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1 **Viscous sintering kinetics of biopolymer filaments extruded for 3D printing**

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9

10 **Abstract**

11 The characteristic time for viscous sintering of thermoplastics is an important parameter in
12 industrial processes such as welding, rotational moulding but also additive manufacturing. For
13 Additive Manufacturing by Material Extrusion (AM-ME), it gives information about
14 spreading dynamics. An experimental setup was designed to characterize the viscous sintering
15 of cylindrical filaments (extruded for AM-ME) under controlled thermal conditions. It
16 consists of a small thermally controlled oven, coupled with an image acquisition system to
17 follow-up the coalescing cylinders' cross section shape. The evolution of the bonding angle
18 and the convexity index can be calculated to evaluate the temperature dependence of the
19 characteristic time for viscous sintering and the final sintering quality. This approach was
20 applied to glycerol plasticized zein, a biopolymer formulated for AM-ME processing. A
21 processing window (120-130°C) was identified where a high convexity index is reached
22 within a characteristic sintering time close to that of ABS in AM-ME processing conditions.

23

24 **Keywords**

25 Image analysis; Material extrusion; Model; Viscous sintering; Zein

26

27 1. Introduction

28 The viscous sintering kinetics of thermoplastic polymers has been a key for the understanding
29 and optimization of widely spread industrial processes such as welding and rotational
30 moulding and more recently 3D printing by Selective Laser Sintering (SLS) [1, 2]. In these
31 processes involving spherical particles, the classical model of Frenkel [3] developed for
32 ceramics (and later corrected by Eshelby [4] to satisfy the continuity equation) was first
33 applied: a Newtonian viscous flow under the action of surface tension between two identical
34 spherical objects of initial radius a_0 [m] is generally assumed (Fig. 1). However, an
35 experimental study on rotational moulding polymers showed limitations of the Frenkel-
36 Eshelby's model [5]. Thus, a modified model was proposed in order to take into account the
37 variation of the radius a during sintering and to extend the description of initial coalescence
38 stages [6]:

$$39 \frac{d\theta}{dt} = \left(\frac{a_0 \cdot \mu}{\Gamma} \right)^{-1} \cdot \frac{2^{-\frac{5}{3}} \cdot \cos(\theta) \cdot \sin(\theta) \cdot (2 - \cos(\theta))^{\frac{1}{3}}}{(1 - \cos(\theta)) \cdot (1 + \cos(\theta))^{\frac{1}{3}}} \quad (\text{Eq. 1})$$

40 Where $a(t)$ [m] and $x(t)$ [m] are respectively the radius of the particles and the radius of the
41 neck (Fig. 1, step 2), which define the bonding angle $\theta(t)$ [rad]:

$$42 \theta = \sin^{-1} \left(\frac{x}{a} \right) \quad (\text{Eq. 2})$$

43 Eq. 1 is thus governed by the characteristic time for viscous sintering $t_{vs1} = \left(\frac{a_0 \cdot \mu}{\Gamma} \right)$ [s]. The
44 surface tension of the polymer melt, Γ [N.m⁻¹], acts as a driving force, whereas the melt
45 viscosity, μ [Pa.s], acts as a limiting one during coalescence.

46 For sintering of particles of polymers typically used in rotational moulding (HDPE and
47 LLDPE) under isothermal conditions, the numerical solution of Eq. 1 showed significantly
48 better predictions than the Frenkel-Eshelby's model [6]. The experimental data were obtained

49 using an optical microscope equipped with a temperature controlled heat chamber, to monitor
50 the coalescence of polymer particles placed on a glass plate.

51 Actually, Eq.1 was later used by its authors to model bond formation between polymer
52 filaments in Additive Manufacturing (AM) by Material Extrusion process (AM-ME, known
53 under the trade name “Fused Deposition Modelling”, FDM): The same experimental approach
54 was applied to study the coalescence of thin slices of extruded filaments of ABS, a standard
55 amorphous polymer for AM-ME process, under optical microscope [7]. More recently, a
56 different experimental setup was proposed to study the sintering of real filaments of semi-
57 crystalline thermoplastic polymers dedicated to AM-ME [8]: two extruded filaments are
58 placed in a transparent oven allowing monitoring the coalescence of the filaments upon
59 controlled heating temperature ramps. In this case, images acquisition (1frame/5s) allowed the
60 measurement of the bonding neck as a function of time. Such experiments validated the
61 predictions of the model (Eq. 1) for PLA, the main semi-crystalline polymer used in AM-ME,
62 as well as for PEEK at higher temperature.

63 However, the application of Eq.1 to model bond formation between polymer filaments in
64 AM-ME is questionable for two reasons:

65 1) Eq. 1 is supposed to describe the sintering kinetics of spherical particles, not
66 cylindrical filaments. To our knowledge, the only model for the reliable prediction of
67 sintering kinetics for two identical cylinders was proposed by Hopper [9]. This model
68 cannot be expressed in a single differential equation. It is based on the geometrical
69 description of the two cylinders cross section by an inverse ellipse of constant area.

70 The author gives the numerical solution in the form of a table of values of:

71
$$\left(\frac{\Gamma.t}{\mu.a_0} \cdot \frac{1}{\sqrt{2}}\right) = \left(\frac{t}{t_{vs2}} \cdot \frac{1}{\sqrt{2}}\right) \text{ vs. } \left(\frac{x}{a_0} \cdot \frac{1}{\sqrt{2}}\right).$$

72 The $\frac{1}{\sqrt{2}}$ factor actually comes from the assumption that after complete coalescence, a
73 single cylinder of radius $a_f = \sqrt{2}.a_0$ is obtained. Compared to the predictions of the

74 model for spherical particles (Eq. 1) those from Hopper's model for cylinders show
75 similar results at the beginning of sintering, up to $x/a_0 = 0.8$. However, noticeable
76 differences, about 10%, are obtained at the completion of coalescence, with final x/a_0
77 $= 1.41$ for Hopper's model and $x/a_0 = 1.26$ when applying Eq. 1 [6]. However,
78 Hopper's model was not used in later works on cylinder coalescence [7, 8].

