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1 **Electrochemical chloride extraction to repair combined carbonated and**
2 **chloride contaminated reinforced concrete**

3

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22

23 **Abstract**

24

25 The increasing international interest in contemporary architecture has drawn attention
26 to the numerous listed buildings made of reinforced concrete in Europe, and
27 especially in France. The main source of deterioration of this cultural heritage is the
28 corrosion of rebars through carbonation or chloride contamination, but also often by a
29 combination of both. The present study explored this combined corrosion mechanism
30 in reinforced concretes, and investigated Electrochemical Chloride Extraction (ECE)
31 as a technique to stop or decrease corrosion. The analytical approach was based on
32 physico-chemistry, electrochemical measurements, Raman spectroscopy and SEM
33 examinations. The results evidenced the aggressiveness of the combined
34 carbonation and chloride-induced corrosion, and demonstrated the efficiency of the
35 ECE treatment in terms of chloride extraction and reduction of corrosion rate. It
36 appears that ECE treatment only reduces corrosion activity by increasing pH to a
37 value of 10. Nevertheless, the long term durability of the treatment is questionable as
38 the return to a sound concrete passivity is not obtained.

39

40 **Keywords**

41 Electrochemical chloride extraction; reinforced concrete; carbonation; Raman micro-
42 spectroscopy

43

44 1 Introduction

45 Concrete is now part of the world cultural heritage landscape, as evidenced by the
46 recent Unesco listing of the famous German Bauhaus architecture, the Polish
47 Centennial Hall in Warsaw and the center of the French city Le Havre (rebuilt by
48 Auguste Perret) for their outstanding universal value [1].

49 The Redmonest European Project revealed that at least 1500 buildings made of
50 concrete are now registered in Belgium, France, and Spain. The survey performed
51 within the project shows that the protection of this contemporary heritage is
52 exponential in France, where the number of listed concrete monuments increased
53 from 200 in the 1990's to more than 800 in the 2010's [2, 3].

54 This architectural heritage is unfortunately affected by several types of deterioration,
55 the most deleterious of which is certainly rebars corrosion. Several phenomena are
56 involved in this process. The oldest of these historic concretes were cast at a time
57 when mix design or casting were still a new and developing technology, meaning that
58 poor initial concrete quality or insufficient concrete covers can sometimes be
59 encountered. It is usual to measure carbonation depth of several centimeters in
60 concrete made in the 1920s or 1940s, with open porosity of up to 20% [4, 5]. When
61 those carbonated concretes are subjected to marine chlorides or to de-icing salts, the
62 double contamination can contribute to severe corrosion. In historic concrete, this
63 leads to a massive and unacceptable loss of original materials.

64 The standard technique to cure this deterioration is patch repair. However, the 2007
65 CONREPNET European project showed that patches for repairing reinforced
66 concrete corrosion were not efficient over time [6]. Among the reasons for this lack of
67 durability, the compatibility of the patch materials with the parent historic concrete

68 was the main reason for early failure (within 2 years). The authors suggest that
69 longer term failure could be attributed to the location of the repair patch, which only
70 concerns the spall area and not the surrounding concrete, which is still carbonated or
71 chloride polluted. There was therefore a need for additional treatments to address
72 degradations induced by corrosion. Electrochemical realkalization and chloride
73 extraction were studied for this purpose [7-11].

74 Corrosion has been extensively studied in chloride-polluted concrete [12-22] or in
75 carbonated reinforced concrete [23, 24], but the combined effect of the two
76 contaminants has rarely been investigated.

77 The primary aim of the present study was to investigate the corrosion mechanism
78 resulting from combined carbonation and chloride contaminations. This issue was
79 explored using artificially carbonated concrete with either endogenous (chloride
80 added to the mix) or exogenous (wet and dry cycles) chlorides.

81 In a second step, an electrochemical chloride extraction was studied. Chloride
82 content, pH evolution, and corrosion rates were characterized. Special attention was
83 paid to the evolution of corrosion products during treatment using an analytical
84 approach that combined Raman micro-spectroscopy and SEM observations.

85 **2 Materials and methods**

86 **2.1 Samples and ageing procedures**

87 The reinforced micro-concrete samples were cylinders (10 cm high and 4 cm
88 diameter) with a central rebar. Two cements were studied, namely an ordinary
89 Portland cement (CEM I) and a blast furnace slag cement (CEM III/A). These two
90 cements are of interest: the former was widely used for many years, and the latter
91 was extensively used between the two world wars and its use is currently increasing.

92 Rebar was composed of smooth carbon steel with a diameter of 5 mm and an active
93 surface of 10cm² delimited with cathaphoretic paint (Fig. SI1-1). A rather high
94 water/cement ratio (0.65) was used for concrete formulation to obtain high porosity
95 and thus accelerate the ingress of contaminants (carbonation and chloride ions). This
96 high water/cement ratio is representative of the ratio used in historic concretes.

97 Four sample series were prepared based on two criteria, namely:

98 - Contamination content, i.e. either chlorides added to the mix and followed by
99 carbonation (referenced G), or carbonation followed by wetting/drying cycles in
100 a salted solution (referenced I), and

101 - Cement type (CEM I or CEM III/A, respectively referenced 1 and 3).

102 Therefore, four series named G1, G3, I1, and I3 were studied

103 A precise description of the sample production and contamination can be found in
104 Supplementary Information 1.

105 2.2 Electrochemical chloride extraction

106 The electrochemical chloride extraction (ECE) treatment is illustrated in Figure 1.
107 ECE was conducted on 37 specimens of each sample series. A cathodic current
108 density of -100 $\mu\text{A}/\text{cm}^2$ of steel was applied with a power supply between the rebar
109 and a titanium/platinum grid (counter-electrode) for 8 weeks, corresponding to a total
110 charge of 1344 A.h/m². These current density and duration conditions are in
111 accordance with those reported in the technical specification or standards for chloride
112 extraction [25] and realkalization [26]. A disodium tetraborate solution (25g/L of
113 Na₂B₄O₇ · 10H₂O) electrolyte was used as a 9 pH buffer corresponding to a
114 carbonated concrete. Moreover, some samples were immersed in the electrolyte then

115 studied to evaluate the lixiviation of chloride ions without current (no polarization).
116 Three samples from each series were analyzed after 3, 7, 14, 28, and 56 days of
117 treatment: two were dedicated to destructive analysis and the third was used for non-
118 destructive electrochemical characterizations.

