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Article

Prediction of Contact Angle of Nanofluids by Single-Phase Approaches [†]

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Abstract: Wettability is the ability of the liquid to contact with the solid surface at the surrounding fluid and its degree is defined by contact angle (CA), which is calculated with balance between adhesive and cohesive forces on droplet surface. Thermophysical properties of the droplet, the forces acting on the droplet, atmosphere surrounding the droplet and the substrate surface are the main parameters affecting on CA. With nanofluids (NF), nanoparticle concentration and size and shape can modify the contact angle and thus wettability. This study investigates the validity of single-phase CA correlations for several nanofluids with different types of nanoparticles dispersed in water. Geometrical parameters of sessile droplet (height of the droplet, wetting radius and radius of curvature at the apex) are used in the tested correlations, which are based on force balance acting on the droplet surface, energy balance, spherical dome approach and empirical expression, respectively. It is shown that single-phase models can be expressed in terms of Bond number, the non-dimensional droplet volume and two geometrical similarity simplexes. It is demonstrated that they can be used successfully to predict CA of dilute nanofluids' at ambient conditions. Besides evaluation of CA, droplet shape is also well predicted for all nanofluid samples with ±5% error.

Keywords: contact angle; nanofluid; Bond number

1. Introduction

Wettability is the property of a solid surface contacted with a liquid within a surrounding fluid (liquid or gas) and its quantity is defined by the contact angle (CA). Wettability is important for the industrial applications such as phase change heat transfer, oil recovery and liquid coating. Contact angle (CA) is the angle between liquid–gas (or liquid–liquid) interface and liquid–solid interface for a droplet on a solid surface. The CA strongly depends on solid, liquid and surrounding fluid properties. If CA is smaller than 90°, it means that the liquid wets the solid surface. For CA greater than 90°, the liquid has lower wettability. CA is also dependent on liquid type and surface properties. Surface material including chemical composition and morphology, roughness and contamination make the CA and thus wetting properties. Since CA is predicted by the balance of interfacial/surface

Energies **2019**, 12, 4558 2 of 16

forces at triple point where solid, liquid and surrounding fluid contact, surrounding fluid properties play a role in wettability and CA evaluation. Besides these main parameters, temperature is another important affecting parameter for CA. Increase of temperature results in evaporation of the droplet and modifies CA.

It was also found that addition of nanoparticles (at least one dimension <100 nm) into conventional heat transfer fluids affects their thermophysical properties and results in interesting enhanced heat transfer ability. These suspensions were called as nanofluid (NF) [1]. In order to increase the markets' uptake of nanofluids, thermophysical properties of nanofluids have been studied widely [2–9]. However, surface tension and wettability behavior of NF is still at the beginning compared to other properties. Estellé et al. [10] have reviewed the surface tension and wettability and have concluded that nanoparticle nature, shape, size, content and concentration are governing parameters on surface tension and wettability. Some studies reported that the addition of nanoparticles increases the CA [11–14]. However, also a reduction in CA has also been observed in [15-17]. Lu et al. [18] also mentioned that increase in concentration decreases the spreading area of NF. However, effect of addition of nanoparticles changes with temperature [19]. Chinnam et al. [20] analyzed particle size, concentration and temperature effect on CA of NFs and developed a correlation. CA was also recently described as a relevant thermophysical property for dilute nanofluids [19]. As a result of round robin test carried out by nine independent European institutes, physically founded CA correlations dependent on temperature and droplet volume are developed from the experimental data. With zero-volume approximation, it was shown that limiting contact angle is dependent only on temperature at certain substrate and certain atmosphere.

More recently, wetting behavior of molten salt nanofluids and phase-change material nano-emulsions was studied by Grosu et al. [21]. They used wettability control to propose new methods to predict specific heat and thermal conductivity of molten salts and their nanofluids accurately. Moreover, Cabaleiro et al. [22] found that addition of a phase change material into water decreases the CA up to 52%.

Generally, measurement of CA is not easy and can have limited accuracy due to the stability of nanofluid and measurement methods. For practical applications, it is important to obtain accurate CA data of NF and models could be useful. So, the aim of this study is to evaluate the relevance of single-phase liquids models for the prediction of contact angle and droplet shape of nanofluids. Such an investigation is here reported for the first time where a comparison of different models is proposed for a large variety of nanofluids. A previous study [23] aimed to predict CA of dilute NFs by using single phase models, which were based on force balance and energy balance on the droplet surface. The previous study [23] was extended by considering a theoretical and an empirical model to improve the accuracy. Theoretical model was a spherical dome approach and empirical model was developed by Wong et al. [24]. Moreover, prediction of droplet shape was studied. All models were expressed in terms of Bond number (*Bo*) and geometrical similarity simplexes of droplets.

