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# Experimental study on ammonia/hydrogen/air combustion in spark ignition engine conditions

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## Abstract

The mitigation of climate change implies the increasing use of variable renewable energy sources. Energy storage and transport solutions will contribute to ensure the stability, reliability and flexibility of the energy systems in that context. Ammonia is a well-known chemical of formula  $\text{NH}_3$  and, amongst other electrofuels, a promising energy carrier and carbon-free combustible fuel. In the present experimental study, engine performance, combustion characteristics and pollutant emissions of a recent spark ignition engine fueled with premixed ammonia/hydrogen/air mixtures were assessed. Gaseous ammonia blends in a wide range of hydrogen fuel fractions and equivalence ratios were tested at two different engine loads. Results show performances comparable with conventional fuel operation when the appropriate promotion strategies are used. Specifically, blending up to 20% hydrogen in the fuel by volume improves the cyclic stability and avoids misfires, while granting the best work output and indicated efficiencies near stoichiometry. Higher hydrogen fractions result in depleted efficiency, attributed to higher wall heat losses. The combustion duration is directly correlated to the LBV of the mixtures, thus being accelerated by hydrogen blending. The accelerating effect of hydrogen is particularly remarkable during the initial stage of the combustion. Hydrogen appears therefore mainly as an ignition promoter. Increasing the engine load improves the furnished work and allows to extend the operating boundaries in terms of mixture composition.

## Keywords

Ammonia ; Hydrogen ; Spark ignition engine ; Sustainable fuel ; Performance ; Emissions

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## 1. Introduction

Ammonia (NH<sub>3</sub>) is increasingly considered as a prominent enabler of the ongoing transition towards high shares of Variable Renewable Energy Sources (VRES) in the energy systems, as stated in *The Future of Hydrogen*, a recent report by the International Energy Agency [1]. Indeed, VRES should account for more than 50% of the total primary energy supply by 2050 to comply with the global warming mitigation objectives of the Paris Agreement, according to the Intergovernmental Panel on Climate Change [2]. In this new energy paradigm, energy storage and transport solutions will contribute to the efficiency and sustainability of the energy systems.

Ammonia, along with other electrofuels, i.e. energy-dense chemicals producible from electricity, water and any other renewable feedstock, appears as such a renewable and carbon-free energy carrier. It exhibits a high hydrogen content of 17.8% by mass, a volumetric energy density of 11.3 GJ/m<sup>3</sup> when stored in liquid form at 1.1 MPa and 300 K, and is as such an efficient hydrogen carrier.

In order to avoid costly ammonia-to-hydrogen conversions and depending on the final energy use, direct ammonia combustion can be considered. Related research efforts have been summarized recently by Valera-Medina et al. [3]. Those mainly focus on overcoming the unfavorable combustion properties of NH<sub>3</sub>, illustrated in Table 1 by its low Laminar Burning Velocity (LBV), high auto-ignition temperature and narrow flammability range, as well as addressing the challenge of nitrogen-based pollutant emissions. To that aim, several practical combustion technologies were investigated, including gas turbines [4,5], compression-ignition engines, mostly in dual fuel configurations [6-16] and Spark Ignition (SI) engines [17-34].

**Table 1.** Ammonia properties and comparison with other fuels at 300 K and 0.1 MPa. Data from [3,23,35]

	Ammonia	Methanol	Hydrogen	Methane	Gasoline
Formula	NH <sub>3</sub>	CH <sub>3</sub> OH	H <sub>2</sub>	CH <sub>4</sub>	-
Storage	Liquid	Liquid	Compressed	Compressed	Liquid
Storage temperature (K)	300	300	300	300	300
Storage pressure (MPa)	1.1	0.1	70	25	0.1

Density under storage conditions (kg.m <sup>-3</sup> )	600	785	39	187	~740
Lower Heating Value (LHV) (MJ.kg <sup>-1</sup> )	18.8	19.9	120	50	44.5
Volumetric energy density (GJ.m <sup>-3</sup> )	11.3	15.6	4.7	9.35	33
Stoich. air-fuel ratio by mass	6.05	6.44	34.6	17.3	15
LBV @ $\phi = 1$ (m.s <sup>-1</sup> )	0.07	0.36	3.51	0.38	0.58
Auto-ignition temp. (K)	930	712	773-850	859	503
Research Octane Number	130	119	>100	120	90-98
Flammability limits in air (vol.%)	15-28	6.7-36	4.7-75	5-15	0.6-8

46

47 The flexibility of the internal combustion engine makes it appealing for NH<sub>3</sub> fuel use, especially when assist-  
48 ing the ignition with a spark. SI engines can be run on ammonia blends at high compression ratio (CR) without  
49 risk of engine knock thanks to the high octane number of ammonia. This was demonstrated in early studies,  
50 where single-cylinder and multi-cylinder SI engine were successfully run on pure ammonia fuel [17–19].  
51 However, gasoline-like performances were only achieved by using one or several promoting strategies, in-  
52 cluding an improved ignition system, increasing the engine load or CR and H<sub>2</sub> doping of the NH<sub>3</sub> fuel. A  
53 minimum H<sub>2</sub> amount depending on the engine speed and CR of some percent by mass was necessary to ensure  
54 satisfying performance and decrease NH<sub>3</sub> emissions but at the cost of increased NO<sub>x</sub> emissions.

55 Contemporary studies also investigated ammonia/gasoline fueling of SI engine, either to reduce carbon-based  
56 emissions of gasoline engines, or to promote the combustion with ammonia as a main fuel. Granell et al.  
57 proposed a 70% NH<sub>3</sub> / 30% gasoline blend by energy as a good trade-off at full load in a Collaborative Fuel  
58 Research (CFR) engine [21,22]. The authors suggested supercharging the engine instead of increasing the CR,  
59 due to the detrimental thermodynamic consequences of the early spark advance required by the NH<sub>3</sub> fuel.  
60 Engine-out NH<sub>3</sub> emissions proportional to the NH<sub>3</sub> input are reported, up to 22000 ppmvw for stoichiometric

61 NH<sub>3</sub>/air at CR=10:1. Ryu et al. investigated direct gaseous NH<sub>3</sub> injection in a CFR engine (CR = 10:1) with  
62 gasoline as the base fuel, and reported acceptable performance but high nitrogen-based specific emissions  
63 [36]. The same authors suggested to partly dissociate NH<sub>3</sub> prior to direct injection, to use the beneficial effect  
64 of H<sub>2</sub> on the combustion efficiency, and reduce the pollutant emissions [32].

