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# FeBr<sub>2</sub>-Catalyzed Bulk ATRP Promoted by Simple Inorganic Salts

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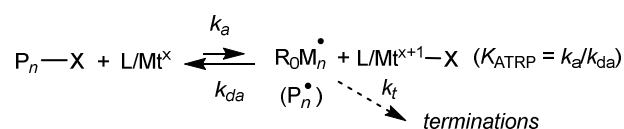
**KEYWORDS:** ATRP, iron, inorganic salts, methyl methacrylate.

**ABSTRACT:** The Atom Transfer Radical Polymerization of MMA in bulk at 70°C, using ethyl 2-bromo-phenylacetate as initiator, is quite rapid and very well controlled when catalyzed by FeBr<sub>2</sub> in the presence of small amounts of simple inorganic salts (chlorides, bromides, iodides, hydroxides, carbonates, bicarbonates, sulfates), comparing favorably in all respects, including technical simplicity, with the previously reported protocols that make use of salts of large organic cations or neutral organic ligands as promoters. A detailed investigation of the KBr-promoted process, supported by DFT calculations, suggests that the active form of the catalyst is a 1:1 adduct, which is stabilized in solution by weak MMA coordination to give an ion-paired K<sup>+</sup>[Fe<sup>II</sup>Br<sub>3</sub>(MMA)]<sup>-</sup> species with a tetrahedral anion. The addition of 18-crown-6 provides a less soluble but more active catalyst. FeCl<sub>2</sub> performs less efficiently and the additions of small amounts of water to the system do not significantly affect the polymerization rate, whereas larger quantities result in rate reduction. The quality of the control is further improved when using 0.1 equivalents of the FeBr<sub>3</sub> deactivator.

## Introduction

Atom transfer radical polymerization (ATRP) is one of the most successful reversible deactivation radical polymerization (RDRP) methods to control the chain growth of more activated monomers such as acrylates, methacrylates and styrenics, yielding well-defined polymers with predictable molecular weights as well as narrow molecular weight distributions.<sup>1-9</sup> Copper complexes, in combination with ligands that can tune the moderating equilibrium constant (Scheme 1) over more than 9 orders of magnitude,<sup>10-12</sup> offer the widest flexibility.<sup>5, 7, 13, 14</sup> However, there is growing interest in using iron-based catalysts,<sup>15-21</sup> in light of the greater availability and low cost of this metal, and especially because of its lower toxicity and higher biocompatibility.<sup>22-24</sup>

### Scheme 1. General mechanism of ATRP initiation.



Numerous iron-based catalysts have been employed so far, generally based on Fe<sup>II</sup>X<sub>2</sub> (X = halide) stabilized by ligands such as phosphines, imines, amines, and various other neutral ligands including *N*-heterocyclic carbenes and carboxylic acids.<sup>15-21</sup> Organic ligands can not only facilitate the dissolution of the iron salt in organic media but also tune the metal redox potential. These iron-based catalysts, generally carried out in polar solvents, are most successful for the ATRP of methacrylates.<sup>25</sup> Previous work in our own group has focused on the ATRP of methyl methacrylate (MMA) in the presence of stabilizing ligands/solvents such as PPh<sub>3</sub>,<sup>26</sup> polar solvents

(such as DMF, NMP, MeCN or PEG<sub>200</sub>)<sup>27-30</sup> and in deep eutectic solvents.<sup>31</sup>

There are also a number of contributions on “organic ligand-free” Fe-based ATRP, where the ligand role is played by an inorganic anion (typically a halide) from a salt, in combination with either FeX<sub>2</sub> and an alkyl halide initiator (direct activation)<sup>32-37</sup> or with FeX<sub>3</sub> and AIBN (reverse activation)<sup>32, 38</sup> or in other protocols (AGET,<sup>39-44</sup> ARGET,<sup>45</sup> ICAR,<sup>46</sup> etc.). To the best of our knowledge, all these precedents made use of salts with large organic cations (“onium” salts such as tetrabutylammonium or -phosphonium, imidazolium, or tetrazonium). When such salts are low-melting (ionic liquids), they have also been used as solvents.<sup>40</sup> It is also relevant to mention that, in a few cases, the beneficial role of additional additives, generally fully inorganic bases (i.e. with alkali or alkaline-earth metals) was highlighted. For instance, the rates of the styrene<sup>39</sup> or MMA<sup>42</sup> AGET ATRP using FeCl<sub>3</sub>, ascorbic acid as the reducing agent and tetrabutylammonium bromide (TBABr) or tetrabutylphosphonium bromide (TBPBr) as ligand were shown to be enhanced in the presence of catalytic amounts of inorganic bases (NaOH, Na<sub>3</sub>PO<sub>4</sub>, NaHCO<sub>3</sub> and Na<sub>2</sub>CO<sub>3</sub>).

In a recent contribution, we have illustrated that simple inorganic salts [Cat<sup>+</sup>]<sub>n</sub>X<sup>n-</sup> (Cat<sup>+</sup> = alkali metal; X<sup>n-</sup> = chloride, bromide, iodide, carbonate, bicarbonate, sulfate, bisulfate, nitrate, hydroxide and hexafluorophosphate) are able, by themselves, to activate the typical ATRP initiator ethyl 2-bromo-phenylacetate (EBrPA) to produce the EPA<sup>•</sup> radical and a [Cat<sup>+</sup>]<sub>n</sub>(XBr)<sup>n-</sup> adduct, though this equilibrium does not provide a suitable persistent radical effect for a controlled polymerization of MMA.<sup>47</sup> We now report that addition of FeBr<sub>2</sub> to these systems affords a rapid MMA polymerization process, faster than the previously reported ones with more complex organic cations, yet with an equal or better level of

control. To the best of our knowledge, an activating effect for Fe<sup>II</sup> ATRP catalysts by fully inorganic salt additives, in the absence of other organic molecules or salts, has not previously been reported. These new and simpler polymerization conditions constitute a significant advance in terms of the practical application of ATRP, because they combine the use of a readily available, inexpensive and non-toxic metal with equally available and inexpensive inorganic salts as ligands. The application of these polymerization conditions to other monomers will also be briefly shown. Finally, we will also present simple but apparently unprecedented considerations on Fe<sup>II</sup> coordination chemistry that establish the role of the [FeBr<sub>3</sub>(MMA)]<sup>-</sup> complex as the active ATRP catalyst and help rationalize our results in comparison with those already available in the literature.

### Experimental section

**Materials.** Methyl methacrylate (MMA, 98+%, Sinpharm), Methyl acrylate (MA, 98+%, Sinpharm), Butyl acrylate (BA, 98+%, Sinpharm), Butyl methacrylate (BMA, 98+%, Sinpharm) was passed through a column filled with neutral alumina, dried over calcium hydride (CaH<sub>2</sub>), distilled under reduced pressure and stored in a freezer under argon. Ethyl  $\alpha$ -bromophenylacetate (EBrPA, 95%, Alfa Aesar), ethyl  $\alpha$ -bromoisobutyrate (EBriB, 98%, Alfa Aesar), methyl 2-bromoisobutyrate (MBriB, 95+%, Alfa Aesar), (1-bromoethyl)benzene (PEBr, 97%, Alfa Aesar), ethyl 2-bromopropionate (EBrP, 98%, Alfa Aesar), methyl 2-bromopropionate (MBrP, 98%, Alfa Aesar), 2-bromopropionitrile (BPN, 98%, Alfa Aesar), 2-Chloropropionitrile (CPN, 98%, Alfa Aesar). iron(II) bromide (FeBr<sub>2</sub>, 98+%, Alfa Aesar), iron(II) chloride (FeCl<sub>2</sub>, 98+%, Alfa Aesar), iron(II) chloride tetrahydrate (FeCl<sub>2</sub>·4H<sub>2</sub>O, 99.95%, Macklin), 2,2,6,6-Tetramethylpiperidine 1-oxyl (TEMPO, 98%, Sigma Aldrich) were used without further purification. Sodium carbonate (Na<sub>2</sub>CO<sub>3</sub>), sodium bicarbonate (NaHCO<sub>3</sub>), potassium carbonate (K<sub>2</sub>CO<sub>3</sub>), potassium bicarbonate (KHCO<sub>3</sub>), potassium hydroxide (KOH), sodium hydroxide (NaOH), trisodium phosphate (Na<sub>3</sub>PO<sub>4</sub>), disodium hydrogen phosphate (Na<sub>2</sub>HPO<sub>4</sub>), sodium dihydrogen phosphate (NaH<sub>2</sub>PO<sub>4</sub>), sodium sulfate (Na<sub>2</sub>SO<sub>4</sub>), potassium sulfate (K<sub>2</sub>SO<sub>4</sub>), rubidium sulfate (Rb<sub>2</sub>SO<sub>4</sub>), cesium sulfate (Cs<sub>2</sub>SO<sub>4</sub>), sodium nitrate (NaNO<sub>3</sub>), potassium nitrate (KNO<sub>3</sub>), sodium bisulfate (NaHSO<sub>4</sub>), lithium chloride (LiCl), sodium chloride (NaCl), potassium chloride (KCl), lithium bromide (LiBr), sodium bromide (NaBr), potassium bromide (KBr), rubidium bromide (RbBr), cesium bromide (CsBr), sodium iodide (NaI), potassium iodide (KI), tetra-*n*-butylammonium bromide (TBABr), magnesium chloride (MgCl<sub>2</sub>), calcium chloride (CaCl<sub>2</sub>), potassium hexafluorophosphate (KPF<sub>6</sub>) and lithium trifluoromethylsulfonate (LiOTf), all from Sinpharm, were also used as received. Laboratory Reagent grade ( $\geq$  99.5%) N,N-dimethylformamide and toluene were purchased from VWR Chemicals and used after distillation.

