid using an ion exchange membrane, 3263 polymers have been developed from these molecular units. Due 3264 to the steric encumbrance of these polymers, a simple porous 3265 membrane is sufficient to prevent the two compartments from  $_{3266}$  mixing. Ten Ah L<sup>-1</sup> electrolytes are made by dissolving these 3267 polymers in 2 M NaCl solution. The battery thus formed is 3268 capable of cycling up to current densities of 50 mA cm<sup>-2</sup> 3269 without significant loss of capacity. The properties are stable

over 90 cycles with a loss of less than 10% in capacity. The  $_{3270}$  energy density of redox fluids is in the order of 10 W L<sup>-1</sup>.  $_{3271}$ 

Liu's group (Utah State University) has developed several 3272 types of chemistry based mainly on viologen derivatives 3273 (negative) and either ferrocene derivatives or dibromine in 3274 positive compartment (Figure 22c).<sup>443,444</sup> In particular, they 3275 used a sulfonate substituted viologen derivative to make a 3276 mixed organic/inorganic ( $Br_2$ ) RFB. The output voltage of the  $_{3277}$ cell is about 1.4 V. The synthesized molecule has been tested 3278 in a neutral medium (NH<sub>4</sub>Br) at concentrations up to 1.5 M 3279 (3 N). The power densities obtained are as high as  $227 \text{ mW cm}^{-2}$   $_{3280}$ for a current density of 300 mA cm<sup>-2</sup>. The stability in charge and 3281 discharge over 50 cycles shows a loss of capacity per cycle of 3282 0.11%; the energy efficiency is 78% at 40 mA cm<sup>-2</sup>. The energy <sub>3283</sub> density of these ORFBs is 30.3 Wh L<sup>-1</sup>. Tests have shown that 3284 the use of carbon nanotubes on current collectors improves 3285 battery performance, significantly reducing overpotential 3286 issues. This group has also developed ammonium-substituted 3287 ferrocene derivatives to improve solubility in aqueous media 3288 (>2 M in 2 M NaCl). The batteries produced have a cell 3289 voltage of 1 V and energy efficiencies that are highly dependent on 3290 current density (72% at 40 mA cm<sup>-2</sup> and 43% at 100 mA cm<sup>-2</sup>).  $_{3291}$ Aging studies carried out over 700 cycles have shown very high 3292 stability (about 0.00014% loss of capacity per cycle). 32.93

Narayanan et al.<sup>445,446</sup> from University of Southern California 3294 have developed an ORFB where posolyte and negolyte are 3295 quinone based: disulfonated anthraquinone (AQDS) or mono- 3296 sulfonated in negative compartment and disulfonated *ortho-* 3297 benzoquinone (BQDS or tiron) as positive electrolyte 3298 (Figure 22d). These two compounds have high solubility in 3299 acid electrolytes. The cell voltage is 0.8 V at a current density 3300 of 80 mA cm<sup>-2</sup>. This voltage drops sharply as the current 3301 density increases. Several cell geometries and current collectors 3302 (carbon felts) have been tested to increase the performance of 3303 these batteries. The energy efficiency of a battery composed of 3304 BQDS and AQDS 1 M is 70% over 100 cycles. In any case, due 3305 to the reactivity of these redox molecules, these batteries have 3306 low cycling stability. 3307

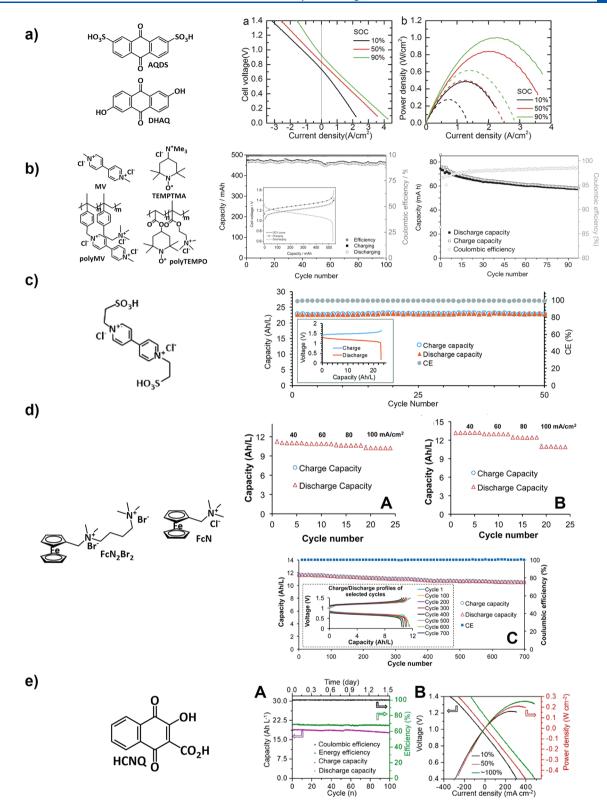
Finally, Jin et al.<sup>432</sup> from Nanjing University have modified a 3308 naphthoquinone by substituting it with a carboxylate group 3309 (HCNQ) to increase solubility in a neutral or basic medium 3310 (Figure 22e). The battery made with an alkaline electrolyte 3311 (KOH 1 M) and 0.5 M HCNQ combined with ferrocyanide 3312 exhibits an output voltage of 1 V. Power densities of 3313 250 mW cm<sup>-2</sup> were measured at a current density of about 3314 400 mA cm<sup>-2</sup>. The capacity loss measured over 50 cycles is 3315 0.12% per cycle, probably resulting from the reactivity of the 3316 reduced form of HCNQ. To increase stability, it would be 3317 necessary to modify the structure of these quinones to block 3318 hydroxylation reactions. 3319