65 That capability of molecular hydrogen of being producible in-situ through ammonia dissociation, possibly by  
66 recycling exhaust heat and requiring no additional tank, grants it a potential advantage over other combustion-  
67 promoting fuels. Therefore, further researchers investigated the use of hydrogen-enriched ammonia in SI en-  
68 gines. Koike et al. studied a single-cylinder SI engine (CR = 14:1) fueled with premixed stoichiometric  
69 NH<sub>3</sub>/H<sub>2</sub>/air and NH<sub>3</sub>/gasoline/air mixtures [29]. Stable operation was achieved for 10 – 60 LHV% of H<sub>2</sub> (12.6  
70 – 66.1 mol.%) or 40 – 100 LHV% gasoline (8 – 100 mol.%) fuel fractions for light load (Indicated Mean  
71 Effective Pressure, *IMEP* = 0.2 MPa), and up to 100 % NH<sub>3</sub> for high load (*IMEP* = 0.8 MPa). An auto-thermal  
72 cracker was successfully operated to provide H<sub>2</sub> from NH<sub>3</sub> dissociation. Similarly, Frigo and Gentili studied  
73 a twin-cylinder commercial SI engine fueled with premixed stoichiometric NH<sub>3</sub>/H<sub>2</sub>/air mixtures at half and  
74 full load and several engine speeds [27]. They found a minimum hydrogen-to-ammonia energy ratio of 7% at  
75 full load and 11% at half load to ensure stable engine operation, but with decremented performance with  
76 respect to gasoline operation. Maximum NO<sub>x</sub> emissions of 1700 ppm and surprisingly low NH<sub>3</sub> emissions are  
77 reported, although the latter have only been detected through a threshold sensor. Comotti and Frigo extended  
78 the previous study by demonstrating the successful use of a catalytic cracking reactor for in-situ H<sub>2</sub> production  
79 [24]. Mørch et al. fueled a CFR engine with NH<sub>3</sub>/H<sub>2</sub> blends at various CR, with a metal ammine complex as  
80 NH<sub>3</sub> reservoir [23]. They showed increased engine performance and similar NO<sub>x</sub> emissions with respect to  
81 gasoline operation, thanks to the possibility of knock-free CR increase. Best performance is found at stoichi-  
82 ometry for 10 mol.% H<sub>2</sub> in the fuel. Selective Catalytic Reduction is suggested as a meaningful way to mitigate  
83 NO<sub>x</sub> emissions, thanks to appropriate exhaust temperatures and NH<sub>3</sub> availability, with the major challenge of  
84 avoiding NH<sub>3</sub> slip at the exhaust. Westlye et al. focused on nitrogen-based pollutant emissions of a CFR engine  
85 fueled with 80 mol.% NH<sub>3</sub> / 20 mol.% H<sub>2</sub> lean blends, and further demonstrated the feasibility of SCR for  
86 pollutants mitigation [30].

Therefore, the suitability of ammonia as an efficient carbon-free SI engine fuel has been demonstrated in the literature, and the relevance of H<sub>2</sub> as a combustion promoter has been underlined. However, most of the experimental data were obtained in outdated or basic engine geometries and covered only a partial range of mixture compositions. The objective of the present work is thus to actualize and extend the experimental database for NH<sub>3</sub>/H<sub>2</sub>/air combustion in a SI engine, so as to conduct further analysis that should provide useful understanding on ammonia combustion properties. To that end, one cylinder of a recent commercial SI engine was fueled with premixed gaseous NH<sub>3</sub>/H<sub>2</sub>/air mixtures for a wide range of mixture compositions at and beyond full load. Measurements for part-load operation close to stoichiometry were published elsewhere [33,34]. The experimental set-up and the operating conditions are first introduced. Extensive data derived from in-cylinder pressure and exhaust gas measurements are then presented, analyzed and discussed.

## 2. Experimental and numerical methods

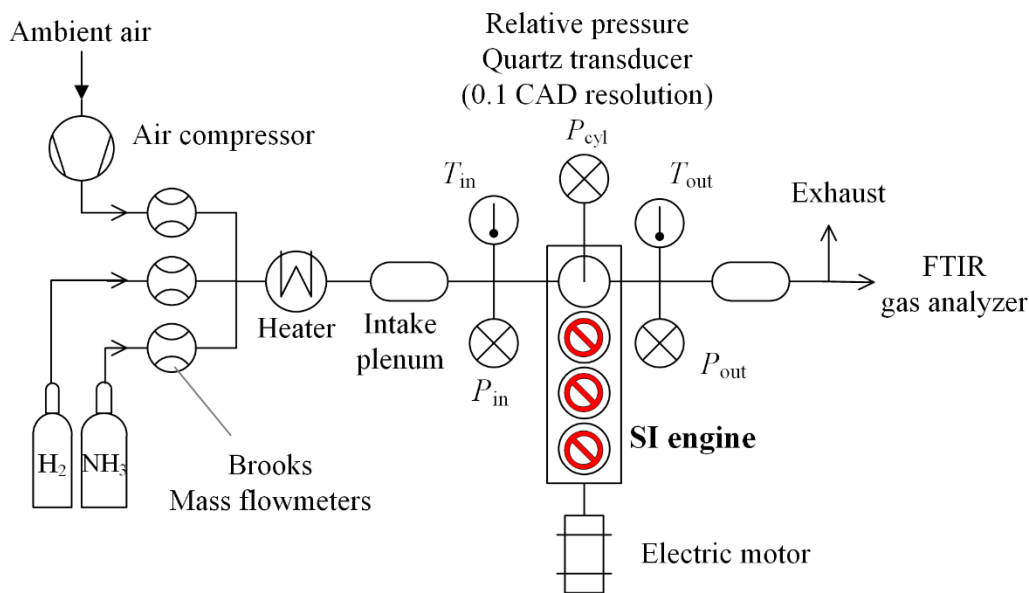
### 2.1. Engine setup

The engine used for the experiments is a recent four-cylinder four-stroke SI engine, retrofitted to a single-cylinder by fueling only one cylinder. The engine specifications are shown in Table 2. This engine benefits from improved aerodynamics, thanks to its piston bowl optimized for gasoline direct injection, granting it a tumble ratio of about 2.4 [37].

**Table 2.** Engine specifications

Model	PSA EP6DT
Stroke	85.8 mm
Bore	77 mm
Connecting rod length	138.5 mm
Displacement volume	399.5 cm <sup>3</sup>
Geometric compression ratio	10.5:1
Valves	4
Engine speed	1500 rpm

106 A constant engine speed of 1500 rpm is imposed to the engine by an electric motor. A Kübler optical encoder  
 107 monitors the angular position of the main shaft with a 0.1 Crank Angle Degree (CAD) resolution. Type K  
 108 thermocouples and piezo-resistive pressure transducers are used to monitor the intake and exhaust temperature  
 109 and pressure, respectively. The temperature of the cooling fluid is set and monitored at 353 K. The flows of  
 110 the reactive gases, including dried ambient compressed air, bottled ammonia and bottled hydrogen are moni-  
 111 tored by means of Brooks thermal mass flowmeters with 0.7% accuracy on their full scale, preheated to the  
 112 intake temperature of 323 K and premixed in an intake plenum prior to injection. The original spark plug is  
 113 used with a coil charging time of 2 ms. A water-cooled AVL piezoelectric pressure transducer measures the  
 114 in-cylinder pressure with a 0.1 CAD resolution and a measuring range of 0 – 25 MPa. The absolute in-cylinder  
 115 pressure is obtained by equalizing the previous signal with the mean absolute intake pressure,  $P_{in}$ , 20 CAD  
 116 after inlet valve opening (pressure pegging). The exhaust gas composition is monitored by means of a Gasett  
 117 Fourier-Transform InfraRed (FTIR) gas analyser. The wet exhaust concentrations of  $H_2O$ ,  $NH_3$ ,  $NO$ ,  $NO_2$  and  
 118  $N_2O$  were measured simultaneously for each test with a time step of 5 s. Figure 1 shows a scheme of the  
 119 experimental setup.