79 2) Recent experimental [10] and modelling results [11] suggest that viscous sintering
80 is not the main phenomenon involved in bond formation during AM-ME. Infrared
81 thermography measurements [10] during the process showed that the cooling rate of
82 the deposited filaments is extremely fast (≈ 100 °C/min) and that the temperature at the
83 interface between two filaments does not stay above the glass transition temperature
84 more than 1 to 2 s. For that reason, a recent modelling work [11] insists on the role of
85 polymer chain interdiffusion at the interface between filaments (Fig. 1, step 3), which
86 occurs much faster than viscous sintering kinetics described by Eq.1, and is known to
87 be a key phenomenon affecting the final quality of the bond adhesion [12]. However,
88 the same authors point out that their model neglects the polymer spreading dynamics
89 at the filaments interface that necessarily precedes and affects chain interdiffusion
90 [11]. Indeed, it is known that spreading dynamics are governed by a same
91 characteristic time $\left(\frac{a_0 \cdot \mu}{r}\right)$ [13], that is to say the same characteristic time involved in
92 viscous sintering t_{vs1} , or $t_{vs2} = \left(\frac{a_0 \cdot \mu}{r}\right)$ [s].

93 Therefore, while studying viscous sintering kinetics of filaments does not mimic the whole
94 complexity of AM-ME, it provides an interesting way to access the temperature dependence
95 of a characteristic time that is of strong interest in the perspective of a detailed understanding
96 and modelling of this process. So, the present work has the following objectives:

- 97 - The design of an experimental setup allowing the monitoring of the coalescence of
98 polymer filaments by a camera, at temperatures ranging from the extrusion
99 temperature used in AM-ME, down to significantly lower temperatures.
- 100 - The development of an image advanced analysis of the frames taken by the camera
101 to sharply characterize the sintering kinetics.
- 102 - The identification of the characteristic time for viscous sintering at different
103 temperatures by modelling the experimental data by both Eq. 1 (spherical particles
104 approximation) and the model of Hopper for cylinders.

105 This approach is applied to a biopolymer recently pointed out as a candidate for the AM-ME
106 process and formulated in this purpose: Zein, a protein from corn, with potential applications
107 as a biomaterial taking advantage of its bioresorbability [14].

108

109 **2. Experimental**

110 *2.1. Raw materials and plasticized zein processing*

111 Commercial zein in the powdery state (Ref. Z3625, containing 5% moisture) and glycerol,
112 used as a plasticizer, were purchased from Sigma-Aldrich (Saint-Quentin-Fallavier, FR).
113 These materials were mixed in a household kneader (De'longhi Kenwood; Clichy, FR) for 2
114 min at 20 °C, to obtain the formulation based on zein with 20w% glycerol. This mixture was
115 processed with a twin-screw microcompounder (Haake Minilab, Thermo Scientific GmbH;
116 Karlsruhe, DE) at 130 °C, to extrude the plasticized zein through a cylindrical die ($\varnothing_{\text{filament}} = 2$
117 mm). The extruded filaments were cut as cylinders with a constant length, $L_{\text{filament}} = 5$ mm, for
118 subsequent fusion bonding trials. Longer cylinders (20 mm) were also cut for Dynamic
119 Mechanical Analysis.

120 *2.2. Cylindrical filament sintering experimental setup*

121 The “hardware” experimental setup (Fig. 2-a) is inspired by the design recently described by
122 Bakrani *et al.* [8] for the sintering of two horizontally adjacent extruded filaments. However,
123 various parameters have been optimized for the specific objectives of the present work:

124 - The internal dimensions of the oven ($20 \times 10 \times 50 \text{ mm}^3$) are significantly reduced.
125 Such a small volume of this thermostated chamber allows rapid heating of the cavity
126 machined in a sole parallelepiped aluminium block. The front of the cavity is a
127 transparent glass plate, while the back is equipped with 3 LEDs ($\varnothing_{\text{LED}} = 3.6 \text{ mm}$, 6500
128 K, 39 lm; OSRAM Opto Semiconductors, Regensburg, DE) mounted in series for
129 backlighting the two cylinders.

130 - A great attention was paid to thermal control and monitoring: the oven was equipped
131 with a temperature controller (Model 1/16 DIN with automated PID, $48 \times 48 \times 100$
132 mm^3 ; RKC Instrument Inc.; Tokyo, JP) and 4 electrical thermal resistances ($\varnothing_{\text{resistance}} =$
133 6.5 mm and $L_{\text{resistance}} = 40 \text{ mm}$, $P = 30 \text{ W}$ each; RS Pro Components SAS, Beauvais,
134 FR) embedded at each of the four corners of the oven. The regulation thermocouple
135 (Type T) was located at the middle of the horizontal upper wall of the oven, in contact
136 with the metal surface. A second thermocouple (type K) was located in the medium
137 part of the oven cavity in order to monitor the environment temperature (T_{oven} , [$^{\circ}\text{C}$]).

138 - A high image acquisition rate was used (1 frame.s^{-1}): A CMOS camera (EXO model,
139 SVS-Vistek GmbH; Seefeld, DE) equipped with a 20 mm length optical extension and
140 a magnifying lens (Computar model 5.6-32 C macroX10; CBC, Cary, NC, US) has
141 been placed in front of the glass window (Fig. 2-b). This camera allows the acquisition
142 at 1 frame.s^{-1} of contrasted images coded on 8 bits (256 grey levels, as Tagged Image
143 Format files “.TIF”) of the cylinders’ cross section. The resolution was determined
144 with a Vernier calliper for each sintering sequence. The average value was found at
145 $150 \text{ pixels.mm}^{-1}$.

146 The experimental procedure involves three successive steps:

147 i) Setting the desired sintering temperature T_{set} on the temperature controller, from 80
148 °C to 140 °C. In this interval, it takes about 7 min to reach a stabilized value $T_{\text{oven}} = T_{\text{set}} \pm 0.1$
149 °C in the cavity.

150 ii) Introducing the filaments after opening and closing the transparent window. After
151 this opening/closing sequence, the temperature of the cavity slightly decreases but it takes 10
152 to 20 s for the system to stabilize again at $T_{\text{oven}} \approx T_{\text{set}}$.