2. Materials and Methods

2.1. Nanofluids

To assess the relevance of different single-phase models for the prediction of nanofluid contact angle, experimental data for distilled water (DIW) as a single-phase reference fluid and base fluid of nanofluids with GO, Au, SiO_2 and Al_2O_3 nanoparticles were utilized. Au, Al_2O_3 and GO NFs here employed were fully characterized in [19] where preparation and thermophysical properties evaluation including density are also reported.

For preparation of SiO₂ NF, silica raw material with density of 2000 kg/m³ at 20 °C (SIPERNAT[®] 22S, Evonik Industries AG, Germany) was dispersed unfractionated. NF had pH- value of 10.5 with stabilization by KOH. Mean agglomerate size of particles was measured as 177 nm by using Dynamic Light Scattering analysis (Zetasizer Nano ZS, Malvern Instruments GmbH, Germany). Density of SiO₂

Energies **2019**, 12, 4558 3 of 16

NF was calculated with the mixture rule (Equation (1)) [25]. Thermal conductivity of SiO_2 nanofluid was measured by using 3ω method [26]. Measurements were conducted at 24 °C with three repetitions. Main information for all nanofluids are compiled in Table 1 showing the difference in concentration, size, shape and density of nanoparticles, and density and thermal conductivity of NF.

$$\rho_e = (1 - \phi_{p,v})\rho_f + \phi_{p,v}\rho_p. \tag{1}$$

Nanoparticle	Particle Size	Particle Shape	ϕ_p	Density of Nanoparticle (kg/m³)	Density of NF (kg/m³)	Thermal Conductivity Ratio (k _{NF} /k _{DIW})
Gold (Au)	Particle diameter: 8.34 nm	Spherical	0.001 wt. % (0.000052 vol.%)	1,9300	997.25	0.999
Silica (SiO ₂)	Particle diameter: 117 nm	Spherical	3.935 wt. % (2 vol.%)	2000	1017.06	1.008
Graphene oxide (GO)	Extension of particle: 770 to 900 nm Thickness: 2 nm to	Flake	0.01 wt. % (0.005679 vol.%)	1500–1900	997.25	0.9964
Alumina (Al ₂ O ₂)	10 nm Particle Diameter: 123 + 2 nm	Spherical	0.4 wt. % (0.1 vol. %)	3987	997.25	0.9961

Table 1. Characteristics of working fluids.

2.2. Experiments on Contact Angle Measurements and Determination of Geometrical Parameters

Experiments were performed in different institutes. The CA data of DIW, Au, Al_2O_3 and GO NFs were collected at İzmir Kâtip Çelebi University (İKÇÜ), Universitat Jaume I Castelló (UJI) and Université Rennes 1 (UR1) and were taken from [19]. CA of SiO_2 nanofluid was measured at ILK-Dresden (ILK). Sessile drop method was used in all institutes. Devices used in institutes and experimental conditions such as temperature T, droplet volume V and relative humidity RH used by each institute for the different liquids are described in Table 2.

Table 2.	Devices,	temperature,	relative	humidity	and	droplet	volume	of	experimental	study in
each inst	itute.									