Concerning ORFBs, the aqueous medium is undoubtedly 3320 the one with the best performance in terms of energy efficiency 3321 and current density. Contrary to what was anticipated, the 3322 solubility of redox molecules in aqueous medium is not much 3323 lower than what can be measured in organic medium. The 3324 power and energy densities are high and in some cases at 3325 the same level as those found in the case of inorganic BFRs 3326 (vanadium). Although different conversion cell geometries are 3327 being tested in some studies, it would now be useful to 3328 conduct systematic studies to try to minimize losses due to 3329 ohmic drops, or problems related to cross diffusion through 3330 the membrane. In general, many of these systems suffer from 3331

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**Figure 22.** (a) Performance of ORFB composed of AQDS and  $Br_2$  showing both the cell voltage vs current density and the power density vs current density (reproduced with permission from ref 440. Copyright 2016 The Electrochemical Society). (b) Cycling capacity and efficiency of ORFB made of: MV and PEMPTMA (center); polymerized MV and TEMPO (left) (reproduced with permission from refs 441 and 442. Copyright 2015 John Wiley and Sons and Nature Publishing Group). (c) Cycling curve and aging behavior of the ORFB developed by Liu et coworkers. Concentration of redox molecule 1 M in NH<sub>4</sub>Br (reproduced with permission from ref 443. Copyright 2019 The Royal Society of Chemistry). (d) Capacity vs cycle number at different current densities for (A) FcNCl, (B) FcN<sub>2</sub>Br<sub>2</sub> at 0.5 M, and (C) cycling stability of FcNCl/ MV battery (0.5 M electrolyte) over 700 cycles (reproduced with permission from ref 444. Copyright 2017 American Chemical Society). (e) Capacity vs cycle number at different current densities for an HCNQ cell (0.5 M) in A. Corresponding voltage and power density vs current density in B (reproduced with permission from ref 432. Copyright 2018 American Chemical Society).

3332 poor cyclability, particularly in concentrated conditions, due to 3333 the numerous possible decomposition reactions.

## 9.3. All-Organic Redox-Flow Batteries

3334 Redox batteries using an organic solvent have been strongly 3335 developed in the literature during the years 2000-2010, mainly 3336 with compounds from coordination chemistry with several stable 3337 redox states; more recently, the use of organic molecules has 3338 strongly increased. The main advantage of working with organic 3339 solvents is to have larger potential windows and therefore to 3340 increase the energy density. The voltages obtained with devices 3341 where both fluids circulate are at most in the order of 2.5 V. This 3342 is mainly due to the fact that when the molecules are in solution 3343 no SEI can be formed. SEI layers are formed on the surface of 3344 particles inserting Li at very low potential and protect the 3345 solvents from decomposition. Due to main solvent stability 3346 window, it is necessary that the redox potential of the com-3347 pound used in the negative electrolyte should be at the most in 3348 the order of 1 V vs Li<sup>+</sup>/Li. Therefore, hybrid devices have been 3349 developed combining a Li-based negative and an organic positive 3350 flow cell. Another difficulty comes from organic electrolytes: 3351 low ionic conductivity, about 100 times lower than aqueous 3352 electrolytes. This results in important ohmic drop and decreases 3353 the voltage efficiency. Thus, a complete optimization of the cell 3354 core would be necessary to counter this phenomenon.

Various cells configurations are used to test new compounds 3355 3356 by (i) associating two organic redox couples, (ii) carrying test 3357 in symmetric cells, or (iii) Li/RFB hybrid cells. The latter, due 3358 to the low potential of Li, have very high energy density, up to 3359 about 200 Wh L<sup>-1</sup> but power density remains very low due to  $_{3360}$  current limitation (less than 1 mA cm<sup>-2</sup>). However, to date, no 3361 redox solvent-based electrolyte battery has been able to achieve 3362 a true industrial scale demonstrator. Many questions remain to 3363 be answered, such as the associated costs, safety, and solubility, 3364 electrolyte viscosity, which is generally very high in concen-3365 trated organic media, and calendar and cycling stability over 3366 very long periods. For example, there are few studies where 3367 highly concentrated electrolytes (0.5-1 M) are tested in flux 3368 configuration mainly due to the high solutions viscosity. The 3369 few systems we have selected to discuss are the most advanced 3370 and representative of these devices.

**9.3.1. Main Results in Mix Configuration (Li/Organic** 3372 **RFB).** The Pacific Northwest National Laboratory (PNNL) 3373 has particularly tested several types of strategies and redox 3374 molecules in mixed configuration.<sup>447–449</sup> First, anthraquinone 3375 derivatives modified to increase their solubility were used, then 3376 TEMPO, and finally ferrocene derivatives. As the latter does 3377 not provide better properties than other approaches, it will not 3378 be discussed in this review, only the first two strategies are 3379 described below.

