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## Cross-linking of poly(butylene terephthalate) by reactive extrusion using Zn(II) epoxy-vitrimer chemistry

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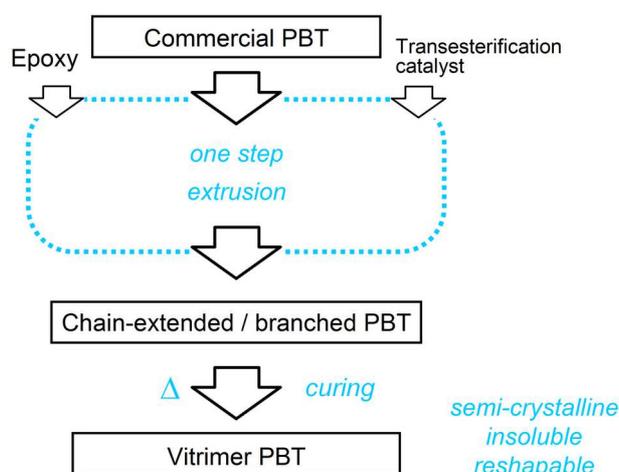
### Abstract

Poly(butylene terephthalate) (PBT) vitrimers were prepared by reactive extrusion from industrial PBT thermoplastics using Zn(II)-catalyzed addition and transesterification chemistry. PBT thermoplastics are characterized by a high degree of crystallinity, high melting temperature and high crystallization rate, but right above their melting temperature their mechanical resistance disappear and they show a tendency to drip. We compared -OH and -COOH end-group additions on epoxies in the presence of two different catalysts, 2-methyl imidazole (2-MI) and zinc acetyl acetonate ( $\text{Zn}(\text{acac})_2$ ). With 2-MI, chain extension reactions were efficiently catalyzed in a few minutes at 270 °C but no gelation was observed. With  $\text{Zn}(\text{acac})_2$ , -COOH addition and transesterification led to efficient cross-linking within a few minutes at 270 °C. Such cross-linked material combines the crystalline properties of PBT and dimensional stability above the melting temperature. PBT materials cross-linked through epoxy-vitrimer chemistry are not soluble. However, compared with radiation cross-linked PBT, vitrimer PBT is processable and can be reshaped and recycled.

## Introduction

Vitrimers, the third category of polymer materials, are networks made of chemically cross-linked polymers in which thermally stimulated exchange reactions permit network topology rearrangements while keeping constant the number of bonds and cross-links. In contrast to the two other categories of polymers, i.e., thermoplastics and thermosets, vitrimers combine insolubility and ability to flow when heated. The viscosity of vitrimers is controlled by the rate of the exchange reactions. The first vitrimers<sup>1</sup> were based on epoxy-acid and epoxy-anhydride chemistry and Zn(II)-catalyzed transesterification exchanges. Subsequently, a number of monomers and exchange reactions have been used to synthesize vitrimers.<sup>2-13</sup>

The objective of this study is to show how the original Zn(II)-epoxy chemistry can be applied to synthesize semi-crystalline polyester vitrimers from commercial thermoplastic grades by a cross-linking method that can be used on an industrial scale. Our efforts focused on poly(butylene terephthalate) (PBT). The strategy is presented in Figure 1.



**Figure 1** Flowchart of the chemical concept towards production of cross-linked PBT vitrimers with the help of epoxy vitrimer chemistry.

The formation of a chemically cross-linked polymer network is usually carried out either by reacting monomers with an average functionality greater than two or by cross-linking a pre-existing thermoplastic polymer. In both cases, the process passes through a critical stage, the gelation point at which an infinite network is formed. Beyond the gelation threshold the system becomes an insoluble solid with a definite shape. During the synthesis of a vitrimer, a

permanent covalent network is also formed; however, the network can change its topology thanks to exchange reactions. We use transesterification reactions to build the network. At the same time transesterification reactions impart to the network its dynamic properties at high temperatures. Interestingly, the same reaction, transesterification, is employed when PBT is produced from dimethyl terephthalate..

PBT is a semi-crystalline engineering plastic used in numerous industrial products, such as printed circuit board connectors, automobile parts, electrical appliance components and medical devices. In 2002 the production around the world exceeded 350 ktons<sup>14</sup> and raised up to 830 ktons in 2012.<sup>15</sup> PBT has a high degree of crystallinity, typically 35-40% after injection molding which can be raised to 60% by annealing.<sup>14,16</sup> Compared to polyamides, PBT has a low moisture absorption which makes it a good option for electrical insulation applications.<sup>17</sup> Water absorption of PBT is less than 0.1% after 24 h<sup>14</sup> and is about 0.5% in the saturated state. As a comparison, poly(amide-6) (PA-6) can absorb between 2 and 8% of water and its properties are strongly dependent on humidity.<sup>16-17</sup>

Commercial PBT, with  $M_n$  ranging from 5,000 to 45,000 g/mol, is hardly entangled.<sup>18</sup> The elastic modulus is approx. 2 GPa at room temperature and in the 100 MPa range at temperatures between  $T_g$  of approx. 45 °C and  $T_m$  of approx. 225 °C.<sup>14,16,19</sup> However, above the melting temperature, PBT exhibits low viscosity and PBT parts can flow under their own weight which significantly impacts the use of this polymer in high temperature applications. A radiation-induced cross-linking method is commonly used to improve the heat resistance of PBT.<sup>20-22</sup> Typical irradiation at a dose of 200 kGy makes it possible to obtain high values of the gel fraction (> 99%).<sup>23</sup> The radiation-induced cross-linking process is irreversible. It needs to be performed on the parts in their final shape using electron or gamma radiation facilities.

In this paper, we describe a cross-linking method based on reactive mixing and extrusion.<sup>24-30</sup> Usually, in reactive extrusion, precautions are taken to avoid gelation during the process. Indeed gelation can block the extruder. Here, thanks to the exchangeable nature of bonds the composition can be adjusted to assure the processability during a reactive mixing stage. When necessary, cross-linking can be completed after reactive mixing in an annealing step.

# 1 Experimental

## 1.1 Materials

Two different PBT materials, specifically synthesized for this study, were obtained from SABIC. One referred as "High PBT" has molar masses of  $M_n = 47$  kg/mol,  $M_w = 100$  kg/mol and end group concentrations of  $[\text{COOH}] = 37$  meq/kg,  $[\text{OH}] = 23$  meq/kg. The other, referred as "Low PBT" has  $M_n = 23$  kg/mol,  $M_w = 48$  kg/mol,  $[\text{COOH}] = 17$  meq/kg and  $[\text{OH}] = 120$  meq/kg. Before use, PBT pellets were dried for 16 h at 120 °C under vacuum.

Diglycidyl ether of bisphenol A (DGEBA) with an  $[\text{OH}]/\text{epoxy}$  ratio lower than 0.03, and an oligo-bisphenol A-co-epichlorohydrine solid epoxy resin, with an  $[\text{OH}]/\text{epoxy}$  of approx. 1.2, both produced by the Dow Chemical Company were used. 2-Methylimidazole (99%), NaCl (99%), ethyl acetate (99.5%), 3-chloro-1,2-propanediol (98%), pentaerythritol tetrakis(3,5-di-tert-butyl-4-hydroxy hydro cinnamate) (Irganox 1010, 98%) and bisphenol-A (99%) were purchased from Sigma Aldrich. Zinc(II) acetyl acetonate ( $\text{Zn}(\text{acac})_2$ ) (23.5 to 26.0 wt% Zn) was purchased from Acros Organics. 1,1,2,2-tetrachloroethane (98%), sodium hydroxide pellets (98%), hydrochloric acid, 36% w/w aqueous solution and 4-heptyl benzoic acid were purchased from Alpha Aesar. These products were used as received. Synthesis of bisphenol-A bis(2,3-dihydroxypropyl) ether is described in SI.

## 1.2 Reactive mixing

Modified PBT samples were prepared by reactive mixing. Typically, 10 g of well-dried PBT pellets were introduced via a hopper, together with the diepoxide (DGEBA, 0 to 0.4 g), the esterification catalyst (2-MI, 0 to 5 mg) or trans-esterification catalyst ( $\text{Zn}(\text{acac})_2$ , 0 to 36 mg) and an antioxidant (Irganox 1010, 10 mg) into a DSM Xplore 15-cc twin-screw mini-compounder under a nitrogen flux. The rotor speed and the temperature were set respectively at 60 rpm and 270 °C. Mixing time was typically fixed at 10 min. The axial force exercised on the barrel of the compounder, which can be used to follow qualitatively the change of viscosity, was recorded as a function of the residence time. In some experiments, aliquots of the reactive mixture were taken out from the compounder to perform ex-situ end-group analysis by FTIR spectroscopy. At high loading (3.6 wt%) of diepoxide, part of the reactive mixture was purged out from the compounder after 5 min mixing to keep the axial force under the 8,000 N limitation of the equipment.

