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A. Dépée, P. Lemaitre, T. Gelain, A. Mathieu, M. Monier, et al.. Theoretical study of aerosol particle electroscavenging by clouds. Journal of Aerosol Science, 2019, 135, pp.1-20. 10.1016/j.jaerosci.2019.04.001 . hal-02527503

HAL Id: hal-02527503 https://hal.science/hal-02527503

Submitted on 26 Nov 2020

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Contents lists available at ScienceDirect

Journal of Aerosol Science

journal homepage: www.elsevier.com/locate/jaerosci

Theoretical study of aerosol particle electroscavenging by clouds

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ARTICLE INFO

Keywords: Aerosol particle scavenging Brownian motion Collection efficiency Electrophoresis Images charge

ABSTRACT

This paper describes a theoretical model which computes the collection efficiency of aerosol particles by droplets, due to the combined action of dynamic (inertia, weight and drag) and electrophoresis forces acting on an aerosol particle of radius $0.004 \le a \le 1.3 \,\mu\text{m}$ around a droplet of radius $15 \le A \le 100 \,\mu\text{m}$. The electrostatic forces are defined following the concept of image charges. In the given particle range, the Brownian motion must be considered and was consequently added to the model. A novel approach is developed, based on the Langevin's theory and solved using an Itô process. Results of electroscavenging related to natural atmospheric ionisation, as well as for strongly charged aerosol particles released after a nuclear accident, are presented with pressure and temperature representative of the mid-troposphere (-17°C, 540 hPa). The droplet charges considered in the paper are representative of weakly and strongly electrified clouds. The values of collection efficiency computed are convenient for incorporation into cloud models and to study scavenging of aerosol particles by clouds whether for climate, pollution or nuclear safety issues.

1. Introduction

Aerosol particles (APs) play an important role for weather and climate. Since they act on cloud formation and their concentration, chemical composition and size distribution affect the droplet size distributions and precipitation (Tao, Chen, Li, Wang, & Zhang, 2012), they control cloud cover which in turn modulates albedo (Twomey, 1974) - changing the Earth's energy budget. Furthermore, APs have been reported as causing respiratory disorders in humans (Limbach et al., 2007). Consequently, APs are essential in major environmental and medical challenges where the processes involving their production or removal are active areas of research.

In an atmospheric environment, AP concentration derives from the equilibrium between the formation and removal processes. They are primarily generated by sea spray, wind-driven dust, volcanic eruptions and human activities releases - and secondarily generated by homogeneous nucleation of gaseous species and ion-induced nucleation. The AP sizes range from 1 nm to several hundred microns (Jaenicke, 1993), which is highly dependent on their origin. Also, the AP atmospheric lifetime is related to their size. Indeed, just hours after emission, the heaviest particles settle on the ground due to gravity and the smallest particles, which are sensitive to Brownian motion, diffuse and coagulate. Intermediate particle sizes are referred to as the accumulation size mode (Whitby, 1973), with diameter from 0.08 to $2 \mu m$. In this size range, in the absence of cloud and precipitations, the APs have no

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https://doi.org/10.1016/j.jaerosci.2019.04.001

Received 21 December 2018; Received in revised form 26 March 2019; Accepted 1 April 2019 Available online 29 April 2019







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efficient removal process and can remain in the troposphere for one week up to several months (Jaenicke, 1993). The tropospheric lifetime of this AP size mode is determined by interactions between APs and clouds, and called wet removal. Hence, an understanding of wet removal processes is a fundamental topic in local pollution studies (Chang, 1986; Jylhä, 1999; Okita, Hara, & Fukuzaki, 1996).

In pollution events, radioactive releases from a nuclear accident can jeopardise both ecosystems and human health. Substantial efforts are needed to understand the radioactive material's life cycle in the atmospheric environment and forecast where and when these releases will reach the ground. Besides, studies have shown that after the Chernobyl nuclear accident (1986), far from the reactor, caesium-137 (*C*137*s*) atoms were attached incorporated into the accumulation size mode and transported over long distances on a continental scale (Baltensperger, Gäggeler, Jost, Zinder, & Haller, 1987; Devell et al., 1986; Jost et al., 1986; Pöllänen, Valkama, & Toivonen, 1997). Thus, in such cases wet removal is the dominant process for radionuclides scavenging (Jylhae, 1991; Sparmacher, Fülber, & Bonka, 1993; Baklanov & Sørensen, 2001).

Wet removal can be distinguished into two mechanisms - the below-cloud scavenging and the in-cloud scavenging. Below the cloud, APs can be collected by precipitation meanwhile, in-cloud, APs can be activated into hydrometeors or collected by cloud droplets. Moreover, the scavenging of multiple APs by a droplet that then evaporates can cause AP coagulation and be a loss process for small AP. On average, the in-cloud removal is the most efficient mechanism. Indeed, Flossmann (1998) has shown numerically that for a convective cloud, 70% of the AP mass scavenged results from the in-cloud removal. This result is coherent with Laguionie et al. (2014) who deduced from measurements that, for every type of cloud, on average 60% of the net scavenging is due to the clouds.

In most of the current models, wet removal is quantified by a scavenging coefficient A (Baklanov & Sørensen, 2001; Chate et al., 2003; Quérel, Monier, Flossmann, Lemaitre, & Porcheron, 2014a; Sportisse, 2007). This parameter is defined as the fraction of APs captured by drops per unit time (definition in Appendix A). For pragmatic purposes, this parameter is quite often computed to be a function of bulk quantities readily available from measurements, such as the precipitation rate on the ground (Scott, 1982; Jylhä, 1999; Mircea, Stefan, & Fuzzi, 2000; Quérel, Roustan, Quélo, & Benoit, 2015). Few significant experimental works have been dedicated to comparing theoretical descriptions of the scavenging coefficient with measurements. These recent reports have concluded that the current descriptions need improvements. Indeed, the theoretical scavenging coefficients are underestimated (Volken & Schumann, 1993; Laakso et al., 2003; Chate et al., 2003; Chate, 2005; Mathieu et al.,), sometimes by up to three orders of magnitude. In fact, this kind of expression is quite convenient but describes the wet removal at the mesoscale and does not include microphysical effects appearing in-cloud. This description can then be more or less reliable to define the AP removal by raindrops but fails to describe the in-cloud removal. In fact, no description of the in-cloud removal is available in the literature for bulk models while this mechanism dominates (as previously mentioned).

Therefore, this study focuses on the in-cloud AP collection through a parameter directly correlated to the scavenging coefficient, referred to as the collection efficiency (EC). The collection efficiency is the ratio between the AP mass (or number) collected by the droplet over the AP mass (or number) within the volume swept by the droplet for a given AP radius. It can also be defined as the ratio of the cross-sectional area inside which the AP trajectories are collected by the droplet over the cross-sectional area of the droplet. Several papers have been dedicated to theoretically and experimentally estimating this parameter under a wide variety of conditions (Greenfield, 1957; Grover, Pruppacher, & Hamielec, 1977; Lemaitre et al., 2017; Mohebbi, Taheri, Fathikaljahi, & Talaie, 2003; Quérel et al., 2014a; Slinn, 1977; Wang, Grover, & Pruppacher, 1978; Wang & Pruppacher, 1977). For millimetric raindrops, three main mechanisms lead to the collection - Brownian motion, inertial impaction and interception, meanwhile phoretic effects like diffusiophoresis, thermophoresis and electrophoresis are pushed to the background. Indeed, due to the very large terminal velocity of the millimetric raindrops, the associated drag force is significantly stronger compared to the phoretic forces. This fact has been theoretically demonstrated by Grover et al. (1977) and experimentally validated by Quérel et al. (2014b) for diffusiophoresis. However, for the in-cloud collection of APs, the droplets are in the micrometric size range so the drag force has the same order of magnitude as the phoretic effects. Consequently, AP collection by cloud droplets is strongly affected by the phoretic effects (Wang et al., 1978).

It is well known that cloud droplets (Takahashi, 1973) as well as radioactive and non-radioactive APs (Harrison, 1992; Clement & Harrison, 1992, 1995a, 1995b, 2000) are electrically charged. Few theoretical works have studied the impact of the electrostatic forces on AP collection by micron-size droplets (Tinsley, Rohrbaugh, & Hei, 2001, 2006, 2000; Jaworek et al., 2002). Since the APs fall in the accumulation mode size in clouds, more thorough examinations have been performed by Tinsley (2010) and Tinsley and Zhou (2015), in coupling the electrostatic forces with the Brownian motion. Nevertheless, both studies consider a droplet radius less than 15 µm with weakly charged droplets and APs.

The present paper extends previous works to droplet radii ranging up to $100 \,\mu$ m. Strongly charged droplets and APs are also considered to model stratiform/convective clouds and radioactive APs respectively. Finally, the Brownian motion modelling sets this paper apart from the work of Tinsley (2010) and Tinsley and Zhou (2015) which only considered a random walk affecting the AP location. A more precise Lagrangian method is developed here and based on the recent paper of Cherrier, Belut, Gerardin, Tanière, and Rimbert (2017). The AP radius range considered ($a \in [4 \text{ nm}; 1.3 \,\mu\text{m}]$) is the same as that chosen in Tinsley and Zhou (2015), to cover all the AP sizes prone to exist in the atmosphere. Assuming the largest APs ($a > 1.3 \,\mu\text{m}$) settle on the ground or are activated in droplets following the Köhler theory (see Pruppacher et al., 1998) Sect. 6.5), they have not been considered in our study.

Our paper is divided into three sections. First, the electric charges considered in the paper are justified. The Lagrangian model is then fully described and verified. Finally, numerical results are given and discussed.

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Droplet radius	Droplet charge (convective case)	Droplet charge (stratiform case)
15 μm 25 μm 37.5 μm 50 μm 75 μm 100 μm	$\begin{array}{c} 9.4\times10^{3} e \\ 2.6\times10^{4} e \\ 5.9\times10^{4} e \\ 1.0\times10^{5} e \\ 2.3\times10^{5} e \\ 4.2\times10^{5} e \end{array}$	$\begin{array}{c} 2.2 \times 10^2 e \\ 4.3 \times 10^2 e \\ 7.3 \times 10^2 e \\ 1.1 \times 10^3 e \\ 1.8 \times 10^3 e \\ 2.6 \times 10^3 e \end{array}$

 Table 1

 Estimated droplet charge according to the measurements of Takahashi (1973).

2. Electric charges considered in the study

2.1. Cloud droplet electric charges - order of magnitude

In our paper, the droplet charge range is extended beyond the values studied by Tinsley and Zhou (2015) which have only focused their study on weakly electrified clouds. Several mechanisms are involved in cloud charging such as the diffusion of ions, convection and the drop breakup (the description can be found in Pruppacher et al., (1998), Section 18.5). Takahashi (1973) measured the droplet charge *Q* in both weakly (warm clouds) and strongly electrified clouds (thunderstorm). Two experimental data sets are given in Pruppacher et al., (1998) (sect. 18.4) and through these measurements the mean droplet charge for both types of clouds can be evaluated. The droplet charge range considered in this article is presented in Table 1., following the droplet radius range under investigation. The electric sign of the cloud droplets is variable according to the authors (Takahashi, 1973). Indeed, the predominant electric sign changes with the sampling position in the cloud, the type of cloud and the droplet size. Thus, both signs are considered in this paper.

