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Sulfur-based electrode using a polyelectrolyte binder studied *via* coupled *in situ* synchrotron X-ray diffraction and tomography

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Abstract

Polyelectrolytes are promising binders for sulfur cathodes of Li/S batteries, with an ability to control the diffusion of polysulfides into the electrolyte, but their impact on the microstructural evolution of the electrode with cycling is presently unknown. In this study, coupled *in situ* synchrotron X-ray diffraction and tomography analyses are performed during the 1st and 11th cycles of a sulfur-based electrode made with poly(diallydimethylammonium) bis(trifluoromethane sulfonyl)imide as a polyelectrolyte binder. Sulfur deposited at the end of the 1st charge is mainly β -S₈ but some α -S₈ is also deposited during the 1st charge on the unreacted α -S₈ particles. No α -S₈ is detected at the 11th cycle, suggesting that remaining α -S₈ reacts progressively with cycling. The carbon-binder domain is not discernible due to spatial and contrast resolution limitations and thus, its evolution with cycling and its specific role on the sulfur dissolution and deposition processes cannot be clearly established. However, the fact that there is no collapsing of the electrode in the sulfur-depleted zones (in contrast to what was observed in literature with a conventional binder such as PVDF) suggests that the present polyelectrolyte is an efficient binder to preserve the electrode architecture upon cycling.

<u>Keywords:</u> sulfur electrode, Li/S batteries, polyelectrolyte bonder, in-situ X-Ray tomography, in-situ X-Ray diffraction

1. Introduction

With the inability of today's Li-ion batteries to fully meet electric vehicle (EV) requirements and the rarefaction and high cost of some of its materials, especially cobalt¹, it has become a necessity to search for a successor to the Li-ion system. For this purpose, the lithium-sulfur (Li/S) system is currently one of the most promising technologies.² Elemental sulfur is both low-cost and abundant and can provide a theoretical specific capacity of 1675 mAh g⁻¹, leading to a theoretical energy density of 2567 Wh kg⁻¹ for Li/S system *versus* 387 Wh kg⁻¹ for typical graphite/LiCoO₂ system.³ However, the Li/S system is based on an entirely different chemistry than Li-ion batteries and faces several issues, such as insufficient cycle life and volumetric energy density, which need to be addressed and resolved before possibility of commercialization.

Charge transfer in Li/S batteries is operated via a series of chemical and electrochemical reactions involving dissolution and precipitation of sulfur species, inducing important morphological changes of the positive electrode. The phase transformation of the positive active material upon discharge (from initial solid S_8 to precipitated solid Li₂S) involves going through the formation of soluble species (Li₂S_n, $8 \ge n > 2$).⁴ The dissolution of these intermediate polysulfide species and their diffusion to the lithium metal electrode can lead to several of the main issues of Li/S systems, such a progressive loss of active material, self-discharge, or "shuttle reactions", causing low coulombic efficiency and reduced cycle life. Therefore, many different ways are investigated in order to get a better control on these mechanisms on a molecular scale, including works on electrolyte composition⁵, separator modifications⁶, or nano-scale sulfur encapsulation.⁷

Polyelectrolytes are polymers composed of ionizable groups charged either positively or negatively. Thanks to their combined polymer and electrolyte properties, they have been used in various applications, among which corrosion protective coatings.^{8,9} In a recent work¹⁰, the

usability of polyelectrolyte binders for sulfur-based electrodes has been demonstrated and have shown highly promising performance in terms of capacity retention and rate capability at high areal sulfur loading, making their operation possible with high accessible capacity (up to $\sim 8 \text{ mAh cm}^{-2}$) at high C-rates (up to 2 C) and with high areal sulfur loadings (up to 8.1 mg cm⁻²). This is related to the ability of the cationic polyelectrolyte binder to (*i*) restrict the diffusion of soluble polysulfide species from the porous carbon sulfur host into the electrolyte due to the preferential and strong electrostatic interactions of the lithium polysulfides with the cationic polymer backbone and (*ii*) facilitate the lithium ion transport in the sulfur electrode thanks to the reconfigurable network of mobile anions associated with the cationic polymer backbone. On the other hand, the binder can also have a major influence of the mechanical properties (adhesion and cohesion strengths) of the electrode, which are likely to impact on the morphological degradation of the electrode (*e.g.* collapse, delamination from the current collector) associated with the sulfur dissolution upon cycling. To the best of our knowledge, the impact of the polyelectrolyte type binder on the morphological evolution during cycling of sulfur electrodes has never been evaluated.

