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Ugo Pelay, Lingai Luo, Yilin Fan, Driss Stitou, Cathy Castelain. Integration of a thermochemical energy storage system in a Rankine cycle driven by concentrating solar power: Energy and exergy analyses. *Energy*, 2019, 167, pp.498-510. <10.1016/j.energy.2018.10.163>. <hal-02364774>

HAL Id: hal-02364774

<https://hal.science/hal-02364774v1>

Submitted on 27 Nov 2020

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Integration of a Thermochemical Energy Storage System in a Rankine Cycle Driven by Concentrating Solar Power: Energy and Exergy Analyses

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Abstract:

This paper proposes and investigates novel concepts on the integration of a thermochemical energy storage (TCS) system in a concentrating solar power (CSP) plant. The TCS material used is calcium oxide reacting with water and the power cycle studied is a Rankine cycle driven by CSP. Firstly, three integration concepts on the coupling of the TCS system with the Rankine cycle are proposed, including the thermal integration concept, the mass integration concept and the double turbine concept. Then, an energy analysis is performed to determine and compare the theoretical overall energy efficiency of the proposed concepts. After that, an exergy analysis is also carried out for the selected integration concepts so as to evaluate and compare the overall exergy efficiency of the installation with TCS integration.

The results show that the turbine integration concept has the highest overall energy efficiency (0.392), followed by the thermal integration concept (0.358) and the mass integration concept (0.349) under ideal conditions with 11 h of charging and 13 h of discharging. The energy storage density using calcium hydroxide as the storage media is estimated to be about 100 kWh_e·t⁻¹. Exergy analysis results also indicate that the turbine integration concept seems to be the best option under the tested conditions.

Keywords: Thermal energy storage (TES); Thermochemical; Rankine cycle; Concentrating solar power (CSP); Integration concept; Calcium hydroxide; exergy analysis

Declarations of interest: none

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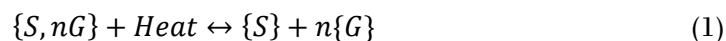
40 I. Introduction

41
42 The increasing energy demand, the environmental protection issue and the national energy
43 independence all over the world call for researches aiming at more efficient use of renewable energy
44 such as solar energy. Among various solar energy technologies, the Concentrating Solar Power (CSP)
45 plants are expected to play an important role in the energetic scenarios owing to its advantages in
46 terms of high efficiency, low operating cost and good scale-up potential [Cáceres 2013; Zhang 2013;
47 Dunham 2014; Balghouthi 2016]. According to IRENA [2016], the CSP deployment would reach
48 44 GW in the reference scenario (Remap 2030). It is estimated that the CSP would contribute up to
49 11.3% of the electricity production in the year 2050, with 954 GW of installed capacity [IEA 2014;
50 del Río 2018].

51
52 One of the advantages of CSP technology is the possibility of integrating a thermal energy
53 storage (TES) function, permitting the production of electricity any time when it is the most needed
54 and valuable, whether during the peak hours, nights, or cloudy intervals [Zhang 2016; Dowling
55 2017; Alva 2018]. To do this, a TES system at high temperature should be designed and installed
56 properly between the solar field and a power cycle. Although adding a TES system usually increases
57 the investment cost of the CSP plant, it improves significantly its adaptability and dispatchability.
58 CSP plants (existing or under construction) having TES systems at high temperature are
59 summarized in recent reviews [e.g., Tian 2013; Kuravi 2013; Pelay 2017a; b]. The storage capacity
60 in terms of discharging time is generally between 3 to 8 hours, and recently up to 15 hours
61 (Gemasolar, Spain) aiming at round-the-clock electricity production driven by solar energy [Dunn
62 2012].

63
64 The most commonly used storage technology is based on the sensible heat storage, in which
65 the thermal energy is stored/released by raising/decreasing the temperature of a storage material.
66 This technology is the most mature and deeply investigated, with a wide variety of both liquid (e.g.,
67 pressurized water, molten salt, mineral oil, etc.) and solid (e.g., sand, rock, cast iron, etc.) materials
68 being used for CSP applications [Gil 2010; Tiskatine 2017]. Some recent developments are also
69 reported, such as on the use of industrial wastes or by-products [Ortega-Fernández 2015; Gutierrez
70 2016], chloride salts [Myers 2016], lithium coupled with molten salts [Cabeza 2015], or solid particles
71 [Zhang 2017a; Calderón 2018]. However, their limited energy density (usually between 60
72 $\text{kWh}_{\text{th}}\cdot\text{m}^{-3}$ (200 °C-300 °C) for sand, rock and mineral oil, and 150 $\text{kWh}_{\text{th}}\cdot\text{m}^{-3}$ for cast iron (200 °C-
73 400 °C) [Fernandes 2012]) increases significantly the size of TES systems. Latent heat storage
74 materials such as Phase Change Materials (PCMs) are also proposed for CSP applications owing to
75 their higher storage capacity [Gil 2010; Pitié 2013; Sharma 2015; Zhang 2017b; Chirino 2018]. But
76 their small thermal conductivity (commonly 0.2 - 0.8 $\text{W}\cdot\text{m}^{-1}\cdot\text{K}^{-1}$) usually limits the heat transfer,
77 resulting in very slow charging and discharging processes [Nithyanandam 2015]. Some new
78 advances on the effective encapsulation of PCMs [Zhang 2014; Parrado 2015] as well as the
79 enhancement of thermal conductivity are summarized in recent papers [Xu 2015; Liu 2016; Alva
80 2018].

82 Besides the sensible and latent heat storage technologies, the thermochemical storage (TCS)
83 is a promising solution for its highest storage capacity (up to 10 times greater than latent storage
84 [Pardo 2014a]), wide accessible temperature range and long storage duration at ambient
85 temperature [Prieto 2016]. This technology is mainly based on reversible chemical reactions (e.g.,
86 gas-solid) involving absorbing or releasing a large amount of reaction heat:



88
89 The charging stage uses solar energy for the decomposition of $\{S, nG\}$ associated with the
90 condensation of the gas while the discharging stage brings the solid and gas into contact for heat
91 release by the exothermic reaction. TCS material candidates at a medium or high temperature (300–
92 1000 °C) for CSP application include metallic hydrides, carbonates system, hydroxides system,
93 redox system, ammonia system and organic system [Kuravi 2013]. Their mains characteristics,
94 advantages/disadvantages and experimental feedback are reviewed and summarized in [Pelay
95 2017a].

96
97 Beyond the testing of new TCS materials [e.g., Deutsch 2017; Valverde 2017;
98 Bagherisereshki 2018] and proper reactor designs [e.g., Álvarez De Miguel 2013; Schmidt 2017;
99 Wokon 2017; Pan 2017] and pilot scale testing [Tescari 2017a; b], the TCS system must be coupled
100 in a proper way with the vapor generator of the power cycle (e.g., Rankine cycle) in a CSP plant.
101 However, relatively little attention seems to be given to this integration issue. Recently, Cabeza et
102 al. [2017] proposed a new concept of consecutive TCS reactions (either one cycle or two coupled
103 cycles) and its implementation in CSP plants, with the purpose of eliminating reversibility problems
104 and therefore improving the overall efficiency. Ortiz et al. [2017] proposed possible integration
105 schemes of calcium looping (CaO-CaCO₃) for power production by direct or indirect means. Their
106 results showed highest plant efficiencies up to 45–46% using a closed carbon dioxide Brayton power
107 cycle. Noteworthy is the very recent work of Schmidt and Linder [2017], in which an integration
108 option of the TCS system into a CSP plant has been proposed and analyzed. Their analysis showed
109 that a storage efficiency up to 87% might be reached when the required steam production during
110 discharge is thermally integrated into the Rankine steam cycle.

111
112 From the above literature survey, one may find that the research on how to integrate the
113 TCS system to the power cycle of the CSP plant is insufficient. Actually, it is an essential issue for
114 the implementation and application of TCS technology, calling for deeper and extensive
115 investigations. The main objectives and originalities of this paper are therefore threefold: (1) to
116 propose various novel integration concepts of TCS system into the Rankine cycle driven by CSP,
117 for both charging and discharging stages; (2) to perform a detailed energy analysis of the proposed
118 integrated concepts and to evaluate impacts of various influencing factors on the overall energy
119 efficiency of the CSP plant; and (3) to discuss and compare the second law efficiency of the proposed
120 integration concepts through an exergy analysis.

121
122 This paper is organized as follows. In section 2, the selected gas-solid reaction and material
123 are briefly introduced and the key issue on how to manage the water vapor from the TCS reactor is

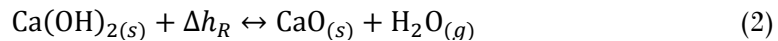
124 identified. Three novel TCS integration concepts (thermal integration, mass integration and turbine
125 integration) are proposed and described in section 3. The performance modelling of the three
126 integration concepts based on energy analysis is presented and discussed in section 4. Section 5
127 provides an exergy analysis of the integration concepts. Finally, main conclusions and future work
128 are summarized in section 6.

130 2. Thermochemical reaction and its operation

131
132 In this section, we briefly introduce the selected gas-solid reaction and materials, as well as
133 the identified key issues for the integration of TCS unit into the Rankine cycle.