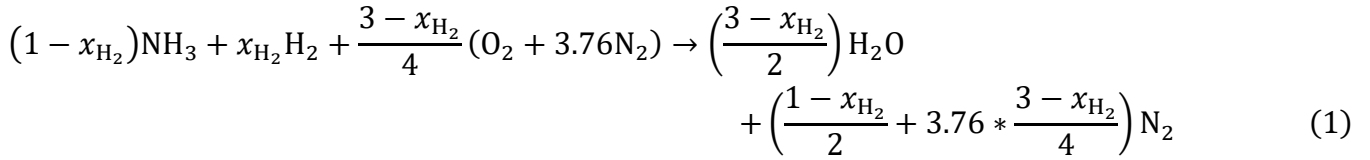


120  
 121 **Figure 1.** Scheme of the experimental setup

122 **2.2. Operating conditions**

123 The global stoichiometric reaction of  $NH_3/H_2$ /air combustion is as:

124



with  $x_{H_2}$ , the hydrogen molar fraction in the fuel mixture. Non-stoichiometric mixtures are defined by the equivalence ratio,  $\phi$ :

$$\phi = \frac{\frac{X_{H_2} + X_{NH_3}}{X_{air}}}{\left(\frac{X_{H_2} + X_{NH_3}}{X_{air}}\right)_{st}} \quad (2).$$

$X_s$  represents the molar fraction of the species  $s$  in the reactive mixture, and subscript “st” stands for stoichiometric. The stoichiometric air/fuel ratio by mass is about 6 for pure  $NH_3$  fuel and thus more than twice smaller than for gasoline, as shown in Table 1, but increases slightly with hydrogen enrichment. The investigated operating conditions are summarized in Table 3, and are intended to cover a broad range of mixture compositions representative of possible ammonia/hydrogen operating modes of SI engines at and beyond full load. In order to make optimal performance considerations, the spark ignition timing (SIT) is set to maximize the net Indicated Mean Effective Pressure ( $IMEP_n$ ), a quantification of the net work furnished by the expanding gas on the piston. This is equivalent to the Maximum Brake Torque (MBT) timing, but the absence of direct torque measurement due to the friction losses caused by the three unproductive pistons led to the previous approach. Cycle-to-cycle variability is considered by recording 100 consecutive pressure cycles for each test. Averaged values over 100 cycles are presented in this paper.

**Table 3.** Overview of the operating conditions.

Intake temperature (K)	Intake pressure (MPa)	H <sub>2</sub> fraction in the fuel		$\phi$
323	0.1, 0.12	By volume	[0 – 0.6]	[0.6 – 1.2]
		By energy (LHV)	[0 – 0.54]	
		By mass	[0 – 0.15]	

### 2.3. Combustion analysis and laminar burning velocity calculation



146 A precise determination of the CR and detection of the Top Dead Center (TDC) position is required for an  
147 accurate analysis based on the in-cylinder pressure signal and calculated in-cylinder volume. Therefore, the  
148 methodology proposed by Tazerout et al. [25-26] for CR determination and pressure-volume lag elimination  
149 is implemented within the classical analysis of the cylinder pressure-volume data proposed by Heywood [40].  
150 Crevice effects are neglected and no in-cylinder mass variation are considered between Inlet Valve Closing  
151 (IVC) and Exhaust Valve Opening (EVO). Performance indicators such as the  $IMEP_n$  and its coefficient of  
152 variation over 100 cycles  $COV_{IMEP}$  can be deduced accurately, as well as the bulk in-cylinder temperature  
153 between IVC and EVO. The latter is determined by means of the ideal gas law, assuming the gas temperature  
154 to be equal to the inlet temperature  $T_{in} = 323$  K at IVC. The combustion analysis is also performed by calcu-  
155 lating the net heat release rate (HRR) by means of the first law of thermodynamics in a one-zone model. The  
156 in-cylinder heat capacity at constant pressure is calculated using the bulk in-cylinder temperature and an in-  
157 cylinder charge composition modeled by a representative mixture of burned and unburned gases weighted by  
158 the burned mass fraction (that can be determined iteratively), assuming complete combustion. The gross HRR  
159 from the combustion is estimated by considering the wall heat losses by means of the model of Hohenberg  
160 [41]. Combustion phasing in the cycle is established by assessing the crank angles at which 10%, 50% and  
161 90% of the cumulated gross heat release is reached, yielding CA10, CA50 and CA90, respectively.

