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# FEEDBACK CONTROL OF COAXIAL ATOMIZATION BASED ON THE SPRAY LIQUID DISTRIBUTION

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We demonstrate a novel implementation of real-time feedback control on the structure of the spray produced by a two-fluid coaxial atomizer. The ratio of angular to longitudinal gas flow rates, called swirl ratio, as well as the total amount of gas coflow are used as the actuation at the nozzle. The swirling and swirl-free gas flow rate are individually set by the control algorithm, with the control objective set based on an optical absorbance radial profile that is related to the liquid volume fraction across the spray. We analyzed the liquid volume fraction profiles measured in open loop by means of singular value decomposition and principal component analysis (PCA) and found that the different states of the spray across a wide range of operating conditions can be described with fidelity by three principal components. The control algorithm maps the resulting state PCA projections to the control variables. Real time control of the spray is achieved over a wide range of operating conditions (gas-to-liquid momentum 1-20 and swirl ratios 0-1).

**KEY WORDS:** real-time feedback control, two-fluid coaxial atomization, multiphase flow, Principal Component Analysis

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#### 1. INTRODUCTION

droplet size and/or spatiotemporal distributions).

Liquid sprays are involved in many environmental phenomena (e. g. ocean sprays) and engineering processes (e. g. combustion fuel sprays, coating processes). The development of control strategies for sprays has been of great interest for the fuel combustion community, as is evident in numerous examples of active control for fuel combustors that have been documented in the last couple of decades (Billoud et al., 1992; Coker et al., 2006; Conrad et al., 2007; Jones et al., 1999; McManus et al., 1993; Muruganandam et al., 2005; Murugappan et al., 2003). However, as indicated in a recent review (Arai, 2019), ample opportunities remain for the development of new active control strategies for sprays (spray control is referred to here as closed-loop feedback actuation on the atomization and droplet dispersion stages to achieve a particular spray structure,

12 The response of coaxial two-fluid atomizers to a wide range of swirling and non-swirling gas co-flows has been investigated extensively (Aliseda et al., 2008; Eggers and Villermaux, 2008; Lasheras et al., 1998; Marmottant and Villermaux, 2004), providing the theoretical and exper-14 imental basis for this feedback control work. Additionally, over the last decade data reduction methods have been extensively applied for the reduced order description and control of fluid 16 flows (Blanchard and Sapsis, 2019; Grenga et al., 2018; Hervé et al., 2012; Huang et al., 2017; 17 Krolick and Owkes, 2018; Leclercq et al., 2019; Mohan and Gaitonde, 2017; Rabault et al., 18 2019; Rowley and Dawson, 2017; Schmid et al., 2011; Tallet et al., 2016). Here, we present 19 a method to perform feedback closed-loop control of a spray atomizer where the control input 20 consists of measurements of light attenuation across the depth of the spray at 10 gas diameters 21 downstream of the nozzle and where the control actuation is on the swirl and no-swirl gas flow rates (defined over ranges that span the desired momentum ratios and swirl ratios of interest). 23 The goal of this technical note is to demonstrate, for the first time, feasibility of real-time spray 24 control in a two-fluid atomizer, using a three-parameter Principal Component Analysis (PCA) 25 description of the state of the spray from fast measurements and a two-input control algorithm.