134 2.1. Reaction used as TCS storage media

135
136
137 Various hydrates and hydroxides have been proposed as potential TCS materials, as
138 summarized in some latest papers [e.g., Aydin 2015; André 2016; Liu 2016; Prieto 2016; Pelay 2017a;
139 Zhang 2016]. Among them, the CaO/H₂O couple has been deeply studied with a great amount of
140 experimental feedback [e.g., Azpiazu 2003; Michel 2012; Schaube 2013a; b; Pardo 2014b; Yan 2016;
141 2017; Sakellariou 2017]. It is found to be a pertinent candidate as TCS material for CSP application
142 with various features, including for high-temperature use (450~600 °C), good reversibility,
143 operating pressure close to the atmospheric pressure, low material cost, environment-friendly and
144 high energy density (about 3 GJ·m⁻³), etc. As a result, it is selected *a priori* for this conceptual study.
145 The reaction formula is shown in Eq. (2).



147
148 For a reaction temperature at 500 °C, the equilibrium pressure equals to 0.1 MPa (1 bar).
149 Under this condition, the reaction heat (Δh_R) is found to be 104 kJ·mol(CaO)⁻¹=5774.56 kJ·Kg(H₂O)⁻¹
150 [Schaube, 2011].

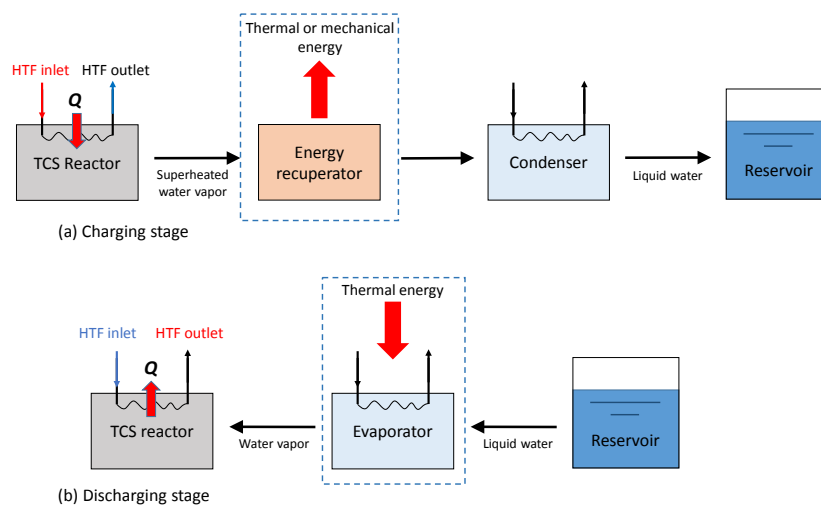
151 152 153 2.2. Management of the water vapor from the TCS reactor

154
155 The integration of TCS reactor in a solar power plant is a so-called passive concept in which
156 the storage medium (CaO) is kept motionless and heated-up or cooled-down by the circulation of a
157 heat transfer fluid (HTF) [Pelay 2017a]. When used as TCS material in a CSP plant, water vapor at
158 high temperature produced by the decomposition during the charging stage should preferably be
159 condensed to saturated liquid and stored in a separate reservoir at ambient pressure (0.1 MPa).
160 Hence the required volume for the storage unit is greatly reduced. Meanwhile, the superheated
161 steam (500 °C) contains a significant amount of thermal energy, a part of which is possible to be
162 recovered so as to increase the overall efficiency of the whole system, as shown in Fig. 1a. Instead
163 of condensing the water vapor directly at the outlet of the TCS reactor by an additional condenser,
164 alternative energy valorization options are actually available, either to produce extra electricity
165 through an additional turbine or to preheat the steam of the Rankine cycle.

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During the discharging stage, the exothermic synthesis happens when CaO and water vapor are in contact. Supposing that the CSP plant is driven only by solar energy, it is necessary to find a heat source to vaporize water stored previously in the liquid form through an evaporator, as shown in Fig. 1b. This heat source should have a higher temperature than that of liquid water to be evaporated (e.g., 100 °C at 1 bar).

As a result, the positioning of TCS reactor in the whole system and the way of managing water vapor are key issues for an energy-efficient integration of TCS unit into the Rankine cycle. Different integration concepts shown in the following section will highlight the options proposed for these key points.



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Figure 1. Management of water vapor as a key issue for energy-efficient TCS integrations into the Rankine cycle. (a) charging stage; (b) discharging stage.

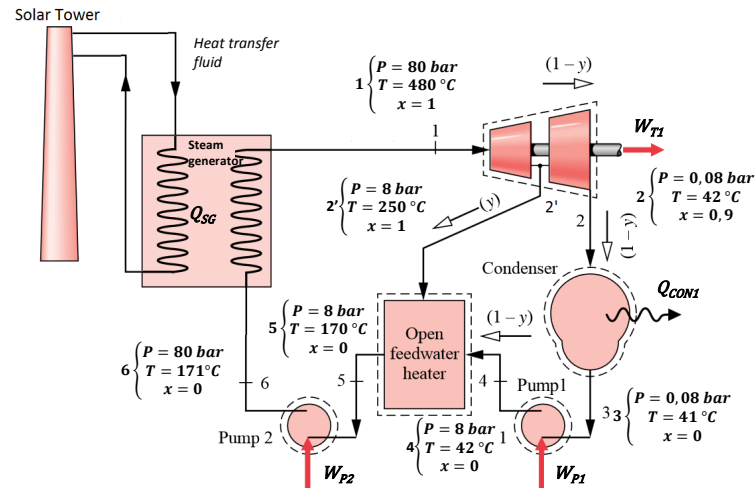
3. TCS integration concepts

In this section, we shall firstly present a conventional regenerative Rankine cycle driven by CSP without storage as a reference case [Moran, 2003]. Then, three novel integration concepts of TCS unit into the Rankine cycle are proposed and described, named as thermal integration, mass integration and turbine integration.

3.1. Conventional Rankine cycle without TES

Figure 2 shows a representative schematic view of the conventional regenerative Rankine cycle driven by CSP. The main components in this cycle include a steam generator, a turbine, a condenser, an open feedwater heater and pumping and piping accessories. Solar energy is firstly absorbed by the solar receiver at the top of solar tower and transferred to the HTF. This amount of thermal energy is then utilized in converting water contained in generator (point 6) into superheated steam at the suitable pressure and temperature (point 1). The superheated steam then flows through

199 the turbine. While doing work in the turbine, the pressure of steam is reduced. The steam leaving
 200 the turbine (point 2) passes through the condenser and is condensed into liquid at low pressure for
 201 recycling. An open (or direct-contact) feedwater heater serves as a mixing chamber where the steam
 202 extracted from the turbine (point 2') mixes with the feedwater leaving the pump (point 4). Ideally,
 203 the mixture leaves the heater as the saturated liquid at the heater pressure (point 5). This steam
 204 regeneration configuration usually enhances the thermal efficiency of the Rankine cycle at the cost
 205 of lower electricity production rate due to steam extraction.
 206



207
 208 Figure 2. Schematic view of a conventional regenerative Rankine cycle driven by CSP without TES [Moran 2003]

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 210

211 3.2. Concept 1: Thermal integration (Thermal Int.)

212

213 The Thermal Int. concept is shown in Fig. 3. The added TCS unit comprises of a TCS reactor,
 214 a water reservoir, a second condenser and two heat exchangers. There are three fluid circuits in the
 215 integrated system: the solar circuit as energy supply, the principal Rankine circuit for power
 216 generation and the TCS circuit for energy storage. Note that although the working fluids are
 217 identical as pure water or steam, the principal Rankine circuit and the TCS circuit are independent
 218 of each other without direct mass contact or exchange. Hence, this concept is named as Thermal
 219 Int. because there is only heat exchange between the TCS circuit and the Rankine circuit.
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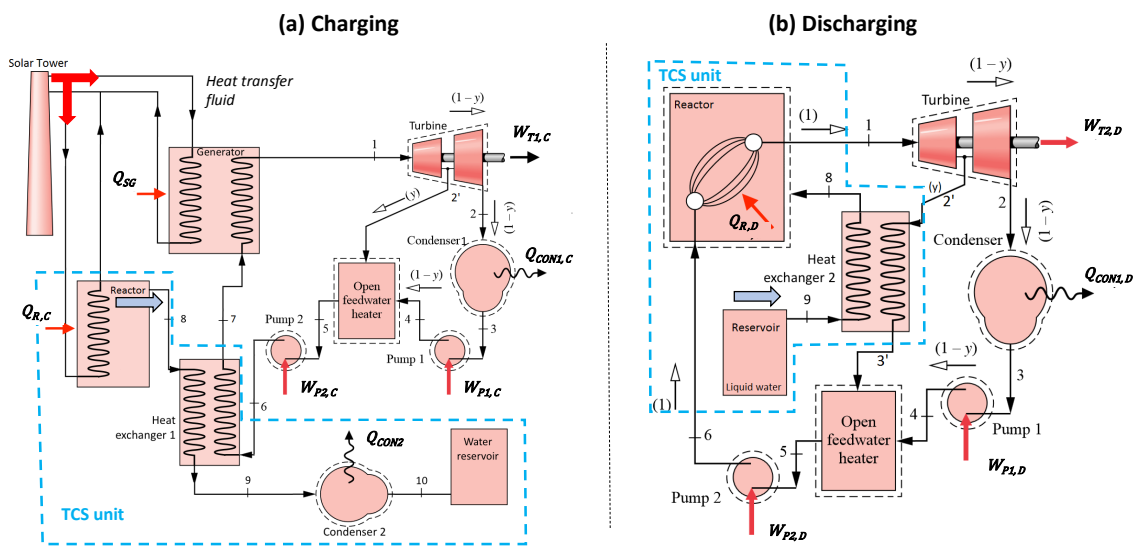
222 During the charging stage (Fig. 3a), the HTF (e.g., pressurized air or molten salt) from the
 223 solar tower offers the steam generator sufficient amount of thermal energy to run the principal
 224 Rankine cycle. Meanwhile, it heats the Ca(OH)_2 reactive salts in the TCS reactor up to 500 °C at 1
 225 bar to initiate the decomposition. The water vapor generated in the TCS reactor is partially
 226 condensed in the heat exchanger 1, then completely condensed in the condenser 2 and finally be
 227 stored as the saturated liquid (100 °C, 1 bar) in a separate water reservoir. The sensible and latent
 228 heat released by the water vapor will be used to preheat the working fluid of the principal Rankine
 229 circuit via heat exchanger 1. The CaO reaction product (and subsequent reactant) remains in the
 230 TCS reactor. This integration concept permits the steady operation of the principal Rankine circuit
 231 for power production and the TES in parallel.