In situ X-ray diffraction (XRD) and X-ray computed tomography (XRCT) are without contest some of the most powerful analytical tools to characterize the structural and morphological changes of battery electrodes upon cycling.¹¹ XRCT is a non-destructive 3D imaging technique that enables the extraction of crucial quantitative parameters such as volume fraction, size distribution, tortuosity or connectivity of the different phases inside the electrodes. In order to access those parameters, the different phases (*e.g.* active material, carbon and binder additives, electrolyte, current collector, separator) need to be differentiated ("segmented") through image processing and analytical procedures. The use of a synchrotron X-ray source not only enables phase contrast imaging, which accentuates the differentiation,

but also grants a better spatial resolution (few tens of nm *versus* few μ m for laboratory X-ray sources) and shorter acquisition times.

For the past years, *in situ* laboratory XRD^{12–15}, and *in situ* synchrotron XRD^{16–23} have been used to monitor the evolution of crystalline sulfur species in various positive electrode formulations. In most studies, diffraction peaks from α -S₈ and β -S₈ are identified and their evolution is quantified during discharge and charge. In some cases, Li₂S peaks were also identified^{13,16,21}, and in some more rare cases, polysulfide species were observed.^{17,24} Although *in situ* synchrotron XRCT has been used by many groups to characterize lithiumion battery electrodes, such as silicon-based anodes^{25,26}, LiCoO₂²⁷ or NMC²⁸ positive electrodes, it is only very recently that S-based electrodes have started to be investigated.^{29–} ^{31,19} Yermukhambetova et al. studied sulfur evolution at a nanometric scale in conventional electrodes.²⁹ Zielke *et al.* were able to follow the dissolution and deposition of sulfur inside a porous carbon electrode.³⁰ Tonin *et al.* confirmed these observations by combining *operando* XRCT with XRD and also characterizing the morphological changes in the lithium anode.³¹ Yu *et al.* combined several X-ray based techniques to follow the evolution of sulfur clusters as well as Li₂S formation and the influence of current density.¹⁹

In the present work, a sulfur cathode integrating a polyelectrolyte binder (poly(diallydimethylammonium) bis(trifluoromethane sulfonyl)imide) is studied by coupled *in situ* synchrotron XRD and XRCT performed during the 1st and 11th cycles. Those techniques were chosen in order to assess if the use of this polyelectrolyte binder has an impact on the electrode morphology evolution during cycling and degradation, on top of its aforementioned advantageous properties. The sulfur dissolution and deposition processes are observed and their occurrence depending on the cycling stage, spatial position in the electrode and size of the sulfur particles is highlighted. The absence of electrode collapsing in the sulfur-depleted zones is also highlighted.

2. Experimental

2.1.Polyelectrolyte binder synthesis

The polyelectrolyte binder used in this work was a poly(diallydimethylammonium) bis(trifluoromethane sulfonyl)imide, abbreviated PDDA-TFSI. It is obtained by exchanging the CI^{\circ} anion of PDDACl with the TFSI^{\circ} anion of LiTFSI.^{10,32} To do so, 2.4 g (0.015 monomer mole) of PDDACl solubilized in water (20 wt%, Sigma-Aldrich) was mixed with 5 g (0.017 mole) of LiTFSI salt (99.95%, Sigma-Aldrich) and 150 mL of deionized water and was stirred for 72 hours. A dense and insoluble light-colored precipitate formed in the mix, which was centrifuged allowing the supernatant solution to be removed. The obtained precipitate was then quickly dried and was mixed again with 2 g (0.007 mole) of LiTFSI in 80 mL of acetone, ensuring the full completion of the anionic exchange reaction, as confirmed from ¹⁹F NMR analysis (not shown). After 12 hours of stirring, the mixture was concentrated by evaporating the acetone. It was then precipitated in 500 mL of deionized water under stirring for several hours, before being filtered and dried.

2.2. Materials and electrode preparation

The synthetized PDDA-TFSI was used as a binder material in composite sulfur electrodes. As received sulfur (S) powder (-325 mesh, 99.5%, Alfa Aesar) was used as active material and carbon black (CB) (Super P Li, Timcal) as a conductive additive. The electrode composition was fixed to 70/20/10 wt% (S/CB/binder). An aluminum foil (20 µm thick, current collector. Polyvinylidene MTI) difluoride (PVdF) was used as and carboxymethylcellulose (CMC) binders were also used in composite electrodes to compare the electrochemical performance of the different binders. Depending of the nature of their binder (PDDA-TFSI, PVdF and CMC), the three electrodes formulations were respectively labelled as PDDA, PVdF and CMC.