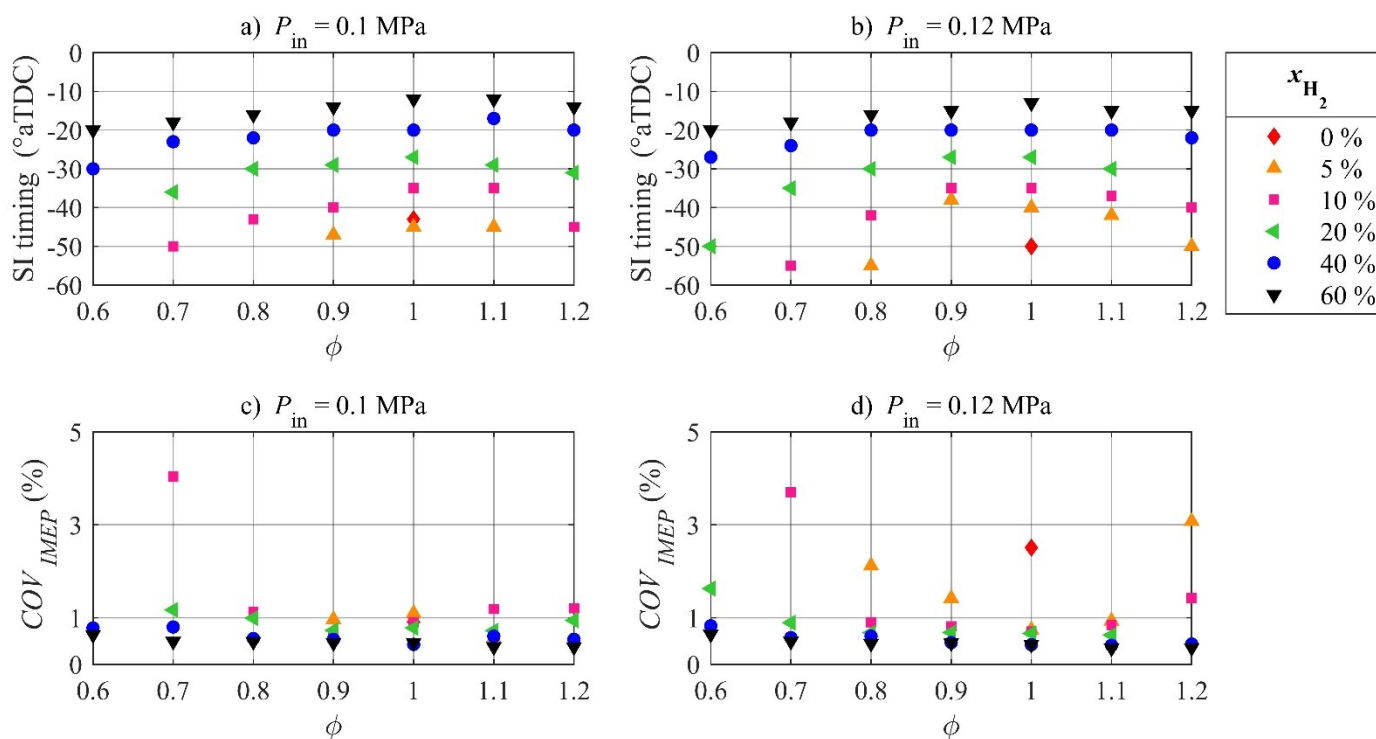
162 The laminar burning velocity of the reactive mixtures under the thermodynamic conditions at SI timing is  
163 calculated by means of a newly developed LBV correlation for  $NH_3/H_2$ /air flames proposed by Goldmann and  
164 Dinkelacker [42] on the basis of the detailed reaction mechanism of Mathieu and Petersen [43]. This correla-  
165 tion takes the presence of hydrogen in the fuel into account and was validated against measurements at normal  
166 temperature and up to 500 kPa of pressure for various mixture compositions.

### 168 3. Results and discussion

#### 169 3.1. Engine performance

170 The engine was operated successfully with an excellent cycle-to-cycle stability for a wide range of  $H_2$  fractions  
171 and equivalence ratios, when the spark ignition was sufficiently advanced, as shown in Figure 2a and 2b. An  
172 acceptable cyclic variability boundary was set at  $COV_{IMEP} \leq 5\%$  (coefficient of variation of the  $IMEP_n$ ), but  
173 most of the conditions verified  $COV_{IMEP} \leq 3\%$ , as shown in Figure 2c and 2d. It should be emphasized here

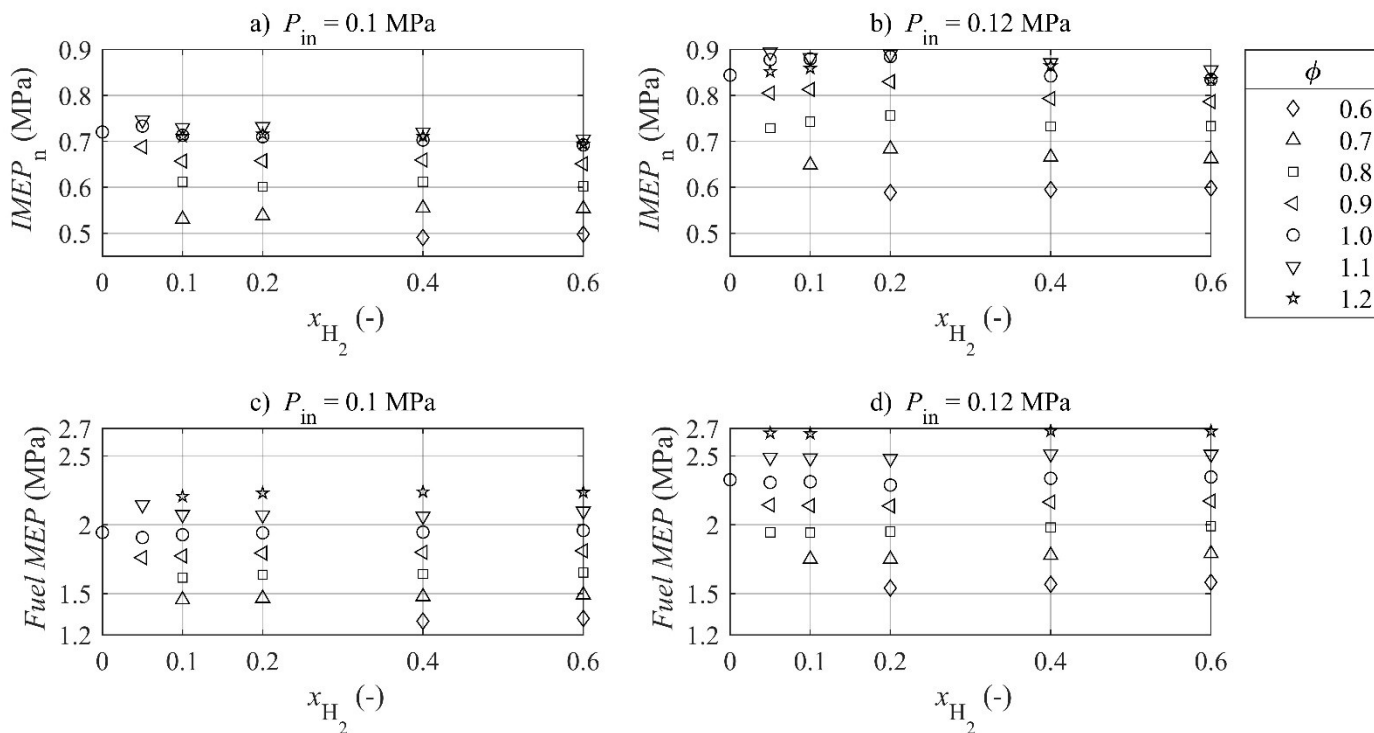
174 that stable operation could be achieved for a stoichiometric  $\text{NH}_3/\text{air}$  mixture for both intake pressures. Only  
 175 mixtures with high hydrogen fraction were found suitable for very lean operation. When increasing the  $\text{NH}_3$   
 176 content in the fuel, advancing the SI timing is unsurprisingly required to maintain the cyclic stability and reach  
 177 the maximum power output, as shown in Fig. 2a and 2b. This is primarily attributed to the low LBV of  $\text{NH}_3$   
 178 that slows down the early stages of the flame propagation, and explains the bell-shaped dependence of the SI  
 179 timing to the equivalence ratio. For a given fuel blend, the SI timing closest to TDC is obtained near stoichi-  
 180 ometry, corresponding to the region of maximum LBV.