231

232 During the discharging stage (Fig. 3b) when solar energy is not available, the liquid water
 233 stored in the reservoir is firstly heated up and vaporized by the high temperature steam extracted
 234 from the turbine of the principal Rankine circuit via the heat exchanger 2. The saturated vapor
 235 (100 °C, 1 bar) enters then into the TCS reactor and reacts with the CaO for the synthesis of Ca(OH)₂.
 236 The heat released from this exothermic reaction in the TCS reactor runs the principal Rankine cycle
 237 steadily under the same operational conditions (temperature, pressure and steam mass flow-rate) as
 238 during the charging stage. In this case, the TCS reactor also serves as the steam generator.

239
 240 The positive aspect of this concept is that it is technically simple to implement whereas the
 241 disadvantage is that a separate reservoir is required to store the liquid water resulting from the TCS
 242 reaction, implying a higher capital cost.

243



244
 245 Figure 3. Schematic view of the thermal integration concept. (a) charging stage; (b) discharging stage [Luo 2016].

246

247

248 3.3. Concept 2: Mass integration (Mass Int.)

249

250 The Mass Int. concept is shown in Fig. 4. Compared to the conventional Rankine cycle as
 251 shown in Fig. 2, a TCS unit is added including a TCS reactor, a second condenser, a throttle valve,
 252 a third pump and two heat exchangers. There are still three fluid circuits in the installation: the
 253 solar circuit, the principal Rankine circuit and the TCS circuit. But different from the above-
 254 mentioned Thermal Int. concept, the principal Rankine circuit and the TCS circuit are coupled and
 255 share the same working fluid (pure water or steam) with mass exchange. As a result, this concept is
 256 named as Mass Int.

257

258 During the charging stage (Fig. 4a), the water vapor generated in the TCS reactor is partially
 259 condensed in the heat exchanger 1, depressurized by the throttle valve, completely condensed in the
 260 condenser 2 and finally stored as the saturated water (41 °C, 0.008 MPa) in the water reservoir
 261 shared with the principal Rankine circuit. The sensible and latent heat released by the common

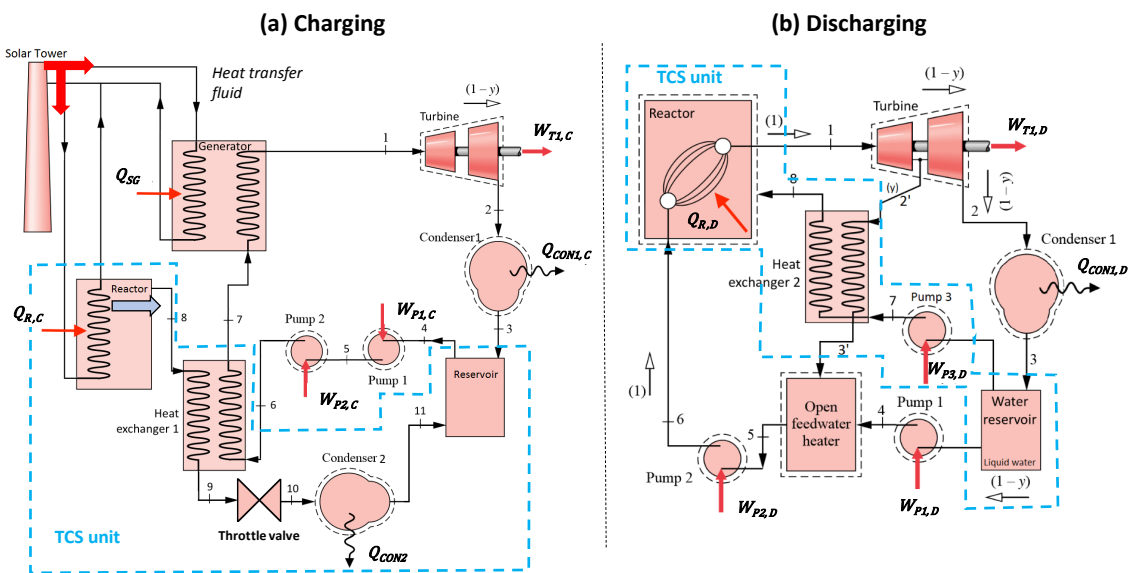
262 water vapor will be used to preheat the working fluid of the Rankine cycle via the heat exchanger 1
 263 located upstream of the steam generator.

264

265 During the discharging stage (Fig. 4b), the liquid water stored in the reservoir will be
 266 pressurized by pump 3 and then evaporated by exchanging heat with the extracted steam via the
 267 heat exchanger 2. The saturated vapor (100 °C, 0.1 MPa) enters the TCS reactor and reacts with the
 268 CaO reactive salts stored inside. Again, the TCS reactor serves as the steam generator to run the
 269 Rankine cycle steadily under the same operational conditions as during the charging stage.

270

271 The Mass Int. concept seems less interesting than the Thermal Int. concept because more
 272 components are required for the TCS unit, implying higher capital costs. Moreover, the mixing of
 273 working fluids between the principal Rankine circuit and the TCS circuit could bring further
 274 technical difficulties because of the massive fines formation. An efficient filtration system (e.g.,
 275 sintered metal fiber or ceramic filters [Smolders 2000]) may have to be implemented for dust removal
 276 to prevent the eventual damage of the turbine. A special design of the TCS reactor coupled with
 277 metal filter may also be considered [Schmidt 2017].
 278



279

280 Figure 4. Schematic view of the mass integration concept. (a) charging stage; (b) discharging stage [Luo 2016].

281

282

283 3.4. Concept 3: Turbine integration (Turbine Int.)

284

285 Figure 5 presents a schematic view of the Turbine Int. concept. Additional components of
 286 the TCS unit include a TCS reactor, a second turbine, a second condenser, a third pump, a water
 287 reservoir and a heat exchanger. The principal Rankine circuit and the TCS circuit are completely
 288 independent of each other during the charging stage (no heat or mass exchange) and thermally
 289 coupled during the discharging stage.

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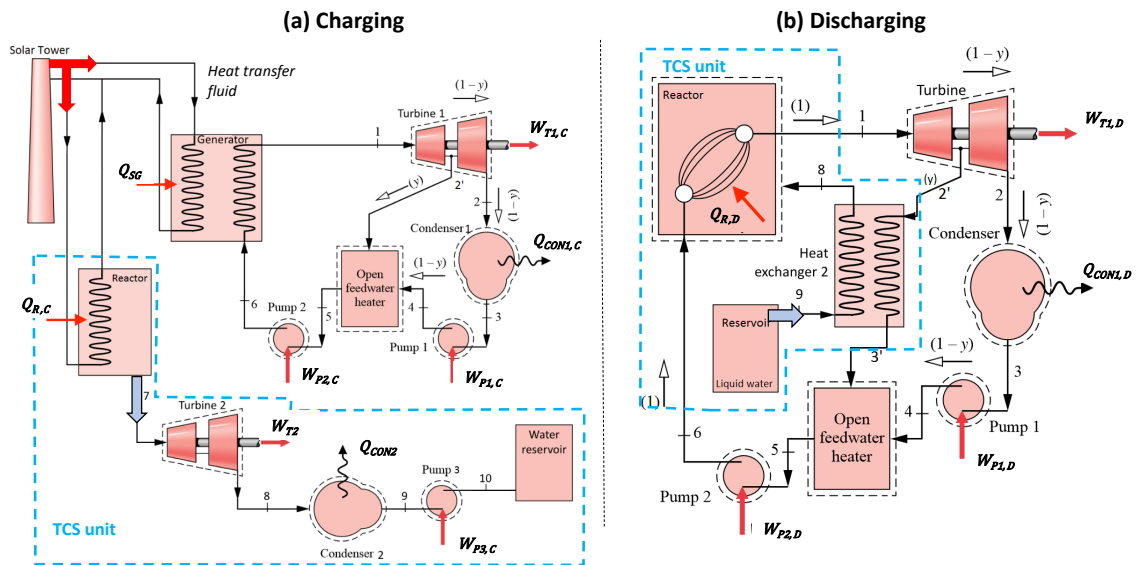
291 During the charging stage (Fig. 5a), the water vapor generated in the TCS reactor passes
 292 through the turbine 2, condensed in the condenser 2 and finally stored as the sub-saturated water

293 (41.5 °C, 0.1 MPa) in a water reservoir. A part of its thermal energy is valorized as power production
 294 via the second turbine. The integration concept for the discharging stage (Fig. 5b) is the same as
 295 that of Thermal Int. concept, in which water stored in the reservoir will be evaporated by
 296 exchanging heat with the extracted steam via the heat exchanger 2.