153 iii) Starting image acquisition.

154 For each temperature T_{set} , experimental trials have been triplicated. In order to monitor
155 precisely the temperature of the filaments, a fourth series of experiments was performed in
156 which a thin thermocouple (type K, $\varnothing_{\text{thermocouple}} \approx 0.4$ mm) was located inside one of the two
157 filaments, to measure the temperature at the core of the extruded material (T_{filament} , [°C]). The
158 filament was finely drilled to its half-length in order to insert the thermocouple tip.

159 *2.3. Image analysis*

160 In the initial images, the section of the two extruded filaments and their fusion bonding neck
161 appear as a dark shape on a bright background (Fig. 2-b). An example of their evolution
162 during a sintering sequence at a temperature $T_{\text{set}} = 130$ °C is shown on Fig. 3-a.

163 The successive steps of the image analysis involve: (i) the selection of the region of interest
164 (ROI) by cropping the initial image; (ii) the segmentation by image thresholding carried out
165 with ImageJ (free software; National Institute for Health, US), to obtain binary images with
166 one white object on a black background; (iii) the morphological analysis (implemented on
167 Matlab; The MathWorks Inc., Natick, MA, US).

168 The following morphological descriptors have been defined in order to calculate the bonding
169 angle evolution $\theta(t)$ (Eq. 2):

170 - The minimum vertical length, L_{Min} , equal to $2.x$ (Fig. 1), corresponding to the
171 bonding neck length.

172 - The two maximum vertical lengths, L_{MaxL} and L_{MaxR} , for the left and right areas,
173 respectively (Fig. 3-b). Their average value, L_{Max} , is used to calculate the equivalent radius of
174 the filaments given by:

$$175 \quad a = \frac{L_{Max}}{2} = \frac{(L_{MaxL} + L_{MaxR})}{4} \quad (\text{Eq. 3})$$

176 Application of Eq. 2 gives the bonding angle:

$$177 \quad \theta = \sin^{-1}\left(\frac{x}{a}\right) = \sin^{-1}\left(\frac{L_{Min}}{L_{Max}}\right) \quad (\text{Eq. 4})$$

178 Additional morphological descriptors were defined in order to calculate a convexity index of
179 the system, I_{Convex} (Fig.3-b):

180 - The left (S_L) and right (S_R) cylinder's areas.

181 - The convex area, S_{Convex} , corresponding to the whole object of the segmented images.

182 It includes S_L and S_R , and the concavities between filaments.

183 A sketch depicting S_L , S_R and S_{Convex} is shown on Fig. 3-b. The convexity index, I_{Convex} [-], is
184 defined as:

$$185 \quad I_{Convex} = \frac{(S_L + S_R)}{S_{Convex}} \quad (\text{Eq. 5})$$

186 I_{convex} reaches the value 1 if the fusion bonding leads to a perfect welding of filaments,
187 without any residual concavity between them [15].

188 2.4. Characterization of plasticized zein

189 Dynamic Mechanical Analysis (DMA, Model 50N-O1dB; Metravib, Lyon, FR) was
190 performed on cylindrical filaments. Prior to DMA trials, extrudates were coated with a
191 silicone-based hydrophobic grease to limit their dehydration. The mechanical active length
192 between the two grips was set at 10 mm and the extrudates were characterized in the tensile
193 mode at 1Hz, with a strain set at 0.1 % and heating rate $3 \text{ }^\circ\text{C}\cdot\text{min}^{-1}$.

194

195 **3. Results and discussion**

196 The typical evolution of the oven and filament temperatures at the start of sintering
197 experiments is shown on Figure 4. At $t = 0$, the transparent window is closed and temperature
198 (and image) acquisition is started. As stated in the experimental section, it typically takes 10
199 to 20 s for T_{oven} to come back to the regulated T_{set} value. However, it can be seen that it takes
200 more time for the filament core to heat up. It was assumed that the system reached steady
201 state for $(T_{\text{oven}} - T_{\text{filament}}) < 5$ °C. Typically that corresponds to 35 s at 130 °C, slightly higher
202 than the value of 15 to 20 s, reported in the case of thermomicroscopy trials at 190 °C on
203 thermoplastic particles ($\varnothing \approx 0.5$ mm) between glass plates [5].

204 The time dependences of the bonding angle and the convexity index obtained from image
205 morphological analysis are plotted on Figure 5. In order to compare the sintering rates at
206 different temperatures, the slopes $d\theta/dt$ [$\text{rad}\cdot\text{s}^{-1}$] were evaluated for $t = 35$ s (Table 1). This
207 time was chosen on the basis of filament temperature measurements to ensure isothermal
208 steady conditions (Fig. 4). The maximum (final) values of the convexity index ($I_{\text{convex_final}}$) are
209 also reported in Table 1. Three different behaviours can be depicted:

210 - For the lowest temperatures (80 °C and 100 °C), the sintering kinetics are very slow
211 ($d\theta/dt$ about $3\cdot 10^{-4}$ $\text{rad}\cdot\text{s}^{-1}$ and $28\cdot 10^{-4}$ $\text{rad}\cdot\text{s}^{-1}$, respectively; Table 1) and sintering is far from
212 being complete even for long residence times: the final convexity index values, close to 0.9,
213 are reached after more than 800 s (out of the plot range). This means that the concavities
214 between the sintered filaments still represent 10 % of the cross section surface, with final
215 bonding angles remaining low ($\theta_{\text{final}} < 0.4$ and 0.8 rad, respectively; Table 1).

216 - For the highest temperature (140 °C), sintering appears very fast ($d\theta/dt > 0.06$ $\text{rad}\cdot\text{s}^{-1}$)
217 (Fig. 5-a and Table 1). However, the convexity index curve (Fig. 5-b) suddenly drops
218 around 30 s. This drop reflects an expansion of the material due to the formation of bubbles

219 because of plasticizer vaporization. The induced variations in filament dimensions lead to a
220 jagged bonding angle curve (Fig. 5-a). It also has to be noted that the values plotted are
221 average values, whereas the standard deviations are very large in this case (Table 1).