### 1.3 FTIR spectroscopy

End-group analyses were carried out using the spectroscopic method developed by Ward and Kosky.<sup>31-33</sup> Films were prepared by compression molding at 240 °C followed by rapid cooling in iced water resulting in samples with a thickness between 100 and 300 μm. The films were dried for 16 h at 90 °C before measurements. Samples were investigated by FTIR spectroscopy in transmission in the 4,000-400 cm<sup>-1</sup> spectral range. First, the zero hydroxyl and carboxyl absorption levels were determined by using a deuterium exchanged sample (obtained by immersion in D<sub>2</sub>O at 90 °C for 24 h and dried 16 h at 90 °C). Then, the spectra of the PBT materials were analyzed relative to the background level after normalization to take into account the actual thickness of each sample. The absorbance values corresponding to hydroxyl and carboxyl chain end-groups were measured at 3,550 and 3,270 cm<sup>-1</sup>, respectively (see SI, figure S1). Absolute calibration was done by recording the spectrum of the starting materials for which the end-group concentrations were known.

The reactive mixtures used for the model reactions were obtained by dissolving the reagents 4-heptyl benzoic acid, bisphenol-A bis(2,3-dihydroxypropyl ether), bisphenol-A diglycidyl ether, zinc(II) acetylacetonate and 2-methylimidazole in acetone. Stoichiometric ratios of 1:1 acyl-epoxy, 1:1 primary hydroxyl-epoxy and 0.05:1 catalyst-epoxy were used. The FTIR spectra were recorded at 4 cm<sup>-1</sup> spectral resolution by using a Bruker TENSOR 37 spectrometer equipped with a DTGS detector and fitted with a Specac Golden Gate ATR heating cell. Samples were deposited on the ATR diamond heated at 200 °C resulting in a quick evaporation of acetone. The disappearance of the 910 cm<sup>-1</sup> absorption peak ( $\nu_{\text{COC}}$  epoxy) was monitored at a rate of one spectrum per minute (average of 32 scans) to determine the epoxy conversion (see SI, figure S2) In order to measure the initial height of the absorption peak and its evolution at short times (< 1 minute) with sufficient accuracy, the experiment was repeated at a collection rate of 12 spectra per minute (average of 4 scans) using a liquid-nitrogen cooled MCT detector. The conversion was determined by the Lambert-Beer law from the normalized change of absorbance at 910 cm<sup>-1</sup>.

### 1.4 Swelling tests

To determine the gel fraction, 50 mg of compound was immersed in 5 mL of 1,1,2,2-tetrachloroethane for 16 h at 120 °C. The gel was carefully separated from the solution, washed in chloroform during 24 h, dried at 40 °C for 16 h and weighted.

## 1.5 Thermal analysis

Dynamic Mechanical Thermal Analysis (DMTA) experiments were carried out using a TA Instruments Q800 analyzer operating in film tension mode. Heating ramps were applied at 3 °C/min from 10 to 260 °C. Rectangular samples with a 5 mm × 1.5 mm cross-section and about 10 mm length were tested at 1 Hz frequency and 15 μm amplitude. Differential scanning calorimetric (DSC) measurements were performed using a DSC Q1000 from TA Instruments. The sample was heated to 235 °C at 10 °C/min, held at 235 °C for 2 min, then cooled to -90 °C at 10 °C/min, and finally heated to 235 °C at 10 °C/min. Melting temperatures,  $T_m$ , and crystallization temperatures,  $T_c$ , were determined as the temperatures of maximum endothermic (resp. exothermic) heat flow in DSC. The degree of crystallinity of the samples,  $\chi_c$ , was determined by comparing the enthalpy of melting,  $\Delta H_m$ , measured by DSC at 10 °C/min to the value reported in the literature for 100% crystallinity  $\Delta H_m = 140 \text{ J/g}$ .<sup>14</sup>

## 1.6 Rheometry

Annealing experiments were monitored by rheometry using an Anton Paar MCR 501 analyzer operated with a 25 mm diameter parallel plate geometry. Samples of 1.5 mm thickness were investigated at 270 °C under nitrogen. The variations of  $G'$  and  $G''$  were recorded over time in the periodic oscillation regime ( $\gamma = 0.5\%$  and  $\omega = 1 \text{ rad}\cdot\text{s}^{-1}$ ).

Frequency sweep experiments were performed using an ARES G2 rheometer. The measurements were carried out in the oscillatory shear mode using a 25 mm diameter parallel plate geometry. Frequency sweeps between 0.02 and 100 rad/s were carried out at 1% strain. Stress relaxation profiles were recorded using an ARES G2 rheometer in the 25 mm diameter parallel plate geometry on samples with thickness of 1.5 mm at a deformation of 1%. Values of zero-shear viscosity,  $\eta$  and relaxation time,  $\tau$  were evaluated from the relaxation modulus,

$G(t)$  through the equations:  $\eta = \int G(t)dt$ ;  $\tau = \frac{1}{\eta} \int tG(t)dt$ .

## 2 Results

### 2.1 Reactive mixing of PBT

An overview of the characteristics of the compounds prepared and investigated in this work is presented in Table 1. The time variation of the -COOH and -OH end-group concentrations, as measured by FTIR spectroscopy, is plotted in Figures 2A and 2B. In Figure 2C, the axial force signal monitored by the system during mixing is also presented. An increase of this signal is expected in case of chain extension, branching and/or cross-linking reactions, whereas a decrease is expected in case of polymer chain scission reactions.

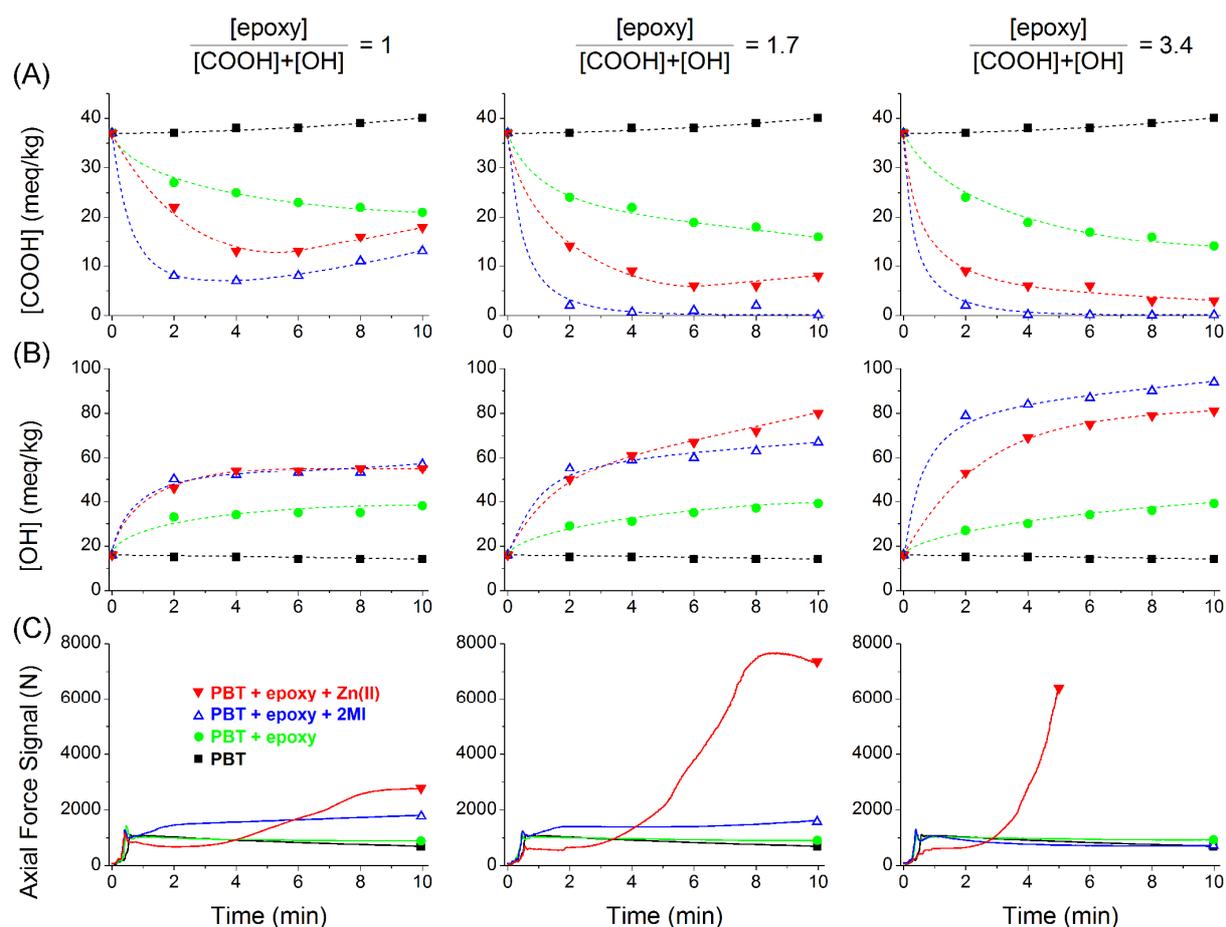
When extrusion is performed without DGEBA and catalyst on the high molecular weight PBT, compound **1** (black squares in Figure 2) the axial force is basically constant. In parallel the amount of -COOH groups during extrusion increases (Figure 2A). The measured increase of -COOH groups (from 37 to 40 meq/kg) is not larger than 10%. Experiments performed on high and low  $M_w$  PBT, with and without catalyst (see SI, figure S3) confirm that such an increase is systematically observed. The increase can be assigned to the thermal degradation of end groups through THF elimination.<sup>34-39</sup>

When DGEBA is added to PBT, compounds **2a-2d** (green circles in Fig 2), we observe during mixing a decrease of the -COOH groups and an increase of the -OH groups concentrations. Evidently, the epoxy groups react with the carboxylic acid end-groups of PBT. However, the axial force signal does not change significantly and even in the presence of epoxy groups in excess, the consumption of -COOH groups is slow and not complete after 10 minutes of mixing.