297

298 The main feature of this concept is the additional power production in parallel of the one
 299 provided by the principal Rankine circuit during the charging stage. However, the implementation
 300 of this second turbine, which is partially used only during the charging stage, implies higher capital
 301 cost for the CSP plant.

302



303

304 Figure 5. Schematic view of the turbine integration concept. (a) charging stage; (b) discharging stage [Luo 2016].

305

306

307 4. Energy analysis of different TCS integration concepts

308

309 This section presents a detailed energy analysis of three proposed concepts of TCS
 310 integration into the Rankine cycle of a CSP plant. Firstly, the performance modelling of each
 311 individual components and of the system as a whole will be described under ideal operating
 312 conditions (as indicated in Fig. 1). Then a parametric study on various influencing factors will be
 313 performed so as to identify appropriate functioning points for different integration concepts towards
 314 performance comparison.

315

316

317 4.1. Performance modelling

318

319 The performance analysis is based on the conservation of mass and energy. To simplify the
 320 calculation, the following assumptions are made, while the influences of certain factors will be
 321 discussed through the parametric study in the later section. Note that the solar receiver and the
 322 solar tower have not been included in the current analysis. It is supposed that the solar field provides

323 the required amount of thermal energy for the power production of the Rankine cycle and the TES
324 during the charging stage.

325

326 (A1) Steady-state operation;

327 (A2) Isentropic compression and expansion processes ($\eta_{isen}=1$);

328 (A3) Evaporation and condensation at constant pressure;

329 (A4) Negligible heat loss; negligible pressure drop of piping system;

330 (A5) During the charging, the water vapor at 500 °C and 0.1 MPa is released from the TCS
331 reactor; during the discharging, the saturated vapor (100 °C, 0.1 MPa) is injected into
332 the TCS reactor; 100% conversion rate of the TCS reactor ($\nu=1$), no mass leakage
333 during the storage;

334 (A6) The power output rate from the turbine of the principal Rankine circuit $W_{T1} = 100 \text{ MW}_{el}$.

Table I. Mass and energy conservation equations for the performance modelling of Rankine cycle with or without TCS integration.

Component	Reference case	Thermal Int.		Mass Int.		Turbine Int.		Note
		charging	discharging	charging	discharging	charging	discharging	
Principal Rankine circuit	Turbine 1 (T1)	$T_{T1}^{in} = 480 \text{ }^\circ\text{C}$, $P_{T1}^{in} = 8.0 \text{ MPa}$; $P_{T1}^{out} = 0.008 \text{ MPa}$; $P_{T1}^{ext} = 0.08 \text{ MPa}$ $W_{T1,C(D)} = m_{Rankine,C(D)}[(h_{T1}^{in} - h_{T1}^{ext}) + (1 - y_{C(D)})(h_{T1}^{ext} - h_{T1}^{out})]$ (3) $\eta_{T1,C(D)} = \frac{h_{T1}^{ext} - h_{T1}^{in}}{h_{T1,isen}^{ext} - h_{T1}^{in}} = \frac{h_{T1}^{out} - h_{T1}^{ext}}{h_{T1,isen}^{out} - h_{T1}^{ext}}$ (4)						N1
	Condenser 1 (CON1)	$Q_{CON1,C(D)} = m_{Rankine,C(D)}(1 - y_{C(D)})(h_{CON1}^{in} - h_{CON1}^{out})$ (5) $P_{CON1}^{in} = P_{CON1}^{out}$						N2
	Pump 1 (P1)	$W_{P1,C(D)} = m_{Rankine,C(D)}(1 - y_{C(D)})(h_{P1}^{out} - h_{P1}^{in})$ (6) $\eta_{P1,C(D)} = \frac{h_{P1,isen}^{out} - h_{P1}^{in}}{h_{P1}^{out} - h_{P1}^{in}}$ (7)						N3
	Feedwater heater (FH)	$y_{C(D)}h_{FH}^{in1} + (1 - y_{C(D)})h_{FH}^{in2} = h_{FH}^{out}$ (8) $P_{FH}^{in1} = P_{FH}^{in2} = P_{FH}^{out}$ (9)		-	-	(8) (9)		
	Pump 2 (P2)	$W_{P2,C(D)} = m_{Rankine,C(D)}(h_{P2}^{out} - h_{P2}^{in})$ (10) $\eta_{P2,C(D)} = \frac{h_{P2,isen}^{out} - h_{P2}^{in}}{h_{P2}^{out} - h_{P2}^{in}}$ (11)						N4
	Steam generator (SG)	$Q_{SG} = m_{Rankine}(h_{SG}^{out} - h_{SG}^{in})$ (12) $P_{SG}^{in} = P_{SG}^{out}$ (13)		-	(12) (13)	-	(12) (13)	-
TCS circuit	TCS reactor (R)	-	$\gamma Q_{R,C} = m_{TCS,c}\Delta h_R$ (14) $Q_{R,D} = \gamma m_{TCS,D}(h_{R,D}^{out} - h_{R,D}^{in})$ (15)	(14)	(15)	(14)	(15)	N5
	Condenser 2 (CON2)	-	$Q_{CON2} = m_{TCS,c}(h_{CON2}^{in} - h_{CON2}^{out})$ (18) $P_{CON2}^{in} = P_{CON2}^{out} = 0.1 \text{ MPa}$ (19)	-	(18)	(18)	(20)	-
	Heat exchanger 1 (HX1)	-	$\frac{h_{HX1,Rankine}^{out}}{m_{Rankine,C}}(h_{HX1,TCS}^x - h_{HX1,TCS}^y) + h_{HX1,Rankine}^{in}$ (21) $\frac{h_{HX1,TCS}^{out}}{m_{Rankine,C}}(h_{HX1,Rankine}^y - h_{HX1,Rankine}^x) + h_{HX1,TCS}^{in}$ (22)	-	(21) (22)	-	-	N6
	Heat exchanger 2 (HX2)	-	-	$m_{TCS,D}(h_{HX2,TCS}^{out} - h_{HX2,TCS}^{in}) =$	-	(23)	-	(23)

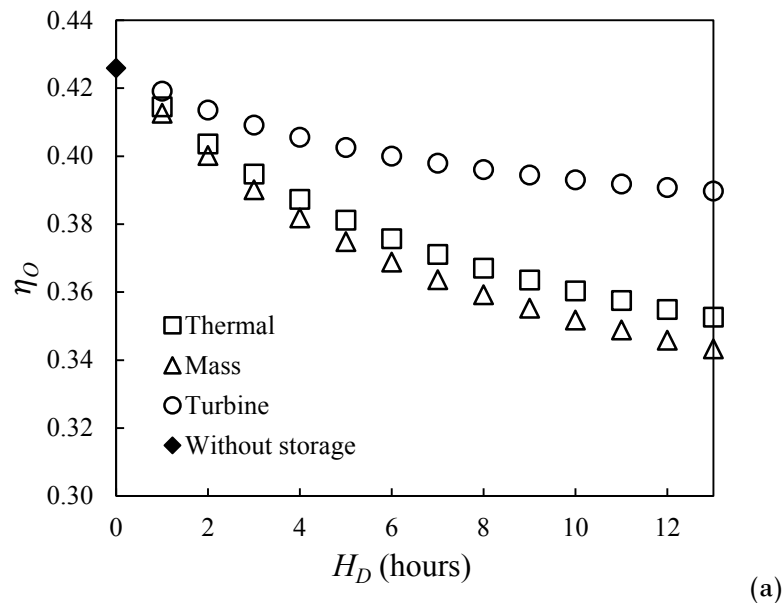
				$y_D m_{Rankine,D} (h_{HX2,Rankine}^{in} - h_{HX2,Rankine}^{out})$ (23)				
Water reservoir (WS)	-	Saturated water at 0.1 MPa		Saturated water at 0.008 MPa		Sub-saturated water (41.5 °C) at 0.1 MPa		N7
Throttle valve (TV)	-	-	-	$h_{TV}^{in} = h_{TV}^{out}$ $P_{TV}^{in} = 0.1 \text{ MPa}; P_{TV}^{out} = 0.008 \text{ MPa}$ (24)	-	-	-	
Pump 3 (P3)	-	-	-	-	$P_{P3}^{in} = 0.008 \text{ MPa}; P_{P3}^{out} = 0.1 \text{ MPa}$ $W_{P3,C(D)} = m_{TCS,C(D)} (h_{P3}^{out} - h_{P3}^{in})$ (25) $\eta_{P3,C(D)} = \frac{h_{P3,isen}^{out} - h_{P3}^{in}}{h_{P3}^{out} - h_{P3}^{in}}$ (26)	-	-	
Turbine 2 (T2)	-	-	-	-	-	$P_{T2}^{out} = 0.008 \text{ MPa}$ $W_{T2} = m_{TCS} (h_{T2}^{in} - h_{T2}^{out})$ (27) $\eta_{T2} = \frac{h_{T2}^{out} - h_{T2}^{in}}{h_{T2,isen}^{out} - h_{T2}^{in}}$ (28)	-	
Overall energy efficiency of the installation	$\frac{\eta_o = W_{T1} - W_{P1} - W_{P2}}{Q_{SG}}$ (29)	$\eta_o = \frac{(W_{T1,C} - W_{P1,C} - W_{P2,C})H_C + (W_{T1,D} - W_{P1,D} - W_{P2,D})H_D}{(Q_{SG} + Q_{R,C})H_C}$ (30)	$\eta_o = \frac{(W_{T1,C} - W_{P1,C} - W_{P2,C})H_C + (W_{T1,D} - W_{P1,D} - W_{P2,D} - W_{P3,D})H_D}{(Q_{SG} + Q_{R,C})H_C}$ (31)	$\eta_o = \frac{(W_{T1,C} + W_{T2,C} - W_{P1,C} - W_{P2,C} - W_{P3,C})H_C + (W_{T1,D} - W_{P1,D} - W_{P2,D})H_D}{(Q_{SG} + Q_{R,C})H_C}$ (32)				N8
<p>N1: saturated steam at the turbine extraction; $y_C=0$ for Mass Int. concept.</p> <p>N2: $y_C=0$ for Mass Int. concept.</p> <p>N3: saturated water at the inlet of P1; $y_C=0$ for Mass Int. concept.</p> <p>N4: $T_{P2}^{in} = 41.6 \text{ °C}$ for the discharging stage of Thermal Int. and Mass Int.; saturated water for the rest of concepts.</p> <p>N5: H_C and H_D are the number of operating hours for charging and for discharging, respectively; γ is the conversion rate of the TCS reactor; Eq. (15) implies that a portion of reaction heat is consumed to heat the saturated vapor (100 °C 0.1 MPa) to the equilibrium temperature of reaction (500 °C 0.1 MPa).</p> <p>N6: X and Y are intermediate points located at the hot side (TCS) and cold side (Rankine) of the HX1, respectively; saturated steam at X point; $T_{HX1,TCS}^{out} - T_{HX1,Rankine}^Y = 5 \text{ °C}$ (pinch point of HX1).</p> <p>N7: no thermal losses during the storage period.</p> <p>N8: Q_{SG} and $Q_{R,C}$ are the amount of heat provided by the HTF; the solar field (solar receiver) is not included in the analysis.</p>								