119 2.3 Analytical techniques

120 2.3.1 Phenolphthalein test

121 Phenolphthalein (0.5 % in ethanol) was used to determine realkalization progress
122 during the treatment. A pink color is obtained for a pH of 9 or more, whereas the
123 concrete remains colorless for lower pH values.

124 2.3.2 Chloride titration

125 Regarding the chloride extraction evolution, the free and total chloride contents of
126 concrete were measured by AgNO_3 potentiometric titration [27-28] on the first
127 centimeter around the rebar on two of the three samples. The free and total chloride
128 contents of concrete were simultaneously determined on the non-polarized samples
129 after 14, 28 and 56 days.

130 2.3.3 Electrochemical characterizations

131 Electrochemical characterizations were conducted at each step of the set-up: after
132 curing, after ageing (chloride or carbonation or reverse) and during ECE treatment
133 (depending on the treatment duration). Linear polarization resistance (LPR) and
134 electrical concrete resistance R_e were measured using a 5-channel Bio-Logic
135 VMP2Z potentiostat (details in SI2). Corrosion rate i_{corr} ($\mu\text{A}/\text{cm}^2$ of steel) was
136 calculated according to the Stern-Geary equation (Eq.1)

$$137 \quad i_{\text{corr}} = B/(R_p.S) \quad (\text{Eq. 1})$$

138 Where [29]: $B = 26 \text{ mV}$, R_p (ohm) is obtained from the linear polarization resistance
139 and the electrical concrete resistance (R_e), and S is the active steel surface (10 cm^2
140 in this study).

141 2.3.4 Raman micro-spectroscopy

142 The Raman spectrometer equipment was a HORIBA Jobin Yvon LABRAM consisting
143 of an Olympus BX40 microscope confocally coupled to a 300 mm focal length
144 spectrograph. The latter was equipped with a holographic grating (1800 grooves/mm)
145 and a Peltier-cooled CCD detector (1024×256 pixels). The spectra were obtained
146 with 632.817nm radiation from an internal 10mW HeNe laser with neutral density
147 filters and 0.7mW attaining the surface of the sample to avoid any thermal effect. For
148 *in situ* studies, a 50× ULWD (Ultra-Long Working Distance) allows the recording of
149 Raman spectra with a working distance of 8 mm.

150 Electrodes for *in situ* Raman spectroscopy were specially designed for this study. As
151 shown in Figures SI1-2, Raman spectroscopy samples were cut from double-
152 contaminated concrete samples. A glass window was glued on top of the freshly
153 polished sample shortly before the experiment, as represented in Figure 2. The
154 electrode was immersed window-up in disodium tetraborate solution with 5mm left
155 outside the electrolyte to ensure that the steel was polarized in a pore solution that
156 had to cross 17.5 mm of concrete and had no direct contact with the atmosphere.
157 Spectra were recorded solely at the rebar concrete interface. Spectra during
158 corrosion initiation were obtained at open circuit potential. Treatment was then
159 applied with an Autolab galvanostat using the same current density ($-100 \mu\text{A}/\text{cm}^2$) as
160 previously described. Spectra were then recorded for each sample subjected to
161 cathodic polarization.

162 3 Results and discussion

163 3.1 Initial characterizations

164 Table 1 shows the characterizations of chloride content, pH, and corrosion rate
165 before treatment.

166 Levels of chloride content in the samples were sufficiently high compared to critical
167 content to induce corrosion [30] and was found to be within the range of chloride
168 threshold provided in states of the art [12, 13].

169 The pH value of the 17.5 mm concrete cover was close to 9 (phenolphthalein was
170 colorless) demonstrating the complete carbonation of the concrete samples [31-33].

171 Corrosion rates indicated a passive state for sound concrete. However, corrosion
172 current in the carbonated and chloride-contaminated samples was close to 10
173 $\mu\text{A}/\text{cm}^2$ for all four series, and corresponded to a high level of corrosion in reinforced
174 concrete [29]. This value was higher than those observed in samples with a single
175 contaminant, and highlighted the aggressiveness of the combined contamination
176 (Table 1).

177 3.2 Chloride extraction

178 During the ECE treatment, the negatively charged chloride ions migrated from the
179 rebar to the electrolyte. The efficiency of the electrochemical chloride extraction
180 treatment was considered to be the ratio of the initial chloride content minus the
181 remaining chloride content (after each duration time) divided by the initial chloride
182 content. Figure 3 presents the results of the chloride extraction efficiency versus
183 treatment duration for the I1 series and for the corresponding non-polarized samples.
184 Chloride ions were in a free form because carbonation induced a release of bonded
185 chlorides (as evidenced by the free and total chlorides content values, which are

186 similar in Figure 3). As the four series all showed the same behavior, the results of
187 the three other series can be found in Figure SI3.

188 For the treated samples, an increase of extracted chloride content with increased
189 treatment duration was observed for the four series. Moreover, the extraction was
190 found to be more efficient during the initial stage of the treatment, as previously
191 described by different authors [34-36]. After 28 days, the efficiency of the extraction
192 was close to 90% for G1, G3 and I1 and was close to 75% for I3 samples (Figure 3
193 and Figure SI3-1). These high extraction efficiencies can be explained by a porous
194 and thin concrete cover, and by chloride ions that are likely in the free form. The
195 extraction of chloride ions was also observed for the non-polarized samples, but was
196 attributed to a lixiviation phenomenon.

197 Chloride extraction resulting from the electrochemical treatment was faster than the
198 lixiviation phenomenon (similar values were obtained only after 56 days).

199 In an *in situ* situation involving better quality concrete with better quality (thicker
200 and/or less porous), ECE treatment would require a longer duration. In this case, the
201 end of the treatment correspond to the attaining of a chloride content target, for
202 example.