<sup>3380</sup> Wang et al.<sup>447</sup> proposed to modify anthraquinones with <sup>3381</sup> PEG groups (15D3GAQ) to promote the solubility of the <sup>3382</sup> molecule as well as the complexing effect toward Li ions. The <sup>3383</sup> electrolyte is composed of a solution of LiPF<sub>6</sub> 1 M in PC. This <sup>3384</sup> solvent forms a stable SEI with respect to Li metal. The static <sup>3385</sup> cell is composed of a Li sheet and a simple Celgard separator <sup>3386</sup> that confines the redox molecule to the positive compartment; <sup>3387</sup> the concentration of 15G3GAQ being 0.25 M. An average <sup>3388</sup> voltage of 2.3 V is measured when the battery is cycled to <sup>3390</sup> to a cycling current of 0.5 mA cm<sup>-2</sup> but collapse beyond that. <sup>3391</sup> Two plateaus corresponding to the two consecutive transfers <sup>3392</sup> of 1 electron are observed respectively at 2.15 and 2.40 V (during charging), respectively. An energy efficiency of 82% is 3393 measured; the cycling stability evaluated over 40 cycles shows a 3394 loss of about 0.8% in capacity per cycle. The measured energy 3395 density is about 25 Wh  $L^{-1}$ , with the low concentration used to 3396 make the electrolyte (0.5 M in electron) being compensated by 3397 the output cell voltage (2.3 V). 3398

Xu, Wang, and co-workers found that TEMPO was highly  $_{3399}$  soluble in carbonate solvents.<sup>448</sup> Thus in an EC/PC/EMC  $_{3400}$  mixture (4:1:5 w/w) 2.3 M LiPF<sub>6</sub>, TEMPO is soluble up to  $_{3401}$  2 M. However, it should be noted that the solutions obtained  $_{3402}$  are very viscous and difficult to circulate (67.1 cP at 2 M,  $_{3403}$  4.02 cP at 0.1 M). The flow cell consists of a Li/graphite mixed  $_{3404}$  negative electrode, a porous physical separator, and a carbon  $_{3405}$  felt through which the electrolyte circulates. The energy density  $_{3406}$  was measured with the cell at 2 M TEMPO and 126 Wh L<sup>-1</sup>,  $_{3407}$  with an energy efficiency of 70%. Stability in concentrated  $_{3408}$  condition does not seem very high, in dilute solution (0.1 M),  $_{3409}$  capacity losses are about 0.2% per cycle. As there is no ceramic  $_{3410}$ 

Finally, Lu et al.<sup>450</sup> reported the use of 10-methylpheno- 3412 thiazine (MPT) melted, then mixed with carbon black 3413 (Ketjenblack EC-600JD), and finally ground when solidified. 3414 The electrolyte consists of a saturated solution of MPT (0.3 M) 3415 in an EC/DEC 1 M LiPF<sub>6</sub> mixture to which the ground solid 3416is added. The MPT in solution acts as a redox shuttle to 3417 electrochemically address the solid MPT. It should be noted 3418 that without carbon, solid MPT is not electroactive. Mixtures 3419 of 0%, 20%, and 40% (in vol.) solid and electrolyte were tested. 3420 The electrolytes were tested in static and flow cells. The flow 3421 cell is composed of a Li sheet, a ceramic separator (LAGP) and 3422 of the electrolyte circulating on a carbon paper. On the cycling 3423 curves (Figure 23b), the electrolyte alone (0%) has a plateau at 3424 3.55 V vs Li<sup>+</sup>/Li and a capacity of 7 Ah L<sup>-1</sup>, which corresponds 3425 to 87% of the theoretical capacity. With 20% mixture, the 3426 cycling curves maintain the same behavior, but the capacity is 3427 increased to 27 Ah  $L^{-1}$ . The 50% mixture allows to reach a  $_{3428}$  capacity of 55 Ah  $L^{-1}$ , which corresponds to an electron  $_{3429}$ concentration of 2.23 M. The energy density of the 40% 3430 electrolyte is 190 Wh L<sup>-1</sup>, one of the highest energy densities 3431 demonstrated to date. This is mainly due to the high cell 3432 voltage (3.55 V) even if the MPT/carbon Ketjenblack mixture 3433 significantly increases the capacity of the solution. 3434

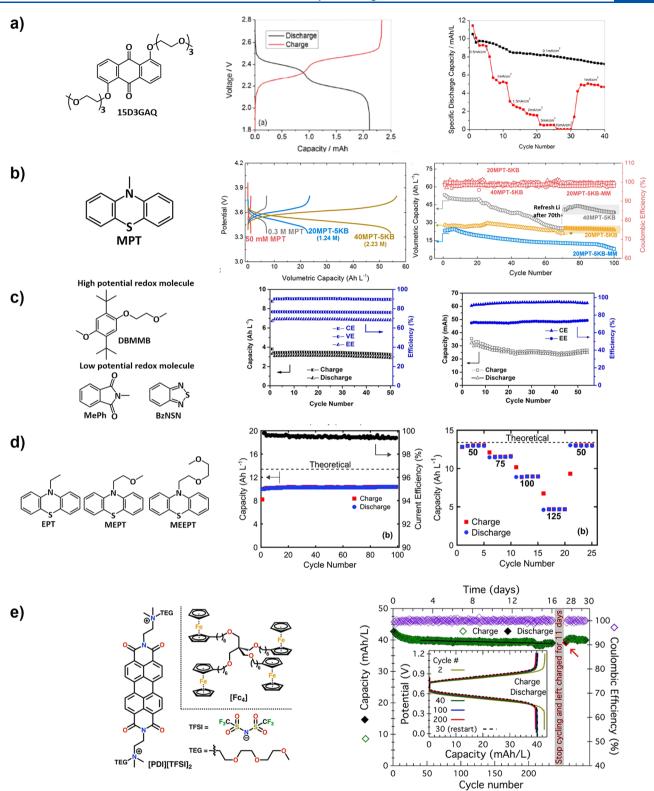
The main problem with these mixed Li/organic molecules 3435 flow cell approaches comes from the very low current densities 3436 (often less than 1 mA  $cm^{-2}$ ) that can be passed through the 3437 device. This is particularly true if the separator between the 3438 two compartments is a ceramic membrane. When the separator 3439 is porous, it would appear that the SEI formed on the surface 3440 of the Li in the carbonates is beneficial. It would act as an ion 3441 exchange membrane while blocking electron transfers to the 3442 redox molecules. Thus, molecules in solution close to the 3443 negative electrode could not be reduced, which would explain 3444 the high Coulombic efficiency of these devices. On the other 3445 hand, at high concentration in redox molecules, the SEI is 3446 modified and/or no longer succeeds in blocking these electron 3447 transfers and the Coulombic efficiency falls strongly 3448 (Coulombic efficiency 99% at 0.1 M, 91% at 0.8 M, 85% at 3449 1.5 M, and 84% at 2 M).<sup>448</sup> Finally, these devices do not allow 3450 the power and energy density to be separated; they are 3451 therefore more limited in terms of application. 3452