222 - In the interval [120, 130°C], the maximum (final) values of the convexity index are
223 close, from 0.972 to 0.987, indicating an almost perfect sintering without residual concavity
224 and high final bonding angle, $\theta_{\text{final}} > 1$ rad (Table 1). The time necessary to reach this final
225 state decreases with temperature, while sintering rates show a threefold increase (from about
226 0.011 to 0.036 rad.s⁻¹).

227 **These results illustrate the significance of the convexity index obtained from morphological**
228 **analysis, as a sensitive indicator of the temperature dependence of the sintering quality.** It
229 allows detecting expansion problems at higher temperatures, and residual concavity at lower
230 ones.

231 The values of θ and $d\theta/dt$ at $t = 35$ s in Table 1 can be used to evaluate the characteristic time
232 for viscous sintering t_{vs1} simply by using Eq. 1 [6]. The same determination with Hopper's
233 model [9] requires the calculation of a master curve (Fig. 6): On this curve ($d\theta / d(t/t_{vs2})$) is
234 plotted as a function of θ . The values were calculated from the numerical data $\left(\frac{\Gamma \cdot t}{\mu \cdot a_0} \cdot \frac{1}{\sqrt{2}}\right) =$
235 $\left(\frac{t}{t_{vs2}} \cdot \frac{1}{\sqrt{2}}\right)$ vs. $\left(\frac{x}{a_0} \cdot \frac{1}{\sqrt{2}}\right) \approx \left(\sin \theta \cdot \frac{1}{\sqrt{2}}\right)$ given in Hopper's article. For each temperature, taking
236 the value of θ at $t = 35$ s, the value of t_{vs2} is given by the following relation after reporting our
237 experimental data on the master curve:

$$238 \left(\frac{d\theta}{d\left(\frac{t}{t_{vs2}}\right)}\right) = t_{vs2} \cdot \left(\frac{d\theta}{dt}\right) \quad (\text{Eq. 6})$$

239 The comparison of the characteristic times for viscous sintering obtained with Eq. 1 and
240 Hopper's model master curve, given in Table 1 as the ratio t_{vs1}/t_{vs2} , shows that, except for the
241 lower temperatures (80-100 °C), the assumption that cylinders sintering can be modelled by
242 Eq. 1 developed for spherical particles is quite reasonable.

243 We have reported the values of the characteristic time for viscous sintering obtained using the
244 Hopper's model, t_{vs2} , on Figure 7. The processing window for fast sintering in AM-ME is
245 shown as a grey area. Figure 7 also shows the main mechanical relaxation associated to the
246 glass transition of plasticized zein filament observed in DMA. At 25 °C, the material is in the
247 glassy state, with a storage modulus E' close to 1 GPa. This modulus decreases with
248 temperature, taking values close to the loss modulus E'' which displays a maximum at $T_{peak_E''}$
249 $\approx 45 - 48$ °C, close to the glass transition temperature previously determined by differential
250 scanning calorimetry, $T_g = 42$ °C for the same composition [16]. Beyond 75-80 °C, the
251 moduli measurements become unreliable due to creeping. Actually, in a previous rheological
252 study on zein plasticized by glycerol, we showed that in this temperature range, the material
253 starts to flow, under shear, the loss modulus being higher than the storage modulus [16]. For
254 lower temperatures, above the relaxation associated to the glass transition, sintering is still
255 possible, but slow, with characteristic times much larger than 100 s. For higher temperatures,
256 at 140 °C, the expansion of the material ascribed to plasticizer evaporation perturbs the
257 coalescence. Finally, in the 120-130 °C range, corresponding to $T_g + 80-90$ °C, the estimated
258 characteristic time for viscous sintering decreases from 82 s to 25 s.

259 The values obtained for the viscous sintering of plasticized zein melt can be compared to
260 those of ABS at its AM-ME processing temperature $T = 240$ °C. Assuming $|\eta^*|_{ABS_240^\circ C} =$
261 5100 Pa.s, $\Gamma_{ABS_240^\circ C} = 29$ mN.m⁻¹ and $2.a0_{ABS_240^\circ C} = 0.47$ mm [7, 17], we obtain $t_{vs_ABS_240^\circ C}$
262 ≈ 41 s. This value is very close to the one estimated in this study for the characteristic
263 sintering time of plasticized zein. In previous studies, the processability of plasticized zein by
264 AM-ME was first ascribed to its rheological behaviour at 120-130 °C [16], similar to that of
265 ABS at 230-270 °C. This similarity is confirmed for the characteristic time for viscous
266 sintering and suggests that the values of surface tension of the two polymers in the molten
267 state are also close.

268 In future works, the experimental design and image morphological analysis system described
269 in the present study could be used to characterize the viscous sintering behaviour of other
270 materials, and especially those developed for AM-ME. Moreover, in the present work, we
271 considered only the shape evolution of the two cylinders cross section. As pointed out in the
272 introduction, the quality of the bond obtained by sintering involves polymer chains
273 interdiffusion through the bonding interface (Fig. 1, step 3). The experimental device may
274 actually be used to produce samples for variable sintering times, in order to test the evolution
275 of adhesion with time and temperature.

276

277 **4. Conclusions**

278 An experimental setup has been designed for the characterization of viscous sintering between
279 two polymer cylinders. It consists of a small thermally controlled oven, coupled with an
280 image acquisition system. The coalescing cylinders' cross section shape is determined as a
281 function of time by morphological analysis. The two key variables monitored are the bonding
282 angle and the convexity index. The knowledge of the evolution of the bonding angle allows
283 quantifying the temperature dependence of the characteristic time for viscous sintering, t_{vs} ,
284 while the convexity index, I_{convex} , is shown to be a sensitive indicator of the temperature
285 dependence of the sintering quality.

286 This approach is illustrated in the case of glycerol plasticized zein, a biobased thermoplastic
287 material formulated for Additive Manufacturing by Material Extrusion (AM-ME). A narrow
288 processing window (120-130 °C, corresponding to $T_g + 80-90$ °C) is identified using the
289 values of t_{vs} and I_{convex} obtained at different sintering temperatures. In this window, the value
290 of t_{vs} for glycerol plasticized zein is close to the one of ABS at its typical AM-ME processing
291 temperature.