DIW	Au NF	GO NF	SiO ₂ NF	Al ₂ O ₃ NF
T = 24.2 °C RH = 40% V = 4.6 μL	T = 23.7 °C RH = 40% V = 9.8 μL	T = 23.1 °C RH = 36% V = 4.1 μL		
T = 22.0 °C RH = 67% V = 10 μL			T = 25.0 °C RH = 64.5 % $V = 10 \mu\text{L}$	
T = 24.0 °C RH = 54% V = 5.1-71.1 µL T = 21.0 °C RH = 24%	$T = 24.0 ^{\circ}\text{C}$ RH = 54% $V = 5.3-68.6 \mu\text{L}$ $T = 21.0 ^{\circ}\text{C}$ RH = 24%	$T = 24.0 ^{\circ}\text{C}$ RH = 54% $V = 8.4-35.4 \mu\text{L}$ $T = 21.0 ^{\circ}\text{C}$ RH = 24%	·	T = 24.0 °C RH = 54% V = 5.5-28.8 μL T = 21.0 °C RH = 24% V = 20.9 μL
	T = 24.2 °C RH = 40% V = 4.6 μL T = 22.0 °C RH = 67% V = 10 μL T = 24.0 °C RH = 54% V = 5.1–71.1 μL T = 21.0 °C	$\begin{array}{ccccc} \textbf{DIW} & \textbf{Au NF} \\ \hline T = 24.2 ^{\circ} \textbf{C} & T = 23.7 ^{\circ} \textbf{C} \\ \textbf{RH} = 40\% & \textbf{RH} = 40\% \\ \textbf{V} = 4.6 \mu \textbf{L} & \textbf{V} = 9.8 \mu \textbf{L} \\ \hline T = 22.0 ^{\circ} \textbf{C} \\ \textbf{RH} = 67\% & \textbf{V} = 10 \mu \textbf{L} \\ T = 24.0 ^{\circ} \textbf{C} & \textbf{T} = 24.0 ^{\circ} \textbf{C} \\ \textbf{RH} = 54\% & \textbf{RH} = 54\% \\ \textbf{V} = 5.1-71.1 \mu \textbf{L} & \textbf{V} = 5.3-68.6 \mu \textbf{L} \\ T = 21.0 ^{\circ} \textbf{C} & \textbf{RH} = 24\% & \textbf{RH} = 24\% \\ \hline \end{array}$	$T = 24.2 ^{\circ}\text{C} \qquad T = 23.7 ^{\circ}\text{C} \qquad T = 23.1 ^{\circ}\text{C}$ $RH = 40\% \qquad RH = 40\% \qquad RH = 36\%$ $V = 4.6 \mu\text{L} \qquad V = 9.8 \mu\text{L} \qquad V = 4.1 \mu\text{L}$ $T = 22.0 ^{\circ}\text{C}$ $RH = 67\% \qquad V = 10 \mu\text{L}$ $T = 24.0 ^{\circ}\text{C} \qquad T = 24.0 ^{\circ}\text{C}$ $RH = 54\% \qquad RH = 54\% \qquad RH = 54\%$ $V = 5.1-71.1 \mu\text{L} \qquad V = 5.3-68.6 \mu\text{L} \qquad V = 8.4-35.4 \mu\text{L}$ $T = 21.0 ^{\circ}\text{C} \qquad RH = 24\% \qquad RH = 24\%$ $RH = 24\% \qquad RH = 24\%$	$\begin{array}{c ccccccccccccccccccccccccccccccccccc$

Main steps of the CA measurements performed by each institute are described in the following paragraph. The reader is also referred to [19] for more details. Attention Theta Goniometer (Biolin Scientific, (Sweden/Finland)) was used in the experiments carried out by IKQU. After calibration of the device, surface tension of liquids was measured and then introduced to device software as property to find CA. In 10 s, 125–140 images of droplet were captured. CA was evaluated by fitting the droplet shape with the Young-Laplace equation.

UR1 calibrated the commercial device (DSA-30 Drop Shape Analyzer (KRÜSS GmbH, Germany)) from gauges with known CAs of 30°, 60° and 120°, and a maximum relative deviation was obtained as 0.52%. Droplet was positioned at the surface by using 15-gauge needle with an outer diameter of

Energies **2019**, 12, 4558 4 of 16

1.835 mm. After positioning, CA values were measured in a few seconds. Further information on setup, experimental procedure and image analysis was given in [19].

Lab-made device developed by UJI was combination of camera, syringe, indirect LED light source and micrometer carrier. The droplet regulator, which holds the syringe, was controlled by a micrometer carrier. Syringe was used to position the droplet on the solid surface at a controlled volume. LED panel light was used to obtain high contrast by background illumination. This device allows the prediction of CA and volume of the droplet by image processing.

CA was measured at ILK by using the lab-made device [19]. In the setup [19], the droplet was positioned by a micropipette (VWR Pipettor 2–20 μ L) on the solid substrate. Digital reflex camera (Canon EOS 40D) equipped with close-up lens (Tamron, SP 90 mm F/2.8, Di MACRO 1:1, VC USD; Japan) was used to capture the droplet images. In order to obtain accurate CA, contrast of images improved by using light disperser and light source with 129 LEDs. Images of droplet were stored at a laptop and contact angle of each droplet was predicted by using ImageJ [27] software with extension "drop analysis" [28]. Contact angle of the droplet was determined for both sides and mean contact angle was used. Experiments of CA measurement were conducted in ILK for constant volume at 10 μ L.

CA of DIW and NFs was measured on the solid stainless steel substrate with thickness of 5 mm and an averaged roughness of 1.4 μ m. For each institution, solid substrates were manufactured from single round stock with same lathe to provide same material and surface quality for all substrates. Properties of the solid substrate were presented in [19] with details.

In addition to CA, surface tension (σ_{lg}) of the working fluids was evaluated experimentally at UR1 (DIW, Au NF, Al₂O₃ and GO NF) and İKÇÜ (SiO₂ NF; Table 3). In both institutes, the pendant drop method was employed to define the σ_{lg} . DSA-30 Drop Shape Analyzer (KRÜSS GmbH, Germany) and Biolin Scientific, (Sweden/Finland) were used at UR1 and İKÇÜ, respectively. In İKÇÜ, surface tension of DIW was measured before SiO₂ NF. For both working fluids, the volume was kept constant at 10 μ L and three measurements were carried out. There is no significant deviation between replicates and between experimental values of DIW with NIST data [29] at a given temperature. The comprehensive description of the experimental procedure used for the surface tension measurement at UR1 can be found in [30].