2.2. Radioactive AP electric charge evaluating

The charge q of the non-radioactive AP results mainly from cosmic radiations and ground radioactivity, creating ions which attach to the AP. It is assumed that its electric charge follows a Boltzmann distribution. Moreover, when the AP enters the cloud it can induce an increase of the AP charge through an in-cloud space charge generated by the downward flow of current in the global electric circuit (Zhou & Tinsley, 2007). Thus, |q| ranged from 0 to 50 e which fits with the range used by Tinsley et al. (2015). Only the positive sign is considered for symmetry reasons of the electrostatic force expression (Equation (7)) between the droplet charge (where both signs are used) and the AP charge.

During a decay, the radioactive AP charges itself according to the beta or alpha particle emitted. Once emitted, the particle ionises the surrounding environment, creating a large number of ions which recombine with each other or diffuse and then attach to the radioactive AP. Clement and Harrison (1992) developed a theoretical model to calculate the mean radioactive AP charge. A complete description of radioactive AP charging can be found in their work.

In the case of a radionuclide release occurring in the atmosphere, the radioactive AP is strongly diluted in the non-radioactive AP. The Clement and Harrison model (1992) is then simplified and the mean radioactive AP charge q_{mean} is given in Clement and Harrison (1995b, 1995a, 2000) by:

$$q_{mean} = \frac{\eta \varepsilon_0}{e\mu_n},\tag{1}$$

where η is the radioactive decay rate of the AP, μ_{-} is the electrical mobility of the negative ions, n_{-} the concentration of the negative ions given by:

$$n_{-} = \left(n_{b-}^{2} + I \frac{(Z+1.91)\eta}{\alpha}\right)^{\frac{1}{2}},\tag{2}$$

where n_{b-} is the background negative ion concentration, *Z* is the radioactive AP number concentration, *a* the ion recombination coefficient and *I* is the ion pair production per decay. For a β -decay, *I* is equal to $E_{max}/(3\omega_i)$ with E_{max} the maximum beta particle energy and ω_i the mean energy required to form an ion pair. In Appendix A the numerical values used to evaluate the q_{mean} are given.

The present paper focuses on caesium particles (C^{137}) which can induce long-term contamination of the ground and persist for decades in the atmosphere through a long half-time (30 years). After the discharge of radioactive materials from the Fukushima Daiichi nuclear power plant (FDNPP), few studies have been performed in order to evaluate the decay rate and the caesium particle concentration. Kaneyasu, Ohashi, Suzuki, Okuda, and Ikemori (2012) analysed the air in the later stage of the accident from 28th April to 26th May (after the first nuclear plumes). They measured the caesium attached to the sulphate particles, in the accumulation mode size range (with a radioactive AP radius < 0.35μ m). They evaluated a low decay rate for the radioactive AP and a very high concentration. Finally, the radioactive materials emitted from FDNPP in the later stage which can be transported over long distances on a continental scale have similar charges compared to the non-radioactive AP. Nevertheless, Adachi, Kajino, Zaizen, and Igarashi (2013) measured the properties of the caesium-bearing particles released in the early stage of the accident (during the first nuclear plumes). They found a low caesium-bearing particle concentration *Z* of 10 m⁻³ with a large decay rate η of 1.4 Bq per particle. These



Fig. 1. Computational domain - the injection disc of AP and airflow around the droplet (scheme not scaled).

measurements represent an upper limit of the radioactive AP charge, even though these caesium-bearing particles are heavy and beyond the accumulation mode size with a mean radius of $1.3 \mu m$ (Adachi et al., 2013). Thus, this part of the radioactive materials emitted from FDNPP has only been transported on the scale of Japan.

Through the Adachi et al. (2013) measurements, the Clement and Harrison (1992) model for the mean radioactive AP charge in a non-confined environment (Clement & Harrison, 1995a, 2000) gives $q_{mean} \approx +600 e$. Thus, in the current paper, the AP charge q ranges from 0 to 600 e. Simulations were performed with zero, five, twenty and fifty elementary charges for the non-radioactive case following Tinsley and Zhou (2015). Also, an AP charge of six hundred elementary charges is used in order to evaluate the upper limit of the collection efficiency related to strongly charged radioactive APs which were released in the early stage of the FDNPP accident. It is assumed this upper limit is set for the whole AP size range, even if the Adachi et al. (2013) measurements were performed for heavy APs with a mean radius of $1.3 \mu m$.

3. Model description

3.1. Overview

In the present model, the collection efficiency of AP by droplets is evaluated from Lagrangian tracking of the AP around a droplet which falls at terminal velocity in air. The Cartesian coordinate system \mathscr{R} = (X, Y, Z) was used in the study, where the droplet is placed at the origin. For practical reasons, AP are considered spherical. Moreover, for a droplet radius of up to 140 μ m, there is a negligible deformation of the spherical droplet geometry (Pruppacher & Beard, 1970). Thus, in the range considered, the droplet is also a sphere.

An injection disc of an AP, noted Dk_{inj} , is set upstream of the droplet and centred on the *Z* axis as shown in Fig. 1. The distance between the disc and the droplet centre is far enough from the droplet to avoid any disturbance of the airflow by the droplet which could initially affect AP motions. It was found that 8 droplet radii *A* is a suitable distance, a wider distance increased the computation time without affecting the results. Downstream of the droplet, the APs are tracked up to 6*A* in case of rear captures due to the electrostatic forces, the Brownian motion or gravitational settling. The disc intercepted by the droplet in Dk_{inj} is called $Dk_{inj,A+a}$, equal to a disc radius of the sum of the droplet (*A*) and AP (*a*) radii.

As in Cherrier et al. (2017), the collection efficiency is evaluated by the ratio of the AP number set initially in $Dk_{inj,A+a}$ over the AP number collected by the droplet at the end of the computation (see section 3.3.5). The AP coagulation is neglected in the model.

3.2. Flow field modelling

In the present model, droplets are set as simple collector since the in-cloud droplet concentration are overall low enough - about 50 droplets per cubic centimetre (Squires & Twomey, 1958) - to lead to a droplet-droplet mean distance larger than the mean boundary layer thickness. The assumption is made that the effect of the flow around the AP on the motion of the droplet can be neglected. Indeed, according to Tinsley, Zhou, and Plemmons (2006), there is no significant disturbance on the airflow if the AP mass m_{AP} is more than thousand times lower than the droplet mass M_A ($m_{AP}/M_A \leq 10^{-3}$) as is the case in the AP and droplet ranges considered here. Thus, the flow surrounding the droplet is only caused by its fall.

The internal circulation is not modelled in the current model since there is no effect on the external flow around the droplet. Indeed, LeClair, Hamielec, Pruppacher, and Hall (1972) have shown that for water droplet with Re < 10 the external flow patterns are insensitive to the interior flow and the drag coefficient for a rigid sphere differs by less than 1% from the drag coefficient for a fluid sphere. More recently, Oliver and Chung (1987) extended the computations of LeClair et al. (1972) to moderate Reynolds number

Re < 50. The maximum Reynolds number considered is the current paper is 7.42 ($A = 100 \mu m$).

The turbulence in the cloud can also have an impact on the AP collection and the collection efficiency since it may affect the APs/ droplets location and motion (Shaw, 2003). However, the effects of the turbulence have been neglected here.

A 3D computational domain must be used due to the Brownian motion which is a 3D process. Nevertheless, the airflow caused by the falling droplet is purely axisymmetric in the droplet range considered ($A \le 100 \,\mu$ m and $Re \le 7.42$, see Pruppacher et al., (1998), Sect. 10.2). Thus, for every time step and every AP, we define the plane including the Z-axis and an AP (see Fig. 1) and we compute the airflow in this 2D computational domain in order to get the fluid velocity at the AP location $U_{f@AP}$. The flow field modelling is subdivided into two cases following the droplet radius *A*.

3.2.1. $A \leq 30 \ \mu m$ - analytical expressions

For a low Reynolds number ($Re \ll 1$), the non-linear term in the Navier-Stokes equation can be neglected. Thus, an analytical expression can be found which leads to the well-known Stokes flow expression. This solution results from the assumption that the advective inertial forces are small compared to the viscous forces - which is true near the droplet but incorrect for an increasing distance. This is called the "Stokes paradox".

Here, the flow surrounding the droplet is modelled according to Tinsley et al. (2006) - the Oseen (OS) expression is used far from the droplet ($r^* > 5$), the Proudman-Pearson (PP) expression near the droplet ($r^* < 2$). A smooth transition is applied between both expressions ($2 \le r^* \le 5$) such as the weight is 0 (resp. 1) at $r^* = 5$ for the OS expression (resp. PP) and 1 (resp. 0) at $r^* = 2$ (r^* , the AP-droplet distance normalised by the droplet radius A). Indeed, the OS expression corrects the Stokes paradox far from the droplet. Thus, the PP expression is used near the droplet to solve this problem which is an asymptotic expansion between the Stokes flow and OS expression. The analytical expressions can be found in Tinsley et al. (2006) where the terminal velocity of the droplet $U_{\infty,A}$ and its Reynolds number Re are both computed from the Beard model (Beard, 1976) - see Appendix A for more details.

3.2.2. $A > 30 \,\mu m$ - numerical solver

Beyond a droplet radius $A > 30\mu m$ (Re > 0.41), a numerical solver (ANSYS CFX) is used in order to get more accurate airflow modelling. Two examples are illustrated in Fig. 2 for droplet radii 37.5 μ m and 100 μ m. The computational field of the simulation has been provided as [-15,15] and [0,20] on the Z and X axis respectively and the square cell size was 2×10^{-2} (normalised by the droplet radius). It is assumed the airflow is homogeneous beyond the computational field. Then, if an AP trajectory leaves the computational field in the X axis, the airflow velocity is set equal to the airflow velocity of the boundary at the same Z.

3.3. Analytical Lagrangian integration scheme used in the AP tracking

Since the major part of the AP radius range considered in the paper ([4 nm; 1.3 µm]) is smaller or comparable to the mean free path of air molecules (104 nm in an air temperature and pressure of 256.15 K and 540 hPa modelling the mid-troposphere) - the Brownian motion has to be considered. In the current paper, the Brownian motion modelling was performed following the Lagrangian approach of Langevin (1908) where the vector force equations of a colloidal AP around a droplet are given by Minier and Peirano (2001) and used in several recent papers (Cherrier et al., 2017; Henry et al., 2014; Mohaupt, 2011; Mohaupt, Minier, & Tanière, 2011) summarised by:

$$\begin{cases} d\mathbf{X}_{AP}(t) = \mathbf{U}_{AP}(t)dt \\ d\mathbf{U}_{AP}(t) = \frac{\mathbf{U}_{f@AP}(t) - \mathbf{U}_{AP}(t)}{\tau_{AP}}dt + B_{\nu}d\mathbf{W}_{t}, \end{cases}$$
(3)



Fig. 2. ANSYS CFX simulation - Airflow evaluating around a droplet of radius (**a**, left) 37.5 μ m ($U_{\infty,A} = 17.4 \text{ cm s}^{-1}$, Re = 0.59) and (**a**, right) 100 μ m ($U_{\infty,A} = 82.4 \text{ cm s}^{-1}$, Re = 7.43). The colors represents the airflow velocity amplitude while the arrows are the velocity vectors. (For interpretation of the references to color in this figure legend, the reader is referred to the Web version of this article.)

with \mathbf{X}_{AP} the AP location vector, $\mathbf{U}_{f@AP}$ the fluid velocity at the AP location, \mathbf{U}_{AP} the AP velocity vector, *t* the time, B_{ν} is the diffusion coefficient accounting for Brownian motion and τ_{AP} the AP relaxation time. $d\mathbf{W}_t$ is the Wiener process increment which is a stochastic process modelling the random walk due to the Brownian motion of the APs.