S and CB powders were manually ground in an agate mortar for 15 minutes with addition of a few drops of cyclohexane in order to get a homogeneous composite. After evaporation of the cyclohexane, the resulting S+CB powder was recovered. The PDDA-TFSI binder was weighed and dissolved in N-methyl-2-pyrrolidone (NMP) (anhydrous, 99.5%, Sigma Aldrich) until a 12 wt% solution was obtained. It was then poured into a silicon nitride vial along with three silicon nitride milling balls, to which the S+CB powder was added. The slurry was mixed using a Fritsch Pulverisette 7 mixer at 500 rpm for 1 hour. The resulting homogenized ink was coated onto the Al current collector using a doctor-blade technique, where the blade gap was tailored in order to keep the areal sulfur loading of the electrodes as constant as possible. A blade gap of 300 μ m gave a dry coating of 70±5 μ m with a sulfur loading of 2±0.3 mg_{sulfur} cm⁻². The electrodes were dried at 60°C for 24 hours in a vacuum oven before being cut into discs (Ø14 mm for coin cells and Ø2.5 mm for synchrotron cells) and stored in an argon-filled glove-box. PVdF and CMC-based electrodes were constructed in a similar way as described in our previous work.³³

2.3.Cell assembly

Conventional CR2032 two-electrode coin cells were used for the electrochemical testing of the electrodes. The cells were assembled in the glove box by stacking the sulfur electrode, a thick polyolefin non-woven tissue (Viledon, Freudenberg) serving as electrolyte reservoir and separator, a polypropylene separator (Celgard 2400) and a disc of lithium metal (MTI) serving as counter and reference electrode. The selected electrolyte had a standard composition of 1 M LiTFSI and 0.1 M lithium nitrate additive (Aldrich) dissolved in a 1/1 volume ratio mixture of tetraethylene glycol dimethyl ether (TEGDME, 99%, Aldrich) and 1,3-dioxolane (DIOX, anhydrous, 99.8%, Aldrich). 150 μ L of electrolyte was poured onto the working electrode and the separators in order to completely soak the porosities of all the materials.

The cell used for *in situ* synchrotron XRCT/XRD measurements was a two-electrode Swagelok cell inspired from previous similar experiments in our group on Si-based electrodes.²⁵ As schematized in **Figure 1**, the S-based electrode diameter was 2.5 mm. The casing of the cell was made of perfluoroalkoxy alkane (PFA) polymer with a reduced wall thickness near the electrodes in order to lower X-ray attenuation during experiments. The positive sulfur electrode was placed onto an additional thick aluminum cylinder to avoid stainless steel connector to be visible in the imaged zone. A spring placed on the negative electrode side ensured the compression and the electrical contact of the cell components.



Figure 1. Schematic diagram of the electrochemical cell used for in situ synchrotron XRCT/XRD experiments

2.4. Electrochemical measurements

Coin cell cycling experiments were performed on a BTS4000 (Neware) battery cycler. For synchrotron experiments, a SP-300 potentiostat/galvanostat (Bio-Logic Science Instruments) was used. The cells were galvanostatically cycled between 1.5 and 3.0 V at a rate of C/50 or C/20. The values of the applied current were calculated based on the loading of each electrode and the theoretical capacity of sulfur (1675 mAh g⁻¹). The capacities are expressed in mAh per g of sulfur.

2.5.In situ synchrotron X-ray tomography and X-ray diffraction

In situ synchrotron XRCT and XRD measurements were performed on beamline ID11 at the European Synchrotron Radiation Facility (ESRF) (Grenoble, France). XRCT and XRD analyses were successively carried out every 30 minutes during the 1^{st} and 11^{th} cycles. The cell was cycled at C/20 and was set to open circuit potential (OCP) during the acquisition of the radiographs and diffraction patterns. The acquisition time of XRCT was ~15 min and ~2 min for XRD, with ~2 min for switching between the two configurations.

The tomography detector was coupled via an optical microscope to a thin phosphor scintillator. The diffraction detector used a fiber optic taper and a thicker phosphor scintillator.³⁴ The energy of the monochromated beam was set at 38 keV ($\lambda = 0.0326$ nm) and a beam size of 1 × 1 mm² for XRCT. The PyHST2 software³⁵ was used to reconstruct the 3D tomographic volumes of 1433 × 1433 × 490 µm³ with an isotropic voxel size of 0.7 µm (meaning a spatial resolution of about 1.4 µm). The dimensions of the imaged zone were calibrated to cover the whole active height of the cell, from the aluminum current collector on the positive electrode side to the stainless steel collector on the lithium electrode side. In order to reduce the size of the image stacks and facilitate the image analyses, the studied zone was subsequently cropped from the bottom of the positive electrode up to the separator, corresponding to an analyzed volume of 1433 × 1433 × 70 µm³. The grayscale values in the presented pictures correspond to the attenuation coefficient, therefore denser and more attenuating regions appear brighter. All image processing and quantitative analyses were performed using the Fiji software.³⁶

The XRD detector was placed at a distance of 25 cm of the sample. The energy of the beam was the same as XRCT measurements, and the incident beam size was restricted down to $50 \times 50 \ \mu\text{m}^2$ at FWHM. A total of 20 successive 2D XRD images were obtained for each

cycling step, one diffraction scan being acquired in 20 µm steps along the vertical axis of the electrochemical cell. This way, the whole active height of the cell was covered, from the Al current collector on the positive electrode side up to the stainless steel collector on the negative electrode side. The 2D XRD pictures were integrated to obtain full XRD patterns. The background signal was measured on an empty Swagelok cell and was removed by subtraction from the XRD patterns.