203 3.3 pH evolution

204 During treatment, water hydrolysis leads to hydroxyl ion formation. An increase of
205 concrete pH around the rebar is therefore expected. Figure 4a presents the results of
206 the pH evolution (pink ring thickness) versus treatment duration for the four series.
207 Figures 4b and 4c show pictures of the phenolphthalein color after 28 and 56 days for
208 I1 series. The thickness of the realkalized concrete around the rebar increased with
209 time. According to [26], the treatment is efficient if the realkalized concrete around the

210 rebar is equal to the diameter of the rebar if the latter measures less than one
211 centimeter in diameter, or 1 cm for larger rebar diameters. The results shown in
212 Figure 4a demonstrate that the realkalization was efficient after 14 days for all four
213 series: the ring thickness was larger than the 5 mm rebar diameter. After 56 days of
214 treatment, it was equal to 9, 10, 12 and 14 mm respectively for G3, G1, I1, and I3
215 series., As expected, no realkalized ring was observed for the non-polarized
216 samples.

217 3.4 *In situ* Raman micro spectroscopy

218 Before treatment, an induction time of 12 hours to 5 days was compulsory to obtain
219 active corrosion around the rebar after immersion in tetraborate solution. Control of
220 the corrosion current gave the same order of magnitude (10 to 50 $\mu\text{A}/\text{cm}^2$) as those
221 observed in previously described samples. The higher values were attributed to the
222 rebar cross section that was also exposed to the pore solution.

223 Raman spectra obtained at this stage are reported on Figure 5a and 5c with
224 reference Raman spectra of Green Rust (GR) grown respectively in chloride (Figure
225 5b) or carbonate (Figure 5d) solution according to the protocols described in SI1-2.
226 The four series tested mainly showed spectrum 5a, while some spots on G1 samples
227 indicated spectrum 5c.

228 The main differences between the two types of Green Rust spectra are the gap and
229 the position between the two main bands, which are respectively 70 cm^{-1} [500-430]
230 for $\text{GR}(\text{Cl}^-)$ and 75 cm^{-1} [510-435] for $\text{GR}(\text{HCO}_3^-)$, and the presence of two smaller
231 bands at 320 and 360 cm^{-1} for $\text{GR}(\text{Cl}^-)$. Clearly spectrum a) is linked to $\text{GR}(\text{Cl}^-)$;
232 while spectrum 5c is attributed to $\text{GR}(\text{CO}_3^{2-})$.

233 The presence of these compounds attests a fast corrosion process in which chloride
234 is incorporated within corrosion products as the anions in Green Rust structure to
235 counterbalance the presence of iron III. GR(Cl⁻) are known to be thermodynamically
236 unfavored compared to carbonate (or sulphate)-based GRs [37]. The localized
237 observation of GR(CO₃²⁻) on G samples shows inhomogeneous distribution of
238 chloride ion concentration in pore solution.

239 The stability of GR spectra over several days also shows that our setup efficiently
240 protects the concrete rebar interface from atmospheric oxidation. This reflects the
241 situation in real concrete, where oxygen penetration is a slow process [38].

242 During treatment, once corrosion was proved to occur by the formation of spots of
243 Green Rust, a cathodic current of -100 $\mu\text{A}/\text{cm}^2$ was added to the system. Raman
244 spectra were periodically recorded during this treatment. The spectra observed
245 during the reduction process are depicted in Figure 6 for I1 sample.

246 After polarization is turned on, the characteristic band of magnetite Fe₃O₄ appears at
247 670 cm^{-1} . With time, a progressive increase is observed in magnetite bands, causing
248 a decrease in Green Rust bands until they almost completely disappear. All the
249 studied series behaved in the same manner, the only differences being the induction
250 time and the growing rate of magnetite, which both varied from one sample to the
251 other (SI 4). However, magnetite was the predominant band for all samples after 24
252 hours of polarization.

253 After longer polarization time (more than one day), new Raman spectra were
254 recorded for a few spots around the rebar. They are depicted in Figure 7a for I1
255 sample and in Figure 7b for G3 sample. Similar behavior was also recorded for I3
256 sample (not shown). No information was obtained for G1 sample after 24 hours due

257 to a high interface fluorescence. Figure 7a presents the evolution of the Green Rust
258 bands, with a rapid decrease in the intensity of the 500 cm^{-1} band compared that of
259 the 430 cm^{-1} band. A shift of the 430 cm^{-1} band towards a lower wavenumber (410
260 cm^{-1}) is also observed. Moreover, after 2 days a new band appears in the 3600 cm^{-1}
261 range (see insert in Figure 7a) corresponding to O-H stretching vibration at 3575
262 cm^{-1} . These values were in accordance with reference [39] and indicated the
263 formation of $\text{Fe}(\text{OH})_2$ in I1 series. In Figure 7b, after 3 days of treatment, two new
264 bands appeared in the Raman spectrum: 205 cm^{-1} and 280 cm^{-1} . They correspond to
265 mackinawite Fe_{1-x}S [40] in G3 series (also observed for I3 series, not shown). The
266 presence of sulfide is due to the blast furnace material contained in cement 3 (CEM
267 III/A) [22].

268
269 *In situ* Raman spectroscopy analysis of the chloride extraction treatment made it
270 possible to collect information on corrosion mechanisms. First, as expected in a
271 medium pH range containing anions such as chloride, carbonate, or sulfate, rebar
272 corrosion takes place through the formation of Green Rust [41]. This iron II
273 hydroxide-based compound contains some iron III ions, and the balanced charge is
274 compensated with anions originating from the solution, mainly chlorides in this case.

275 A progressive transformation of Green Rust into magnetite was evidenced during
276 cathodic polarization, as pH in the pore solution near the rebar increases due to the
277 reduction process. The literature indicates that a pH of around 10-11 is necessary for
278 this transformation to take place [42]. Raman spectroscopy showed this process to
279 be relatively fast compared to the treatment duration, and also evidenced the rapid
280 release of chloride anions inserted in corrosion products.

281 However, the local formation of iron II compounds that can be easily oxidized [39-40,
282 43], (hydroxide in CEM I and sulfide in CEM III/A) during long polarization durations,
283 while GR and magnetite are hardly visible in the Raman spectra, is a clear indication
284 of corrosion that is still active in some spots around the rebar.