**9.3.2. Main Results in Liquid All-Organic Cell** 3453 **Configuration.** Argonne laboratory and their collaborators 3454 have optimized the structure of phenolic ethers used as 3455

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**Figure 23.** (a) Cycling performance and rate capability reported by Wang and co-workers of the cell with 0.25 M 15D3GAQ as posolyte and lithium foil as anode (reproduced with permission from ref 447. Copyright 2012 The Royal Society of Chemistry). (b) Cycling performance of the Li/MPT flow cell reported by Lu and co-workers (reproduced with permission from ref 450. Copyright 2018 American Chemical Society). (c) Cycling performances of ORFBs based on MePh/DBMMB 0.3 M in DME– M LiTFSI (left) or BzNSN/DBMMB 0.5 M in ACN 1 M LiTFSI (right) reported by Wei and co-workers (reproduced with permission from refs 452 and 453. Copyright 2016 and 2017 American Chemical Society). (d) Symmetric flow cell characterization of MEEPT 0.5 M in ACN 0.5 M TEABF<sub>4</sub> reported by Milshtein and co-workers (reproduced with permission from ref 454. Copyright 2016 The Royal Society of Chemistry). Constant current cycling at 100 mA cm<sup>-2</sup> (left), capacity vs cycle number at different current densities (right). (e) Molecule used by Sisto and co-workers to develop dialysis membrane-based ORFBs (left) together with the cycling performance (right), reproduced from ref 455.

3456 high-potential molecules in order to increase their solubility, 3457 and stability.<sup>451</sup> DBMMB offers the best compromise in terms 3458 of viscosity, stability and diffusion coefficient. Its redox 3459 potential is about 0.78 V vs Ag<sup>+</sup>/Ag, so it has been retained 3460 and implemented against several low-potential and highly 3461 soluble molecules: BzNSN and N-methylphthalimide 3462 (MePh).<sup>452,453</sup> MePh has a reduction potential of about 3463 -1.79 V vs Ag<sup>+</sup>/Ag in 1 M LiTFSI DME electrolyte. A major 3464 effort has been made to choose a porous membrane of the 3465 Celgard or Daramic-type that is effective in preventing species 3466 mixing and does not generate a too high ohmic drop. 3467 A Daramic 175 membrane was selected to make a complete 3468 redox-flow cell using an equimolar mixture of DBMMB and 3469 MePh at 0.3 M in 1 M LiTFSI DME electrolyte. Although 3470 tested only over about 50 cycles, the cell capacity is constant at  $_{3471}$  about 3 Ah L<sup>-1</sup> for an energy density of 9.3 Wh L<sup>-1</sup>. This cell is 3472 able to work at current densities close to those used in aqueous  $_{3473}$  ones: 50 mA·cm<sup>-2</sup> with no significant degradation of its perfor-3474 mance. At this current level, the energy efficiency remains 3475 above 60%. It is interesting to note that at low current the 3476 Coulombic efficiency is not very good due to the cross diffu-3477 sion of species through the porous membrane while at high 3478 current density the voltage efficiency drops due to the ohmic 3479 drop. The redox potential of BzNSN is -1.58 V vs Ag<sup>+</sup>/Ag in 3480 1 M LiTFSI ACN electrolyte, with its solubility being 2.1 M when considering 2.1 M LiTFSI ACN as the electrolyte. 3481

An electrolyte containing an equimolar mixture of BzNSN 3482 3483 and DBMMB (0.5 M) in 1 M LiTFSI ACN as electrolyte was 3484 cycled in a redox-flow cell composed of two carbon felt elec-3485 trodes and a Daramic type separator (800  $\mu$ m). Due to the 3486 viscosity of the solution and the problems of cross diffusion 3487 through the membrane, the current density applied is 10 mA·cm<sup>-2</sup>. The energy yield is 72%, mainly due to ohmic 3488  $_{3489}$  drops. The energy density is in the order of 6-8 Wh L<sup>-1</sup>. The 3490 stability of the cell is not very good (50 cycles) probably due to 3491 the reactivity at high concentration of the species that compose 3492 the electrolyte. These studies have shown that DBMMB derivatives 3493 are potentially relevant for the design of a fully organic redox-flow 3494 battery. They are extremely soluble in organic electrolytes (2-3 M)3495 and the radicals resulting from their oxidation are stable in DME 3496 solvents. The two low-potential molecules tested, particularly 3497 BzNSN, are soluble up to 5 M, but their solutions are highly 3498 viscous precluding their use in flowing cell.