**Measurements.** <sup>1</sup>H NMR spectroscopy was performed using Bruker AV400, Avance III400 HD and Varian INOVA-400 MHz spectrometers with deuterated chloroform as the solvent and tetramethylsilane (TMS) as the standard. The M<sub>n</sub> and M<sub>w</sub>/M<sub>n</sub> of the polymers were determined by GPC using an Agilent 1100 gel permeation chromatograph equipped with a PLgel 79911GP-104 column (7.5 mm  $\times$  300 mm, 10  $\mu$ m bead size) or a Shimadzu system equipped with a Shimadzu RID-

20A refractive index detector and with two PSS SDV analytical columns (1000 Å and 100000 Å, 5  $\mu$ m, 8  $\times$  300 mm). THF was used as the eluent at a flow rate of 1 mL min<sup>-1</sup> at 35°C. Linear polystyrene standards were used for calibration.

**General polymerization procedure.** Unless otherwise stated, a typical system consisted of [monomer]<sub>0</sub>/[FeBr<sub>2</sub>]<sub>0</sub>/ [initiator]<sub>0</sub>/[inorganic salts]<sub>0</sub> = 200:1:1:2. A Schlenk flask (25 mL) was charged under argon with the salt and sealed by a rubber septum. Then the degassed monomer and initiator were added through degassed syringes. The solution was stirred for 20 min at room temperature. After three freeze-pump-thaw cycles, the flask was immersed in a thermostatic oil bath at the desired temperature. At timed intervals, samples were withdrawn from the flask with a degassed syringe. The monomer conversion was determined gravimetrically after the removal of the unconverted monomer under reduced pressure. The resulting residue was diluted with tetrahydrofuran (THF) and then filtered through a column filled with neutral aluminum oxide to remove any insoluble salt. The poly(methyl methacrylate) (PMMA) solution was then precipitated using an excess of *n*-hexane, and these polymers were dried under vacuum overnight at 80°C for gel permeation chromatography (GPC) characterization.

**Solubility measurements.** In a Schenk tube, neat MMA (3 mL, 2.82 g, 28.17 mmol) and the desired compound(s) (KBr, FeBr<sub>2</sub>, LiBr:FeBr<sub>2</sub> 1:1, KBr:FeBr<sub>2</sub> 1:1, or KBr:16-crown-6:FeBr<sub>2</sub> 1:1:1) were introduced with an MMA/Fe molar ratio of 200:1 (for instance, the amount of FeBr<sub>3</sub> was 30 mg (0.139 mmol)). The mixture was then stirred at 70°C for several hours, in order to reach thermal equilibrium for the solid dissolution process. It was then filtered hot through a filter-cannula into a new and pre-weighed Schlenk tube and the solution was then evaporated to dryness. The residue amount was obtained by weight difference.

**Computational details.** The computational work was carried out using the Gaussian09 suite of programs.<sup>48</sup> Gas-phase geometry optimizations were performed without any symmetry constraint using the BPW91\* functional, which is a reparametrized version of B3PW91 with the same parameters previously optimized for B3LYP.<sup>49</sup> This functional was shown to provide an accurate description of open-shell transition metal complexes, particularly those of Fe<sup>II</sup>.<sup>50</sup> Dispersion effects were taken into account with Grimme's D3 empirical method during optimization (BPW91\*-D3), using SR6 and S8 parameters identical to those optimized for B3PW91.<sup>51</sup> The 6-31G(d,p) basis functions were used for all light atoms (H, C, O). The Br atom was treated at three different levels. The lowest one is via same 6-31G(d,p) basis set as the light atoms. However, since a better description of anionic complexes with outer halogen atoms requires the addition of diffuse functions, a second level used the augmented basis set 6-31+G(d,p) for this atom. In a third level, the Br atom was described by the LANL208d basis,<sup>52</sup> which contains an ECP and a triple-zeta valence shell plus a d polarization function ( $\alpha = 0.434$ ) and a diffused p function ( $\alpha = 0.0376$ ). The Fe atom was treated with the SDD basis set augmented by an f polarization function ( $\alpha = 2.462$ )<sup>53</sup> in combination with the 6-31G(d,p) or 6-31+G(d,p) functions for Br, or with the LANL08(f) basis<sup>54</sup> in combination with the LANL208d basis for Br. The unrestricted formulation was used for the open-shell Fe<sup>II</sup> complexes, yielding only minor spin contamination ( $\langle S^2 \rangle$ ) at convergence was very close to the expected value of 6.0 for all quintet states, the

maximum deviation being 6.013 for  $[\text{FeBr}_2(\text{MMA})_2]$  with the LANL basis functions). The dinuclear  $[\text{Fe}_2\text{Br}_6]^{2-}$  was treated as the spin aligned  $S = 9$  state ( $\langle S^2 \rangle$  was in all cases 20.015 vs. the expected value of 20). All final geometries were characterized as local minima by verifying that all second derivatives of the energy were positive. Thermochemical corrections were obtained at 298.15 K on the basis of frequency calculations, using the standard approximations (ideal gas, rigid rotor and harmonic oscillator). Solvation effects in neat MMA were taken into account by treating the solvent medium as a polarizable continuum with the SMD approach,<sup>55</sup> using  $\epsilon = 6.534$  as the dielectric constant. A further correction of 1.95 Kcal mol<sup>-1</sup> was applied to bring the G values from the gas phase (1 atm) to the solution (1 mol L<sup>-1</sup>) standard state.<sup>56</sup>

## Results and discussion

### 1. Polymerizations with a bromide salt additive

We have recently shown that the MMA polymerization initiated by ethyl 2-bromo-phenylacetate (EBrPA) experiences an activating effect by a variety of inorganic salts.<sup>47</sup> The effect of the alkali metal bromides is reminded in Table 1 (compare entries 2-6 with entry 1). For instance, use of KBr gave 8.1% conversion after 18 h at 90°C (entry 4).<sup>47</sup> This activating effect was shown to involve atom transfer to yield the EPA' radical and a  $\text{Mt}^+(\text{Br}_2^-)$  deactivator (Mt = alkali metal), which is however incapable of providing a good enough persistent radical effect for a controlled chain growth. The more soluble TBABr yielded faster conversion (entry 7) but was equally incapable of controlling the polymerization. We now report that the addition of  $\text{FeBr}_2$  to these systems leads to a quite rapid and well-controlled chain growth, even at a lower temperature (70°C), with  $M_n$  close to target and low  $D$  for all metal systems, see entries 9-14. The polymerization rate is highly metal-dependent, with much slower conversions for the bromides of the heavier metals Rb and Cs (less than 20% conversion after 20 h, entries 12 and 13, whereas a 74.1% conversion was obtained in the presence of LiBr in 1 h (entry 9). Under these conditions, no monomer conversion was observed in the absence of bromide salt additive (entry 8). The effect of these alkali metal bromides on the  $\text{FeBr}_2/\text{EBrPA}$  action in bulk MMA polymerization is similar to that previously reported for several other bromide salts with large organic cations (tetraalkylammonium or -phosphonium,<sup>32, 36, 41, 42, 44, 45</sup> substituted imidazoliums<sup>33</sup> and phosphazanium<sup>35</sup>). The lighter alkali metal bromides (Li, Na, K), however, yield much faster polymerizations than the more soluble TBABr additive under the same operating conditions (entry 14).

The polymerizations carried out in the presence of LiBr, NaBr, KBr and TBABr were investigated in greater details, see Figure 1 (the raw data are available in Table S1; for all polymerization kinetics reported in this contribution, the  $k_{\text{obs}}$  values obtained from the fit of the 1<sup>st</sup> order plots are reported together with the raw data in the Supporting Information). All polymerizations are well-controlled, with linear first-order plots, linear  $M_n$  grown with conversion in close agreement with the theoretical molar masses, and low  $D$  values ( $\leq 1.25$ ). The  $k_{\text{obs}}$  values increase in the order TBA ( $8.7 \cdot 10^{-3}$ ) < K ( $1.16 \cdot 10^{-2}$ ) ~ Na ( $1.15 \cdot 10^{-2}$ ) < Li ( $2.17 \cdot 10^{-2}$ ), all values being in min<sup>-1</sup>. Although these polymerizations appear quite well-controlled, the presence of a significant degree of initial terminations is nevertheless suggested by the positive intercepts of the first-order kinetic plots. These terminations probably produce short chains that are lost during the polymer work-up for

the GPC analysis, thus the observed  $M_n$  values agree rather well with the theoretical ones. An improvement was achieved through addition of  $\text{FeBr}_3$  (vide infra).