#### 1 2. SPRAY TRANSVERSE PROFILE ATTENUATION MEASUREMENTS

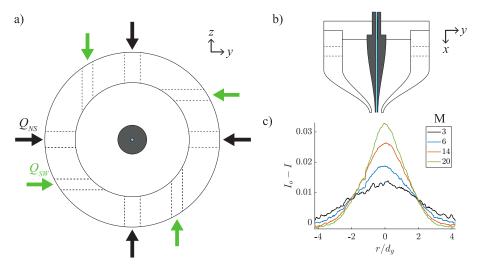
#### 2 2.1 Atomizer and flow loop

- 3 An open-source two-fluid coaxial atomizer \* designed to study atomization physics in a canon-
- 4 ical setting (Machicoane et al., 2018) is used in this experimental implementation of real-time
- 5 feedback control of a spray. The design produces reproducible laminar liquid and turbulent gas
- 6 streams that have been characterized extensively (Machicoane et al., 2019). The liquid is in-
- 7 jected through a straight circular duct and the condition of the liquid going into the atomization
- 8 is fully-developed laminar Poiseuille flow. The gas enters the nozzle through eight inlets per-
- 9 pendicular to the axis, four without angular momentum and four with with a tunable amount of
- 10 angular momentum in the gas co-flow, referred to as the swirl ratio. The gas flow develops along
- 11 the nozzle axis whose inner (the outer wall of the liquid duct) and outer surfaces are shaped with
- 12 cubic splines to provide a smooth acceleration that ensures a gas velocity profile close to a top
- hat at the nozzle exit, with no flow detachment along its inner walls.
- Two electro-valves control the gas flow rates for the no-swirl and swirl inlets independently
- 15 (each line is then split into 4 ducts into the nozzle) and an additional electro-valve controls the
- 16 liquid flow rate. Two views of the nozzle (drawings of side and plan views cut transversely along
- the nozzle axis and the gas inlet plane) are shown in figure 1.
- The relevant non-dimensional groups that we use to characterize this multiphase flow are:
- 19 the swirl ratio  $SR=Q_{ns}/Q_{sw}$ , which compares the swirl gas flow rate,  $Q_{sw}$ , to the no-swirl
- 20 gas flow rate,  $Q_{ns}$ , and the momentum ratio  $M=
  ho_g U_g^2/
  ho_l U l^2$  that is based on the gas and
- liquid average velocity and density,  $U_i = Q_i/A_i$  and  $\rho_i$ , where the subscripts g and l are used
- for gas an liquid respectively, and  $A_i$  is the fluid area.

# 23 2.2 Light attenuation measurements and analysis

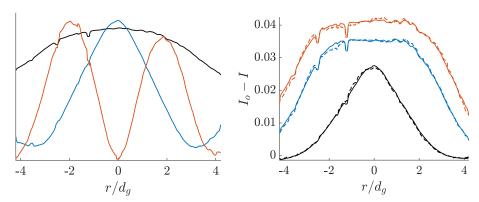
- Light attenuation through line propagation across the spray is measured by a linear CCD camera
- 25 (Thorlabs model LC100) with a red LED panel providing a uniform source of illumination, in

<sup>\*</sup>The atomizer design is made available to the community at http://depts.washington.edu/fluidlab/nozzle.shtml



**FIG. 1:** (a) Transverse cut of the nozzle along the gas inlets plane showing the liquid channel in the middle and the eight inlets for gas. (b) Cross section of the nozzle along the liquid channel axis. (c) Representative samples for the absorbance profiles, in arbitrary units, at different momentum ratios in the absence of swirl.

- a configuration analogous to shadowgraphy. Representative spray transverse profiles of light at-
- 2 tenuation, associated with liquid volume fraction, are shown in figure 1. Despite the low optical
- 3 density of the spray in the mid-field, the attenuation across the spray cross-section is of the order
- 4 of a few percent, which is well within the line camera 12-bit resolution and above the measure-
- 5 ment noise, which was characterized before data collection as 0.04 percent of the unattenuated
- 6 signal.
- We study swirl ratios in the range 0 to 1 and momentum ratios in the range 2 to 20. Data
- 8 shown here spans this range adjusting the control inputs (no-swirl and swirl volume flow rates,
- 9  $Q_{ns}$  and  $Q_{sw}$ , respectively) within these limits. Light attenuation profiles, used as a surrogate
- 10 of the spray liquid volume fraction, were collected in open loop sequence. Said profiles were
- analyzed using principal component analysis. PCA revealed that the three main modes serve as
- 12 a good basis to represent most of the energy in the observed shapes, as shown in figure 2.
- The principal components identified as a basis to represent the light attenuation are normal-
- 14 ized to form an orthonormal basis onto which to project the instantaneously measured profiles.
- 15 As a result, the spray state that is the goal of the control algorithm, can be described as a spatial
- profile using only three parameters. A two by three transfer function relates the 3 values that



**FIG. 2:** (Left) First Three Principal Components in arbitrary units. (Right) Observed profiles (dashed lines) and principal component reconstructions (solid lines), for M=13.6 and SR=0.2,0.5,0.8 from bottom to top.

- define the control goal to the 2 control variables. Given the projections onto the basis vectors, a
- 2 least-squares fit for the flow parameters produces a linear function of the projection parameters.
- 3 Details of the this process are given in appendix A.

#### 4 3. REAL-TIME FEEDBACK CONTROL IMPLEMENTATION

#### 5 3.1 Control Algorithm and Performance

- 6 The real-time control is performed by setting a goal profile in terms of its principal compo-
- 7 nent representation (any three values of the PCA basis, not a preset of values tested a-priori).
- 8 The control algorithm minimizes the root mean square error (RMSE) of the profile measured
- 9 instantaneously relative to the goal profile. This is achieved in two steps. First, an initial guess
- based on the least squares fit indicates the goal for the swirl and no-swirl components of the
- 11 gas flow. Second, the magnitude of the change in both controls is adjusted by the magnitude of
- 12 the root mean square error. A proportional-integral-derivative controller (native Labview imple-
- mentation) is used to control the proportional valves based on the flow meters and the computed
- 14 set-point for the flow rates. This process is iterated to attain a tolerance in the cost function (dif-
- 15 ference between goal and actual light attenuation profiles). A schematic of the control algorithm
- is presented in figure 3.