Kentucky University has developed organically soluble 3499 3500 phenothiazine derivatives.<sup>454</sup> MEEPT has been selected as 3501 the most efficient compound: it is liquid at room temperature, 3502 and its solubility in 0.5 M nBu<sub>4</sub>NBF<sub>4</sub> ACN is greater than 2 M. 3503 It is electrochemically stable, and it is possible to prepare both 3504 forms, neutral and oxidized, easily by chemical methods. The 3505 core of the conversion cell has been optimized to reduce both 3506 ohmic drop and losses related to fluid flowing through the system (channel electrodes). The optimized cell has a resistance of about 3507  $_{3508}$  3.3  $\Omega$  cm<sup>-2</sup>. The assembly was tested in a symmetrical con-3509 figuration with an electrolyte composed of 0.5 M MEEPT at 50%  $_{3510}$  state of charge with a theoretical capacity of 13.4 Ah L<sup>-1</sup>. 3511 In constant current cycling at 50 and 100 mA $\cdot$ cm<sup>-2</sup>, the measured 3512 capacity is respectively 97.3% and 60% of the theoretical capacity. 3513 Over 100 cycles (80.6 h in total) at 100 mA cm<sup>-2</sup>, the capacity is 3514 maintained, and no significant loss is observed.

Columbia University, NY, has developed a flux battery based on perylene diimide derivatives (negative) and ferrocene tetramere (positive), both of which can achieve electron concentrations > 3518 1 M.<sup>455</sup> The interest of this work is to demonstrate that cellulose dialysis membranes, combined with redox compounds 3519 with a large hydrodynamic radius, are very efficient to avoid 3520 mixing the two electrolytes. The authors also carried out studies 3521 on aging both in cycling and calendars (even if carried out in 3522 diluted solution). They were able to demonstrate that in 11 days 3523 in the charged state, no significant loss of capacity was noted. 3524 The cell could be cycled 450 times with an average capacity loss 3525 of 0.00614% per cycle. 3526

All organic redox-flow cell faces a lot of problems to develop 3527 a commercially viable system able to really compete with 3528 aqueous inorganic chemistries. This is mainly due to the fact 3529 that the molecular parameters are all interdependent. The fact 3530 of wanting high cell voltages implies the use of compounds 3531 where reduced (materials with very low potential) or oxidized 3532 (materials with very high potential) forms are poorly stabilized 3533 and therefore very reactive. From a solubility point of view, the 3534 use of highly concentrated solutions further increases decom- 3535 position phenomena. This often results in poor cycling stability 3536 and is in addition to the fact that calendar aging is almost never 3537 achieved or under very diluted conditions that are more 3538 favorable.<sup>456</sup> Organic solutions that are highly concentrated 3539 generally become highly viscous, causing problems for flowing 3540 (pumps power consumption) and voltage efficiencies as these 3541 solutions become less conductive. The diffusion coefficients of 3542 redox species and ions decrease when viscosity increases with 3543 the result of lower apparent electron transfer kinetics. This 3544 results in high overvoltage values and low energy yields, often 3545 well below 60%. This probably explains why there are no flow 3546 cell studies at concentrations above 2 M in the literature, while 3547 several molecules have higher solubility values. The main 3548 interest of the studies in organic media is that due to the 3549 swelling of conventional ion exchange membranes and a high 3550 cross over, combined with low electrolyte conduction (high 3551 overvoltage), the community has been forced to develop 3552 membrane-free approaches, some of which have proven to be 3553 relevant. 3554

### 9.4. Summary

The use of organic molecules to make electrolytes for flow 3555 batteries is now well described in the literature. Dozens of dif- 3556 ferent molecules have been tested in various cell configurations. 3557 From a properties and behavior point of view, electrolytes based 3558 on organic molecules face the same problems as inorganic 3559 compounds: solubility, high viscosity of concentrated solutions 3560 with the result of a decrease in apparent electron transfer kinetics 3561 (overvoltage between charge and discharge), and a high power 3562 consumption by the pumps. Since the intrinsic stability of 3563 organic molecules in solution is lower than the stability of inor- 3564 ganic compounds, cycling and calendar stability are generally 3565 less good.

This stability aspect remains the key point to go further. 3567 Many parameters must be taken into account to understand 3568 the degradation of ORFB performance: molecules in solutions 3569 are much more reactive than in the solid state, in addition they 3570 are in contact with different materials (plastic, stainless steel, 3571 and so on) which can act as catalysts. Most of these com- 3572 pounds are sensitive at least in one redox state to oxygen 3573 traces, which is difficult to prevent in the long term (leakage). 3574 Reactions are also possible, for example, with other com- 3575 ponents of the electrolyte, such as the solvent (substitution 3576 reactions, hydrolysis, ...), the supporting salts, or the molecule 3577 itself (dimerization or polymerization reaction). In addition, 3578 reactivity may change with molecules redox states, a reduced 3579 3580 one will be more sensitive to reactions with an electrophile, 3581 while oxidized molecules will be more sensitive to reactions 3582 with nucleophiles. Therefore, it is necessary that all other 3583 components of the electrolytes be as unreactive as possible. 3584 It can be expected thanks to functionalizations to stabilize a 3585 molecule by blocking some degradation reactions. For 3586 example, the reduced state of dihydroxyanthraquinone tends 3587 to degrade through oxidative coupling. To avoid this side 3588 reaction, the functionalization of hydroxyl groups by PEG, 3589 alkyl carboxylate, or alkyl phosphate chains has been 3590 successfully proposed. However, these new molecules become 3591 sensitive to hydrolysis reactions and degradation reactions can 3592 occur.<sup>431,457</sup> This observation is general; attempting to stabilize 3593 a molecule in a given electrolyte may result in a change of its 3594 reactivity or redox property that makes the molecule less or no 3595 more relevant for the application.