These equations cannot be solved "classically" due to the Wiener process increment which is a stochastic process. In fact, trajectories are not bounded by a finite interval of time, pulling the stochastic integral out of the Riemann-Stieltjes rules. Hence, the stochastic integral calculation rules expressed by Itô et al., (1965) are applied in Equation (3). The particle motion is finally obtained using the analytical Lagrangian integration scheme proposed by Minier and Peirano (2001) which is applicable regardless of the time step Δt (Equation (4)):

$$\begin{aligned} \mathbf{X}_{AP}(t+\Delta t) &= \mathbf{X}_{AP}(t) + \mathbf{U}_{AP}(t)\tau_{AP}\left(1-e^{-\frac{\Delta t}{\tau_{AP}}}\right) + \mathbf{U}_{f@AP}(t)\left[\Delta t - \tau_{AP}\left(1-e^{-\frac{\Delta t}{\tau_{AP}}}\right)\right] \\ &+ B_{\nu}\tau_{AP}\sqrt{\Delta t - 2\tau_{AP}\frac{\left(1-e^{-\frac{\Delta t}{\tau_{AP}}}\right)}{\left(1+e^{-\frac{\Delta t}{\tau_{AP}}}\right)}}\boldsymbol{\xi}_{\chi} + B_{\nu}\tau_{AP}^{2}\frac{\left(1-e^{-\frac{\Delta t}{\tau_{AP}}}\right)^{2}}{\sqrt{2\tau_{AP}\left(1-e^{-\frac{2\Delta t}{\tau_{AP}}}\right)}}\boldsymbol{\xi}_{\psi} , \\ \mathbf{U}_{AP}(t+\Delta t) &= \mathbf{U}_{AP}(t)e^{-\frac{\Delta t}{\tau_{AP}}} + \mathbf{U}_{f@AP}(t)\left(1-e^{-\frac{\Delta t}{\tau_{AP}}}\right) + B_{\nu}\sqrt{\frac{\tau_{AP}}{2}\left(1-e^{-\frac{2\Delta t}{\tau_{AP}}}\right)}}\boldsymbol{\xi}_{\psi} \end{aligned}$$

$$(4)$$

where ξ_{ψ} and ξ_{χ} represent independent vectors of random variables sampled in a standard normal distribution $\mathcal{N}(0,1)$, generated by the Box-Muller method (Box & Muller, 1958).

This analytical Lagrangian integration scheme has been used in the recent paper of Cherrier et al. (2017) giving similar results compared to the Wang et al. (1978) reference paper. The approach only considers the drag force and the Brownian motion, defined by the first and second terms respectively in the velocity variation in Equation (3). In the present paper, the buoyancy force \mathbf{F}_{buoy} (see Appendix A) and the electrophoresis force \mathbf{F}_{elec} are added. In order to use the analytical Lagrangian integration scheme proposed by Minier and Peirano (2001) in Equation (4), a substitution is then applied and summarised in Equation (5):

$$\begin{cases} d\mathbf{X}_{AP}(t) = \mathbf{U}_{AP}(t)dt \\ d\mathbf{U}_{AP}(t) = \frac{\mathbf{U}_{f@AP}^{s}(t) - \mathbf{U}_{AP}(t)}{\tau_{AP}}dt + B_{\nu}d\mathbf{W}_{t}' \end{cases}$$
(5)

where $\mathbf{U}_{f@AP}^*$ is the resulting velocity at the AP location due to the added forces (Equation (6)):

$$\mathbf{U}_{f@AP}^{*}(t) = \mathbf{U}_{f@AP}(t) + \frac{\tau_{AP}}{m_{AP}}(\mathbf{F}_{buoy} + \mathbf{F}_{elec})$$
(6)

The analytical expression for the electrostatic forces is deduced from the image charge theory developed by Jackson (1975) given by Equation (7):

$$\mathbf{F}_{elec} = \frac{q^2}{4\pi\epsilon_0 A^2} \left[\left(-\frac{r^*}{(r^*2-1)^2} + \frac{1}{r^*3} \right) + \left(\frac{1}{r^*2}, \frac{Q}{q} \right) \right], \tag{7}$$

where $r^* = r/A$ is the normalised AP-droplet distance, *A* the droplet radius, ε_0 is the permittivity of free space, *q* and *Q* respectively the AP and droplet charge. In Equation (7), the first term dominates at short-range and is always attractive (due to the image charge of *q* inside the droplet with opposite sign). The second term, which is a Coulomb inverse square force, is repulsive or attractive depending on whether *q* and *Q* have unlike or like signs, prevails at long range with a weak amplitude compared to the image charge term. Further details can be found in Tinsley, Rohrbaugh, Hei, and Beard (2000).

Each particle trajectory is then calculated by iteratively updating its position with the analytical Lagrangian integration scheme (Equation (4)) where $\mathbf{U}_{f@AP}$ is substituted by $\mathbf{U}_{f@AP}^*$. It is assumed that there is no interaction between the APs during the computation. Also, the droplet is considered unaffected by the electrostatic forces induced by the AP charge. As mentioned in Grover and Beard (1975), since the AP and the droplet acceleration are equal to the electric force divided by the respective masses, the ratio of the droplet acceleration over the AP acceleration is $m_{AP}/M_A \leq 10^{-3}$ (where M_A is the droplet mass) in the droplet and AP range considered in this paper. Thus, the droplet acceleration is more than a thousand times lower than the AP acceleration which means the droplet motion is essentially unaffected during the AP travel around the droplet.

3.4. Boundary conditions

3.4.1. Injection disc

Initially, each AP is assigned an initial position according to a uniform statistical distribution. The initial velocity of each AP is set to the airflow velocity at the AP location. Far from the droplet, it is equal to (Equation (8)):

$$U_{AP}(0) = U_{f@AP}(0) = \begin{bmatrix} 0\\0\\U_{\infty,A} \end{bmatrix}$$
(8)

The injection disc radius (R_{Dkim}) is sized to account for every microphysical effect leading to the AP collection where the radius is

optimised by following Equation (9):

$$R_{Dkinj} = A + a + x_{bro} + Ax_{max}$$
⁽⁹⁾

In this sum, A + a is the radius of a cylinder of air which contains all AP susceptible to be collected by the droplet during its fall (impaction and interception processes). x_{bro} extends this cylinder to account for the maximum AP displacement possible due to the Brownian motion. The Fokker-Planck equation is used to evaluate x_{bro} (Equation (10)):

$$P(x|x_0, t_1) = \frac{1}{\sqrt{4\pi D_b t_1}} \exp\left(-\frac{(x_1 - x_0)^2}{4D_b t_1}\right),\tag{10}$$

where D_b is the Einstein-Stokes coefficient, x_0 the initial AP location and t_1 the AP time spent between x_0 and x. $P(x|x_0, t_1)$ is the likelihood of being at the AP location x given the initial x_0 location after t_1 . To evaluate x_{bro} , t_1 is set to the distance of the injection disc from the droplet over the droplet terminal velocity ($t_1 = 8A/U_{\infty,A}$). Moreover, x_{bro} is computed for every AP radius by considering a likelihood of 99.9%, setting x_0 to zero. This means, 99.9% of the AP assigned in the injection disc will statistically have a displacement due to the Brownian motion below x_{bro} .

To account for the electrostatic forces, a 2D Lagrangian tracking is used in order to get the initial maximum distance x_{max} from the axis Z (normalised by the droplet radius) which lead to the AP collection. The AP is injected upstream from the droplet at a distance of 8A where it is assumed the airflow is not affected by the droplet. The drag force and the electric effects are only considered in this calculation (no weight, no inertia and no Brownian motion). The integration scheme is the same as the one described in Tinsley et al. (2001). However, the airflow is still computed according to section 3.2.

3.4.2. AP number in the injection disc

The APs are injected following a uniform statistical distribution. One thousand APs are initially injected in the disc intercepted by the droplet ($Dk_{inj,A+a}$). Then, the whole injection disc $R_{Dk_{inj}}$ is randomly filled with the same density than $Dk_{inj,A+a}$. A first realisation (initialisation of the injection disc and computation of the AP trajectories) is provided in order to get a first evaluation of the number of APs collected by the droplet $N_{AP,col}$. If $N_{AP,col} < 1000$ APs collected, the initialisation of the injection disc is restarted and extra AP are injected until 1000 AP collections to ensure a reliable number of significant figures and to converge quickly following the Monte Carlo method (see section 3.4.5).

3.4.3. AP capture conditions

It is assumed that the APs stick to the droplet once they collide with it. The retention efficiency is set to unity. Thus, an AP collection occurs as soon as an AP touches the droplet surface and its tracking is over. In addition, if an AP leaves the computational domain without collision with the droplet, the collection is missed and the modelling of its movement finishes.

The first type of AP collection happens at the end of a time step when the AP distance from the droplet is lower than the sum of the AP and droplet radius. The first condition is given by Equation (11). Whereas this condition includes all types of scavenging effects (Brownian, phoretic and dynamic), a second condition refers to only the Brownian capture occurring during large time steps. This second condition is based on the bridge theory (Henry et al., 2014) summarised by Equation (12). Moreover, when the AP distance from the droplet is very low, the AP pass sometimes through the droplet during a time step due to the electrostatic force tends to infinity when r^* tending to unity (Equation (7)). Instead of decreasing the time step to face this strong force close to the droplet (increasing the calculation time), a third AP collection is considered in the model. As a result, if the APs cross the droplet during a time step, it is considered as collected.

$$d_{AP,d}^{2} = \sum_{i=1}^{3} (X_{AP,i} - X_{d,i})^{2} \le (A + a)^{2}$$
(11)

where $X_{AP,i}$ (resp. $X_{d,i}$) is the position of the AP (resp. the droplet centre) on the axis *i*, *n* the dimension of the computational domain and $d_{AP,d}$ is the droplet-AP distance.

$$\begin{cases} \frac{\exp^{2(A+a)} \frac{(d_{AP,d}(t) + d_{AP,d}(t \Delta t) - A - a)}{B_{r}^{2} \tau_{AP}^{2} \Delta t} - 1}{\frac{2d_{AP,d}(t) d_{AP,d}(t + \Delta t)}{e^{2} r_{AP}^{2} \Delta t} - 1} \geq \lambda \\ \frac{d_{AP,d}(t) = \sqrt{\sum_{i=1}^{3} (X_{AP,i}(t) - X_{d,i}(t))^{2}}}{d_{AP,d}(t + \Delta t) = \sqrt{\sum_{i=1}^{3} (X_{AP,i}(t + \Delta t) - X_{d,i}(t + \Delta t))^{2}}}, \end{cases}$$
(12)

where λ is a random variable sampled in a uniform distribution.

3.4.4. Time step

The analytical integration scheme (Equation (4)) of Minier and Peirano (2001) can handle the both borderline cases of the ballistic ($\Delta t \ll \tau_{AP}$, AP motion mostly governed by the dynamical effects) and diffusion ($\Delta t \gg \tau_{AP}$, AP motion mostly governed by the Brownian motion) regimes. Then, Δt varies from $10^3 \times \tau_{AP}$ to $10^{-1} \times \tau_{AP}$ when *a* varying from 4 nm to 1.3 μ m with a factor 1, 1/2, 1/3, 1/5, 1/7 and 1/10 when the droplet radius is respectively 15, 25, 37.5, 50, 75 and 100 μ m.