3. Results and discussion

3.1.Electrochemical performance

The electrochemical performance of the electrode fabricated using polyelectrolyte PDDA binder was compared to the two more conventional formulations (PVdF and CMC) by cycling of coin cells at C/50 at room temperature. **Figure 2a** shows the evolution of the specific discharge capacities of all three formulations during 50 cycles. As already shown in our previous work³³ and in the literature³⁷, PVdF and CMC formulations show similar performance, with an initial discharge capacity of respectively 640 mAh g⁻¹ and 610 mAh g⁻¹, quickly dropping during the first ten cycles to reach a value around 250 mAh g⁻¹ after 50 cycles. On the other hand, the PDDA formulation presents an improved initial discharge capacity of 1050 mAh g⁻¹ with a lower capacity decay upon cycling to reach a nearly stable discharge capacity of 730 mAh g⁻¹ after 50 cycles, hence almost 3 times the capacity of the previous formulations. These results are in accordance with the study of Li *et al.* showing a higher initial capacity and a better capacity retention during prolonged cycling of S-based electrode with polyelectrolyte PDDA-TFSI binder compared to conventional PVdF binder.¹⁰



Figure 2. (*a*) Evolution with cycling of the discharge capacities of PDDA, PVDF and CMC electrodes cycled in coin cell at C/50 and (b) First discharge/charge curves of a PDDA electrode cycled in coin cell and synchrotron cell at C/20. In all cases, the electrode loading is $2\pm0.3 \text{ mg}_{sulfur} \text{ cm}^{-2}$.

Figure 2b compares the voltage profiles of the PDDA electrode at C/20 during the 1st cycle performed in a CR2032 coin cell and in the synchrotron cell used for XRD and XRCT experiments. The interruptions in the voltage profile of the synchrotron cell correspond to the XRD-XRCT acquisition steps during which the cell was let in open circuit. These OCP periods of ~20 min per acquisition step are deleted in **Figure 2b**. First, it can be seen that the initial discharge capacity of the coin cell at C/20 is lower than at C/50, here reaching 810 mAh g⁻¹ (*vs.* 1050 mAh g⁻¹ at C/50 in **Figure 2a**). The discharge capacity of the synchrotron cell at C/20 is lower, with an initial value of 660 mAh g⁻¹. Most of the difference in the discharge capacities of the two cell configurations resides in the length of the second discharge plateau, noticeably shorter for the synchrotron cell. During this plateau, the polysulfide species (Li₂S_n, 8 ≥ n > 2) dissolved in the electrolyte are reduced in shorter polysulfide chains and solid products Li₂S₂/Li₂S are formed. A shorter plateau can mean a lower amount of solid products being precipitated associated with an incomplete reduction reaction. The charge capacity of the synchrotron cell is also noticeably smaller, *i.e.* 470 mAh g⁻¹ compared to 680 mAh g⁻¹ with the coin cell. A possible explanation is that some dissolved

polysulfides diffuse outside the electrode during the successive OCP periods (cumulated duration of ~6 h over the first discharge/charge period of ~14 h) and thus become inaccessible for further electrochemical reaction. However, cycling experiments performed with the synchrotron cell but without current interruption periods display similar performance (not shown). Actually, as evidenced in **Figure 2b**, the electrode polarization is much higher with the synchrotron cell than with the coin cell, resulting in a less deep (incomplete) discharge. Its higher polarization resistance may be due to an imperfect contact of the S-electrode with the current collector because of its small size and the lower compression of the cell, as this phenomenon has been observed on all our tested synchrotron cells, whatever the sulfur electrode formulation. In particular, a homogenous pressure inside the synchrotron cell is more difficult to control due to the reduced size of the electrodes (2.5 mm diam.) even if a spring has been used. This is also in accordance with the presence of an inactive zone at the center area of the S-based electrode in the synchrotron cell, as shown below from the XRCT analysis.

3.2. In situ synchrotron X-ray diffraction

Figure 3a-b shows the evolution of the diffraction patterns focused on the 3.0-4.0 Å d-spacing region during the 1st and 11th cycles respectively, along with the corresponding voltage profiles. The patterns obtained during discharge and charge are represented in blue and red respectively. **Figure 3c-d** are color maps of the evolution of the XRD peak intensities upon cycling.