For compounds 3a-3d (open blue triangles in Figure 2), the mixing of PBT with DGEBA is performed in the presence of 2-methylimidazole (2-MI), a known catalyst for the epoxy-acyl addition reaction.<sup>40-42</sup> In this case, the decrease of the -COOH and increase of -OH concentrations are fast, consistent with epoxy-acyl additions, giving rise to hydroxy-esters. For instance, at a 1:1 stoichiometry the concentration of acid groups decreases to lower than 20% the initial value within 2 min of mixing (Figure 2A, left). During this period, a slight increase of the axial force is observed. When an excess of epoxy is used (middle and right panels of Figure 2), the consumption of the -COOH groups is completed within 2-3 minutes

**Table 1:** Characteristics of prepared blends. \*Determined by GPC using a PS standard with universal calibration. †Determined from DMTA traces at T = 235 °C and f = 1 Hz. ‡Reactive mixing has been followed by curing. ♦Not measurable by DMTA.

Compound	Starting material		DGEBA	Catalyst		Mixing time	Insoluble fraction	E' †
	$M_n^*$ (kg/mol)	$\frac{[\text{epoxy}]}{[\text{OH}]+[\text{COOH}]}$	Quantity (wt%)	Type	$\frac{[\text{catalyst}]}{[\text{OH}]+[\text{COOH}]}$	min	%	kPa
1	47	0	0	none	0	10	0	
2.a	47	1.0	1.1	none	0	10	0	
2.d	47	3.4	3.6	none	0	10	0	
3.a	47	1.0	1.1	2-MI	0.1	10	0	
3.d	47	3.4	3.6	2-MI	0.1	10	0	
4.a	47	1.0	1.1	Zn(acac) <sub>2</sub>	0.1	10	4	
4.b	47	1.2	1.3	Zn(acac) <sub>2</sub>	0.1	10	38	<100*
4.c	47	1.7	1.7	Zn(acac) <sub>2</sub>	0.1	10	43	150
4.d	47	3.4	3.6	Zn(acac) <sub>2</sub>	0.1	10	75	810
5	47	1.7	1.7	Zn(acac) <sub>2</sub>	0.1	2 <sup>‡</sup>	0	
6	23	1.7	4.2	Zn(acac) <sub>2</sub>	0.1	2 <sup>‡</sup>	0	



**Figure 2** Chemical and mechanical monitoring during mixing for three epoxy end-groups ratios. (A) Variation of -COOH end-group content. (B) Variation of -OH group content. (C) Variation of the axial force as a function of reaction time at 270 °C and 60 rpm under N<sub>2</sub> flow.

of mixing with no dramatic effect on the axial force. These observations indicate that 2-MI promotes PBT chain extension.

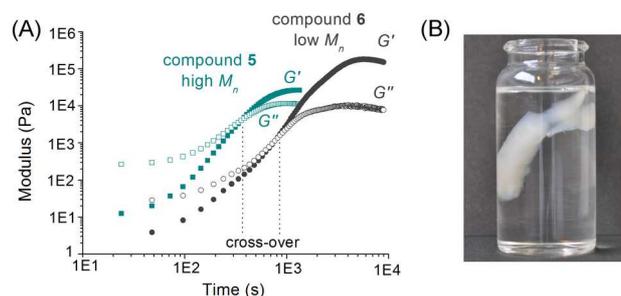
In contrast, when mixing with DGEBA is performed in the presence of the transesterification catalyst Zn(II) acetyl acetonate ( $\text{Zn}(\text{acac})_2$ ), compounds **4a-4d** (filled red triangles in figure 2), the decay of -COOH groups is slower than with 2-MI, indicating that Zn(II) is a less efficient catalyst than 2-MI for the epoxy-acyl addition. However, the increase of -OH group concentration is fast and after five minutes of mixing, the axial force increases abruptly. All these observations suggest that in presence of Zn(II) cross-linking reactions, due to transesterification are efficiently catalyzed.

## 2.2 Curing and gelation

The change of flow properties revealed by a sharp increase of the axial force during mixing in the presence of the transesterification catalyst was analyzed quantitatively by rheometry. Two samples, compounds **5** and **6** respectively based on High-PBT ( $M_n = 47$  kg/mol) and Low-PBT ( $M_n = 23$  kg/mol), were first mixed (2 min at 270 °C) with DGEBA and  $\text{Zn}(\text{acac})_2$ , both at the same molar concentration, in the extruder. Then, the compounds were annealed in-situ in a rheometer at 270 °C. Shortly after extrusion, the measured viscosity was approx. 300 Pa.s for compound **5** and 10 Pa.s for compound **6**. The time dependencies of the storage,  $G'$ , and loss,  $G''$ , moduli are presented in Figure 3A. In both cases, a rise of the moduli was observed within  $10^2$ - $10^3$  seconds. Moreover, the rheological data show that the  $G'$  and  $G''$  plots cross each other, which strongly suggests that gelation takes place in this time range. The cross-over was observed earlier for compound **5** (after about 5 min) than for compound **6** (after about 12 min). However, compound **6** eventually reached a higher value of  $G'$  after complete reaction. Indeed, for PBT of lower molar mass (compound **6**), complete curing with the same molar concentration of diepoxide, yields a higher density of cross-links.

The occurrence of gelation was checked by swelling tests performed in 1,1,2,2-tetrachloroethane, a good solvent for non-cross-linked PBT. Before curing in the rheometer, both compounds **5** and **6** were soluble. After curing in the rheometer, the samples swelled but remained insoluble, confirming gelation. These experiments demonstrate that, despite important differences in molecular weight and end-group concentrations, the materials in both

cases were eventually cross-linked beyond the gel point after full reaction. The same process proved to be efficient for the two used PBT materials.



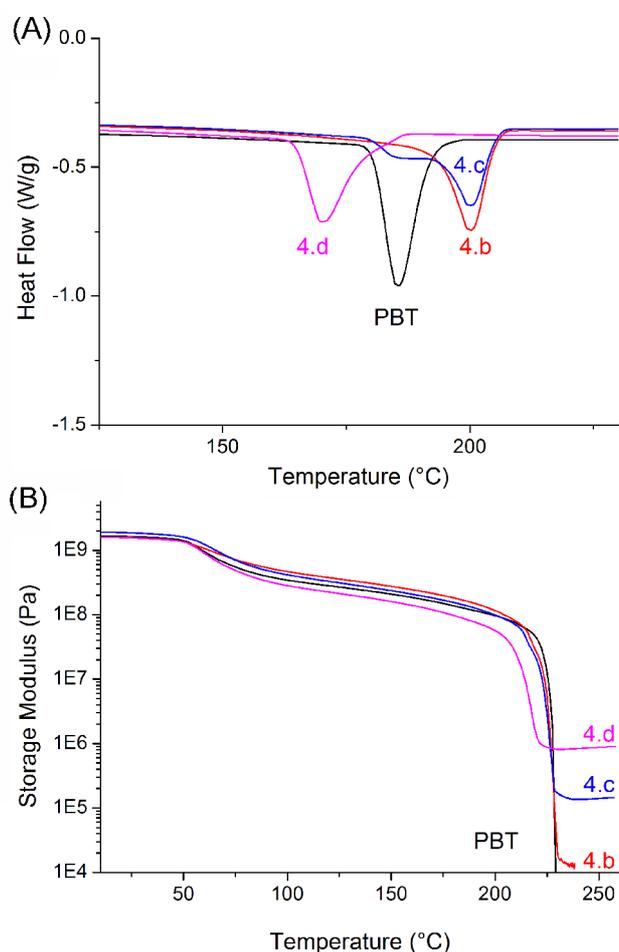
**Figure 3** Gelation: (A) time dependence of the storage shear modulus  $G'$  (filled symbols) and loss modulus  $G''$  (open symbols) at 270 °C after a 2 min reactive mixing stage for PBT of two different molecular weights: compound **5** (squares) and **6** (circles). (B) Swelling of a PBT sample cross-linked beyond gelation (compound **4d**, immersed in TCE at 120 °C for 16 h and then cooled to room temperature).

After 10 min of mixing, the samples were not soluble (Figure 3B). Values of insoluble fractions are reported in Table 1. We observed that all samples extruded without catalyst (compound **1** and compounds **2a-2d**) eventually dissolved. Swelling experiments for samples extruded with the esterification catalyst 2-MI (compounds **3a-3d**) revealed no gel formation during the extrusion time used in this study (10 min). At longer extrusion times, small gel particles were observed for 1.7 and 3.6 wt% loadings of diepoxide as already reported in other studies.<sup>43-44</sup> Eventually, samples mixed with at least one equivalent of DGEBA and the Zn(II) transesterification catalyst (compounds **4a-4d**) systematically showed gelation; an example of unswollen and swollen specimen (compound **4c**) is shown in ESI (figure S4). Moreover, when the [epoxy]/([OH] + [COOH]) ratio was varied from 1.0 to 3.4 eq., the gel fraction increased from 4 to 75%. (Table 1).