324 Mass and energy conservation equations for the individual components and for the whole
 325 system of different concepts are listed in Table 1. Values of thermodynamic properties of water and
 326 steam are determined referring to NIST-JANAF Thermochemical Tables [Chase, 1998]. Detailed
 327 values of main status points of the Rankine cycle with or without TCS integration may be found in
 328 the supplementary material of this paper.

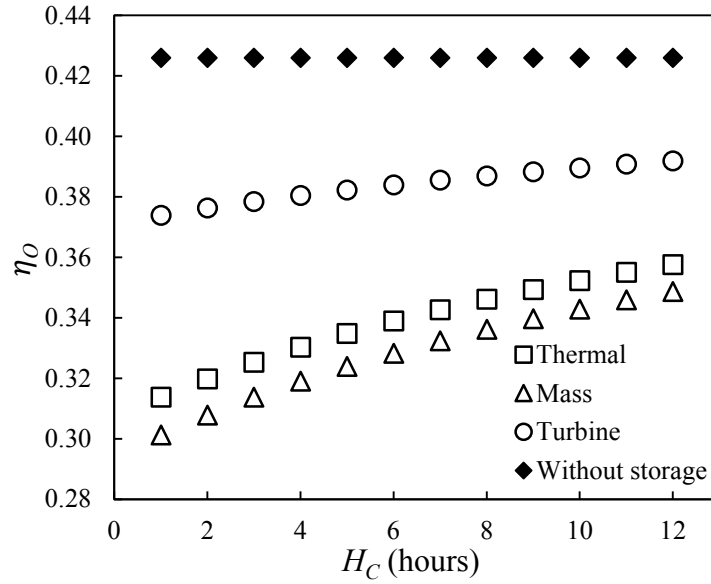
329
 330 Following this modeling procedure, the global performance of three proposed integration
 331 concepts is analyzed and compared with that of conventional Rankine cycle without storage
 332 (reference case). The charging/discharging scenarios examined cover a large variety of operation
 333 possibilities, for the charging time (H_C) varying from 1 hour to 12 hours and the discharging time
 334 (H_D) varying from 0 hour to 13 hours.

335
 336 Figure 6 shows the overall energy efficiency of the installation (η_o) for different integration
 337 concepts under the above-mentioned ideal operational conditions, for various charging (Fig. 6b) and
 338 discharging (Fig. 6a) scenarios. η_o is defined as the total net output work of the Rankine cycle
 339 (during charging and discharging) divided by all the energy absorbed from the HTF of the solar
 340 circuit (during charging), as indicated in Eqs. 29-32.

341
 342 It can be observed from Fig. 6a that for a given charging time ($H_C=11$ h), the values of η_o
 343 with TCS integration are lower than that of the reference case ($\eta_{o,ref}=0.42$) without TCS. This can
 344 be explained by the loss of a part of the energy contained in the superheated vapor produced by the
 345 TCS reactor during the charging hours. A large part of the energy is recovered/valorized via the heat
 346 exchanger 1 (Thermal Int. and Mass Int.) and via the turbine 2 (Turbine Int.). But still, a small part
 347 is lost in the condenser 2. It can also be observed in Fig. 6a that the Turbine Int. has the highest η_o
 348 while the Mass Int. has the lowest. This difference becomes more important with the increasing
 349 number of discharging hours. Figure 6b shows that for a given discharging time ($H_D=12$ h), the η_o
 350 of all concepts of TCS integration increases when the number of charging hours (H_C) increases. It
 351 seems that a low H_D/H_C ratio is favorable to achieve high values η_o when TCS unit is integrated into
 352 the CSP plant.



353



(b)

Figure 6. Overall energy efficiency of the installation (η_0) for different integration concepts under ideal operational conditions. (a) different number of discharging hours ($H_c=11$ h); (b) different number of charging hours ($H_b=12$ h).

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However, longer discharging shows clear advantages in terms of higher dispatchability and higher total power output. As shown in Fig. 7, the daily power output of Turbine Int. could reach 3010 MWh_{el} for 11 hours of charging and 13 hours of discharging (round-the-clock operation), which is augmented by a factor of 2.7 compared to that of the reference case without storage (only 11 hours daily production). The benefits of TCS integration into the CSP plant are therefore highlighted. In real world practice, the operation strategy of the TCS unit certainly deserves detailed investigations by taking various influencing factors into account (e.g., climate condition for charging hour, electricity demand profile for the discharging hour, hourly electricity price for techno-economic consideration, etc.).

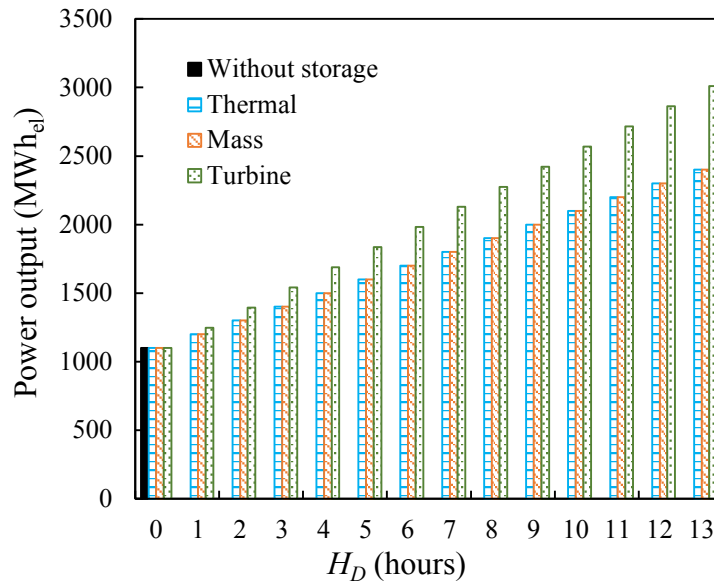


Figure 7. Power production of CSP plants as a function of the number of discharging hours ($H_c=11$ h).

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373 4.2. Parametric study

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375 It should be noted that in section 4.1, the overall energy efficiency is estimated under ideal
376 conditions, neglecting all the losses. From the viewpoint of real-world engineering, it is necessary to
377 evaluate the real performances when actual operational conditions differ from the ideal one. In this
378 section, the impacts of various influencing factors on the overall energy efficiency of the plant are
379 analyzed and discussed. The studied parameters include the isentropic efficiency of turbomachines
380 (turbines and pumps), the steam temperature at the inlet of turbine 1 and the global efficiency of
381 the TCS reactor. Note that to evaluate the separate effect of a certain parameter, only the concerned
382 parameter is varied while others are kept as the ideal operational conditions used for performance
383 modelling in section 4.1.