285 3.5 Corrosion rate

286 ECE treatment aims to decrease or even stop reinforcement corrosion. Figure 8
287 presents the results of corrosion rates versus treatment duration. These
288 measurements were performed 3 months after the end of the treatment period in
289 order to allow the system to recover a stable state (with the exception of time 0). For
290 the four series, the ECE treatment leads to a decrease of the corrosion rates over
291 time, with two or three orders of magnitude (log scale). From days 14 to 56 of
292 treatment (corresponding to durations after which free chloride content was below
293 0.4%), corrosion rates decreased to values below $0.1 \mu\text{A}/\text{cm}^2$.

294 Corrosion rates remained in the range 1 to $10 \mu\text{A}/\text{cm}^2$ in the non-polarized samples,
295 where chloride ions had been removed by lixiviation but were still carbonated.

296 These results show that chloride extraction and pH increase are both needed to slow
297 down the corrosion of the reinforcement and that realkalization is mandatory.

298 Raman spectroscopy shows that the chloride ions that are bonded to the corrosion
299 products were released at the beginning of the cathodic treatment and were therefore
300 completely extracted. On the lixiviated samples, the chlorides that were bonded to
301 the corrosion products remained at the rebar/concrete interface. They can be
302 released by the oxidation of GR into iron III oxyhydroxides, and can thus cause
303 further corrosion.

304 Nevertheless, corrosion rates for after treatment remained one order of magnitude
305 higher than for the sound concrete for all contaminated samples. The passive state of
306 the rebar in the sound concrete was not therefore recovered in the samples. This was
307 confirmed by the presence of iron II revealed by Raman spectroscopy, indicating that
308 corrosion was still active on some spots.

309 3.6 Durability

310 In a previous study dealing with an impressed current realkalization treatment applied
311 to carbonated reinforced concrete, the pH increased from 9 to 10-11 after treatment
312 (quantitative pH determination from powders in solution), inducing a decrease in the
313 corrosion rates [44, 45]. Although the pH remained constant with time, corrosion
314 rates gradually increased again, and finally reached the corrosion rate values
315 observed for untreated carbonated reinforced concrete 30 months after the end of
316 treatment. This behavior was explained by the fact that the increase in pH was not
317 sufficient, as the sound pH concrete value of 13 was not recovered [45]. Identical
318 cement (CEM I) and mortar composition and similar experimental conditions were
319 used in this previous study and in the present study. Based on this, the hypothesis of
320 similar behavior can be assumed. Moreover, Tlili et al. [46] observed a limit for the pH
321 increase in carbonated solution due to a buffer effect. Figure 9 presents SEM
322 observations of realkalized samples thirty months and five years after treatment.
323 They exhibit a doubling of the corrosion layer thickness (15 to 30 μm) over time (30
324 to 60 months), evidencing a reactivation of corrosion.

325 Therefore, although the electrochemical treatment applied to reinforced concrete with
326 a double contamination seems to be efficient in extracting chlorides and reducing
327 reinforcement corrosion, the long-term efficiency with regard to pH evolution needs to
328 be examined in greater detail.

329 4 Conclusions

330 This study considers rebar corrosion in combined carbonated and chloride
331 contaminated concrete. The aggressiveness of the combined contaminants
332 compared to that of a single one (carbonation or chloride ions) was highlighted by
333 corrosion rate results and the detection of chlorides in Green Rust by *in situ* Raman
334 spectroscopy.

335 Whatever the cement type and the contamination mode, the efficiency of
336 electrochemical chloride extraction treatment was demonstrated by 90% chloride
337 extraction and a decrease of the corrosion rate by three orders of magnitude. An
338 increase of pH up to a value of 10 was also observed. The same amount of chlorides
339 was extracted in ECE-treated samples and non-polarized lixivated samples, but the
340 corrosion rate retained its initial value in the latter. This shows that a pH increase is
341 mandatory to reduce corrosion. At a microscale, this can be related to the
342 transformation of Green Rust into magnetite, as observed by Raman spectroscopy
343 during the treatment. This pH-driven modification released chloride anions that were
344 bonded to the corrosion products.

345 However, the long-term durability of the treatment is uncertain. Corrosion rate
346 decrease and pH increase did not reach the respective sound concrete values. The
347 presence of iron II compounds casts doubt on the passivity of the rebar.

348 This primary aim of this study was to find a restoration solution for historic concretes
349 affected by both carbonation and chloride contamination than can also be used for
350 civil engineering structures. In the latter case, permanent Impressed Current
351 Cathodic Protection (ICCP) can be easily implemented to stabilize the corrosion

352 decrease. The invasiveness and the irreversibility of the ICCP treatment are a
353 challenge in the preservation of historic concretes.

354

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358

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Figure captions

Figure 1: Electrochemical chloride extraction set-up.

Figure 2: Top view of the electrode with glass used for in situ Raman spectroscopy.

Figure 3: Free ■ and total ▲ fraction of extracted chlorides for the internal part during treatment and free □ and total △ fraction of extracted chlorides for the internal part of the non-polarized samples versus treatment duration for I1 series.

Figure 4: Diameter of realkalized concrete around the rebar versus treatment duration for ■ G1, □ I1, ● G3, ○ I3 series (a) and examples of phenolphthalein test for I1 samples ((b) 28 and (c) 56 days).

Figure 5: a), c) In situ Raman spectra of the metal concrete interface after immersion in tetraborate solution; b) reference Raman spectrum of GR(Cl⁻) and d) reference Raman spectrum of GR(CO₃²⁻)

Figure 6: In situ Raman spectra evolution with polarization time, 600s exposure time, a spectrum every 13 minutes, spectra have been offset for sake of clarity. I1 series, tetraborate solution, cathodic current $I = -100 \mu\text{A}/\text{cm}^2$

