Dynamic mesh adaptation for moving fronts and interfaces: application to the modeling of premixed flames and primary atomization

V. Moureau, P. Bénard, G. Lartigue CORIA, CNRS UMR6614, Normandie Univ, UNIROUEN, INSA Rouen

R. Mercier, M. Cailler – SAFRAN Tech, Magny-les-Hameaux

A. Froehly – LMB/INRIA Bordeaux, France

In memoriam C. Dobrzynski – LMB/INRIA Bordeaux, France

Tetrahedron VI workshop, 3rd of October, 2019, INRIA Saclay







Context: aeronautical engines









Aeronautical engine design is driven by two major constraints

Fuel efficiency

- Economic constraints
 reduced fuel consumption
 reduced CO₂ emissions
- Global efficiency of the engine



Pollutant emissions

- International regulations
 - CAEP regulations



Large-Eddy Simulation in the aeronautical context

- LES solves the large scales and models the small scales
- It is well suited to the high-fidelity simulation of aeronautical burners
- Challenges
 - Unsteady, multi-scale, multi-physics flows
 - Need to exploit modern super-computers







JOLIOT-CURIE, PRACE/GENCI at the Très Grand Centre de Calcul, CEA 9 Petaflops, 124 000 cores

The CFD platform: YALES2

- Developed by CORIA and the French Combustion Community
 - 250+ researchers/engineers trained at CORIA since 2009
 - 150+ articles (Google Scholar)

CNRS – UNIVERSITE et INSA de Rouen

• A unique network to ease collaboration and transfer of numerics and models to the industry



The CFD platform: YALES2

- Features
 - Unstructured meshes (complex geometries) and adaptive grid refinement
 - Low-Mach number Navier-Stokes equations (incompressible and variable density) solved with a projection method
 - Double-domain decomposition [3] and hybrid OpenMP/MPI communications
 - Highly efficient solvers for linear system inversion (PCG, DPCG)
 - 4th-order central finite-volume method and 4th-order time integration
 - Two-phase flows (Lagrangian particles)
 - Spray and atomization (Levelset)
 - Combustion modeling (Tabulated or complex chemistry, NOx prediction model...)
 - Suited for massively parallel computing (>32 000 procs)





YALES2 web site, <u>http://www.coria-cfd.fr</u>
 SUCCESS web site, <u>http://success.coria-cfd.fr</u>

6

HPC: in-core and parallel performances

- MPI and hybrid coarse-grain OpenMP/MPI
- Two-level domain decomposition [1]

In-house linear solvers

- Enables to fit in L2 cache memory
- Used for the preconditioning of the linear solvers

16384 16384 Linear scaling 2.2B Yales2 with A-DEF2 solver Ο Δ Yales2 with RA-DEF2(d) solver Ο 12288 12288 $\nabla \cdot \left(\frac{1}{\rho} \nabla P\right) = \frac{\nabla \cdot \mathbf{u}^{\star}}{\Delta t}$ Speed-up 8192 8192 Weak scaling for a low-Mach number 4096 4096 turbine blade calculation on the Curie machine at TGCC, CEA Malandain et al., JCP 2013 4096 16384 8192 12288 Number of cores



[1] Moureau et. al., CR Mecanique, 2011

Prediction of pollutant emissions in realistic burners: Application to a low-NOx helicopter engine

- LES from J. Lamouroux, SAFRAN Helicopter Engines, in 2015
- 376M elements for 2 injectors, tabulated chemistry, dedicated NOx model [1]



[1] Pecquery et al. (2014) Comb. Flame 161(2)

Future large-scale computations in the industry

• Simulation time for an aeronautical combustor with a mesh of 10 billion tets (2025+ target)



- Many issues have to be addressed
 - Mesh management, solving of large linear systems, load balancing of chemistry integration, data-mining, ...

High-fidelity simulation of semi-industrial burners

- LES of the lean-premixed PRECCINSTA burner with finite-rate chemistry (Sankaran et al. scheme, 17 species, 73 reactions) and heat loss [1]
- 2018 FIRELES PRACE project, 16384 cores on Curie



[1] P. Bénard et al. (2018) Int. Comb. Symp., Dublin

When can we expect a DNS of semi-industrial burners?



- LES of PRECCINSTA burner
 - 17 species, 72 reactions
 - 150 microns
 - 877M tets, 4M CPUh
 - 16,384 cores, 1 week



• Alternative to reach DNS faster ?