In most cases, crossover phenomena through the mem-3597 branes are harmful. To compensate forthis, the development of 3598 stable molecules in at least three stable redox states, which can 3599 serve both as posolytes and as negolytes (such as vanadium), 3600 would greatly improve the stability of ORFBs. This would 3601 also allow the reservoirs to be rebalanced when the transfer 3602 of solvent by electro-osmosis becomes too high. All these 3603 constraints result in rather low overall energy yields (655%) 3604 compared to other battery-based storage systems (90%) but 3605 much better than the cycle associated with hydrogen: 3606 "electrolyzer, storage, fuel cell" whose total efficiency is around 3607 25%. From the grid point of view, the real advantage of RFBs is 3608 that they decouple power and energy; they are the only storage 3609 systems that allow this.

For the development and credibility of ORFBs, it is now 3610 3611 necessary to rationalize the tests and studies carried out in the 3612 literature. Indeed, few tests are carried out under the same 3613 conditions and these are generally not representative of the 3614 final application. For example, it is important that systems 3615 should be tested at the highest possible concentrations. Systematic 3616 studies of cycling and calendar aging must be carried out. During 3617 cycling studies, it is important that the time of each cycle be 3618 representative of the RFB application (i.e., 4 to 12 h of energy 3619 storage). With regard to the flow rates used to carry out the 3620 measurements, very often they are disproportionately high to 3621 compensate for the high viscosity of the concentrated solu-3622 tions. Moreover, depending on the cell geometry used, the flow 3623 rate does not have an important meaning. It would be more 3624 interesting to indicate the linear velocity of the fluid on the 3625 surface of the electrodes and to keep these values as low as 3626 possible to avoid that the pumps consume more energy than 3627 the energy stored in the battery.

### **10. CONCLUDING REMARKS**

3628 Almost 170 years after the invention of the first operational 3629 rechargeable battery by G. Planté thanks to metal-based elec-3630 trode materials, this tutorial review was intended to highlight 3631 several opportunities offered at the turn of the 21st century by 3632 the reversible redox chemistry to promote innovative electro-3633 chemical devices based on naturally abundant chemical 3634 elements (including biomass) while improving the environ-3635 mental footprint. Indeed, we have shown in this article that the 3636 world has drastically changed since Planté's invention through 3637 the ongoing modernization of our societies but at the price of 3638 continuous consumption of both energy and nonrenewable 3639 materials at the expense of the environment.<sup>115</sup> Changing the 3640 historic roadmap followed by our current energy engineering is nowadays mandatory in the general interest. In this context, 3641 global demand for batteries multiplies to store renewable energy, 3642 promote electromobility, and power the continued development 3643 of portable electronics and emerging technologies (mobile 3644 devices, IoT, AI, robotics, etc.). Seeking to develop innovative, 3645 efficient, and less polluting and energy consuming chemistries 3646 is therefore important today while jointly developing better 3647 recycling solutions (and second use). 3648

Depicted as a parallel and relatively recent research field in 3649 the history of rechargeable electrochemical storage systems, we 3650 have sequentially summarized the present state-of-the-art and 3651 highlighted important works that have contributed to the recent 3652 progress in organic-based rechargeable systems by covering all 3653 possible technologies and cell configurations to date. The 3654 as-obtained performance figures have been described without 3655 avoiding limitations. Some of the key performance metrics of 3656 organic electrode compounds such as specific energy, working 3657 potential, and cycling stability already look promising, and 3658 material design strategies specific to these metrics have been 3659 preliminarily established. Challenges remain for developing 3660 efficient storage solutions that simultaneously excel in all these 3661 metrics. It seems probable that the practical use of organics for 3662 the electrochemical storage in a near future could be through 3663 the development of ORFBs due to their attractive features of 3664 high power density and low cost for large-scale energy storage. 3665

In terms of solid electrode materials (for "sealed" batteries), 3666 electroactive molecules with simple structures such as simple 3667 quinones could offer the best balance between high discharge 3668 potential and high specific capacity, but stable cycling requires 3669 proper immobilization of these molecules which, until now, 3670 cannot be done without impacting potential and capacity. Two 3671 directions may directly counter this dilemma. The first is a 3672 chemical path revolving no-compromise immobilization. Rational 3673 connection of molecular building blocks complemented by 3674 suitable synthesis methods has been successful in preserving 3675 the full redox characteristics of active cores as seen in OEMs 3676 like PAQS and P(NDI2OD-T2). The second is to suit OEMs 3677 with solid electrolytes where dissolution is a nonissue. Solid- 3678 state batteries are emerging as an alternative to the traditional 3679 liquid electrolytes to enable safer and higher-energy batteries. 3680 The nondissolving nature of solid electrolytes is an additional 3681 perk specifically useful for organic batteries. In addition, p-type 3682 materials could offer access to molecular (metal-free) batteries 3683 as well as possible assemblies with n-type systems to promote 3684 dual-ion cells. 3685