292

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297 **References**

- 298 [1] J. Boyd, W.T.J. West, S. Wu, E.S. Takacs, J. Vlachopoulos, M.R. Thompson, Automated
299 image analysis to characterize the melt densification stage of polymer sintering processes,
300 *Polymer Testing* 60 (2017) 242-249.
- 301 [2] L. Xin, M. Boutaous, S.H. Xin, D.A. Siginer, Multiphysical modeling of the heating phase
302 in the polymer powder bed fusion process, *Additive Manufacturing*, 18, (2017).121-135.
- 303 [3] J. Frenkel, Viscous flow of crystalline bodies under the action of surface tension, *Journal*
304 *of Physics (USSR)* 9 (1945) 385- 391.
- 305 [4] J. Eshelby, Discussion of ‘Seminar on the Kinetics of Sintering’. *Metallurgical*
306 *Transactions* 185 (1949) 796–813.
- 307 [5] C.T. Bellehumeur, M.K. Bisaria, J. Vlachopoulos, An experimental study and model
308 assesment of polymer sintering. *Polymer Engineering and Science* 36(17) (1996) 2198-2207.
- 309 [6] O. Pokluda, C.T. Bellehumeur, J. Vlachopoulos, Modification of Frenkel’s Model for
310 Sintering, *AIChE Journal*, 43(12) (1997) 3253-3256.
- 311 [7] C. Bellehumeur, L. Li, Q. Sun, P. Gu, Modeling of bond formation between polymer
312 filaments in the fused deposition modeling process, *Journal of Manufacturing Processes* 6
313 (2004) 170-178.
- 314 [8] S. Bakrani, F. Chabert, V. Nassiet, A. Cantarel, C. Garnier, Toward improvement of the
315 properties of parts manufactured by FFF (Fused Filament Fabrication) through understanding
316 the influence of temperature and rheological behaviour on the coalescence phenomenon, *AIP*
317 *Conference Proceedings* 1896, 040008 (2017), doi: 10.1063/1.5008034.
- 318 [9] R.W. Hopper, Coalescence of Two Equal Cylinders: Results for Creeping Viscous Plane
319 Flow Driven by Capillarity, *Communications of the American Ceramic Society* (1984) C262-
320 C264.

- 321 [10] J.E. Seppala, K.D. Migler, Infrared thermography of welding zones produced by polymer
322 extrusion additive manufacturing, *Additive Manufacturing* 12, Part A (2016) 71-76.
- 323 [11] C. McIlroy, P.D. Olmsted, Disentanglement effects on welding behaviour of polymer
324 melts during the fused-filament-fabrication method for additive manufacturing, *Polymer* 123
325 (2017) 376-391.
- 326 [12] C.A. Butler, R.L. McCullough, R. Pitchumani, J.W. Gillespie, An analysis of
327 mechanisms governing fusion bonding of thermoplastic composites, *Journal of Thermoplastic*
328 *Composite Materials* 11(4) (1998) 338-363.
- 329 [13] R.S. Crockett, P.D. Calvert, The liquid-to-solid transition in stereodeposition techniques,
330 7th Solid Freeform Fabrication (SFF) Symposium, Univ Texas Austin, Conference
331 Proceedings, (1996) 257-264.
- 332 [14] L. Chaunier, S. Guessasma, S. Belhabib, G. Della Valle, D. Lourdin, E. Leroy, Material
333 extrusion of plant biopolymers: opportunities & challenges for 3D printing, *Additive*
334 *Manufacturing* 21 (2018) 220-233.
- 335 [15] D. Legland, J. Beaugrand, Automated clustering of lignocellulosic fibres based on
336 morphometric features and using clustering of variables, *Industrial Crops and Products* 45
337 (2013) 253-261.
- 338 [16] L. Chaunier, G. Della Valle, M. Dalgarrondo, D. Lourdin, D. Marion, E. Leroy,
339 Rheology and structural changes of plasticized zeins in the molten state, *Rheologica Acta*
340 56(11) (2017) 941-953.
- 341 [17] Q. Sun, G.M. Rizvi, C.T. Bellehumeur, P. Gu, Effect of processing conditions on the
342 bonding quality of FDM polymer filaments, *Rapid Prototyping Journal* 14(2) (2008) 72-80.

343 **Figure captions**

344 **Figure 1.** Fusion bonding steps at high temperature between two model circular thermoplastic
345 particles: 1- intimate contact, 2- apparition of a bonding neck, 3- neck growth due to polymer
346 diffusion through interface and 4- randomization for long time.

347

348 **Figure 2.** Scheme and photos of the experimental sintering device to follow up the
349 coalescence of polymer cylinders: (a) Thermally regulated oven ($20 \times 10 \times 50 \text{ mm}^3$) equipped
350 with an internal backlighting and a CMOS camera with magnifying lens for image
351 acquisition. (b) Photos of the experimental device and example of cylinders' cross section
352 initial image, at $t = 0 \text{ s}$, of a sintering sequence between two zein-based extruded filaments at
353 130°C with $\varnothing_{\text{filament}} = 2 \text{ mm}$.

354

355 **Figure 3.** Successive steps presented for some selected images acquired during 60 s of a
356 typical sintering sequence at 130°C between two zein-based extruded filaments: (a)
357 Acquisition of images in 256 grey levels; after selection of the Region Of Interest (ROI),
358 segmentation by thresholding (binary image); pre-treated images ready for the morphological
359 analysis with the automated identification of each of the two initial filaments sections. (b)

360 Sketch depicting the morphological descriptors S_L , S_R and S_{Convex} used for the calculation of
361 the convexity index, I_{Convex} (Eq. 5).

362

363 **Figure 4.** Evolutions of the temperatures in the oven and at the core of zein-based extruded
364 filaments for $T_{\text{set}} = 80^\circ\text{C}$, 100°C and 130°C .

365

366 **Figure 5.** Evolutions of the bonding angle, θ [rad], (a) and the convexity index, I_{convex} [-], (b)
367 during the sintering of two zein-based extruded filaments at different temperatures.