181  
182 **Figure 2.** Optimized Spark Ignition Timing and Coefficient of Variation of the  $IMEP_n$ .

183 Figure 3 shows the  $IMEP_n$  as a quantification of the piston work, along with a “Fuel Mean Effective Pressure”  
 184 ( $FuelMEP$ ) for the ratio between the cyclic energy input on a LHV basis and the displaced volume. The  
 185  $FuelMEP$  is an increasing function of the intake pressure and the equivalence ratio, but volumetric hydrogen  
 186 enrichment of the fuel at given  $\phi$  does not modify the energy content of the fuel/air mixture, as the lower  
 187 volumetric energy density of  $\text{H}_2$  happens to be compensated by its lower stoichiometric air-fuel ratio, as shown  
 188 in Fig. 3c and 3d. As a result, the  $IMEP_n$  increases as the equivalence ratio is increased up to 1.1, as shown in  
 189 Fig. 3a and b. In spite of excess fuel presence when  $\phi = 1.1$ , the extra work obtained at this equivalence ratio  
 190 may be explained by the maximum LBV reached close to that value as compared to stoichiometry [42], al-  
 191 lowing to operate closer to an ideal thermodynamic cycle. Further increase of the equivalence ratio only results

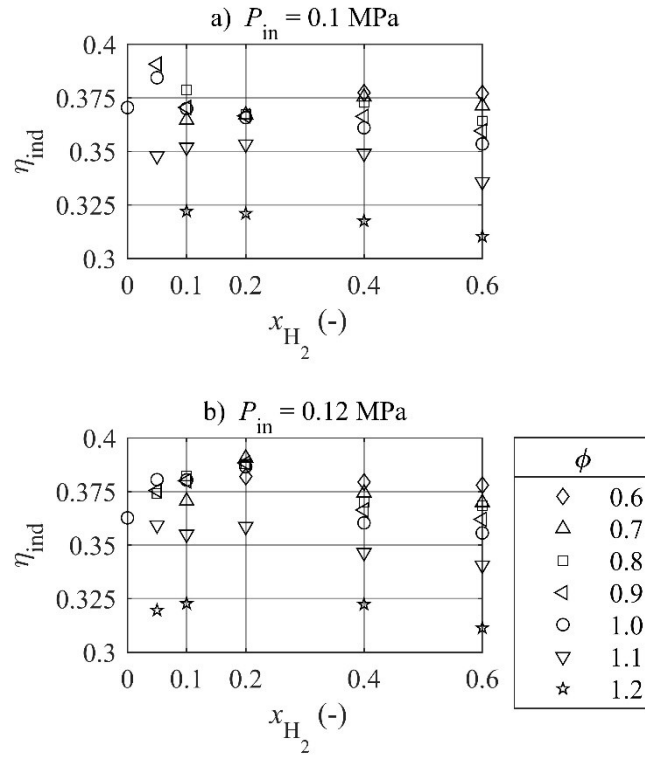
192 in more excess fuel with no LBV benefit, thus explaining the stagnation or decrease of the  $IMEP_n$  when  $\phi =$   
 193 1.2. In spite of nearly identical  $Fuel\ MEP$ , mixtures with low to moderate hydrogen fractions exhibit higher  
 194 maximum  $IMEP_n$  than highly enriched mixtures, consistently with the observations in [23]. Unsurprisingly,  
 195 increasing the intake pressure allows to increase the power output up to values typical of full-load conventional  
 196 fuel operation of the engine.



197

198 **Figure 3.** Net Indicated Mean Effective Pressure and Fuel Mean Effective Pressure.

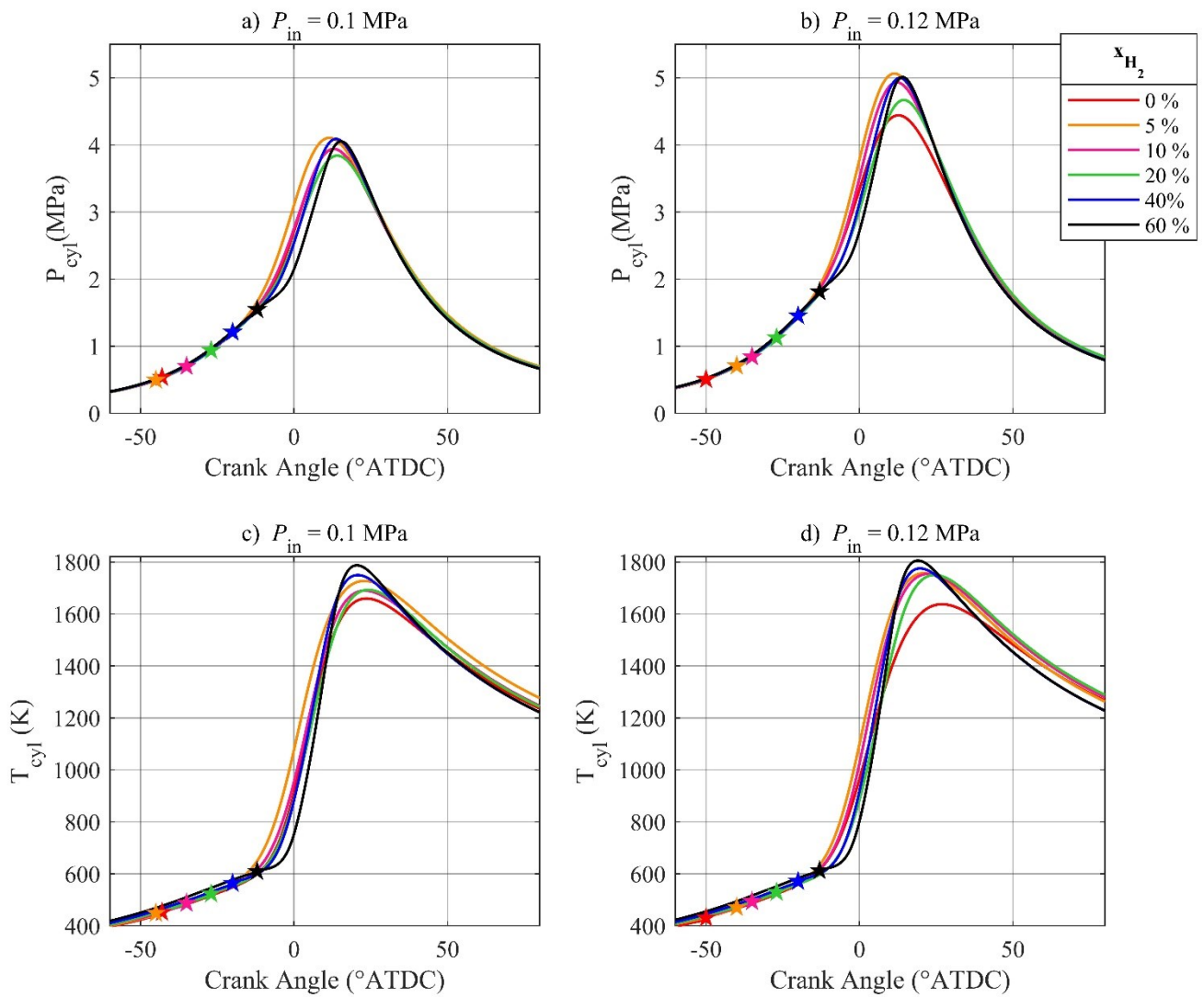
199 The ratio of the  $IMEP_n$  and the  $Fuel\ MEP$  yields the indicated efficiency and is shown in Figure 4. It is opti-  
 200 mal for slightly hydrogen-enriched near-stoichiometric lean mixtures with highest values close to 39%. The  
 201 dependence on the intake pressure is not fully consistent but tends to indicate a slight improvement of the  
 202 indicated efficiency as the load is increased. Highly hydrogen-enriched near-stoichiometric mixtures experi-  
 203 ence a depleted indicated efficiency, assumedly due to higher wall heat losses linked to high flame tempera-  
 204 tures, but the efficiency improves when operating towards leaner equivalence ratios while the flame temper-  
 205 atures decrease accordingly.