Continued evolution of organic batteries will inevitably 3686 involve a better understanding of involved electrochemical mecha- 3687 nisms (especially in the solid state) as well as the development of 3688 new OEMs, which is both a strong suit for organic compounds 3689 from the fundamental study point of view and a potential 3690 uncertainty for practical applications. Organic compounds are 3691 known to have good tuning knobs to manipulate the molecular 3692 structures and many subsequent properties, but complicated 3693 functionalization can drive up synthesis cost. Two currently 3694 practiced approaches could lead to a balance between per- 3695 formance and cost. One scours through structures that can be 3696 synthesized from cheap raw materials via simple, few-step, and 3697 high-yield reactions, the other prioritizes function and 3698 performance with no specific focus on minimizing cost. At an 3699 early stage of research and development, the former approach 3700 rarely affords high-performance candidates due to the limited 3701 options, while the latter could end up with prohibitive costs. 3702 Overtime, however, the building blocks found by the former and 3703

3704 the design strategies established by the latter will merge the two	ASSOCIATED CONTENT	3766
3705 approaches and strike the balance.	Supporting Information	3767
3706 Beyond the direct using of redox-active organics as the main		
3707 active electrode compounds, other functionalities can be used	The Supporting Information is available free of charge	
3708 in an electrochemical cell such as the hybridization of the	https://pubs.acs.org/doi/10.1021/acs.chemrev.9b00482.	3769
3709 conventional inorganic active materials with organic redox-	Evolution of the global EV stock by vehicle's cate	gory; 3770
3710 active polymers giving rise to fast electrode kinetics. Thus let	estimated world LIB manufacturing capacity	for 3771
3711 us recall that electrical properties of solid composite electrodes	automotive applications, International trade flows	, and 3772
3712 are critical to electrochemical performances, whatever the	LIB cell manufacturing capacities in 2016; critica	l raw 3773
3713 considered technology. This is especially the case for thick	Materials in the EU, 2017; world mining ind	lustry 3774
3714 electrodes which are highly sought-after because they enable in	production for materials used in LIBs in 2016	; the 3775
3715 principle simultaneous increase in volumetric and specific	concept of renewable organic battery; selection of re	edox- 3776
<sup>3716</sup> energy densities and decrease in price. It is estimated that 20 to	active units used in ORFBs. (PDF)	3777

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The authors declare no competing financial interest.	3803
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#### **Biographies**

Philippe Poizot was born in Crépy en Valois (France) in 1975. After a 3805 Master of Science in analytical chemistry and electrochemistry 3806 (University of Paris VI, 1998), he obtained his Ph.D. degree in 3807 Materials Science (2001) focused on "conversion reactions" under the 3808 guidance of J.-M. Tarascon at the University of Picardy Jules Verne 3809 (UPJV-LRCS) in Amiens, France. After a postdoctoral training with 3810 J. A. Switzer at the University of Missouri-Rolla (USA) to develop 3811 the electrodeposition of nanostructured materials, he came back to 3812 UPJV-LRCS as Associate Professor in 2002. In 2007, he proposed the 3813 concept of "renewable" batteries by promoting novel electrode 3814 materials based on redox-active organic compounds deriving from 3815 biomass. In 2012, he was appointed as full Professor at University of 3816 Nantes (Institut des Matériaux Jean Rouxel, IMN-CNRS, Nantes, 3817 France). His current research topics are mainly focused on 3818 rechargeable batteries, molecular electrochemistry, and the develop- 3819 ment of organic batteries in both aqueous and nonaqueous 3820 electrolytes. He is a recipient of the Bronze Medal of the French 3821

3717 80% of power losses in the case of a thick electrode originate 3718 from insufficient electronic conduction.<sup>458</sup> The design of 3719 electronic conductivity at different scales is not easy, because it 3720 is currently based on the use of carbon-based conductive addi-3721 tives that are difficult to disperse homogeneously on the one 3722 hand, and on the other hand, that renders difficult the manu-3723 facturing of thick composite electrodes, because of the unstable 3724 nature of the electrode inks. In addition, the loss of intercluster 3725 and interparticle contacts due to volume variations of active 3726 materials is a major cause of the aging of battery electrodes.<sup>459</sup> 3727 It is therefore mandatory to add polymeric binders (insulators), 3728 with the downside of a difficult compromise between electronic <sup>3729</sup> conductivity and mechanical properties of the composite <sup>3730</sup> electrode.<sup>460</sup> The use of electron conducting binders or even 3731 redox binders ("smart binder") appears therefore quite 3732 attractive, since it would enable the design of electrodes with 3733 lower amount of carbon and binder additives. This objective  $_{3734}$  was pursued in the particular case of LiMPO<sub>4</sub> (M = Fe, Mn). 3735 As early as 2006, Goodenough and co-workers showed that 3736 carbon-coated LiFePO<sub>4</sub> particles can be directly connected 3737 to the current collector using a matrix of p-doped PPy or 3738 PAni,<sup>461-463</sup> while Gräetzel was actually the first to connect 3739 non-carbon-coated LiMPO<sub>4</sub> (M = Fe, Mn) particles to the 3740 current collectors using molecular wires.<sup>464</sup> In the latter, the 3741 Fermi levels of the organic matter and the active material need 3742 to be adjusted while the adsorbed wires should be percolated 3743 to allow for cross-surface charge. This approach was also recently 3744 investigated by Nishide and Oyaizu using nonconjugated radical 3745 polymers (radicals are densely introduced as the pendant groups) that were specifically designed for fast charging of LiFePO<sub>4</sub> 3746 or LiCoO2. 465 Schougaard and co-workers also showed a poly(3,4-ethylenedioxythiophene) coating at the surface of bare 3748 LiFePO<sub>4</sub> particles advantageously replaced the carbon coating.<sup>4</sup> 3749 Targeting the contemporary concerns of industry-relevant 3750 electrodes and especially thicker ones, Gaubicher and Blan-3751 chard<sup>467</sup> used a short thiophene-based  $\pi$ -conjugated system as a 3752 molecular junction between uncoated LiFePO4 and multiwall 3753 carbon nanotubes within undensified 2 mAh cm<sup>-2</sup> electrodes. 3754 Electrochemical and electrical properties of such electrodes 3755 demonstrate the key role of molecular junctions to reach power 3756 and cyclability performances comparable to those of carbon-3757 coated LiFePO<sub>4</sub> electrodes. 3758 To conclude, although this research activity is still in its 3759 3760 infancy and much remains to be done to get attractive per-