Working Fluid	T (°C)	RH (%)	σ_{lg} (mN/m)	Standard Deviation
DIW	21	24	72.960	0.06
GO NF	21	24	73.345	0.125
Au NF	21	24	72.77	0.13
Al_2O_3 NF	21	24	72.005	0.255
SiO ₂ NF	22.8	40	70.13	0.25

Table 3. Surface tensions of the working fluids.

Finally, the geometrical parameters (δ , r_d and R_0) used in the models that are described in the next section were obtained by CA image analysis. Such an analysis has been performed with an image processing program called Fiji [31] as shown in Figure 1. Pixel-to-mm ratio with respect to a reference dimension for the images from the institutes is defined to spatial calibration of each data set.

Energies **2019**, 12, 4558 5 of 16

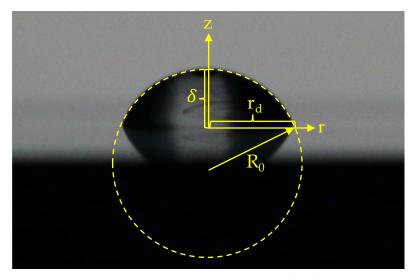


Figure 1. Geometrical parameters on droplet.

2.3. Single-Phase Models for Prediction of Contact Angle

In this section, the models developed for the CA evaluation of single-phase liquids are presented. The first model considered was developed by Vafaei and Podowski [32], which is based on the force balance of gravity and surface forces on the droplet surface. Reason behind the gravity force is to the hydrostatic force of the variable droplet height and the surface forces are result of external pressure and surface tension. Vafaei and Podowski [32] proposed a model for the prediction of droplet volume that writes as follow:

$$V = \frac{2\pi\sigma_{lg}r_d^2}{\rho g} \left(\frac{\rho g\delta}{2\sigma_{lg}} + \frac{1}{R_0} - \frac{\sin\theta_d}{r_d}\right). \tag{2}$$

Here ρ denotes density and V are droplet baseline radius and volume. As geometrical parameters r_d , δ and R_0 are the droplet baseline radius, apex height and curvature, respectively. θ_d is the contact angle of the droplet. Droplet volume equation (2) was reformulated by using non-dimensional numbers: Bond number (Bo), which is the ratio of gravitational and surface forces, two geometrical similarity simplexes— G_1 and G_2 —which describe the droplet geometry and V^* as the non-dimensional droplet volume.

$$sin\theta_d = \frac{1}{2}Bo G_1 + G_2 - Bo V^*;$$
 $G_1 = \frac{\delta}{r_d};$
 $G_2 = \frac{r_d}{R_0};$
 $V^* = \frac{V}{2\pi r_d}^3;$
(3)

where Bo is

$$Bo = \rho g r_d^2 / \sigma_{lg}. \tag{4}$$

In the definition of Bo number characteristic length equals to r_d , which is defined by Kuiken [33]. Moreover, Stacy [34] reported that characteristic length equals to radius at the droplet equator and wetting radius for non-wetting droplets and for wetting droplets, respectively.

The second model we have considered was proposed by Yonemoto and Kunugi [35] (YK model), which is based on the energy balance for various-sized droplets on a solid surface. This correlation writes

$$\frac{\rho g \delta V}{2} = \pi r_d^2 \sigma_{lg} (1 - \cos \theta_s) - \pi r_d \delta \sigma_{lg} \sin \theta_s. \tag{5}$$

A non-dimensional form is obtained by dividing (5) by the gravitational potential $\rho g \delta V/2$.

Energies **2019**, 12, 4558 6 of 16

$$1 = X^* - Y^*;$$

$$X^* = \frac{2\pi r_d^2}{\delta V} \frac{\sigma_{Ig}(1 - \cos\theta_s)}{\rho g} = \frac{(1 - \cos\theta_s)}{Bo \ V^* \ G_1};$$

$$Y^* = \frac{2\pi r_d}{V} \frac{\sigma_{Ig} \sin\theta_s}{\rho g} = \frac{\sin\theta_s}{Bo \ V^*}.$$
(6)

YK model is used for only spherical droplets. Therefore, employing the correlation for $\theta_s = \arcsin\left(\frac{r_d \sin \theta_d}{r_{ds}}\right)$ given in [32] Equation (5) is rewritten. The contact angle for spherical droplets is denoted by θ_s and its baseline radius by r_{ds} .