**Figure 4.** Indicated efficiency.

### 3.2. Combustion analysis

Figure 5 shows the in-cylinder pressure data, along with the bulk in-cylinder temperature for stoichiometric mixtures. Pentagram symbols identify the spark ignition. While the thermodynamic conditions at ignition may differ with respect to the fuel hydrogen fraction due to the optimization of the SIT, the magnitude of the in-cylinder pressure rise remains comparable especially for atmospheric intake pressure. However, the estimated bulk in-cylinder temperatures shown in Figs. 5c and 5d exhibits higher peaks for highly hydrogen-containing mixtures, thus supporting the assumption of higher wall heat losses for such mixtures near stoichiometry.



215

216

**Figure 5.** Measured in-cylinder pressure and estimated bulk in-cylinder temperature for  $\phi = 1.1$ . Symbols:

217

spark ignition.

218

Remarkably, the crank angle of occurrence of the maximum in-cylinder pressure is weakly affected by the

219

variations of the mixture composition, as shown in Figure 6. This indicates that, in spite of a wide variation

220

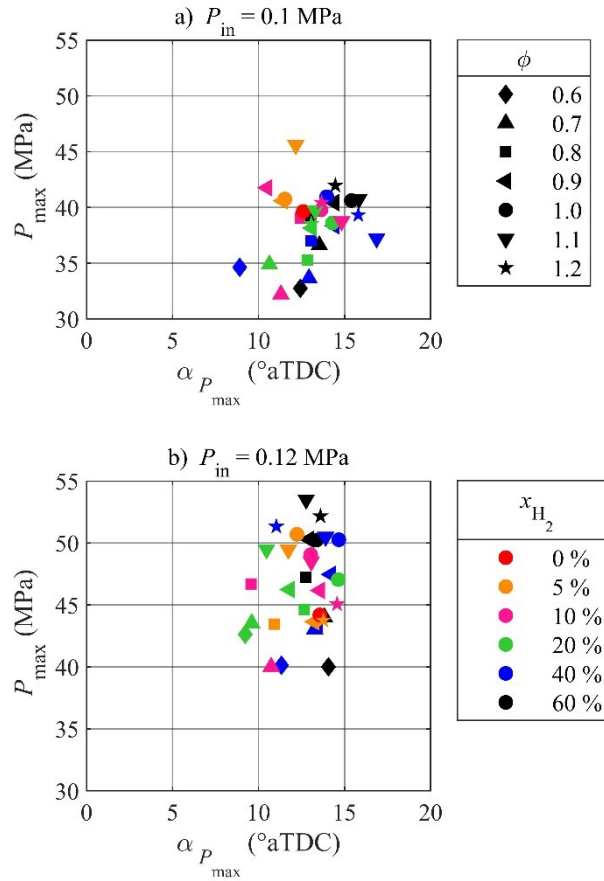
range of the spark ignition timing, the peak in-cylinder pressure is almost constantly phased in the cycle when

221

the optimum  $IMEP_n$  is reached. However, a certain data scatter remains, probably partly due to the manual

222

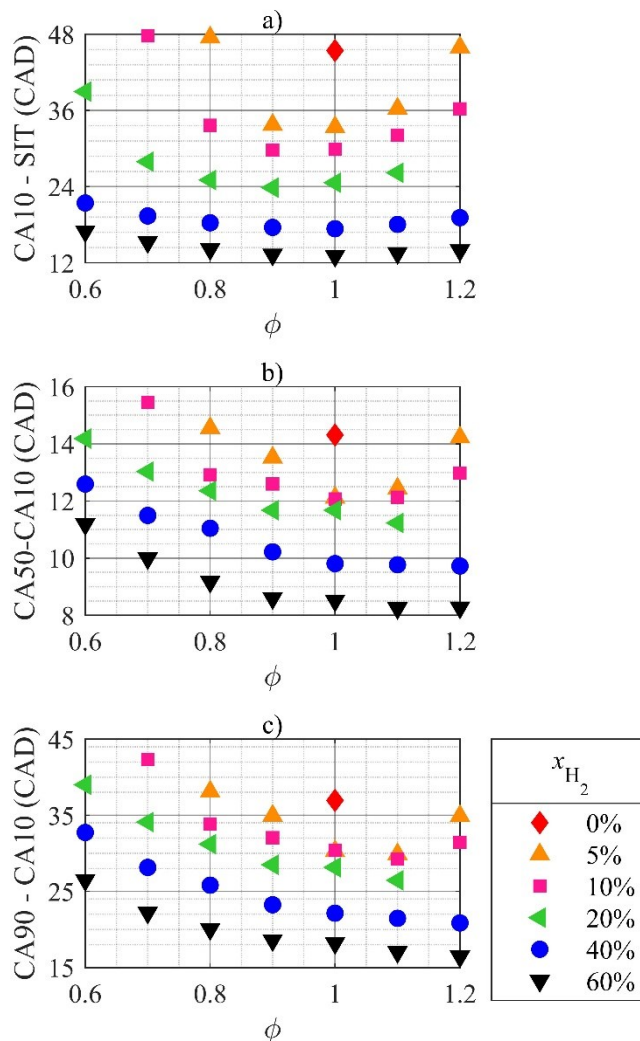
tuning of the optimized spark ignition timing.