**Chemical Reviews** 

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3761 formances, redox-active organic compounds can be perceived 3762 today more than ever as an alternative chemical choice 3763 depending on the targeted application. We hope that this 3764 review will be a source of original and fresh ideas for our 3765 readers.

3822 Society for Encouragement and Progress (2002) and was a Junior 3823 Fellow of the Institut Universitaire de France (2012–2017).

3824 Joël Gaubicher was born in Saint-Germain-en-Laye (France) in 1972. 3825 He studied chemistry and materials engineering in Paris. After 3826 obtaining a Ph.D. from the P&M Curie University of Paris, he joined 3827 the University of Waterloo, Canada, as a postdoctoral fellow with 3828 Prof. L. F. Nazar where he worked on phosphates and borates for Li 3829 ion battery. In 2001, he obtained a full CNRS researcher position at 3830 the Institut des Matériaux Jean Rouxel in Nantes and developed 3831 research programs dealing with Li metal polymer, Li-ion, Na-ion, and 3832 Li/S batteries and supercapacitors. His main interests deal with solid 3833 state electrochemistry of inorganic and organic materials as well as 3834 synthesis and electrochemical mechanisms mainly through operando 3835 characterizations. He was the recipient of a CNRS award for his 3836 research in 2013. More recently, he has been developing aqueous 3837 battery and supercapacitor chemistries based on organic electroactive 3838 materials.

3839 Stéven Renault was born in Longjumeau (France) in 1980. He 3840 studied biochemistry and chemistry and obtained his Ph.D. in 3841 chemistry from Université de Rennes 1 in 2007 focused on drug 3842 design and medicinal chemistry. After working as a postdoctoral 3843 fellow in Amiens, he joined the group of Kristina Edström and Daniel 3844 Brandell in the Ångström Advanced Battery Center (Uppsala 3845 University, Sweden) as a researcher in 2011. Since 2018, he joined 3846 Université de Nantes as an Associate Professor at the Institut des 3847 Matériaux Jean Rouxel. His research interests focus on Li/Na/Mg 3848 organic batteries and Li–air batteries.

3849 Lionel Dubois was born in Strasbourg (France) in 1973. He studied 3850 chemistry at "Ecole Nationale Superieure de Chimie de Paris". After 3851 obtaining a Ph.D in molecular chemistry from Grenoble Alps 3852 University he joined the University of Groningen (NL) as a 3853 postdoctoral fellow with Prof. B. L. Feringa where he worked on 3854 new iron based catalyst for alkane oxidation by molecular oxygen. 3855 Then he moved to the NMR laboratory of the French Atomic Energy 3856 Commission in Saclay under the direction of Dr. H. Desvaux on the 3857 development of laser polarized xenon NMR. In 2004, he obtained an 3858 assistant professor position at the University Institute of Technology 3859 of Castres (France), before being recruited as researcher at the French 3860 Atomic Energy Commission (CEA) in Grenoble in 2005. He 3861 developed a program related to the use of molecular chemistry for 3862 communication and information technologies and since 2011 has 3863 been working on the use of molecular compounds for energy storage. 3864 In 2017 he took the head of the "Molecular Architecture Conception 3865 and Electronic Process" laboratory of the CEA—Grenoble. His main 3866 interest deals with coordination chemistry, synthesis of new ligands, 3867 graphene chemistry, solution electrochemistry, and diverse spectros-3868 copies (NMR, EPR) or operando experiments for energy applications, 3869 mainly organic batteries and supercapacitors.

3870 Yanliang Liang was born in Guangzhou (China) and studied materials 3871 physics and chemistry at Nankai University (China). He conducted 3872 his Ph.D. research on organic batteries and photovoltaics under the 3873 supervision of Prof. Jun Chen at Nankai University. After receiving his 3874 Ph.D. in 2012, he worked as a postdoctoral fellow with Prof. Yan Yao 3875 at University of Houston on low-cost safe battery technologies. He is 3876 now a Research Assistant Professor at University of Houston focusing 3877 on energy storage materials and next-generation battery develop-3878 ments.

3879 Yan Yao was born in Nantong (China) and studied materials science 3880 in Fudan University (China). He conducted his Ph.D. research on 3881 organic photovoltaics under the supervision of Prof. Yang Yang at 3882 UCLA. He served as a senior scientist at Polyera Corporation from 2008 to 2010 and a postdoctoral fellow at Stanford University under 3883 the supervision of Prof. Yi Cui from 2010 to 2012. He joined the 3884 University of Houston as Assistant Professor of Electrical and 3885 Computer Engineering in 2012 and is now Associate Professor. His 3886 research interests focus on developing new materials for Li ion 3887 batteries and post-Li battery chemistries such as organic, Na, Mg, and 3888 solid-state batteries. 3889

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