$$1 + \cos\theta_s = \frac{\sin^2\theta_d}{G_1(BoV^* + \sin\theta_d)}. (7)$$

Moreover, the spherical dome model (SD model), which is based on the tangent of only dimensions of the droplet (δ and r_d), analyzed in [24] was rewritten in terms of geometrical similarity simplex, G_1 , and validity was studied for nanofluids.

$$\theta_d = 2arctan\left(\frac{\delta}{r_d}\right) = 2arctan(G_1).$$
 (8)

Finally, Wong et al. [24] (W model) developed an empirical formulation, expressed in Equation (9), to predict contact angle of liquids, which was reported as being valid for any substrate and droplet materials. This empirical model uses the contact angle, droplet volume, height and width ($W=2r_d$) and allows us to find two of them by using known other two parameters.

$$\theta_d = 1.41 - 0.678\delta + 0.143W + 0.307\delta^2 - 0.0757\delta W - 0.00457W^2 -0.0453\delta^2 W + 0.0310W^2 \delta - 0.00457W^3.$$
(9)

2.4. Prediction of Droplet Shape

In addition to CA prediction from single phase models, the sessile droplet shape of NFs is compared to the following approach. Thus, Vafaei and Podowski [32] reported that droplet shape could be predicted by force balance on the droplet surface as well as CA as following:

$$z = \delta - \frac{\sigma_{lg}}{\rho g} r^2 \left(\frac{3c_1}{r} + 4c_2 + 5c_3 r + 6c_4 r^2 \right). \tag{10}$$

Coefficients (c_1, c_2, c_3, c_4) were determined by applying boundary conditions:

$$z(r_d) = 0. (11)$$

$$\left. \frac{dz}{dr} \right|_{r=0} = 0. \tag{12}$$

$$\left. \frac{d^2z}{dr^2} \right|_{r=0} = -\frac{1}{R_0}. \tag{13}$$

$$V = \int_0^\delta \pi r^2 dz. \tag{14}$$

Applying one more boundary condition $z(-r_d) = 0$ and power series assumption ($c_3 = 0$), Equation (10) was re-arranged by using geometrical similarity simplexes.

$$\frac{z}{r_d} = G_1 - \frac{G_3 G_4}{2} - G_1 G_4^4 + \frac{G_3 G_4^3}{2};$$

$$G_3 = \frac{r}{R_0};$$

$$G_4 = \frac{r}{r_d}.$$
(15)

Energies 2019, 12, 4558 7 of 16

Considering the origin is at the center of the wetting circle, r is the horizontal axis and z is the vertical axes of the droplet (Figure 1).

3. Results and Discussion

In this study, validity of contact angle models, which were developed for single-phase fluids, was investigated. In the figures, filled symbols (\bullet) were for models and empty symbols (\bullet) were used for experimental results. Due to the measurement uncertainties and in order to evaluate their influence, numerical results from the models were corrected with increasing R_0 by 2% and it was presented as a red cross in the figures (\times).

Error between experimental and predicted CA was determined by using mean absolute percentage error (MAPE) and was denoted as Ω in the study. It is found as:

$$\Omega = \frac{100}{n} \sum_{t=1}^{n} \left| \frac{\theta_{dexp,t} - \theta_{dpred,t}}{\theta_{dexp,t}} \right|. \tag{16}$$

3.1. Contact Angle Prediction with Single-Phase Models

Figures 2 and 3 show the validity of VP model for DIW and the different nanofluids. DIW as expected for a single-phase liquid has good agreement with the model (for various volume $\Omega=2.32\%$ and for constant volume $\Omega=6.34\%$). Due to the low concentration and the small particle size, the Au and Al₂O₃ NF shows also reasonable good agreement with $\Omega=2.07\%$ and $\Omega=4.07\%$, respectively. However, the VP model seems to be not valid for GO ($\Omega=8.52\%$) and SiO₂ NFs ($\Omega=30.46\%$). Large graphene flakes in GO NF and higher concentration (3.935 wt.%) of SiO₂ NF may be the reason of preventing the application of the VP model.

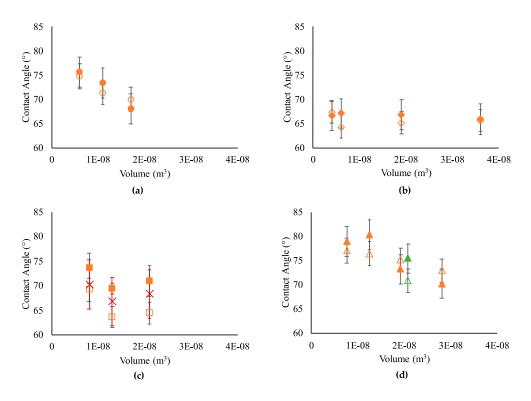


Figure 2. VP model validity for fluids at various volumes. Working fluids are (**a**) distilled water (DIW), (**b**) Au nanofluid (NF), (**c**) GO NF and (**d**) Al₂O₃ NF. Colors indicate: orange—Universitat Jaume I Castelló (UJI) and green—Université Rennes 1 (UR1).