368

369 **Figure 6.** Master curve for the Hopper's model and experimental points.

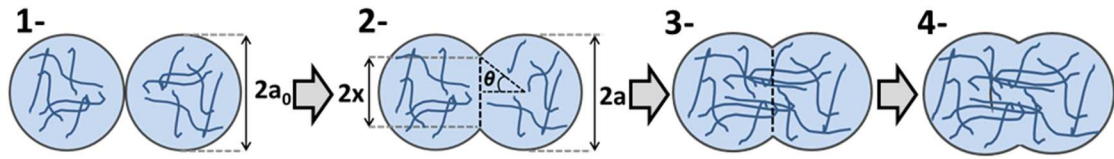
370

371 **Figure 7.** Thermomechanical properties of a zein-based extruded filament assessed by DMA
372 (E' , the storage modulus [Pa] and E'' , the loss modulus [Pa]) and average characteristic time
373 for viscous sintering using the Hopper's model (from Table 1). Peak of the loss modulus, E'' ,
374 is indicated by a black vertical arrow and the processing window by AM-EM is represented as
375 a grey area.

376

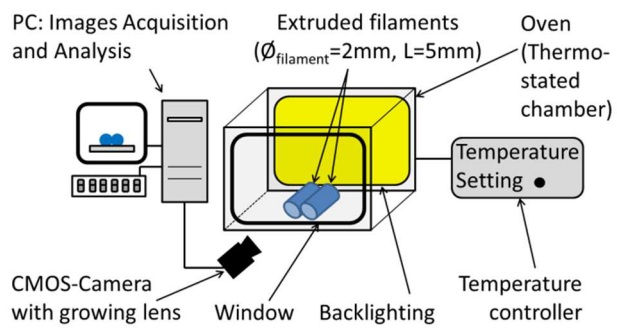
377

378 **Figure 1.** Chaunier *et al.*



379

a-



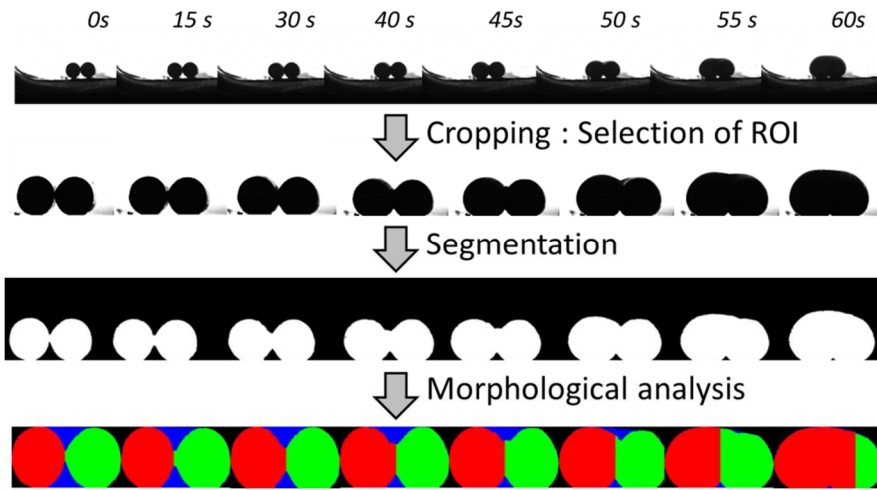
b-



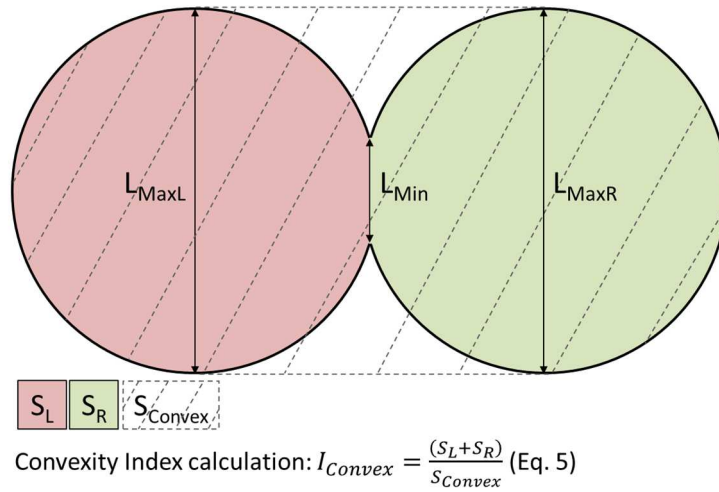
380

381 **Figure 2.** Chaunier *et al.*

a-

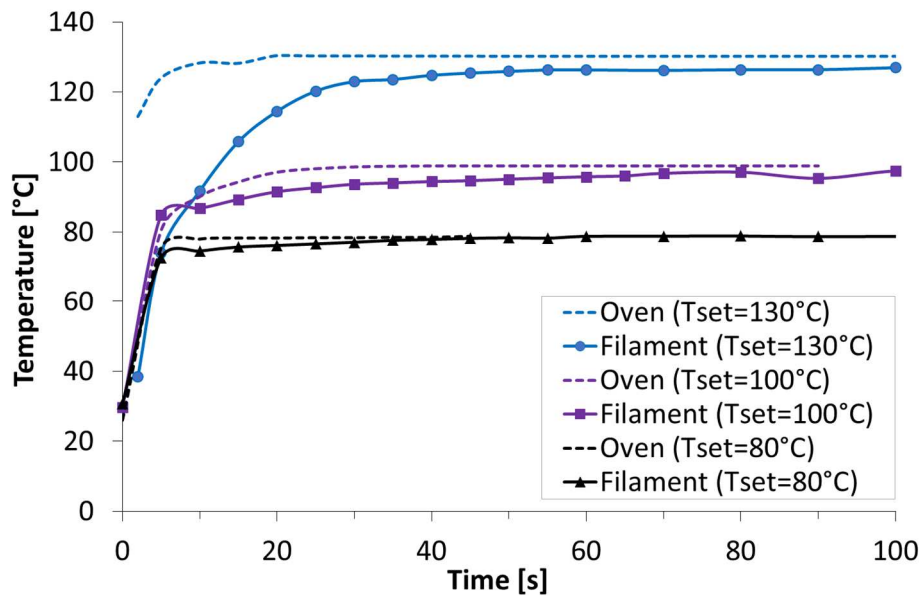


b-



384 **Figure 3.** Chaunier *et al.*

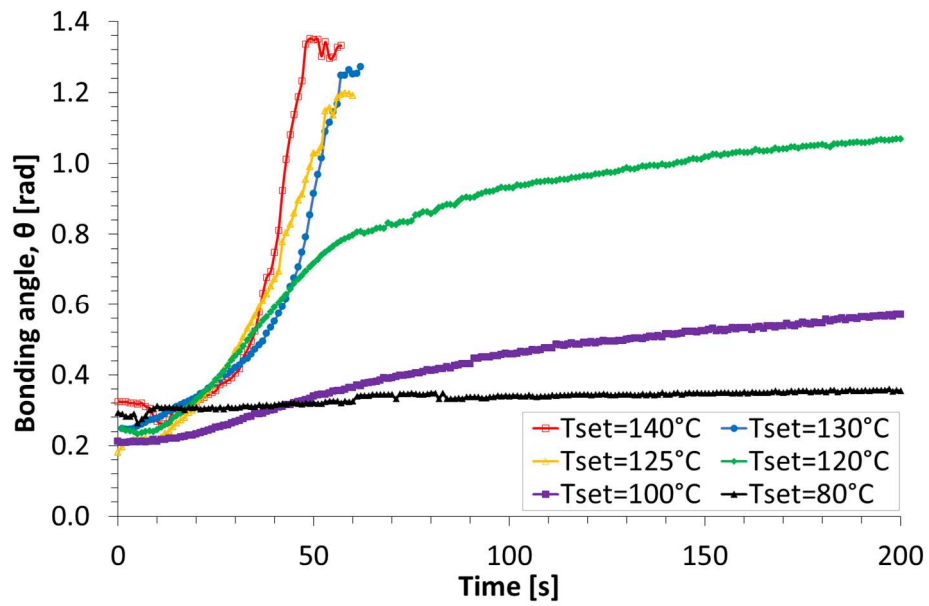
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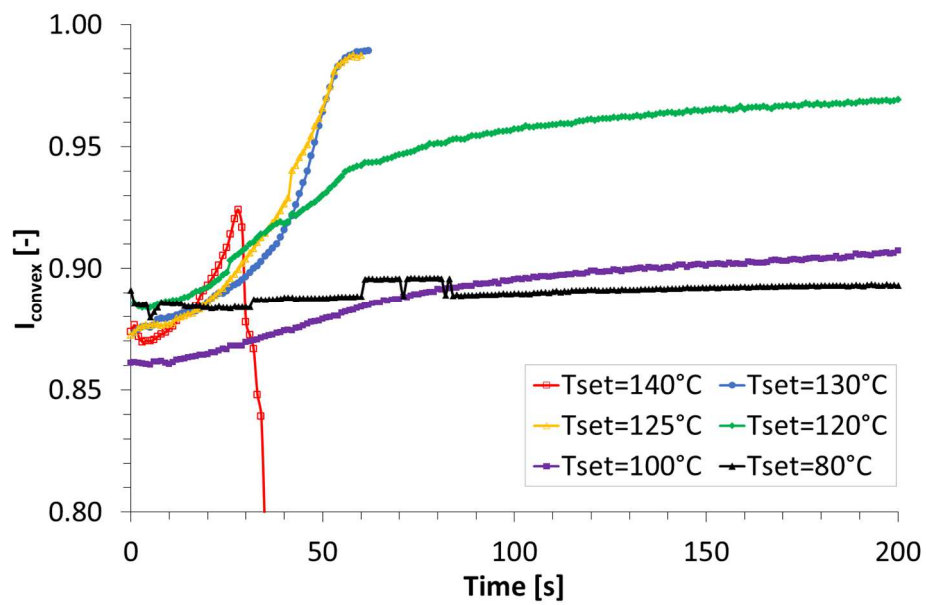
386