The system with KBr as additive was selected for additional investigations. The radical nature of the polymerization process was proven by a polymerization run under the same conditions as in entry 11, but with addition of TEMPO 45 min after starting the reaction, when the conversion was 38.7%. Continued heating at 70°C for 2 h did not further increase the conversion (see SI, Figure S1 and Table S2). In addition, the <sup>1</sup>H NMR analysis of the recovered polymers from the experiments run in the presence of LiBr, NaBr and KBr showed identical mm:mr:rr ratios, within the integration error, to a PMMA obtained by free radical polymerization initiated by AIBN, see Figure S2. This result not only confirms the radical nature of the process, it also shows a negligible influence of the salt additive on the chain propagation stereochemical control. A chain extension experiment, carried out with the PMMA-Br product of entry 1 (Table 1) as macroinitiator, gave rise to a chain length increase in line with the expected target values, maintaining a monomodal distribution and a low dispersity (Table S3 and Figure S3). Polymerizations run in the presence of KBr and with dilution by a polar (DMF) or a non-polar (toluene) solvent (MMA:solvent (v/v) = 2:1) provide in both cases similar control but slower rates, as expected (Table S4 and Figure S4). At the polymerization temperature, the KBr salt is more soluble in the presence of DMF and less soluble in the presence of toluene, relative to the bulk monomer conditions.

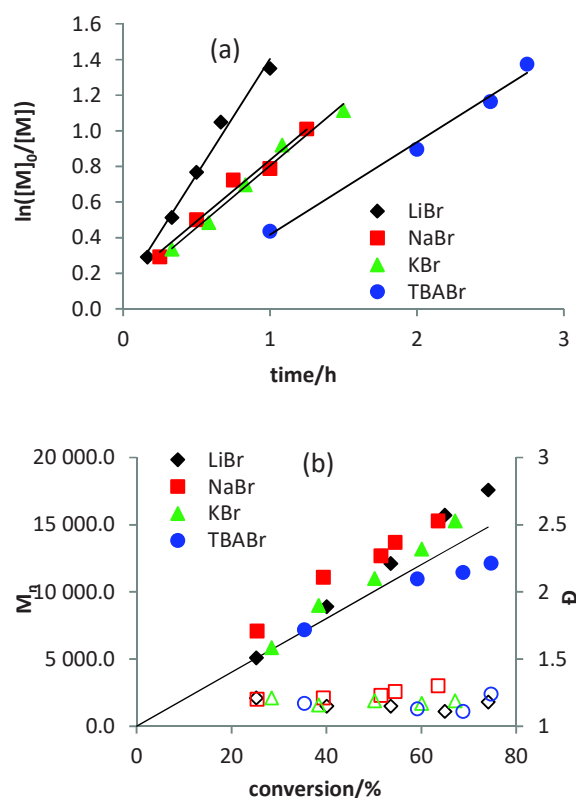


Figure 1. First-order plots (a) and evolution of  $M_n$  and  $D$  with conversion (b) for the bulk  $\text{FeBr}_2$ -catalyzed and EBrPA-initiated MMA polymerization in the presence of different bromide salts.  $[\text{MMA}]:[\text{FeBr}_2]:[\text{EBrPA}]:[\text{salt}] = 200:1:1:2$ ,  $T = 70^\circ\text{C}$ .

**Table 1. FeBr<sub>2</sub>-catalyzed MMA ATRP: effect of inorganic bromide salts.<sup>a</sup>**

	Initiator	Catalyst	Additive	T/°C	Time/h	Conv./%	M <sub>n</sub> ,th/g mol <sup>-1</sup>	M <sub>n</sub> ,GPC/g mol <sup>-1</sup>	Đ	Ref.
1	EBrPA	none	none	90	12.0	2.3	700	11400	1.37	47
2	EBrPA	none	LiBr	90	12.0	9.6	2200	26600	1.34	47
3	EBrPA	none	NaBr	90	12.0	13.0	2800	62600	1.71	47
4	EBrPA	none	KBr	90	18.0	8.1	1900	146800	2.16	47
5	EBrPA	none	RbBr	90	12.0	5.1	1300	20400	1.68	47
6	EBrPA	none	CsBr	90	12.0	4.8	1200	17800	1.76	47
7	EBrPA	none	TBABr	90	18.0	36.7	7600	655400	2.49	47
8	EBrPA	FeBr <sub>2</sub>	none	70	15.0	0.0	-	-	-	This work
9	EBrPA	FeBr <sub>2</sub>	LiBr	70	1.0	74.1	15100	17600	1.18	This work
10	EBrPA	FeBr <sub>2</sub>	NaBr	70	2.0	65.6	13400	15300	1.30	This work
11	EBrPA	FeBr <sub>2</sub>	KBr	70	1.5	67.2	13700	15200	1.19	This work
12	EBrPA	FeBr <sub>2</sub>	RbBr	70	12.0	19.9	4000	4600	1.17	This work
13	EBrPA	FeBr <sub>2</sub>	CsBr	70	12.0	6.3	1500	1700	1.15	This work
14	EBrPA	FeBr <sub>2</sub>	TBABr	70	2.75	74.7	15000	12100	1.24	This work

<sup>a</sup>Conditions: bulk polymerization, [MMA]:[FeBr<sub>2</sub>]:[EBrPA]:[Additive] = 200:1:1:2.

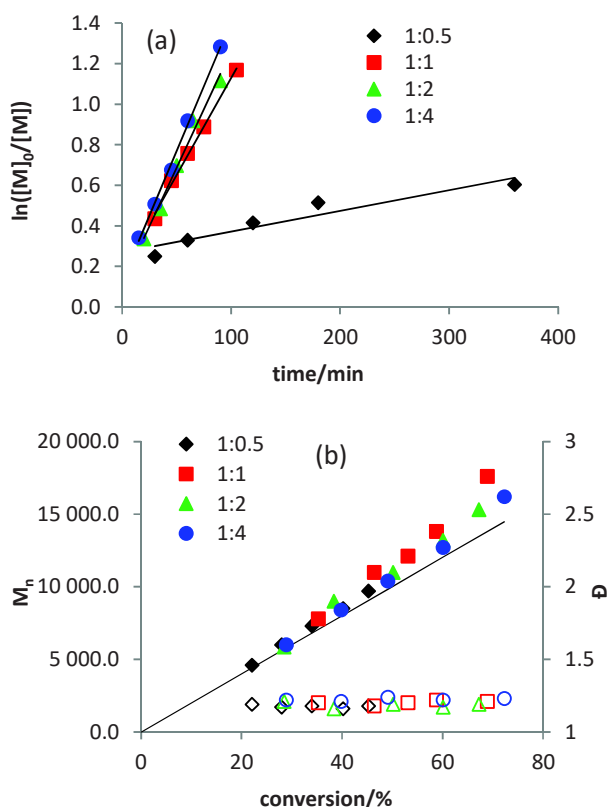


Figure 2. First-order plots (a) and evolution of  $M_n$  and  $\bar{D}$  with conversion (b) for the EBrPA-initiated bulk MMA polymerizations with FeBr<sub>2</sub> activation and different Fe<sup>II</sup>/KBr ratios.

The effect of the Fe<sup>II</sup>/KBr ratio is shown in Table S5 and Figure 2. Using only 0.5 equivalents of KBr relative to FeBr<sub>2</sub> resulted in a much slower rate ( $k_{\text{obs}} = 1.03 \cdot 10^{-3} \text{ min}^{-1}$ ) than with the stoichiometric amount ( $k_{\text{obs}} = 9.6 \cdot 10^{-3} \text{ min}^{-1}$ ) while the polymerization was still quite well-controlled. A further increase beyond the stoichiometric amount (2 and 4 equivalents)

did not have a large effect ( $k_{\text{obs}} = 1.2 \cdot 10^{-2}$  and  $1.3 \cdot 10^{-2} \text{ min}^{-1}$ , respectively), suggesting that the active species has a 1:1 FeBr<sub>2</sub>/KBr ratio. More specifically, as it will be discussed in the next section, the nature of the active catalyst appears to correspond to the tetrahedral monoanionic [Fe<sup>II</sup>Br<sub>3</sub>(MMA)]<sup>-</sup> complex.