Energies **2019**, 12, 4558 8 of 16

It was found, that the VP model was very sensitive against tiny experimental errors following the determination of R_0 . To illustrate this, R_0 was increased artificially by just 2% and additional results presented in Figure 2 for GO NF, and Figure 3 for DIW and SiO₂. CA data of GO NF fit much better with the VP model with this correction. Ω decreased from 8.52% to 4.19% for GO NF. Unlike GO NF, CA of SiO₂ NF was not affected from the increase of R_0 (Ω = 27.79%). This shows the influence of nanoparticle content on the applicability of V–P model with nanofluids.

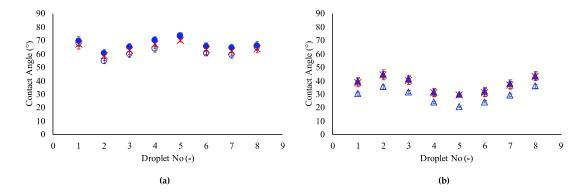


Figure 3. VP model validity for fluids at constant volume. Working fluids are (a) DIW and (b) SiO₂ NFs.

The modified YK model was in good agreement with experimental results for DIW, Au, Al_2O_3 and GO nanofluids. As shown in Figure 4, all the data was in the range of the $\pm 10\%$ error band. However, the results for the SiO_2 NF (Figure 5) show again that a single-phase model was not appropriate for a highly concentrated nanofluid.

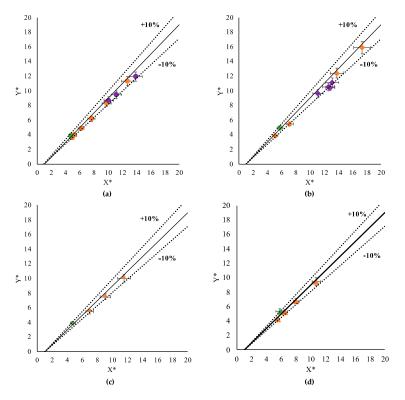


Figure 4. Yonemoto and Kunugi (YK) model validity for fluids at various volumes. Working fluids are (a) DIW, (b) Au NF, (c) GO NF and (d) Al_2O_3 NF. Colors indicate: orange—UJI, green—UR1 and purple—İzmir Kâtip Çelebi University (İKÇÜ).

Energies 2019, 12, 4558 9 of 16

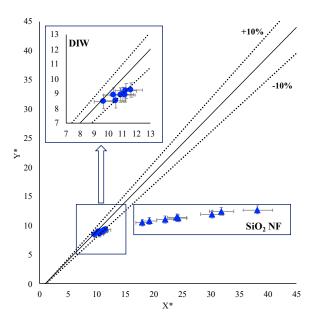


Figure 5. YK model validity for fluids at constant volume.

Figures 6 and 7 show that the SD model was valid for DIW ($\Omega=4.71\%$), Al $_2O_3$ NF ($\Omega=3.78\%$) and Au NF ($\Omega=7.18\%$). Vafaei and Podowski [32] mentioned that as volume decreases the shape of the droplet is more spherical. Although the volume range was narrow for this study, change of the droplet shape with volume was obviously clear. For GO nanofluid at the highest volume, CA was underpredicted compared to experimental results with $\Omega=7.35\%$. The reason could be the shape and size of the graphene flakes. Different from the other theoretical models, predicted SiO $_2$ data with the SD model was much collapsed with the experimental data with $\Omega=10.71\%$ where DIW had $\Omega=3.90\%$.

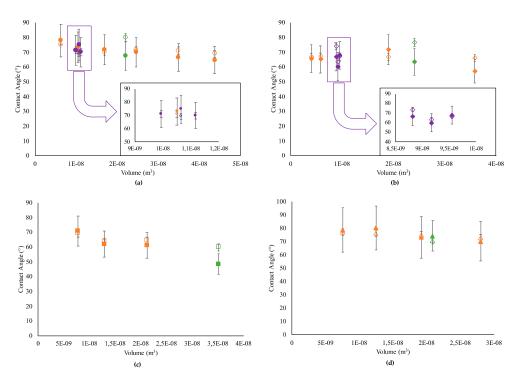


Figure 6. Spherical dome (SD) model validity for fluids at various volumes. Working fluids are (a) DIW, (b) Au NF, (c) GO NF and (d) Al₂O₃ NF. Colors indicate: orange—UJI, green—UR1 and purple—İKÇÜ.