### 2.3 Thermal analysis

The results of DMTA and DSC experiments are reported in Figure 4 and in SI, Figure S4. Figure 4A shows the cooling curves of the pristine and modified PBT samples as recorded by DSC. In the **1**, **4a-4d** series the crystallization temperature  $T_c$  and degree of crystallinity  $\chi_c$  vary non-monotonically as a function of the amount of diepoxide. The pristine PBT shows a crystallization exotherm with a peak minimum at 186 °C. For loadings of DGEBA lower than 1.7 wt% (compounds **4a-4c**), the crystallization temperature increases ( $T_c = 200-202$  °C), together with a slight increase of the degree of crystallinity for compound **4a** (Figure S5C) meaning that in the cross-linked materials low loadings of diepoxide have a nucleation effect. This is also reflected in the DMTA data (Figure 4B) where higher values of  $E'$  between  $T_g$

and  $T_m$  are found suggesting a higher degree of crystallinity for compounds **4b** and **4c**. At 3.6 wt% loading (compound **4d**), the melting and crystallization temperatures as well as the degree of crystallinity are lower than those of pristine PBT and, consequently, the observed  $E'$  value between  $T_g$  and  $T_m$  is also lower. Thus, modification of PBT has two opposite effects: on one hand, cross-linking reduces the ability to crystallize; on the other hand, modifiers have a nucleation effect. At low loadings of diepoxide, these two effects practically compensate each other and thus, compounds **4a**, **4b** and **4c** show similar values of  $T_c$ ,  $T_m$  and  $\chi_c$ . At high loading (compound **4d**) nucleation does not increase anymore but cross-links' density is clearly detrimental to crystallization. Consequently, compound **4d** shows lower  $T_c$ ,  $T_m$ , and  $\chi_c$  values.



**Figure 4:** (A) DSC traces obtained on cooling of the pristine and modified PBTs. (B) DMTA analysis:  $E'$  storage modulus of PBT (black) and compounds **4b-4d** (green).

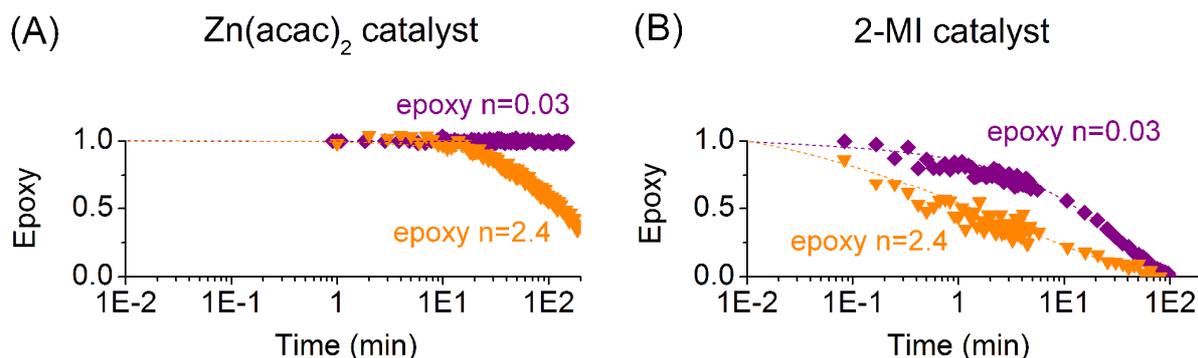
In the vicinity of the glass transition and melting temperatures, all DMTA traces show well-defined drops of  $E'$  similar to those observed in PBT. But in contrast to pristine PBT, compounds **4c-4d** show a non-vanishing elastic modulus above  $T_m$  at the level of 100 kPa to 1

MPa, characteristic of an elastomeric substance, which is another confirmation of cross-linking.

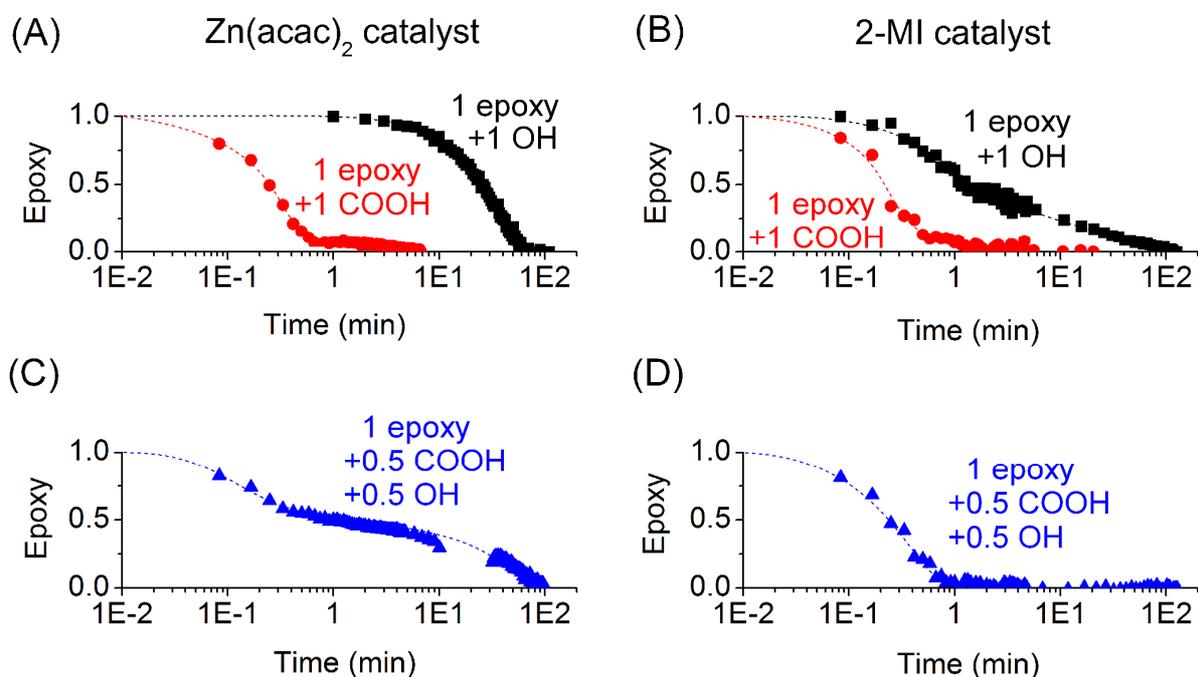
As for elastomeric properties, data presented in Figures 3A and 4B demonstrate that by adjusting the characteristics of the starting material and stoichiometry one can vary at will the duration of the pre-gel period and the stiffness of the final network.

### 2.3 Model reactions

The kinetics of reactions that are likely to occur during extrusion were investigated by using FTIR spectroscopy in ATR mode. We chose 200 °C as a compromise between conditions close to the usual extrusion temperatures and the possibility to measure quick variations with a semiconductor IR detector. Månson *et al.* used model molecules to investigate the reactivity of poly(ethylene terephthalate) (PET) end-groups with a multi-epoxy without any catalyst.<sup>45</sup> They observed that the reaction between the -COOH and epoxy groups is fast and effective, whereas the reaction between the -OH and epoxy groups appeared less efficient. Testud *et al.* investigated the polytransesterification of multifunctional hydroxyester monomers in the presence of various catalysts.<sup>46</sup> They found that Zn(II) efficiently catalyze transesterification and identified etherification through dehydration of alcohols as a possible side reaction. The model molecules used in our study are depicted in Table S1. 4-Heptyl benzoic acid was selected because of its low melting temperature (98 °C), low volatility and high compatibility with the epoxy resin. Bisphenol-A bis(2,3-dihydroxypropyl) ether was chosen to mimic the terminal hydroxyl functionalities. For the epoxy model, we used the same compound as in extrusion experiments, namely epoxy n=0.03, which practically does not contain hydroxyl groups. To investigate the role of hydroxyl side groups that could be formed during addition reactions, we used the oligo(bisphenol A-co-epichlorohydrin) prepolymer epoxy (n=2.4), which has a [OH]/epoxy ratio of approximately 1.2. In all model reaction studies the catalyst concentration was fixed at 5 mol%. Reactions were followed by measuring the epoxy signal at 910 cm<sup>-1</sup>, the absorbance was normalized with respect to its initial value. Epoxy + acid addition reactions in the presence of imidazole<sup>42,47-51</sup> and Zn(II)<sup>48,50,51</sup> catalysts were investigated. Here, we additionally focus on understanding of the effect of hydroxyl groups on these reactions.



**Figure 5** Variation of the epoxy concentration at 200 °C for two different resins: epoxy n=0.03 (with no OH groups) and epoxy n=2.4 (with a few OH groups) after a catalyst Zn(acac)<sub>2</sub> (A) or 2-MI (B) is added.



**Figure 6** Variation of the epoxy concentration at 200 °C for the epoxy n=0.03 resin mixed with 4-heptyl benzoic acid and/or bisphenol A bis(2,3-dihydroxypropyl) ether. (A) and (C) catalyzed by Zn (II), (B) and (D) catalyzed by 2-MI. Variation after a catalyst Zn(acac)<sub>2</sub> (A) or 2-MI (B) is added.