Further polymerizations carried out with a variable monomer/Fe<sup>II</sup> ratio yielded polymers with target  $M_n$  values, scaling with the MMA/Fe ratio, always with  $\bar{D} < 1.25$  (Table S6 and Figure S5a). Interestingly, the polymerization rates also scale approximately with [FeBr<sub>2</sub>] (see Figure 3), which suggests that the catalyst is mostly or fully dissolved in the polymerization medium. Indeed, a solubility test shows that whereas FeBr<sub>2</sub> and KBr are only little soluble in neat MMA (saturated solutions at 70°C have respectively [FeBr<sub>2</sub>] = 0.012 mol L<sup>-1</sup> and [KBr] = 0.0098 mol L<sup>-1</sup>), the solubility increases substantially upon addition of KBr (1 equiv) to yield [KFeBr<sub>3</sub>] = 0.026 mol L<sup>-1</sup> for a saturated solution at 70°C. At the highest Fe<sup>II</sup>/MMA ratio (1:200, corresponding to a theoretical amount of 0.047 mol L<sup>-1</sup>), the mixture is supersaturated and indeed undissolved catalyst is initially observed in the polymerization mixture. However, homogeneous solutions were observed for the polymerizations carried out with 1:400, 1:600 and 1:800 ratios (corresponding to 0.0235, 0.0176 and 0.0117 mol L<sup>-1</sup>, respectively, *i.e.* lower than the experimentally measured concentration at saturation).

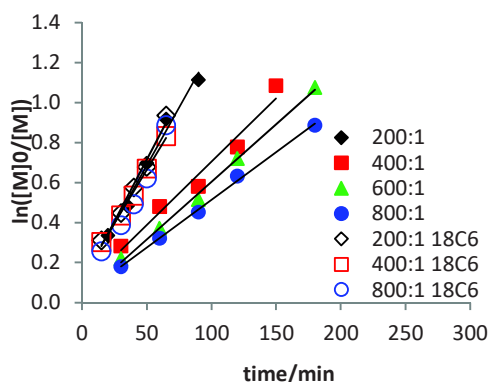


Figure 3. First-order plots the bulk  $\text{FeBr}_2$ -KBr-catalyzed and EBrPA-initiated MMA polymerization at  $70^\circ\text{C}$  with variable  $[\text{MMA}]:[\text{FeBr}_2]$  ratios and in the absence or presence of 18-crown-6 (18C6). Conditions:  $[\text{MMA}]:[\text{FeBr}_2]:[\text{EBrPA}]:[\text{KBr}]:[18\text{C6}] = x:1:1:2:y$  ( $x = 200, 400, 600, 800; y = 0$  or  $1$ ).

Additional polymerizations were also carried out under the same conditions, except for the presence of one equiv of 18-crown-6 (18C6) per KBr, which is known to strongly bind the  $\text{K}^+$  ion (Table S6). This complexing agent is also known to render potassium salts more lipophilic, generally increasing their solubility in organic solvents. However, unexpectedly, the resulting  $\text{K}(18\text{C6})\text{FeBr}_3$  turned out to be less soluble than  $\text{KFeBr}_3$ , as qualitatively indicated by the greater amount of undissolved catalyst and by the fainter color of the decanted solution. The concentration at saturation in neat MMA at  $70^\circ\text{C}$  was measured as  $0.017 \text{ mol L}^{-1}$ , *i.e.* ca. half the saturation concentration of  $\text{KFeBr}_3$ . The polymerizations run with this catalyst gave again a good first-order kinetic behavior, but the observed rate constants in this case were essentially independent on the MMA/Fe ratio (Figure 3). This is consistent with the fact that all polymerization mixtures are saturated in catalyst, even at the highest dilution ( $\text{MMA}/\text{Fe}^{\text{II}} = 800:1$ ). A further point of interest is that the observed rate constants for the  $\text{K}(18\text{C6})\text{FeBr}_3$ -catalyzed polymerization are greater than for the  $\text{KFeBr}_3$ -catalyzed polymerizations run at the same MMA/Fe ratio, even though the catalyst concentration is lower and reaching approximately equal  $k_{\text{obs}}$  values only at the highest dilution. This reveals a critical role of the cation in the regulation of the ATRP equilibrium (see further discussion below). The ATRP catalyzed by the  $\text{K}(18\text{C6})\text{FeBr}_3$  system is not only faster, but also better-controlled, than that catalyzed by  $\text{KFeBr}_3$ , with  $\bar{D}$  values down to 1.03 (Figure S5b).

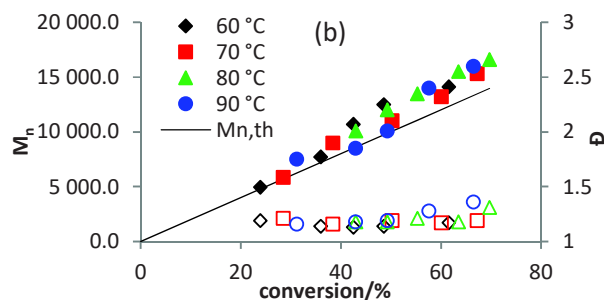
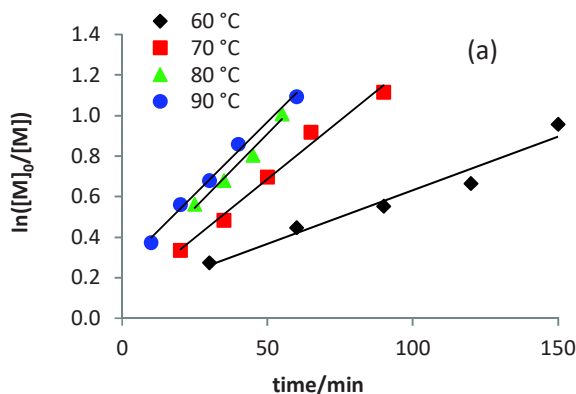
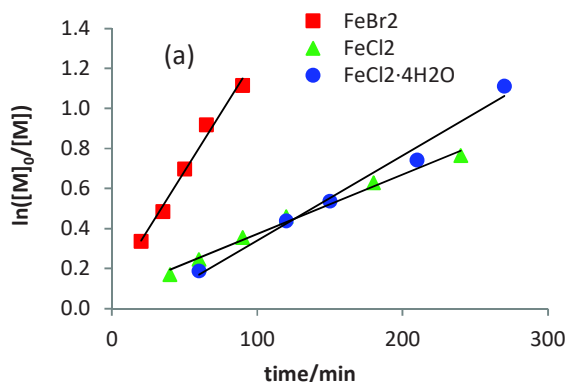


Figure 4. First-order plots (a) and evolution of  $M_n$  and  $\bar{D}$  with conversion (b) for the bulk  $\text{FeBr}_2$ -KBr-catalyzed and EBrPA-initiated MMA polymerization at different temperatures.  $[\text{MMA}]:[\text{FeBr}_2]:[\text{EBrPA}]:[\text{KBr}] = 200:1:1:2$ .

Exploration of the temperature effect for the polymerization run with a MMA/Fe ratio of 200 showed a significant rate decrease when lowering T from  $70$  to  $60^\circ\text{C}$ , whereas the rate did not significantly increase at higher temperatures, see Table S7 and Figure 4. This phenomenon can be attributed to the higher impact, at higher temperatures, of terminations in the initial phase of the process, resulting in a significant decrease of the chain carriers. This is also indicated by the greater positive intercept of the first-order plot in Figure 4a. On the other hand, the level of control remained quite acceptable under all conditions, with  $M_n$  values quite close to target and  $\bar{D} < 1.3$ . Thus,  $70^\circ\text{C}$  appears as the most suitable polymerization temperature and was maintained for the additional studies.

A screening of the polymerization using different initiators showed slow initiation for several of them (e.g. CPN, MBrP, EBrP, PEBr), as evidenced by the presence of an induction time (negative intercept in the first-order kinetic plot) and/or by lower  $k_{\text{obs}}$  in the kinetics plot (see Table S8 and Figure S6), as well as by greater molar masses than the target values in the  $M_n$  vs. conversion plot. On the other hand, EBrPA, EBiB and MBiB gave the highest and reasonably similar polymerization rates, with  $M_n$  values close to target. These results are in line with the common knowledge that only the fastest initiators, which yield more stabilized radicals and are associated with a greater  $K_{\text{ATRP}}$  (Scheme 1), are suitable for the polymerization of MMA.<sup>57-59</sup> The investigations were therefore continued with EBrPA as initiator.