384

- 385 • *Isentropic efficiency of turbomachines η_{isen}*

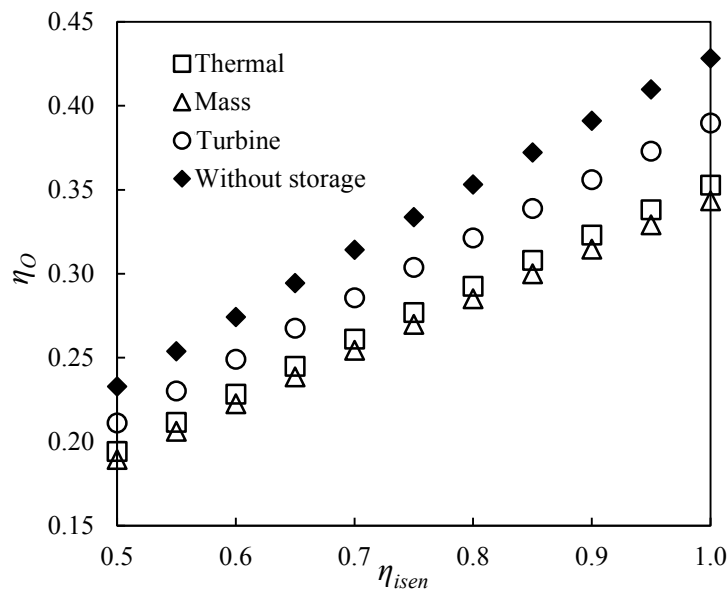
386

387 We define the parameter η_{isen} as the isentropic efficiency of turbine or pumps, to represent
388 non-isentropic compression or expansion processes. Different values of η_{isen} from 0.5 to 1.0 are tested
389 and added to the relevant energy conservation equations for turbines and pumps to determine the
390 values of main status points of the cycle. Note that for simplification purpose, the equal value of
391 η_{isen} is assumed for all turbomachines.

392

393 Figure 8 represents the variation of η_o values for different concepts as a function of the
394 isentropic efficiency of turbomachines. The negative effect of non-isentropic compression/expansion
395 of turbines and pumps can be clearly observed. Each 10% decrement of η_{isen} results in about 4.2-
396 4.5% reduction in the η_o .

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399 Figure 8. Overall energy efficiency (η_o) as a function of the isentropic efficiency (η_{isen}) of turbines and pumps ($H_c=11$ h;

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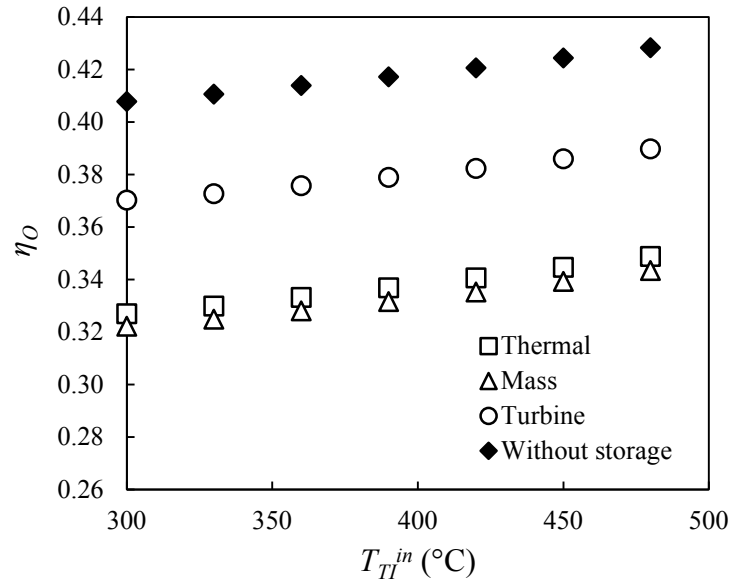
$H_D=13$ h).

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- *Steam temperature at the inlet of turbine 1*

Increasing the steam temperature at the inlet of turbine 1 (T_{T1}^{in}) means the increased temperature of the superheated steam at the outlet of the steam generator (during charging) and the TCS reactor (during discharging). This usually leads to the augmented turbine work output. It may be observed from Fig. 9 that the η_o value increases almost linearly with the increasing T_{T1}^{in} for all the studied concepts.



411

Figure 9. Overall energy efficiency (η_o) as a function of the steam inlet temperature of the turbine T1 ($H_C=11$ h; $H_D=13$ h).

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However, an excessive increase of T_{T1}^{in} may cause the turbine damage. Moreover, higher T_{T1}^{in} requires higher HTF temperature of the solar circuit during the charging and the higher reaction temperature of the TCS reactor during the discharging. Since the equilibrium temperature of $\text{Ca}(\text{OH})_2$ synthesis is related to the pressure (e.g., 540 °C at 0.2 MPa) [Schaube 2012; Zhang 2016], the TCS reactor may have to be pressurized to render higher reaction temperature. This imposes a higher requirement on the TCS reactor design and operation as well as the more complicated control strategy for the whole installation. As a result, $T_{T1}^{in} = 480$ °C (500 °C, 0.1 MPa for the TCS reactor) is selected as an appropriate operational parameter.

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 423
 424

- *TCS reactor efficiency γ*

425

Another influencing factor is the reactor's efficiency, which is defined as the ratio of the effective heat released to the theoretical reaction heat for discharging, or the ratio of the theoretical heat needed to the effective heat absorbed for charging. This factor is closely linked with various aspects including the structure and size of the reactor, the reversibility of the TCS reaction and the chemical stability of the stored materials. Since it is difficult at this stage to quantify the respective impact of each aspect, we introduce the parameter γ as the *global TCS reactor efficiency* taking all

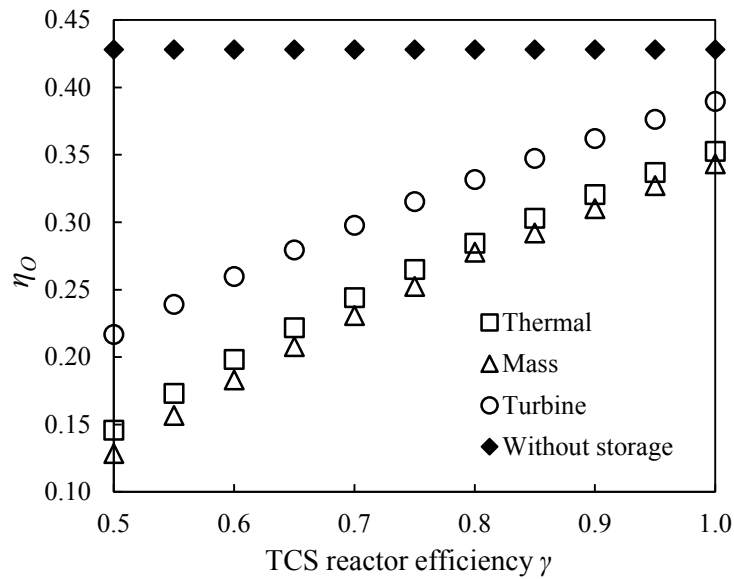
432

433 the related effects into account. We also assume identical γ for charging and for discharging, as
 434 indicated in Table 1. Note that the assumption of constant and identical γ values may not be
 435 appropriate in real practice, since the reversibility of the CaO/Ca(OH)₂ pair will decrease with the
 436 increasing number of operation cycles.

437

438 Figure 10 shows the calculated results of η_o as a function of the global TCS reactor efficiency
 439 γ . It can be observed that the η_o value decreases with the reduced global reactor efficiency. When γ
 440 of the TCS reactor drops from 1.0 to 0.8, the η_o value decreases about 5% for Turbine Int., and
 441 about 7% for Mass Int. and for Thermal Int. Turbine Int. concept still has the best overall energy
 442 efficiency.

443



444

445 Figure 10. Overall energy efficiency (η_o) as a function of the TCS reactor efficiency γ ($H_C=11$ h; $H_D=13$ h).

446

447 Besides the negative impact on the overall energy efficiency, the losses that we studied will
 448 also increase the amount of storage materials needed, thus requiring a larger size of the TCS reactor
 449 for their storage and operation. In real world engineering, special attention should be given to avoid
 450 or minimize the losses to a lower limit.

451

452

453 4.3. Comparison of 3 proposed integration concepts

454

455 The parametric study carried out in section 4.2 permits evaluating the impacts of some
 456 influencing factors on the overall energy efficiency and determining more realistic operational
 457 conditions with respect to the ideal conditions used for performance modelling in section 4.1. Based
 458 on the results obtained, a comparison of the three proposed integration concepts under more realistic
 459 operational conditional is presented in Table 2. Note that detailed values of various parameters are
 460 obtained under the assumptions of $\eta_{isen}=0.85$, $T_{T1}^{in} = 480$ °C, $\gamma=0.95$, $W_{T1,C(D)} = 100$ MW and
 461 round-clock operation ($H_C=11$ h; $H_D=13$ h).

462

463 A size estimation of the TCS unit has been made and the results are recapitulated in Table
464 2. It is shown that the Thermal Int. concept needs a smaller quantity of TCS material (9571 t) than
465 the Mass Int. (10013 t) and the Turbine Int. (9998 t) for 13 hours discharging time. It is because the
466 water vapor from the TCS reactor is stored as saturated liquid (100 °C, 0.1 MPa) for the Thermal
467 Int. whereas for Mass Int. and Turbine Int. concepts, the water is stored at 41.5 °C. Therefore, a bit
468 more quantity of TCS materials is needed for the latter two concepts to compensate this temperature
469 difference.