3.4.5. AP collection efficiency determination

The collection efficiency is defined as the ratio of the number of AP collected $N_{AP,col}$ by the droplet over the number of AP initially included in $Dk_{inj,A+a}$ assigned as $N_{AP,Dk_{inj,A+a}}$ (Fig. 1). This parameter depends on the droplet radius *A*, the AP radius *a*, the relative humidity *RH* due to the thermo- and diffusiophoresis forces, the AP and droplet charge (*q* and *Q*) caused by electrostatic force (Equation (13)):

$$E_{c,i}(a, A, q, Q, RH) = \frac{N_{AP,col}(a, A, q, Q, RH)_i}{N_{AP,Dk_{inj,A+a}}(a, A, q, Q, RH)_i}$$
(13)

Thus, the collection efficiency is determined by initialisation of the injection disc (see section 3.4.1). Every AP trajectories are computed related to the analytical Lagrangian scheme described in Equation (4) and the $N_{AP,col}$ is updated online following the three AP capture conditions described in section 3.4.3. The AP collection by the droplet is a stochastic process through the Brownian motion integrated into the AP vector forces (Equation (5)). The capture efficiency E_c is then computed using a Monte Carlo method according to Cherrier et al. (2017). Indeed, E_c is obtained by averaging a set of *n* successive realisations (Equation (14)) where a realisation involves the initialisation of the APs in the injection disc, the computation of all trajectories until the APs are collected or missed by the droplet (i.e. the APs leave the computational domain downstream of the droplet). In the present model, 50 realisations are computed in order to get a reliable value of the collection efficiency (see section 3.5).

$$E_{c}(a, A, q, Q, RH) = \frac{1}{n} \sum_{i=1}^{n} E_{c,i}(a, A, q, Q, RH),$$
(14)

where $E_{c,i}$ is the collection efficiency computed at the *i*-th realisations.

3.5. Validation and convergence

As Cherrier et al. (2017), the Browian motion modelling has been verified. The root mean square displacement of the particle is compared to the theoretical expression $\sqrt{\langle x^2(t) \rangle}$ of Einstein (1956) given in Equation (15).

$$\sqrt{\langle x^2(t)\rangle} = \sqrt{2D_{im}D_bt},\tag{15}$$

where D_{im} is the dimension of the computational domain and t the computational time.

The flow velocity at the AP location disturbed by the added forces $U_{f@AP}^*$ is set to zero in the analytical integration scheme (Equation (4)). The initial AP velocity is zero and the AP location is the origin of the Cartesian coordinate system. The number of time step for each AP is computed to have an integration time of 10 ms. To compare the Brownian motion in the simulation to theory, the root mean square displacement is calculated from 4000 AP trajectories for each AP radius. It results a discrepancy less than 1% is observed between the model and the theory for the whole AP radius range.

Furthermore, we have verified the airflow velocity convergence. The meshes are generated through ANSYS CFX where the grid used for the discretisation is unstructured and composed of quadrilateral cells whose mesh density increases near the drop surface. Then, the meshes are post-processed in order to get a uniform grid from the raw data. A cell size is set to ensure that the results are independent of the resolution. Indeed, it was verified that the collection efficiency did not vary if the grid is refined. It was found that a cell size of 2×10^{-2} (normalised by the droplet radius *A*) is suitable. During a realisation, the exact values are computed through interpolations.

The injection disc radius ($R_{Dk_{inj}}$) convergence has been verified in a third validation test in order to ensure the collection efficiency is unaffected by the increasing of the $R_{Dk_{inj}}$.

Fourth, the statistical convergence of the collection efficiency E_c has been ensured. In the current model, the number of AP injected is set to have at least 1000 APs collected by the droplet during every realisation. A Shapiro-Wilk test (Shapiro & Wilk, 1965) with a significance level of 95% is computed to verify that the obtained efficiencies are normally distributed. After which, the confidence interval on E_c is estimated through a Student-t distribution test with a level of 95%. For at least 1000 APs collected, it was found that 50 realisations allow computing E_c with a confidence interval of 2% for a 4 nm AP radius (sensitive to Brownian motion) whereas a 1.3 μ m AP radius (non-sensitive to Brownian motion) gives a confidence interval smaller than 0.01%.

Finally, the present Lagrangian model has been tested under mid-tropospheric conditions ($T_{air} = 256.15 K$, $P_{air} = 540$ hPa, RH = 100%) with an AP density of 500 kg m⁻³ presented in Fig. 3a. Thus, the current model has been compared to the Tinsley and Zhou (2015) model (Fig. 3b). The results are very close to the Tinsley and Zhou (2015) values, which confirms the performances of the model. Note that it is not a direct comparison since Tinsley and Zhou (2015) consider the collision rate coefficient R_c (also called collection kernel) instead of the collection efficiency E_c here. In order to compare both data model, the Tinsley and Zhou (2015) data have been formulated in E_c since both quantities are directly correlated (see Appendix A).

It is important to emphasize that the variations are really different considering E_c instead of R_c . Indeed, while the E_c in general decreases with increasing droplet radius (Fig. 4), R_c increases since the terminal velocity of the droplet and the cross sectional area both increase rapidly (their product increases approximately as the fourth power of droplet radius up to about 50 µm radius).

4. Results of simulation and discussion

All numerical results are given as table in supplementary material. Simulations have been performed to evaluate the collection efficiency for 13 AP radii $0.004 \le a \le 1.3 \,\mu\text{m}$ and 6 droplet radii A = 15, 25, 37.5, 50, 75 and $100 \,\mu\text{m}$ - following the conditions



Fig. 3. (a, left) Collection efficiency for the whole AP radius range and few cases of AP and droplet charges under the mid-tropospheric conditions $(T_{air} = 256.15 K, P_{air} = 540 hPa, RH = 100\%)$ and an AP density of 500 kg m⁻³. The red, purple and blue curves represent an AP charge of 5, 20 and 50 e respectively. The droplet charges are directly mentioned on the curves (in e). Dotted lines are the extrapolation when an EC value is below 10^{-5} . The points are the simulation results meanwhile the dashed lines are the collection efficiency EC_{Wang} coming from the well-known diffusion kernel of Wang et al. (1978). (b, right) Indirect comparison between the current model (solid line) and the Tinsley and Zhou (2015) model (dotted line).

summarised in Table 2. The AP charge q is set to 0, 5, 20, 50 and 600 e, in order to model the AP charge which can appear in clouds for a non-radioactive and radioactive AP case (section 2.2). The droplet charge is set - from the electrically neutral case to the electric charge Q according to Takahashi (1973) for both stratiform and convective cloud case - depending on the droplet radius referred to Table 1. A relative humidity of 100% is considered to ensure no diffusiophoresis and thermophoresis effects on the collection efficiency. The simulations have been made for mid-tropospheric conditions (- 17°C, 540 hPa) and an average AP density of 1500 kg. m^{-3} . It should be noticed that the collection efficiencies below 10^{-5} have been determined but not been statistically converged to reduce the computation time. Results below 10^{-5} are then not presented here.

4.1. Case without electrostatic forces (q = Q = 0 e)

Fig. 4 shows the collection efficiency (EC) related to the AP radius for the whole droplet size range considered in the study. The points represent the numerical results of the current model and the dashed lines refer to the collection efficiency EC_{Wang} related to the diffusion kernel K_{Wang} of Wang et al. (1978) where $EC_{Wang} \approx K_{Wang}/(\pi \cdot U_{\infty,A} \cdot (A + a)^2)$ (expressions can be found in Appendix A).

- The following results can be noticed:
- No matter the droplet size, for an AP radius smaller than 40 nm, a decrease of the EC is observed when the AP radius increases. More precisely, it can be noticed that our simulations perfectly fit EC_{Wang} which means that the EC is purely driven by the Brownian motion for these AP sizes. This is the reason why, for a given AP size, the EC decreases for larger droplet radii. Also, for an increasing droplet radius, the travel time of the AP around the droplet decreases with a higher airflow velocity. Thus, the AP collection due to the Brownian motion has less time to operate (since $\langle x^2(t) \rangle$ is proportionate to \sqrt{t} in Equation (15)). It is worthwhile to note that the collision rate efficiency has the opposite variation here - increasing for smaller droplet radii (Zhang, Tinsley, & Zhou, 2018). This is due to the ventilation f_p in the diffusion kernel K_{Wang} (Appendix A) of Wang et al. (1978) which increases with the shorter interaction times. In fact, there is less depletion of the AP concentration by the immediately preceding scavenging in the air that the droplet is falling through.
- For small droplets ($A \leq 37.5 \, \mu m$)
- For 40 nm $\leq a \leq 0.5 \,\mu m$, the collection efficiency keeps decreasing for larger particles but there is a difference between the



Fig. 4. Results of the simulations for the whole droplet radius range under the mid-tropospheric conditions ($T_{air} = 256.15 K$, $P_{air} = 540$ hPa, RH = 100%) without electric charges on the droplet and AP (q = Q = 0e). The solid lines are the fittings of the simulation results and the dashed lines are EC_{Warg} - the collection efficiency related to the diffusion kernel of Wang et al. (1978).

Table 2			
Conditions	of si	mulatio	n.

Parameter	Numerical value		
Air density - ρ_{air}	$0.73 \text{kg} \text{m}^{-3}$		
Air pressure - Pair	540 hPa		
Air temperature - Tair	256.15 K		
Air viscosity - η_{air}	$1.63 \times 10^{-5} \text{ kg m}^{-1} \text{ s}^{-1}$		
AP density - ρ_{AP}	1500 kg m^{-3}		
AP radius - a	∈[4 nm; 1.3 μm]		
Droplet radius - A	15/25/37.5/50/75/100 µm		
Mean free path of air molecules - λ_{air}	104 nm		
Relative humidity - RH	100%		
Reynolds number - Re	0.04/0.18/0.59/1.30/3.70/7.43		
Terminal velocity of the droplet - $U_{\infty,A}$	$3.01/8.16/17.4/28.8/54.8/82.4 \mathrm{~cm~s^{-1}}$		

current model - which gives higher values - and the model EC_{Wang} of Wang et al. (1978). Indeed, the larger the AP radius is, the more significant the discrepancy is. In this AP size range, the collision between the AP and the droplet is still dominated by the Brownian motion, nevertheless, inertia mechanisms cannot be neglected any more. On the one hand, the effect of the Brownian motion declines and the mean AP displacement relatively to the streamlines decreases, and on the other hand, the intercept effect increases - which intensifies for large AP and small droplets. It should be noted that the AP inertia also plays a small but increasing role in the AP radius range for wider AP and droplet radii. So, for $A \leq 37.5 \,\mu m$ and $40 \,\text{nm} \leq a \leq 0.5 \,\mu m$, the efficiency is still dominated by the Brownian motion but the relative contributions of the interception and the inertia increases.

- To explain the large decrease of the collection efficiency for $0.5 \mu m < a \le 1.3 \mu m$ and $A \le 37.5\mu m$, a simple case without diffusion is considered. The trajectory of an AP injected on the droplet axis - the coordinate system is centred on the falling droplet - is computed and the AP goes up and slows down near the droplet because of the airflow velocity which falls to zero at the droplet interface. For those droplet radii, there is a stagnation region (Zhang & Tinsley, 2018) beyond the collection limit - sum of a + A - where the AP falls faster than the upward airflow. Then, since there is not enough inertia and the diffusion and phoretic forces are neglected, the AP comes to rest relatively to the droplet and will never be collected. Also, if the AP is injected

nearby the ascending axis, the AP approaches the droplet until it reaches this stagnation region. At this point, the AP does not move following the ascending axis but horizontally moves to the side due to the horizontal component of the airflow velocity. These both cases are illustrated in Fig. 1 of Zhang and Tinsley (2018). Therefore, the collection efficiency drops while the AP weight increases with its radius. This effect is strongly dependent on the AP density (Zhang & Tinsley, 2018).