A possible way to reach our target simulations faster

- Simulation of a premixed flame with dynamic h-adaptation
- F-TACLES combustion model [1], refinement ratio = 6



• A prerequisite is to know how to perform parallel h-adaptation

Outline

- Context & Motivation
- Parallel mesh adaptation
 - Principle
 - Load balancing and data transfer
 - Example
- Dynamic mesh adaptation
 - Metric definition and adaptation triggering
 - Examples
 - Performances
- Improvements to the dynamic mesh adaptation process
- Conclusions & perspectives

Objectives

- To design a dynamic mesh adaptation method with the constraints:
 - Tailored for distributed-memory system (10,000+ cores)
 - Efficient enough to be called every 10 fluid iterations
 - Compatible with the modeling approach (finite-volume + LES)
 - No remeshing at material interfaces to avoid interpolation errors
- Some choices
 - Isotropic mesh adaptation
 - Parallelism handled by the flow solver (interpolation, data transfer)
- A first check if these objectives are reachable for tets
 - Reduced computation cost of fluid solver: 30 to 500 μ s/iter/node
 - Adaptation of a distributed mesh with MMG: order of 100 $\mu s/node$



A moving interface method for parallel h-adaptation on distributed memory systems

- Principle with a single-level domain decomposition [1] $\mathcal{M}_{\rm init}$





Final mesh

(courtesy A. Froehly - ParMMG)

A moving interface method for parallel h-adaptation on distributed memory systems

- Generalization to a 2-level domain decomposition [1]
- The MMG library [2] from INRIA/IMB adapts the mesh (vol/surf) on each rank
- Skewness is the main measure of the mesh quality
- Example for 4 processors

•

IC



Input metric to MMG

- At each adaptation step, a metric is given to MMG: $\mathcal{M}_{
 m step}$
- \mathcal{M}_{step} has to be different from \mathcal{M}_{target} because it is not compatible at the interfaces and walls





 $\begin{cases} \mathcal{M}_{step} = \mathcal{M}_{current} & \text{at the interface} \\ \mathcal{M}_{step} = \mathcal{M}_{target} & \text{away from interface} \\ \mathcal{M}_{step} = FMM(\mathcal{M}_{current}, \mathcal{M}_{target}, h_{grad}) & \text{in between} \end{cases}$

Constraint load balancing

- The first method is based on edge-weighted graph partitioning
- A graph of the element groups is built
- METIS is called on the master rank with $\omega_{
 m interface} = 100 \, \omega_{
 m inside}$





Optimized transfer of cell groups

- Outer loop:
 - List all the sending operations (rank N to rank M)
 - Shuffle these sending operations
 - Perform as many parallel sending operations as possible
- Inner loop: rank N sends cell groups to rank M
 - Pack the cell groups on rank N in a single real array
 - **Non-blocking** send/recv of the pack
 - Unpack the cell groups on rank M
 - Rebuild **connectivity** on ranks N, M and connected ranks
- Remarks
 - One cell group is a few MB => the MPI latency is still reasonable (a few 100 μs to 1 ms)
 - Packing/unpacking and rebuilding the connectivity are the time consuming algorithms

Example: user-independent LES of aeronautical burners

- 2018 TERATEC/Usine Digitale award
- First LES Design of Experiment performed at SAFRAN TECH in 2018
 - 9 combustion LES for injection system design (30h per run !)



Outline

- Context & Motivation
- Parallel mesh adaptation
 - Principle
 - Load balancing and data transfer
 - Example
- Dynamic mesh adaptation
 - Metric definition and adaptation triggering
 - Examples
 - Performances
- Improvements to the dynamic mesh adaptation process
- Conclusions & perspectives

A simple metric definition for material interfaces

• The target metric is based on the distance to the interface (flame front or liquid/gas interface)





When to remesh?

• Metric definition

$$\mathcal{M} = \alpha \mathcal{M}_{\text{front}} + (1 - \alpha) \mathcal{M}_{\text{background}}$$

with $\begin{vmatrix} \alpha = f(S, N_p) \\ S : \text{Front sensor} \\ N_p : \text{Ncells propagation} \end{vmatrix}$

- When to remesh ? [1,2]
- Each $N_a \Delta t$
- Given N_p we can derive a CFL-like condition for N_a:

$$CFL^{DMA} = \frac{|\mathbf{u} \cdot \mathbf{n}_{\Phi}| * N_a \Delta t}{N_p \mathcal{M}_{front}}$$



• How to choose N_p ? Depends on the interface dynamics

The Flame Brush Thickness

- The FBT can be defined as the region where the flame evolves
- The same can be defined for other material interfaces



How to choose the size of refined mesh region (N_p) ?

• Determine optimal N_p



- Dynamic or static adaptation ? Depends on the Flame Brush Thickness (FBT)
- /!\ Choice has to be considered at each new numerical setup (target cell size, etc...). N_p is constant in the following examples.