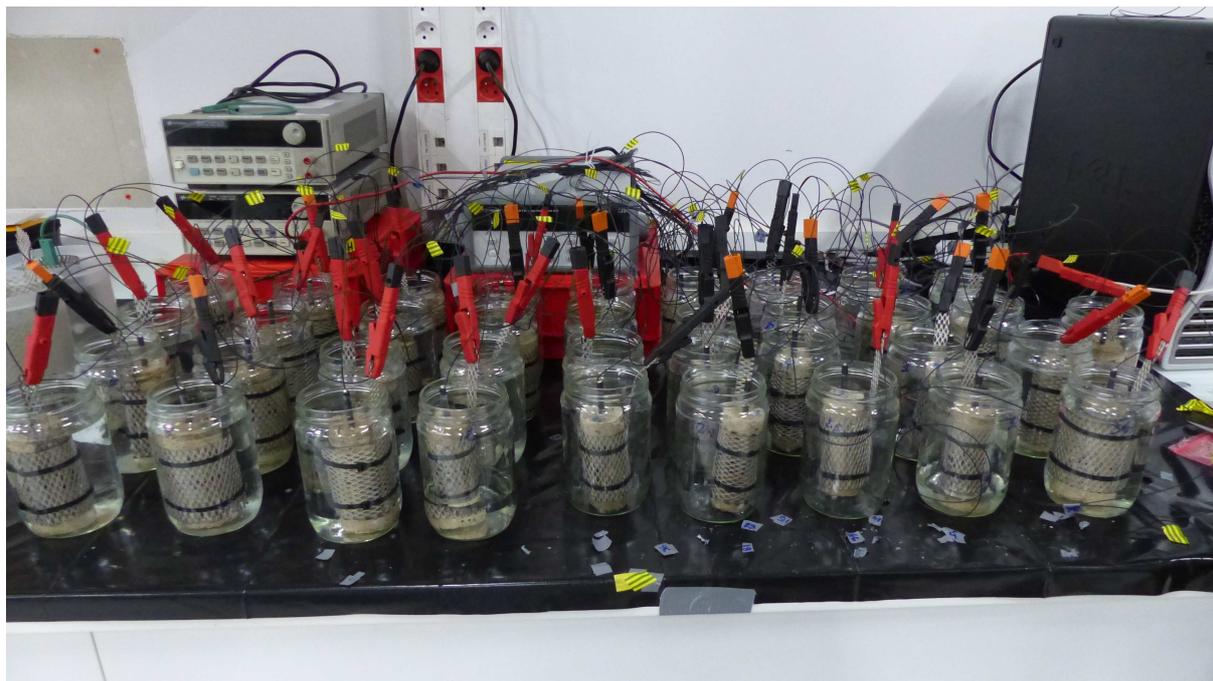
Figure 7: In situ Raman spectra evolution with long polarization time; spectra have been offset for sake of clarity, tetraborate solution, cathodic current $I = -100 \mu\text{A}/\text{cm}^2$, a) I1 series inset: O-H stretching range and b) G3 series

Figure 8: Corrosion current for ●G1, ■G3, ▼I1 ▲I3 series polarized in tetraborate solution and ○G1, □G3, ▽I1 △I3 non polarized sample versus treatment duration.

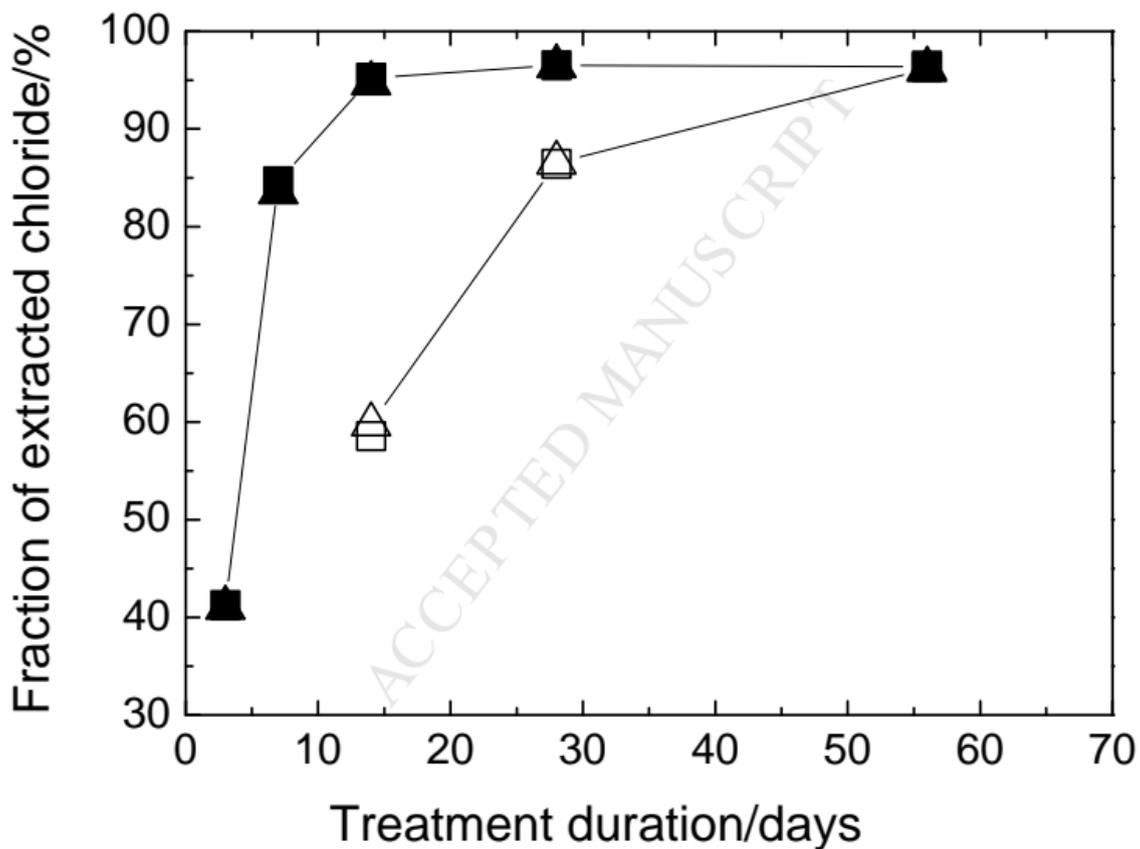
Figure 9: Corrosion products layers after the realkalization treatment a) 30 months after (thickness = 15 μm) and b) 60 months after (thickness = 30 μm). R: rebar, C: concrete