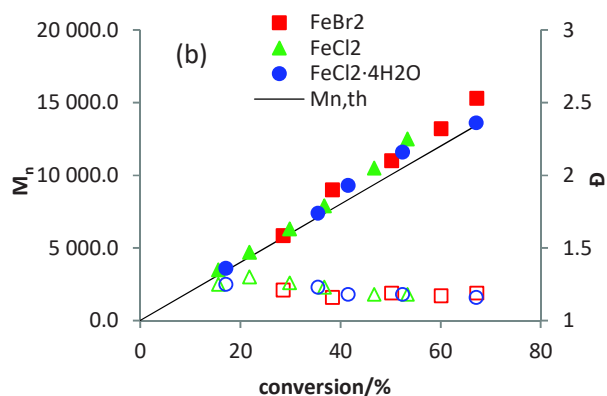


Figure 5. First-order plots (a) and evolution of  $M_n$  and  $D$  with conversion (b) for the EBrPA-initiated bulk MMA polymerizations ( $[MMA]:[MtX_2]:[EBrPA]:[KBr] = 200:1:1:2$ ) using different metal catalysts at 70°C ( $MtX_2 = FeBr_2, FeCl_2, FeCl_2 \cdot 4H_2O$ ).

A brief investigation of different Fe<sup>II</sup> catalysts for the standard EBrPA-initiated bulk polymerization in the presence of 2 equivalents of KBr has given the results shown in Table S9 and Figure 5. The polymerization is much faster with FeBr<sub>2</sub> than with FeCl<sub>2</sub>. Use of the hydrated form of the chloride salt, FeCl<sub>2</sub>·4H<sub>2</sub>O, did not significantly affect the polymerization rate, but shows a small induction time (negative intercept of the first-order kinetic plot), possibly related to the need to replace the coordinated water molecules in order to obtain the catalytically active species. All polymerizations are equally well-controlled (Figure 5b). A comparison of rates between the FeCl<sub>2</sub>- and FeBr<sub>2</sub>-catalyzed ATRP of MMA was also previously made in the presence of the phosphazene halides  $[(Me_2N)_2P=N]_{y_4}P^+X^-$  ( $X = Cl, Br$ ),<sup>35</sup> although based only on a single point measurement rather than on kinetics studies. All FeX<sub>2</sub>/Y<sup>-</sup> combinations ( $X, Y = Cl, Br$ ) gave rather similar and much slower rates (ca. 75-90% conversions in 72 h at 60°C) relative to those of Figure 5. The greater dependence on the nature of the iron salt in our study may be related to the lower solubility of  $K^+[Fe^{II}Cl_2Br(MMA)]^-$  relative to  $K^+[Fe^{II}Br_3(MMA)]^-$ , while the two salts may have comparable solubility when associated to the large phosphazene cation. The rest of the study was therefore limited to FeBr<sub>2</sub> as catalyst.

A significant improvement of the polymerization control, while retaining a quite rapid monomer conversion, could be achieved by introduction of a small amount of FeBr<sub>3</sub> deactivator (0.1 equivalents relative to the FeBr<sub>2</sub> activator). The results for the three lighter alkali metal salts are provided in Table S10 and Figure 6. The improved quality can immediately be assessed by the lower dispersity values, which decrease to < 1.1 at high conversions. A reduced degree of initial terminations, as expected when working in the presence of deactivator, is indicated by the close-to-zero intercepts. A more detailed comparison of the polymerization kinetics for each bromide salt is shown in the SI (Figure S7).

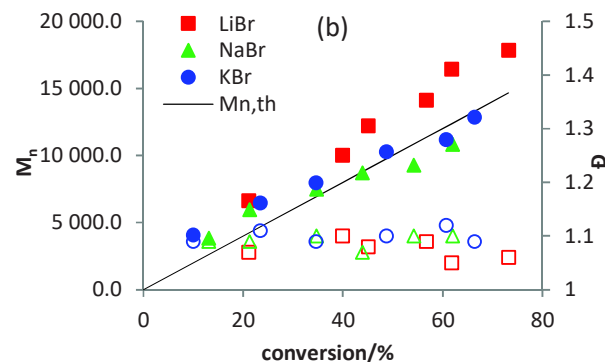
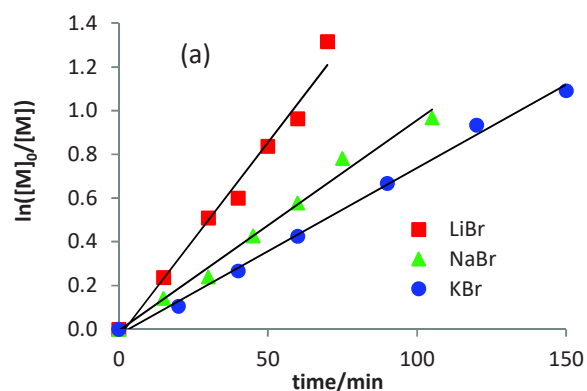


Figure 6. First-order plots (a) and evolution of  $M_n$  and  $D$  with conversion (b) for the EBrPA-initiated bulk MMA polymerizations with FeBr<sub>2</sub>-MtBr activation ( $Mt = Li, Na, K$ ) in the presence of FeBr<sub>3</sub> ( $[MMA]:[FeBr_2]:[FeBr_3]:[EBrPA]:[MtBr] = 200:1:0.1:1:2$ ) at 70°C.

In each case, the first order plot obtained in the presence of FeBr<sub>3</sub> shows an equally good or better linear correlation and an intercept much closer to zero, relative to the corresponding plot obtained in the absence of FeBr<sub>3</sub>. The  $k_{obs}$  values are not greatly reduced by the FeBr<sub>3</sub> presence because of the lower impact of initial terminations. Indeed, a significant amount of FeBr<sub>3</sub> is also generated by terminations in the polymerizations run without the initial addition of this reagent. For instance, the faster LiBr system gives a  $k_{obs}$  value of  $2.17 \cdot 10^{-2} \text{ min}^{-1}$  in the absence of initial Fe<sup>III</sup> and  $1.78 \cdot 10^{-2} \text{ min}^{-1}$  in the presence of Fe<sup>III</sup>. Finally, the KBr system was also tested in the presence of deliberately added water. In the presence of only 2 equivalents per FeBr<sub>2</sub>, a slight induction time is observed as indicated by the negative intercept of the 1<sup>st</sup> order plot and the rate slightly increased ( $8.6 \cdot 10^3 \text{ min}^{-1}$ , vs.  $7.6 \cdot 10^3 \text{ min}^{-1}$ , see Table S10 and Figure S8), although these effects are very small. Note that the same phenomenon was also pointed out above when comparing the kinetics of the polymerization catalyzed by FeCl<sub>2</sub> and FeCl<sub>2</sub>·4H<sub>2</sub>O. This result allows us to conclude that different rates observed for the salts with different cations do not originate from random differences in the hydration of the various additives, which had been nonetheless obtained commercially as anhydrous materials and stored in the dry box. When using, however, a much larger excess of water (60 equivalents per FeBr<sub>2</sub>), the polymerization became much slower (Table S10 and Figure S8), as a consequence of the decreased catalyst solubility as evidenced by the formation of an oily deposit. A similar rate decrease upon addition of

water was also observed for the EBrPA-initiated ATRP of MMA in anisole.<sup>45</sup>

## 2. Nature of the catalytically active species for the FeBr<sub>2</sub>/Br<sup>-</sup> system.

Dissolution of FeBr<sub>2</sub> in non-ionizing donor solvents is likely to generate neutral 4-coordinate Fe<sup>II</sup>Br<sub>2</sub>L<sub>2</sub> complexes (L = solvent molecule), as suggested by the X-ray structures of several Fe<sup>II</sup>X<sub>2</sub>L<sub>2</sub> complexes (X = Cl, Br, I),<sup>60-64</sup> including two unpublished structures (DIZXUH and NENWEK) in the Cambridge Crystallographic Structural Database (CCSD), whereas ionizing solvents that generate cationic complexes give rise to 5- or 6-coordinated complexes. For the bulk polymerization of MMA, the monomer itself is likely to assume the ligand role via the more donating carbonyl O lone pair, therefore generating the tetrahedral complex FeBr<sub>2</sub>(MMA)<sub>2</sub>. The bromide anion is known to add to FeBr<sub>2</sub> to yield tetrahedral [Fe<sup>II</sup>Br<sub>4</sub>]<sup>2-</sup> when used in large excess in a polar solvent,<sup>65</sup> whereas use of a stoichiometric amount yields a monoanionic tetrahedral [FeBr<sub>3</sub>L]<sup>-</sup> adduct in the presence of neutral donors L. Complexes of this kind have been isolated and fully characterized, in combination with various cations, for L = THF,<sup>66, 67</sup> N-heterocyclic carbenes,<sup>66</sup> or tertiary phosphine (PR<sub>3</sub>).<sup>68, 69</sup> In the absence of sufficiently donating ligands, the dinuclear dibromo-bridged complex [Fe<sub>2</sub>Br<sub>6</sub>]<sup>2-</sup> ion may also be generated. The latter is yet unreported in discrete molecular systems, but was observed in the crystal structure of KFeBr<sub>3</sub>.<sup>70</sup> Therefore, the controlling equilibrium in bulk MMA probably involves the tetrahedral [FeBr<sub>3</sub>(MMA)]<sup>-</sup> catalyst as activating species and the known<sup>65</sup> tetrabromoferrate(III) ion, [Fe<sup>III</sup>Br<sub>4</sub>]<sup>-</sup> as deactivator (It is of interest to compare our experimental results for the polymerization rate as a function of Br<sup>-</sup>/FeBr<sub>2</sub> ratio with those reported in the literature. For our FeBr<sub>2</sub>/KBr system, the amount of bromide salt does not affect the rate when added in greater amounts than 1 equivalent per FeBr<sub>2</sub> (Figure 2). On the other hand, Matyjaszewski *et al.*<sup>32</sup> have shown that the rate of the FeBr<sub>2</sub>/[*n*Bu<sub>4</sub>E]Br-catalyzed (E = N, P) MMA polymerization (as well as those of styrene and MA) decreases upon increasing the salt/FeBr<sub>2</sub> ratio. This behavior is consistent with the greater ability of the more soluble TBABr to displace the coordination equilibrium towards the [Fe<sup>II</sup>Br<sub>4</sub>]<sup>2-</sup> species (*K*<sub>2</sub> in **Erreur ! Référence non valide pour un signet.**), thus reducing the available amount of the active tricoordinated [FeBr<sub>3</sub>]<sup>-</sup> complex. The less soluble KBr, on the other hand, does not provide a sufficient mass effect to accomplish this transformation, while being able to produce K[FeBr<sub>3</sub>(MMA)]<sup>-</sup> extensively via equilibrium *K*<sub>1</sub> in **Erreur ! Référence non valide pour un signet.**. In this respect, as shown in the previous section, the solubility of KFeBr<sub>3</sub> is greater than that of FeBr<sub>2</sub> and much greater than that of KBr.