Figure 5A shows the evolution of epoxy concentration in the absence of acid groups when Zn(acac)<sub>2</sub> is used. In the absence of hydroxyl groups, no reaction takes place. In contrast, when the resin contains -OH side groups, after 10 minutes, the concentration of epoxy groups decreases. Such a decrease can be attributed to the occurrence of -OH + epoxy addition reactions. The situation is very different when the 2-MI catalyst is used (Figure 5B).

Reactions occur even when hydroxyl groups are not present. A possible explanation of these results could be that 2-MI initiates the anionic polymerization of the epoxy resin.

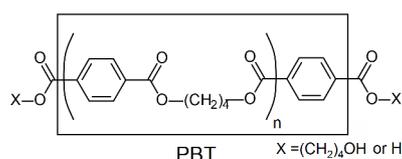
Figure 6A and 6B show the evolution of epoxy groups concentration, as measured by FTIR when acid or alcohol are added in stoichiometric proportions  $[\text{COOH}]/[\text{epoxy}]$  (resp  $[\text{OH}]/[\text{epoxy}] = 1$ ). For both Zn(II) and imidazole catalysts, acid + epoxy reactions are quite rapid. Concerning the alcohol, the decrease of epoxy groups concentration due to alcohol + epoxy addition is faster with 2-MI as catalyst. Figures 6C and 6D show the decay of epoxy groups concentration in the presence of both acid and alcohol at  $[\text{COOH}]/[\text{epoxy}] = [\text{OH}]/[\text{epoxy}] = 1/2$ . Clearly, when the Zn(II) catalyst is present (Figure 6C) at least two processes take place. First, within a minute, acid groups react with epoxies. The alcohol + epoxy addition is much slower and takes about 100 minutes to be completed. Comparison with Figure 6A shows that the two reactions are practically independent. Since in the presence of 2-MI catalyst, epoxy + alcohol addition can occur at the same time as epoxy + acid addition can occur from the beginning, the situation is more complex (Figure 6D). In the presence of acid, epoxy + alcohol addition seems to be faster, after a few minutes no epoxy groups are left.

In parallel to addition reactions, once ester bonds are formed, transesterification reactions occur. The FTIR spectroscopy does not give any indication about the kinetics of such reactions. Transesterification reactions in the presence of Zn(II) were studied in detail by gas chromatography coupled with mass spectrometry in references 1, 52-55. In ESI, we included additional measurements for 2-MI by the same technique (Figure S6). At 150 °C, the characteristic time to reach 50% conversion in the presence of 5 mol% Zn(II) is 1 hour. Using reported value of the activation energy (130 kJ/mol)<sup>55</sup> the estimated time to reach the same conversion at 200 °C is of about 1.2 min. Hence, we expect that when Zn(II) catalyst is used, transesterification and formation of cross-links can occur even before all esters bonds are formed. In contrast with 2-MI the time recorded to yield 50% conversion by transesterification (ESI) is of about 25 min. Therefore, when 2-MI is used, linear or slightly branched chains can be formed first and much longer time is required to make cross-links by transesterification.

## 3 Discussion

### 3.1 Vitrimer network formation

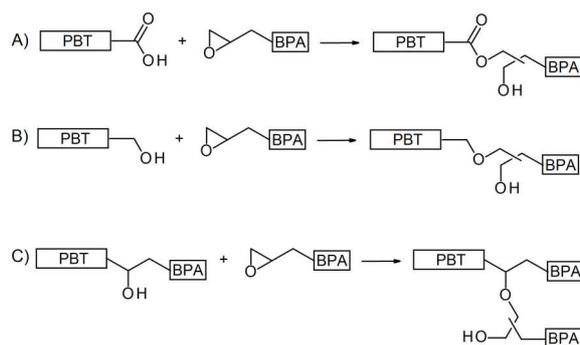
PBT is an industrial product. Depending on the manufacturer, grade and batch number, the end-group composition can vary. Typically aromatic acid end groups,  $-X = -H$  in Scheme 1, are present at a level between 10 to 80 meq/kg.<sup>16</sup> The remaining end-groups are essentially primary hydroxy groups coming from the butanediol monomer,  $-X = -(CH_2)_4OH$  in Scheme 1.



**Scheme 1** Chemical structure of PBT.

During processing (extrusion, injection molding, etc) the degradation of hydroxybutyl end-groups is well documented<sup>34-39</sup> resulting *i*) in a small amount of olefinic end groups and *ii*) to a rearrangement of  $-X = -(CH_2)_4OH$  into  $-X = H$  end groups through THF elimination. This second, more important degradation reaction results in an increase of the carboxylic acid end-group fraction. During extrusion of PBT in the absence of any additive (black squares in Figure 2) the number of acid groups increases. Figure 2A indicates that in the conditions used here at 270 °C after 10 minutes the increase of acid concentration is approx. 10% the initial concentration.

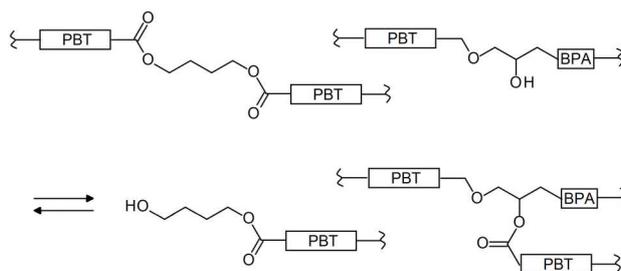
The reactive mixing of PBT with diepoxides without added catalyst has been extensively studied. It was found that chain extension can occur.<sup>43-44</sup> Cross-linking was only reported for high epoxy content and very long reaction times. Our study of  $-COOH$  and  $-OH$  concentrations during the reaction without added catalyst (Figure 2A and 2B, green circles) seem to fully confirm the existence of addition reactions (Scheme 2A and 2B). The axial force in extrusion (Figure 2C) did not increase substantially and samples after mixing for 10 min were soluble demonstrating the absence of gelation.



**Scheme 2:** Illustration of possible addition reactions during reactive mixing of PBT with epoxides: (A) esterification of carboxyl end groups and (B) etherification of hydroxyl end groups. (C) Branching from the secondary hydroxyl groups produced from reactions (A) and (B).

In the presence of catalysts, the situation is more complex (Figure 2). During the mixing the axial force increases indicating the increase of viscoelasticity of the mixture (Figure 2C). When 2-MI is used as a catalyst, (Figure 2, open blue triangles) the increase of axial force is moderate. The consumption of  $-\text{COOH}$  groups and increase of  $-\text{OH}$  groups show that chain extension through addition reactions (scheme 2A-2B) occur. In principle branching and cross-linking from lateral hydroxyl groups produced during addition reactions could also occur (Scheme 2C). Solubility tests show that after mixing all samples were soluble (Table 2). We conclude that 2-MI catalyst is very efficient to promote esterification and etherification. However, it is not very efficient to promote transesterification. As a result, it is not efficient to promote formation of a permanent network.

In contrast to 2-MI, when Zn(II) catalyst is used, a particularly abrupt increase of the axial force is observed after a few minutes of mixing. The solubility studies demonstrate formation of a permanent network (Table 2). The study of  $-\text{COOH}$  and  $-\text{OH}$  variations (Figure 2A and 2B) seem to indicate that Zn(II) promotes chain extension less efficiently than 2-MI. Studies of model molecules confirm this observation. They also indicate that Zn(II) promotes fast transesterification. The increase of axial force, an indication of cross-linking, seem to occur only when a large fraction of the initially present  $-\text{COOH}$  groups is consumed. Addition reactions lead to formation of both ester bonds and lateral hydroxyl groups. As a result, Zn (II) catalyst is able to induce cross-linking (Scheme 3). The gelation transition can be controlled by the amount of diepoxy present in the mixture.



**Scheme 3** Illustration of the transesterification towards the formation of a new end-group.

Eventually, a dehydration of alcohols reaction that produces ether bridges could be also evoked. When reacting alcohols and esters in bulk in the presence of Zn(II) catalyst, Testud *et al.* observed minor formation of ethers byproducts even though vacuum was applied and stoichiometric conditions were favourable:<sup>46</sup>  $[\text{OH}] > 5 \text{ eq./kg}$  and  $[\text{OH}]/[\text{ester}] > 2$ . In our case, however, monitoring of  $[\text{OH}]$  gives concentrations not exceeding 100 meq/g, *i.e.* an  $[\text{OH}]/[\text{ester}]$  ratio of the order of 0.01. It is therefore unlikely that dehydration could play an important role. Still, for long reaction times when transesterification is not catalyzed, it could eventually contribute to some cross-linking.

### 3.2 Vitrimer network properties

Reactive mixing of diepoxy and PBT polymers yields permanent networks when mixing is performed in the presence of Zn(II) catalyst. The solubility tests indicate that cross-linking degree increases when the diepoxy fraction is increased. For example, when the fraction of DGEBA varies from 1.2 to 3.6 wt%, the insoluble fraction increases from 4 to 75 wt%. The increase of cross-linking density with diepoxy fraction is also confirmed by the DMTA experiments at 1 Hz. Above the melting temperature a plateau modulus is observed for high diepoxy contents and it varies between 0.15 to 0.8 MPa when the diepoxy fraction varies from 1.7 to 3.6 wt%.