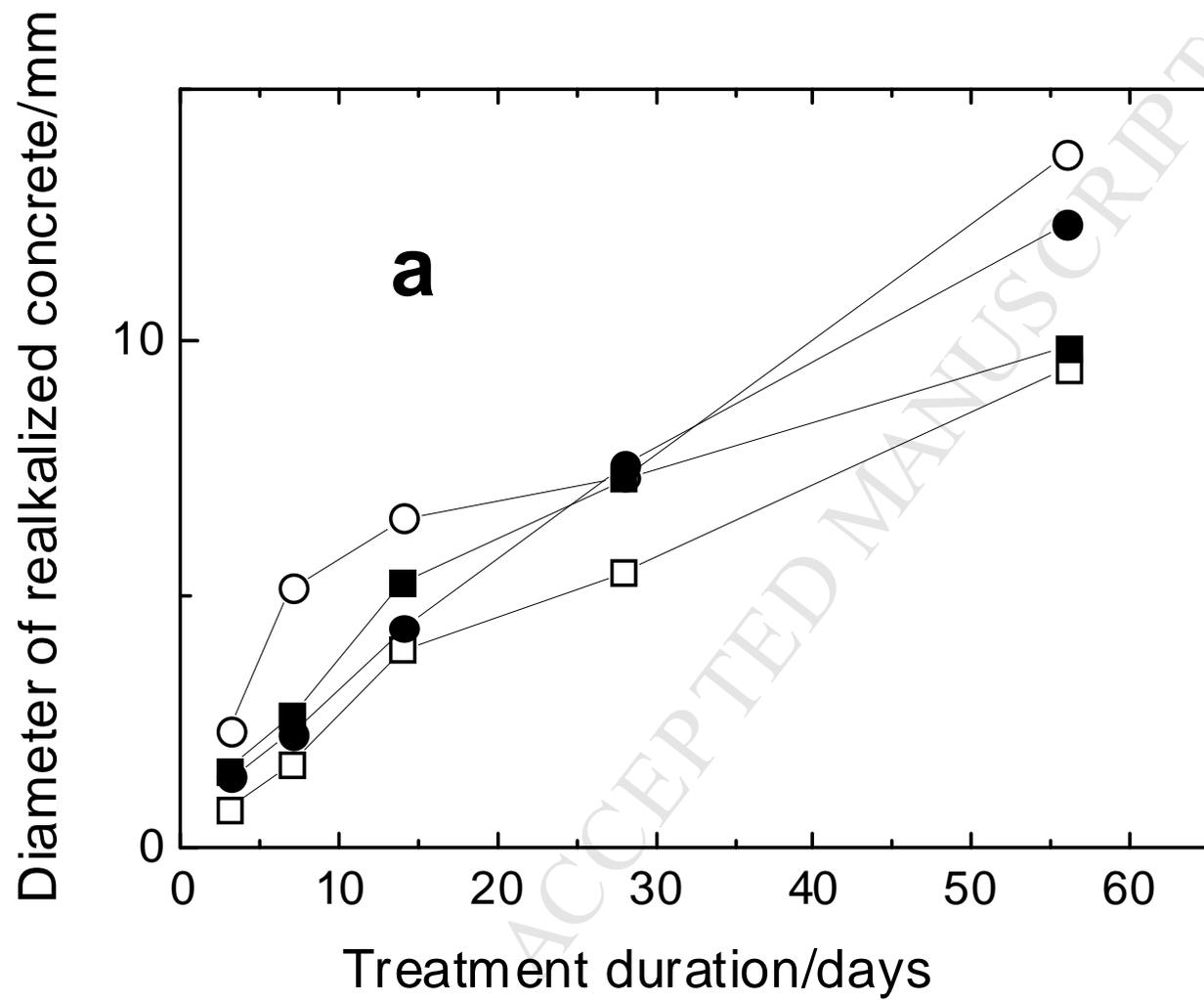
Table 1: Characterizations before treatment: corrosion rate ($\mu\text{A}/\text{cm}^2$), pH value and chloride content (% weight of cement) for the four series.

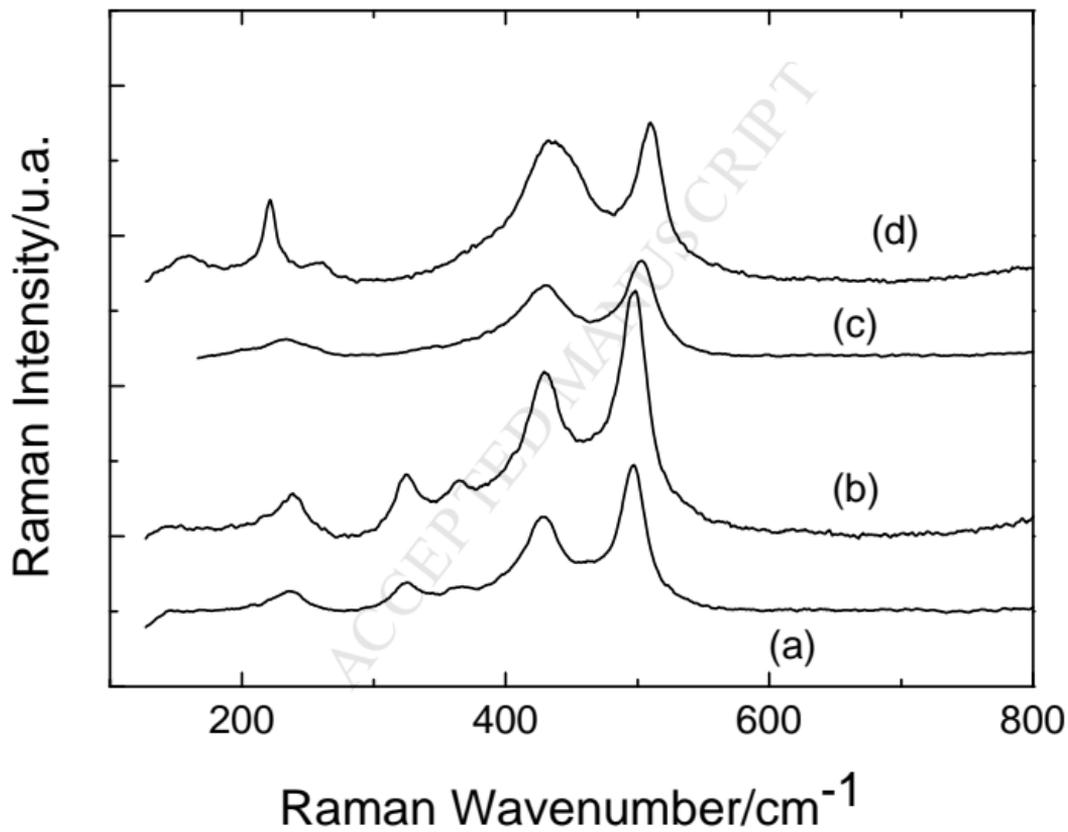
| series | sound concrete | Cl^- contaminated | CO_2 contaminated | $\text{Cl}^- + \text{CO}_2$ contaminated | | |
|--------|---|----------------------------|----------------------------|--|--|-----|
| | $i_{\text{corr}}/\mu\text{A}\cdot\text{cm}^{-2}$ (standard deviation) | | | pH | Free chloride content (% weight of cement) | |
| G1 | 0.00 | 0.02 | | 10.99 (1.82) | 9 | 1.4 |
| I1 | 0.00 | | 2.72 | 9.34 (3.27) | 9 | 0.9 |
| G3 | 0.01 | 0.06 | | 7.82 (1.07) | 9 | 2.1 |
| I3 | 0.01 | | 8.80 | 9.39 (4.87) | 9 | 1.1 |