Scheme 2). The weak coordinating power of MMA insures its rapid dissociation during the atom transfer activation process.

It is of interest to compare our experimental results for the polymerization rate as a function of Br<sup>-</sup>/FeBr<sub>2</sub> ratio with those reported in the literature. For our FeBr<sub>2</sub>/KBr system, the amount of bromide salt does not affect the rate when added in greater amounts than 1 equivalent per FeBr<sub>2</sub> (Figure 2). On the other hand, Matyjaszewski *et al.*<sup>32</sup> have shown that the rate of the FeBr<sub>2</sub>/[*n*Bu<sub>4</sub>E]Br-catalyzed (E = N, P) MMA polymerization (as well as those of styrene and MA) decreases upon increasing the salt/FeBr<sub>2</sub> ratio. This behavior is consistent with the greater ability of the more soluble TBABr to displace the

coordination equilibrium towards the [Fe<sup>II</sup>Br<sub>4</sub>]<sup>2-</sup> species (*K*<sub>2</sub> in **Erreur ! Référence non valide pour un signet.**), thus reducing the available amount of the active tricoordinated [FeBr<sub>3</sub>]<sup>-</sup> complex. The less soluble KBr, on the other hand, does not provide a sufficient mass effect to accomplish this transformation, while being able to produce K[FeBr<sub>3</sub>(MMA)]<sup>-</sup> extensively via equilibrium *K*<sub>1</sub> in **Erreur ! Référence non valide pour un signet.**. In this respect, as shown in the previous section, the solubility of KFeBr<sub>3</sub> is greater than that of FeBr<sub>2</sub> and much greater than that of KBr.

## Scheme 2. Moderating ATRP equilibrium by FeBr<sub>2</sub> in the presence of bromide salts.

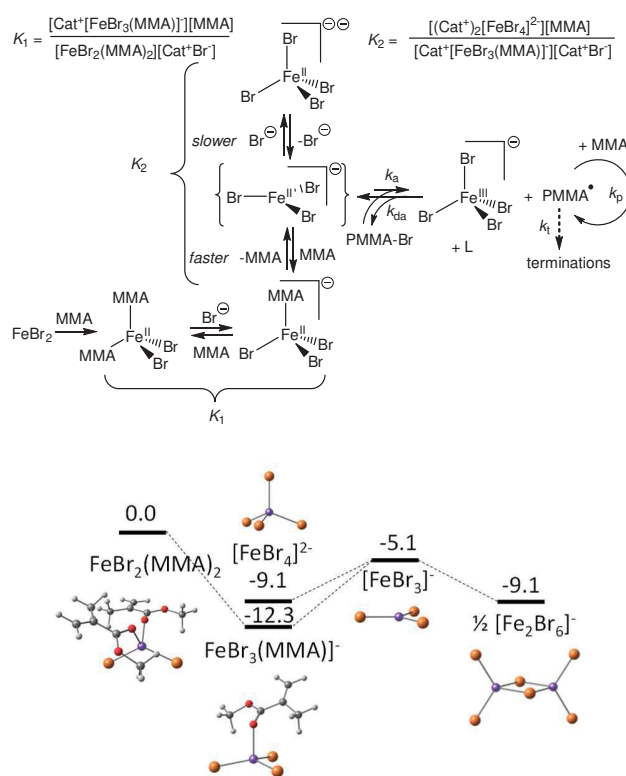


Figure 7. DFT-calculated Gibbs energy changes (in kcal mol<sup>-1</sup>), for the addition of the bromide ion to complex [FeBr<sub>2</sub>(MMA)<sub>2</sub>], obtained using the 6-31+G\*\* basis set for the Br atom.

In order to further substantiate the above propositions, calculations of equilibria involving MMA and Br<sup>-</sup> coordination to FeBr<sub>2</sub> were conducted by the DFT approach to obtain relative Gibbs energies in the standard state (298 K, 1 mol L<sup>-1</sup>) in MMA solution, using a polarizable continuum model to take solvation effects into account, but did not consider the interaction with the cation (see the Experimental section for details). All calculations were carried out for the high-spin (*S* = 2) configuration, as experimentally established for coordination compounds of FeBr<sub>2</sub> with weak field ligands.<sup>71</sup> The more reliable results obtained with the higher quality 6-31+G\*\* basis set for the Br atom are summarized in Figure 7 (other computational results are compared in the SI section, see Figure S9 and related discussion). The starting [FeBr<sub>2</sub>(MMA)<sub>2</sub>] complex, which serves as a reference point, optimized to a tetrahedral geometry as expected. Exchange of one MMA ligand with bromide, yielding the anionic [FeBr<sub>3</sub>(MMA)]<sup>-</sup> complex, provides a stabilization of 12.3 kcal mol<sup>-1</sup>. The



MMA coordination is quite weak, since dissociation to yield the putative tricoordinated  $[\text{FeBr}_3]^-$  costs only  $7.2 \text{ kcal mol}^{-1}$ . Weak MMA coordination is also clearly indicated by the optimized geometry, with a relatively long Fe-O distance and a flattened  $\text{FeBr}_3^-$  moiety (see the optimized parameters in Table S11 and discussion in the SI). The unsaturated  $[\text{FeBr}_3]^-$  intermediate can be stabilized by coordination of an additional bromide ion with a gain of  $4.0 \text{ kcal mol}^{-1}$  or by dimerization with the same Gibbs energy gain, but these are not as effective as the stabilization by MMA coordination. Thus, the most stable structure in the  $\text{FeBr}_2/\text{MMA}/\text{Br}^-$  system, even in the presence of excess bromide, is suggested by these calculations to be the anionic  $[\text{FeBr}_3(\text{MMA})]^-$  complex. To the best of our knowledge, none of the previously reported investigations on  $\text{FeX}_2\text{-X}^-$  catalyzed ATRP ( $\text{X} = \text{Cl}, \text{Br}$ ) have provided concrete evidence of the nature of the catalytically active species, nor made the proposition that this may be a monoanionic  $[\text{FeX}_3(\text{L})]^-$  complex.