Energies 2019, 12, 4558 10 of 16

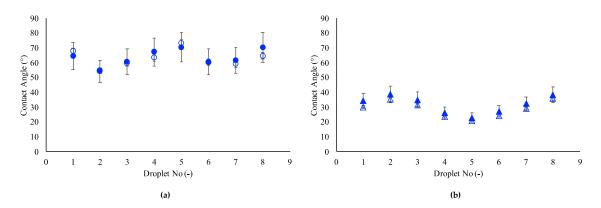


Figure 7. SD model validity for fluids at constant volume. Working fluids are (a) DIW and (b) SiO₂ NF.

In addition to these theoretical models, the empirical model developed by Wong et al. [24] allowed us to predict contact angle of nanofluids at lower concentrations (Figure 8). Ω value was calculated for DIW for various volumes, DIW at constant volume, Au NF and GO NF were 5.77%, 3.53%, 4.70% and 5.26%, respectively. CA data of Al₂O₃ NF (Ω = 9.78%) predicted by the W model is different for smaller volumes. However, increase in volume results in more accurate results with the W model. The reason could be that the concentration highly affects on CA at lower volumes for this model. Similar behavior was observed for also SiO₂ NF. The W model was not suitable for highly concentrated nanofluids as shown in SiO₂ NF (Ω = 144.46%) results in Figure 9.

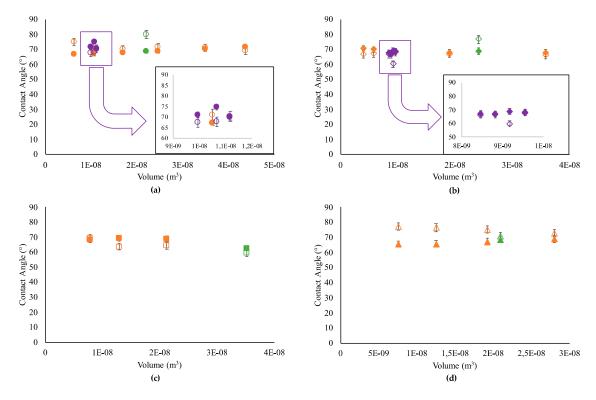


Figure 8. Wong et al. (W) model validity for fluids at various volumes. Working fluids are (a) DIW, (b) Au NF, (c) GO NF and (d) Al₂O₃ NF. Colors indicate: orange—UJI, green—UR1 and purple—İKÇÜ.

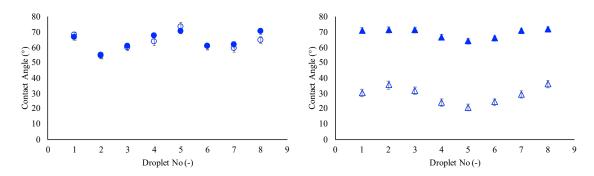


Figure 9. W model validity for fluids at constant volume. Working fluids are (a) DIW and (b) SiO₂ NF.

3.2. Droplet Shape Prediction

Vafaei and Podowski [32] also developed a model to predict droplet shape based on force balance (Equation (15)). This subsection presents the validity of this model for nanofluids considered in this study. For volume dependent analysis, droplets had a maximum 21 μ L of volume (Figure 10). For constant volume analysis of DIW and SiO₂ NF, droplets that had maximum, minimum and average contact angles were chosen (Figure 11).

Droplet shape was predicted with $\pm 5\%$ error for all cases without influence of shape and concentration of nanoparticles, and volume of the droplet. This $\pm 5\%$ error band could include measurement errors in geometrical parameters and experimental errors.

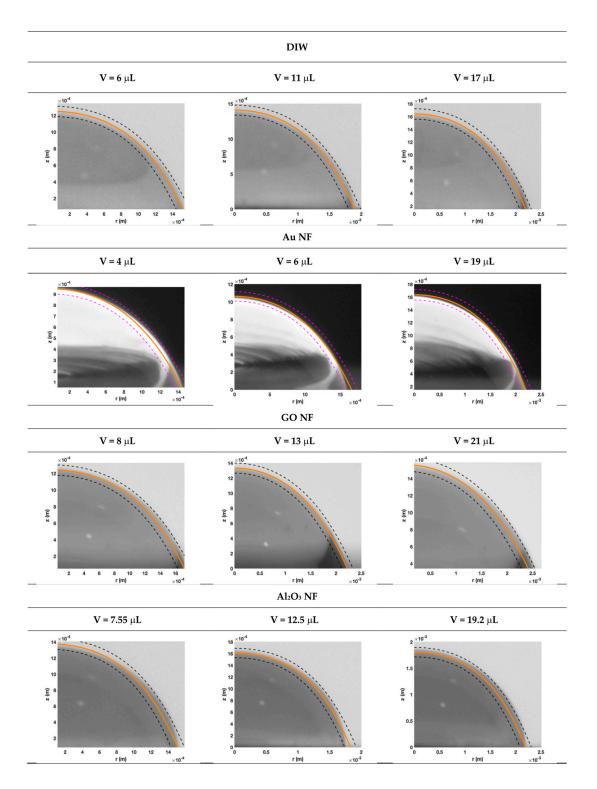


Figure 10. Droplet shape prediction at various volumes (—shows Equation (14) and—shows the $\pm 5\%$ errors).