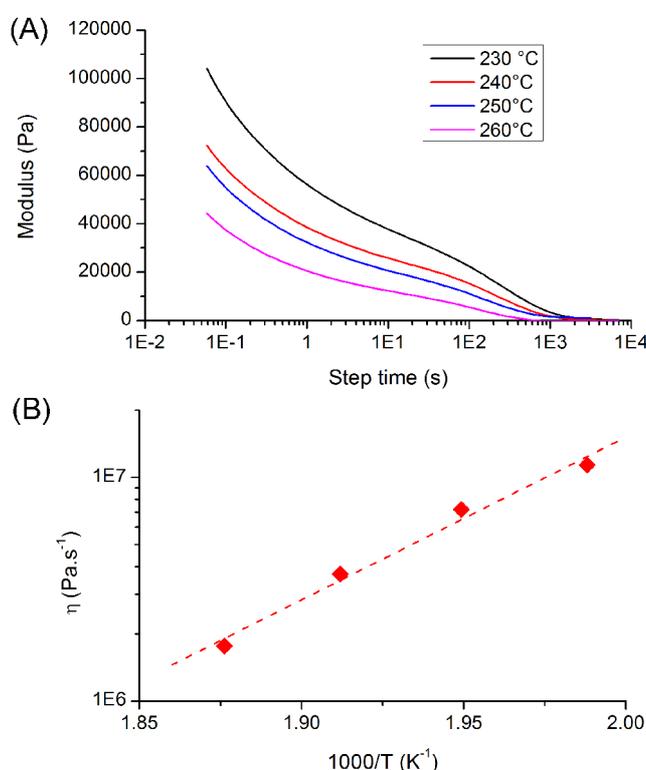
It is not necessary to carry out the reactive mixing step to complete reaction. Isothermal curing after a short reactive mixing time at temperatures above the melting temperature can be used to increase the cross-linking degree as demonstrated by rheology and solubility experiments (Figure 3). These experiments combined with kinetic studies (Figure 2) show that the molecular weight of the precursor PBT gives an additional handle to control the cross-

linking degree. For the high molecular weight PBT, the number of -OH and -COOH groups is low and the same molar fraction of epoxy leads to a less cross-linked material.

Interestingly, cross-linking does not perturb crystallization. The crystallization is fast and the degree of crystallinity is basically maintained (Figure 4A).

In contrast to PBT cross-linked by irradiation, PBT cross-linked by Zn(II) epoxy-vitrimer chemistry can flow above the melting temperature. As an example, Figure 7 shows the stress relaxation results and the variation of viscosity as a function of temperature for compound **4c**.

Figure 7B shows an Arrhenius dependence  $\ln(\eta) \sim 1/T$ , as hitherto observed in vitrimers. The value of the activation energy is of about 140 kJ/mol.

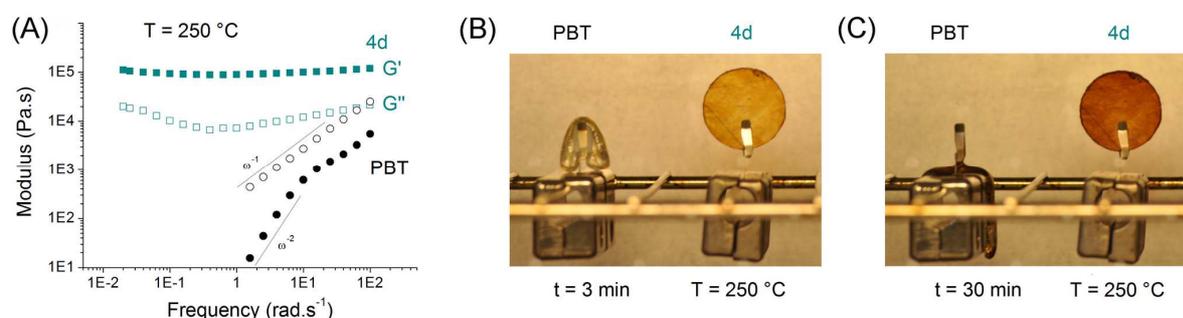


**Figure 7** (A) Plots of stress relaxation experiments on compound **4c**, (B) Variation of the viscosity as a function of inverse temperature  $1000/T$  showing Arrhenius dependence.

The elastic modulus above  $T_m$ , viscosity and relaxation time can be tuned by the amount of diepoxy. Thus, the relaxation time at 230 °C is 500 s for compound **4c** and 1300 s for compound **4d**. The long relaxation times above the melting temperature bring good dimensional stability to PBT vitrimers. For the PBT with highest cross-linking, compound **4d** the value of viscosity is about  $\eta \sim 10^8$  Pa.s at 250 °C. This value is huge in comparison with the viscosity of standard PBT, which ranges from 30 to 900 Pa.s at 250 °C.<sup>16</sup> The frequency sweep experiments illustrate nicely this difference (Figure 8A). At 250 °C, PBT before

modification, shows the characteristics of a non-entangled polymer melt. The value of viscosity, inferred from the  $G''(\omega) \sim \omega$  terminal regime variation is approx. 200 Pa.s. At the same temperature, the vitrimer PBT (compound **4d**) shows elastomeric plateau properties with no evidence of any terminal regime down to an angular frequency of  $10^{-2} \text{ s}^{-1}$ . Indeed, for this compound, the relaxation time given by stress relaxation experiments is much larger than 100 s.

Figures 8B and 8C illustrate the good dimensional stability of vitrimers in comparison with standard PBT. We show the appearance of compression-molded coin-sized specimens made of these two materials after a residence times of 3 minutes and 30 minutes respectively in an oven at 250 °C in air.



**Figure 8** (A) Angular frequency dependence of storage modulus  $G'$  (filled symbol) and loss modulus  $G''$  (open symbols) at 250 °C for PBT (circles), compound **4d** (squares). (B) Appearance of PBT and compound **4d** disks after 3 min in an oven at 250 °C. (D) Appearance of PBT and compound **4d** disks after 30 min in an oven at 250 °C.

After 3 min in the oven, both samples have become transparent but pristine PBT immediately flows, whereas the shape of the PBT vitrimer part is retained. Under its own weight a coin-sized specimen undergoes a stress of about  $\rho.g.h \sim 100 \text{ Pa}$ , where  $\rho$  is the density of the polymer,  $g$  the gravitational acceleration and  $h$  the height of the specimen. With a viscosity of 200 Pa.s the expected strain rate  $\dot{\gamma} = \sigma/\eta$  is of about  $0.5 \text{ s}^{-1}$ . Thus, without surprise, the coin shape is not recognizable after 3 minutes. For the vitrimer PBT part, however, the strain rate is approx.  $\dot{\gamma} = 10^{-6} \text{ s}^{-1}$  and deformation is hardly detectable on this time scale. The fixed shape is also a demonstration that the compression-molded part was thoroughly relaxed. The same two samples after 30 minutes are shown in Figure 8C. Pristine PBT has dripped outside the framing field, but the vitrimer PBT is still in place. One can see in the picture that after 30 minutes at 250 °C in some oxidation took place, as shown by the brownish color, but interestingly the shape of the specimen is not much altered. Thus, similarly to radiation cross-

linked PBT, PBT cross-linked with the help of epoxy-vitrimer chemistry can handle high temperatures for a relatively long time, whereas the standard PBT flows immediately above the melting temperature.

## Conclusion

Research and development of vitrimers confronts two challenges. The first challenge concerns the translation of unique combination of vitrimer properties into novel materials and applications. Literature on design of weldable long fiber composites<sup>56-58</sup> and nanocomposites,<sup>59</sup> photo-responsive carbon-nanotube composites,<sup>60-61</sup> UV-curable thiol-ene vitrimers for patterning and nanoimprint lithography,<sup>62</sup> moldable and multi-functional liquid-crystalline elastomer actuators,<sup>63,64</sup> shape memory polymer networks<sup>65-69</sup> show some interesting directions and potential uses. The second challenge is to develop dynamic covalent chemistries that will allow bringing vitrimer properties to currently produced thermoplastics and thermosets. Developments in the area of fully bio-based vitrimers,<sup>2,10,70</sup> amorphous polyesters,<sup>4</sup> polyurethanes and polyureas<sup>7,12,69,71,72</sup> or of polymers with C-C backbones<sup>13,73</sup> are promising examples. In this article, we have developed a semi-crystalline PBT vitrimer via an industrial process, reactive mixing, starting from standard base materials, i.e. PBT thermoplastic, and an epoxy resin. Epoxy chemistry is particularly convenient as it allows chain extension and branching without release of small molecules. In principle, reacting PBT with multifunctional alcohols could also yield a PBT dynamic network. However, to advance the reaction, small molecules have to be eliminated and a different synthetic route, solid-state polymerization (SSP), is better adapted for this purpose.<sup>74</sup>

The PBT vitrimers obtained through reactive mixing with diepoxides retain the properties of PBT thermoplastics such as a high degree of crystallinity, while they gain the properties of a cross-linked material such as dimensional stability above melting temperature. Indeed, in contrast to PBT thermoplastics, above melting temperature PBT vitrimers exhibit a rubbery elastic plateau and relax stresses only after a long time. The rubbery plateau and stress relaxation times can be tuned by adjusting the molecular weight of the starting materials and the amount of cross-linker used. The same is true for PBT vitrimers obtained by SSP and both types of materials were found to show an Arrhenius dependence of viscosity with very close  $E_a$  values. Interestingly, PBT vitrimers can be obtained within a few minutes by reactive

mixing whereas several hours are necessary by SSP. When reactions are completed, both types of materials show a slight yellowish aspect, due to the presence of the Zn(II) catalyst.