- * Accordingly, for $A = 15 \,\mu m$, the collection efficiency does not collapse to zero thanks to the Brownian motion which allows either for the AP to be collected in the stagnation region or to come closer to the collection limit for AP initially from the side. For $A = 25 \,\mu m$, the reduction of the collection efficiency is greater than for $A = 15 \,\mu m$ since it is less likely for the AP to come closer to the collection cross section through the effect of the Brownian motion. It should be noticed that, in both cases, the AP inertia can also improve the AP collection in the stagnation region but this mechanism has second-order importance compared to the Brownian motion.
- * In the case of $A = 37.5 \,\mu m$, the collection efficiency still decreases but not as much as for $A = 25 \,\mu m$ for two reasons. First, the AP inertia is not a second-order process any more in the AP collection. Also, the stagnation region beyond the distance of collection is reduced because the airflow velocity is faster for larger droplets and the normalised collection limit is smaller.
- There is a minimum collection efficiency computed by the model which can be seen for $A = 75 \ \mu m$ and $A = 100 \ \mu m$, but occurs at $a > 1.3 \ \mu m$ for the smaller droplets (not shown). It can be observed that, for an increase of the droplet radius, this minimum of what is called "Greenfield gap" (Greenfield, 1957) moves to smaller APs. Also, the collection efficiency starts to become higher than EC_{Wang} for a smaller AP when a larger droplet is considered. These variations come from the AP inertia which becomes more and more important when the mass is increasing as the cube of the AP radius. Indeed, the inertia becomes so strong that the AP continues upward relative to the droplet and impacts it.

4.2. Case with varying droplet and AP charges

Simulation results are presented in Figs. 5–10, corresponding respectively to droplet radii from 15 to 100 μ m. The collection efficiencies related to the diffusion kernel of Wang et al. (1978) are also referred to as a dashed line for every droplet radius (*EC*_{Wang}). In all the figures, the points indicate the simulation results, the red, purple, blue and yellow curves represent an AP charge of 5, 20, 50 and 600 *e*, respectively. The droplet charges are directly mentioned on the curves in number of elementary charge (*e*) (see Fig. 7).



Fig. 5. Results of the 15 µm droplet radius under the mid-tropospheric conditions ($T_{air} = 256.15 K$, $P_{air} = 540$ hPa, RH = 100%). The points are the simulation results meanwhile the dashed lines are the collection efficiency EC_{Wang} related to the diffusion kernel of Wang et al. (1978). The red, purple, blue and yellow curves represent an AP charge of 5, 20, 50 and 600 *e* respectively. The droplet charges are directly mentioned on the curves (in *e*). Dotted lines are the extrapolation when an EC value is below 10^{-5} . (For interpretation of the references to color in this figure legend, the reader is referred to the Web version of this article.)



Fig. 6. Results of the 25 µm droplet radius under the mid-tropospheric conditions ($T_{air} = 256.15 \text{ K}$, $P_{air} = 540$ hPa, RH = 100%). The points are the simulation results meanwhile the dashed lines are the collection efficiency EC_{Wang} related to the diffusion kernel of Wang et al. (1978). The red, purple, blue and yellow curves represent an AP charge of 5, 20, 50 and 600 *e* respectively. The droplet charges are directly mentioned on the curves (in *e*). Dotted lines are the extrapolation when an EC value is below 10^{-5} . (For interpretation of the references to color in this figure legend, the reader is referred to the Web version of this article.)

First, the trends without electrostatic forces observed in the previous section, are still visible for large AP even though strong AP and droplet charges are key in reducing their effects. The contributions of both terms in the electrostatic forces' expression (Equation (7)) can be observed in the simulation.

4.2.1. Domination of the short-range attractive term

For zero droplet charge, the contribution of the Coulomb inverse square term in Equation (7) is zero (curves labelled 0 in Figs. 5–10). In this case, it can be observed that the EC increases with the AP charge q, this agrees with results from Tinsley et al. (2000) and Jaworek et al. (2002). This is due to the short-range attractive force between the AP charge and its image inside the droplet which is proportional to q^2 . Also, for zero droplet charge and a given AP charge q and droplet radius A, the factor by which the collection efficiency increases compared to the curve without electrostatic forces (Q = q = 0 e) is reduced when the AP radius a is decreased. The relative magnitude of the contribution of the short-range attractive term declines for small AP radius since the Brownian motion becomes the major part of the AP collection, even if the absolute effect of the electrostatic term increases since the electric mobility of the AP is higher. Also, the short-range attractive term dominates near the Greenfield gap - in which the effect of the Brownian motion becomes weak and the dynamical effects (inertia and interception) are not yet large enough - and the domination extends towards the small AP radius when the AP charge is increased.

Note that this is valid for the droplet charge Q near zero. On the contrary, the contribution of the short-range image charge attractive term is second-order compared to the Coulomb inverse square term for strongly electrified droplets.

4.2.2. Domination of the coulomb inverse square term

For the strongly electrified droplet computed in the present paper, the effect of the droplet charge Q exists for the whole AP size range considered in this paper. Indeed, for large product $q \times Q$, the Coulomb inverse square force dominates at large distance over the dynamical effect, even though the electric mobility of the AP is small. Thus, for large AP, the collection efficiency is increased or decreased depending on whether the Q and q have unlike or like signs and also the product $q \times Q$. For a small AP charge (q = 5 e) typical of the atmospheric AP with a droplet charge naturally found in a convective cloud (Q = 10000 e for $A = 15 \mu m$ or Q = 30000 e for $A = 25 \mu m$), simulations have shown that the Coulomb inverse square term is so repulsive that the whole collection efficiencies in the AP size range studied are bellow 10^{-5} .



Fig. 7. Results of the 37.5 µm droplet radius under the mid-tropospheric conditions ($T_{air} = 256.15 K$, $P_{air} = 540$ hPa, RH = 100%). The points are the simulation results meanwhile the dashed lines are the collection efficiency EC_{Wang} related to the diffusion kernel of Wang et al. (1978). The red, purple, blue and yellow curves represent an AP charge of 5, 20, 50 and 600 *e* respectively. The droplet charges are directly mentioned on the curves (in *e*). Dotted lines are the extrapolation when an EC value is below 10^{-5} . (For interpretation of the references to color in this figure legend, the reader is referred to the Web version of this article.)

For the weakly electrified droplet ($Q \approx \pm 10^2 e$ for $A = 15 \,\mu m$, $Q \approx \pm 10^3 e$ for $A = 100 \,\mu m$), the contribution of the Coulomb inverse square force increases for decreasing AP radius *a*. It can be observed through the effect of the droplet charge *Q* which is minor for AP larger than about 0.3 μ m and become more and more important for tiny AP radius *a* no matter the droplet charge polarity - in line with the simulation of Tinsley and Zhou (2015). This is mainly due to the AP electric mobility which is proportional to the inverse AP radius *a*.

The domination of the Coulomb inverse square term can also be illustrated with:

- The decrease of the EC when the Coulomb inverse square force is repulsive appears for small AP.
- The curves with the products of the AP and droplet charges $q \times Q$ equal and negative tends to the same value of EC for small AP. For example, in Fig. 8 the curve for q = 5 e and Q = -10000 e coincides with the curve for q = 50 e and Q = -1000 e as the AP radius *a* is reduced. This is due to the Coulomb inverse square force which dominates at large distance for small AP and which is proportional to $q \times Q$ far away from the droplet.

4.2.3. The transition region between both dominations

For same sign AP and droplet charges, the transition from the domination of the Coulomb inverse square force to the one of the short-range attractive force is evident in the simulation results. The larger the droplet and AP charges are, the more the transition appears for large AP radius *a*. For example, for $A = 15 \mu m$ (Fig. 5), for q = 600 e and Q = 100 e, the EC is led by the short-range attractive force for AP larger than 30 *nm* since the values are bigger than the case without electrostatic effects (q = 0 e and Q = 0 e). For a < 30 nm, the EC collapses and tends to zero when the AP radius decreases. Indeed, the Coulomb inverse square force opposes to the dynamical effects and prevents the AP from getting closer to the droplet and from involving the contribution of the short-range attractive force in the AP collection. The EC keeps decreasing for small AP because the repulsive force keeps getting stronger through an increasing AP electric mobility.

4.2.4. Impact of the droplet radius on the electrophoresis

The EC is less influenced by the electrostatic effects for a given AP radius *a* and an increasing droplet radius *A*. It can be observed for both terms in Equation (7):



Fig. 8. Results of the 50 µm droplet radius under the mid-tropospheric conditions ($T_{air} = 256.15 \text{ K}$, $P_{air} = 540$ hPa, RH = 100%). The points are the simulation results meanwhile the dashed lines are the collection efficiency EC_{Wang} related to the diffusion kernel of Wang et al. (1978). The red, purple, blue and yellow curves represent an AP charge of 5, 20, 50 and 600 *e* respectively. The droplet charges are directly mentioned on the curves (in *e*). Dotted lines are the extrapolation when an EC value is below 10^{-5} . (For interpretation of the references to color in this figure legend, the reader is referred to the Web version of this article.)

- For example when $a = 1.3 \ \mu m$ and Q = 0e, the EC is enhanced by more than two orders of magnitude when the AP charge *q* varies from 0 to 600 *e* considering a droplet size $A = 15 \ \mu m$ (Fig. 5), and by less than one order of magnitude for a droplet radius $A = 100 \ \mu m$ (Fig. 10).
- For a = 4 nm and q = 20 e, the effect of the droplet charge Q = -200 e and 200 e compared to the case Q = 0e respectively leads to a EC discrepancy from +595% and -99.9% for a droplet radius $A = 15 \mu m$ (Fig. 5), to +23% and -23% for a droplet radius $A = 75 \mu m$ (Fig. 9).

It can be explained through an increase of the airflow velocity which enhances the dynamical effects. Then, the AP inertia becomes important in reducing the contribution of the electrostatic forces but also any kind of phoretic forces as developed in the work of Wang et al. (1978). That is why in our study we consider strongly electrified clouds from the Takahashi (1973) measurement since the weak droplet charges Q used in Tinsley and Zhou (2015) have a minimal effect on the EC for large droplets. Indeed, for $A = 100 \,\mu m$, the highest difference (for the minimum AP radius $a = 4 \,nm$) between the case $Q = -300 \,e$ and $Q = 0 \,e$ is less than + 6% when the AP is weakly electrified ($q = 5 \,e$) and almost + 37% in the extreme case where the AP is radioactive ($q = 600 \,e$). Nevertheless, a weak AP charge characterising the atmospheric AP must be studied since its effects on the EC is strong - coupled with a droplet charges Q which can be found in clouds. For $A = 100 \,\mu m$, $a = 4 \,nm$ and $q = 5 \,e$, the EC increases by a factor of 176 if a droplet charge $Q = -400000 \,e$ rather than the neutral case ($Q = 0 \,e$) is considered.