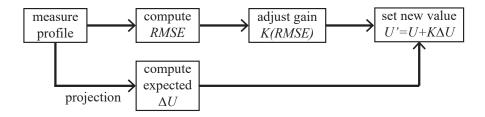
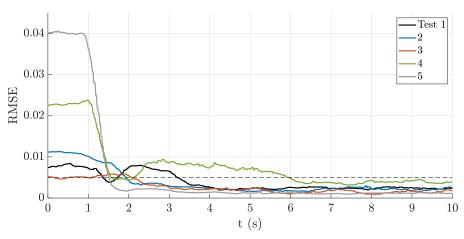


FIG. 3: Control diagram for our proposed method.



**FIG. 4:** Root mean square errors along time, between the goal profile and the instantaneous profile for five cases corresponding to videos in supplementary material.

- The control algorithm is tested on a variety of random conditions (see videos in supple-
- 2 mentary materials), showing quick and robust convergence to each of the random goal profiles
- 3 (figure 4). The proportional valves used for both gas inputs have response times of the order of
- a fraction of a second, and this sets the characteristic time required for the system to stabilize.
- 5 Interestingly, in some cases the convergence is non-monotonic as both control parameters are
- 6 varied. The RMSE increases as the control changes both inputs semi-independently, and then
- 7 drastically diminish as one control parameter reaches its optimum value, with the control al-
- 8 gorithm then refining convergence by fine-tuning the other input in small increments. This can
- 9 cause large changes of the spray features, which explain why the RMSE can increase before
- 10 decreasing to below tolerance.

## 1 4. CONCLUSIONS

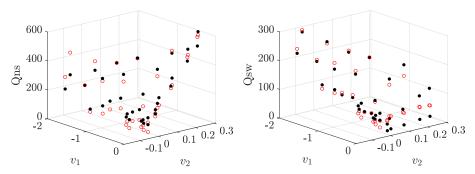
- 2 We achieved real-time feedback control of a high momentum spray based on a low dimensional
- 3 representation of spray light attenuation that can be measured as a surrogate of liquid volume
- 4 fraction and processed in real-time. To the best of our knowledge, this is the first instance of the
- 5 implementation of such control in the literature. The control algorithm showed robust perfor-
- 6 mance and response times well-matched to the available actuation in this high-momentum spray
- 7 (in the order of fractions of a second). It is possible to rigorously correlate the light attenua-
- 8 tion profile to physically meaningful characteristics of the spray, such as liquid volume fraction,
- 9 opening the opportunity to use the proposed control strategy to maintain certain spray quality for
- 10 a variety of applications where quantitative goals (not random profiles) are well-defined. Future
- 11 work will focus on these aspects, as well as on implementing multiphysics control actuation,
- such as electrohydrodynamic effects and acoustic forcing.

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- 16 views and conclusions contained herein are those of the authors only and should not be inter-
- 17 preted as representing those of ONR, the U.S. Navy or the U.S. Government.

#### 18 APPENDIX A. LINEAT LEAST SQUARES FIT OF CONTROL PARAMETERS

- We varied the values of the control parameters  $Q_{ns}$  and  $Q_{sw}$  so as to uniformly sample the mo-
- 20 mentum and swirl ratios of interest (as the spray physics are dominated by these nondimensional
- groups). The evolution of the principal component coefficients  $v_i$  with  $Q_{sw}$  and  $Q_{ns}$  is roughly
- 22 linear. Each control parameter can be varied independently of the other which justifies the use of
- 23 a linear fit (e.g.  $v_i \approx a + bQ_{ns} + cQ_{sw}$ ).
- 24 Figure A.5 shows the observed and predicted values of the swirling and non-swirling com-
- 25 ponents of the gas flow rate based on a linear least squares fit to the principal component rep-
- 26 resentation of the corresponding profiles. It can be observed that the fit reproduces the overall



**FIG. A.5:** Observed (black dots) and predicted (red circles) values of the no-swirl (Left) and swirl (Right) gas flow rates.

trends reasonably well  $(R^2 \approx 0.9)$  and that it fails mostly for low values of the gas flow rate.

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