Table 2. Comparison on the energy performance of three proposed integration concepts under more realistic operating conditions ($\eta_{isen}=0.85$, $T_{T1}^{in} = 480$ °C, $\gamma=0.95$, $W_{T1,C(D)} = 100$ MW and round-clock operation ($H_C=11$ h; $H_D=13$ h).

	η_o	Operational data			Heat exchange rate						Work exchange rate			Size of storage unit		
		$m_{Rankine}$ (kg·s ⁻¹)	m_{TCS} (kg·s ⁻¹)	γ	SG (MW)	CON1 (MW)	CON2 (MW)	HX2 (MW)	HX1 (MW)	R (MW)	T1 (MW)	T2 (MW)	P1+2+3 (MW)	Mass of water stored (t)	Mass of CaO stored (t)	
Thermal Int.	Discharging	0.295	144	80	0.67	-	78.0	-	181.4	-	378.7	100	-	1.0	3079	9571
	Charging		91	95	0	190.8	188.7	194.4	-	97.3	548.3	100	-	0.6		
Mass Int.	Discharging	0.286	151	84	0.72	-	87.0	-	210.3	-	396.2	100	-	1.0	3221	10013
	Charging		91	99	0	187.1	188.8	228.3	-	121.2	573.7	100	-	0.6		
Turbine Int.	Discharging	0.327	151	84	0.72	-	87.1	-	210.0	-	395.6	100	-	1.50	3217	9998
	Charging		102	92	0.20	268.3	169.4	251.4	-	-	531.6	100	53.7	1.0		

462 The energy storage density is roughly estimated to be about $100 \text{ kWh}_{\text{el}}\cdot\text{t}^{-1}$. This value is
463 about seven times higher than that of existing CSP plants using molten salt as energy storage media
464 (eg. for Andasol1 Spain, the heat reservoir consists of two tanks measuring 14 m in height and 36 m
465 in diameter and containing 28500 tons of molten salts, enough to run the turbine for about 7.5 hours
466 at $50 \text{ MW}_{\text{el}}$ [Pelay 2017b]. The energy storage density is calculated to be $13.1 \text{ kWh}_{\text{el}}\cdot\text{t}^{-1}$). Higher
467 energy storage density implies more compact storage unit and less heat loss of the storage reservoirs.

468
469 A first comparison between the three proposed integration concepts can then be made.
470 Firstly, the Turbine Int. concept is the most interesting ($\eta_o=0.327$) in terms of overall energy
471 efficiency. However, a second turbine is needed, implying the higher initial cost. Particular attention
472 should be given to the purity of steam leaving the TCS reactor that may cause the mechanical failure
473 of the second turbine. Efficient filtration measures are indispensable for dust removal as has been
474 discussed above. Secondly, the Mass Int. concept is the least attractive ($\eta_o=0.286$). In fact, the
475 mixing of working fluids between principal Rankine circuit and the TCS circuit may not be a good
476 option again due to the purity issue that could be vital to the turbine. Finally, the Thermal Int.
477 concept does not possess the highest overall energy efficiency, but its simple and robust design makes
478 it relatively easy towards implementation. Moreover, relatively small volumes of reservoirs are
479 required based on the size estimation reported above.

480
481

482 5. Exergy analysis of different TCS integration concepts

483

484 The previous section presents a comparison of the three proposed integration concepts based
485 on the energy analysis (first law of thermodynamics). Meanwhile, an exergy balance will also be
486 beneficial by providing supplemental insights on the quality of the energy, taking the irreversibility
487 notion of the processes into account [Dincer 2002; Rosen 2003; Kang 2018]. The main purpose of
488 this section is hence to evaluate and compare the overall exergy efficiency of the three proposed
489 integration concepts through an exergy analysis. Note that the exergy analysis and the modelling
490 results presented hereafter are obtained under realistic operating conditions ($\eta_{\text{isen}}=0.85$ and $\gamma=0.95$)
491 as specified in sections 4.3.

492
493

494 5.1. Performance modelling for the exergy analysis

495

496 Exergy as a thermodynamic notion means the maximum work extracted from a stream as
497 the stream reaches the dead state [Bejan, 1988]. The total exergy of a system Ex includes four
498 components, namely physical exergy, kinetic exergy, potential exergy and chemical exergy [Rosen
499 2003]. Neglecting the potential and kinetic exergy changes, the exergy balance of different
500 components may be modelled as follows.

501

- 502 • *Turbine or pump*

503

$$\dot{l} = mT_0 \cdot \Delta s \quad (33)$$

$$\varepsilon = 1 - \dot{l}/(\dot{E}x_{in} + m\Delta h) \quad (34)$$

504

- *Heat exchanger*

506

$$\dot{l} = -(\Delta\dot{E}x_{hot} + \Delta\dot{E}x_{cold}) \quad (35)$$

$$\varepsilon = 1 - \dot{l}/(\dot{E}x_{hot_{in}} + \dot{E}x_{cold_{in}}) \quad (36)$$

507

- *Steam generator or condenser*

509

$$\dot{l} = mT_0\Delta s + \frac{T_0}{T}Q \quad (37)$$

$$\varepsilon = 1 - \dot{l}/\dot{E}x_{in} \quad (38)$$

510

- *TCS reactor*

512

$$\dot{l}_R = \sum \dot{E}x_{in_{tot}} - \sum \dot{E}x_{out_{tot}} - \left(\sum \dot{l}_{tot} - \dot{l}_R \right) \quad (39)$$

513

514 Where h (J·kg⁻¹) is the specific enthalpy, $\dot{E}x$ (W) the exergy and s (J·K⁻¹·kg⁻¹) the specific
 515 entropy. \dot{l} (W) is the exergy destruction of the component and ε is the exergy efficiency of the
 516 component. The overall exergy efficiency of the CSP plant η_{ex} is defined as the ratio of the exergy
 517 extracted by turbine(s) to the amount of exergy provided by the HTF of the solar circuit.

518

$$\eta_{ex} = \frac{\sum \dot{E}x_{out}}{\sum \dot{E}x_{in}} \quad (40)$$

519

520

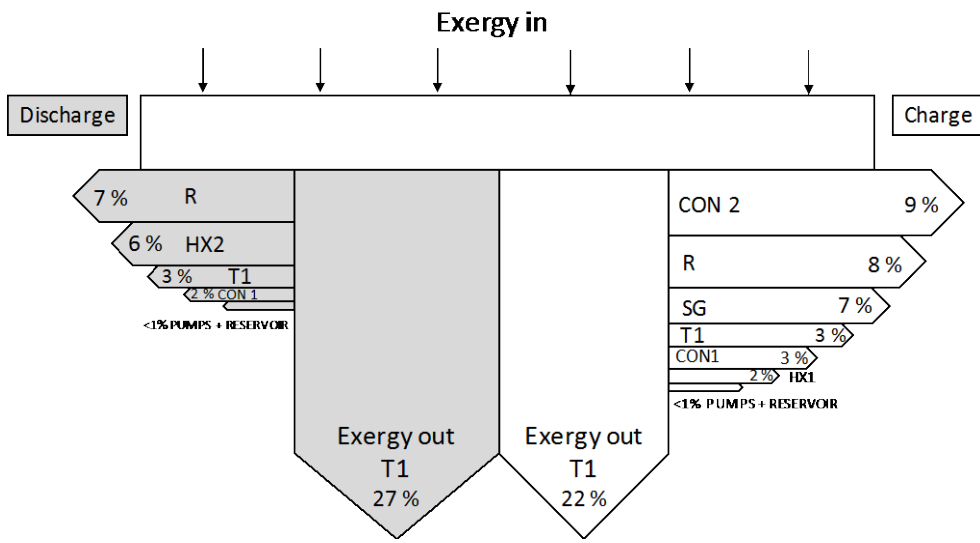
5.2. Results and discussion

522

523 An exergy analysis has been performed for the three proposed integration concepts. Figure
 524 11 shows the exergy flow-chart for each integration concept comprising of both the charging and
 525 the discharging stages. Note that the reference temperature T_0 was chosen as 5 °C, a value lower
 526 than those of the whole system. It allows an easier reading and interpretation of the results obtained.