Figure 3. XRD patterns acquired during the 1^{st} cycle (a) and 11^{th} cycle (b) and color intensity mapping of corresponding patterns (c,d)

At the initial state, the observed XRD peaks can be attributed to α -S₈ and are marked with a (*) symbol in **Figure 3a**. In accordance with JCPDS 01-078-1888, these peaks can be observed at 3.09 Å (α -S₈(135)), 3.12 Å (α -S₈(313)), 3.22 Å (α -S₈(117)), 3.34 Å (α -S₈(311)), 3.45 Å (α -S₈(026)), 3.57 Å (α -S₈(133)) and 3.86 Å (α -S₈(222)). The intensity of those peaks decreases along the whole discharge. This is highlighted in **Figure 4**, which displays the relative variation of the added α -S₈ peak areas as a function of the depth-of-discharge (DOD) and state-of-charge (SOC) levels during the 1^{st} cycle. The α -S₈ dissolution mainly occurs during the first plateau (first 4 steps of discharge) but is also observed during the second discharge plateau and is not fully completed at the end of the 1st discharge. This result differs from the study of Tonin et al.³¹ showing from operando synchrotron XRD analyses the complete disappearance of the α -S₈ peaks during the 1st discharge plateau. As previously said, this may be associated with some contact problem in our synchrotron cell, impacting on its discharge efficiency. No Li₂S peak can be detected at the end of the discharge. It can be explained by the low degree of crystallinity of the formed Li₂S that can preclude its clear detection by XRD.³⁸ This can also indicate an incomplete polysulfide reduction with the preferential formation of amorphous Li₂S₂ instead of crystalline Li₂S, in accordance with the low discharge capacity extracted from the 2^{nd} plateau region (~350 mAh g⁻¹). At the very end of the 1st charge (starting around 70% of SOC), β -S₈ peaks, marked with a (+) symbol in **Figure 3a**, appear at 3.16 Å (β -S₈(311)), 3.34 Å (β -S₈(103)), 3.53 Å (β -S₈(122)) and 3.70 Å $(\beta$ -S₈(-122)) in accordance with JCPDS 01-077-6252, even though a constant slight shift of about 0.04 Å⁻¹ can be noticed in the XRD observations. This shift only affects β -S₈. Hence, the fact that both α -S₈ and β -S₈ are crystallized at the same time may induce compatibility stresses inside the metastable β -S₈, possibly causing the observed shift in the β -S₈ peaks. Some of the initial α -S₈ peaks also gain slightly in intensity at the end of the charge (Figure 4), which is unexpected. As discussed below from the XRCT data, it might be related to the presence of unreacted α -S₈ in the electrode, acting as nucleation sites for the partial oxidation of the polysulfides in α -S₈ instead of β -S₈.



Figure 4. Evolution of the the added α -S₈ XRD peak area during the 1st cycle

Figure 3b presents the evolution of the diffraction peaks of the same PDDA electrode during its 11th cycle. Most of the peaks detected at 0% DOD and 100% SOC can be attributed to the β -S₈ phase. There is no clear evidence of the presence of the α -S₈ phase, suggesting that most of the α -S₈ remaining at the end of the 1st cycle has reacted progressively during the following cycles and was redeposited as β -S₈ at the end of each charge. A wide "peak" centered at around 3.3 \AA^{-1} appears at ~90% of DOD and remains through the beginning of the charge. This wide peak is here attributed to Li_2S (111) identified at 3.28 Å⁻¹ in accordance with JCPDS 01-077-2874. The presence of partly crystalline Li_2S at the 11th cycle indicates that the polysulfide species have been more completely reduced into crystalline Li₂S during the second discharge plateau, compared to the 1st cycle. Finally, an intense peak can be observed at around 3.7 Å in Figure 3c-d, which is associated with another intense peak detected at about 4.1 Å (not shown). No significant evolution in their intensity can be noticed during the 11th cycle. However, their intensity varies depending on the XRD acquisition area along the vertical axis of the cell, with a maximal intensity observed near the S cathode/separator interface, as shown in Figure S1 in supplementary information. Note that these two peaks were also detected at the 1st cycle but with a lower intensity. Their origin is presently unclear but they could result from the reaction of the polysulfides with the cell casing.

3.3.In situ synchrotron X-ray tomography

Figure 5a-c shows the evolution of a selected lateral (*i.e.* parallel to the current collector) slice of the positive electrode during the 1st cycle at different states of discharge and charge, namely at the initial state (0% DOD), at the end of the discharge (100% DOD) and at the end of the charge (100% SOC). The cross-section view of the electrode is also represented below each lateral image, with the aluminum current collector being visible in light gray. Video S1 in supporting information shows the evolution of these lateral and transversal views during the whole 1st cycle. The lateral slice was selected to be representative of the morphological evolution of the electrode and is close to the interface with the separator. As mentioned in the experimental section, lighter elements appear in a brighter gray. Four different phases can be identified on these images: (i) the fibers of the separator in the darker gray level; (ii) the large sulfur particles or particle clusters (*i.e.* with a diameter higher than $\sim 2 \mu m$) in white; (*iii*) the sulfur-rich phase in light gray, containing the lower diameter sulfur particles not distinguishable from the binder, carbon black and submicrometric pores/interstices due to spatial resolution limitation but the sulfur presence is indicated by the overall lighter gray level of the region and (iv) the porous sulfur-free phase in mid-tone gray, filled with electrolyte and also containing the undiscernible binder and carbon black.