The key action of the bromide anion in promoting the  $\text{FeBr}_2$  catalytic activity can be understood on the basis of the computational results:  $\text{Br}^-$  coordination labilizes the MMA ligand, thus kinetically helping its dissociation, which is needed during the atom transfer activation. This rationalizes the greater catalytic activity of  $[\text{FeBr}_3(\text{MMA})]^-$  relative to the neutral  $[\text{FeBr}_2(\text{MMA})_2]$  complex. The calculations suggest that the  $[\text{FeBr}_3]^-$  intermediate is better stabilized by MMA coordination, yielding complex  $[\text{FeBr}_3(\text{MMA})]^-$  back, than by additional  $\text{Br}^-$  to yield  $[\text{FeBr}_4]^{2-}$ , although this relative stabilization is very sensitive to the computational level (see SI) and we should also underline that the effect of ion pairing with the cation was not considered in the calculations. Ion pairing indeed appears to have a significant effect, as shown by the much faster  $k_{\text{obs}}$  in the presence of the much less soluble  $\text{K}(18\text{C}6)^+$  salt. As is well-established,<sup>1-9</sup>  $k_{\text{obs}}$  is proportional to  $k_p$ , to  $K_{\text{ATRP}} (= k_a/k_{\text{da}})$ , and to the  $[\text{Fe}^{\text{II}}]/[\text{Fe}^{\text{III}}]$  ratio (all constants are defined in It is of interest to compare our experimental results for the polymerization rate as a function of  $\text{Br}^-/\text{FeBr}_2$  ratio with those reported in the literature. For our  $\text{FeBr}_2/\text{KBr}$  system, the amount of bromide salt does not affect the rate when added in greater amounts than 1 equivalent per  $\text{FeBr}_2$  (Figure 2). On the other hand, Matyjaszewski *et al.*<sup>32</sup> have shown that the rate of the  $\text{FeBr}_2/[\text{mBu}_4\text{E}]\text{Br}$ -catalyzed ( $\text{E} = \text{N}, \text{P}$ ) MMA polymerization (as well as those of styrene and MA) decreases upon increasing the salt/ $\text{FeBr}_2$  ratio. This behavior is consistent with the greater ability of the more soluble TBABr to displace the coordination equilibrium towards the  $[\text{Fe}^{\text{II}}\text{Br}_4]^{2-}$  species ( $K_2$  in **Erreur ! Réf rence non valide pour un signet.**), thus reducing the available amount of the active tricoordinated  $[\text{FeBr}_3]^-$  complex. The less soluble KBr, on the other hand, does not provide a sufficient mass effect to accomplish this transformation, while being able to produce  $\text{K}[\text{FeBr}_3(\text{MMA})]^-$  extensively via equilibrium  $K_1$  in **Erreur ! Réf rence non valide pour un signet.** In this respect, as shown in the previous section, the solubility of  $\text{KFeBr}_3$  is greater than that of  $\text{FeBr}_2$  and much greater than that of KBr.

Scheme 2). The propagation rate constant  $k_p$  is not affected by the catalyst nature and it is hard to believe that the presence of crown ether reduces dramatically the generation of the  $\text{Fe}^{\text{III}}$  deactivator. Therefore, it is likely that the cation strongly affects the ATRP equilibrium position. A low permittivity medium such as neat MMA most probably does not allow the extensive generation of free ions, hence the catalyst is likely to be mostly present in the form of ion pairs. The ion pairing in

$\text{K}^+[\text{Fe}^{\text{II}}\text{Br}_3(\text{MMA})]^-$  and  $\text{K}^+[\text{Fe}^{\text{III}}\text{Br}_4]^-$  (where  $\text{K}^+$  is probably surrounded by a number of MMA molecules) must therefore energetically stabilize the  $\text{Fe}^{\text{II}}$  species, relatively to the  $\text{Fe}^{\text{III}}$  species, to a greater extent than the ion pairing in  $\text{K}(18\text{C}6)^+[\text{Fe}^{\text{II}}\text{Br}_3(\text{MMA})]^-$  and  $\text{K}(18\text{C}6)^+[\text{Fe}^{\text{III}}\text{Br}_4]^-$ .

### 3. Polymerizations with salts of other anions.

The effect of additional inorganic salts, representative of those used in our recent study of EBrPA activation, were also tested in combination with  $\text{FeBr}_2$ . The results with the lighter alkali metal chlorides, run in the presence of 0.1 equivalents of  $\text{FeBr}_3$ , are shown in Figure 8 (raw data in Table S13). As for the corresponding light alkali metal bromides, the chlorides yield well controlled polymerizations with relatively similar  $k_{\text{obs}}$  to those of the corresponding bromides. The lithium salt gives once again the fastest polymerization, but the K system is in this case faster than the Na one and almost as fast as the Li one. The polymerizations run in the absence of  $\text{FeBr}_3$  show the same phenomena already discussed above for the bromide system (non-zero intercept,  $k_{\text{obs}}$  close to those measured with  $\text{FeBr}_3$ , see Figure S10). A kinetic experiment was also run in the presence of  $\text{CaCl}_2$ , but only in the absence of  $\text{FeBr}_3$ , yielding a slightly slower polymerization but still with good control (Figure S11). The corresponding polymerization with  $\text{MgCl}_2$ , run under the same conditions was even slower (21.7% conversion after 1.5 h) but still gave a quite well-controlled process ( $M_n = 4900 \text{ g mol}^{-1}$  vs. a theoretical molar mass of  $4345 \text{ g mol}^{-1}$ , with  $\bar{D} = 1.17$ ). In these polymerization, it is likely that the mixed halide  $[\text{Fe}^{\text{II}}\text{ClBr}_3]^-$  deactivator, resulting from the activation of the bromine-terminated chains by  $[\text{Fe}^{\text{II}}\text{ClBr}_2]^-$ , produces chlorine-terminated chains, similar to what was shown in the polymerization of MMA from a Br-terminated PMA macroinitiator when using  $\text{Cu}^+\text{Cl}$  as catalyst.<sup>72</sup>

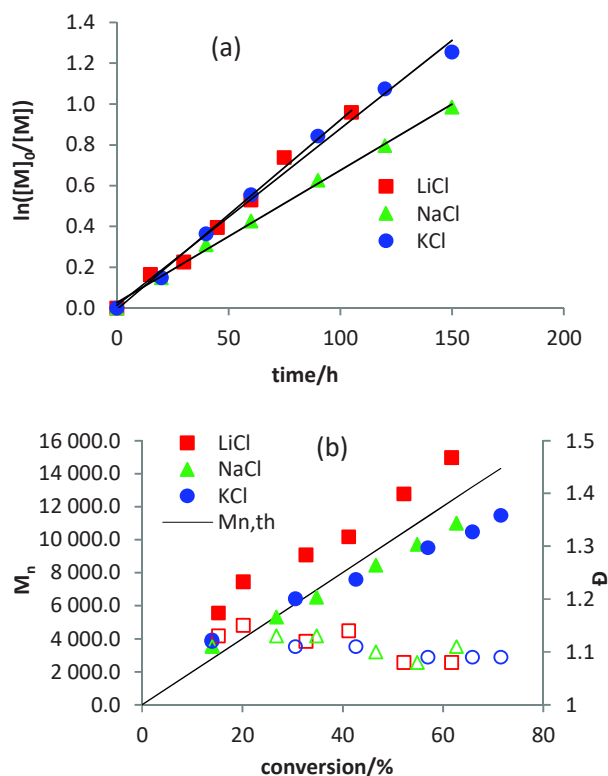


Figure 8. First-order plots (a) and evolution of  $M_n$  and  $\mathcal{D}$  with conversion (b) for the EBrPA-initiated bulk MMA polymerizations with  $\text{FeBr}_2$ -MtCl activation (Mt = Li, Na, K) in the presence of  $\text{FeBr}_3$  ([MMA]:[ $\text{FeBr}_2$ ]:[ $\text{FeBr}_3$ ]:[EBrPA]:[MtCl] = 200:1:0.1:1:2) at 70°C.

Controlled polymerizations were also observed in the presence of iodide salts (NaI and KI), with slightly lower  $k_{\text{obs}}$  than those of the corresponding chlorides and bromides. The data are collected in Table S14 and Figure S12. The observed rate constants for the three halides (Cl, Br, I), measured in the absence of  $\text{FeBr}_3$ , are respectively (in  $10^3 \text{ min}^{-1}$ ): 6.9, 11.5 and 5.9 for the Na salts, 6.4, 11.6 and 4.7 for the K salts, and 10.5 and 21.7 for the Li chloride and bromide. Note, however, that a comparison of these rates is not very meaningful because the observed rate constants are affected by the extent of initial terminations, producing  $\text{FeBr}_3$ , as well as by halide exchange.<sup>47</sup> The presence of salts with non-coordinating anions ( $\text{KPF}_6$  and  $\text{LiOTf}$ ) polymerizations led to significantly slower polymerizations (Table S15 and Figure S13), though faster than the  $\text{FeBr}_2$  control without additives (Table 1, entry 8), and proceeded again with quite good control. For instance, lithium triflate system gave a 35% conversion after 6 h at 70°C, using again bulk conditions with an MMA/ $\text{FeBr}_2$ /EBrPA/LiOTf molar ratio of 200:1:1:2. This demonstrates that even these weakly coordinating anions are able to interact with  $\text{FeBr}_2$  and provide more active ATRP catalysts. Given the relative low rates of these processes, they were not optimized by addition of  $\text{FeBr}_3$ . Polymerizations run in the presence of weakly coordinating anions have been previously reported, but only in polar solvents.<sup>25</sup> The alkali metal sulfates gave even slower (in the order Na > K > Rb > Cs) and more poorly controlled polymerizations, requiring 12 h to reach a 50 % monomer consumption at 90 °C for the faster  $\text{Na}_2\text{SO}_4$  system, see Table S15. Finally, the polymerizations run in the presence of  $\text{NaNO}_3$ ,  $\text{KNO}_3$  and  $\text{NaHSO}_4$  as additives gave no conversion whatsoever. In these cases, the polymerization mixtures showed a rapid color change, suggesting that the  $\text{FeBr}_2$  catalyst undergoes oxidation to  $\text{Fe}^{\text{III}}$ . This was confirmed by a UV-visible study, see Figure S14. Thus, no polymerization may occur because the activator is quantitatively converted into the deactivator. Oxidation of  $\text{Fe}^{\text{II}}$  by nitrate salts is not surprising, since  $\text{Fe}^{\text{II}}$  nitrate is known to autodecompose to  $\text{Fe}^{\text{III}}$  products at high temperatures.<sup>73</sup> Oxidation by  $\text{NaHSO}_4$  contrasts with the stability in the presence of the corresponding sulfate and may be attributed to the increase of the sulfate oxidizing ability in a more acidic environment.