CO

- Metric definition based on a progress variable
- Same resolution as 110M (300 microns) but with 38M cells (x3 speed-up)
- Volume/surface adaptation with MMG5.3 and YALES2 2018.11



- Metric definition based on a progress variable
- Same resolution as 878M (150 microns) but with 260M cells (x4.5 speed-up)
- Volume/surface adaptation with MMG5.3 and YALES2 2018.11



O

CNRS – UNIVERSITE et INSA de Rouen

- Comparison of the dynamically adapted results to static cases [1]
- Progress variable iso-contour:

CNRS – UNIVERSITE et INSA de Rouen



• The small-scale wrinkling depends only on the finest cell size

- Is the flame wrinkling similar between 150µm dynamic and 150µm static?
- Flame curvature distribution computed as the divergence of the isosurface c=0.7 normal



- 3D head-on collision of 2 equal-size droplets with reflexive separation [1]
- This is a very challenging case as dynamics is governed by surface tension [2]



Time: 0.000000 s



Water/Air
We = 23
Oh =
$$0.0047$$

 $\Delta x_{min} = 6\mu m$
 $\Delta t_{adapt} = 0.35\mu s$
30M cells
420 cores

200,000 total iterations10,000 adaptation iterations

• 3D head-on collision of 2 equal-size droplets with reflexive separation [1]



Experiment [1]

Simulation





CNRS – UNIVERSITE et INSA de Rouen

- High-Weber number example: kerosene jet-in-cross flow [1,2]
- Up to 1.6 billion tets on 8192 cores



• Parametric study of the kerosene jet-in-cross flow [1,2]









- Simulation of oil churning [1,2] by M. Cailler, SAFRAN TECH
- 206 million tets on 1250 cores (Cobalt, CEA), adaptation cost = 42%



Performances

• Two-phase flow simulation on 1024 cores (Intel Xeon Skylake 2.4GHz)



Performances

- Two-phase flow simulation on 1024 cores (Intel Xeon Skylake 2.4GHz)
- Cost of graph coloring+MMG and data transfer in the adaptation steps



- Despite packing/unpacking send/recv and fully parallel transfers, the total data transfer cost is around 600 μ s/node, which is non negligible

CO

Outline

- Context & Motivation
- Parallel mesh adaptation
 - Principle
 - Load balancing and data transfer
 - Example
- Dynamic mesh adaptation
 - Metric definition and adaptation triggering
 - Examples
 - Performances
- Improvements to the dynamic mesh adaptation process
- Conclusions & perspectives

Metric error-based adaptation

- Aim: better control of the adaptation triggering
- Relative metric error

$$\epsilon = \max\left(\left|\frac{\mathcal{M}_{\text{current}} - \mathcal{M}_{\text{target}}}{\mathcal{M}_{\text{target}}}\right|\right)$$

- Triggering: $\epsilon > 0.5$ in the refined region
- This criterion simply states that the metric must keep its value in the refined region
- Example: water droplet convection



Improved error-based load balancing

- The load balancing step can be enhanced by addressing the bad quality cells and the metric errors via agglomeration coloring
- Proposed coloring algorithm
 - Identify all cell groups with bad quality cells and metric error
 - For all flagged cell groups
 - Pick a bad quality cell group and agglomerate with connected other bad quality cell group
 - Stop if large enough
 - For all flagged colors
 - Repeat agglomeration with unflagged connected cell groups
 - Stop if large enough
 - Agglomerate the rest until reaching the number of colors (or ranks)



The mesh is not perfectly balanced but contiguous (if initial mesh is).
 METIS is still called at the final step to ensure load balance

Performances of new strategy

Convection of water droplet ٠

Previous adaptation strategy

Metric error trigerring Error-based load balancing



Outline

- Context & Motivation
- Parallel mesh adaptation
 - Principle
 - Load balancing and data transfer
 - Example
- Dynamic mesh adaptation
 - Metric definition and adaptation triggering
 - Examples
 - Performances
- Improvements to the dynamic mesh adaptation process
- Conclusions & perspectives

Conclusions and prospects

- Dynamic mesh adaptation of material interfaces on distributed memory systems is feasible and is a solution to achieve more accuracy for a given cell count
- It has been employed for many industrial applications in 2018 and 2019 and has proven to be mandatory for certain cases
- Many theoretical and numerical developments are still required
 - Modeling of space/time commutation errors in LES
 - Sub-grid scale models for front capturing methods
 - Performance model for better time control of adaptation
 - Better load balancing algorithms
- A further step could be parallel 4D finite-volume adaptive methods. Does someone has a good 4D simplex-based remesher?

Acknowledgments

- PhDs and postdocs of the YALES2 team
- A. Pushkarev, G. Balarac LEGI, Grenoble
- CPU hours from PRACE, GENCI and CRIANN