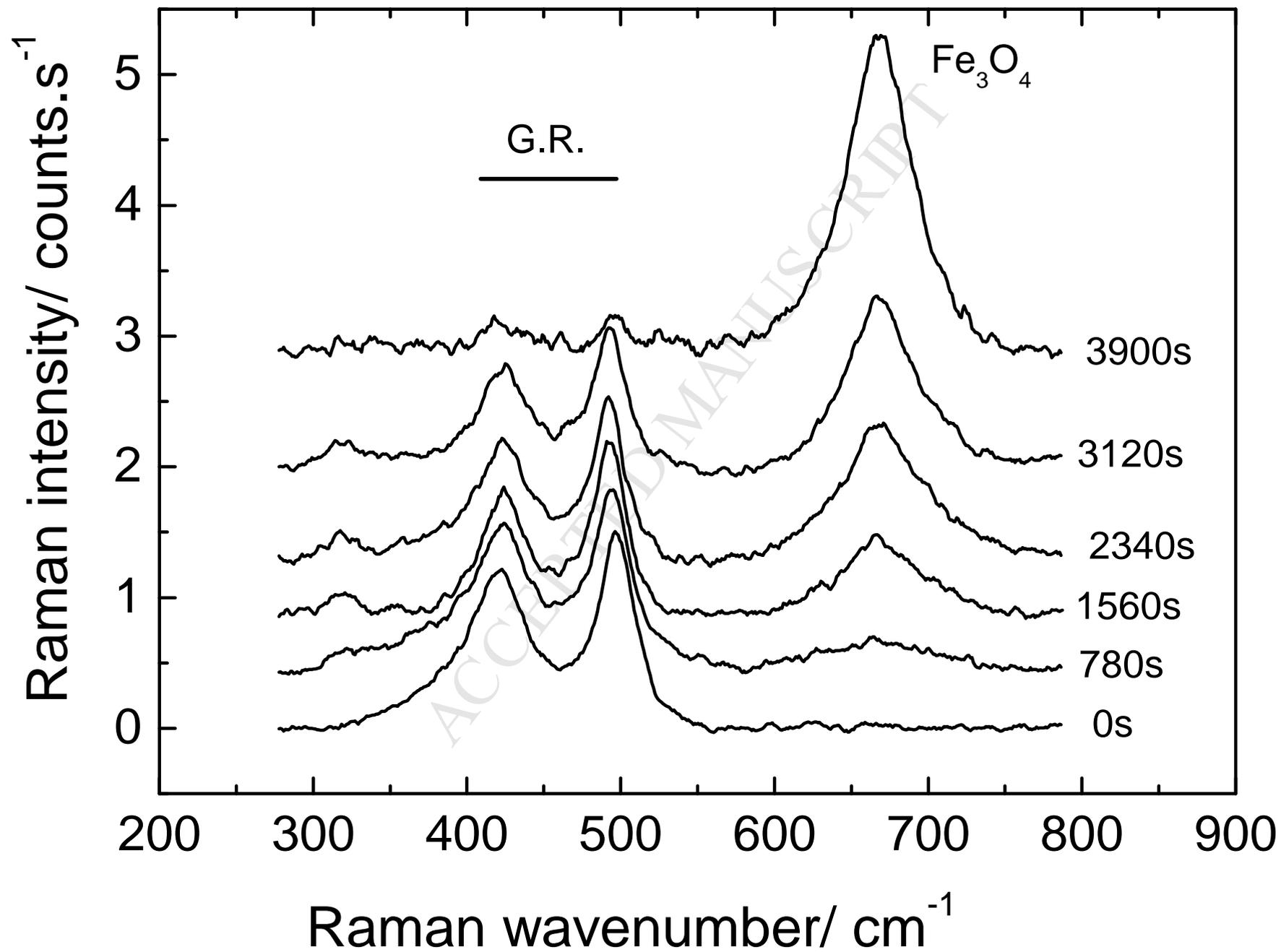


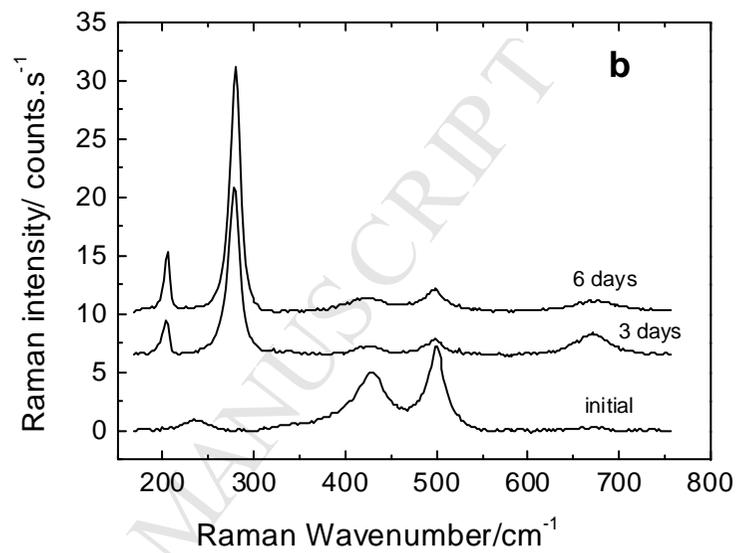
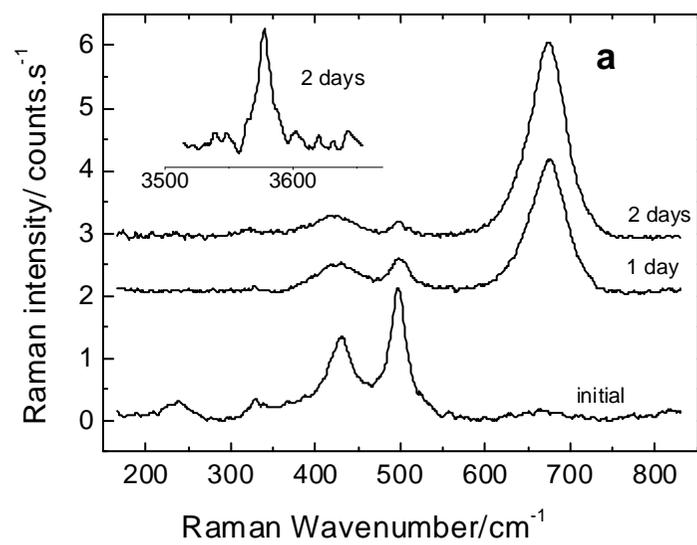


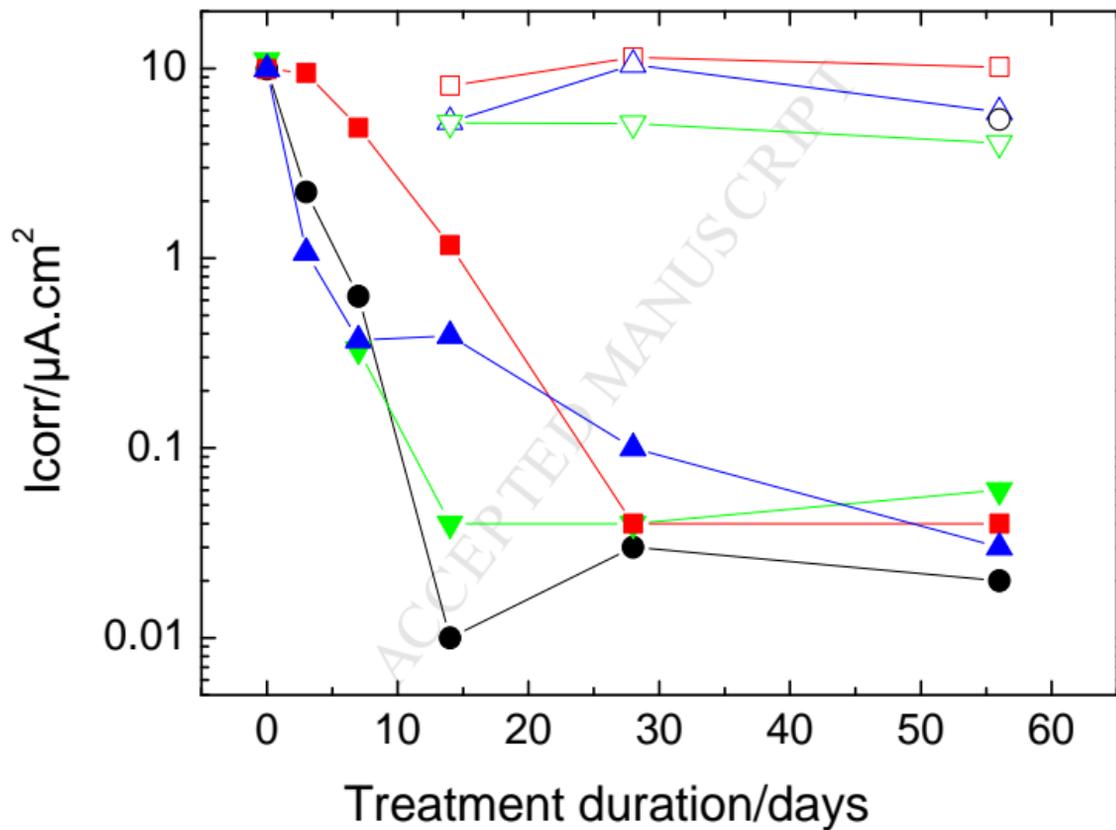


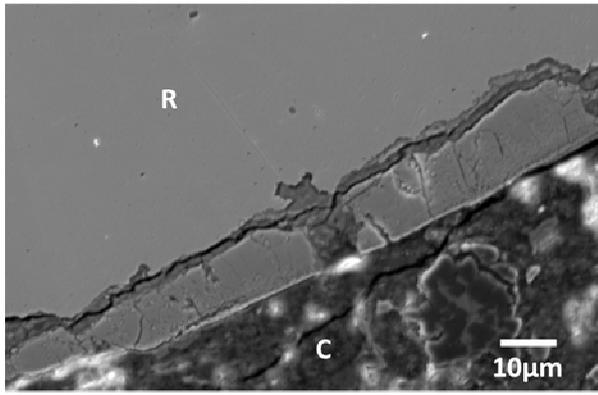




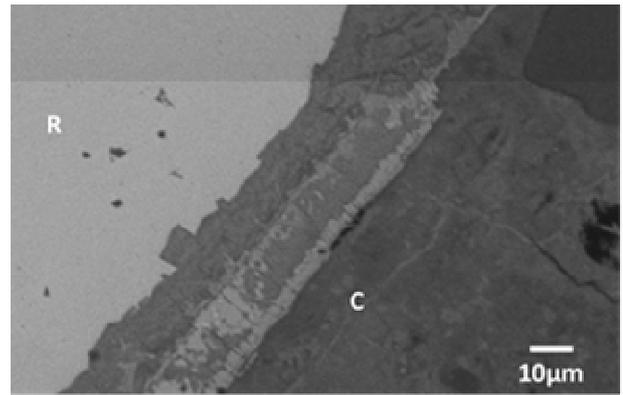








a)



b)

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Highlights

- High corrosion rate show the aggressiveness of combined contamination (Cl^- , CO_2).
- Electrochemical chloride treatment is provisionally efficient.
- Long term durability of ECE is questionable (pH increase is insufficient).