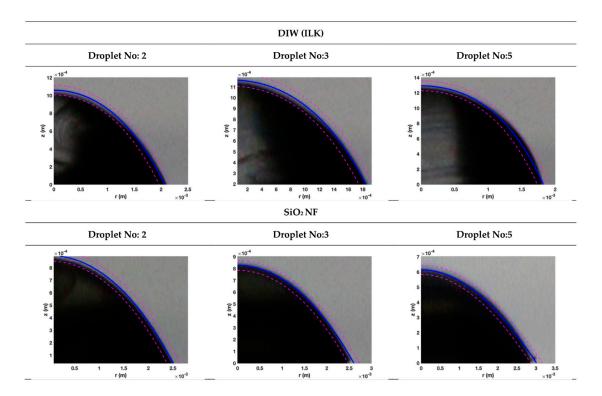


Figure 11. Droplet shape prediction at constant volume (—shows Equation (14) and—shows the $\pm 5\%$ errors).

4. Conclusions

The aim of this study was to evaluate the reliability of three theoretical models and one empirical model developed for single-phase liquids for describing the correlation between contact angle, geometrical parameters and forces/energy balance of nanofluid sessile droplets. Four types of water-based nanofluids were considered varying the size, shape and nature of nanoparticles as well as the concentration.

Single-phase models were expressed in terms of Bo, which depends on surface tension and density, non-dimensional volume V^* and geometrical simplexes and they were used for prediction of dilute NFs' CA. Although the measurement of the required geometrical parameters for prediction of CA demands high precision to obtain accurate results, it is concluded that concentration is the main factor to affect applicability of models for NFs. Although the force balance-based VP model was too sensitive to measurement errors for GO NF and CA of dilute NFs (Au, GO and Al_2O_3 NF) could be predicted by both the VP model and energy balance-based YK model. Moreover, the empirical W model was valid for dilute NFs (Au and GO NF) and higher volumes of Al_2O_3 NF. However, significant differences were obtained for highly concentrated SiO_2 NF in these theoretical models and empirical model. Additional effects like disjoining pressure, convective flows inside the droplet, etc. could be the reasons of differences in results of different models. Beside them, the SD model is suitable for almost all samples due to the spherical shape of droplets as a result of smaller volumes. However, higher error band of SD model is the limitation for accurate prediction of CA. It was also shown that the droplet shape of all NFs could be well predicted from a model based on force balance.

To conclude, further research is now needed to resolve and improve the limitation of the measurement of dimensions and for the development of a useful and generic CA model by investigation of additional possible effects such as temperature, a wider range of nanoparticle size and shape varying the nanoparticle concentration.

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Resources, N.Ç., P.E. and R.M.-C.; Data Curation, N.Ç. and M.H.B.; Writing—Original Draft Preparation, N.Ç.; Writing—Review and Editing, Z.H.K., P.E., R.M.-C. and M.H.B.; Visualization, N.Ç., Z.H.K., P.E., R.M.-C. and M.H.B.; Supervision, M.H.B.; Project Administration, N.Ç., Z.H.K. and M.H.B.

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Nomenclature

Во	Bond Number (-)
c	Coefficients

g Gravitational Acceleration (m/s²)
G Geometrical Similarity Simplex (-)
k Thermal Conductivity (W/mK)
r Droplet Wetting Radius (m)
R Radius of Curvature (m)
RH Relative Humidity (%)

V Volume (m³)

W Width of the droplet (m) T Temperature (°C)

Abbreviations

CA Contact Angle DIW Distilled Water

İKÇÜ Izmir Katip Çelebi University

ILK ILK-Dresden NF Nanofluid

UJI Universitat Jaume I Castelló

UR1 Université Rennes 1

Subscripts

0 At the apex d Droplet e Effective f Base Fluid lg Liquid-Gas p Particle s Spherical v Volumetric

Greek Letters

- σ Surface Tension (mN/m)
- δ Location of Apex (m)
- ρ Density (kg/m³)
- θ Contact Angle (°)
- Ω Mean Absolute Percentage Error (%)
- ϕ Concentration of NF (%)

Energies **2019**, 12, 4558 15 of 16

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