Figure 5. Lateral and transversal XRCT images of the electrode at (a) 0% DOD, (b) 100% DOD and (c) 100% SOC of the 1^{st} cycle. (d) Enlargement of (c). The red dashed line in the lateral images corresponds to the position of the transversal images. The blue square corresponds to the selected active zone shown in Fig. 6.

It can be seen in **Figure 5a** that at 0% of DOD, most of the imaged area is occupied by the sulfur containing phase, where bigger sulfur particles are also visible. Some fibers from the separator are visible, as the chosen slice is located close to the electrode-separator interface. The porosity of the electrode appears mostly filled with electrolyte, as no gas phase (likely to be visible in black) can be identified. In **Figure 5b** (100% DOD), it can be observed that a lot of the sulfur phase has been dissolved, leaving the porous carbon-binder domain

(CBD) filled with electrolyte. The size of some of the larger sulfur particles visible in this dissolved area have also been reduced during the discharge process. However, it can be seen that a large area of sulfur-rich phase situated at the center of the electrode remains at the end of the discharge, suggesting that this zone is not electrochemically active during the first discharge. This is in accordance with our previous XRD observation showing some α -S₈ remaining at the end of the 1st discharge. This inactive zone (also observed in other cells using different binder formulation) may originate from the uneven surface of the aluminum current collector conjugated to an insufficient compression of the synchrotron cell, resulting in an imperfect contact of the electrode film on the Al current collector. Based on the volume of the segmented sulfur-rich region at the end of the 1st discharge, the inactive portion of the electrode corresponds to around 40% of the observed volume. Considering that the observed volume represents ~33% of the whole electrode volume, the inactive zone represents ~13% of the whole electrode volume, assuming there is no other inactive zone in the part of the electrode which is not observed. This partly explains the difference in the initial discharge capacity between the synchrotron cell and the coin cell. As it can be seen in Video S1, the dissolution of the sulfur phase starts from the edges of the electrode and moves inwards to its center. Considering the very slow lateral displacement rate of the front dissolution (~40 µm h⁻ ¹), it can be hardly explained by some difference in Li-ion diffusivity depending on their lateral position in the electrode. This unexpected phenomenon may rather indicate the present of a potential gradient in the electrode resulting from the higher contact resistance at the electrode center.

As mentioned in the XRD results section, it is unclear whether Li_2S was formed at the end of the 1st discharge. However, due to its nanometric size, it could not be visible on the tomography images because of resolution limitations and has not yet been directly observed by XRCT in the literature. The deposition of β -S₈ during discharge is clearly observable in **Figure 5c** and **Video S1**. This deposition starts again from the edges of the electrode and progresses inwards. It can also be seen that the β-S₈ follows a deposition pattern, where deposited sulfur acts as preferred nucleation sites, forming elongated agglomerates as shown in the enlarged image (**Figure 5d**). Supporting this assertion, part of the sulfur deposition also starts from the edges surrounding the inactive central zone and on the incompletely dissolved larger sulfur particles. This is also in agreement with the XRCT observations of Yermukhambetova *et al.*, suggesting that the remaining sulfur particles deep within the electrode act as favorable nucleation sites for sulfur deposition.²⁹ Furthermore, as mentioned in the XRD experiments section, if most of the deposited sulfur at the end of the charge is β-S₈, some α-S₈ also seems to have been electrodeposited during the charge. This could mean that the sulfur electrodeposited onto remaining α-S₈, which did not react during the discharge, follows the same crystalline pattern and is electrodeposited as orthorhombic α-S₈.



Figure 6. Lateral and transversal XRCT images focused on an electrochemically active zone of the electrode at (a) 0% DOD, (b) 100% DOD and (c) 100% SOC of the 1st cycle. The red dashed line in the lateral images corresponds to the position of the transversal images.

Figure 6a-c shows lateral and transversal XRCT slices focused on an electroactive zone of the electrode zone (delimited by the blue square in **Figure 5b**) at 0% DOD, 100% DOD and 100% SOC of the 1st cycle. As seen in the transversal images, there is no evidence of collapsing of the electrode upon cycling. Actually, the decrease of the electrode thickness at