We have shown that alcohol-epoxy and acid-epoxy addition reactions and transesterification reactions, which determine the relative kinetics of chain extension, chain branching and cross-linking can be conveniently controlled by the choice of a catalyst, the molecular weight of precursor PBT chains and the diepoxide content. In terms of industrial processing, such a control provides tools to combine an optimal and versatile manner of extrusion, object molding and thermal post-curing steps. In particular, it is possible to find conditions that avoid long residence time in the extruder and high viscosity during injection molding.

In conclusion, vitrimer epoxy based chemistry yields a versatile method to permanently cross-link semi-crystalline PBT thermoplastics without a need to use radiation chemistry facilities. Cross-linked PBT vitrimers can be reshaped and welded. Advantageous properties of PBT vitrimers bode well for their industrial applications for example in electric appliances and electronics for which keeping the integrity of electrical insulation in case of accidental overheating is essential.

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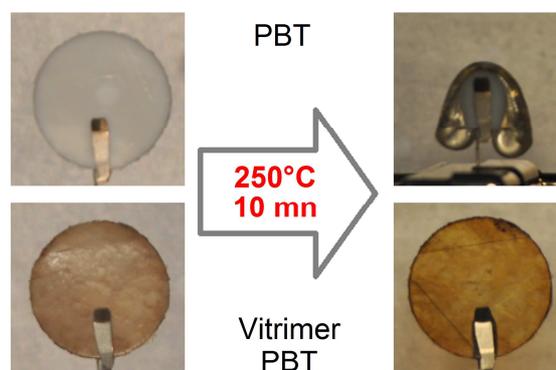
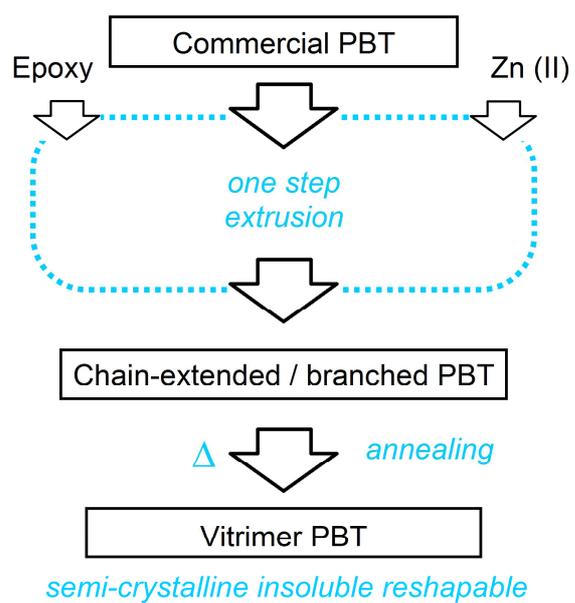
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## Graphical Abstract



# Crosslinking of PBT by reactive extrusion using Zn(II) epoxy-vitrimer chemistry

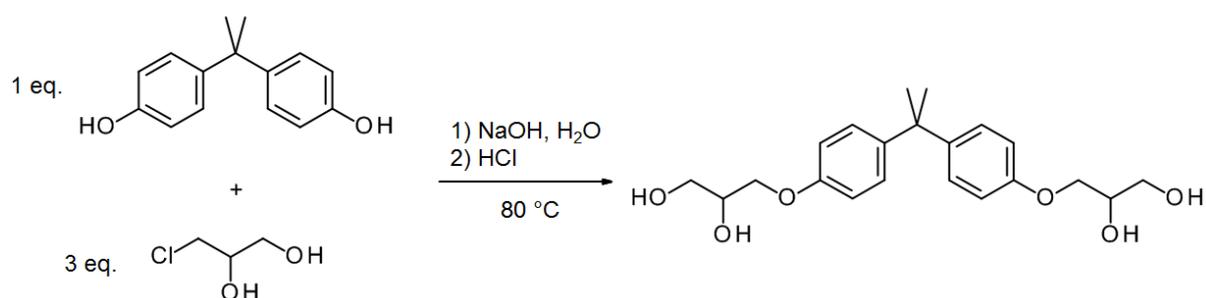
Adrien Demongeot,<sup>†</sup> Ramon Groote,<sup>‡</sup> Han Goossens,<sup>‡</sup> Theo Hoeks,<sup>‡</sup> François Tournilhac,<sup>\*,†</sup> Ludwik Leibler<sup>\*,†</sup>

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## Supplementary Information

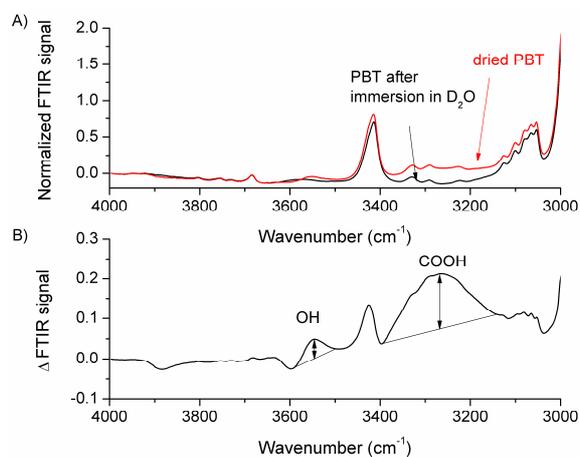
### Synthesis of bisphenol A bis(2,3-dihydroxypropyl) ether



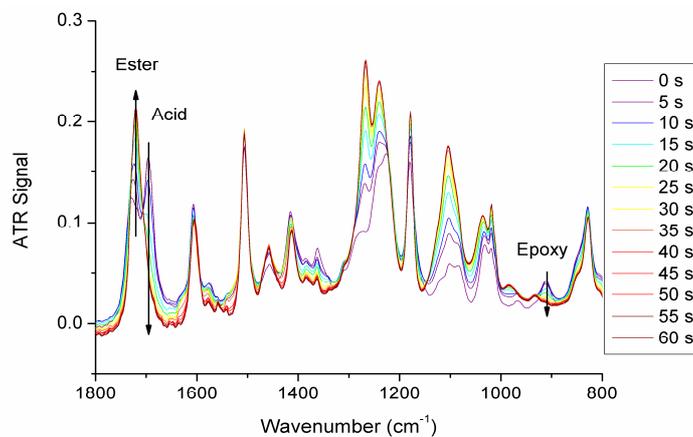
**Scheme 1** Synthesis of bisphenol A bis(2,3-dihydroxypropyl) ether.

In a 500 mL two necks round bottom flask attached to a condenser, a solution of sodium hydroxide (7.26 g, 0.18 mol) in water (120 mL) was placed. With stirring, bisphenol A (10.3 g, 45 mmol) were added. The mixture was heated to 80 °C under a nitrogen atmosphere. Then, 3-chloro-1,2-propanediol (11.4 mL, 0.14 mol) was slowly added dropwise with a purged syringe. Stirring was continued for 16 hours at 80 °C. Subsequently, the solution was allowed to cool down to room temperature. After cooling, a solution of hydrochloric acid (16.0 mL, 0.18 mol) in water (120 mL) was added and the mixture stirred at 80 °C for an hour. Again the solution was allowed to cool down to room temperature. The mixture was decanted and the organic phase was extracted in ethyl acetate. This solution was washed three times with NaCl-saturated water (80 mL) and distilled water (80 mL), dried over anhydrous magnesium sulfate, and filtered. The obtaining solid was purified by

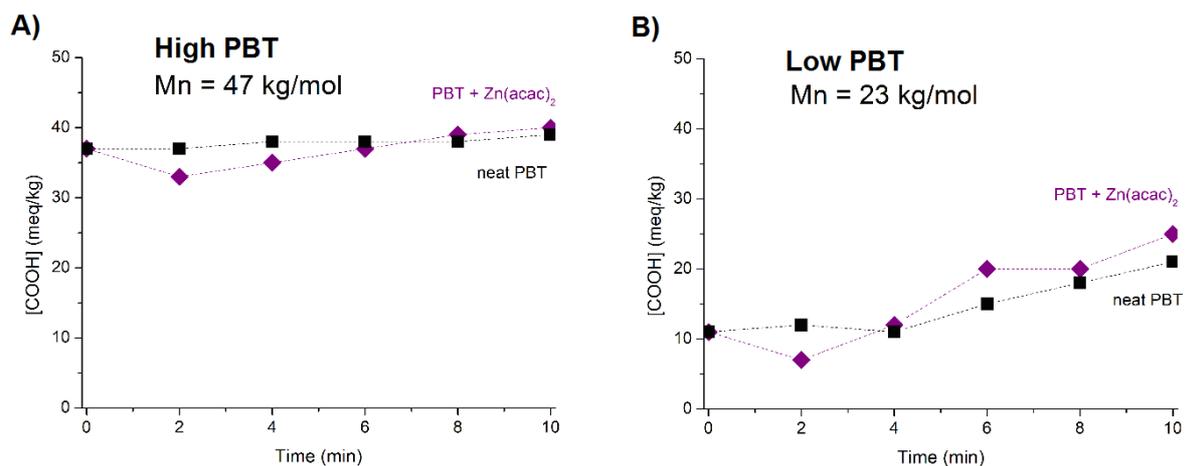
chromatography eluting with ethyl acetate. The product was dried in vacuum at 50 °C for 16 hours. The final product is a white crystalline solid (MP=86-87°C).