#### 4. Polymerizations with inorganic bases

Investigations were also conducted in the presence of inorganic bases, comprising hydroxides (NaOH, KOH), carbonates ( $\text{Na}_2\text{CO}_3$ ,  $\text{K}_2\text{CO}_3$ ), bicarbonates ( $\text{NaHCO}_3$ ,  $\text{KHCO}_3$ ) and the sodium phosphates ( $\text{Na}_3\text{PO}_4$ ,  $\text{Na}_2\text{HPO}_4$  and  $\text{NaH}_2\text{PO}_4$ ). These studies were motivated by the established promoting effect of inorganic bases in  $\text{FeX}_2$ -catalyzed ATRP processes (X = Cl, Br), although all published contributions involved the simultaneous presence of other ligands, *e.g.* TBABr for the NaOH- and  $\text{Fe}(\text{OH})_3$ -promoted AGET bulk polymerization of styrene<sup>39</sup> as well as for the NaOH, BMImOH,  $\text{Na}_2\text{CO}_3$ ,  $\text{NaHCO}_3$ , or  $\text{Na}_3\text{PO}_4$ -promoted AGET bulk polymerization of MMA,<sup>42, 44</sup> and deep eutectic solvents for the  $\text{Na}_2\text{CO}_3$ -promoted MMA ATRP.<sup>31</sup> In the latter case, the solvent itself may play a ligand role. It is also relevant to note that, in a single case, the promoting effect of bases in the absence of any

other ligand was highlighted for the AGET MMA bulk polymerization. However, that investigation used bases containing an organic cation: BMImOH,  $(\text{BMIm})_2\text{CO}_3$ ,  $(\text{BMim})\text{HCO}_3$  and  $(\text{BMim})_3\text{PO}_4$ .<sup>43</sup> It was therefore of interest to verify whether purely inorganic bases may be able to promote, by themselves, the catalytic activity of  $\text{FeBr}_2$  for the bulk MMA ATRP.

Initial experiments carried out without any additional  $\text{FeBr}_3$  at the slightly lower temperature of 60°C gave, as for the above-described polymerization with other inorganic salts, high polymerization rates and good control, with  $M_n$  close to target and low  $\mathcal{D}$  in all cases (Table S16 and Figure S15). The  $k_{\text{obs}}$  is highest with NaOH ( $8.6 \cdot 10^{-3} \text{ min}^{-1}$ ), but all hydroxides, carbonates and bicarbonates gave relatively fast polymerizations. The phosphate systems are slower, in the order  $\text{Na}_3\text{PO}_4 > \text{Na}_2\text{HPO}_4 > \text{NaH}_2\text{PO}_4$ . In addition,  $\text{Na}_3\text{PO}_4$  showed an induction phenomenon. Tests with variable  $\text{FeBr}_2$ /base ratios were conducted for the  $\text{Na}_2\text{CO}_3$  system yielding, like for the KBr system, an increase of polymerization rate up to a 1:1 molar ratio and subsequent stagnation (Table S17 and Figure S16). This suggests that the active species for the carbonate system is again a 1:1 complex. The presence of small amounts of water (2 equivalents per  $\text{FeBr}_2$ ) has a weak effect on the polymerization rate, although more significant than in the case of the  $\text{FeBr}_2$ -KBr system discussed above, whereas using 60 equivalents of water greatly reduced the rate, for the same reason (precipitation of the iron catalyst), see Table S16 and Figure S17.

The experiments with the Na and K hydroxide, carbonate and bicarbonate were repeated in the presence of 0.1 equivalent of  $\text{FeBr}_3$ , yielding the results shown in Table S18 and Figure 9. All bases gave similar polymerization rates ( $k_{\text{obs}}$  in the narrow 0.0025-0.004  $\text{min}^{-1}$  range) and a better control relative to the corresponding experiments in which  $\text{FeBr}_3$  was not initially present, with dispersities around 1.1 or lower.

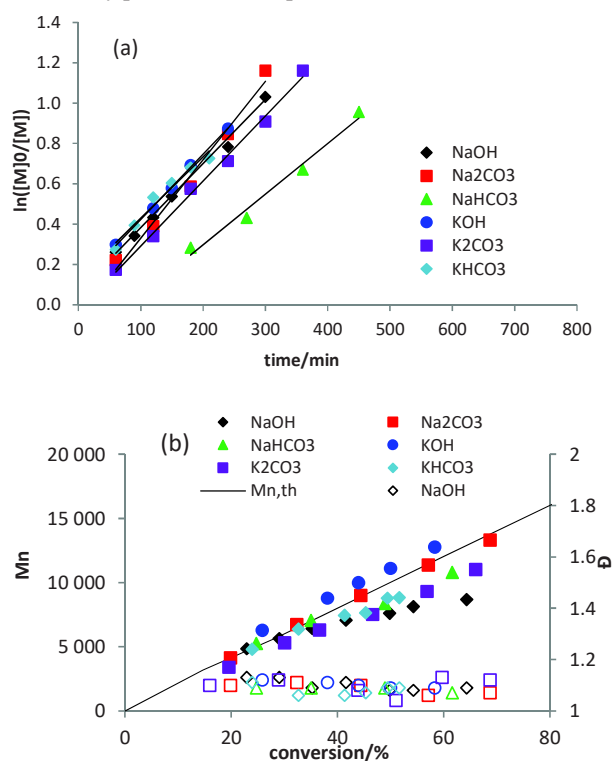


Figure 9. First-order plots (a) and evolution of  $M_n$  and  $\mathcal{D}$  with conversion (b) for the EBrPA-initiated bulk MMA polymerizations with FeBr<sub>2</sub>-base activation (base = Na or K hydroxide carbonate or bicarbonate) in the presence of FeBr<sub>3</sub> ([MMA]:[FeBr<sub>2</sub>]:[FeBr<sub>3</sub>]:[EBrPA]:[base] = 200:1:0.1:1:2) at 60°C.

### 5. Polymerizations of other monomers

A limited number of experiments were also conducted with methyl and *n*-butyl acrylate (MA, BA) and *n*-butyl methacrylate (BMA), in order to establish the potential generality of this simplified ATRP protocol. Initial tests, carried out in the presence of Na<sub>2</sub>CO<sub>3</sub>, gave relatively rapid but poorly controlled polymerizations of the acrylates, with  $M_n$  much greater than expected and high  $\mathcal{D}$  (see details in Table S19), whereas the BMA polymerization gave more promising results. Additional polymerizations were therefore conducted only for BMA. Using KOH and KBr as additives, the polymerizations were relatively well controlled, with good agreement between measured and expected  $M_n$  values. However, the resulting  $\mathcal{D}$  values (1.19-1.34 at high conversions) were higher than those obtained for MMA under the same conditions, see Table S20.

### Conclusion

In this contribution, we have shown that simpler procedures than previously reported ones for the FeBr<sub>2</sub>-catalyzed ATRP of methyl methacrylate lead to better results (faster polymerizations, equal or better control of the molecular weight and molecular weight distribution). Using simple inorganic salts as catalyst promoters, rather than salts of large organic cations or neutral ligand additives, has several advantages, which include facile availability, reduced cost, and reduced toxicity. Keys to the performance of these inorganic salts are the significant solubility of the activated catalyst, e.g. KFeBr<sub>3</sub>, in the bulk monomer and participation of the cation, through ion pairing with the anionic activator and with the anionic deactivator, in modulating the atom transfer equilibrium. This was clearly shown by the different activity of FeBr<sub>2</sub>/MtBr with different Mt cations (Li, Na, K, Rb, Cs) and also by the effect of the addition of 18-crown-6 to the KBr system. Interestingly, the K(18C6)<sup>+</sup> system is less soluble and at the same time more active. Finally, the combination of the experimental results and the DFT calculations has identified the tricoordinated [FeBr<sub>3</sub>] intermediate, which is weakly stabilized by MMA coordination, as the active catalyst.

### ASSOCIATED CONTENT

**Supporting Information.** Details of polymerization kinetics, UV-visible spectra and DFT calculations (23 pages). This material is available free of charge via the Internet at <http://pubs.acs.org>.

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### ABBREVIATIONS

ATRP, atom transfer radical polymerization; EBrPA, ethyl  $\alpha$ -bromophenylacetate; MMA, methyl methacrylate; PRE, persistent radical effect.

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