527

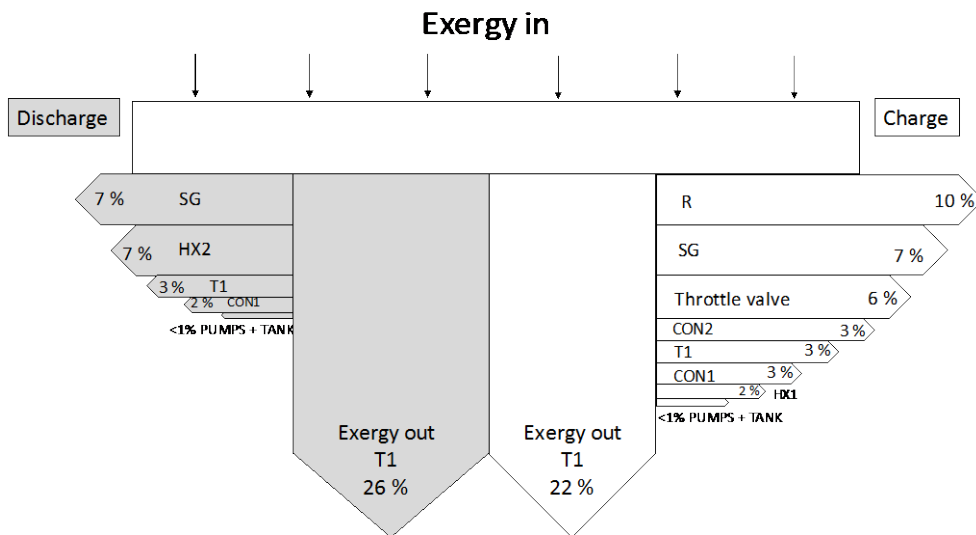
528 The exergy flow-chart for the Thermal Int. concept is shown in Fig. 11a, indicating that the
 529 overall exergy efficiency (η_{ex}) equals to 0.49. It can be observed that the highest exergy destructions
 530 happen in the TCS reactor and in the heat exchanger (HX2) during discharging whereas in the steam
 531 generator, in the TCS reactor and in the condenser (CON2) during charging. These exergy
 532 destructions are mainly due to the irreversibilities caused by the large amount of heat transfer in
 533 these components. Note that exergy destructions in the reservoir and in pumps are negligible. A
 534 close look at each component indicates that the CON2 with a very low exergy efficiency ($\varepsilon_{CON2}=0.19$)
 535 during charging stage is the main cause of exergy destruction.



537

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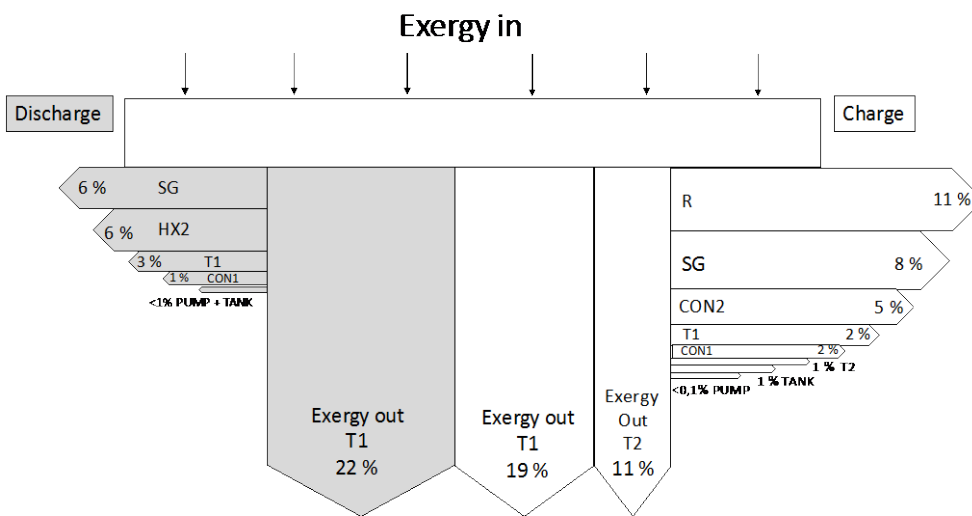
(a)



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540

(b)



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542

543

(c)

Figure 11. Exergy flow-chart and overall exergy efficiency (η_{ex}) for three proposed integration concepts. (a) Thermal integration concept; (b) Mass integration concept; (c) Turbine integration concept.

544

545 The Mass Int. concept has a slightly lower η_{ex} value (0.48). It can be observed from Fig. 11b
546 that the TCS reactor is the main component of exergy destruction during charging and discharging.
547 The HX2 during discharging, the SG and throttle valve (TV) during charging also have high exergy
548 destructions compared to those in reservoirs or pumps. Similar to the Thermal Int. concept, these
549 losses are mainly due to the irreversibilities caused by the large amount of heat transfer in these
550 components. An option to improve the ε_{TV} is to release the fluid at a pressure higher than 0.008
551 MPa. Nevertheless, the condensed water should be stored separately instead of sharing a common
552 reservoir which is the distinguishing feature of the Mass Int. concept.

553

554 The Turbine Int. concept has the highest exergy efficiency ($\eta_{ex}=0.52$) among the three.
555 Figure 11c indicates that the highest exergy destructions happen in the TCS reactor and in the HX2
556 during discharging whereas in the TCS reactor, in the SG and in the CON2 during charging. The
557 TCS reactor represents the highest exergy destruction of the system while the CON2 has the lowest
558 exergy efficiency ($\varepsilon_{CON2}=0.27$).

559

560 In brief, the exergy analysis of the three proposed integration concepts confirms that, in
561 terms of overall exergy efficiency of the installation, the Turbine Int. concept is the most attractive
562 ($\eta_{ex}=0.52$), followed by the Thermal Int. concept ($\eta_{ex}=0.49$) and then the Mass Int. concept
563 ($\eta_{ex}=0.48$).

564

565

566 **6. Conclusion and prospects**

567

568 This paper presents a conceptual study of three different TCS integration concepts in a
569 Rankine cycle driven by CSP. The TCS material used in this study is the CaO/Ca(OH)₂ couple. Based
570 on the energy and exergy analyses, main conclusions could be reached as follows.

571

572 • Different integration concepts are feasible by coupling the TCS system with a Rankine cycle
573 and by carefully determining flow circuit configurations and working conditions for
574 charging and discharging stages.

575

576 • The overall energy efficiency of the installation under ideal conditions is evaluated to be
577 0.358 for the Thermal Int. concept, 0.349 for the Mass Int. concept and 0.392 for the Turbine
578 Int. concept, respectively ($H_C=11$; $H_D=13$). Compared to the reference case without storage,
579 the TCS integration decreases the overall energy efficiency but improves the adaptability
580 and dispatchability of CSP plants with the increased power production.

581

582 • The energy storage density using calcium hydroxide as storage media is roughly estimated
583 to be about 100 kWh_{el}·t⁻¹; this value is about seven times higher than that of existing CSP
584 plant with a sensible heat storage using molten salt (about 13.1 kWh_{el}·t⁻¹).

585

- 586 • Different types of losses would cause a reduced overall energy efficiency of the installation.
 587 Non-isentropic compression/expansion and poor efficiency of the TCS reactor would have
 588 significant negative impacts on the overall energy efficiency.
 589
- 590 • Among the three proposed integration concepts, the Turbine Int. concept seems to be the
 591 best option with the highest overall energy and exergy efficiencies under the tested
 592 conditions.
 593

594 It should be noted that this study has focused on the integration conception issue, and
 595 promising findings have been obtained for this essential step. Nevertheless, a number of scientific &
 596 technological barriers remain to be overcome for the real implementation of TCS systems in CSP
 597 plants. Our ongoing work includes the dynamic simulation of each individual components (including
 598 the solar receiver and the TCS reactor) and the whole installation under real conditions. The techno-
 599 economic considerations in TCS evaluation are also our study focus, so as to assess the feasibility of
 600 such TCS integration into a real CSP plant. The results obtained on these remaining issues will be
 601 presented in future papers.
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 603
 604

605 **Acknowledgement**

606

607 This work was supported by the French ANR within the project In-STORES (ANR-12-
 608 SEED-0008). The authors also wish to thank the colleagues of laboratory PROMES (CNRS UPR
 609 8521) also involved in this ANR project, for fruitful and inspiring discussions.
 610
 611
 612

613 **Nomenclature**

614

615 *Latin letters*

616	$\dot{E}x$	exergy, W
617	H	charging or discharging time, h
618	h	specific enthalpy, $\text{kJ}\cdot\text{kg}^{-1}$
619	\dot{l}	exergy destruction, W
620	m	mass flowrate, $\text{kg}\cdot\text{s}^{-1}$
621	n	number of mole
622	P	pressure, Pa
623	Q	heat exchange rate, W
624	s	specific entropy, $\text{kJ}\cdot\text{kg}^{-1}\cdot\text{K}^{-1}$
625	T	temperature, $^{\circ}\text{C}$
626	T_0	reference temperature, 5°C
627	W	work exchange rate, W
628	x	mass fraction of vapor

629	y	fraction of extracted steam
630	X, Y	intermediate points for the modeling of HX1
631		
632		
633	<i>Greek symbols</i>	
634	γ	global reactor efficiency
635	ε	exergy efficiency of component
636	Δh_R	reaction heat, $\text{kJ}\cdot\text{kg}^{-1}$
637	η_o	overall energy efficiency
638	η_{isen}	isentropic efficiency of turbine and pumps
639	η_{ex}	overall exergy efficiency
640		
641		
642	<i>Subscripts/superscripts</i>	
643	C	charging stage
644	D	discharging stage
645	el	electricity
646	ext	extraction
647	in	inlet
648	isen	isentropic
649	out	outlet
650	steam	steam
651	th	thermal
652	tot	total
653		
654		
655	<i>Abbreviation</i>	
656	CON	condenser
657	CSP	concentrating solar power
658	FH	feedwater heater
659	HTF	heat transfer fluid
660	HX	heat exchanger
661	Int.	integration
662	P	pump
663	PCM	phase change material
664	R	reactor
665	Rankine	Rankine circuit
666	SG	steam generator
667	T	turbine
668	TCS	thermochemical energy storage
669	TES	thermal energy storage
670	TV	throttle valve
671	WS	water reservoir

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