**Figure 6.** Maximum in-cylinder pressure as a function of its crank angle of occurrence,  $\alpha_{P_{max}}$ .

Even though no other major differences are observed on the in-cylinder pressure and temperature curves for different mixtures, the composition of the mixtures does impact the heat release rate and hence the duration of the combustion phases. This is highlighted in Figure 7, where the flame initiation phase between SIT and CA10, the first flame propagation phase between CA10 and CA50 and the combustion duration between CA10 and CA90 are shown as a function of the equivalence ratio in the case  $P_{in} = 0.12$  MPa. Similar results are obtained at  $P_{in} = 0.1$  MPa and are thus not presented here. For hydrogen fuel fractions lower than 20%, the duration of the combustion phases decreases at a faster rate than the hydrogen fraction is increased. It then becomes nearly proportional to the hydrogen fuel fraction for 40% and 60%  $H_2$ . The effect of hydrogen on the initiation phase is always greater than proportional, with 34% and 62% acceleration relative to the pure  $NH_3$  case for stoichiometric mixtures with 10% and 40%  $H_2$ , respectively. This may be partly due to the more favorable thermodynamic conditions due to an ignition closer to TDC in the latter cases, but also to the increase of the turbulent flame speed due to hydrogen addition. The influence of the equivalence ratio appears mainly correlated to the LBV of the mixture, since the different phases are accelerated when increasing  $\phi$  from lean to stoichiometric and decelerated when further increasing it from stoichiometric to rich. A stagnation

239 or further acceleration of the phases as a function of  $\phi$  is observed for mixtures with high  $H_2$  content, due to  
 240 the shift of the peak LBV towards richer mixtures in those cases. This is highlighted in Figure 8, where the  
 241 different combustion phases are plotted as a function of the LBV, estimated at the thermodynamic conditions  
 242 at SIT (cf. Section 2.3).

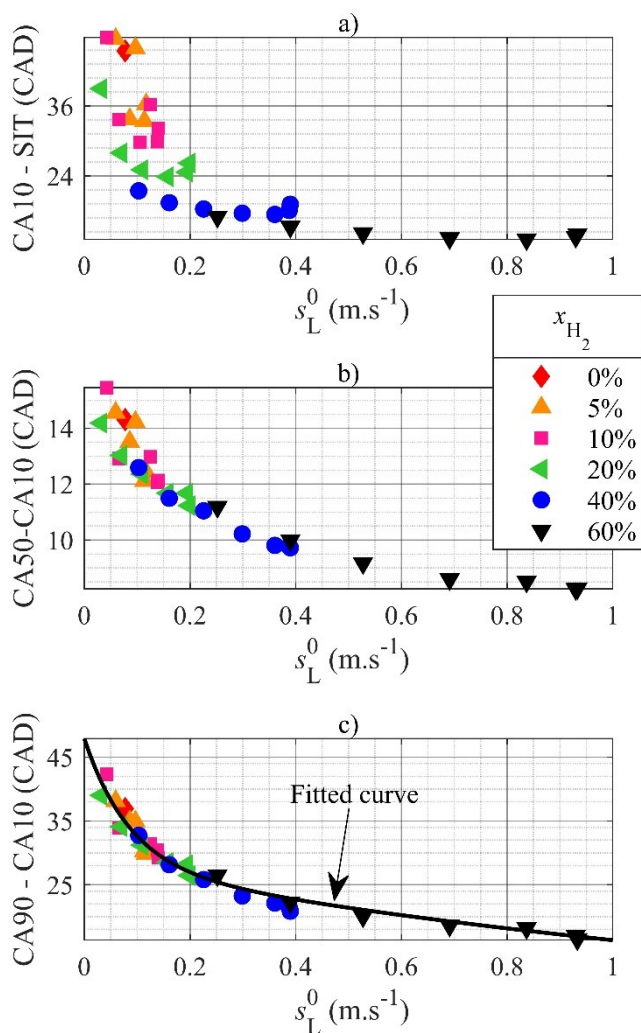


243

244 **Figure 7.** Combustion phases at  $P_{in} = 0.12$  MPa. a) Initiation phase. b) Propagation phase. c) Combustion  
 245 duration.

246 A clear non-linear correlation between the duration of the different combustion phases and the LBV of the  
 247 mixture at SIT is observed, that seem to be independent of the hydrogen fraction in the case of the propaga-  
 248 tion phase and the bulk combustion duration. The data are more scattered for the initiation phase, probably  
 249 due to different ignition behavior, as well as to the manual tuning of the SI timing. The effects of hydrogen  
 250 are believed to be critical during that phase, since it has a strong influence on the flame response to stretch  
 251 and thermal-diffusive instabilities, and thus on the turbulent flame speed that could explain the different

252 slopes in Fig. 8a. Once a quasi-steady combustion regime has been reached, around CA10, the maximal  
 253 flame stretch may be reached, thus explaining the dependence of the combustion duration on the LBV only.  
 254 The following empirical expression of the correlation between the combustion duration and  $s_L^0$  at  $P_{in} = 0.12$   
 255 MPa was determined by means of a least-square algorithm:  
 256 
$$CA90 - CA10 = 20.0037 \cdot \exp(-11.7506 \cdot s_L^0) + 27.9146 \cdot \exp(-0.5374 \cdot s_L^0) \quad (3).$$
  
 257 It appears important to notice that H<sub>2</sub>-containing mixtures with lower LBVs than stoichiometric pure NH<sub>3</sub>  
 258 were successfully operated in the engine, thus indicating that the LBV is not the only governing parameter  
 259 of NH<sub>3</sub> combustion in the engine.



260  
 261 **Figure 8.** Combustion phasing at  $P_{in} = 0.12$  MPa as a function of the calculated mixture LBV under SIT  
 262 thermodynamic conditions.