387 **Figure 4.** Chaunier *et al.*

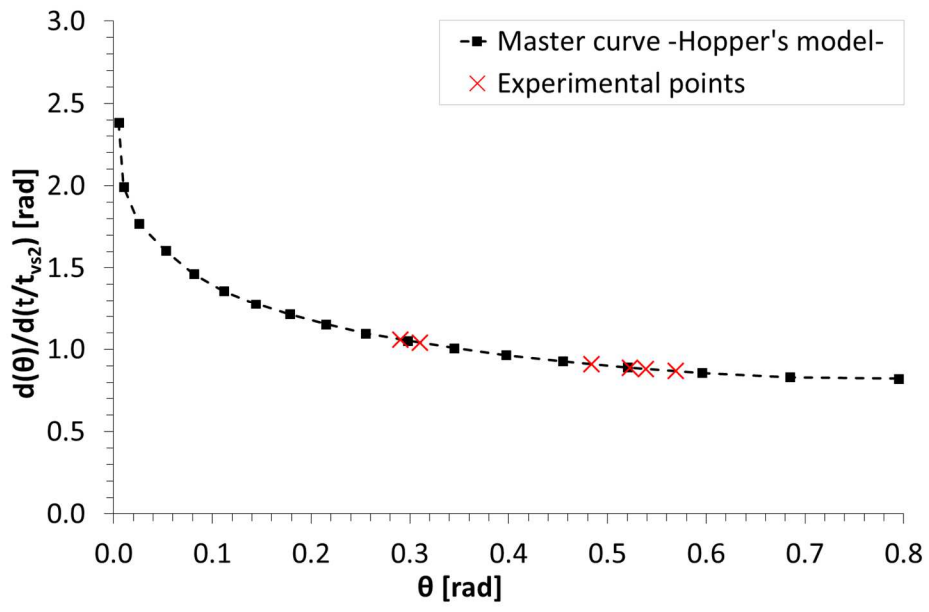
a-



b-



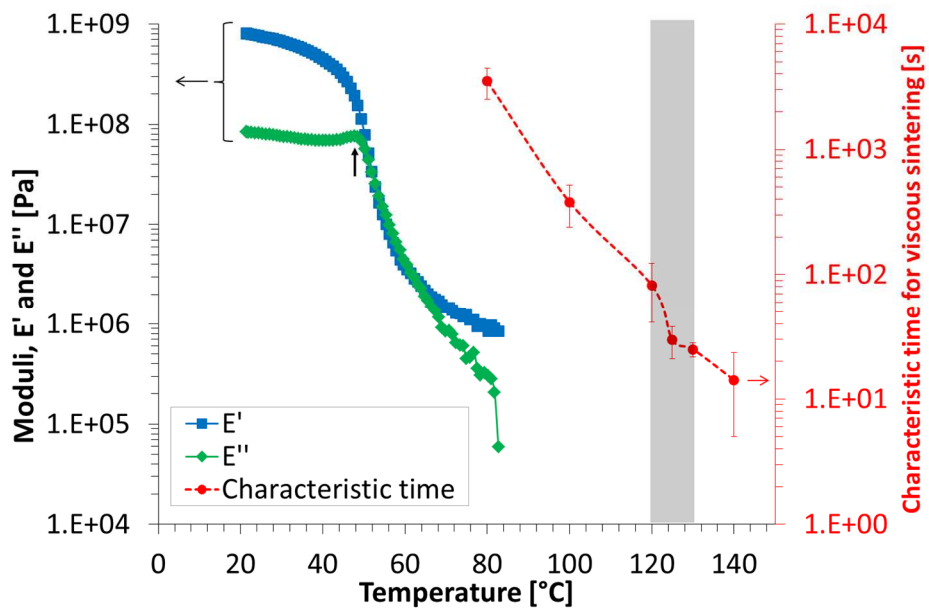
391



392

393 **Figure 6.** Chaunier *et al.*

394



395

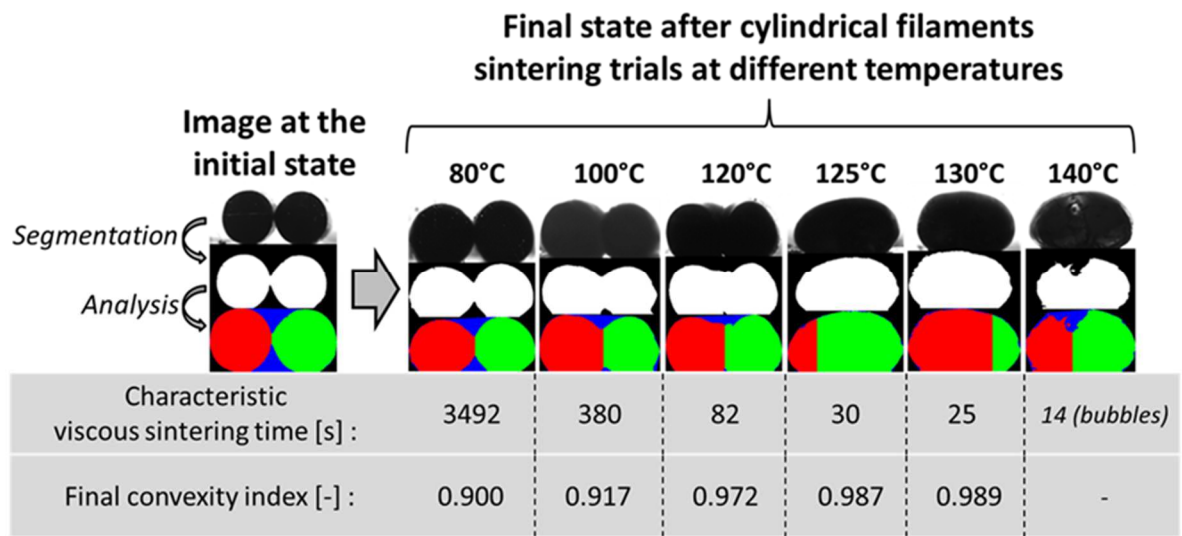
396 **Figure 7.** Chaunier *et al.*

397 **Table 1.** Fusion bonding properties of zein-based extruded filaments (average value \pm
398 standard deviation, for three replicates at each temperature set): Final bonding angle, final
399 convexity index, measured values of bonding angle and bonding rate at 35s and estimated
400 characteristic times for viscous sintering, t_{vs1} (issued from Eq.1; [6]) and t_{vs2} [9].

T_{set} [°C]	Final bonding angle, θ_{final} [rad]	Final convexity index, I_{Convex_final} [-]	θ at $t=35s$ [rad]	$d\theta/dt$ at $t=35s$ [$10^{-4}rad.s^{-1}$]	t_{vs1} (Eq.1) [s]	t_{vs2} (Hopper) [s]	$\frac{t_{vs1}}{t_{vs2}}$ [-]
80	0.39 ± 0.02	0.900 ± 0.011	0.31 ± 0.07	3.0 ± 0.8	5233 ± 1460	3492 ± 974	1.5
100	0.73 ± 0.14	0.917 ± 0.025	0.29 ± 0.03	28 ± 10.4	599 ± 222	380 ± 141	1.6
120	1.10 ± 0.10	0.972 ± 0.001	0.54 ± 0.21	108 ± 53.5	77 ± 38	82 ± 41	0.9
125	1.19 ± 0.05	0.987 ± 0.001	0.57 ± 0.05	294 ± 84.9	27 ± 8	30 ± 9	0.9
130	1.27 ± 0.01	0.989 ± 0.003	0.48 ± 0.04	364 ± 46.2	26 ± 3	25 ± 3	1.0
140	$1.33 \pm 0.27^*$	-	0.52 ± 0.11	625 ± 404.6	14 ± 9	14 ± 9	1.0

401 **High values of standard deviation at the completion of coalescence for $T_{set}=140^{\circ}C$ are due to the vaporization*
402 *of the plasticizer creating bubbles and leading to the expansion of the material*

1 **Graphical abstract**



2

3 Chaunier *et al.*