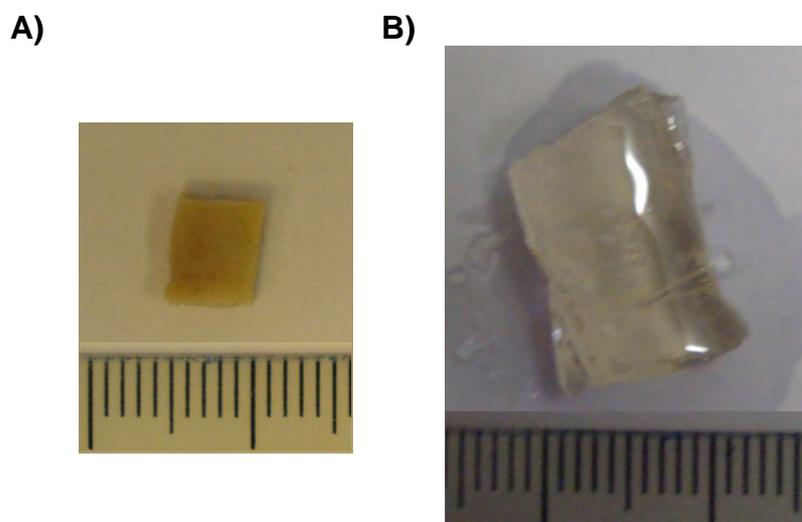
**Figure S1** Determination of [COOH] and [OH] end-group concentration by IR spectrometry. (A) FTIR spectrum of dried PBT (black) and PBT after immersion in D<sub>2</sub>O (B) FTIR signal difference.



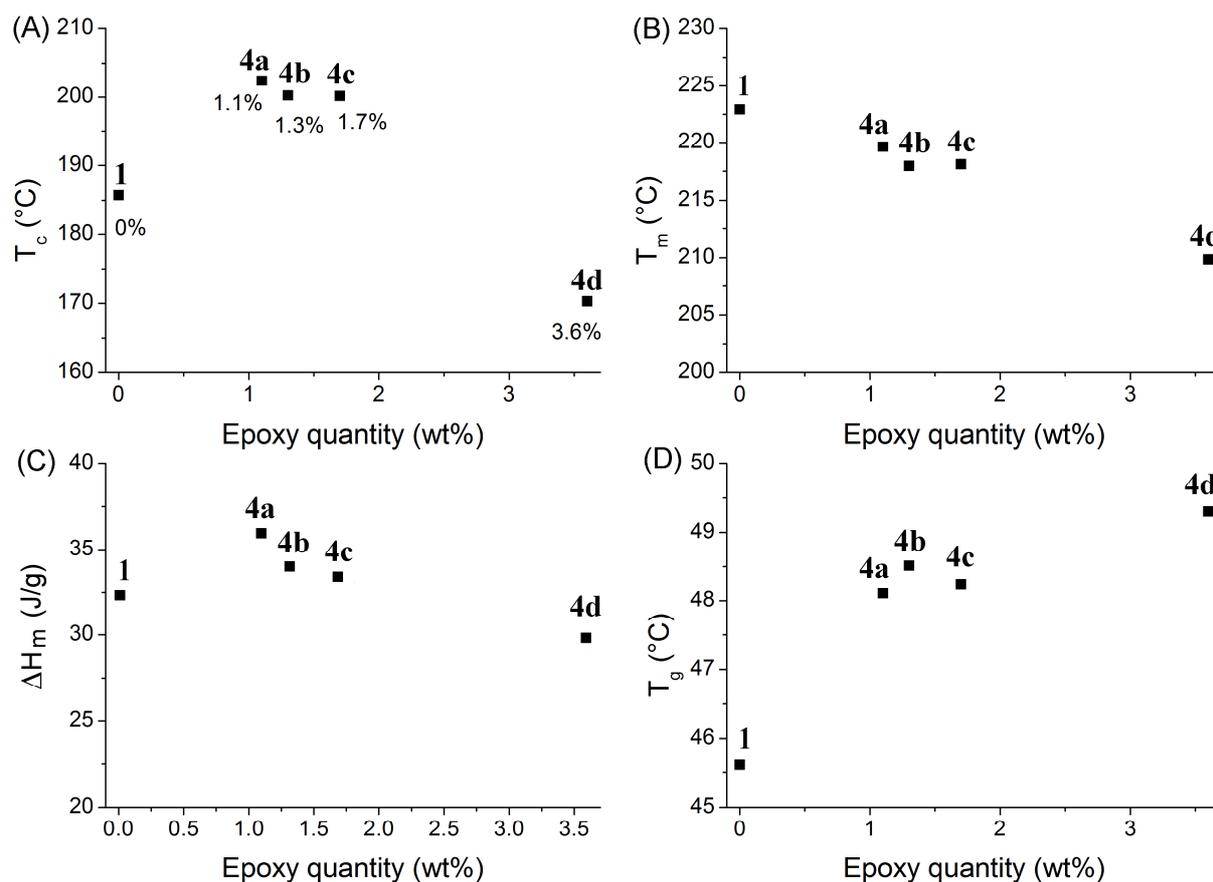
**Figure S2** Determination of epoxy consumption during kinetic experiments with model molecules. Example of ATR-IR spectra showing the epoxy-acid addition catalyzed by Zn (acac)<sub>2</sub> at 200 °C. Spectra were taken every 5s.



**Figure S3** Variation of [COOH] end-group content as a function of extrusion time for PBT of two different molar masses with and without the presence of Zn(acac)<sub>2</sub> at [Zn(II)]/([OH] + [COOH]) molar ratio of 10%.



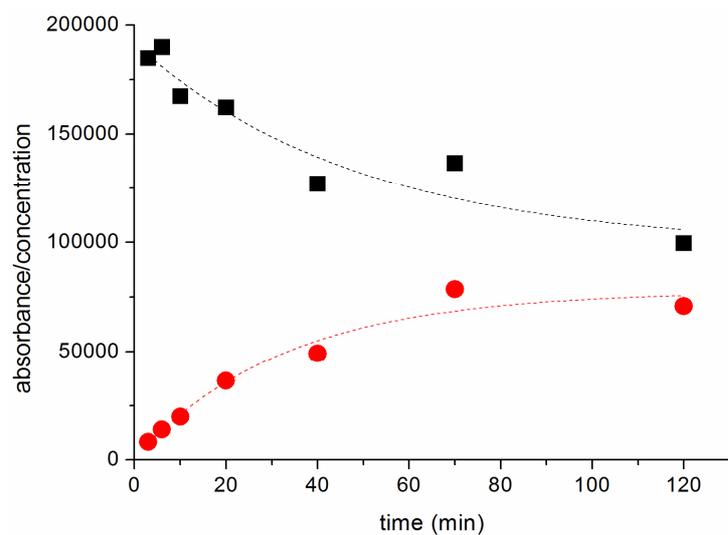
**Figure S4** Visual aspect of an unswollen specimen of compound **4c** (A) and the same after swelling in TCB (B).



**Figure S5** Effect of cross-linking through epoxy vitrimer chemistry on crystallization. Thermal analysis data of compounds **4a-4d** as a function of the epoxy quantity: (A) crystallization temperature, (B) melting temperature, (C) melting enthalpy (integral between 75 and 232°C) measured on 2nd heating, (corresponding degree of crystallinity, compound **1**:  $\chi_c = 23.0\%$ , compound **4a**:  $\chi_c = 25.6\%$ , compound **4b**:  $\chi_c = 24.2\%$ , compound **4c**:  $\chi_c = 23.7\%$ , compound **4d**:  $\chi_c = 21.1\%$ ) and (D) glass transition temperature.

**Table S1** Characteristics of model compounds investigated.

Chemical name	Function	Formula
4-heptyl benzoic acid	acid	
bisphenol A bis(2,3-dihydroxypropyl) ether	alcohol	
diglycidyl ether of bisphenol-A (epoxy n=0.03)	$[OH] \ll [epoxy]$	
oligo(bisphenol A-co-epichlorohydrin) (epoxy n=2.4)	$\frac{[OH]}{[epoxy]} \approx 1.2$	



**Figure S6** Kinetics of model molecules with 2-MI, The reaction is performed at 200°C in bulk between heptyl benzoic and phenyl glycidyl ether in the presence of 5 mol% of 2-MI. Addition takes place within a few minutes, further evolution is analyzed by gas chromatography. The plot shows the time dependance of  $\beta$ -hydroxy-ester (mixture of isomers, black squares) and diester (red disks) concentrations.