5. Conclusion

Simulations were performed for a similar range of AP radius studied in Tinsley and Zhou (2015) through a novel theoretical model of collection efficiency computation which models the Brownian motion with the Langevin approach (1908). A wide range of AP and droplet charges have been considered as typical for the atmospheric AP but also for a radioactive AP released after a nuclear accident like Fukushima. The present paper extends the simulation of Tinsley and Zhou (2015) by computing a wide range of droplet radii from $15 \,\mu m$ to $100 \,\mu m$ and widens the droplet charge interval to strongly electrified clouds in order to study the electrostatic forces which can appear in stratiform and convective clouds through the Takahashi measurements (1973). It results a large contribution of the electrostatic forces in the collection efficiency (EC) for the wide range of droplet radii. Indeed, the EC is increased up to 4 orders



Fig. 9. Results of the 75 µm droplet radius under the mid-tropospheric conditions ($T_{air} = 256.15 \text{ K}$, $P_{air} = 540$ hPa, RH = 100%). The points are the simulation results meanwhile the dashed lines are the collection efficiency EC_{Wang} related to the diffusion kernel of Wang et al. (1978). The red, purple, blue and yellow curves represent an AP charge of 5, 20, 50 and 600 *e* respectively. The droplet charges are directly mentioned on the curves (in *e*). Dotted lines are the extrapolation when an EC value is below 10⁻⁵. (For interpretation of the references to color in this figure legend, the reader is referred to the Web version of this article.)

of magnitude with a droplet and an AP charge representative of convective clouds and radioactive AP, respectively. An EC enhancement has also been found for AP (q) and droplet (Q) charge of same signs for cases where the product $q \times Q$ is moderate, however the EC collapses below 10^{-5} for large products of charge.

Simulations must be applied with caution when an AP density other than that computed in the paper is considered. For large AP, the effect of the AP inertia enhances the EC for increasing AP density. Also, for small droplet radii ($A \le 37.5 \,\mu m$), the contribution of the AP weight is highly dependent on the AP density as shown by Zhang and Tinsley (2018) or Zhang et al. (2018, Fig. 6). Thus, most of the simulations have to be repeated when the AP density strongly differs from 1500 kg m⁻³. Nevertheless, for zero charge on the droplet ($Q = 0 \, e$), the effect of the AP density is not significant for small AP radius even though there is non-zero charge on the AP ($q \neq 0 \, e$). For example, the discrepancy of the EC when the AP density differs from 500 to 4500 kg m⁻³ is less than 4% and 2% for $q = 0 \, e$ and $q = 50 \, e$ respectively, for an AP radius smaller than 80 nm.

To apply the simulation results outside mid-tropospheric conditions (-17°C, 540 hPa), Fig. 8 from Tinsley and Leddon (2013) can be used to estimate the effect of altitude on the collection efficiency. Taking high-tropospheric conditions at altitude 12.5 km (-56°C, 180 hPa) or tropospheric conditions at the surface of the Earth (+15°C, 1013 hPa), the discrepancy is less than 40 and 20% respectively. Finally, to extend the present simulations for other droplets radii, droplet and AP charges, interpolation or moderate extrapolation can be made. The model is also suitable to investigate the impact of the thermophoresis and the diffusiophoresis on the collection efficiency - which have not been studied in the current paper - by getting the temperature and vapour density fields around the droplets and by adding the analytical expression of the forces in Equation (6).

These simulations can also be used for a wide range of applications like climate models, pollution models or cloud models with detailed microphysics like DESCAM (Flossmann, 1998). It is necessary to first obtain the charge distributions on the AP and the droplets. Also, for real situations, the collection efficiencies must be integrated over charge and size distributions of APs and droplets. It provides a simple base for modelling the changes in AP concentration, the ice-forming nuclei in clouds which in turn can impact precipitation or the Earth's energy budget. We plan to predict the radionuclide transfer in the environment after an accidental discharge into the atmosphere and those results are essential for the investigation. An important issue remains the experimental validation of the current model which has not yet been performed.



Fig. 10. Results of the 100 µm droplet radius under the mid-tropospheric conditions ($T_{air} = 256.15 K$, $P_{air} = 540$ hPa, RH = 100%). The points are the simulation results meanwhile the dashed lines are the collection efficiency EC_{Wang} related to the diffusion kernel of Wang et al. (1978). The red, purple, blue and yellow curves represent an AP charge of 5, 20, 50 and 600 *e* respectively. The droplet charges are directly mentioned on the curves (in *e*). Dotted lines are the extrapolation when an EC value is below 10^{-5} . (For interpretation of the references to color in this figure legend, the reader is referred to the Web version of this article.)

Appendix A. Nomenclature

Parameter	Meaning	Expression or Value	Unit	Source
a AD	AP radius	-	m	-
Δ	Droplet radius	_	m	_
B _{AP}	Particle mobility	$\frac{C_u}{6\pi\eta_{air}a}$	Kg ⁻¹ .s	Tinsley <i>et al.</i> (2001)
B _{Beard}	Beard (1976) constant	$\begin{bmatrix} -0.318657 \times 10^{+1} \\ +0.992696 \times 10^{+0} \\ -0.153193 \times 10^{-2} \\ -0.987059 \times 10^{-3} \\ -0.578878 \times 10^{-3} \\ +0.855176 \times 10^{-4} \\ -0.327815 \times 10^{-5} \end{bmatrix}$	-	Beard (1976)
B_{ν}	Diffusion coefficient accounting for Brownian motion	$\sqrt{\frac{2k_b T_{air}}{m_{AP} \tau_{AP}}}$	m. $s^{-\frac{3}{2}}$	Minier and Peirano (2001)
c	Distance of the point charge q' from the droplet centre	$\frac{A^2}{r}$	m	Jackson (1975)
C _u	Stokes-Cunningham slip correction factor	$1 + \left(1.257 + 0.4e^{-\frac{1.10}{K_n}}\right)K_n$	-	Pruppacher et al., 1998), Sect. 11.2
$d_{AP,d}$	Droplet-AP distance	_	m	-
D_b	Einstein-Stokes coefficient	CukbTair 6π) _{air} a	$m^2.s^{-1}$	Pruppacher et al., (1998), Sect. 11.2
Dim	Computional domain dimension	3	-	-
Dk _{inj}	Injection disc of AP	-	-	-