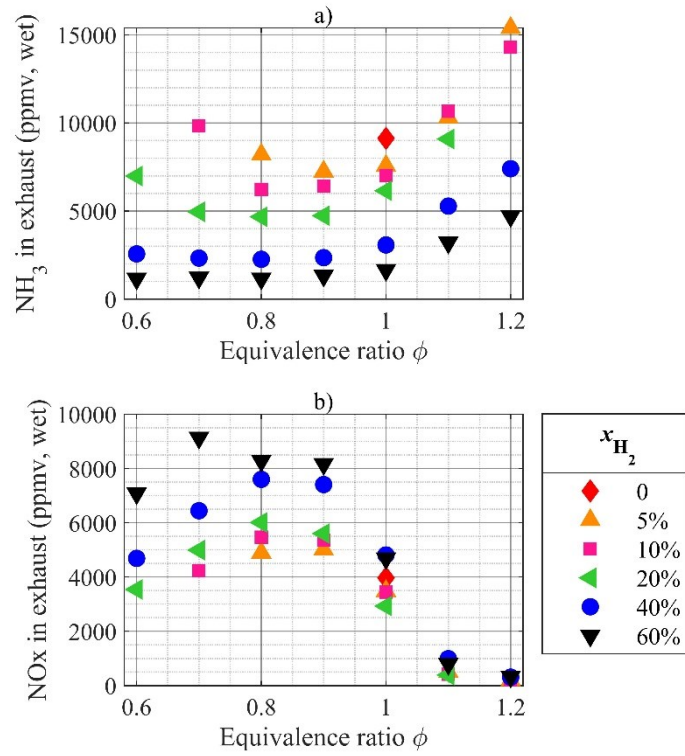
263 **3.3. Pollutant emissions**



264 In order to wrap-up this analysis, pollutant exhaust emissions are shown in Figure 9. Only the measurements  
265 for an intake pressure of  $P_{in} = 0.12$  MPa are depicted, since no qualitative difference with the other case was  
266 observed.  $NH_3$  emissions increase monotonically with the  $NH_3$  fraction in the fuel, as shown in Fig. 9a. Min-  
267 imal emissions are observed for near-stoichiometric lean conditions, tending towards leaner mixtures as  $H_2$  is  
268 added. That observation is not unexpected since it is the usual region for maximum combustion efficiency,  
269 combining the absence of excess fuel with the best reactivity properties. Increasing the hydrogen content  
270 allows to extend the range of acceptable reactivity towards leaner mixtures. When the equivalence ratio is  
271 increased above stoichiometry, the emissions increase significantly due to the presence of excess fuel and  
272 incomplete combustion, reaching very high values of more than 15,000 ppmv. Heading towards very lean  
273 mixtures, the  $NH_3$  emissions increase as well, because of poor combustion efficiency.

274  $NO_x$  emissions are shown in Fig. 9b. Minimal values are obtained for rich mixtures with high ammonia con-  
275 tent. Mixtures with high  $H_2$  fuel fractions exhibit the highest emissions, probably due to higher flame temper-  
276 atures that promote thermal  $NO_x$  formation. Maximal values are found for equivalence ratio 0.8-0.9, as could  
277 be expected due to the presence of excess oxygen. Very high values up to 9000 ppm are observed at lean  
278 conditions, while low values well below 500 ppm are seen at rich conditions, possibly after partial recombi-  
279 nation with unburned  $NH_3$  in the exhaust pipe.

280



**Figure 9.** Pollutant emissions in exhaust at  $P_{in} = 120$  kPa. a) Unburned  $\text{NH}_3$ . b) Total  $\text{NO}_x$ .

Either way, mitigation strategies for both  $\text{NH}_3$  and  $\text{NO}_x$  are required in order to make ammonia acceptable as a fuel for commercial applications. These could be achieved by means of a SCR catalyst, since both heat and  $\text{NH}_3$  reducing agent are available in the exhaust, as demonstrated by Westlye et al. [30]. The feasibility of that approach is verified in Figure 10 that shows the exhaust temperatures measured in the present study. The best operating temperature for usual catalysts are in the range 550-750 K. This could be achieved by operating the present engine in lean conditions. For instance, a mixture with 20%  $\text{H}_2$  in the fuel and  $\phi = 0.7$  exhibits exhaust temperatures in the appropriate range and also balanced  $\text{NH}_3$  and  $\text{NO}_x$  emissions, i.e.  $\text{NH}_3/\text{NO}_x \approx 1$ . Alternatively, exhaust gas recirculation could be used to reduce the exhaust temperatures, while taking advantage of the exhaust  $\text{H}_2$  concentrations that were evidenced in [33,34] for rich mixtures to promote the combustion. If intake  $\text{H}_2$  is to be produced in-situ from ammonia dissociation, the nitrogen co-product will also act as a diluent and thus help reducing the temperatures.

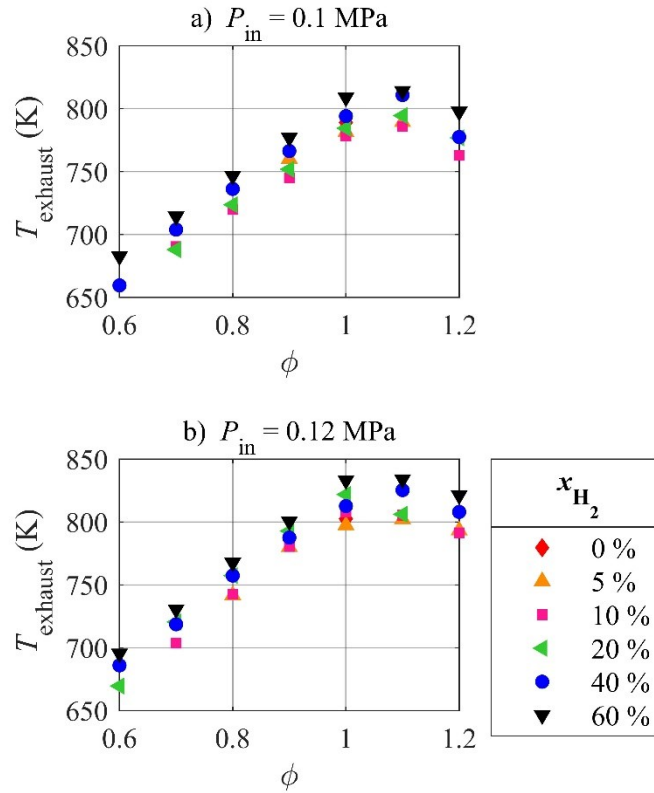


Figure 10. Measured exhaust gas temperature.

#### 4. Summary and conclusions

Experiments were conducted in a modern SI engine in order to assess the feasibility and the characteristics of ammonia combustion at various blended hydrogen fractions, equivalence ratios and intake pressures. In future applications, hydrogen could be provided by in-situ  $\text{NH}_3$  dissociation in a catalytic reformer. The main conclusions are as follow:

- A new measurement database of performance, combustion characteristics and emissions data is provided for numerical validation purposes.
- $\text{NH}_3$  is confirmed as a very suitable SI engine fuel for modern engines since neat ammonia operation could be achieved under supercharged conditions, even slight ones.
- Highest indicated pressure and efficiency were achieved at low and moderate hydrogen addition, at slightly fuel-rich and slightly fuel-lean conditions respectively. However, lean mixtures with high hydrogen content also showed promising performance.
- Supercharged operation is expected to be beneficial in all cases, while increasing the compression ratio remains an open question. In that matter, the interest of engine design modification for optimal  $\text{NH}_3$  fuel operation still needs to be assessed.

- Hydrogen is an ignition promoter, allowing significant performance and stability improvement when added in small quantities, mainly beneficial for the early stages of the combustion. Wall heat losses are thought to play a significant role at high hydrogen fractions.
- The phasing of the combustion is correlated with the Laminar Burning Velocity of the mixture under spark ignition timing conditions, in a non-linear fashion and mainly independently of the hydrogen fraction. However, the LBV does not fully explain the ignition and stability behavior of hydrogen-enriched mixtures with very low LBVs.
- High NO<sub>x</sub> and NH<sub>3</sub> emissions need to be appropriately mitigated in future applications, possibly by means of already existing technologies. A fuel blend with 20% H<sub>2</sub> and  $\phi = 0.7$  exhibited both exhaust temperatures in the range 550-750 K and a NH<sub>3</sub>/NO<sub>x</sub> ratio close to unity, compatible with the use of a dedicated SCR after-treatment system.

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## Declarations of interest

None.

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