the end of the 1st discharge, determined from the transversal displacement of the separator fibers, is estimated at about 7-8 μ m (*i.e.* ~10% of its initial thickness). This suggests that PDDA-TFSI is an efficient binder to preserve the electrode architecture despite the sulfur depletion. In comparison, with PVDF as a binder, a much larger decrease of the electrode thickness was noticed by G. Tonin³⁹. Indeed, a decrease of about 80% of the electrode thickness was observed while discharging the cell, *i.e.* the electrode thickness decreased from \sim 42 µm at the pristine state to \sim 9 µm after the first quasi-plateau. In presence of PVdF binder, the electrode thickness evolution is in good accordance with the porosity created by reduction and dissolution of sulfur. Such electrode collapsing is not observed with the PDDA-TFSI binder, which may be associated with benefic interaction between the binder and the CB or sulfur compounds. In presence of PVdF binder, the electrode thickness evolution is in good accordance with the porosity created by reduction and dissolution of sulfur. Such electrode collapsing is not observed with the PDDA-TFSI binder, which may be associated with benefic interaction between the binder and the CB or sulfur compounds. More details on the volume expansion/contraction of sulfur-based electrodes depending on the binder nature (CMC, PVDF and PDDA-TFSI), evaluated by *operando* dilatometry, will be presented in a future article. Additionally, we can see in the transversal image of Figure 6c that the upper zone of the electrode near the separator is whiter, suggesting a preferential sulfur deposition at the electrode surface.



Figure 7. Lateral and transversal XRCT images of the electrode at (a) 0% DOD, (b) 100% DOD and (c) 100% SOC of the 11th cycle. The red dashed line in the lateral images corresponds to the position of the transversal images

Figure 7a-c shows the same PDDA electrode during its 11th cycle, at the same three states of discharge-charge as Figure 5. The chosen lateral slices are also at the interface between the electrode and the separator. Video S2 in supporting information shows the evolution of the electrode during the whole 11th cycle. As described in the XRD section, most of the observable sulfur (light gray scarce areas) at the initial state (0% of DOD) of the 11th cycle is now β -S₈. It can be seen that the deposition pattern that was visible at the end of the 1st charge is now completely different. The inactive central zone is also not visible anymore. As seen in Video S2, the majority of the sulfur visible in Figure 7a is dissolved in the first 30 minutes of discharge, in accordance with the short duration of the first discharge plateau. In Figure 7b, at 100% DOD, no elemental sulfur seems to be visible anymore, including the larger sulfur particles. This support our conclusion in the XRD section that the remaining α - S_8 of the 1st cycle has progressively reacted during the subsequent cycles. Sulfur deposition at the end of the 11th cycle is also observed (Figure 7c), showing again different patterns. Without pre-existing sulfur acting as preferential deposition sites, sulfur seems to be depositing in a random manner, perhaps dictated by the porosity and the carbon available surface of the carbon-binder domain, which cannot be seen on these images. Finally, even

though XRD results seem to indicate the presence of solid crystalline Li_2S , it cannot be observed in **Figure 7b** because of the nanometric size of Li_2S .



Figure 8. (a) 3D views of the sulfur-rich phase at 0% DOD, 100% DOD and 100% SOC for the 1st cycle, and (b) relative variation during the 1st cycle of the sulfur-rich phase volume in the total analyzed electrode volume of $1433 \times 1433 \times 70 \ \mu\text{m}^3$ (black curve) and in a selected active zone of $376 \times 333 \times 70 \ \mu\text{m}^3$ (blue curve) shown in Fig.6.

Figure 8a shows reconstructed 3D views of the segmented sulfur-rich phase (including also the segmented large S particles) at different stages of the 1st cycle for the total analyzed electrode volume of $1433 \times 1433 \times 70 \ \mu\text{m}^3$. The segmented sulfur-free phase (*i.e.* porous carbon-binder domain filled with electrolyte) is set transparent in this rendering. **Video S3** in supporting information shows the complete evolution in 3D view of the sulfur-rich phase during the 1st cycle. From these segmentations, the relative volume variation of the sulfur-rich phase during the 1st cycle can be determined as shown in **Figure 8b** (black curve). Its volume is normalized at 100% for the initial state. Note that this black curve differs from the

curve extracted from XRD analyses in Figure 4 because here both α -S₈ and β -S₈ are involved. Moreover a large part (40%) of the XRCT analyzed volume is non-active compared to 13% for the XRD analyses. Whereas in theory the elemental sulfur dissolution only occurs during the first discharge plateau, it can be seen here that the volume fraction of sulfur constantly decreases during the discharge. This may be considered as a side effect of the incomplete sulfur reduction in the electrode. It can even be observed that some of the remaining sulfur at the end of the discharge keeps dissolving by contact with the electrolyte at the beginning of the charge. At 100% SOC, the recovered volume of the sulfur-rich phase is calculated about 80%, *i.e.* a 20% loss compared to the initial state. Considering that only 87% of the whole electrode was active during the discharge (from the previously calculated 13% inactive volume), we can estimate a ~69% recovery. Even though it remains biased by the fact that only a portion of the electrode is observed, this value is close to the CE value of 71% calculated from the discharge and charge capacities of the electrode at the 1st cycle (660 and 470 mAh g⁻¹, respectively). A similar segmentation procedure was performed on the selected electroactive area shown in Figure 6 and the relative volume variation of the segmented sulfur-rich phase in this active domain is presented in **Figure 8b** (blue curve). Here, the volume variation of the sulfur-rich phase follows a trend in better agreement with the theory, which predicts that the sulfur reduction occurs mainly during the 1st discharge plateau. The volume of the sulfur phase decreases sharply down to 40-50% of DOD. The remaining volume belongs for the most part to the large sulfur particle included in the selected area, which does not dissolve completely. Then, the volume stays under 5% until 50% of SOC and finally increases again until it reaches a value of ~74% at 100% of SOC.