$Dk_{inj,A+a}$	Cross-sectional area intercepted by the droplet in Dk_{inj}	$\pi (A+a)^2$	m^2	-
dWt	Increment of the Wiener process	_	<u>1</u>	Minier and Peirano
•	1		S2	(2001)
F	Collection efficiency	_	_	(2001)
E	Movieum hate particle energy for the Gassium 197 descu	-	- -	
Emax	Maximum beta particle energy for the Caesium-137 decay	5.12× 10 ⁵	ev	-
EC _{Wang}	Collection efficiency of Wang et al. (1978)	$\approx \frac{K_{Wang}}{2}$	-	Wang et al. (1978)
		$U_{\infty,A}(A+a)^2$		
f_A	Droplet size distribution	-	m ⁻³ .m ⁻¹	-
Ehum.	Buovancy force	_	N	Grover and Beard (1975)
T Duoy	Electronic force			Timelan et al. (2006)
F _{elec}	Electrophoresis force	-	IN	Tinsley et al. (2006)
f_p	Particle ventilation factor	$1 \pm 0.530 N \exp{\frac{-1.1}{N}}$	-	Tinsley and Zhou (2015)
£ (4)	Dandom function	r + olobolitelip it		
J(l)		-	-	-
g	Acceleration of gravity	9.81	m.s ⁻²	-
\mathbf{g}_{net}	Net acceleration of gravity	$\frac{\rho_{AP} - \rho_{air}}{g}$	m.s ⁻²	Grover and Beard (1975)
		PAP		
Ι	Number of ion pair production per decay	Emax	-	Clement and Harrison
		3wi		(1992)
k _b	Boltzmann constant	1.38×10^{-23}	m ² .kg.s ⁻	_
5		100/(10	² .K ⁻¹	
K.	Knudsen number	dair	_	Pruppacher et al (1998)
n n	Andusch humber	a		Sout 11.1
**			0 1	Sect. 11.1
K _{Wang}	Diffusion kernel of Wang et al. (1978)	$4\pi A f_p D_b$	$m^3.s^{-1}$	Wang et al. (1978)
M_A	Droplet mass	_	kg	_
m _{AD}	AP mass	4 3	kø	_
		$\frac{1}{3}\pi a^{3}\rho_{AP}$		
Ν	Cube root of the Péclet number	(2411) $)\frac{1}{2}$	-	Tinsley and Zhou (2015)
		$\left(\frac{2AU_{\infty,A}}{D}\right)^3$		
		$\begin{pmatrix} D_b \end{pmatrix}$		
n_	Concentration of the negative ions	-	m ⁻³	Clement and Harrison
				(1992)
n_{h-}	Background negative ion concentration	10 ⁹	m ⁻³	Clement and Harrison
5	0 0	10		(1992)
Nen	Number of AP collected by the droplet	_	_	
1 AP,col		-	_	_
$N_{AP,Dk_{inj,A+a}}$	Number of AP initially in $Dk_{inj,A+a}$	-	-	-
Pair	Air pressure	-	Pa	-
$P(\mathbf{r} \mathbf{r}_0, t_1)$	Likelihood of being at the AP location x given the initial x_0 location	_	_	_
1 (56,560), 11)	after t			
~			C	
<i>q</i>	AP charge		C	-
q'	Image of the AP charge q	$-\frac{A}{q}q$	С	Jackson (1975)
	Desidual abarra		C	Jackson (1075)
q	Residual charge	$Q = q^{r}$	C	Jackson (1975)
Q	Droplet charge	-	С	-
<i>q_{mean}</i>	Mean radioactive AP charge	-	С	-
r	AP distance from the droplet centre	_	m	_
R	Cartesian coordinate system	(X Y Z)	_	_
D D	Collision rate coofficient		m ³ c ⁻¹	
K _C	Comsion rate coefficient	$E_c \pi (A+a)^2 U_{\infty,A} - U_{\infty,a} $	111 .5	-
		$\approx E_{a}\pi(A + a)^{2}U_{a}$		
		10 E(n (1 + u) C(0,A	-	-
Roku	Radius of the injection disc	$A + a + x(t) + Ax_{max}$	– m	-
R _{Dkinj}	Radius of the injection disc	$A + a + x(t) + Ax_{max}$	– m	-
R _{Dkinj} Re	Radius of the injection disc Reynolds number	$A + a + x(t) + Ax_{max}$ $\left(1 + 2.51\frac{\lambda_{air}}{2}\right)\exp^{Y_{Beard}}$	- m -	- - Beard (1976)
R _{Dkinj} Re	Radius of the injection disc Reynolds number	$A + a + x(t) + Ax_{max}$ $\left(1 + 2.51\frac{\lambda_{air}}{2A}\right)\exp^{Y_{Beard}}$	 m 	– – Beard (1976)
R _{Dkinj} Re r [*]	Radius of the injection disc Reynolds number Normalised AP distance from	$A + a + x(t) + Ax_{max}$ $\left(1 + 2.51\frac{\lambda_{air}}{2A}\right)\exp^{YBeard}$ $\frac{r}{4}$	- m -	– – Beard (1976) –
R _{Dkinj} Re r [*]	Radius of the injection disc Reynolds number Normalised AP distance from the droplet centre	$A + a + x(t) + Ax_{max}$ $\left(1 + 2.51\frac{\lambda_{alr}}{2A}\right) \exp^{YBeard}$ $\frac{r}{A}$	- m -	- - Beard (1976) -
R _{Dkinj} Re r [*] RH	Radius of the injection disc Reynolds number Normalised AP distance from the droplet centre Relative humidity of air	$A + a + x(t) + Ax_{max}$ $\left(1 + 2.51\frac{\lambda_{air}}{2A}\right) \exp^{YBeard}$ $\frac{r}{A}$	- m - -	- Beard (1976) -
R _{Dkinj} Re r [*] RH t	Radius of the injection disc Reynolds number Normalised AP distance from the droplet centre Relative humidity of air Computational time	$A + a + x(t) + Ax_{max}$ $\left(1 + 2.51\frac{\lambda_{air}}{2A}\right) \exp^{Y_{Baard}}$ $\frac{r}{A}$	- m - - s	- Beard (1976) - -
R _{Dkinj} Re r [*] RH t	Radius of the injection disc Reynolds number Normalised AP distance from the droplet centre Relative humidity of air Computational time Time spent to the AP to go from	$A + a + x(t) + Ax_{max}$ $\left(1 + 2.51\frac{\lambda_{air}}{2A}\right) \exp^{YBeard}$ $\frac{r}{A}$	- m - - s s	- Beard (1976) - -
R _{Dkinj} Re r [*] RH t t ₁	Radius of the injection disc Reynolds number Normalised AP distance from the droplet centre Relative humidity of air Computational time Time spent to the AP to go from	$A + a + x(t) + Ax_{max}$ $\left(1 + 2.51\frac{\lambda_{alr}}{2A}\right) \exp^{Y_{Beard}}$ $\frac{r}{A}$ $-$ $-$ $\frac{8A}{U_{\infty A}}$	_ m _ _ s s	- Beard (1976) - - -
R _{Dkinj} Re r* RH t t ₁	Radius of the injection disc Reynolds number Normalised AP distance from the droplet centre Relative humidity of air Computational time Time spent to the AP to go from the injection disc to the droplet	$A + a + x(t) + Ax_{max}$ $\left(1 + 2.51\frac{\lambda_{atr}}{2A}\right) \exp^{YBeard}$ $\frac{r}{A}$ $-$ $\frac{8A}{U_{\infty,A}}$	- m - - s s s	- Beard (1976) - - -
R _{Dkinj} Re r [*] RH t t ₁	Radius of the injection disc Reynolds number Normalised AP distance from the droplet centre Relative humidity of air Computational time Time spent to the AP to go from the injection disc to the droplet Air temperature	$A = A + X(t) + Ax_{max}$ $\left(1 + 2.51\frac{\lambda_{air}}{2A}\right) \exp^{Y}Beard$ $\frac{r}{A}$ $-$ $-$ $\frac{8A}{U_{00,A}}$	- m - - s s	- Beard (1976) - - -
R _{Dkinj} Re r* RH t t ₁ T _{air}	Radius of the injection disc Reynolds number Normalised AP distance from the droplet centre Relative humidity of air Computational time Time spent to the AP to go from the injection disc to the droplet Air temperature	$A = A + x(t) + b = \sum_{\alpha, A}^{\infty} A$ $A = A + x(t) + Ax_{max}$ $\left(1 + 2.51\frac{\lambda_{air}}{2A}\right) \exp^{YBeard}$ $\frac{r}{A}$ $-$ $-$ $\frac{8A}{U_{\infty,A}}$	- m 	- Beard (1976) - - -
R _{Dkinj} Re r* RH t t ₁ T _{air} U _{AP}	Radius of the injection disc Reynolds number Normalised AP distance from the droplet centre Relative humidity of air Computational time Time spent to the AP to go from the injection disc to the droplet Air temperature AP velocity vector	$A + a + x(t) + Ax_{max}$ $\left(1 + 2.51\frac{\lambda_{air}}{2A}\right) \exp^{Y_{Beard}}$ $\frac{r}{A}$ $-$ $\frac{8A}{U_{\infty,A}}$	- m 	- Beard (1976) - - - - -
R_{Dkinj} Re r^* RH t t_1 T_{air} U_{AP} $U_{f@AP}$	Radius of the injection disc Reynolds number Normalised AP distance from the droplet centre Relative humidity of air Computational time Time spent to the AP to go from the injection disc to the droplet Air temperature AP velocity vector Fluid velocity at the AP location	$A + a + x(t) + Ax_{max}$ $\left(1 + 2.51\frac{\lambda_{atr}}{2A}\right) \exp^{Y_{Bard}}$ $\frac{r}{A}$ $-$ $-$ $\frac{8A}{U_{\infty,A}}$	- m s s K m.s ⁻¹ m.s ⁻¹	- Beard (1976) - - - - -
R_{Dkinj} Re r^* RH t t_1 T_{air} U_{AP} $U_{f@AP}$ U_{f}	Radius of the injection disc Reynolds number Normalised AP distance from the droplet centre Relative humidity of air Computational time Time spent to the AP to go from the injection disc to the droplet Air temperature AP velocity vector Fluid velocity at the AP location Unit vector in the radial direction	$A + a + x(t) + Ax_{max}$ $\left(1 + 2.51\frac{\lambda_{air}}{2A}\right) \exp^{Y}Beard$ $\frac{r}{A}$ $-$ $\frac{8A}{U_{\infty,A}}$	- m - s s K m.s ⁻¹ m.s ⁻¹	- Beard (1976) - - - - - - -
R_{Dkinj} Re r^* RH t t_1 T_{air} U_{AP} $U_{f@AP}$ U_{f} U_{P}	Radius of the injection disc Reynolds number Normalised AP distance from the droplet centre Relative humidity of air Computational time Time spent to the AP to go from the injection disc to the droplet Air temperature AP velocity vector Fluid velocity at the AP location Unit vector in the radial direction Unit vector in the orthogradial direction	$A + a + x(t) + b = \sum_{max}^{\infty} A$ $A + a + x(t) + Ax_{max}$ $\left(1 + 2.51\frac{\lambda air}{2A}\right) \exp^{YBeard}$ $\frac{r}{A}$ $-$ $-$ $\frac{8A}{U_{\infty,A}}$	- m - s s K m.s ⁻¹ m.s ⁻¹	- Beard (1976) - - - - - - -
R_{Dkinj} Re r^* RH t t_1 T_{air} U_{AP} $U_{f@AP}$ u_r u_e u_e u_e u_e u_e	Radius of the injection disc Reynolds number Normalised AP distance from the droplet centre Relative humidity of air Computational time Time spent to the AP to go from the injection disc to the droplet Air temperature AP velocity vector Fluid velocity at the AP location Unit vector in the radial direction Unit vector in the orthoradial direction Besulting velocity at the AP location	$A + a + x(t) + Ax_{max}$ $\left(1 + 2.51\frac{\lambda_{air}}{2A}\right) \exp^{YBeard}$ $\frac{r}{A}$ $\frac{R}{U_{\infty,A}}$	- m - s s s K m.s ⁻¹ - - - - - -	- Beard (1976) - - - - - - - - - -
R_{Dkinj} Re r^* RH t t_1 T_{air} U_{AP} $U_{f@AP}$ U_r u_{Θ} $U_{f@AP}$	Radius of the injection disc Reynolds number Normalised AP distance from the droplet centre Relative humidity of air Computational time Time spent to the AP to go from the injection disc to the droplet Air temperature AP velocity vector Fluid velocity at the AP location Unit vector in the orthoradial direction Resulting velocity at the AP location	$A + a + x(t) + Ax_{max}$ $\left(1 + 2.51\frac{\lambda a tr}{2A}\right) \exp^{Y}Beard$ $\frac{r}{A}$ $\frac{r}{A}$ $\frac{R}{U_{00,A}}$	- m - - s s K m.s ⁻¹ - - m.s ⁻¹	- Beard (1976) - - - - - - - - - - - - - - - - - - -
R_{Dkinj} Re r^* RH t t_1 T_{air} U_{AP} $U_{f@AP}$ u_{r} u_{Θ} $U^*_{f@AP}$	Radius of the injection disc Reynolds number Normalised AP distance from the droplet centre Relative humidity of air Computational time Time spent to the AP to go from the injection disc to the droplet Air temperature AP velocity vector Fluid velocity at the AP location Unit vector in the radial direction Unit vector in the orthoradial direction Resulting velocity at the AP location due to the added forces	$A + a + x(t) + Ax_{max}$ $\left(1 + 2.51\frac{\lambda_{air}}{2A}\right) \exp^{Y}Beard$ $\frac{r}{A}$ $\frac{r}{U_{00,A}}$	- m - s s K m.s ⁻¹ - m.s ⁻¹	- Beard (1976) - - - - - - - - - - - - - - - - - - -
R_{Dkinj} Re r^* RH t t_1 T_{air} U_{AP} $U_{f@AP}$ u_{Θ} $U_{f@AP}$ $U_{f@AP}$ $U_{f@AP}$ $U_{f@AP}$ $U_{f@AP}$ $U_{f@AP}$	Radius of the injection disc Reynolds number Normalised AP distance from the droplet centre Relative humidity of air Computational time Time spent to the AP to go from the injection disc to the droplet Air temperature AP velocity vector Fluid velocity at the AP location Unit vector in the radial direction Unit vector in the orthoradial direction Resulting velocity at the AP location due to the added forces Terminal velocity of the droplet	$A + a + x(t) + Ax_{max}$ $\left(1 + 2.51\frac{\lambda_{air}}{2A}\right) \exp^{YBeard}$ $\frac{r}{A}$ $-$ $\frac{Re}{U_{\infty,A}}$ $-$ $-$ $-$ $-$ $-$ $-$ $-$ $-$ $-$ $-$	- m 	- Beard (1976) - - - - - - - - - - - - - - - - - - -
R_{Dkinj} Re r^* RH t t_1 T_{air} U_{AP} $U_{f@AP}$ $U_{f@AP}$ $U_{f@AP}$ $U_{f@AP}$ $U_{g@AP}$ $U_{0,AP}$	Radius of the injection disc Reynolds number Normalised AP distance from the droplet centre Relative humidity of air Computational time Time spent to the AP to go from the injection disc to the droplet Air temperature AP velocity vector Fluid velocity at the AP location Unit vector in the radial direction Unit vector in the orthoradial direction Resulting velocity at the AP location due to the added forces Terminal velocity of the droplet	$A + a + x(t) + Ax_{max}$ $\left(1 + 2.51\frac{\lambda_{air}}{2A}\right) \exp^{Y}Beard$ $\frac{r}{A}$ $-$ $-$ $\frac{8A}{U_{\infty,A}}$ $-$ $-$ $-$ $-$ $-$ $-$ $-$ $-$ $-$ $-$	- m - - s s K m.s ⁻¹ - m.s ⁻¹ m.s ⁻¹	- Beard (1976) - - - - - - - - - - - - - - - - - - -
R_{Dkinj} Re r^* RH t t_1 T_{air} U_{AP} $U_{f@AP}$ U_f u_F u_G $U^*_{f@AP}$ U_{max} U_{max} U_{max}	Radius of the injection disc Reynolds number Normalised AP distance from the droplet centre Relative humidity of air Computational time Time spent to the AP to go from the injection disc to the droplet Air temperature AP velocity otector Fluid velocity at the AP location Unit vector in the radial direction Unit vector in the orthoradial direction Resulting velocity at the AP location due to the added forces Terminal velocity of the droplet AP fall speed disturbed by the added forces	$A + a + x(t) + Ax_{max}$ $\left(1 + 2.51\frac{\lambda_{air}}{2A}\right) \exp^{Y}Beard$ $\frac{r}{A}$ $\frac{r}{A}$ $\frac{R}{U_{00,A}}$ $\frac{r}{A}$ $\frac{r}{A}$ $\frac{r}{A}$ $\frac{r}{A}$	- m 	- Beard (1976) - - - - - - - - - - - - - - - - - - -
R_{Dkinj} Re r^* RH t l_1 T_{air} U_{AP} $U_{f@AP}$ u_r u_Θ $U^*_{f@AP}$ $U_{0,A}$ $U_{\infty,A}$ W_{∞}	Radius of the injection disc Reynolds number Normalised AP distance from the droplet centre Relative humidity of air Computational time Time spent to the AP to go from the injection disc to the droplet Air temperature AP velocity vector Fluid velocity at the AP location Unit vector in the radial direction Unit vector in the orthoradial direction Resulting velocity at the AP location due to the added forces Terminal velocity of the droplet AP fall speed disturbed by the added forces Wiener process	$A + a + x(t) + Ax_{max}$ $\left(1 + 2.51\frac{\lambda_{air}}{2A}\right) \exp^{YBeard}$ $\frac{r}{A}$ $\frac{r}{U_{\infty,A}}$ $\frac{R}{U_{\infty,A}}$ $\frac{n_{air}Re}{2A\rho_{air}}$	- m 	- Beard (1976) - - - - - - - - - - - - - - - - - - -
R_{Dkinj} Re r^* RH t t_1 T_{air} U_{AP} $U_{f@AP}$ u_{r} u_{Θ} $U_{f^{@AP}}$ $U_{{\mathcal{O}},A}$ $U_{\infty,A}$ $U_{\infty,a}$ W_t	Radius of the injection disc Reynolds number Normalised AP distance from the droplet centre Relative humidity of air Computational time Time spent to the AP to go from the injection disc to the droplet Air temperature AP velocity vector Fluid velocity at the AP location Unit vector in the radial direction Unit vector in the orthoradial direction Resulting velocity at the AP location due to the added forces Terminal velocity of the droplet AP fall speed disturbed by the added forces Wiener process	$A + a + x(t) + Ax_{max}$ $\left(1 + 2.51\frac{\lambda_{air}}{2A}\right) \exp^{YBeard}$ $\frac{r}{A}$ $\frac{r}{A}$ $\frac{R}{U_{\infty,A}}$ $\frac{r}{A}$ $\frac{r}{A}$ $\frac{r}{A}$	- m - - s s K m.s ⁻¹ m.s ⁻¹ m.s ⁻¹ m.s ⁻¹ 1 s ²	- Beard (1976) - - - - - - - - - - - - - - - - - - -
R_{Dkinj} Re r^* RH t t_1 T_{air} U_{AP} $U_{f@AP}$ $U_{f@AP}$ $U_{f@AP}$ $U_{f@AP}$ $U_{0,A}$ $U_{\infty,A}$ W_t T_{i}	Radius of the injection disc Reynolds number Normalised AP distance from the droplet centre Relative humidity of air Computational time Time spent to the AP to go from the injection disc to the droplet Air temperature AP velocity vector Fluid velocity at the AP location Unit vector in the radial direction Resulting velocity at the AP location due to the added forces Terminal velocity of the droplet AP fall speed disturbed by the added forces Wiener process	$A + a + x(t) + Ax_{max}$ $\left(1 + 2.51\frac{\lambda_{air}}{2A}\right) \exp^{Y}Beard$ $\frac{r}{A}$	- m - s s K m.s ⁻¹ m.s ⁻¹ m.s ⁻¹ m.s ⁻¹ s ¹ s ²	- Beard (1976) - - - - - - - - - - - - - - - - - - -
R_{Dkinj} Re r^* RH t t_1 T_{air} U_{AP} $U_{f@AP}$ $U_{f@AP}$ U_{T} U_{OAP} U_{T} U_{OAP} U_{T} U_{OAP} U_{M}	 Radius of the injection disc Reynolds number Normalised AP distance from the droplet centre Relative humidity of air Computational time Time spent to the AP to go from the injection disc to the droplet Air temperature AP velocity vector Fluid velocity at the AP location Unit vector in the radial direction Unit vector in the orthoradial direction Resulting velocity at the AP location due to the added forces Terminal velocity of the droplet AP fall speed disturbed by the added forces Wiener process AP location vector 	$A + a + x(t) + Ax_{max}$ $\left(1 + 2.51\frac{\lambda_{air}}{2A}\right) \exp^{Y}Beard$ $\frac{r}{A}$ $\frac{r}{A}$ $\frac{R}{U_{00,A}}$ $\frac{R}{U_{00,A}}$ $\frac{r}{A}$ $\frac{r}{A}$	- m 	- Beard (1976) - - - - - - - - - - - - - - - - - - -
R_{Dkinj} Re r^* RH t t_1 T_{air} U_{AP} $U_{f@AP}$ $U_{f@AP}$ $U_{f@AP}$ $U_{J^*@AP}$ $U_{\infty,A}$ $U_{\infty,a}$ W_t X_{AP} $X_{AP,i}$	 Radius of the injection disc Reynolds number Normalised AP distance from the droplet centre Relative humidity of air Computational time Time spent to the AP to go from the injection disc to the droplet Air temperature AP velocity vector Fluid velocity at the AP location Unit vector in the orthoradial direction Resulting velocity at the AP location due to the added forces Terminal velocity of the droplet AP fall speed disturbed by the added forces Wiener process AP location vector AP position on the axis i 	$A + a + x(t) + Ax_{max}$ $\left(1 + 2.51\frac{\lambda_{air}}{2A}\right) \exp^{YBeard}$ $\frac{r}{A}$ $\frac{r}{A}$ $\frac{R}{U_{\infty,A}}$ $\frac{r}{A}$ $\frac{r}{A}$ $\frac{R}{U_{\infty,A}}$ $\frac{r}{A}$	- m - - s s K m.s ⁻¹ m.s ⁻¹ m.s ⁻¹ m.s ⁻¹ s ² m	- Beard (1976) - - - - - - - - - - - - - - - - - - -
R_{Dkinj} Re r^* RH t t_1 T_{air} U_{AP} $U_{f@AP}$ $U_{f@AP}$ U_r u_{ϕ} $U_{f@AP}$ $U_{w,A}$ $U_{\infty,A}$ $U_{\infty,A}$ $U_{\infty,A}$ V_{t} X_{AP} $X_{AP,i}$ X_{APardi}	 Radius of the injection disc Reynolds number Normalised AP distance from the droplet centre Relative humidity of air Computational time Time spent to the AP to go from the injection disc to the droplet Air temperature AP velocity vector Fluid velocity at the AP location Unit vector in the orthoradial direction Resulting velocity at the AP location due to the added forces Terminal velocity of the droplet AP fall speed disturbed by the added forces Wiener process AP location vector AP position on the axis i Beard (1976) constant 	$A + a + x(t) + Ax_{max}$ $\left(1 + 2.51\frac{\lambda_{atr}}{2A}\right) \exp^{Y}Beard$ $\frac{r}{A}$	- m - - s s s K m.s ⁻¹ m.s ⁻¹ m.s ⁻¹ s ¹ s ² m	- Beard (1976) - - - - - - - - - - - - - - - - - - -
R_{Dkinj} Re r^* RH t t_1 T_{air} U_{AP} $U_{f@AP}$ $U_{f@AP}$ $U_{f@AP}$ $U_{g@AP}$ $U_{0,A}$ $U_{\infty,A}$ $U_{\infty,A}$ W_t X_{AP} $X_{AP,i}$ X_{Beard}	 Radius of the injection disc Reynolds number Normalised AP distance from the droplet centre Relative humidity of air Computational time Time spent to the AP to go from the injection disc to the droplet Air temperature AP velocity vector Fluid velocity at the AP location Unit vector in the orthoradial direction Resulting velocity at the AP location due to the added forces Terminal velocity of the droplet AP fall speed disturbed by the added forces Wiener process AP location vector AP location vector AP position on the axis <i>i</i> Beard (1976) constant 	$A + a + x(t) + Ax_{max}$ $\left(1 + 2.51\frac{\lambda_{air}}{2A}\right) \exp^{Y}Beard$ $\frac{r}{A}$ $-$ $-$ $\frac{8A}{U_{00,A}}$ $-$ $-$ $-$ $-$ $-$ $-$ $-$ $-$ $-$ $-$	- m 	- Beard (1976) - - - - - - - - - - - - - - - - - - -

$X_{d,i}$	Droplet centre in the axis <i>i</i>	0	-	-
$\sqrt{\langle x^2(t) \rangle}$	AP root mean square displacement	$\sqrt{2D_{im}D_bt_0}$	m	Einstein (1956)
x _{max}	Normalised maximal distance from the axis Z the AP is collected	-	-	-
x _{bro}	AP displacement related to the Brownian motion after t_1	-	-	-
<i>x</i> ₀	the inital AP location	0	-	-
YBeard	Beard (1976) constant	$\begin{bmatrix} 1 & X_{Beard}^1 & & X_{Beard}^6 \end{bmatrix} \otimes B_{Beard}$	-	Beard (1976)
Ζ	Radioactive AP number concentration	10	m ⁻³	Adachi et al. (2013)
Greek letters				
α	Ion recombinaison coefficient	1.6×10^{-12}	m ³ .s ⁻¹	Clement and Harrison (1992)
Δt	Time step	-	S	-
ε	Permittivity of free space	8.854× 10 ⁻¹²	m ⁻³ .kg ⁻ ¹ .s ⁴ .A ²	-
η	Radioactive decay rate of the AP	1.4	Bq	Adachi et al. (2013)
η_{air}	Air dynamic viscosity	$1.496 \times 10^{-6} \frac{T_{air}^{1.5}}{T_{air} + 120}$	kg.m ⁻¹ .s ⁻¹	Tinsley <i>et al.</i> (2006, Appendix A)
λ	Random variable sampled in a uniform distribution	-	-	-
λ_{air}	Mean free path of air molecules	21.55 \times n $\frac{T_{air}^{0.5}}{T_{air}^{0.5}}$	m	Tinsley et al. (2006,
		21.55 × Mair Pair	-1	Appendix A)
Λ	Scavenging coefficient	$\int_0^\infty \pi A^2 U_{\infty,A} \times$	S	Sportisse (2007)
		$E_c(a, A, q, Q, RH)f_A(A) dA$		
μ_	Electrical mobility of the negative ions	1.25×10^{-4}	m ² .V ⁻¹ .s ⁻¹	Clement and Harrison (1992)
ξ_{AP}	Vector of random variables for the three AP position components	-	-	Tinsley (2010)
ξ_{ψ}, ξ_{χ}	Independent vectors of random variables sampled in a standard	-	-	Minier and Peirano
1 A	normal distribution $\mathcal{N}(0,1)$			(2001)
Pair	Air density	$1.293 \times \frac{273.15}{T_{air}} \frac{P_{air}}{101325}$	kg.m ⁻³	Ideal gaz law
ρ_w	Water density	1000	kg.m ⁻³	-
ρ_{AP}	AP density	-	kg.m ⁻³	-
τ_{AP}	AP relaxation time	$2Cu\rho_{AP}a^2$	S	Minier and Peirano
		9nair		(2001)
ω_i	Mean energy required to form an ion pair	34	eV	Knoll (2010)

Appendix B. Supplementary data

Supplementary data to this article can be found online at https://doi.org/10.1016/j.jaerosci.2019.04.001.

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