Figure 9. (a) 3D view of the segmented sulfur particles in the electrode and (b) evolution of the volume of selected particles A, B and C during the 1^{st} cycle

Figure 9a shows a reconstructed 3D view of the large sulfur particles in the electrode at the initial state after removing all other phases. **Video S4** in supporting information show their evolution during the 1^{st} cycle. This allows for the quantification of the volume evolution of individual large sulfur particles in the electrode. For this purpose, three sulfur particles have been selected in the electrochemically active zone as indicated in **Figure 9a**: particle *A*

is the largest particle of a cluster located at the edge of the inactive zone at the surface of the electrode, particle B is also located at the edge of the inactive zone but closer to the current collector (lower z position); and particle C is located further away from the central inactive zone at the electrode surface. All the large particles located inside the inactive zone see no change in their morphology. Figure 9b describes the evolution of the volume of the A, B and C particles during the 1^{st} cycle. It can be seen that particle A, which is the largest and the closest to the inactive zone, does not start dissolving until ~60% of DOD. Moreover, it continues to dissolve at the beginning of the charge, probably by redox reaction with the polysulfides present in the electrolyte, until reaching a minimal volume value of about 1200 μ m³, corresponding to ~12% of its initial volume. From ~60% of SOC, its volume starts increasing again due to the oxidation of polysulfides into sulfur to reach 3200 μ m³ at the end of the charge. This tends to support our earlier claim that remaining sulfur acts as nucleation site during sulfur electrodeposition at the end of the charge. Particle B follows a similar trend, also being located at the edge of the inactive zone, with a dissolution starting ~60% of DOD. Due to its lower initial volume, particle B is nearly completely dissolved at the end of the discharge, confirming the major impact of the initial size of the sulfur on their electrodissolution rate. However, the absence of large S particles at the 11th cycle suggests they are fully dissolved within a few cycles. Particle C, having an initial volume similar to particle B but being further away from the inactive central zone, dissolves almost immediately and completely during the first 40% of DOD. This confirms the major impact of the position of the S particles in the lateral x-y plan on their electrodissolution rate in the cell investigated. In contrast, on the basis of the present XRCT data, this is no clear evidence that the transversal position of the S particles in the electrode influences significantly their dissolution rate. However, keeping in mind the presence of a large non-electroactive area due to a weak contact on the current collector in the present synchrotron cell, further observations

would be needed to draw more conclusions on the dissolution kinetics of sulfur particles depending on their localisation in the electrode.

4. Conclusions

This study has confirmed that sulfur electrodes using PDDA-TFSI polyelectrolyte as a binder performs much better than with conventional CMC or PVdF binders in terms of initial capacity and capacity retention with cycling. Even though the role of PDDA-TFSI could not be clearly pointed out, mostly because of spatial and contrast resolution limitation, this work is one of the few currently existing investigations on Li/S electrodes using synchrotron XRD and XRCT. Some phenomena were observed directly for the first time, such as the growing of part of the crystalline sulfur on the residual sulfur in parallel to the growing of new sulfur particles, and the fact that the crystalline form of sulfur appears to be directly associated with the presence of pre-existing sulfur. Indeed α -S₈ are forming on the pre-existing α -S₈ whereas the expected β -S₈ are formed elsewhere. This work also points out the importance of electrode homogeneity and flatness as differences in reactivity kinetic was noticed depending on the particle position inside the electrode, as well as an overall space-dependence of S dissolution (dissolution front) during discharge. Moreover, the absence of electrode collapsing in the sulfur-depleted zones, contrarily to what was observed with PVDF binder in literature, suggests that the present polyelectrolyte is an efficient binder to preserve the electrode architecture upon cycling. Thus, this work paves the way for further investigation on the mechanical properties of polyelectrolyte-type binders for sulfur-based electrodes through advanced operando characterization techniques, while highlighting some new phenomena as mentioned above.

Supporting Information

Evolution of the XRD patterns along the vertical axis of the cell, videos of lateral and transversal XRCT images of the PDDA electrode acquired during the 1st and 11th cycles, video of the sulfur-rich phase in 3D view during the 1st cycle, video of large S particles in 3D view during the 1st cycle.

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